

# SED (1.0): A new, numerically efficient sediment module for the coupling to Earth System Models

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**Abstract.** TEXT

## 1 Introduction

Role of marine sediments for climate and global biogeochemical cycles

Diagenetic Models

How are sediment resolved in Earth System models

Problem with that

Alternative Model approaches, e.g. from coastal reserach

Solution presented here

## 2 Model Description

This section describes the formulation and solution of the model. A glossary of parameters along with their respective units is provided in Table ??

## 2.1 General Model Approach

The calculation of benthic return/uptake and burial fluxes is based on the vertically resolved conservation equation for solid and dissolved species in porous media is given by (e.g. Berner, 1980; Boudreau, 1997):

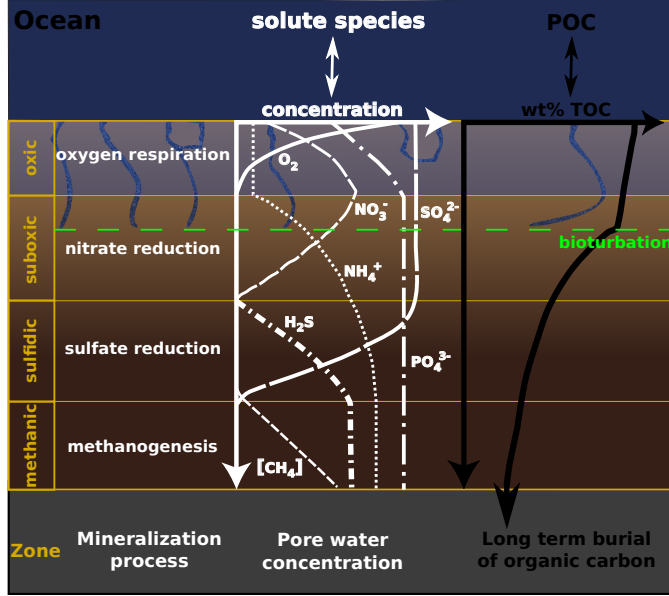
$$\frac{\partial \xi C_i}{\partial t} = -\frac{\partial F}{\partial z} + \xi \sum_j R_i^j \quad (1)$$

where  $C_i$  is the concentration of the biogeochemical species  $i$ ,  $\xi$  equals the porosity  $\phi$  for solute species and  $(1 - \phi)$  for solid species, hence represents the partitioning of species  $i$  into the solute and dissolved phase. The term  $z$  is the sediment depth,  $t$  denotes the time,  $F$  summarises the transport fluxes and  $\sum_j R_i^j$  represents the sum of production/consumption rates  $j$  that affect species  $i$ . The reaction network has to account for the most important primary and secondary redox reactions, equilibrium reactions, mineral dissolution and precipitation, as well as adsorption and desorption processes.

State-of-the-art reaction-transport models generally solve Eq. (1) numerically and thus allow to account for transient conditions, depth-varying parameters or a high degree of coupling between different chemical species. Yet, numerical models are computational expensive, thus rendering their application in an Earth System Model framework prohibitive. An analytical solution of Eq. (1) provides an alternative and computational more efficient approach. Analytical models enjoyed great popularity in the early days of diagenetic modelling due to the low computing power. However, early analytical models were often very problem-specific and only considered one or two coupled species (e.g. Lehrman, Berner) ?? which pubs?. A number of more complex analytical models describing the coupled dynamics of ....were developed (e.g. Billen, 1982; Goloway and Bender, 1982; Jahnke et al., 1982).

Finding an analytical solution to Eq. (1), especially when complex reaction networks are to be considered is not straightforward and generally requires the assumption of steady state. Because the Earth system model relevant variability in boundary conditions and fluxes is generally longer than the characteristic timescales of the reaction-transport processes, the sediment can be described by a series of pseudo steady-states. In addition, the complexity of the reaction network can be reduced by dividing the sediment into distinct zones and accounting for the most pertinent biogeochemical processes within each zone, thus increasing the likelihood of finding an analytical solution to Eq. (1). The model divides the sediment into a bioturbated and a non-bioturbated zone defined by the constant bioturbation depth  $z_{bio}$ . In addition, it accounts for the dynamic redox zonation of marine sediments by dividing the sediment into: 2) an oxic zone situated between the SWI and a dynamically calculated penetration depth of oxygen  $z_{O_2}$ , 3) a denitrification zone situated between  $z_{O_2}$  and a dynamically calculated penetration depth of nitrate  $z_{NO_3}$ , 4) a sulfate reduction zone situated between  $z_{NO_3}$  and a dynamically calculated penetration depth of sulfate  $z_{SO_4}$  and 5) a methanogenic zone situated below

