

# Computational Fluid Dynamics: The Finite-Volume Method

David Apsley



# 1. Introduction

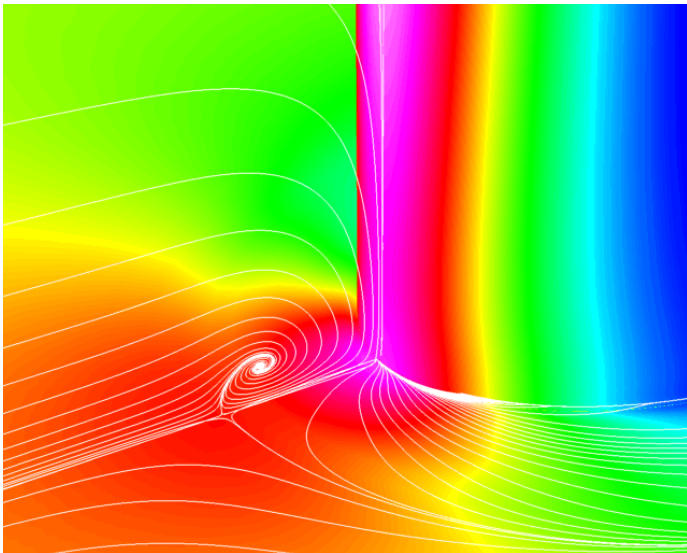
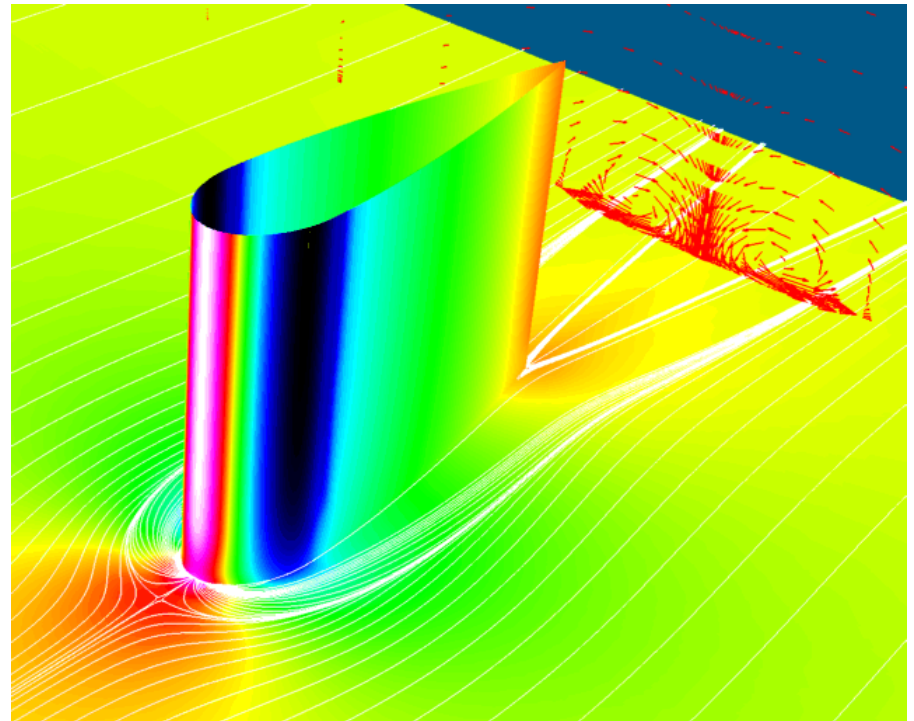
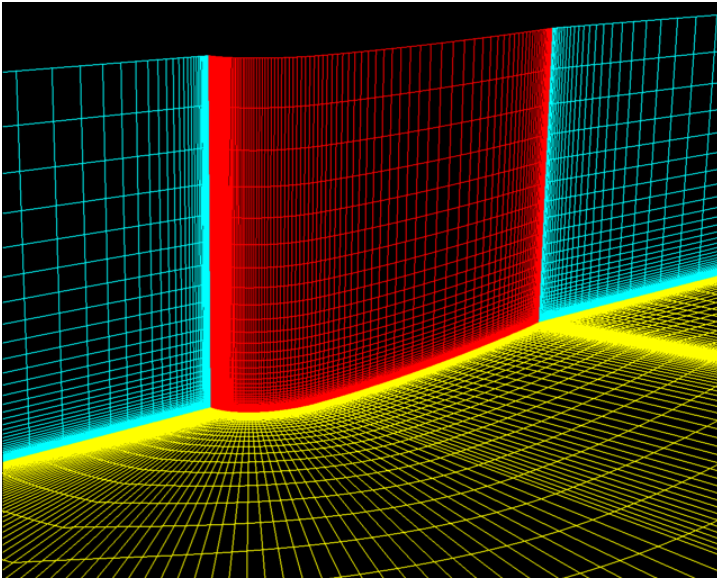


