



1D Numerical Modelling for Lithium-Sulfur Batteries

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INTRODUCTION

Li-S batteries offer high theoretical energy density & cost-effectiveness but face challenges like the shuttle effect & capacity fade. Numerical modelling is essential to better understand and tackle these challenges to maximize the potential of Li-S batteries.

Using a 1D Li-S model developed by Kumaresan [1], with the simplified precipitation/dissolution dynamics proposed by Zhang [2], a bespoke solver tailored for 0D Li-S models was overhauled and optimized to account for the complexity of spatial resolution in 1D models. The Li-S model was tested with error metrics like mass & charge conservation, as well as partial currents, & consecutive charge tests as explored by Ghaznavi & Chen [3,4,5].

NOVEL SOLVER LOGIC

The solver logic that was used to code the algorithms, including the optimized numerical methods, are described in the flow chart below:

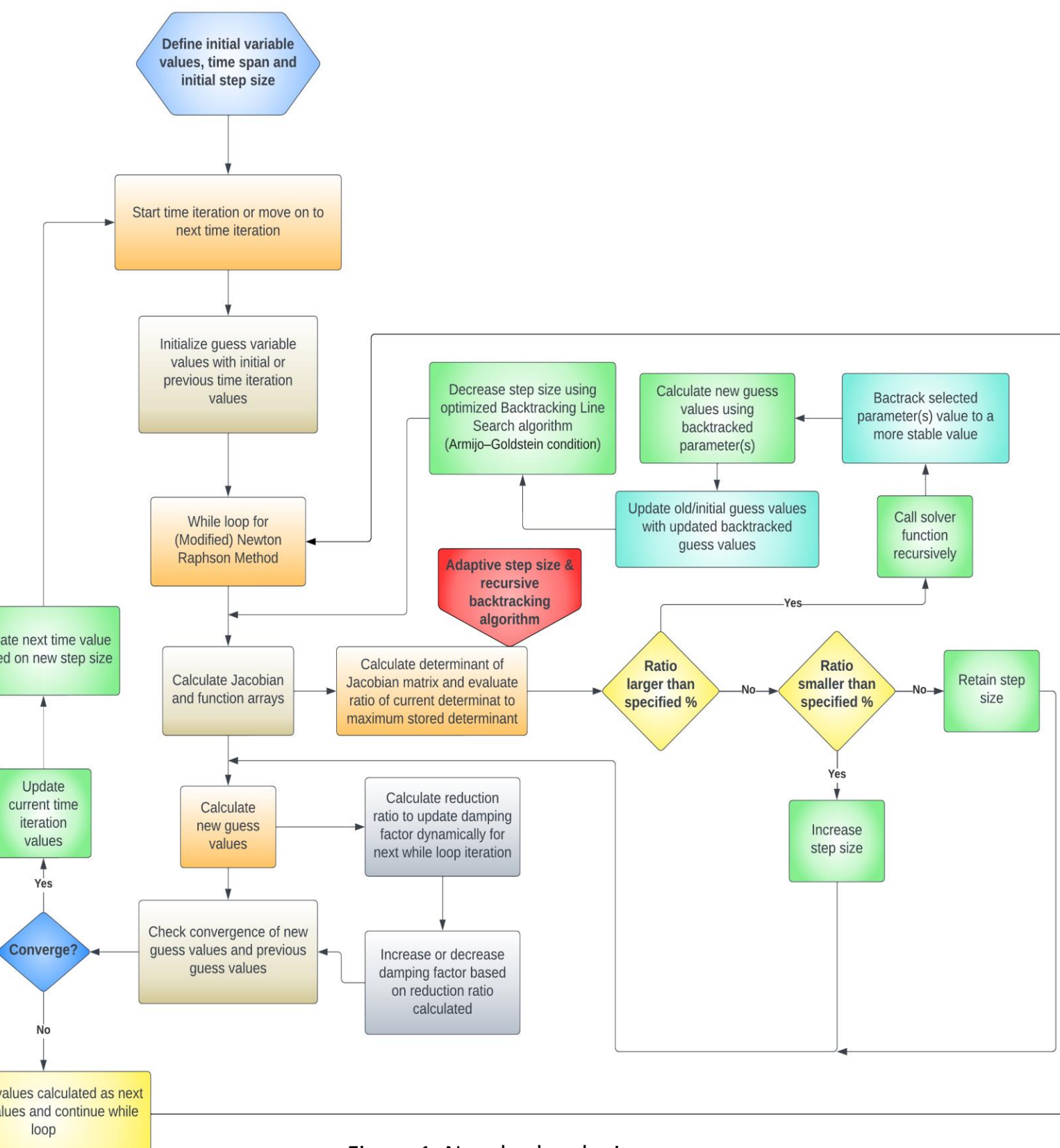
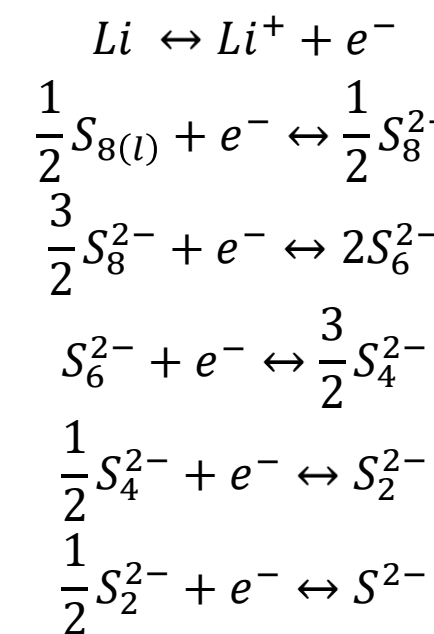


