

	MeOH	EtOH	nPOH	nBOH
zi	0.3	0.2	0.15	0.35
xi	0.3	0.2	0.15	0.35
yi	0.587803	0.240432	0.084591	0.087172

P Sat Data

T	MeOH	EtOH	nPOH	nBOH	$\sum z_i K_i$
50	415	220	88.9	33.7	0.254776
60	629	351.5	148.9	59.2	0.397440
65	767	438	190.1	77.7	0.491328
70	929	542	240.6	99.6	0.602697
75	1119	665	301.9	131.3	0.736763
80	1339	812	376	165	0.892434
82.954784	1489.103	913.6445	428.5951	189.2883	1
85	1593	984	465	206.1	1.074453
90	1884	1185	571	225.9	1.272256
100	2598	1706	843	387.6	1.819355

Equilib Data

T	MeOH K	EtOH K	nPOH K	nBOH K
50	0.546052	0.289473	0.116973	0.044342
60	0.827631	0.4625	0.195921	0.077894
65	1.009210	0.576315	0.250131	0.102236
70	1.222368	0.713157	0.316578	0.131052
75	1.472368	0.875	0.397236	0.172763
80	1.761842	1.068421	0.494736	0.217105
85	2.096052	1.294736	0.611842	0.271184
90	2.478947	1.559210	0.751315	0.297236
100	3.418421	2.244736	1.109210	0.51

	MeOH	EtOH	nPOH	nBOH
zi	0.3	0.2	0.15	0.35
yi	0.469443	0.308239	0.152306	0.070011
xi	0.087822	0.089168	0.135345	0.687021

P Sat Data

T	MeOH	EtOH	nPOH	nBOH	$\sum zi/Ki$
50	415	220	88.9	33.7	10.41582
60	629	351.5	148.9	59.2	6.053770
65	767	438	190.1	77.7	4.667401
70	929	542	240.6	99.6	3.670366
75	1119	665	301.9	131.3	2.835828
80	1339	812	376	165	2.272781
85	1593	984	465	206.1	1.833394
90	1884	1185	571	225.9	1.626451
99.97393591	2596.139	1704.642	842.2910	387.1785	1
100	2598	1706	843	387.6	0.998362

Equilib Data

T	MeOH K	EtOH K	nPOH K	nBOH K	88.9	33.7
50	0.546052	0.289473	0.116973	0.044342	148.9	59.2
60	0.827631	0.4625	0.195921	0.077894	190.1	77.7
65	1.009210	0.576315	0.250131	0.102236	240.6	99.6
70	1.222368	0.713157	0.316578	0.131052	301.9	131.3
75	1.472368	0.875	0.397236	0.172763	376	165
80	1.761842	1.068421	0.494736	0.217105	465	206.1
85	2.096052	1.294736	0.611842	0.271184	571	225.9
90	2.478947	1.559210	0.751315	0.297236	843	387.6
100	3.418421	2.244736	1.109210	0.51		

T = 88.8 Celcius	MeOH	EtOH	nPOH	nBOH	Frac Bal Check
zi	0.3	0.2	0.15	0.35	1
xi	0.187116	0.162368	0.165784	0.486319	1.001588627
yi	0.469325	0.256447	0.126323	0.145520	0.9976170593
Mat Bal Check	0	0	0	0	

Overall Mat Bal

Feed	1
Vapor	0.4
Liquid	0.6

Equilib Data

T Celcius	MeOH K	EtOH K	nPOH K	nBOH K	$\psi(.4) (V/F)$
50	0.546052	0.289473	0.116973	0.044342	1.111175692
60	0.827631	0.4625	0.195921	0.077894	0.8816203808
65	1.009210	0.576315	0.250131	0.102236	0.750227682
70	1.222368	0.713157	0.316578	0.131052	0.6107807295
75	1.472368	0.875	0.397236	0.172763	0.4589820699
80	1.761842	1.068421	0.494736	0.217105	0.3054420553
85	2.096052	1.294736	0.611842	0.271184	0.1476489882
90	2.478947	1.559210	0.751315	0.297236	0.0134016576
90.38206681	2.514841	1.585402	0.764989	0.305365	0
100	3.418421	2.244736	1.109210	0.51	-0.3373657268