# What is ... Computational Fluid Dynamics?

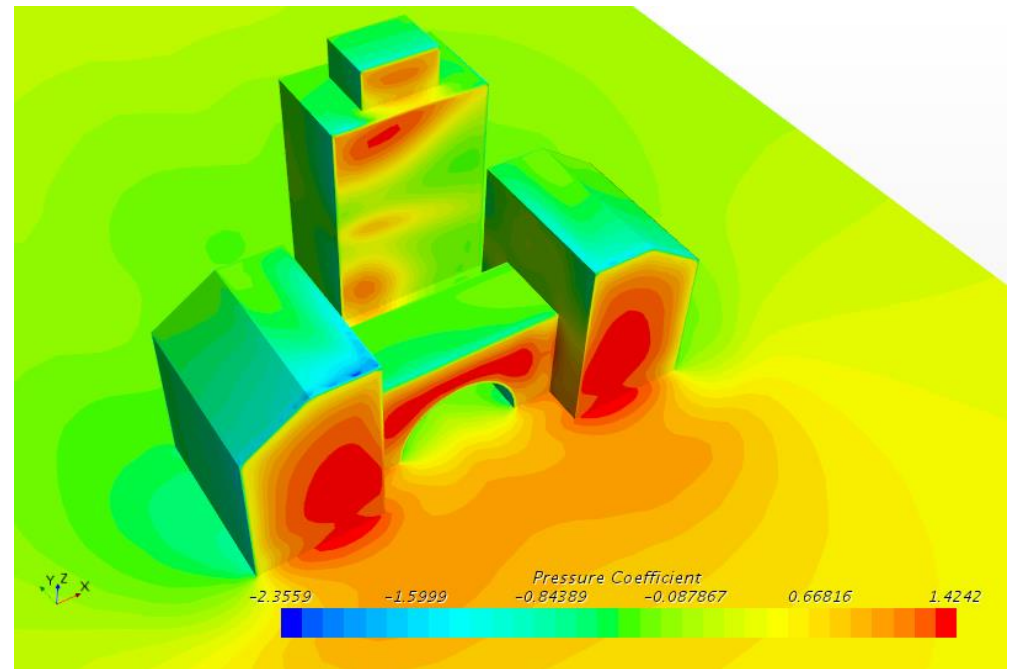
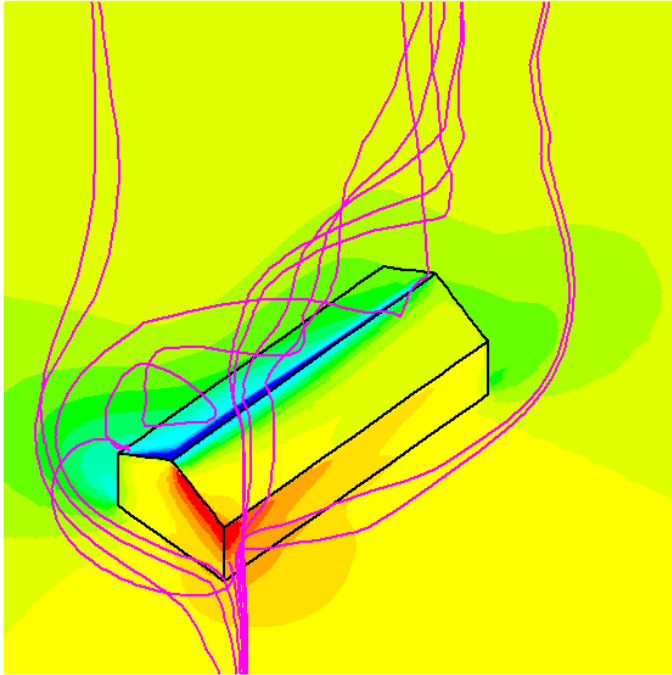
*The use of computers and  
numerical methods to solve  
problems involving fluid flow*



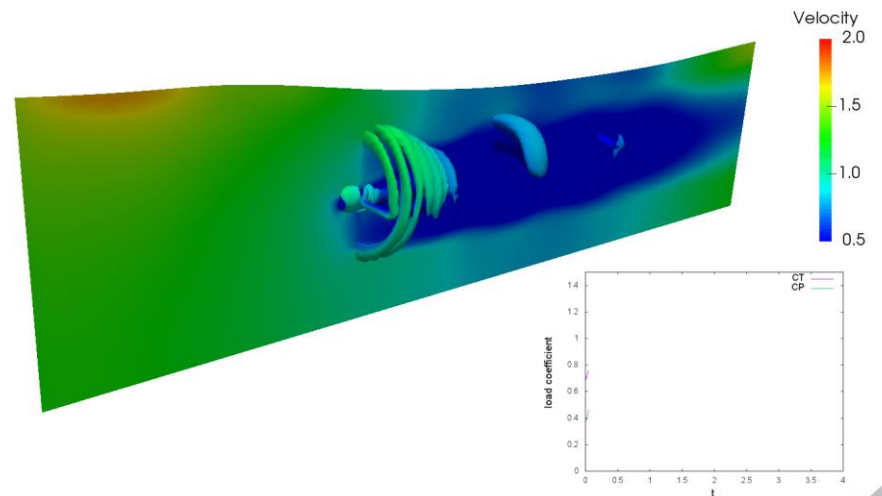
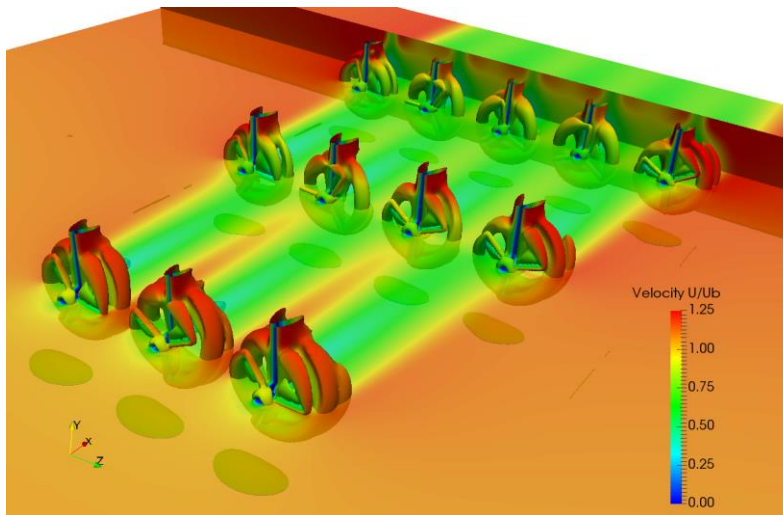
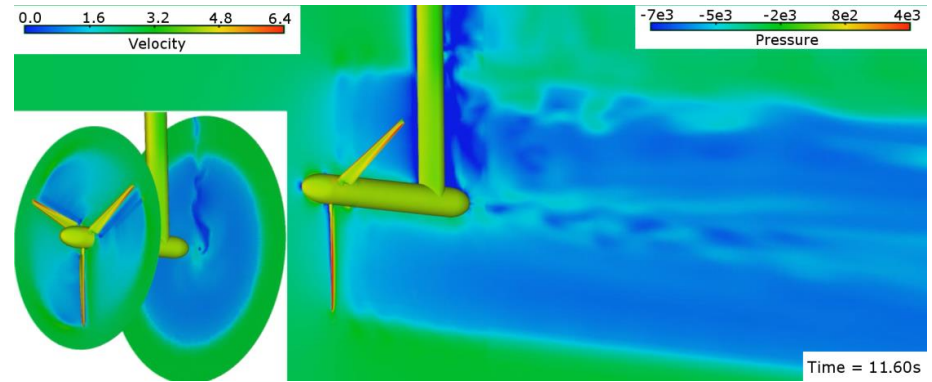
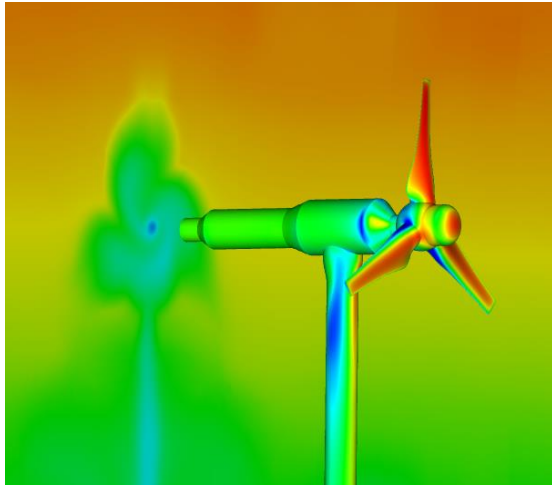
# Aerodynamics