Figure 1. Novel solver logic.

1D Li-S MODEL

The 1D model is given as a 6-stage reaction, with Li electrochemistry in the anode, and a cascade reaction of polysulfide species in the cathode, given as:



EQUATIONS DISCRETISATION

The equations detailed in [1] are discretised using a Backward-Euler formulation, given by:

$$\left. \frac{df}{dt} \right|_{n+1} = \frac{f_{n+1} - f_n}{\delta t}$$

Example discretisation of the time evolution PDE of the species concentrations, C_i is given as such:

$$\frac{\partial D_i^{eff}}{\partial x} = 1.5D_i \sqrt{\epsilon_p^{m,n+1}} \left[\frac{\epsilon_p^{m+1,n+1} - \epsilon_p^{m,n+1}}{\delta x} \right]$$

$$D_i^{eff} = D_i (\epsilon_p^{m,n+1})^{1.5}$$

$$\begin{aligned} \nabla \cdot N_i &= - \left[D_i^{eff} \left(\frac{C_i^{m+1,n+1} - 2C_i^{m,n+1} + C_i^{m-1,n+1}}{\delta x^2} \right) + \left(\frac{C_i^{m+1,n+1} - C_i^{m,n+1}}{\delta x} \right) \left(\frac{\partial D_i^{eff}}{\partial x} \right) \right] \\ &- \frac{z_i F}{RT} \left[D_i^{eff} C_i^{m,n+1} \left(\frac{\phi_2^{m+1,n+1} - 2\phi_2^{m,n+1} + \phi_2^{m-1,n+1}}{\delta x^2} \right) \right. \\ &+ D_i^{eff} \left(\frac{C_i^{m+1,n+1} - C_i^{m,n+1}}{\delta x} \right) \left(\frac{\phi_2^{m+1,n+1} - \phi_2^{m,n+1}}{\delta x} \right) \\ &\left. + C_i^{m,n+1} \left(\frac{\partial D_i^{eff}}{\partial x} \right) \left(\frac{\phi_2^{m+1,n+1} - \phi_2^{m,n+1}}{\delta x} \right) \right] \end{aligned}$$

$$\begin{aligned} \frac{\partial(\epsilon C_i)}{\partial t} &= \epsilon_p^{m,n+1} \left(\frac{C_i^{m,n+1} - C_i^{m,n}}{\delta t} \right) + C_i^{m,n+1} \left(\frac{\epsilon_p^{m,n+1} - \epsilon_p^{m,n}}{\delta t} \right) \\ &= -\nabla \cdot N_i + r_i - R_i \end{aligned}$$

The system of equations are solved via a Newton-Raphson approach, where the Jacobian matrix is formed using the partial derivatives of the residual functions w.r.t the variables. (Residual functions obtained by rearranging & equating discretised equations to zero).

