

# University of Nottingham

## MM2TF2 Thermodynamics and Fluid Mechanics

### Air conditioning and refrigeration

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#### Summary

To understand air conditioning processes and the indicators of moisture and heat content of the environmental air [1]. The main objectives of this experiment were to analyse these processes using a psychrometric chart to seize the air energy and absolute humidity. Then using a p-h diagram (absolute pressure – specific enthalpy diagram) to find the energy change of refrigerant across the cooling heat exchanger.

Based off the findings from the experiment the theoretical data did not quite match the experimental data that was discovered, indicating there were errors, either with equipment or the way that the data was collected. For example, the greatest contrast between the experimental data and the theoretical data was the data collected at point C (the point at where both bulbs are cooled after the first heating). The temperature of the dry and wet bulb that was recorded 15.6°C and 13.9°C respectively, whereas the temperature according to the theoretical data of the dry and wet bulb were 20.5°C and 17.5°C.

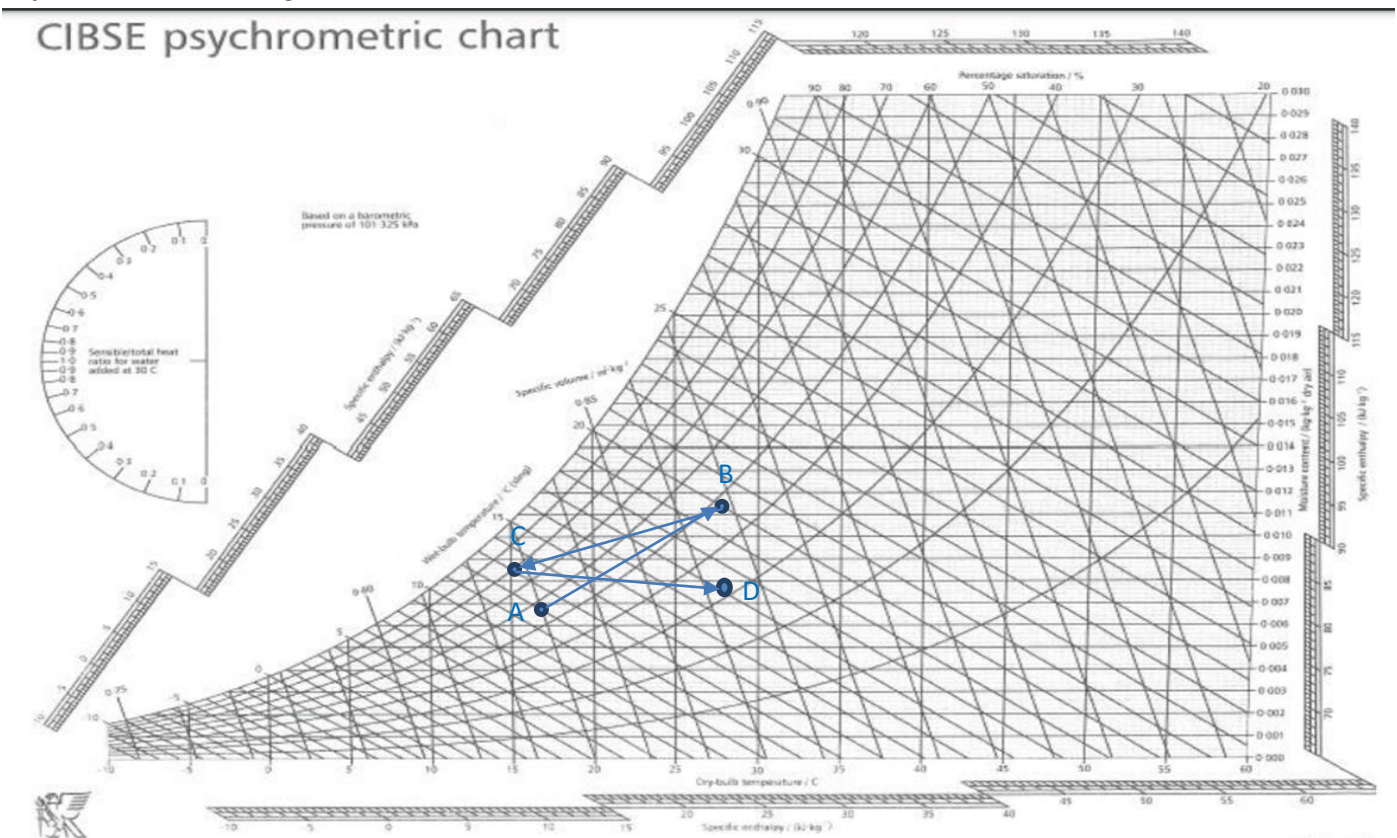
#### Results

Air side data (figure,1)

air side data	1	2	3	4	5	6	Mean	Max	Min	SD
Tdb-in	16	16.8	16.6	16.8	17.4	17	16.8	17.4	16	0.4633213
Twb-in	12.5	12	12	12	12.5	12.5	12.3	12.5	12	0.2738613
Tdb-after-heat	28	26	28.5	28	28.8	28.5	28	28.8	26	1.0132456
Twb-after-heat	20.8	20.4	21	20	20	20.8	20.5	21	20	0.4335897
Tdb-after-cool	14.5	16	16	15	16	16	15.6	24.1	21.4	0.6645801
Twb-after-cool	14	14.5	14	13	14	14	13.9	14.5	13	0.491596
Tdb-after-2nd-heat	27.8	27.6	27.8	27.8	28	28	27.8	28	27.6	0.1505545
Twb-after-2nd-heat	17.5	17.5	17	17	17.5	17.5	17.3	17.5	17	0.2581989
manometer reading	4.4	4.3	4.3	4.4	4.3	4.3	4.3	4.4	4.3	0.0516398