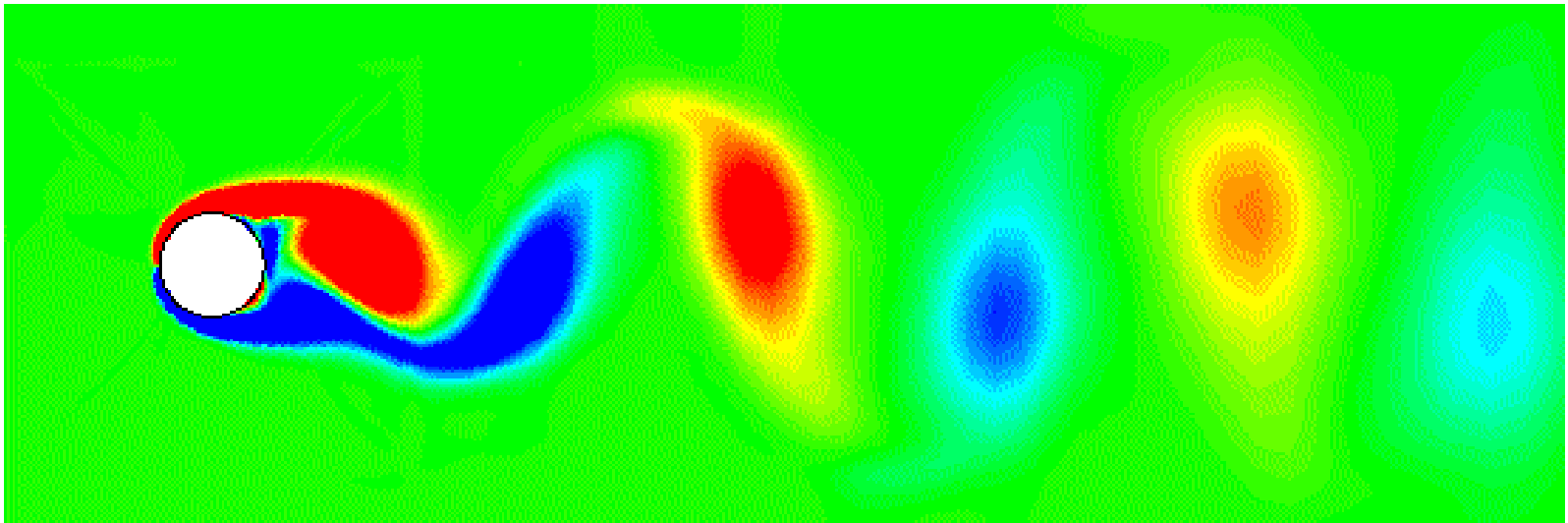
# Wind Loading



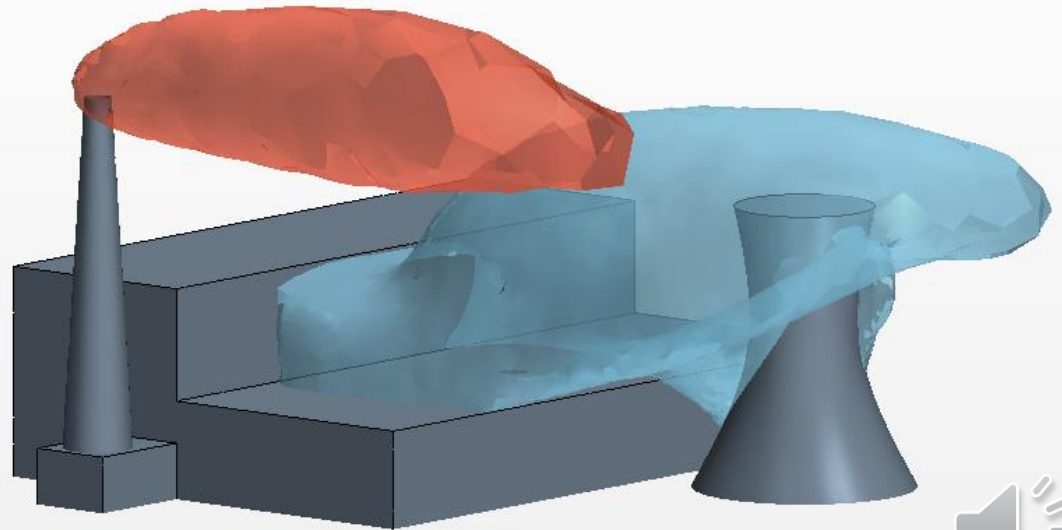
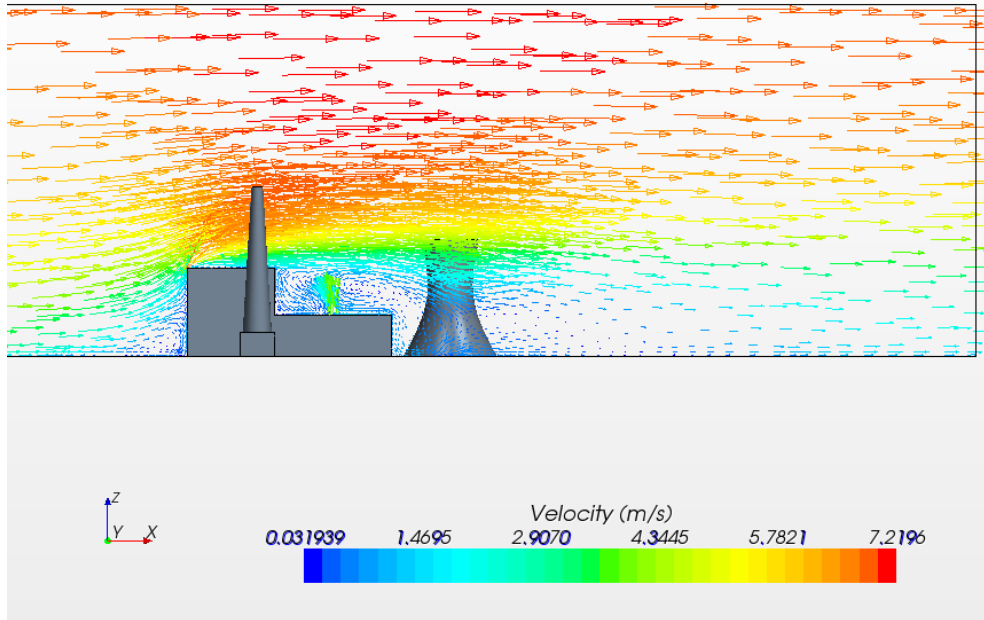
# Turbine Technology