1D Li-S COMPUTATIONAL DOMAIN

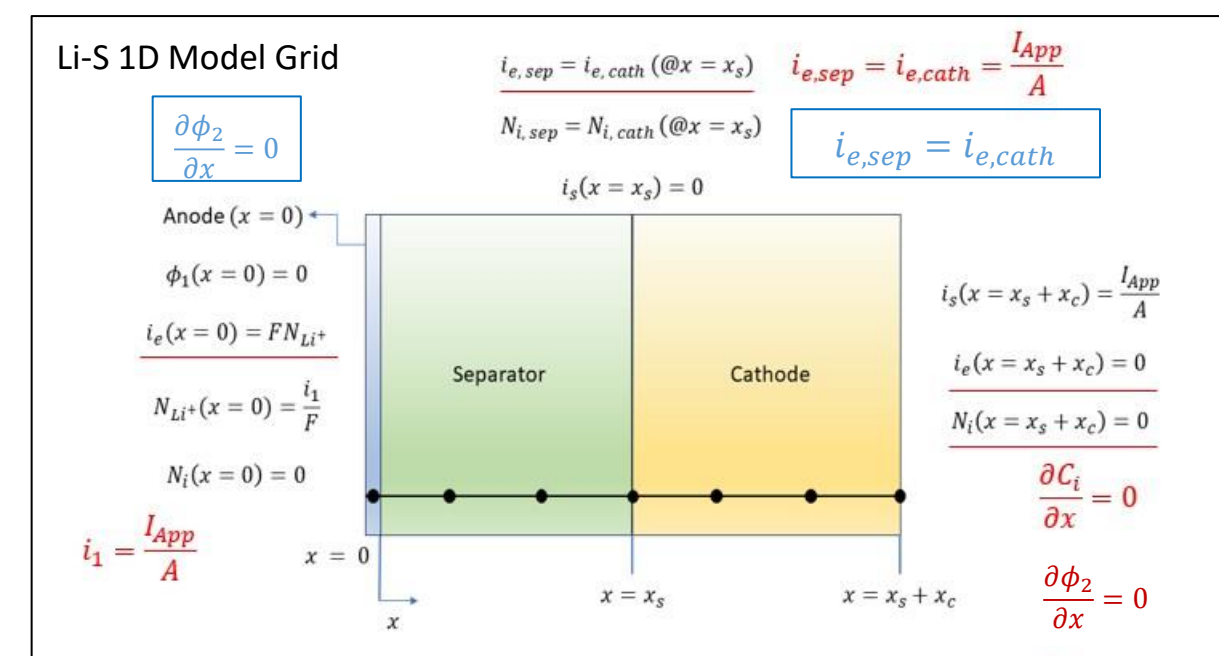


Figure 2. 1D Li-S computational domain with underlying boundary conditions.

1D Li-S MODEL WITHOUT PRECIPITATION/DISSOLUTION DYNAMICS

The precipitation/dissolution dynamics are removed to test solver validity by setting, the rate constant $k_k = 0$

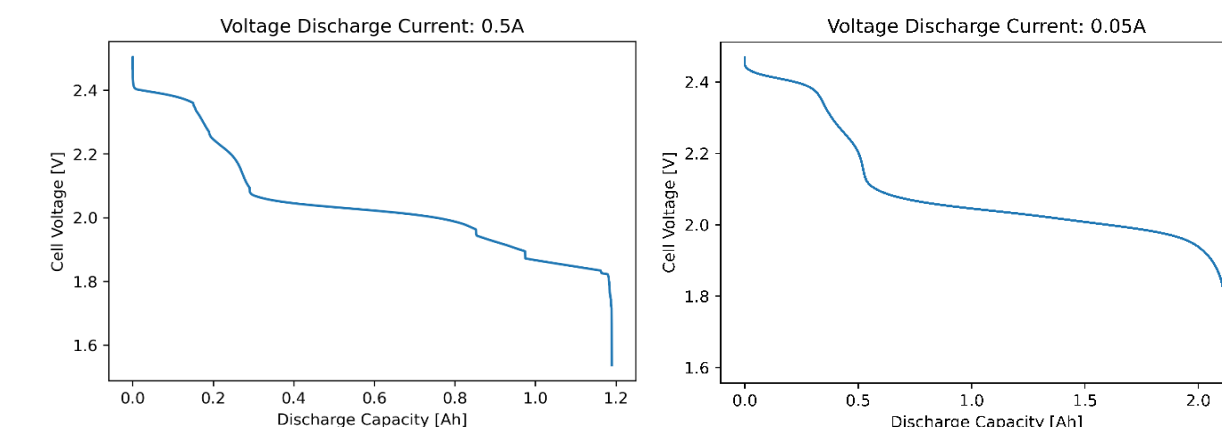


Figure 3. Voltage discharge profiles for 0.5A & 0.05A applied currents.

