

# Global System Analysis of Interconnected Flow Sheet Models for Drug Product Manufacturing to Performance

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*April 26<sup>th</sup>, 2017*



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# The Motivation for a Systems Based Approach to Pharmaceutical Development

Research

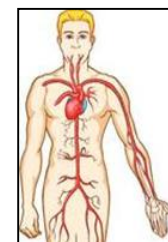
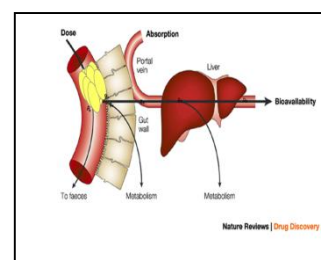
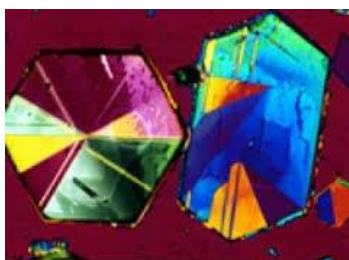
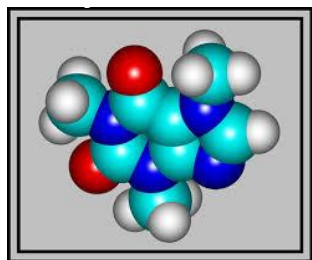
Inventing the right molecule

Development

Creating the right product

Commercialization

Optimizing the operating margin



Advanced multi-scale modeling of all processes

Systems Biology & System Pharmacology

Pharmaceutics

Transforming new chemical entity into medication

Relating properties of drugs and dosage to onset, duration & intensity of action

Biopharmaceutics

Molecular Design

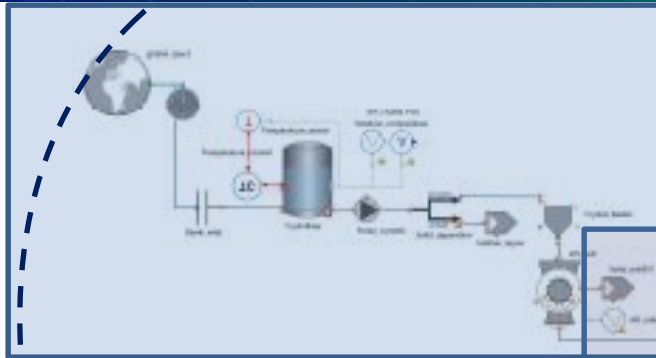
Opportunity to influence molecular design



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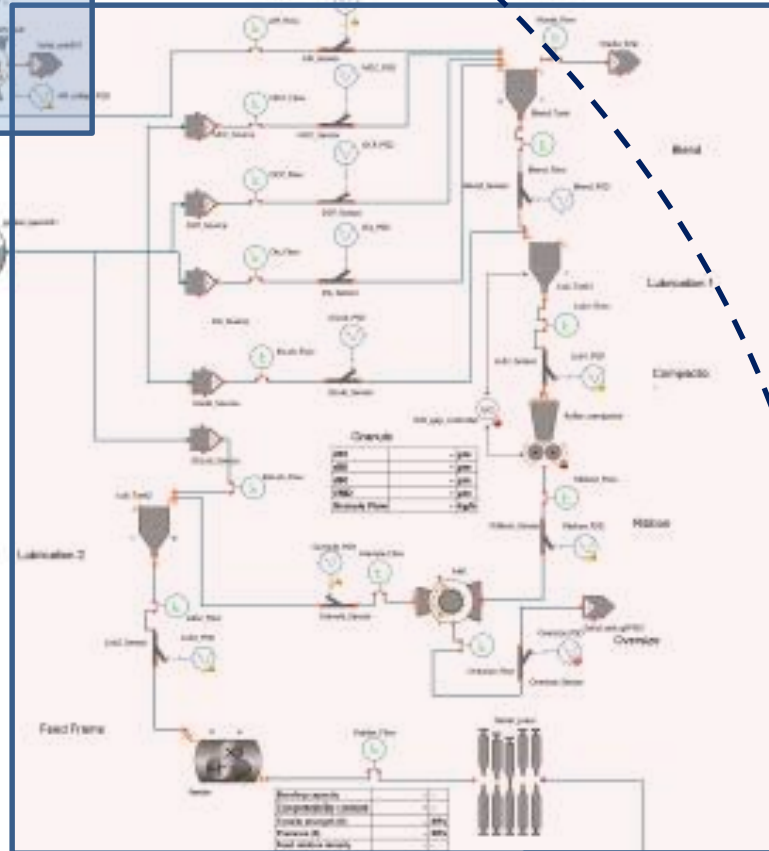
# Long term Vision: Digital Design



**Global System Analysis**

**Early Stage Risk Analysis**

**Optimal Design of product and process**

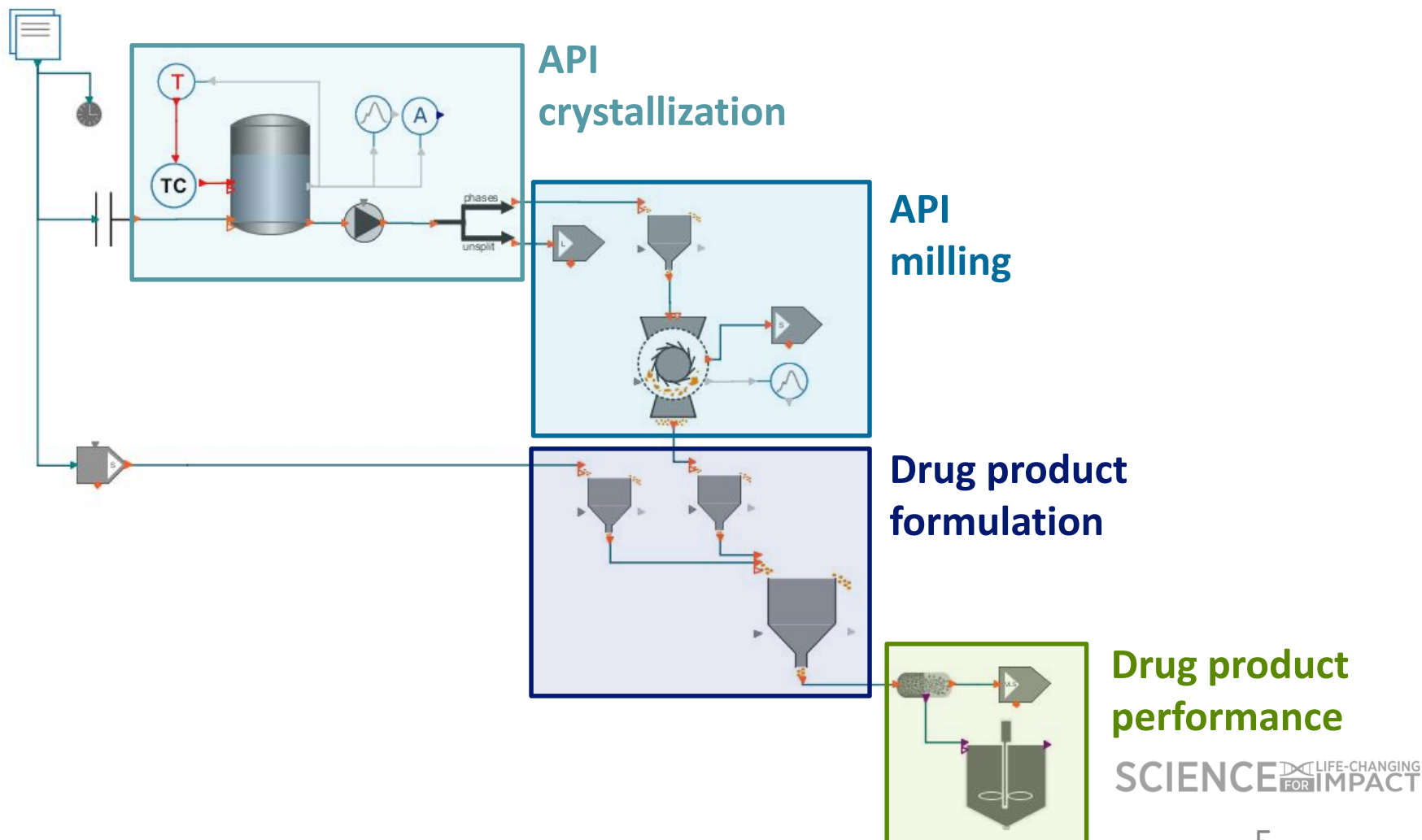
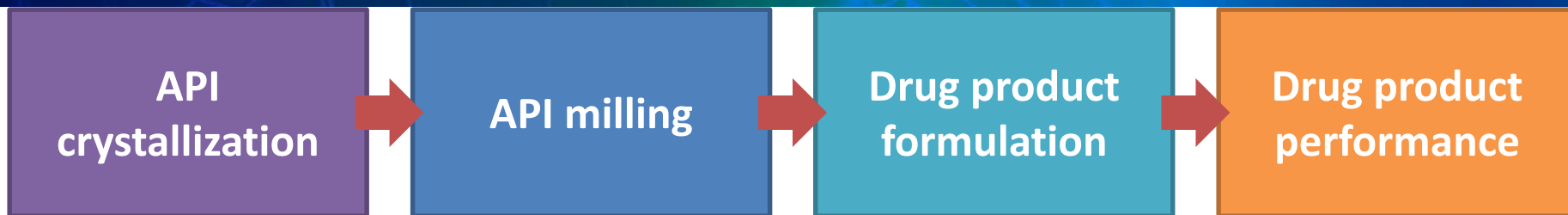


# Organization of the presentation

- Interconnected flowsheet model: Crystallization to Dissolution
  - Batch cooling crystallization model
  - Dry Milling Model
  - In vitro Dissolution Model
- Global System Analysis of individual unit operations
- Global System Analysis of Interconnected flowsheet model
  - First example of GSA applied to complex flowsheet
- Conclusion and Future Direction