Figure,1 – Shows the table of air side data

### Psychrometric chart (Figure, 2)



Figure, 2 shows the four different thermometer points as mean values

### Air side theoretical data (figure,3)

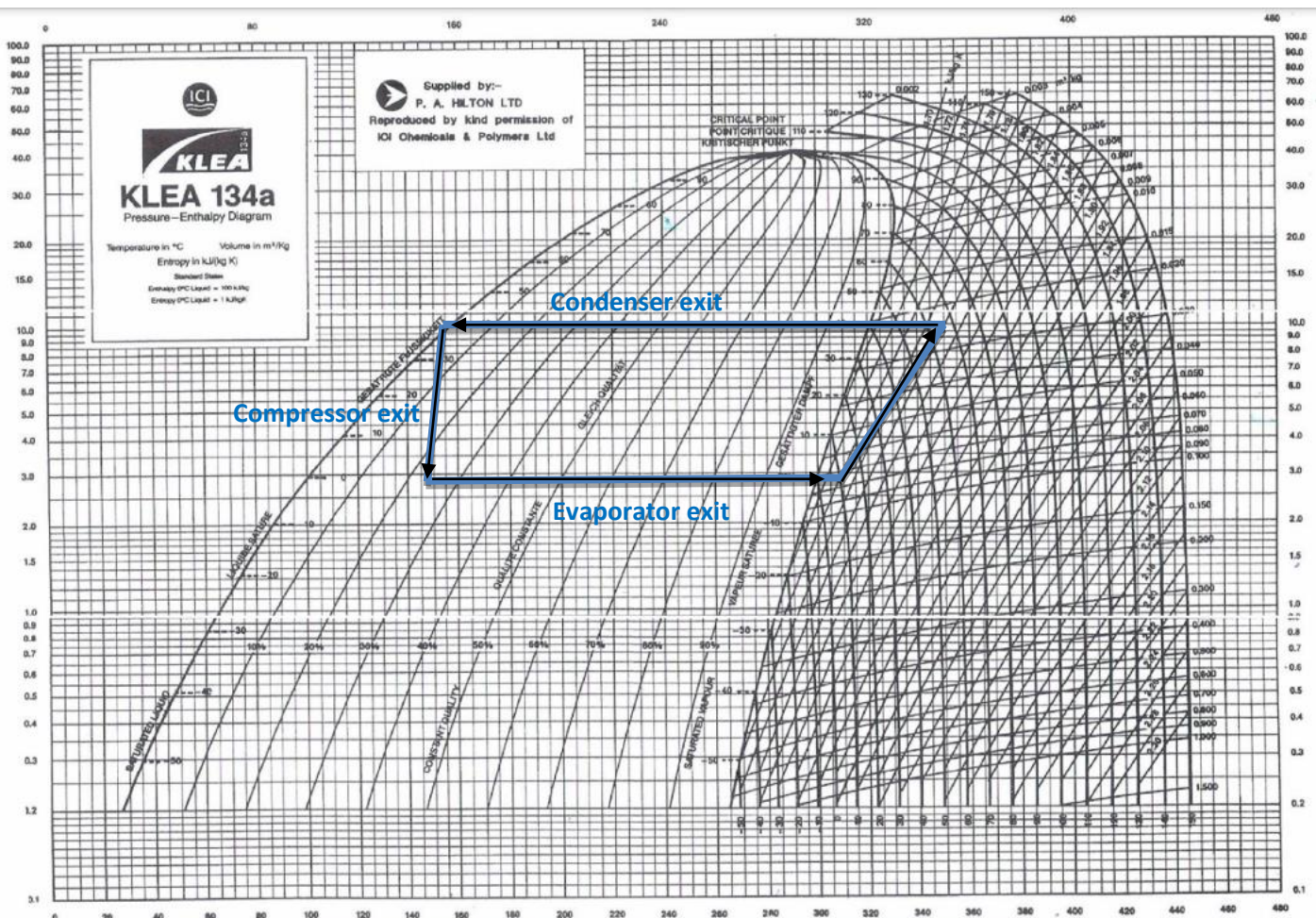
Point	Dry bulb Temperature (°C)	Wet bulb Temperature (°C)	Enthalpy ( $KJ/kg^{-1}$ )
A	24	17	46
B	34.5	23.5	69
C	20.5	17.5	48
D	31.5	20	56.5