The cathodic species time evolution is given as:

$$C_{i,avg} = \frac{1}{L_{cath}} \int_{x=x_s}^{x=x_s+x_c} C_i dx = \frac{1}{L_{cath}} \sum_{\Delta x} C_i \cdot \delta x$$

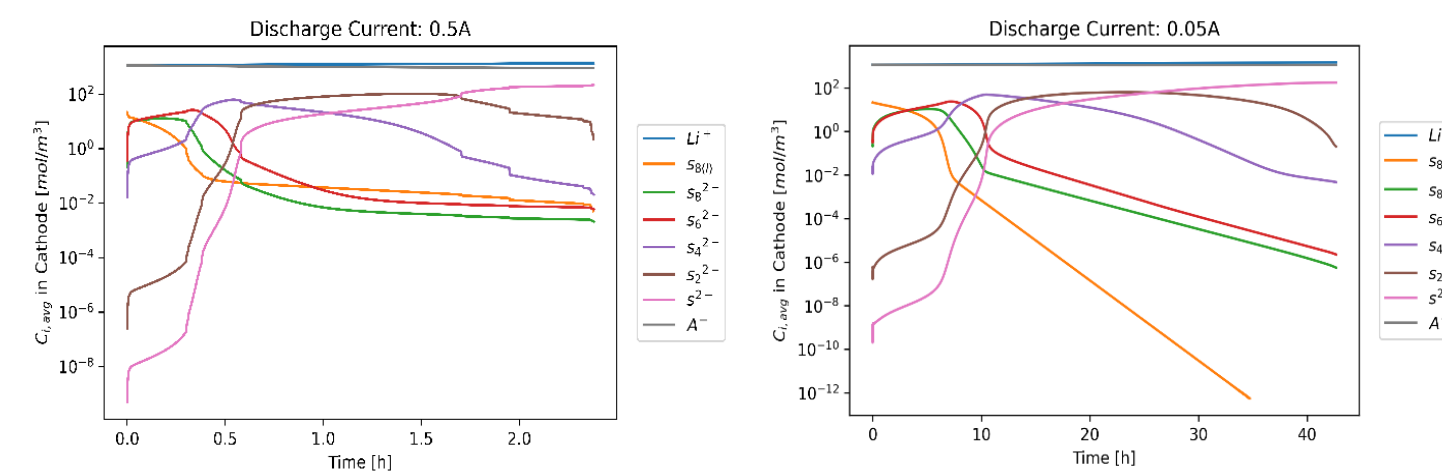


Figure 4. Average species concentrations in the cathode.

The A^- species mass and overall cell charge conservation equations are given by:

$$\begin{aligned} A_{total\ mass}^- &= \frac{1}{x_s + x_c} \int_{x=0}^{x=x_s+x_c} \epsilon_p C_{A^-} dx = \frac{1}{x_s + x_c} \sum_{\Delta x} \epsilon_p C_{A^-} \cdot \delta x \\ \sum_{i=0}^n \epsilon_p z_i C_i &= 0 \end{aligned}$$