# Interconnected flowsheet



Drug product  
performance

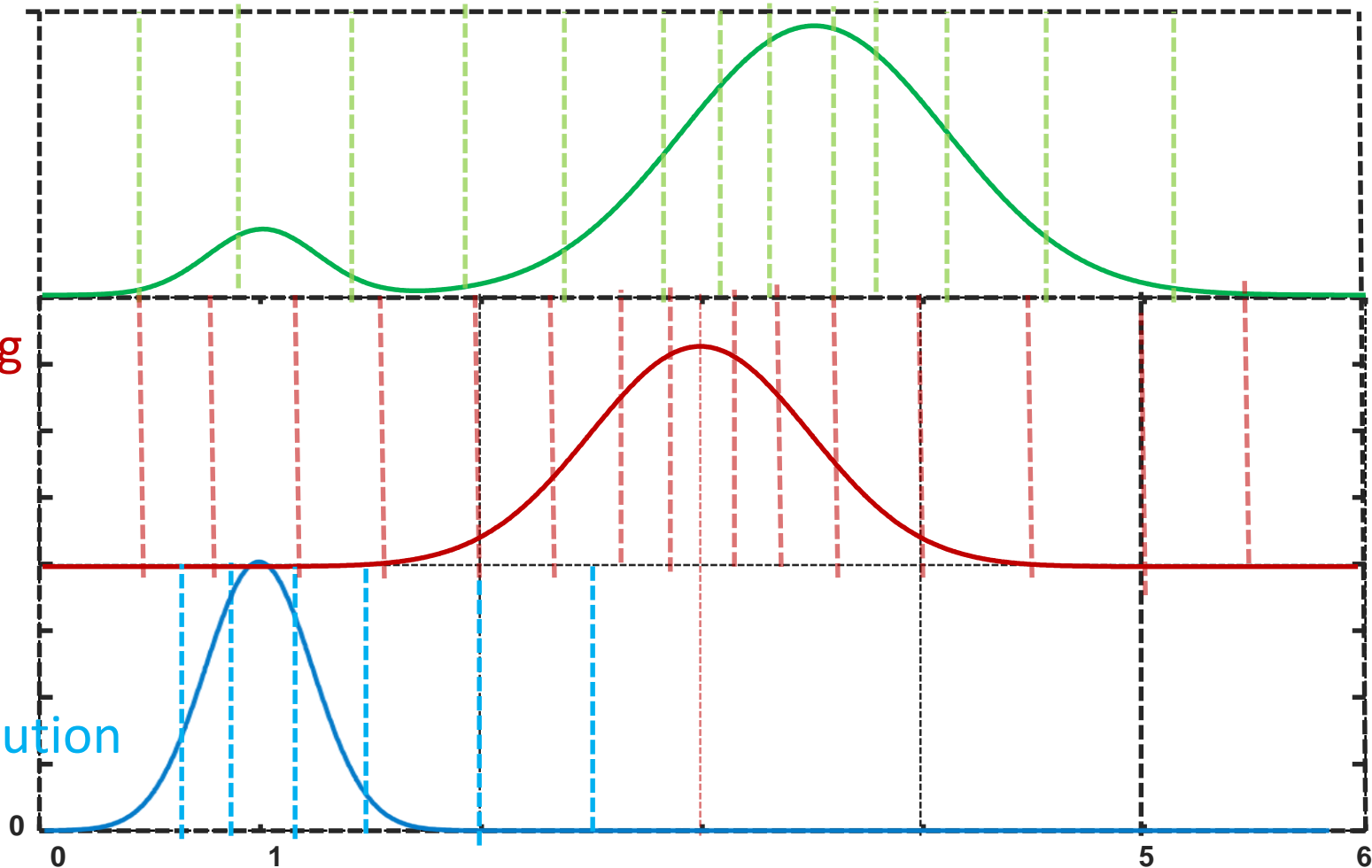
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# Interoperability of different models

Crystallization

Milling

Dissolution



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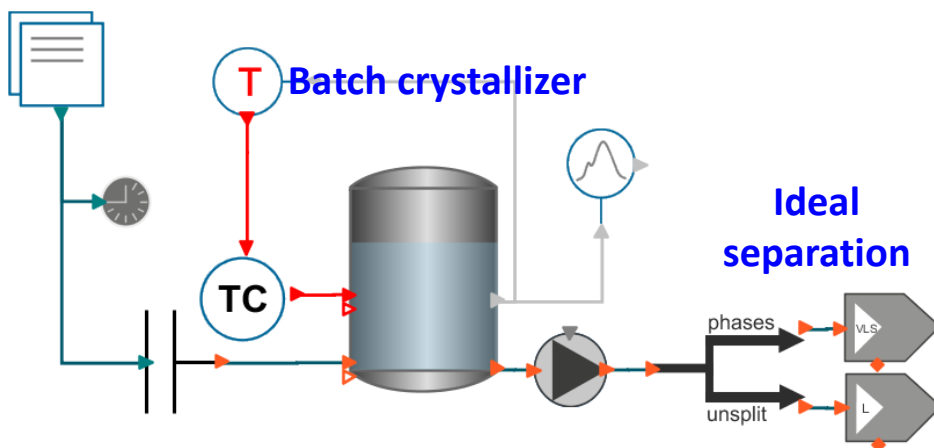
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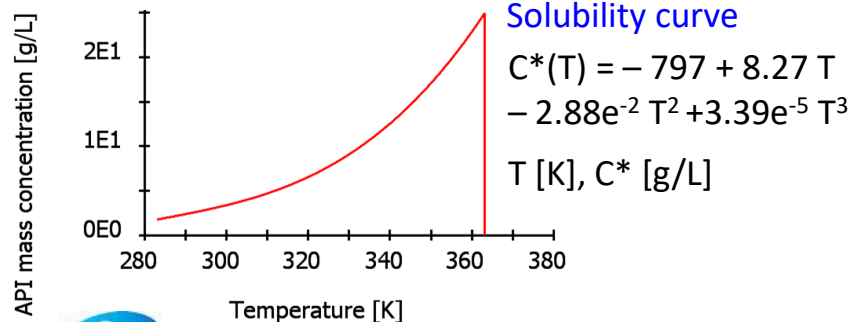


# Crystallization Model

## API crystallization



Growth and dissolution: *Classical two-step kinetics; Garside et al. (1990)*



### Batch recipe:

- 0h - 4h Cooling – piecewise linear ramp for T
  - Initial temperature (60-90°C)
  - Final temperature 10°C
- 4h - 6h Unload – Constant output flowrate

### Input variables:

- Cooling profile: initial temperature (60-90°C)
- Impeller frequency (10-50 rpm)
- API concentration in solution (3-5 %w)
- Initial seed concentration (5-15  $e^{-6}$  g/kg)
- Seed lognormal PSD: peak 15  $\mu$ m; SD 5  $\mu$ m

### Physicochemical parameters:

- Nucleation rate ( $35 \text{ m}^{-3}\text{s}^{-1}$ )
- Growth rate constant ( $5e^{-6} \text{ m/s}$ )
- Growth activation energy ( $1.25e^4 \text{ J/mol}$ )
- API solubility function of T

### Output variables:

- Crystal PSD



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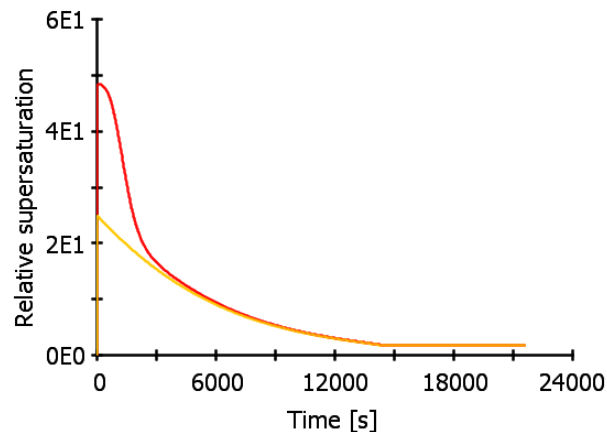
# Results from single Crystallization Simulation

## API crystallization

### Scenario

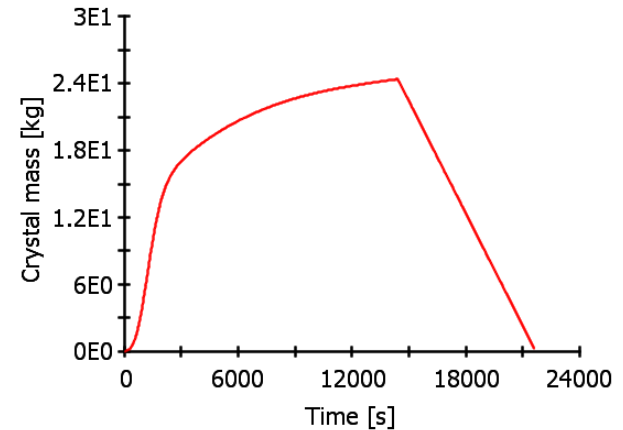
- Cooling profile: initial temperature (90°C)
- Impeller frequency (25 rpm)
- API concentration in solution (5%w)
- Initial seed concentration ( $10 \text{ e}^{-6} \text{ g/kg}$ )

### Solute concentration & solubility

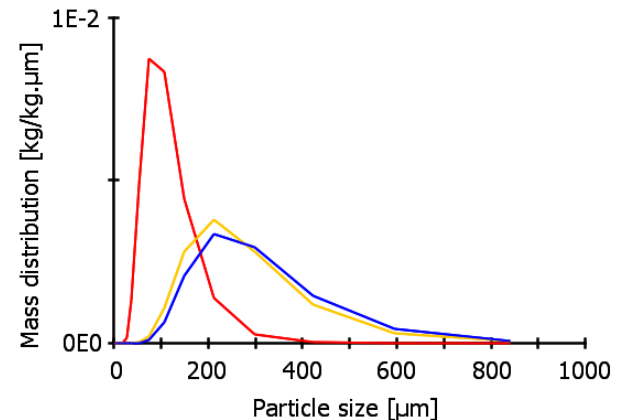


- Mass concentration of solute in solution
- Mass concentration of solute at saturation

### Solution and crystal mass in crystallizer



### Cumulative particle size distribution



- API crystal (10min)
- API crystal (1h)
- API crystal (4h)

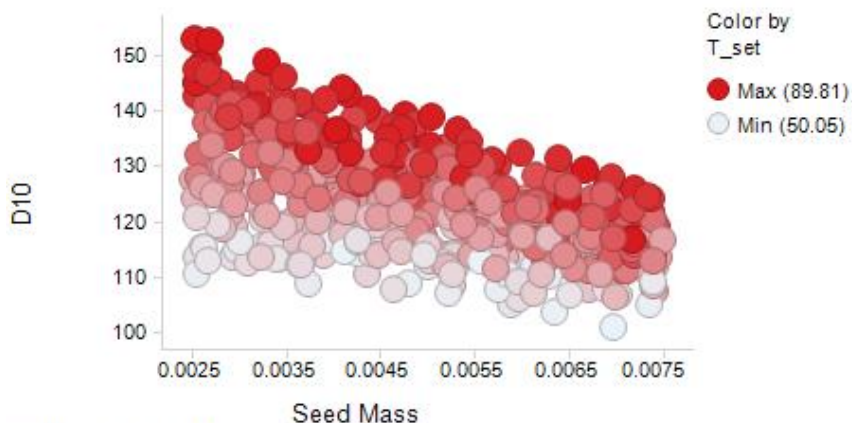


# GSA Algorithm/Methodology

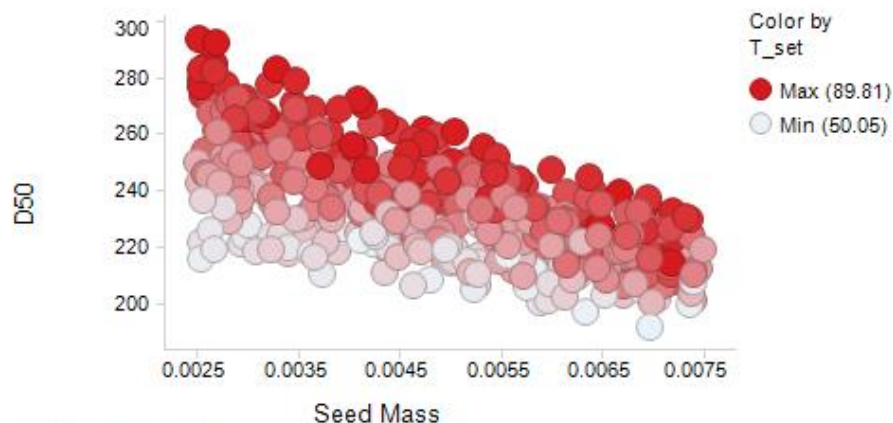
- Define the uncertainty distribution of model parameters and inputs
- Define a Monte Carlo simulations scheme
- Calculate the statistics (mean, variance and distributions) from the model output
- Calculate the Sobol indices using ANOVA decomposition
- Reduce the model keeping only dominant parameters for further analysis