# Vortex Shedding

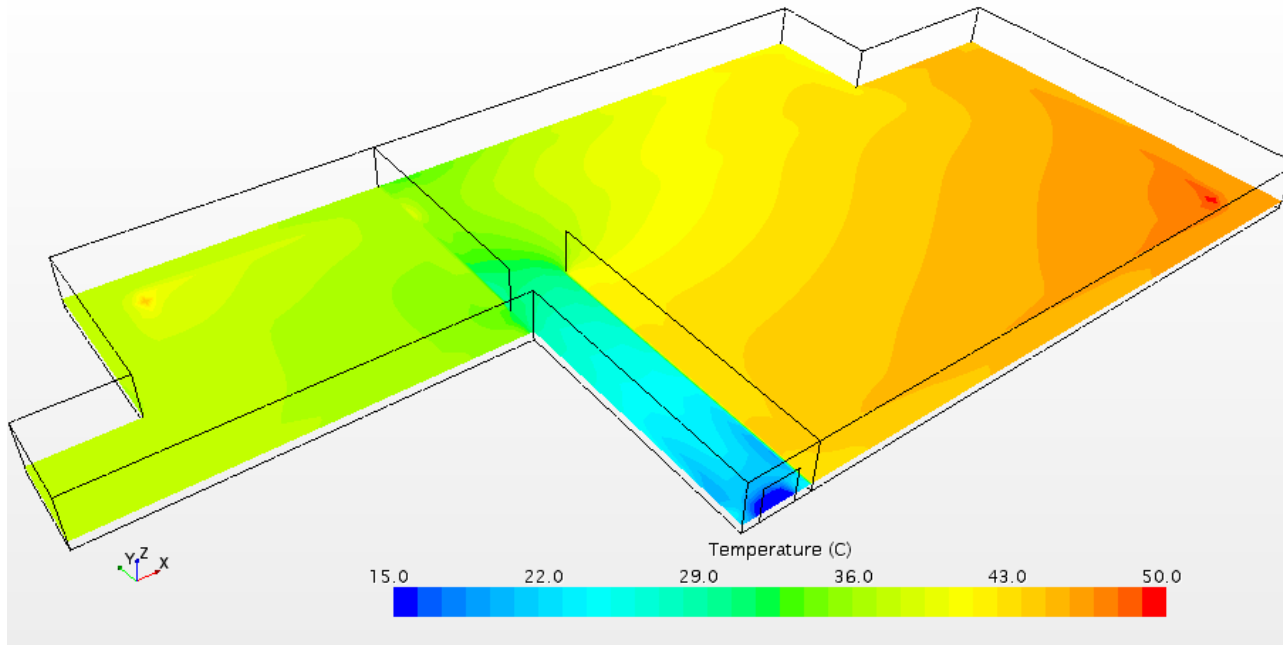
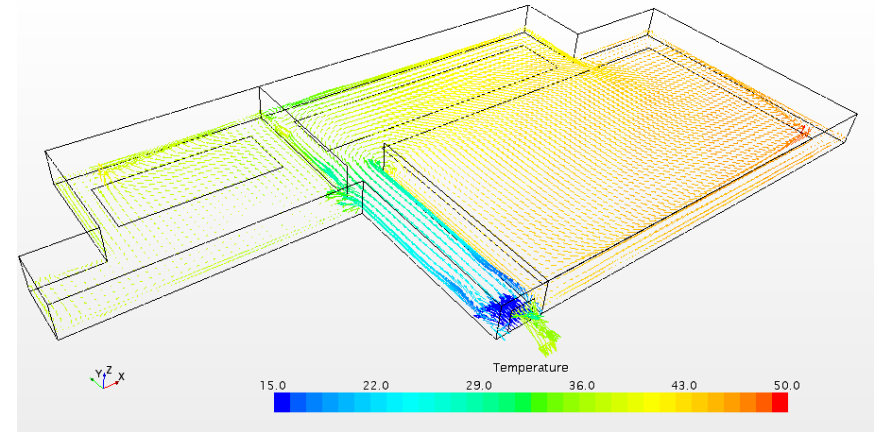
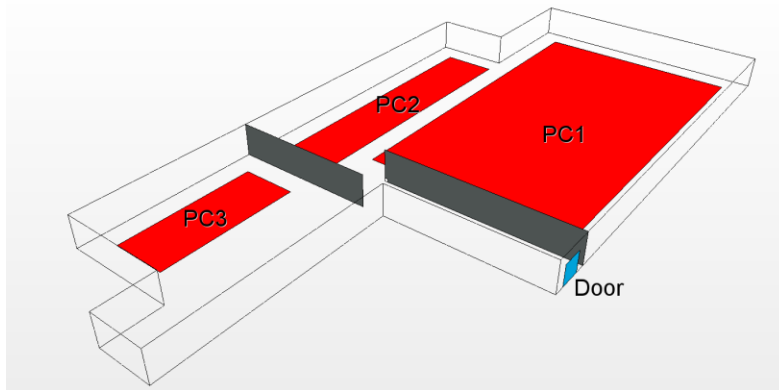