1D Li-S MODEL WITH PRECIPITATION/DISSOLUTION DYNAMICS

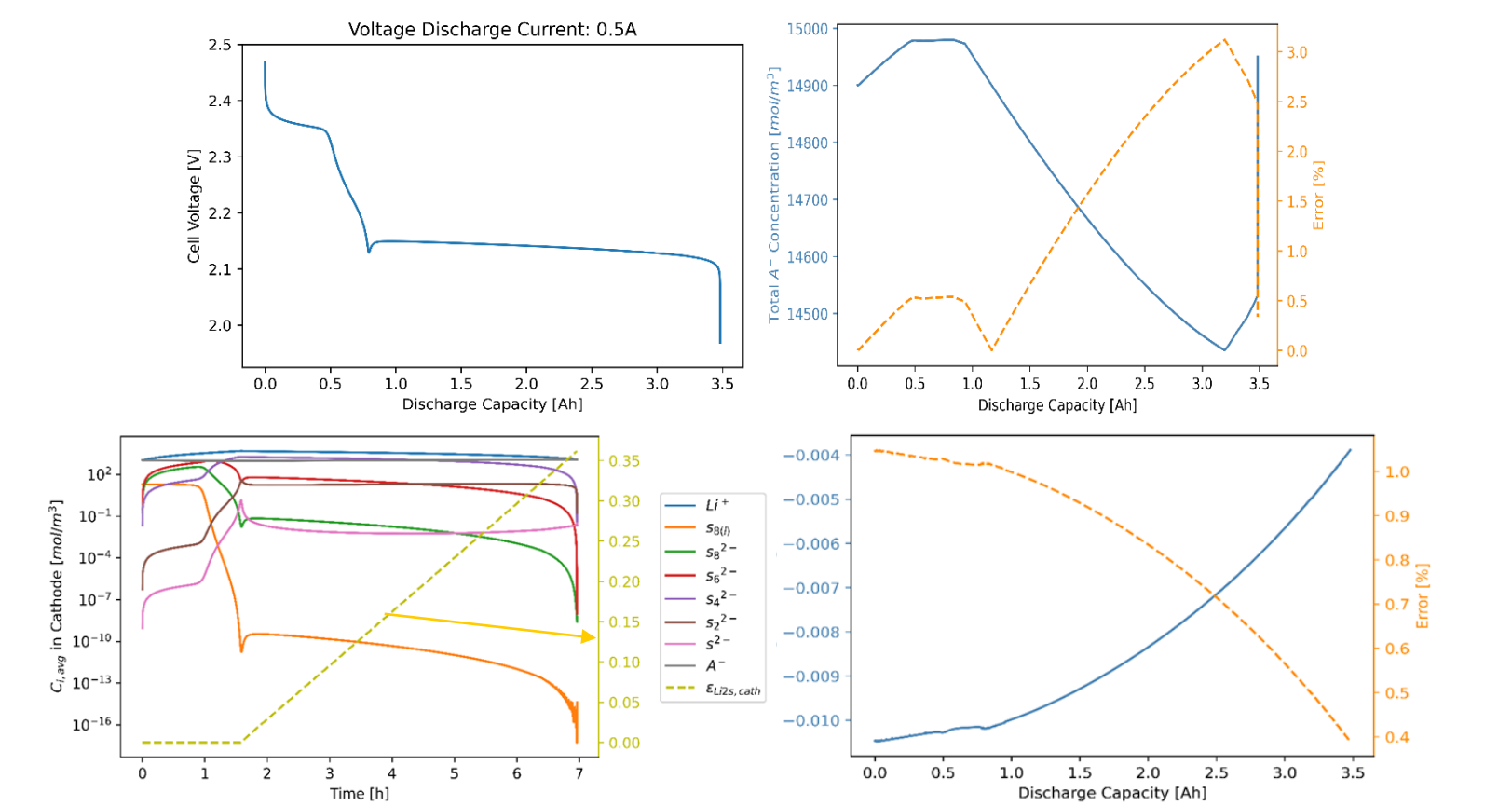


Figure 5. Voltage discharge (top left), A^- mass conservation (top right), species time evolution (bottom left) & cell charge conservation (bottom right) plots.

The normalized partial currents (@ cathode) are calculated as:

$$I_j^N = \frac{1}{I_{app}} \int_{x=x_s}^{x=x_s+x_c} a_v i_j dx = \frac{1}{I_{app}} \sum_{\Delta x} a_v i_j \delta x \quad \& \quad \sum_{j=2}^6 I_j^N = 1$$