# Effect of initial seed mass on Crystal PSD

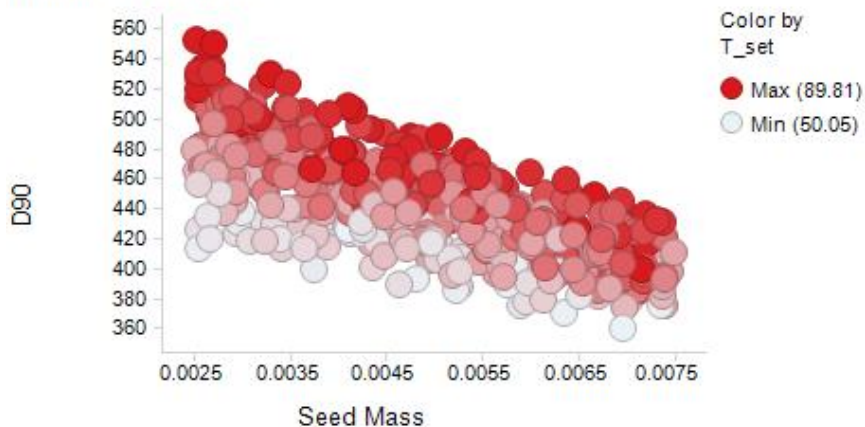
D10 vs. Seed Mass



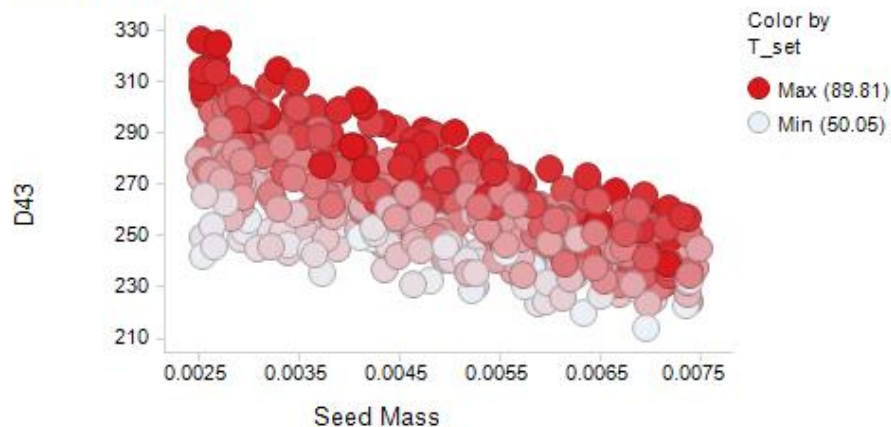
D50 vs. Seed Mass



D90 vs. Seed Mass



D43 vs. Seed Mass



1000 -5000 simulations on 64 core machine

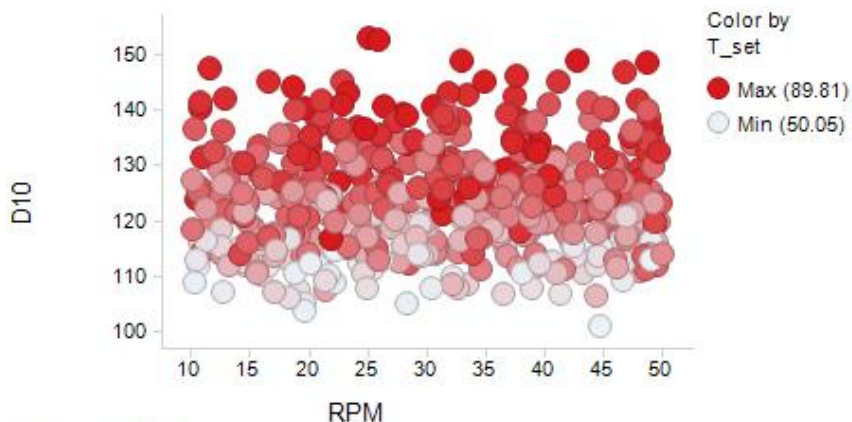


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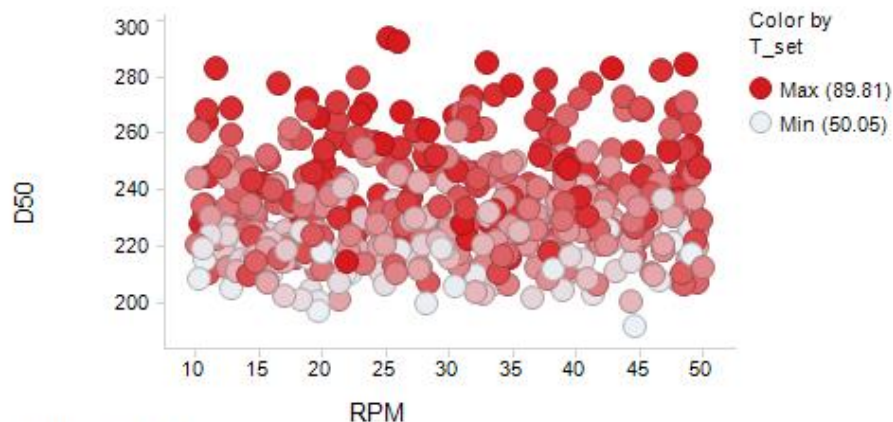
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# Effect of impeller RPM on Crystal PSD