P Sat Data

T Celcius	MeOH	EtOH	nPOH	nBOH
50	415	220	88.9	33.7
60	629	351.5	148.9	59.2
65	767	438	190.1	77.7
70	929	542	240.6	99.6
75	1119	665	301.9	131.3
80	1339	812	376	165
85	1593	984	465	206.1
90	1884	1185	571	225.9
90.38206681	1906.236	1200.359	579.0998	227.4129
100	2598	1706	843	387.6

0.5414607651

0.2047868012

	Flow Tot.	Frac MeOH	Flow MeOH	Frac EtOH	Flow EtOH	Frac nPOH	Flow nPOH	Frac nBOH	Flow nBOH	Check
Feed	100	0.3	30	0.2	20	0.15	15	0.35	35	1
Bottoms	72.222	0.049998615	3.611	0.2576915621	18.611	0.20769294	15	0.484616875	35	1
Distillate	27.778	0.9499964	26.389	0.05000359997	1.389	0	0	0	0	1
Check	1		1		1		1		1	

Given specs are bolded
Initial guesses are italics

Dew Pt. 65.78

Equilib Data

P Sat Data

T Celcius	MeOH K	EtOH K	nPOH K	nBOH K	$\sum x_i d_i / K_i$	T Celcius	MeOH	EtOH	nPOH	nBOH
50	0.54605263	0.289473684	0.116973684	0.04434210526	1.91249215	50	415	220	88.9	33.7
60	0.82763157	0.4625	0.1959210526	0.07789473684	1.25596527	60	629	351.5	148.9	59.2
65	1.00921052	0.576315789	0.2501315789	0.1022368421	1.02809052	65	767	438	190.1	77.7
65.77684856	1.04232880	0.597576907	0.260455487	0.106713943	1	65.7768485	792.169893	454.15845	197.9461704	81.1025966
70	1.22236842	0.713157894	0.316578947	0.1310526316	0.84729256	70	929	542	240.6	99.6
75	1.47236842	0.875	0.397236842	0.1727631579	0.70236347	75	1119	665	301.9	131.3
80	1.76184210	1.068421053	0.494736842	0.2171052632	0.58600772	80	1339	812	376	165
85	2.09605263	1.294736842	0.611842105	0.2711842105	0.49185184	85	1593	984	465	206.1
90	2.47894736	1.559210526	0.751315789	0.2972368421	0.41529554	90	1884	1185	571	225.9
100	3.41842105	2.244736842	1.109210526	0.51	0.30018095	100	2598	1706	843	387.6

Bubble Pt. 94.34

Equilib Data

P Sat Data

T Celcius	MeOH K	EtOH K	nPOH K	nBOH K	$\sum x_i b_i * K_i$	T Celcius	MeOH	EtOH	nPOH	nBOH
50	0.54605263	0.289473684	0.116973684	0.04434210526	0.14768034	50	415	220	88.9	33.7
60	0.82763157	0.4625	0.1959210526	0.07789473684	0.23900330	60	629	351.5	148.9	59.2
65	1.00921052	0.576315789	0.2501315789	0.1022368421	0.30046710	65	767	438	190.1	77.7
70	1.22236842	0.713157894	0.316578947	0.1310526316	0.37415303	70	929	542	240.6	99.6
75	1.47236842	0.875	0.397236842	0.1727631579	0.46532373	75	1119	665	301.9	131.3
80	1.76184210	1.068421053	0.494736842	0.2171052632	0.57137898	80	1339	812	376	165
85	2.09605263	1.294736842	0.611842105	0.2711842105	0.69693822	85	1593	984	465	206.1
90	2.47894736	1.559210526	0.751315789	0.2972368421	0.82582831	90	1884	1185	571	225.9
94.34	2.88693278	1.856914174	0.906738806	0.3896335403	1	94.34	2194.06892	1411.25477	689.121493	296.121490
100	3.41842105	2.244736842	1.109210526	0.51	1.22689587	100	2598	1706	843	387.6