# Dispersion of Pollution



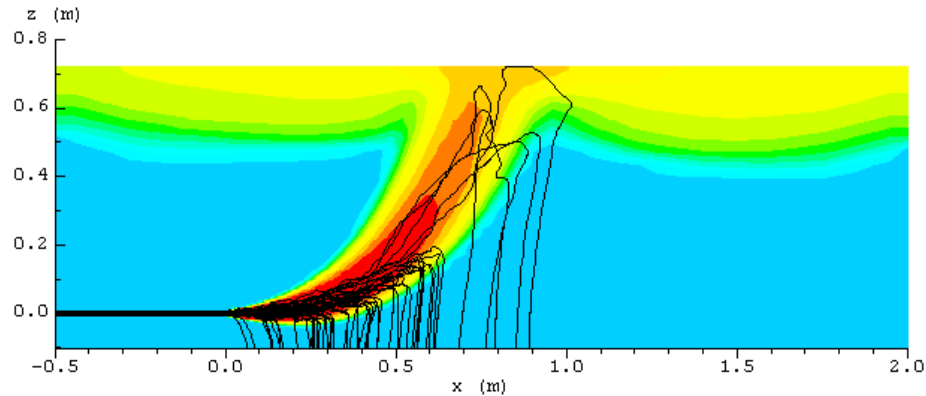


# Ventilation

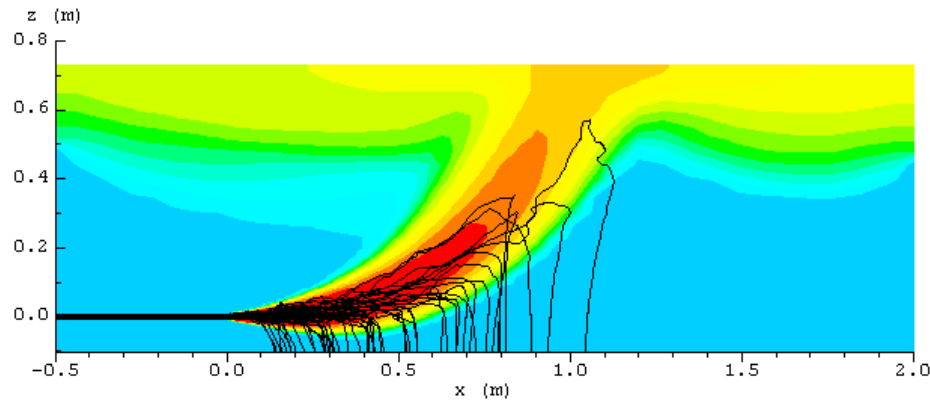


# Particle-Laden Plumes (Sea Outfalls)

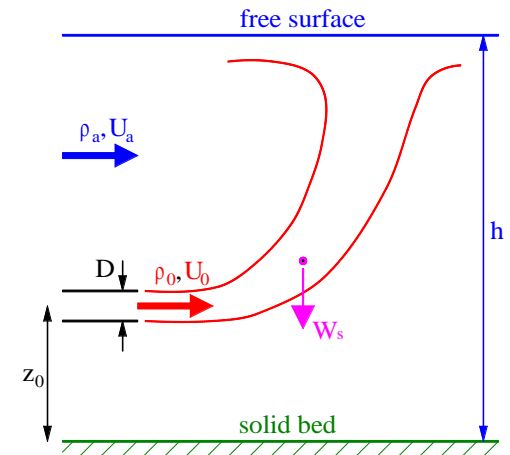
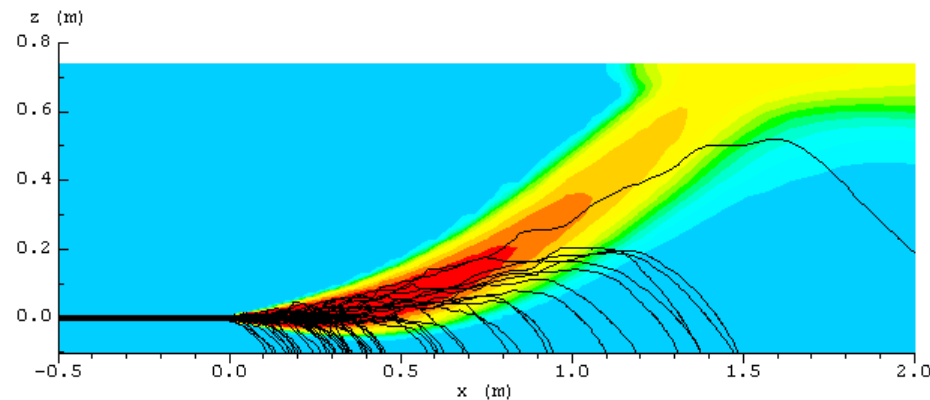
(ex302)  
 $\rho_a = 1040 \text{ kg/m}^3$