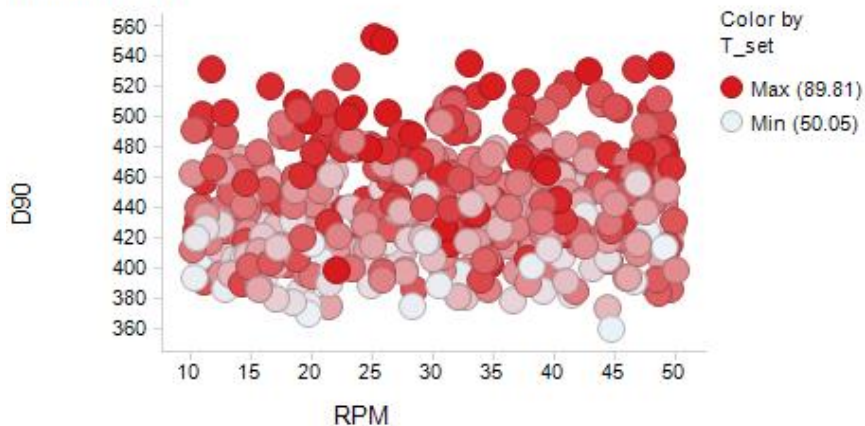
D10 vs. RPM



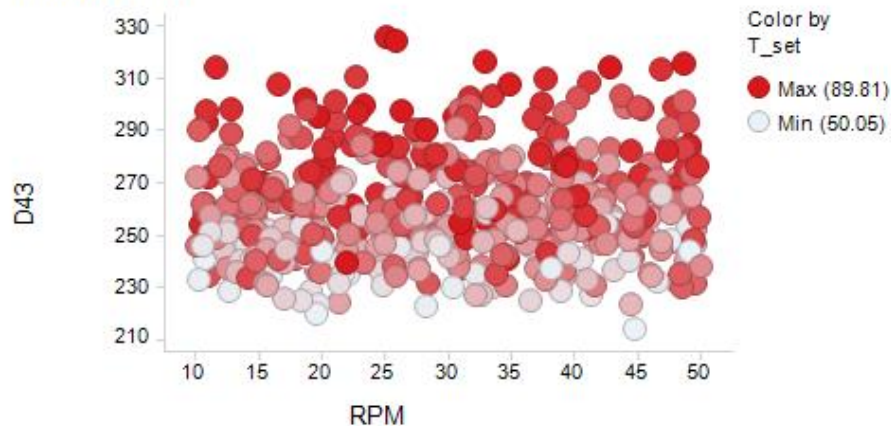
D50 vs. RPM



D90 vs. RPM



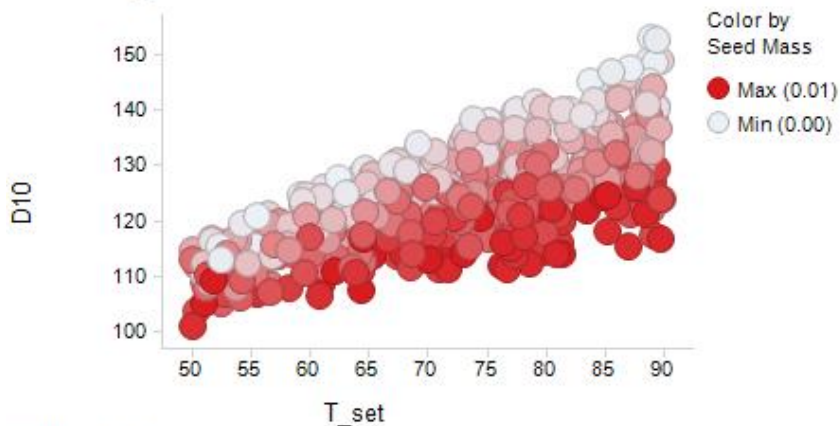
D43 vs. RPM



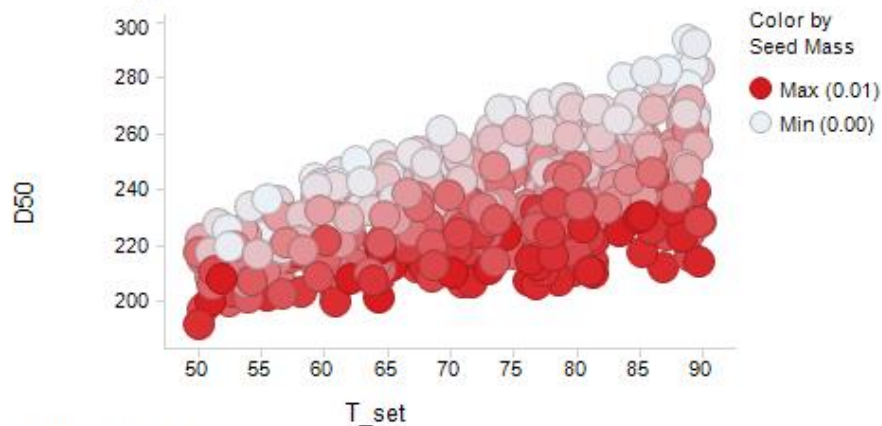


# Effect of Initial Slurry Temperature on Crystal PSD

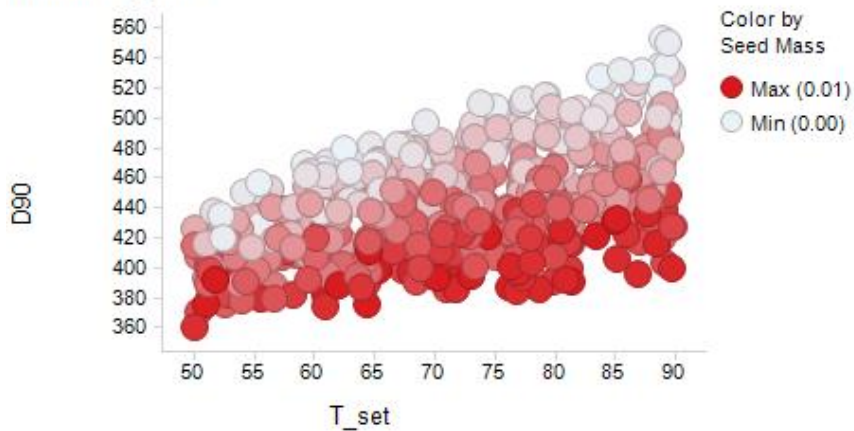
D10 vs. T<sub>set</sub>



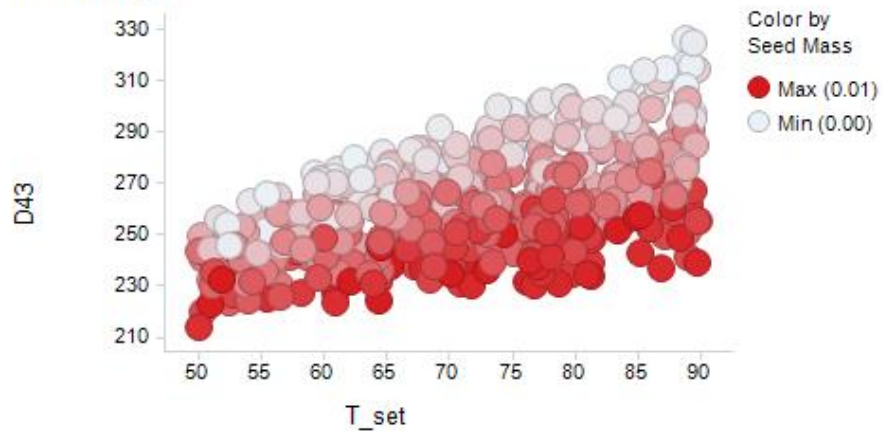
D50 vs. T<sub>set</sub>



D90 vs. T<sub>set</sub>

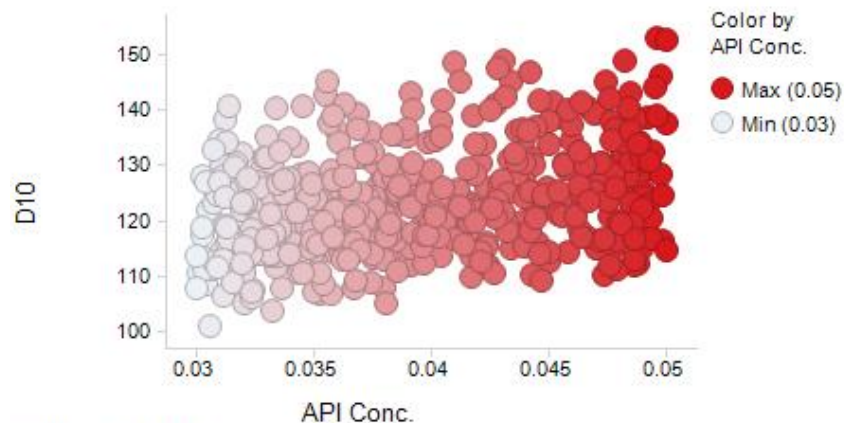


D43 vs. T<sub>set</sub>

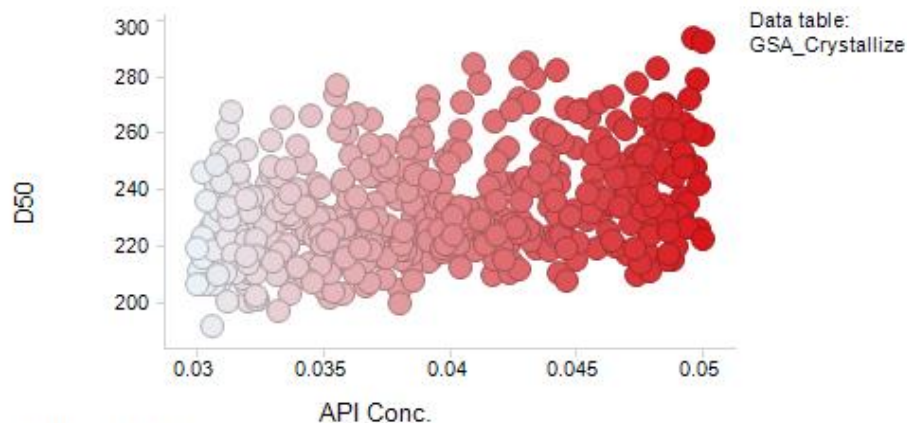


# Effect of Initial API Concentration in Solution on Crystal PSD

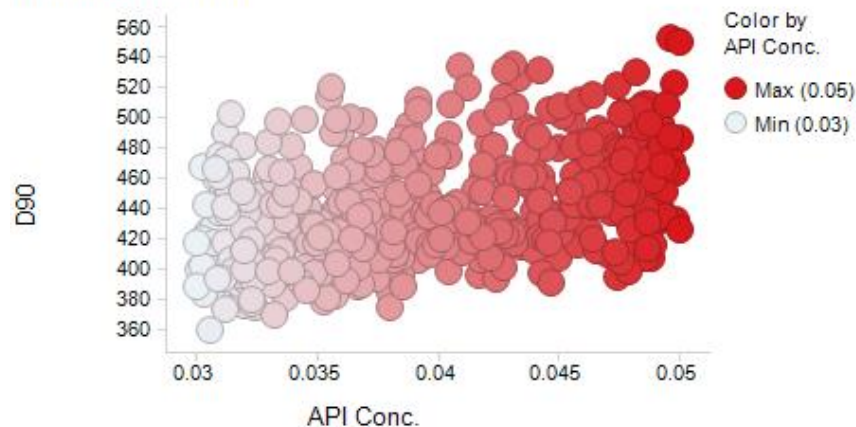
D10 vs. API Conc.



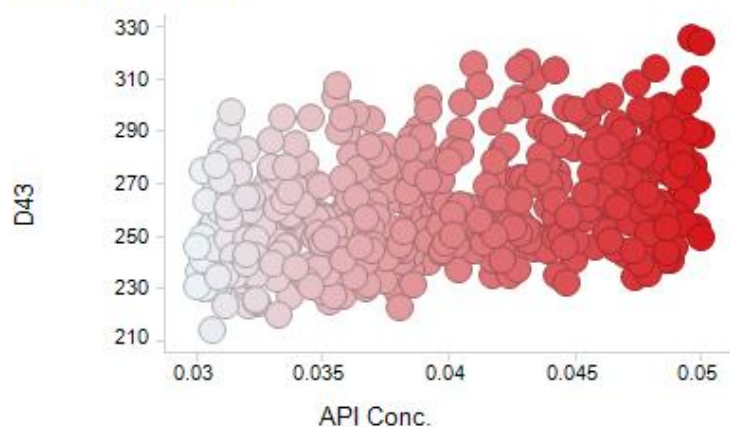
D50 vs. API Conc.



D90 vs. API Conc.

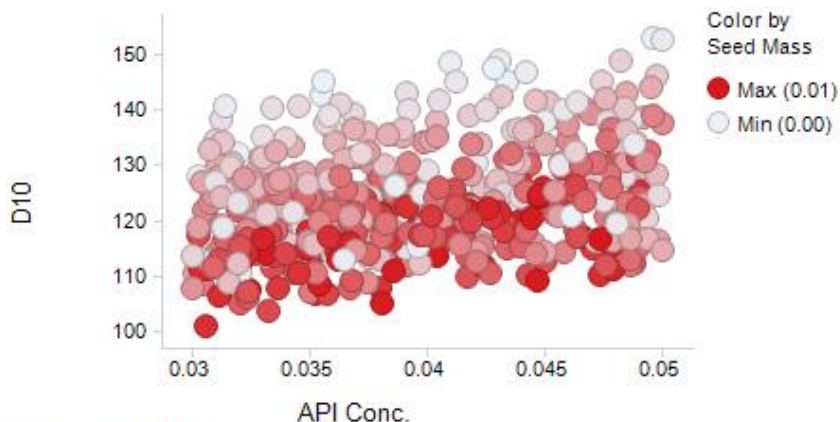


D43 vs. API Conc.

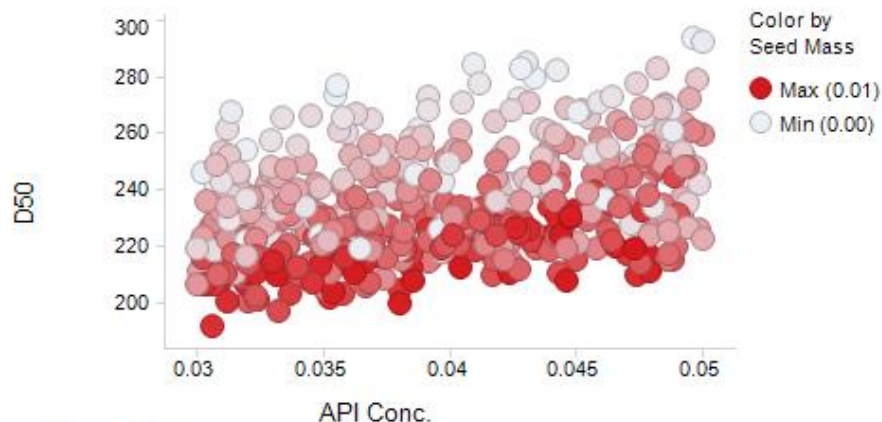


# Effect of Initial API Concentration in Solution on Crystal PSD

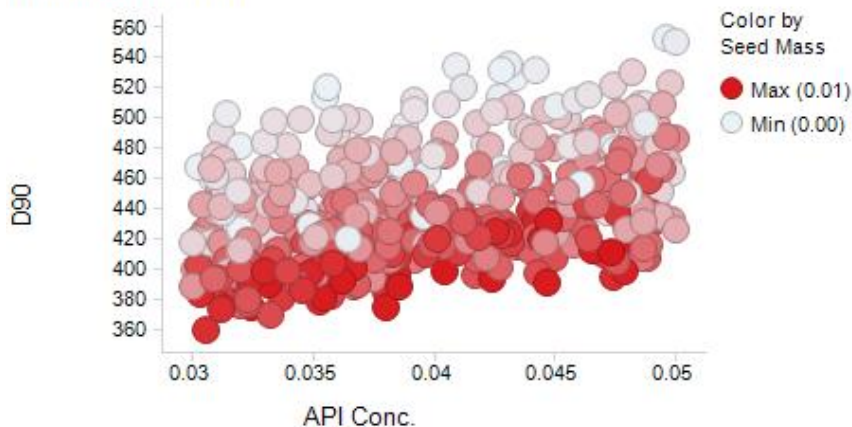
D10 vs. API Conc.



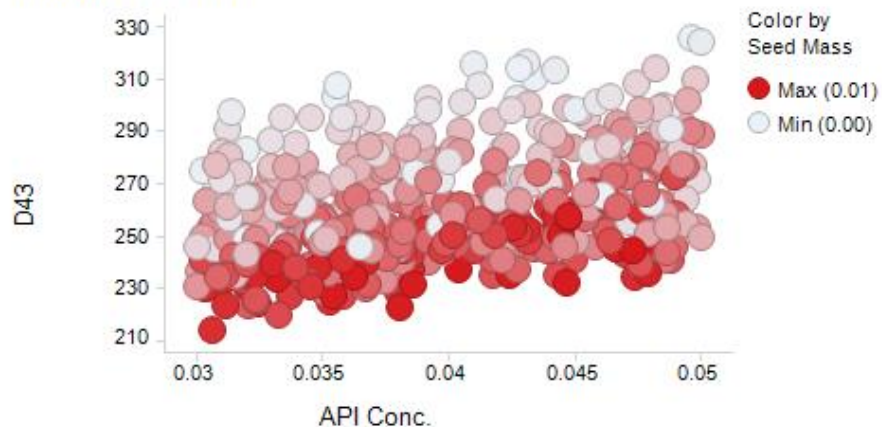
D50 vs. API Conc.



D90 vs. API Conc.