$z_{SO_4}$  (Figure 1). Each zone is characterised by a set of diagenetic equations that encapsulate the most pertinent reaction and transport processes in the respective zone (see section ?? and ?? for more detail).



**Figure 1.** Schematic of the different modelled species and layers in our sediment model. Here showing the case  $z_{ox} < z_{bio} < z_{NO_3} < z_{SO_4}$ .

## 2.2 Transport

The model accounts for both advection and diffusion of dissolved and solid species, assuming that sediment compaction is negligible ( $\frac{\partial \phi}{\partial z} = 0$ ). The diffusion of dissolved species is described via an apparent diffusion coefficient,  $D_{i0}$ . In addition, the activity of infaunal organisms in the bioturbated zone of the sediment ( $z < z_{bio}$ ) causes random displacements of sediments and porewaters and is simulated using a diffusive term (e.g. Boudreau, 1986), with a constant bioturbation coefficient  $D_{bio}$  in the bioturbated zone. The pumping activity by burrow-dwelling animals, the so-called bioirrigation, is encapsulated in a factor,  $f_{ir}$  that enhances the molecular diffusion coefficient,  $D_{mol,i}$  (hence,  $D_{i,0} = D_{mol,i} \cdot f_{ir}$ , Soetaert et al., 1996a). The divergence of the flux is thus given by:

$$\frac{\partial F}{\partial z} = -\frac{\partial}{\partial z} \left( -\xi D_i \frac{\partial C_i}{\partial z} + \xi w C_i \right) \quad (2)$$

where  $D_i$  is the diffusion coefficient of species  $i$  ( $D_i = D_{i,0} + D_{bio} = D_{mol,i} \cdot f_{ir} + D_{bio}$  for dissolved species and  $D_i = D_{bio}$  for solid species) and  $w$  is the burial rate. The bioturbation coefficient  $D_{bio}$  is set to zero below  $z_{bio}$ . In addition, infaunal activity ceases ( $D_{bio} = 0$ ) once bottom waters become anoxic ( $O_2 = 0.0 \text{ mol cm}^{-3}$ ). **last bit not like that in model**

## 2.3 Reaction Network

Earth System models generally track the evolution of the global biogeochemical cycles of organic and inorganic carbon, the essential nutrients (nitrogen, phosphorus) and oxygen with the aim of investigating the evolution of the ocean's redox structure and carbonate system and its feedbacks on global climate. This general aim thus defines a minimum set of state variables and reaction processes that need to be resolved for an efficient representation of the benthic-pelagic coupling in Earth System Models. The sediment model has to provide robust quantifications of organic and inorganic carbon burial fluxes, growth-limiting nutrient, equilibrium invariant and reduced species return fluxes, and oxygen uptake fluxes. As a consequence, the reaction network must explicitly or implicitly account for the most important primary and secondary redox reactions, equilibrium reactions, mineral precipitation/dissolution and adsorption/desorption, resulting in a complex set of coupled reaction-transport equations. The following subsections provide a short discussion of the reaction processes included in the model and [table ?? what to do here?](#) provides an overview of the vertically resolved conservation equations for solid and dissolved species in each layer. Table 4 summarizes the stoichiometric factors and secondary reaction parameters used in the model.