(ex322)  
 $\rho_a = 1020 \text{ kg/m}^3$

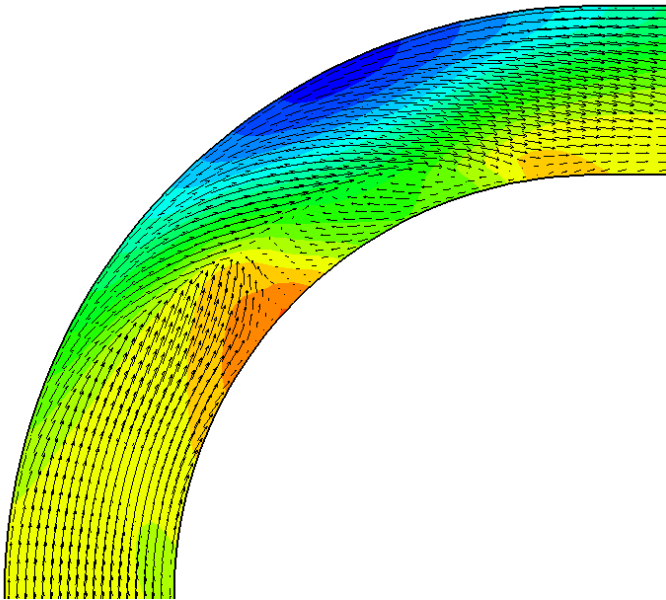


(ex336)  
 $\rho_a = 1020 \text{ kg/m}^3$   
 $U_a = 0.026 \text{ m/s}$

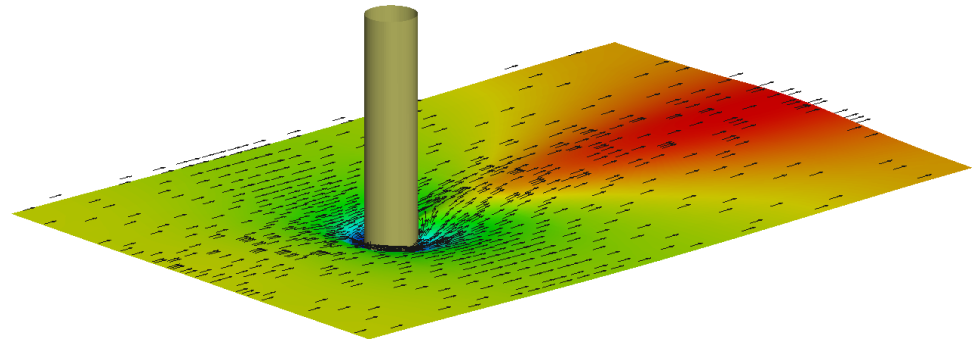


# Sediment Scour

River bend

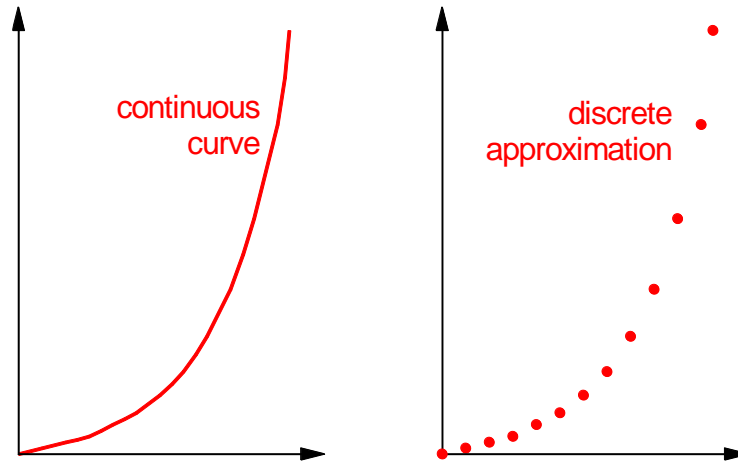


Bridge pier

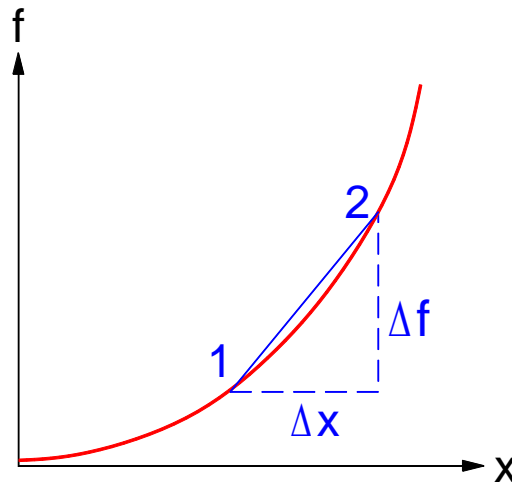


# Discretisation

Field variables:



Equations:



$$\frac{df}{dx} \approx \frac{\Delta f}{\Delta x} = \frac{f_2 - f_1}{x_2 - x_1}$$



# Basic Principles of CFD

## 1. Discretise space:

replace field variables ( $\rho, u, v, w, p, \dots$ ) by values at a finite number of **nodes**

## 2. Discretise equations:

**continuum** equations  $\rightarrow$  **algebraic** equations

## 3. Solve:

large system of **simultaneous equations**



# Stages of a CFD Analysis

- **Pre-processing:**
  - formulate problem (geometry, equations, boundary conditions)
  - construct computational mesh
- **Solving:**
  - discretise
  - solve
- **Post-processing:**
  - analyse
  - visualise (graphs and plots)



# Fluid-Flow Equations

- **Mass:** change of mass = 0
- **Momentum:** change of momentum = force  $\times$  time
- **Energy:** change of energy = work + heat
- **(Other constituents)**

In fluid mechanics, these are normally expressed in **rate** form



# Form of Equations

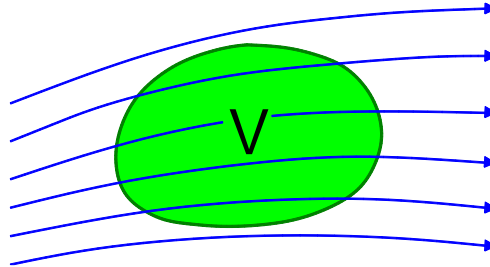
- **Integral** (control-volume)
- **Differential**





# Integral (Control-Volume) Approach

Consider the budget of **any transported physical quantity** in **any control volume**



$$\text{CHANGE} = \text{IN} - \text{OUT} + \text{CREATED}$$

$$\frac{\text{CHANGE}}{\text{time}} + \frac{\text{OUT} - \text{IN}}{\text{time}} = \frac{\text{CREATED}}{\text{time}}$$

$$\left( \begin{array}{c} \text{TIME DERIVATIVE} \\ \text{of amount in } V \end{array} \right) + \left( \begin{array}{c} \text{NET FLUX} \\ \text{through boundary of } V \end{array} \right) = \left( \begin{array}{c} \text{SOURCE} \\ \text{inside } V \end{array} \right)$$

$$\left( \begin{array}{c} \text{TIME DERIVATIVE} \\ \text{of amount in } V \end{array} \right) + \left( \begin{array}{c} \text{ADVECTION + DIFFUSION} \\ \text{through boundary of } V \end{array} \right) = \left( \begin{array}{c} \text{SOURCE} \\ \text{inside } V \end{array} \right)$$

→ **Finite-volume** method for CFD



# Differential Equations For Fluid Flow

- Derived by considering the rate of change **at a point**; i.e. using **infinitesimal control volumes**
- Discretisation gives a **finite-difference** method for CFD
- Several types:
  - fixed-point (“Eulerian”): **conservative**
  - moving with the flow (“Lagrangian”): **non-conservative**
  - **derived variables**; e.g. potential flow

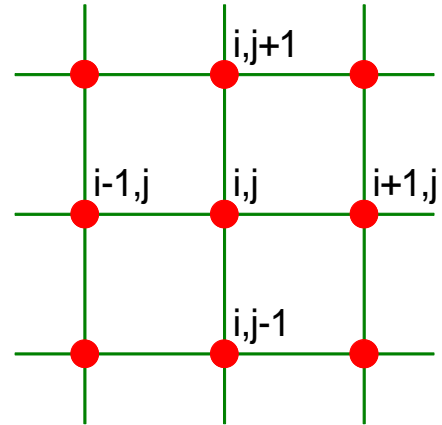


# Main Methods for CFD

- **Finite-difference:**

- discretise **differential** equations

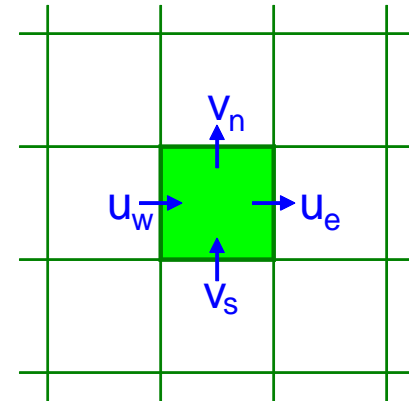
$$0 = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} \approx \frac{u_{i+1,j} - u_{i-1,j}}{2\Delta x} + \frac{v_{i,j+1} - v_{i,j-1}}{2\Delta y}$$