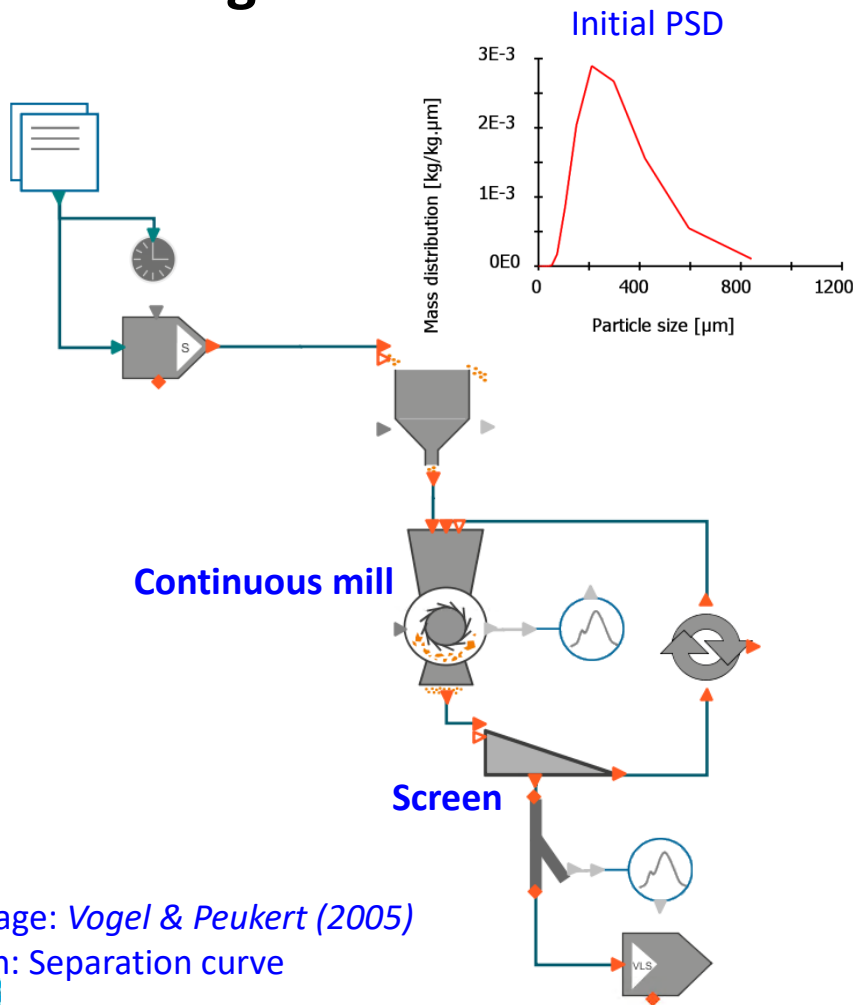
D43 vs. API Conc.





# API Hammer Mill Model

## API milling



Breakage: Vogel & Peukert (2005)  
Screen: Separation curve

### Processing conditions:

0h - 6h Constant operation  
Flowrate 1.5 kg/h

### Input variables:

- Crystal PSD (fixed from crystallizer)
- Impact energy (5,000-10,000 J/kg)
- No. impacts (1-10)
- Power law exponent (0.3-3)
- Screen aperture size (100-1,000  $\mu\text{m}$ )

### Physicochemical parameters:

- Material strength parameter (0.5 kg/Jm)
- Breakage rate constant ( $0.01 \text{ s}^{-1}$ )
- Product of threshold energy and particle size (0.25 Jm/kg)
- Range of non-ideal separation in screen (50  $\mu\text{m}$ )

### Output variables:

- Milled API PSD

# Milling Breakage Parameters

$k$  is the number of successive impacts or stressing events [-],

**Process parameters**

$W_{m,kin}$  is the mass specific impact energy to cause particle breakage [J/kg],

$W_{m,min}$  is the mass specific threshold energy that a particle can absorb without fracture [J/kg],

$q$  is a kernel function to model breakage size distribution ( $q < 0$ ) [-],

**Material parameters**

$x'$  is the fragment size from which on the additional fading of the power law becomes significant [m],

$f_{Mat.}$  characterises the particulate material resistance against fracture in impact comminution [kg/J/m],

$$B_{M,p}(x, y) = \left(\frac{y}{x}\right)^q \frac{1}{2} \left(1 + \tanh\left(\frac{x - x'}{x'}\right)\right)$$

$$P_B(y) = 1 - \exp\left(-f_{Mat} y k (W_{m,kin} - W_{m,min})\right)$$

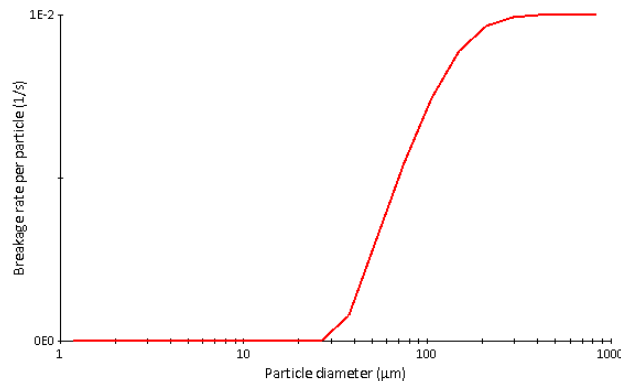
# Results from single mill simulation

## API milling

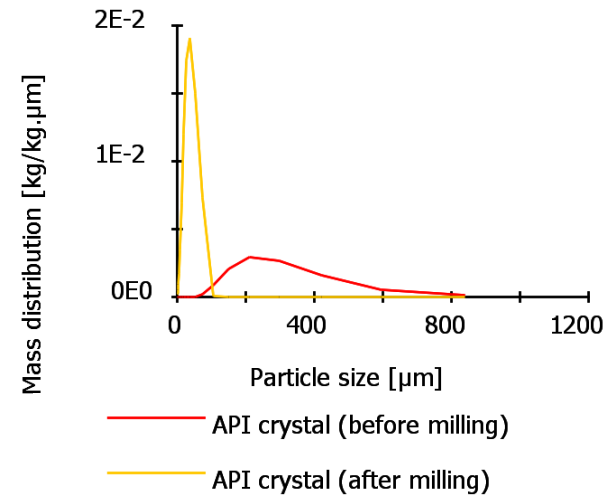
### Scenario

- Impact energy (7,500 J/kg)
- No. impacts (5)
- Power law exponent (2)
- Screen aperture size (100  $\mu\text{m}$ )