### 2.3.1 Organic matter

In marine sediments, organic matter (OM) is degraded by heterotrophic activity coupled to the sequential utilisation of terminal electron acceptors (TEAs), typically in the order of  $O_2$ ,  $NO_3^-$ ,  $Mn(VI)$ ,  $Fe(III)$  and  $SO_4^{2-}$  followed by methanogenesis and/or fermentation. Organic matter degradation is described via a multi-G model approach (Arndt et al., 2013, and references therein), assuming that the bulk OM is divided into discrete compound classes  $C_i$  characterised by specific degradation rate constants  $k_i$ . Such a multi-G approach allows for selective preservation of compound classes according to their degradability,  $k_i$  and, thus, accounts for the change in organic matter degradability with burial. Each compound class is degraded according to first-order kinetics. Organic matter dynamics are thus described by:

$$\frac{\partial C_i}{\partial t} = 0 = D_{C_i} \frac{\partial^2 C_i}{\partial z^2} - w \frac{\partial C_i}{\partial z} - k_i \cdot C_i \quad (3)$$

The solution of Eq. 3 (see section ?? for details) requires the definition of boundary conditions. The model assumes a known concentration/flux at the sediment-water interface and continuity across the bottom of the bioturbated zone,  $z_{bio}$  (Table 1).

### 2.3.2 Oxygen

Oxygen serves as the most powerful terminal electron acceptor for the heterotrophic degradation of organic carbon. In addition, the oxidation of reduced species produced through microbial activity throughout the sediment column further contributes to the consumption of oxygen. The model

**Table 1.** Boundary conditions for organic matter and oxygen.

Boundary	Condition	
$z = 0$	known concentration	1) $C_i(0) = C_{i0}$
$z = z_{bio}$	continuity	2) $C_i(z_{bio}^-) = C_i(z_{bio}^+)$ 3) $D_{bio} \cdot \frac{\partial C_i}{\partial z} \Big _{z_{bio}^-} = 0$
$z = 0$	known concentration	1) $O_2(0) = O_{20}$
$z = z_{bio}$	continuity	2) $O_2(z_{bio}^-) = O_2(z_{bio}^+)$ 3) $(D_{O_2,0} + D_{bio}) \cdot \frac{\partial O_2}{\partial z} \Big _{z_{bio}^-} = D_{O_2,0} \cdot \frac{\partial O_2}{\partial z} \Big _{z_{bio}^+}$
$z = z_{ox}$	$O_2$ consumption	4) $O_2(z_{ox}) = 0$ <b>and/or/at all???</b> $\frac{\partial O_2}{\partial z} \Big _{z_{ox}} = 0$
$z = z_{ox}$	Flux from below with: <b>correct? &amp;</b> <b>why <math>\omega</math> at 5) (delete!?)</b>	5) $-\omega D_{O_2} \cdot \frac{\partial O_2}{\partial z} \Big _{z_{ox}} = F_{red,z_{ox}}$ $F_{red,z_{ox}} = \frac{1-\phi}{\phi} \cdot \int_{z_{ox}}^{\infty} \sum_i (2\gamma_{NH_4} NC_i + \delta SC_i) k_i C_i dz$

explicitly accounts for the consumption of oxygen by heterotrophic degradation and nitrification of ammonium in the oxic layer of the sediment. In addition, the oxygen consumption through the oxidation of reduced species ( $Fe^{2+}$ ,  $Mn^{2+}$ ,  $NH_4$ ,  $H_2S$ ) produced in the suboxic and anoxic layers of the sediment is implicitly taken into account through the flux boundary condition at the dynamic oxygen penetration depth  $z_{ox}$ . This simplification can be justified as it has been shown that these secondary redox reactions mainly occur at the oxic/suboxic interface (Soetaert et al., 1996b). Oxygen is described in  $mol\ cm^{-3}$  liquid and conversion from the solid phase of mineralized organic matter (expressed in  $mol\ cm^{-3}$  bulk sediment) to consumption of dissolved oxygen (or later nutrients) introduce a factor of  $\frac{1-\phi}{\phi}$ , where  $\phi$  is the sediment porosity. Oxygen dynamics are thus described by:

$$\frac{\partial O_2}{\partial t} = 0 = D_{O_2} \frac{\partial^2 O_2}{\partial z^2} - w \frac{\partial O_2}{\partial z} - \frac{1-\phi}{\phi} \sum_i k_i \cdot [OC + 2\gamma_{NH_4} NC_i] \cdot C_i(z) \quad (4)$$

To solve Eq. 4 analytically (see section ??) boundary conditions at three depths are defined (Table 1). The model assumes a known bottom water concentration and the complete consumption of oxygen at the oxygen penetration depth (or zero flux if  $z_{ox} = z_{\infty}$ ). It considers equal oxygen concentration and diffusive flux above ( $z_{bio}^-$ ) and below ( $z_{bio}^+$ ) the bioturbation boundary. In addition, the model imposes a flux of reduced species through the bottom of the oxic zone that is calculated as the reduced substances produced through anoxic mineralization of organic matter below  $z_{ox}$ . Thus, assuming that fractions ( $\gamma_{NH_4}$  and  $\delta$ ) of these reduced species are oxidised at the oxic/suboxic interface.

