

How to implement a new boundary condition and modify a solver without modifying the solver source code

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CFD Online: https://www.cfd-online.com/Forums/members/jherb.html

Github: https://github.com/jmozmoz/OFdevelopments



Overview

- Why?
- Existing code
- Physics
- Overview of implementation
- Code/Steps how to implement => github/commits
- Verification



Motivation

- In new reactor designs, passive safety systems play important role
- Need to simulate evaporation and condensation in the containment
- Need to resolve local phenomena'
 (e. g. local concentration of non-condensable gases)
- Long term goal: Use CFD as additional tool for safety analyses of different phenomena in the containment
- Demonstrate applicability of OpenFOAM to reactor safety/containment relevant phenomena
- Implement wall condensation, because
 - BMWi funded implementation exists for CFX with documentation
 - it is missing in OpenFOAM



Schramm et al., GRS-324, https://doi.org/10.2314/GBV:88267787X



Wall condensation modelling in OpenFOAM

Since OpenFOAM v3.0+ (ESI) thermalHumidityCoupledMixed https://www.openfoam.com/releases/openfoam-v3.0+/boundary-conditions.php https://develop.openfoam.com/Development/OpenFOAMplus/tree/master/src/thermophysicalModels/thermophysicalPropertiesFvPatchField s/liquidProperties/humidityTemperatureCoupledMixed

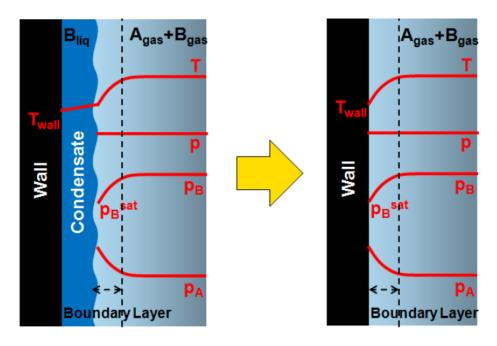
Problems:

- "Macroscopic model": Nu(Tsat, Re(L)), h_m(Sh(Re(L), Sc))
 L: Parameter specified by user
- Possibly wrong implementation of correlation given in T. Bergam et al. Heat and Mass Transfer. 7th Edition. Chapter 10.
 Interpreted as Nusselt number [-] instead of a heat transfer correlation [W/(K m²)]
- chtMultiRegionFoam (OpenFOAM-6)
 Simulate air/vapor mixture (non-reacting) with conjugated heat transfer (https://openfoam.org/release/6/)
 - Use thermophysical Properties of OpenFOAM



Wall condensation modelling in ANSYS CFX

Implementation of a "microscopic" model for turbulent transport



Zschaeck et al., CFD modelling and validation of wall condensation in the presence of non-condensable gases, Nuclear Engineering and Design **279**, pp 137-146 (2014) see also https://doi.org/10.2314/GBV:861756150



Physics

Ideas

- Saturation condition at wall
- ⇒ Vapor concentration at wall given by saturation pressure at wall temperature
- Diffusion in cells next to wall from cell center to wall face

$$\dot{m}_{H_2O} = -\frac{\Gamma_{H_2O,c}}{y_c} \frac{Y_{H_2O,c} - Y_{H_2O,f}}{1 - Y_{H_2O,f}}$$

- Latent heat released at wall
- Mass diffusing to the fluid:
 - Remove it from the fluid
 - Remove specific heat from fluid
 - Add it to wall film

y, wall distance of cell center

 $\Gamma_{H_2O,c}$, diffusivity of H_2O in air

 $Y_{H_2O,c}$, mass fraction of H_2O at cell center

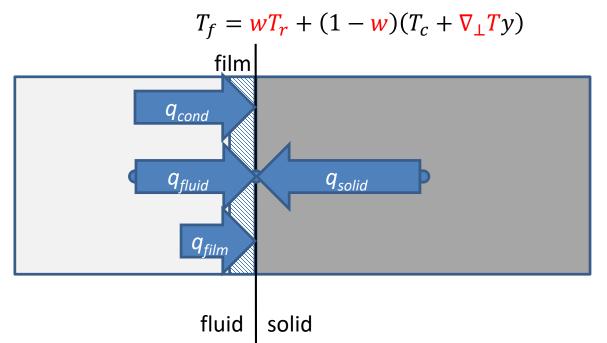
 $Y_{H_2O,f}$, mass fraction of H_2O at wall face