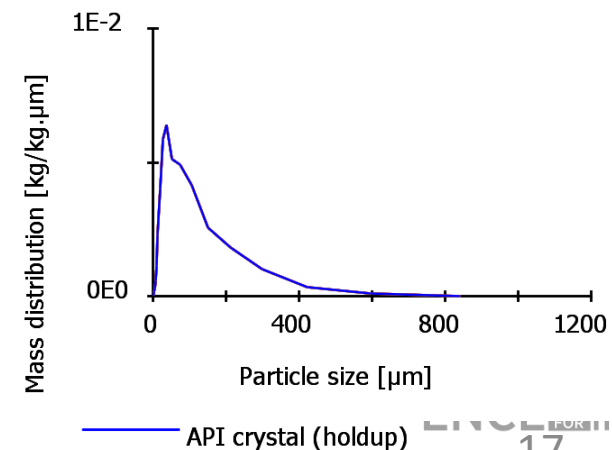
### Breakage rate per particle size



### PSD before and after milling

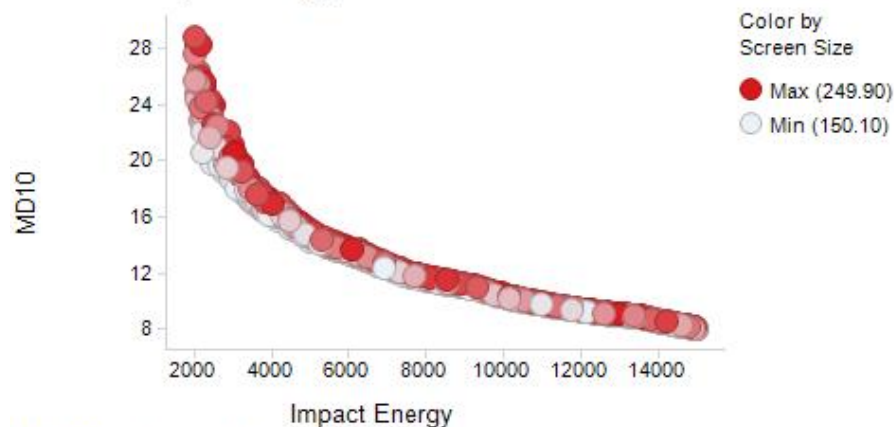


### PSD within the unit

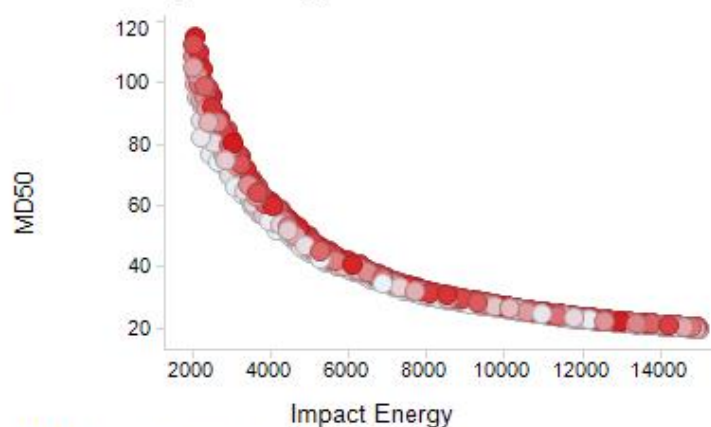


# Effect of Impact Energy on the Milled PSD

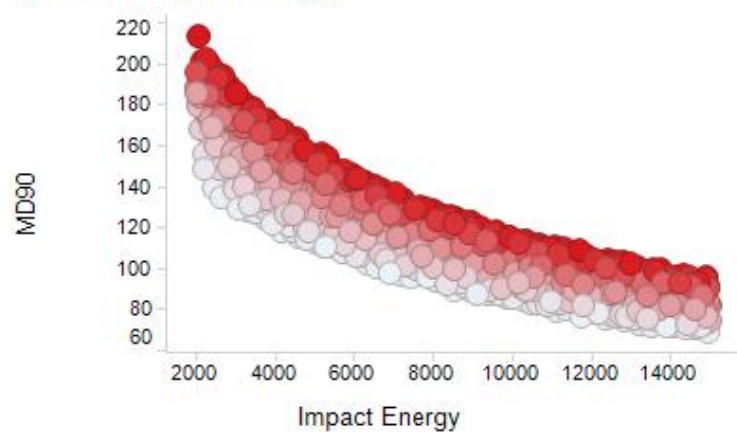
MD10 vs. Impact Energy



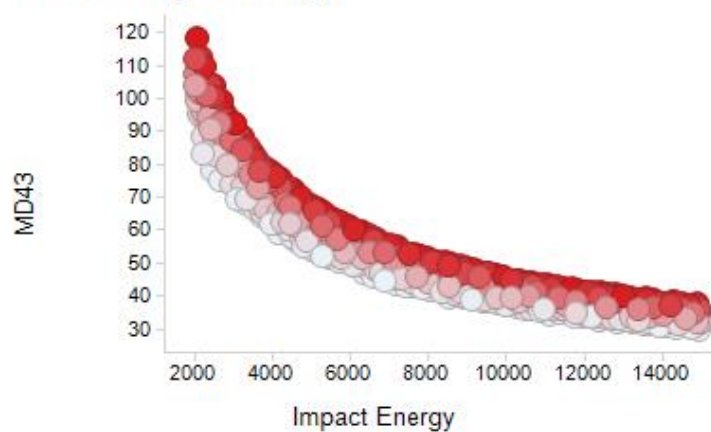
MD50 vs. Impact Energy



MD90 vs. Impact Energy

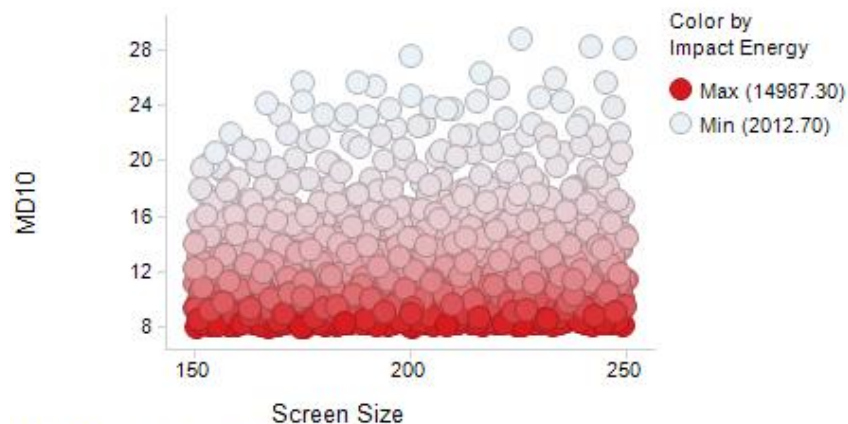


MD43 vs. Impact Energy

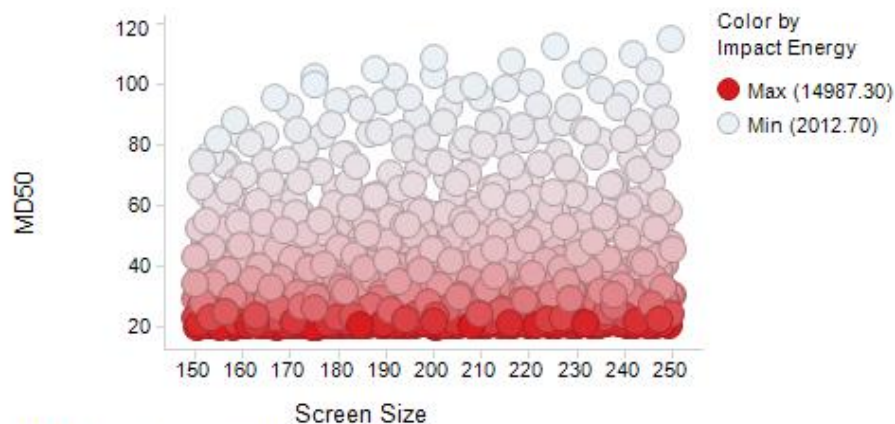


# Impact of Screen Size on Milled PSD

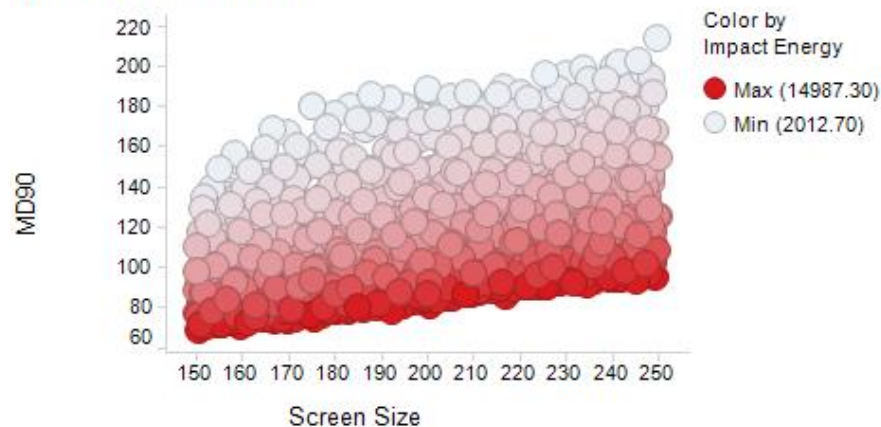
MD10 vs. Screen Size



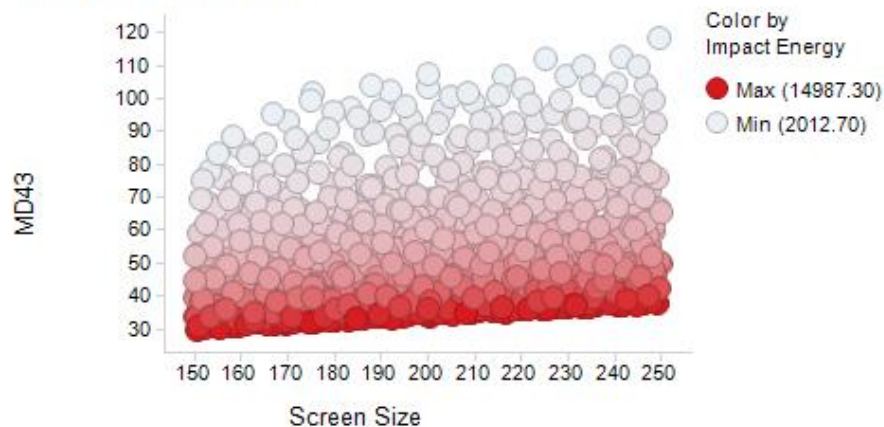
MD50 vs. Screen Size



MD90 vs. Screen Size

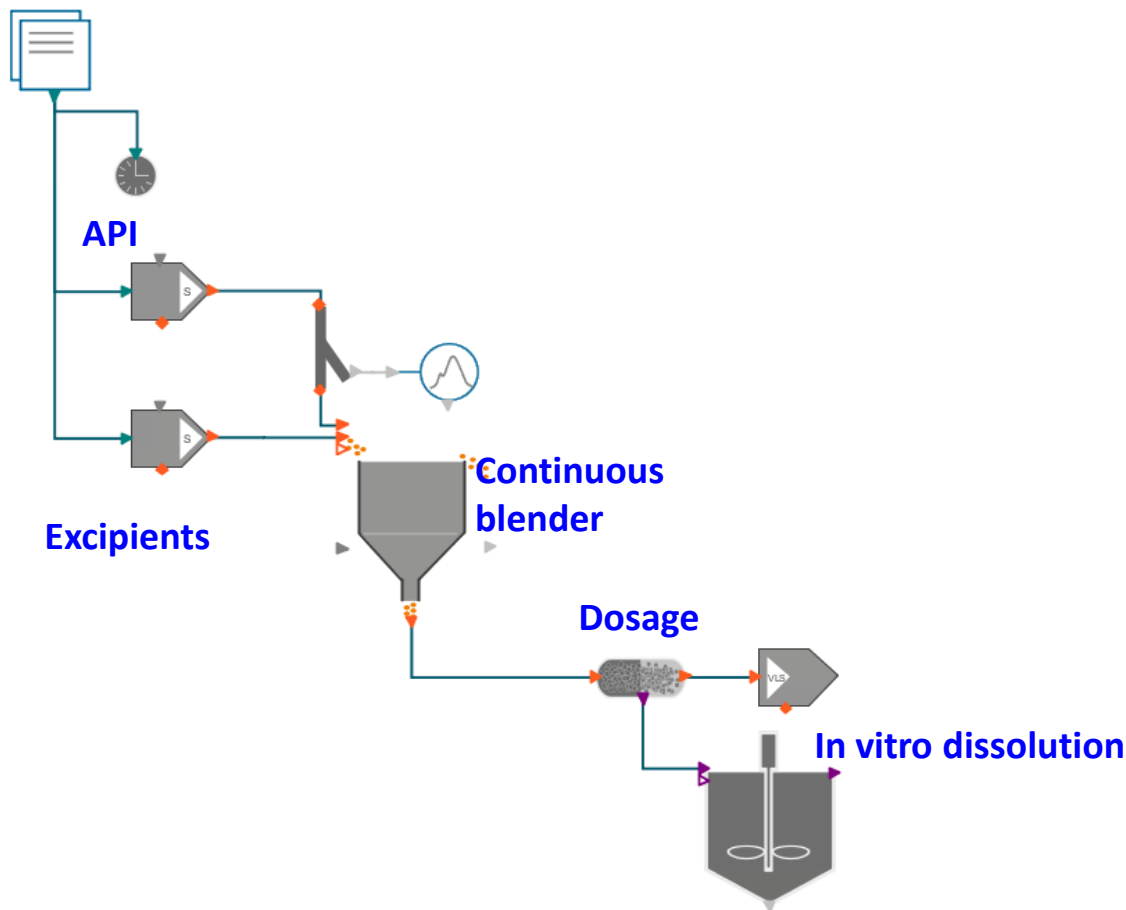


MD43 vs. Screen Size



# In Vitro Dissolution Model

## Drug product formulation and in vitro dissolution



### Processing conditions:

- Media pH (4.5)
- Media volume (250 ml)

### Input variables:

- API PSD (Lognormal with mean size)
- Drug load (10 %w)
- Dosage time (0 h)
- Tablet mass (100-500 mg)
- API diffusivity ( $50\text{-}500\text{ }\mu\text{m}^2/\text{s}$ )

### Physicochemical parameters:

- API solubility (3.25 mg/L)
- Neutral compound

### Output variables:

- API fraction dissolved
- API mass dissolved



# Results from single dissolution simulation

## Drug product formulation and in vitro dissolution

### Scenario

- API PSD (fixed from milling)
- Drug load (10 %w)
- Dosage time (0 h)
- Tablet mass (100 g)
- API diffusivity ( $500 \mu\text{m}^2/\text{s}$ )