- **Finite-volume:**

- discretise **control-volume** equations

$$0 = \text{net mass outflow} = (\rho u A)_e - (\rho u A)_w + (\rho v A)_n - (\rho v A)_s$$



- **Finite-element:**

- represent solution as a weighted sum of **basis functions**

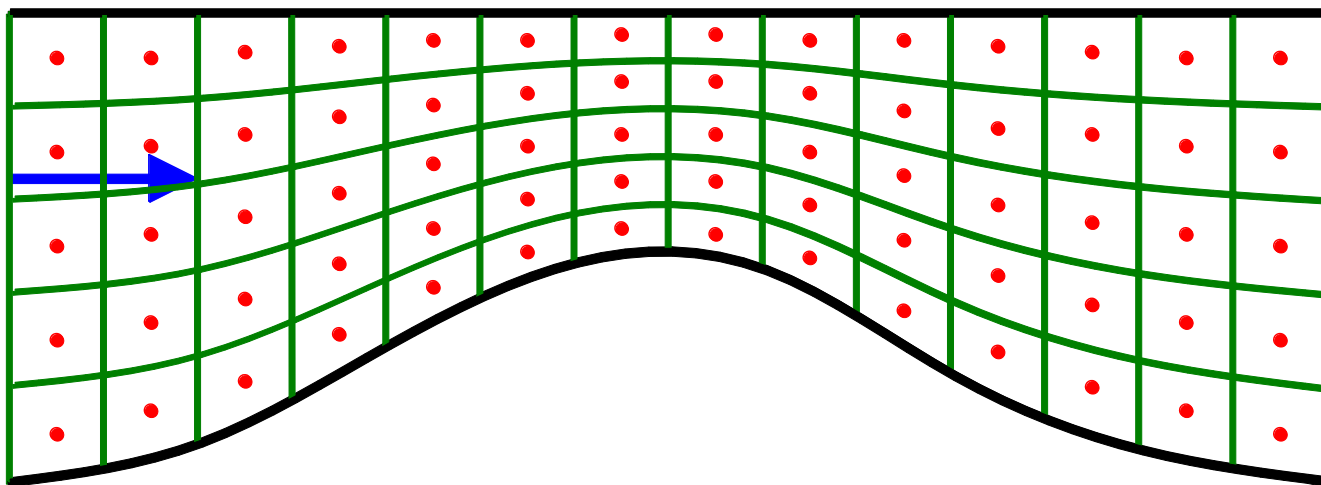
$$u(\mathbf{x}) = \sum u_{\alpha} S_{\alpha}(\mathbf{x})$$



# Advantages of the Finite-Volume Method in CFD

- Rigorously enforces **conservation**
- **Flexible** in terms of:
  - **geometry**
  - **fluid phenomena**
- Directly relatable to **physical quantities**





$$\left( \begin{array}{c} \text{red diagonal lines} \end{array} \right) \left( \begin{array}{c} \text{dashed red line} \\ \phi \end{array} \right) = \left( \begin{array}{c} \text{dashed red line} \\ b \end{array} \right)$$

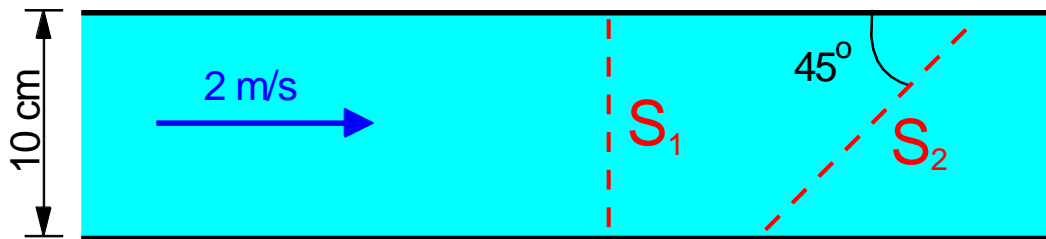


# Examples

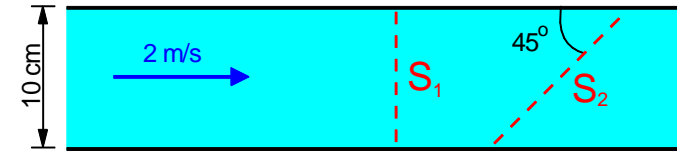


## Example Q1

Water (density  $1000 \text{ kg m}^{-3}$ ) flows at  $2 \text{ m s}^{-1}$  through a circular pipe of diameter  $10 \text{ cm}$ . What is the mass flux  $\dot{C}$  across the surfaces  $S_1$  and  $S_2$ ?



Water (density  $1000 \text{ kg m}^{-3}$ ) flows at  $2 \text{ m s}^{-1}$  through a circular pipe of diameter  $10 \text{ cm}$ . What is the mass flux  $C$  across the surfaces  $S_1$  and  $S_2$ ?



$$\begin{aligned} S_1: \quad \text{mass flux } (C) &= \rho u A \\ &= 1000 \times 2 \times \frac{\pi \times 0.1^2}{4} \\ &= 15.7 \text{ kg s}^{-1} \end{aligned}$$

$$\begin{aligned} S_2: \quad \text{the same!} \quad C &= \rho(u \cos \theta) A \\ C &= \rho u (A \cos \theta) \end{aligned}$$