### 2.3.3 Nitrate and Ammonium

To model nitrate and ammonium dynamics the sediment is partitioned into two geochemical layers (oxic and suboxic), where different equations describe the biogeochemical processes. Above the oxygen penetration depth organic matter mineralization produces ammonium, which is partly nitrified.

fied to nitrate (the fraction  $\gamma_{NH_4}$ ). In the suboxic zone ( $z > z_{ox}$ ), oxygen concentration is zero and nitrate serves as the electron acceptor to respire organic matter, thus nitrate is consumed by denitrification and ammonium is produced. Below the nitrate penetration depth  $z_{NO_3}$ , ammonium is still produced through OM mineralization. Therefore the diagenetic equations for nitrate and ammonium are given by:

1. Layer ( $z \leq z_{ox}$ )

$$\frac{\partial NO_3^I}{\partial t} = 0 = D_{NO_3} \frac{\partial^2 NO_3^I}{\partial z^2} - w \frac{\partial NO_3^I}{\partial z} + \gamma_{NH_4} \frac{1-\phi}{\phi} \cdot \sum_i NC_i \cdot k_i \cdot C_i(z) \quad (5)$$

$$\frac{\partial NH_4^I}{\partial t} = 0 = D_{NH_4} \frac{\partial^2 NH_4^I}{\partial z^2} - w \frac{\partial NH_4^I}{\partial z} + (1 - \gamma_{NH_4}) \frac{1-\phi}{\phi} \cdot \sum_i NC_i \cdot k_i \cdot C_i(z) \quad (6)$$

2. Layer ( $z_{ox} < z \leq z_{NO_3}$  [or  $z_\infty$  for  $NH_4$ ])

$$\frac{\partial NO_3^{II}}{\partial t} = 0 = D_{NO_3} \frac{\partial^2 NO_3^{II}}{\partial z^2} - w \frac{\partial NO_3^{II}}{\partial z} - \frac{1-\phi}{\phi} NO_3 CR \cdot \sum_i k_i \cdot C_i(z) \quad (7)$$

$$\frac{\partial NH_4^{II}}{\partial t} = 0 = D_{NH_4} \frac{\partial^2 NH_4^{II}}{\partial z^2} - w \frac{\partial NH_4^{II}}{\partial z} + \frac{1-\phi}{\phi} \cdot \sum_i NC_i \cdot k_i \cdot C_i(z) \quad (8)$$

The boundary conditions to solve Equations 5 - 12 are summarized in Table 2. The model assumes known bottom water concentrations for both species, the complete consumption of nitrate at the nitrate penetration depth (or zero flux if  $z_{NO_3} = z_\infty$ ) and no change in ammonium flux at  $z_\infty$ . It considers equal concentrations and diffusive fluxes at  $z_{bio}$  and  $z_{ox}$ . In addition, the re-oxidation of upward-diffusing reduced ammonium is considered in the oxic-suboxic boundary condition for nitrate and ammonium.