API mass per dose = 10 mg

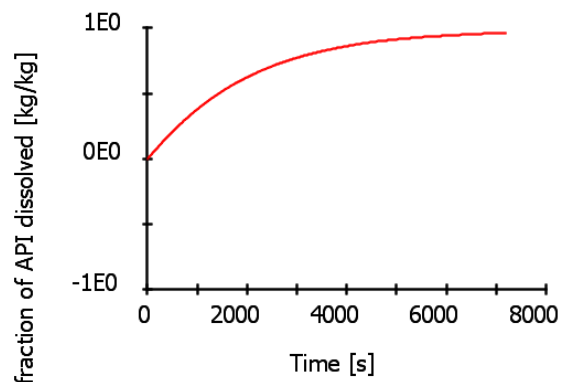
Fraction dissolved in 15 min = 0.346

mg/mg API in dose

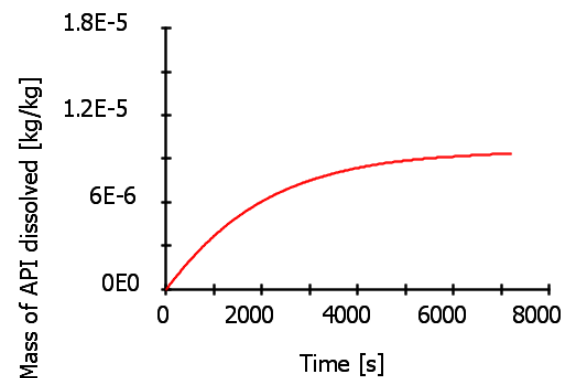
Fraction dissolved in 2 h = 0.965 mg/mg

API in dose

Fraction of total API dosed dissolved

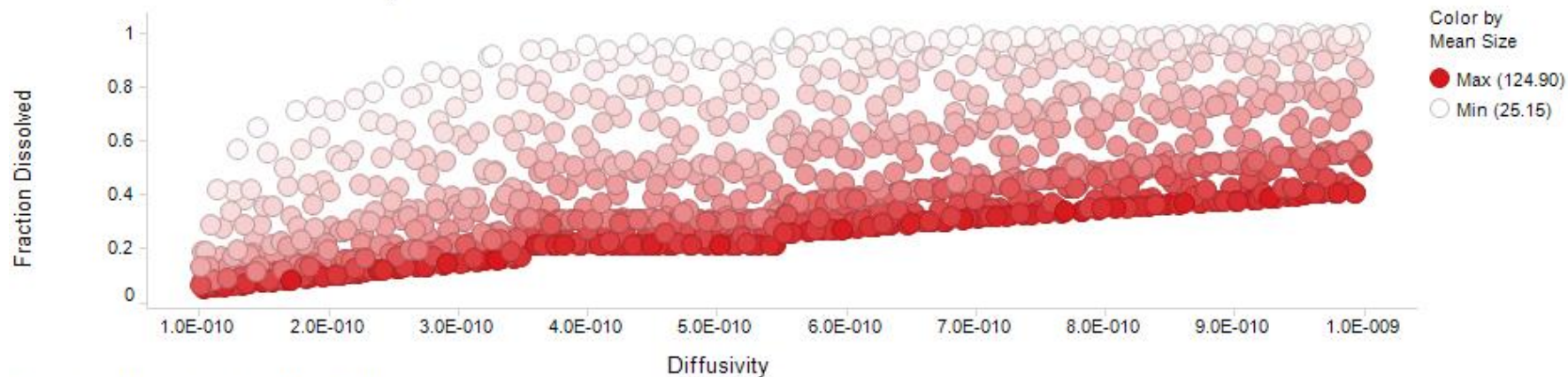


Mass of API dosed dissolved

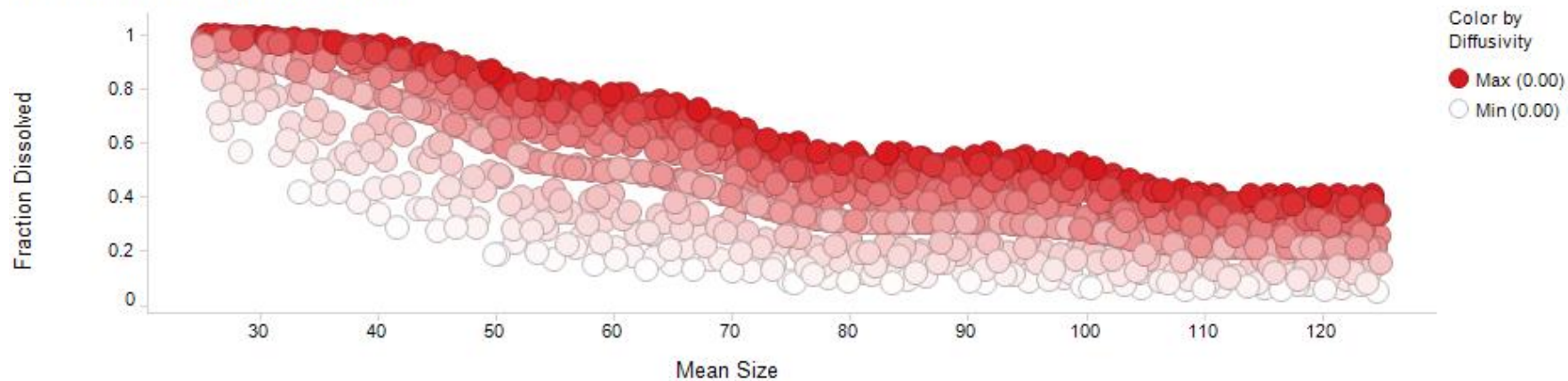


# Dissolution\_diff

Fraction Dissolved vs. Diffusivity

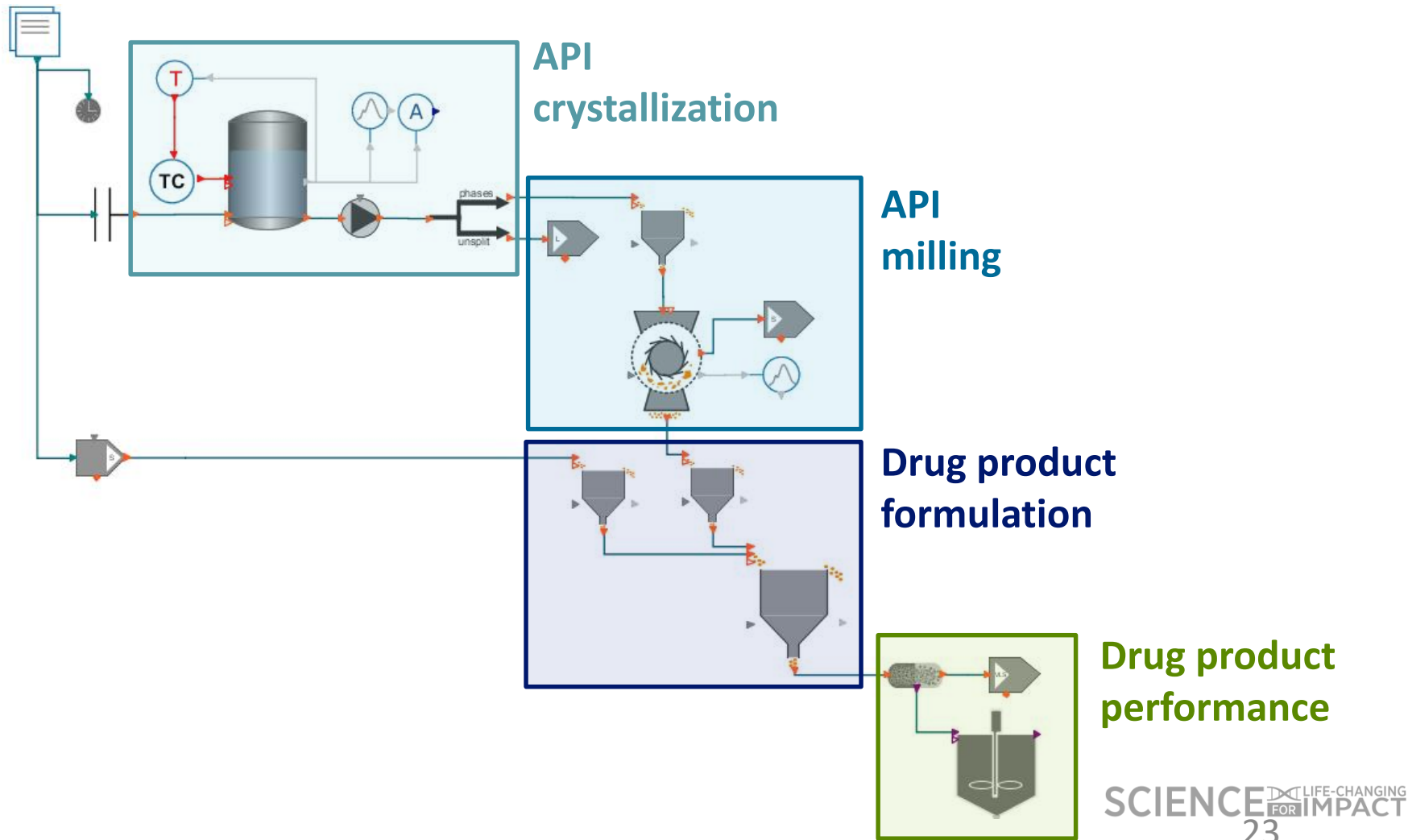


Fraction Dissolved vs. Mean Size



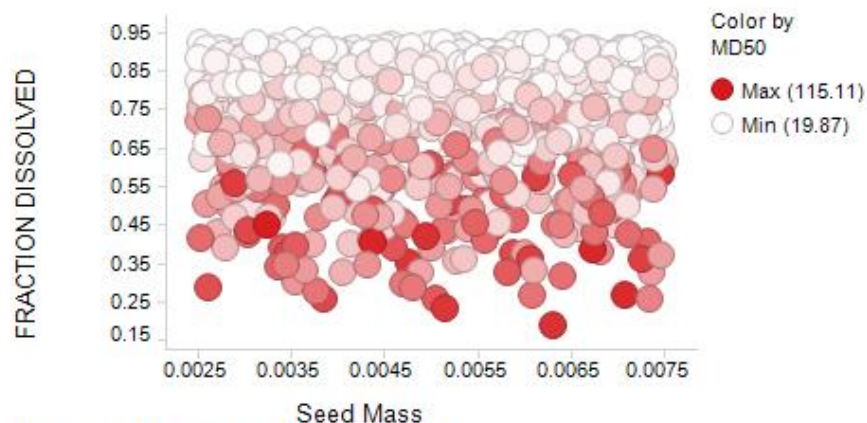
# Interconnected flowsheet

## Interconnected drug manufacturing to performance

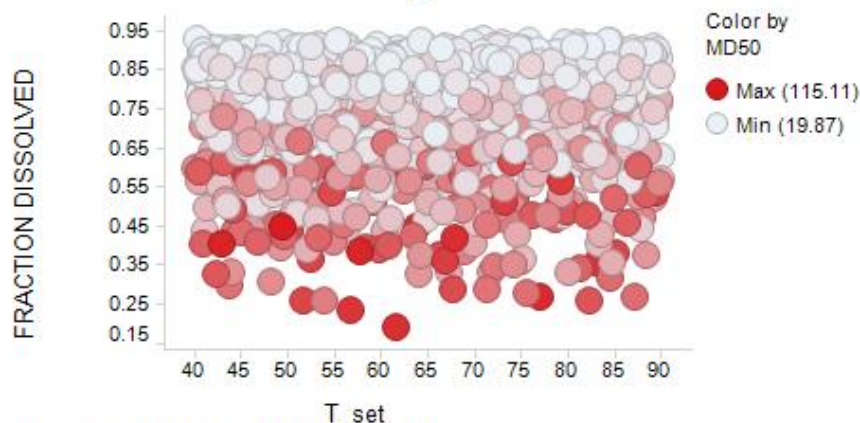


# Effect of Crystallization Process on Fraction Dose Dissolved

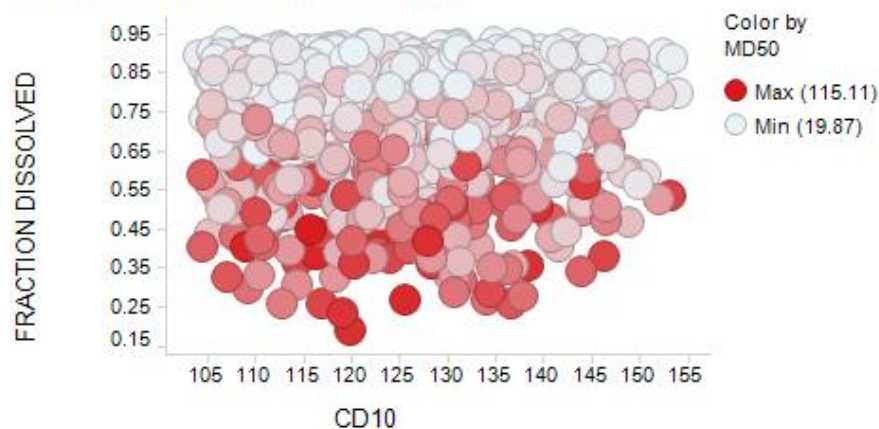
**FRACTION DISSOLVED vs. Seed Mass**



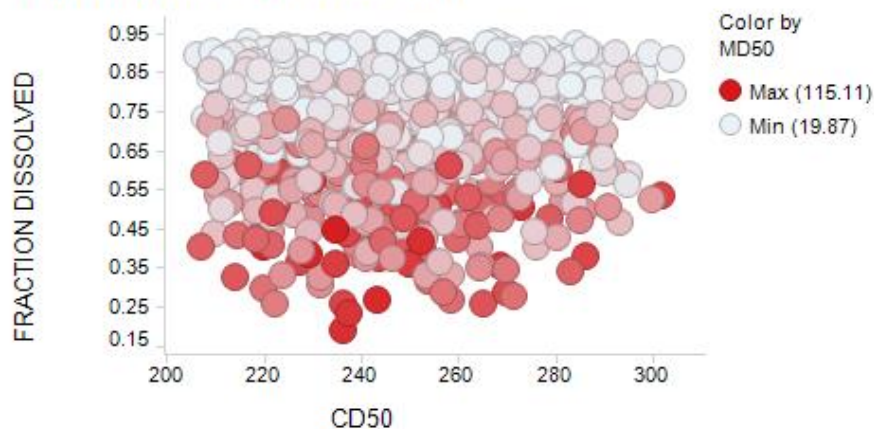
**FRACTION DISSOLVED vs. T\_set**



**FRACTION DISSOLVED vs. CD10**



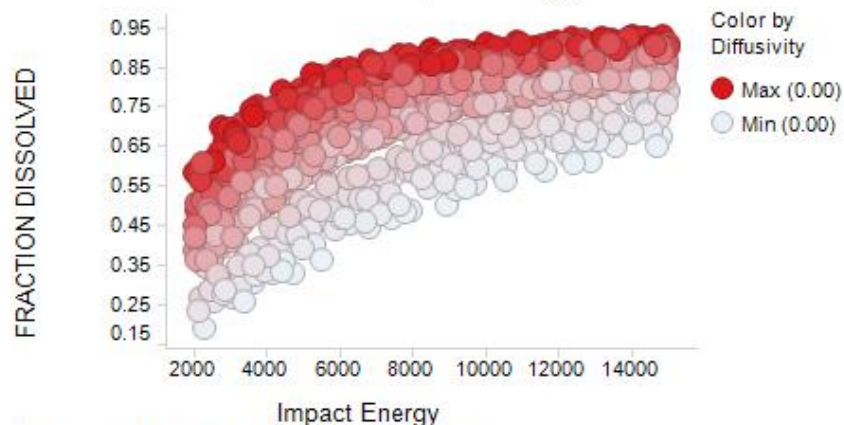
**FRACTION DISSOLVED vs. CD50**



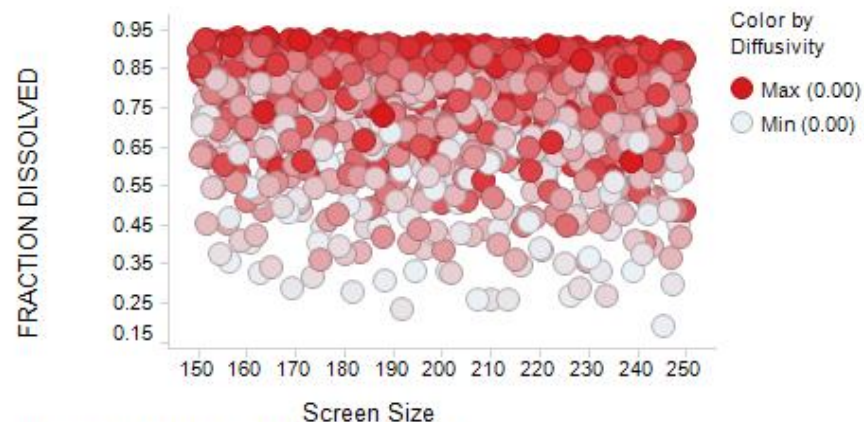


# Effect of Milling Process on Fraction Dose Dissolved

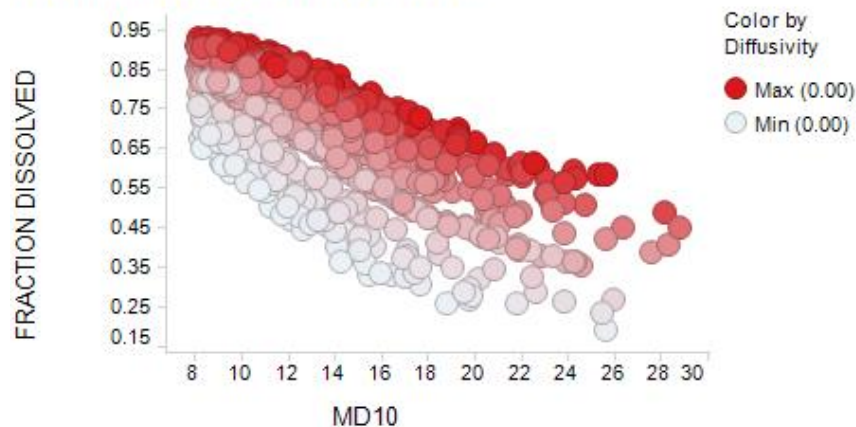
**FRACTION DISSOLVED vs. Impact Energy**



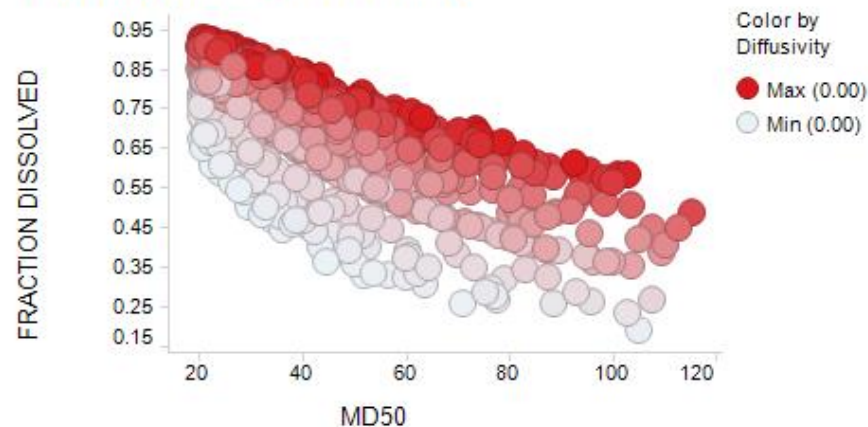
**FRACTION DISSOLVED vs. Screen Size**



**FRACTION DISSOLVED vs. MD10**

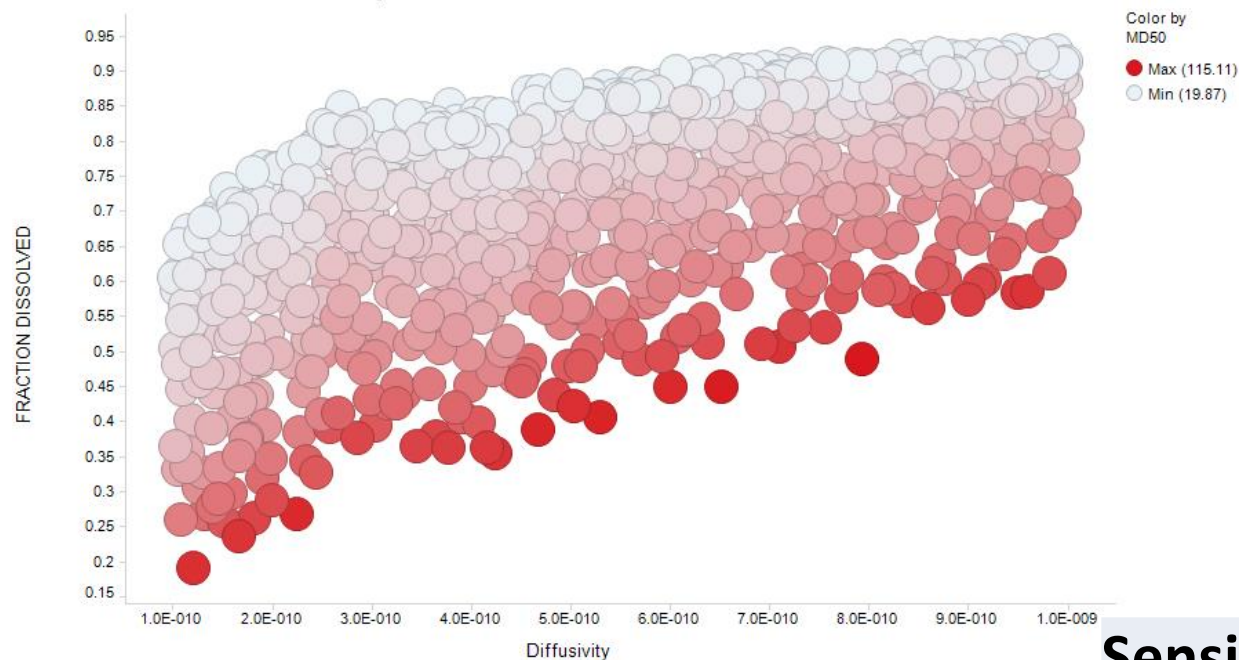