Implementation (1/4)

Boundary condition for temperature:

- Using OpenFOAM class hierarchy (mixedFvPatchScalarField)
- Saturation condition at the wall
 - Vapor concentration for $T_{sat} = T_{wall}$
 - Diffusion from cell center of cell to wall due to different concentration
 - Energy conservation at wall



 $?_f$: face value

?_c: cell center value

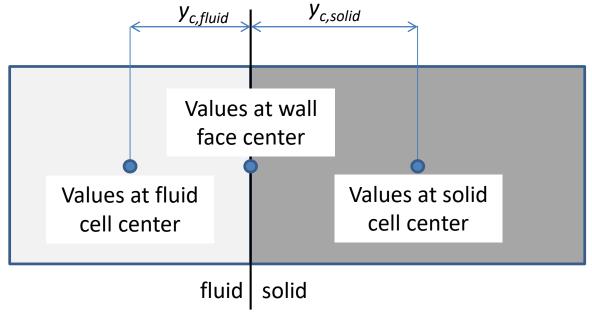
?_r: "reference" value



Implementation (2/4)

Calculate source mass and energy source terms:

$$\begin{split} \dot{m}_{H_2O} &= -\frac{\Gamma_{H_2O,c}}{y_c} \frac{Y_{H_2O,c} - Y_{H_2O,f}}{1 - Y_{H_2O,f}} \\ Y_{H_2O,f} &= X_{H_2O,f} \frac{M_{H_2O}}{M} \\ X_{H_2O,f} &= \frac{p_{H_2O,sat}(T_f)}{p_f} \\ \Gamma_{H_2O,c} &= \frac{\mu}{Sc} + \frac{\mu_t}{Sc_t} \end{split}$$



$$S_{m,H_2O} = \frac{\dot{m}_{H_2O}A_f}{V_c}$$
 $S_{h,H_2O} = S_{m,H_2O}Hs_{H_2O}$

Water film at wall is used to store mass/energy, but does not effect fluid behavior $(T_{film} = T_{wall})$



Implementation (3/4)

```
fvScalarMatrix YiEqn
Add mass source term S_{m,i} to pressure,
density, component equations
                                             fvm::ddt(rho, Yi)
                                               + mvConvection->fvmDiv(phi, Yi)
 fvScalarMatrix rhoEqn
                                               - fvm::laplacian(gammaEff, Yi)
     fvm::ddt(rho)
                                                 reaction.R(Yi)
   + fvc::div(phi)
                                               + fvOptions(rho, Yi)
                                               + filmMassSource
     fvOptions(rho)
                                             );
   + filmMassSource
 );
                                             fvScalarMatrix p_rghEqn
                                                 p_rghEqnComp + p_rghEqnIncomp
                                                 filmMassSource
In OpenFOAM-7 and OpenFOAM-dev
                                               + fvOptions(psi, p_rgh,
                                             rho.name())
                                             );
```



Implementation (4/4)

Add energy source term $S_{h,i}$ to energy equation

```
fvScalarMatrix EEqn
(
    fvm::ddt(rho, he) + fvm::div(phi, he)
    + fvc::ddt(rho, K) + fvc::div(phi, K)
...
    - fvm::laplacian(turbulence.alphaEff(), he)
==
        rho*(U&g)
...
    + fvOptions(rho, he)
    + filmEnergySource
);
```