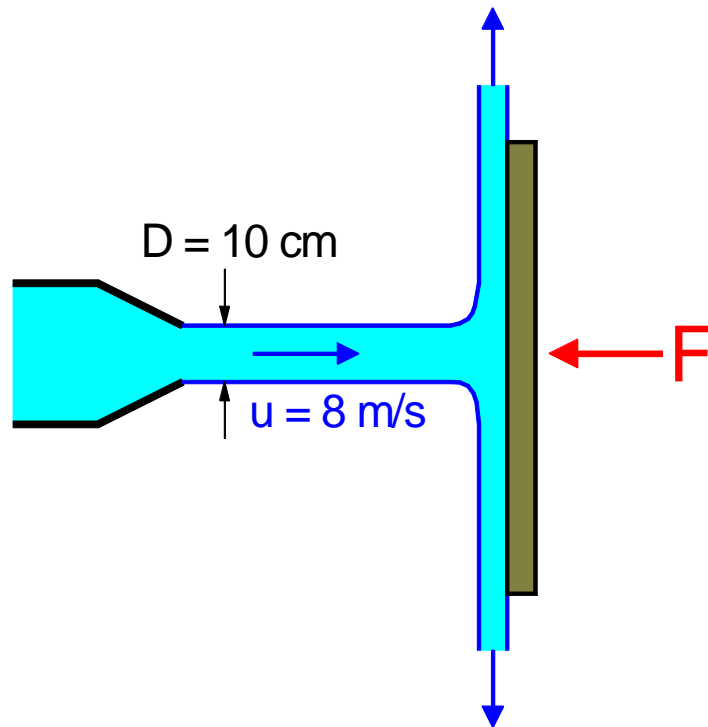
In general:  $C = \rho \mathbf{u} \cdot \mathbf{A}$



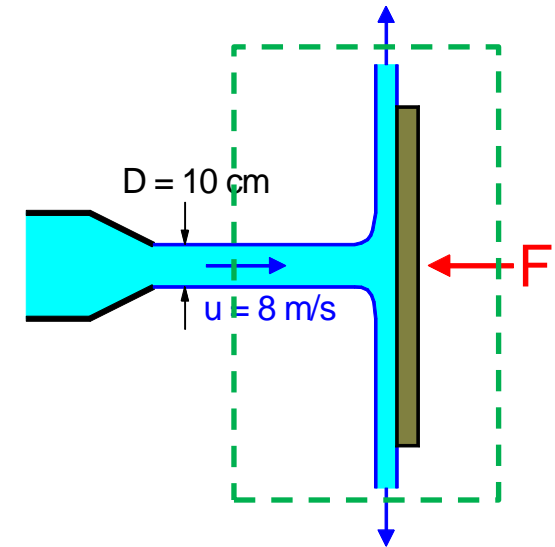


## Example Q2

A water jet strikes normal to a fixed plate as shown. Compute the force  $F$  required to hold the plate fixed.



A water jet strikes normal to a fixed plate as shown. Compute the force  $F$  required to hold the plate fixed.



$$\text{force (on fluid)} = (\text{momentum flux})_{\text{out}} - (\text{momentum flux})_{\text{in}}$$

$$\text{momentum flux} = \text{mass flux} \times \text{velocity}$$

$$-F = 0 - (\rho UA)U$$

$$F = \rho U^2 A$$

$$= 1000 \times 8^2 \times \frac{\pi \times 0.1^2}{4}$$

$$= 503\text{ N}$$



## Example Q3

An explosion releases 2 kg of a toxic gas into a room of dimensions  $30\text{ m} \times 8\text{ m} \times 5\text{ m}$ . Assuming the room air to be well-mixed and to be vented at a speed of  $0.5\text{ m s}^{-1}$  through an aperture of area  $6\text{ m}^2$ , calculate:

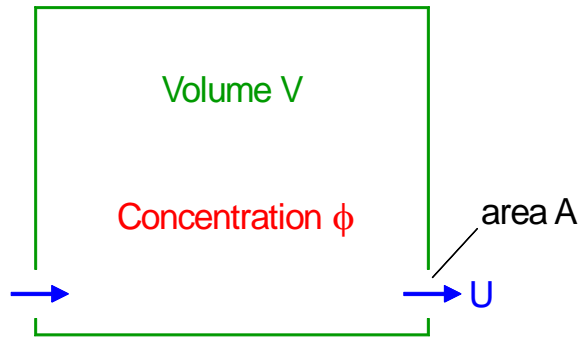
- (a) the initial concentration of gas in ppm by mass;
- (b) the time taken to reach a safe concentration of 1 ppm.

(Take the density of air as  $1.2\text{ kg m}^{-3}$ .)



An explosion releases 2 kg of a toxic gas into a room of dimensions 30 m × 8 m × 5 m. Assuming the room air to be well-mixed and to be vented at a speed of 0.5 m s<sup>-1</sup> through an aperture of area 6 m<sup>2</sup>, calculate:

(a) the initial concentration of gas in ppm by mass;



$$V = 30 \times 8 \times 5 = 1200 \text{ m}^3$$

mass of fluid  $\times$  concentration = mass of toxin

$$(\rho V)\phi_0 = 2 \text{ kg}$$

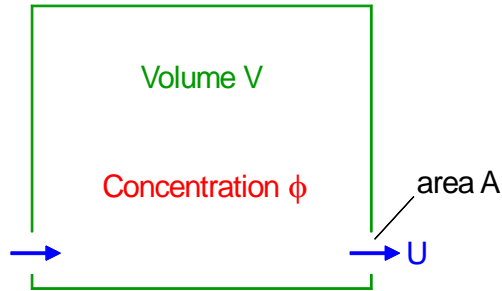
$$\phi_0 = \frac{2}{1.2 \times 1200} = 1.389 \times 10^{-3}$$

1389 ppm



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(b) the time taken to reach a safe concentration of 1 ppm.



$$\phi_0 = 1389 \text{ ppm}$$

$$V = 1200 \text{ m}^3$$

$$A = 6 \text{ m}^2$$

$$U = 0.5 \text{ m s}^{-1}$$

Change in amount of toxin = amount in – amount out

Rate of change of amount of toxin = rate of entering – rate of leaving

$$\frac{d}{dt}(\rho V \phi) = 0 - (\rho u A) \phi$$

$$\frac{d\phi}{dt} = -\left(\frac{uA}{V}\right) \phi, \quad \phi = \phi_0 \text{ at } t = 0$$

$$\frac{d\phi}{dt} = -\lambda \phi \quad \lambda = \frac{uA}{V} = 0.0025 \text{ s}^{-1}$$

$$\phi = \phi_0 e^{-\lambda t}$$

$$e^{\lambda t} = \frac{\phi_0}{\phi}$$

$$t = \frac{1}{\lambda} \ln \frac{\phi_0}{\phi} = \frac{1}{0.0025} \ln(1389) = 2895 \text{ s}$$

$$\approx 48 \text{ min}$$