K Values	MeOH	EtOH	nPOH	nBOH	α Top	α Bottom	α Ave	α Gmean
65.78	1.04	0.60	0.26	0.11	1.74	1.55	1.65	1.646750818

70.00	1.22	0.71	0.32	0.13
75.00	1.47	0.88	0.40	0.17
80.00	1.76	1.07	0.49	0.22
85.00	2.10	1.29	0.61	0.27
90.00	2.48	1.56	0.75	0.30
94.34	2.89	1.86	0.91	0.39

Fenske

N min 9.159875

	MeOH (i)	EtOH(j)
Bottoms Frac	0.04999861	0.257691562
Distillate Frac	0.9499964	0.050003599
Min Stages	9.15987517	

Recalc

N Min 9.159875

	MeOH (i)	EtOH(j)
Bottoms Frac	0.04999927	0.25769495
Distillate Frac	0.94996387	0.05000188
Min Stages	9.15987517	

Redis.

Br EtOH	18.611
Dr EtOH	1.389
(α_i ,r)mPOH	0.46207838
(α_i ,r)mBOH	0.19420313

	POH	BOH
bi	14.9990497	34.99999921
di	0.00095024	0.000000789
bi recalc	14.9990497	34.99999921

Mat Bal Corr.

	Flow Tot.	Frac MeOH	Flow MeOH	Frac EtOH	Flow EtOH	Frac nPOH	Flow nPOH	Frac nBOH	Flow nBOH
Feed	100	0.3	30	0.2	20	0.15	15	0.35	35

Bottoms	72.2210485	0.049999273	3.611	0.257694955	18.611	0.20768252	14.9990497	0.48462324	34.99999921
Distillate	27.778951	0.949963876	26.389	0.05000188807	1.389	0.00003420	0.00095024	0.000000028	0.000000785
Check	1		1		1		1		1

Underwood**R min 2.19852'**

	Flow Tot.	Frac MeOH	Flow MeOH	Frac EtOH	Flow EtOH	Frac nPOH	Flow nPOH	Frac nBOH	Flow nBOH
Feed	100	0.3	30	0.2	20	0.15	15	0.35	35
Distillate	27.778951	0.949963876	26.389	0.05000188807	1.389	0.00003420	0.00095024	0.000000028	0.000000785

K Values	MeOH	EtOH	nPOH	nBOH
65.78	1.04	0.60	0.26	0.11
70.00	1.22	0.71	0.32	0.13
75.00	1.47	0.88	0.40	0.17
80.00	1.76	1.07	0.49	0.22
80.06	1.77	1.07	0.50	0.22
85.00	2.10	1.29	0.61	0.27
90.00	2.48	1.56	0.75	0.30
94.34	2.89	1.86	0.91	0.39

	MeOH	EtOH	nPOH	nBOH
$(\alpha_i, r)_{\infty} T(80.0^\circ\text{C})$	1.64857963		1 0.463191568	0.2032922771
1-q = -0.1				

$\Theta 4$	$\Theta 3$	$\Theta 2$	$\Theta 1$
9.65225	1.19525	0.550986	0.268632
(α_i, r)	$\Theta 3$	(α_i, r)	$\Theta 2$
1.648579631	1.19525	1	0.550986
			0.463191568

Rmin $\Theta 2$ 0.53801892Rmin $\Theta 3$ 2.19852750**Gilliland****N Actual 16.8200'**

Reflux 3

X	0.20036812
Y	0.4601570C
N Actual	16.820055€

Kirkbride

Feed Stage	9		
	Nr/Ns	Ns	Nr
Exact	1.11994094	7.934209542	8.885846137
Rounded		8	9