Energy conservation at the wall (1/2)

$$q_{fluid} = \Delta_{fluid} \kappa_{fluid,eff} (T_{fluid,c} - T_f)$$

$$q_{solid} = \Delta_{wall} \kappa_{wall} (T_{solid,c} - T_f)$$

$$q_{cond} = \dot{m}_{H_2O}L$$

$$q_{film} = \frac{m_{film}}{A_f \Delta t} c_p \left(T_{film}(t) - T_{film}(t - \Delta t) \right)$$

$$= \frac{m_{film}}{A_f \Delta t} c_p \left(T_f - T_f (t - \Delta t) \right)$$

$$q_{fluid} + q_{cond} + q_{solid} - q_{film} = 0$$

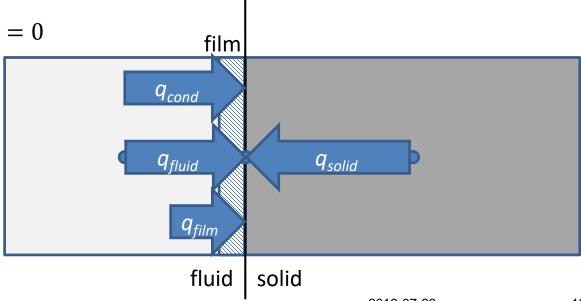
 $\Delta = \frac{1}{y}$, inverse wall distance of cell center

 κ , thermal conductivity

L, latent heat

 A_f , face area

 Δt , time step size





Energy conservation at the wall (2/2)

Sort for T_f , T_c , T_r , $\nabla_{\perp}T$

$$T_f = \mathbf{w}T_r + (1 - \mathbf{w})(T_c + \nabla_{\perp}Ty)$$

$$w = \frac{\Delta_{wall} \kappa_{wall} + \frac{m_{film}}{A_w \Delta t} c_p}{\Delta_{fluid} \kappa_{fluid,eff} + \Delta_{wall} \kappa_{wall} + \frac{m_{film}}{A_w \Delta t} c_p}$$

$$T_r = \frac{\Delta_{wall} \kappa_{wall} T_{solid,c} + \frac{m_{film}}{A_w \Delta t} c_p T_p (t - \Delta t) + \dot{m}_i L}{\Delta_{wall} \kappa_{wall} + \frac{m_{film}}{A_w \Delta t} c_p}$$

$$\nabla_{\perp}T = 0$$



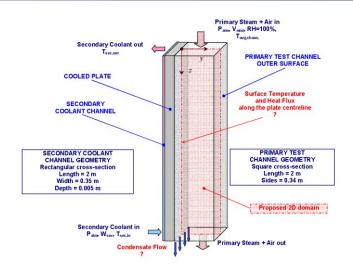
Verification

- OpenFOAM function objects (and swak4foam):
 - patch/wall fluxes
 - integrated values
 - Probes
- Jupyter notebook to visulize results

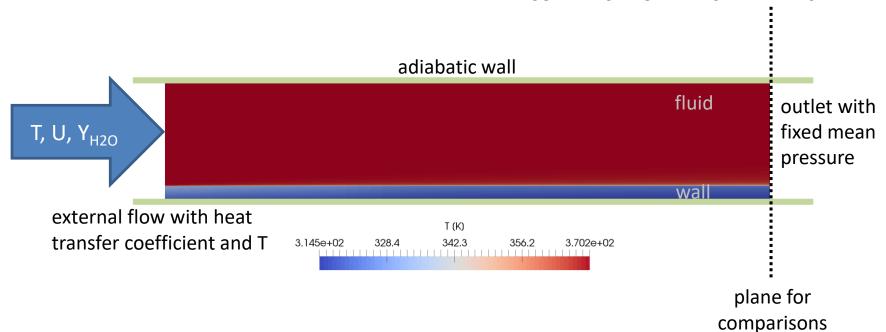


Test Case: Conan Sarnet-Benchmark

- Channel flow with cooled wall
- 2D simulation with modified chtMultiRegionFoam solver (OF-6)