**FRACTION DISSOLVED vs. MD50**



# Effect of API Diffusivity on Fraction Dissolved

FRACTION DISSOLVED vs. Diffusivity



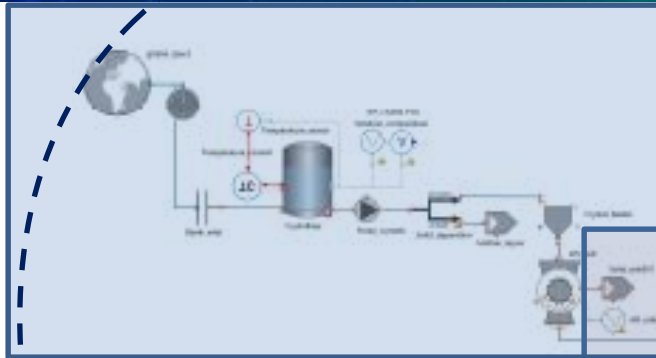
## Sensitivity Indices

Parameters	First Order Effect	Total Effect
Impact Energy	0.58	0.62
Screen Size	0.01	0.01
Seed Mass	0.02	0.00
Tset	0.02	0.00
Diffusivity	0.37	0.41





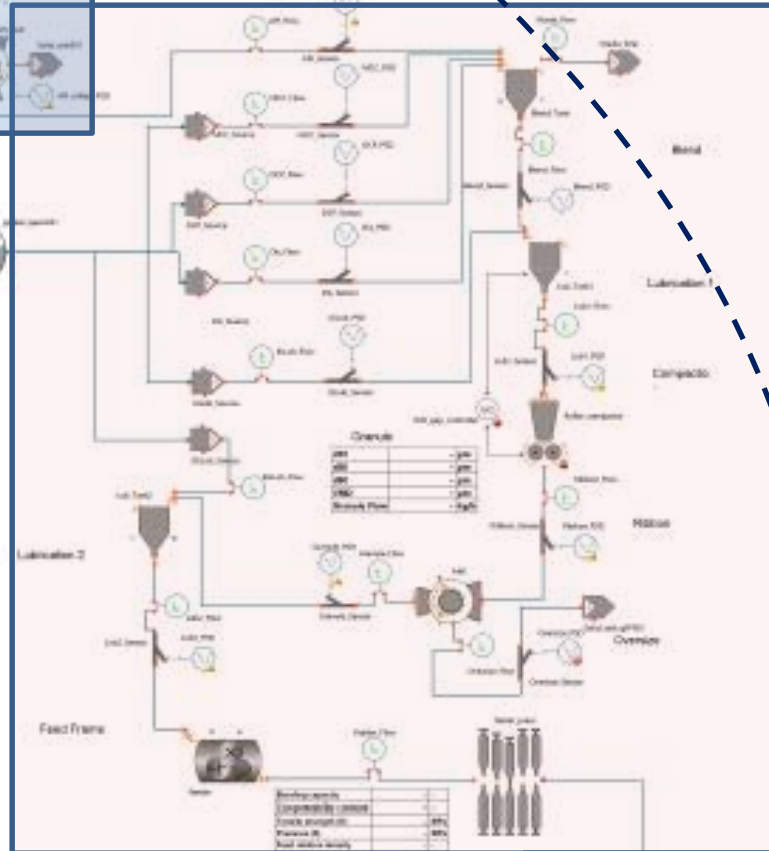
# Long term Vision: Digital Design



**Global System Analysis**

**Early Stage Risk Analysis**

**Optimal Design of product and process**



# Conclusions

- Global System Analysis enables a comprehensive study of interconnected flowsheet models
- Seamless execution of large number of simulation (Virtual DOE) and aggregation of relevant output in a windows based “HPC environment” is a very powerful feature
- Extension to a Linux based HPC environment or Cloud computing infrastructure will be a very desirable feature
- Virtual DOE enables “stress testing of the model” leading to more rigorous verification and also exposing some shortcomings
- Sensitivity Analysis helps in dimensionality reduction
- Seamless, integrated *in silico* modeling from API and drug product manufacture to oral absorption will become part of work-flow



# Acknowledgement

- Ravi Shanker
- Susan Ewing
- Martyn Ticehurst
- Kevin Girard
- Mary am Ende
- Bill Ketterhagen