### Refrigerator Data (Figure, 4)

Refrigerator data	1	2	3	4	5	6	Mean	Max	Min	SD
T-evap out	9	9	8	9	9	9	8.825048	9	8	0.408248
T-compressor out	69	68	68	69	69	69	68.66504	69	68	0.516398
T-condenser out	33	33	33	33	33	33	33	33	33	0
p-high, bar absolute	10	10	10	10	10	10	10	10	10	0
p-low, bar absolute	2.9	2.8	2.8	2.8	2.8	3	2.848996	3	2.8	0.083666
Refrigerator mass	11	11.3	11.2	11.5	11.3	11.2	11.249	16	11	0.164317
condensate collection	205	135	100	103	510	150	167.1467	510	100	156.3698
condensate collection time	9.3	6.2	4.4	5	25.2	4	7.097842	25.2	4	8.155101

Figure,4 – Shows the table of refrigerator data

### Refrigerator cycle Pressure-Enthalpy diagram (Figure, 5)



### Refrigerator theoretical data (figure,6)

Process	Temperature (°C)	Pressure 9 bar abs)
Evaporator exit	10	3
Compressor exit	70	10
Condenser exit	40	saturated
Enthalpy across evaporator ( $KJ Kg^{-1}$ )	Mass flux of refrigerant ( $Kgs^{-1}$ )	Cooling (KW)
307-157	0.015	2.25

## Calculations

### Mass flow rate of air

$\Delta z$  = Mean manometer reading = 4.3mm

$V_d$  = Specific volume of air =  $0.79 m^3 Kg^{-1}$

$$\dot{m}(\text{humid air}) = 0.0517 \sqrt{\frac{\Delta z}{V_d}} \text{ therefore}$$

$$\dot{m}(\text{humid air}) = 0.0517 \sqrt{\frac{4.3}{0.79}} = 0.121 Kg s^{-1}$$

### Enthalpy Calculations

Enthalpy for points A and B =  $\Delta h = 53 - 36 = 17 KJ Kg^{-1}$

### Energy calculation

$$\dot{Q} = \dot{m} \times \Delta h = 0.121 \times 17 = 2.01 KW$$

### Condensate calculation

$$\dot{m} - \text{condensate} = \frac{\text{amount collected (g)}}{\text{time (s)}} = \frac{167.1467}{7.097842} = 23.55 g s^{-1}$$

$$\dot{m} - \text{condensate} = \dot{m} - \text{air} (\omega_2 - \omega_1) = 0.121 \times (0.0118 - 0.0088) \times 1000 = 0.363 g s^{-1}$$

$$\dot{m} - \text{condensate} = \dot{m} - \text{air} (\omega_2 - \omega_3) = 0.121 \times (0.0118 - 0.010) \times 1000 = 0.218 g s^{-1}$$

## Discussion

First, it's important to note that the main aim of this experiment "To understand air conditioning processes and the indicators of moisture and heat content of the environmental air" [1]. Secondly when looking at the theory behind this experiment it states that the temperature of the wet bulb should be lower than the temperature of the dry bulb, this is because there is evaporation when the relative humidity is not 100%. As a result of this evaporation the wet bulb would have a lower temperature.

From figure 1, you can see the different points at which the temperature was measured from the rig and its corresponding humidity at each point. For example, from figure 1 you can see the humidity rise due to the addition of heat and steam from points A to B. Furthermore, from points B to C you can see the cooling of the air therefore

there's a steep decrease in the temperature of the air. Finally, from points C to D you can see a slight decrease in humidity as well as a slight increase in temperature.

It's important to compare the experimental data to the theoretical data as these differences could indicate possible errors. As with any experiment there is a degree of error and uncertainty, some of which you can control and others which you cannot control. For example, a systematic error that could have interfered with the data collection was the reading of the thermometers because they tend to fluctuate quite as well as the readings on them were quite hard to see resulting in less accurate data collection therefore there was also room for human error. To reduce the uncertainty of my data collection as much as possible, 6 results for each variable were measured and a mean was taken, the instruments used in the experiment also had uncertainties for example, the thermometers had an uncertainty value that ranged between  $\pm 0.1$  and  $\pm 1$  depending on the thermometer used from the rig. The condensate collection had an uncertainty of  $\pm 5$ , the manometer had an uncertainty of  $\pm 0.1$  and finally the uncertainties of the collection time and refrigerant mass rate were both  $\pm 1$ .

## Conclusion

Since the experiment was conducted in a control environment it is clear the lab was in fact atmospheric, the rig also showed how the behaviour of air changed after the addition of steam or cooling of the air which is demonstrated by figure 1. Furthermore, from the data collected and the extrapolation of this data you can see the refrigerant cycle as stated in the theory [1] as well as the thermodynamic principles that cause this cycle. Overall, the aims of this experiment were met as the rig did decrease the temperature of the air as it entered through the heat exchange of the refrigerant.

## References

[1] - file:///C:/Users/Local%20Administrator/OneDrive%20-%20The%20University%20of%20Nottingham/Year%202/Thermo/air%20conditioning%20lab/Air-conditioning2021.pdf