Ambrosini et al., SARnet-2 CONDENSATION BENCHMARK No. 2





Walk through code

https://github.com/jmozmoz/OFdevelopments/tree/master/wallCondensationCoupled

- create a boundary condition derived for the OpenFOAM class
 mixedFvPatchScalarField
 (based on turbulentTemperatureRadCoupledMixedFvPatchScalarField)
- create fvOptions derived source terms
- access all necessary fluid and wall fields and properties at the surface
- functions objects in test case
- Python and the libraries pandas, numpy, and matplotlib for postprocessing



How to access fields in boundary conditions (1/2)

E.g. temperture boundary condition:

- Fields on the patch
 - T^{*} *this
 - other scalar fields: const fvPatchScalarField& patchField = patch().lookupPatchField<volScalarField, scalar>(fieldName);
- fields in cells next to patch const fvPatchScalarField& patchInternalField = patchField.patchInternalField()
- fields in full mesh (including cells next to patch) const volScalarField& meshField =

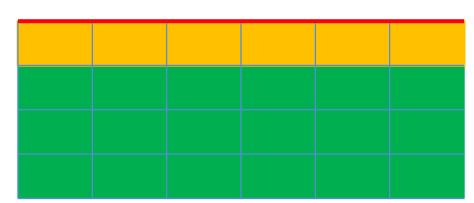
```
static_cast<const volScalarField&>(patchField.internalField());
```



How to access fields in boundary conditions (2/2)

Finding patchInternalField in full mesh:

```
const labelList& faceCells = patch().faceCells();
forAll(faceCells, faceI)
{
    const label cellI = faceCells[faceI];
    meshField[cellI] == patchInternalField[faceI]; // true!
}
```





Code: Heat release at wall

```
void wallCondensationCoupledMixedFvPatchScalarField::updateCoeffs()
                const scalar YsatFace = pSatFace/pFace*Mv/Mcomp_;
                const scalar gamma = muCell + mutFace / Sct;
                // mass flux [kg/s/m^2]
                // positive if mass is condensing
                dm[faceI] =
                    gamma*deltaFace
                   *(Ycell - YsatFace)/(1 - YsatFace);
// Heat flux due to change of phase [W/m2]
        dmHfg = dm*hPhaseChange;
        dHspec = dm*hRemovedMass;
        forAll(faceCells, faceI)
        {
            const label cellI = faceCells[faceI];
            filmMassSource[cellI] =
               -dm[faceI]
               *magSf[faceI]
               /mesh.cellVolumes()[cellI];
            filmEnergySource[cellI] =
               -dm[faceI]*hRemovedMass[faceI]
               *magSf[faceI]
               /mesh.cellVolumes()[cellI];
```



Code: Source terms using fvOptions

```
Foam::fv::wallCondensationSource::wallCondensationSource(
   const basicThermo& thermo =
       mesh_.lookupObject<basicThermo>(basicThermo::dictName);
   fieldNames_.setSize(3);
   fieldNames [0] = thermo.he().name();
   fieldNames [1] = specieName ;
   fieldNames [2] = "rho";
     fieldNames_[3] = "p_rgh"; // we do not need to activate the source
//
                             // for p_rgh, because it will be activated
//
                             // automatically, if rho is active
   applied .setSize(fieldNames .size(), false);
void Foam::fv::wallCondensationSource::addSup(fvMatrix<scalar>& eqn, const label fieldi)
   eqn += filmMassSourceFluid ;
void Foam::fv::wallCondensationSource::addSup(const volScalarField& rho, fvMatrix<scalar>& eqn, const label fieldi)
   if (fieldi == 0)
       eqn += filmEnergySourceFluid_;
   else
       eqn += filmMassSourceFluid ;
```



Acknowlegments

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Supported by:



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- Involvement in development and validation of thermal hydraulics system codes (ATHLET)
- Participation in national and international test and research projects on nuclear safety simulation codes
- Safety analyses for LWR and metal-cooled reactor designs
- Presentation of work results at national and international conferences

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