### 2.3.4 Sulfate and Sulfide

When nitrate is depleted, sulfate reduction is the pathway to mineralize organic matter. To describe sulfate and hydrogen sulfide concentrations in the sediments... Sulfate and sulfide dynamics are thus described by:

1. Layer ( $z \leq z_{NO_3}$ )

$$\frac{\partial SO_4^I}{\partial t} = 0 = D_{SO_4} \frac{\partial^2 SO_4^I}{\partial z^2} - w \frac{\partial SO_4^I}{\partial z} \quad (9)$$

$$\frac{\partial H_2S^I}{\partial t} = 0 = D_{H_2S} \frac{\partial^2 H_2S^I}{\partial z^2} - w \frac{\partial H_2S^I}{\partial z} \quad (10)$$

2. Layer ( $z_{NO_3} < z \leq z_{SO_4}$  [or  $z_\infty$  for  $H_2S$ ])

$$\frac{\partial SO_4^{II}}{\partial t} = 0 = D_{SO_4} \frac{\partial^2 SO_4^{II}}{\partial z^2} - w \frac{\partial SO_4^{II}}{\partial z} - \frac{1-\phi}{\phi} \cdot \sum_i SO_4 C \cdot k_i \cdot C_i(z) \quad (11)$$

$$\frac{\partial H_2S^{II}}{\partial t} = 0 = D_{H_2S} \frac{\partial^2 H_2S^{II}}{\partial z^2} - w \frac{\partial H_2S^{II}}{\partial z} + \frac{1-\phi}{\phi} \cdot \sum_i SO_4 C \cdot k_i \cdot C_i(z) \quad (12)$$

**Table 2.** Boundary conditions for nitrate and ammonium.

Boundary	Condition	
$z = 0$	known concentration	1) $NO_3(0) = NO_{30}$
$z = z_{bio}$	continuity	2) $NO_3(z_{bio}^-) = NO_3(z_{bio}^+)$
		3) $(D_{NO_3,0} + D_{bio}) \cdot \frac{\partial NO_3}{\partial z} \Big _{z_{bio}^-} = D_{NO_3,0} \cdot \frac{\partial NO_3}{\partial z} \Big _{z_{bio}^+}$
$z = z_{ox}$	continuity	4) $NO_3(z_{ox}^-) = NO_3(z_{ox}^+)$
	where:	5) $-D_{NO_3} \cdot \frac{\partial NO_3}{\partial z} \Big _{z_{ox}^-} + \gamma_{NH_4} \cdot F_{NH_4} = -D_{NO_3} \cdot \frac{\partial NO_3}{\partial z} \Big _{z_{ox}^+}$
		$F_{NH_4} = \frac{1-\phi}{\phi} \cdot \int_{z_{NO_3}}^{\infty} \sum_i k_i \cdot NC_i \cdot C_i dz$
$z = z_{NO_3}$	$NO_3$ consumption	6) $NO_3(z_{NO_3}) = 0$ or $\frac{\partial NO_3}{\partial z} \Big _{z_{NO_3}} = 0$
$z = 0$	known concentration	1) $NH_4(0) = NH_{40}$
$z = z_{bio}$	continuity	2) $NH_4(z_{bio}^-) = NH_4(z_{bio}^+)$
		3) $(D_{NH_4,0} + D_{bio}) \cdot \frac{\partial NH_4}{\partial z} \Big _{z_{bio}^-} = D_{NH_4,0} \cdot \frac{\partial NH_4}{\partial z} \Big _{z_{bio}^+}$
$z = z_{ox}$	continuity	4) $NH_4(z_{ox}^-) = NH_4(z_{ox}^+)$
<b>not <math>+(1 - \gamma_{NH_4}) \cdot F_{NH_4}</math>?</b>	where:	5) $-D_{NH_4} \cdot \frac{\partial NH_4}{\partial z} \Big _{z_{ox}^-} - \gamma_{NH_4} \cdot F_{NH_4} = -D_{NH_4} \cdot \frac{\partial NH_4}{\partial z} \Big _{z_{ox}^+}$
		$F_{NH_4} = \frac{1-\phi}{\phi} \cdot \int_{z_{NO_3}}^{\infty} \sum_i k_i \cdot NC_i \cdot C_i dz$
$z = z_{NO_3}$	continuity	6) $NH_4(z_{NO_3}^-) = NH_4(z_{NO_3}^+)$
	flux	7) $D_{NH_4} \cdot \frac{\partial NH_4}{\partial z} \Big _{z_{NO_3}^-} = D_{NH_4} \cdot \frac{\partial NH_4}{\partial z} \Big _{z_{NO_3}^+}$
$z = z_{\infty}$	$NH_4$ flux	8) $\frac{\partial NH_4}{\partial z} \Big _{z_{\infty}} = 0$

See boundary condition in Table 3.