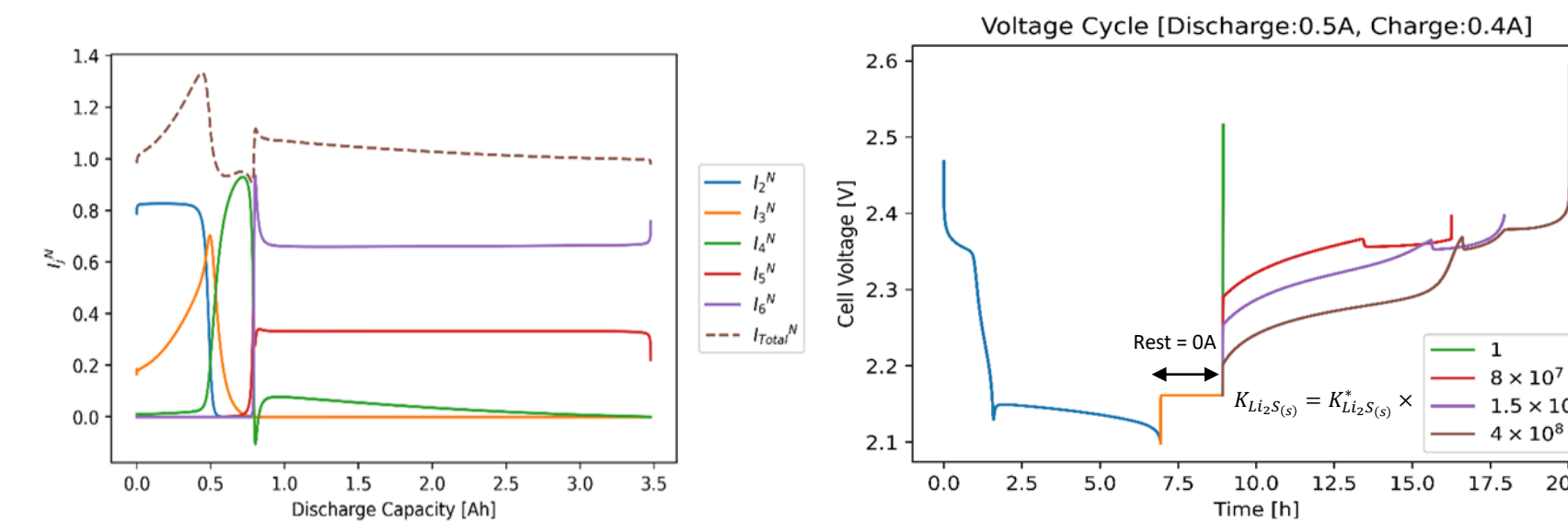


Figure 6. Normalized partial currents (left) & consecutive charge (right) tests.

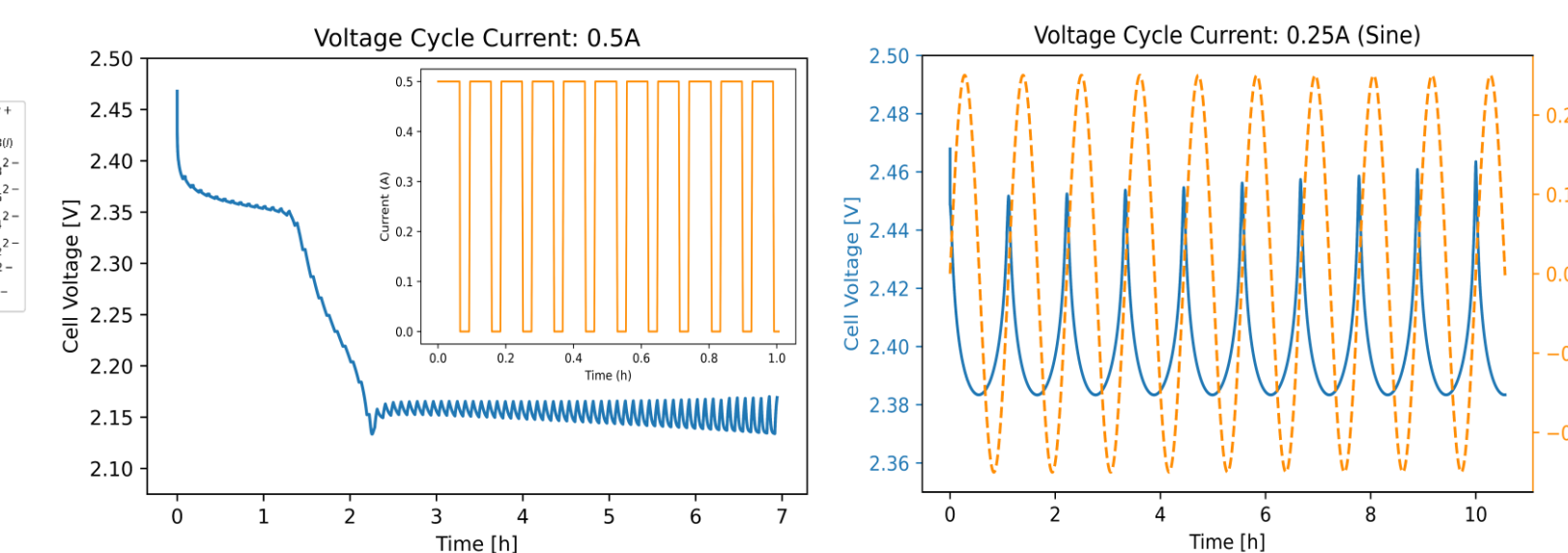


Figure 7. GITT (left) & sinusoidal current (right) tests.

CONCLUSION

- Novel solver works well & efficiently (avg simulation runtime: 10mins).
- Normalized partial currents do not sum to unity (high plateau) due to absence of higher order polysulfide precipitations for model studied.
- Numerical issues during consecutive charge similar to findings of [5].
- Developed solver capable of testing non-constant current simulations evident from GITT & sinusoidal current tests.

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