Sulfate:

BC (5): Diffusive flux at  $z_{ox}$  is equal, considering the flux of reduced substances ( $H_2S$ ) from below

(SD, matlab): flux discontinuity from  $H_2S$  source; include methane region as AOM will produce sulfide as well(?)

BC(9): matlab: Calculate  $SO_4$  consumption below  $z_{so4}$ , by organic matter and indirectly via methane oxidation, **should it not be MC (methane to carbon ratio instead of  $SO_4C$ (???)**

Sulfide:

BC (5): Match at  $z_{ox}$ , layer 1 - layer 2 (continuity, flux discontinuity from  $H_2S$  source), flux of  $H_2S$  to oxic interface (from all sources of  $H_2S$  below), NB: include methane region as AOM will produce sulphide as well **should it be not the same as in  $SO_4$ ???**

BC (9): (flux with AOM production) flux of  $H_2S$  produced by AOM interface (Source of  $H_2S$ ), **don't think the reaction constants are correct in matlab!**

**TODO: MAKE table with reaction parameters (e.g.  $SO_4$ ,  $NC_i$ , ...)!**

**Table 3.** Boundary conditions for sulfate and sulfide. As in MATLAB (in red my suggestions).

Boundary	Condition	
$z = 0$	known concentration	1) $SO_4(0) = SO_{40}$
$z = z_{bio}$	continuity	2) $SO_4(z_{bio}^-) = SO_4(z_{bio}^+)$
	flux	3) $(D_{SO_4,0} + D_{bio}) \cdot \frac{\partial SO_4}{\partial z} \Big _{z_{bio}^-} = D_{SO_4,0} \cdot \frac{\partial SO_4}{\partial z} \Big _{z_{bio}^+}$
$z = z_{ox}$	continuity	4) $SO_4(z_{ox}^-) = SO_4(z_{ox}^+)$
	flux $\gamma_{H_2S}$ below?	5) $-D_{SO_4} \cdot \frac{\partial SO_4}{\partial z} \Big _{z_{ox}^-} + F_{H_2S}(z_{ox}) = -D_{SO_4} \cdot \frac{\partial SO_4}{\partial z} \Big _{z_{ox}^+}$
	where: $\int_{z_{SO_4}}^{\infty}$ here?	$F_{H_2S}(z_{ox}) = \frac{1-\phi}{\phi} \cdot \gamma_{H_2S} \cdot \left( \int_{z_{NO_3}}^{SO_4} \sum_i SO_4 C \cdot k_i \cdot C_i dz + \gamma_{CH_4} \cdot \int_{z_{SO_4}}^{\infty} \sum_i SO_4 C \cdot k_i \cdot C_i dz \right)$
$z = z_{NO_3}$	continuity	6) $SO_4(z_{NO_3}^-) = SO_4(z_{NO_3}^+)$
	flux	7) $D_{SO_4} \cdot \frac{\partial SO_4}{\partial z} \Big _{z_{NO_3}^-} = D_{SO_4} \cdot \frac{\partial SO_4}{\partial z} \Big _{z_{NO_3}^+}$
$z = z_{SO_4}$	SO <sub>4</sub> consumption	8) $SO_4(z_{SO_4}) = 0$
	Flux from below	9) $-D_{SO_4} \cdot \frac{\partial SO_4}{\partial z} \Big _{z_{SO_4}} = F_{SO_4}(z_{SO_4})$
	with: $SO_4 C \cdot \gamma_{CH_4}$ ?	$F_{SO_4}(z_{SO_4}) = \frac{1-\phi}{\phi} \cdot \int_{z_{SO_4}}^{\infty} \sum_i SO_4 C \cdot \gamma_{CH_4} \cdot k_i \cdot C_i dz$ not rather MC instead SO <sub>4</sub> C?
$z = 0$	known concentration	1) $H_2S(0) = H_{2S0}$
$z = z_{bio}$	continuity	2) $H_2S(z_{bio}^-) = H_2S(z_{bio}^+)$
	flux	3) $(D_{H_2S,0} + D_{bio}) \cdot \frac{\partial H_2S}{\partial z} \Big _{z_{bio}^-} = D_{H_2S,0} \cdot \frac{\partial H_2S}{\partial z} \Big _{z_{bio}^+}$
$z = z_{ox}$	continuity	4) $H_2S(z_{ox}^-) = H_2S(z_{ox}^+)$
	flux	5) $-D_{H_2S} \cdot \frac{\partial H_2S}{\partial z} \Big _{z_{ox}^-} + F_{H_2S}(z_{ox}) = -D_{H_2S} \cdot \frac{\partial H_2S}{\partial z} \Big _{z_{ox}^+}$
not as SO <sub>4</sub> !?	where: $1 - \gamma_{H_2S}$ ?	$F_{H_2S}(z_{ox}) = \frac{1-\phi}{\phi} \cdot (1 - \gamma_{H_2S}) \cdot \int_{z_{NO_3}}^{\infty} \sum_i SO_4 C \cdot k_i \cdot C_i dz$
$z = z_{NO_3}$	continuity	6) $H_2S(z_{NO_3}^-) = H_2S(z_{NO_3}^+)$
	flux	7) $D_{H_2S} \cdot \frac{\partial H_2S}{\partial z} \Big _{z_{NO_3}^-} = D_{H_2S} \cdot \frac{\partial H_2S}{\partial z} \Big _{z_{NO_3}^+}$
$z = z_{SO_4}$	continuity	8) $H_2S(z_{SO_4}^-) = H_2S(z_{SO_4}^+)$
	flux (with AOM)	9) $-D_{H_2S} \cdot \frac{\partial H_2S}{\partial z} \Big _{z_{SO_4}^-} + F_{H_2S}(z_{SO_4}) = -D_{H_2S} \cdot \frac{\partial H_2S}{\partial z} \Big _{z_{SO_4}^+}$
correct???	where:	$F_{H_2S}(z_{SO_4}) = \frac{1-\phi}{\phi} \cdot \int_{z_{SO_4}}^{\infty} \sum_i SO_4 C \cdot k_i \cdot C_i dz$
$z = z_{\infty}$	flux	10) $\frac{\partial H_2S}{\partial z} \Big _{z_{\infty}} = 0$

### 2.3.5 Phosphate

To model phosphorus (P) in the sediments the model takes into account the change with depth of phosphate (PO<sub>4</sub>) and iron-bound P, thereby mainly following the description of Slomp et al. (1996) and Gypens et al. (2008). Throughout the sediment column organic matter is mineralized resulting in a release of phosphate to the pore water. In the oxic part of the sediment, this PO<sub>4</sub> either diffuses upward to the water column or is sorbed to Fe oxides forming Fe-bound P (or M)(Slomp et al., 1998). In the suboxic/anoxic zone, PO<sub>4</sub> is not only produced through organic matter degradation but is also released from the Fe-bound P pool due to the reduction of Fe oxides. Furthermore, phosphate concentrations can become high enough in this layer for authigenic mineral formation to occur (Capellen and Berner, 1988). This phosphorus bound in authigenic minerals represents a permanent sink for reactive phosphorus (Slomp et al., 1996). Therefore the diagenetic equations for phosphorus are



**Table 4.** Reaction parameters. Value relates to mol of terminal electron acceptor consumed for 1 mol of organic matter mineralized.

Parameter/Variable	Unit	Value	Description
<b>stoichiometric factors</b>			
OC	<i>mol/mol</i>	1.0	oxygen to carbon ratio
$NC_1$	<i>mol/mol</i>	0.1509	nitrogen to carbon ratio refractory fraction
$NC_2$	<i>mol/mol</i>	0.13333	nitrogen to carbon ratio labile fraction
$SO_4C$	<i>mol/mol</i>	0.5	sulfate to carbon ratio
$MC$	<i>mol/mol</i>	0.5	methane to carbon ratio
<b>secondary reaction parameters</b>			
$\gamma_{NH_4}$	-	1.0	fraction of $NH_4$ that is oxidised in oxic layer
$\gamma_{H_2S}$	-	0.8	fraction of $H_2S$ that is oxidised in oxic layer
$\gamma_{CH_4}$	-	1.0	fraction of $CH_4$ that is oxidised at $z_{SO_4}$

written:

1. Layer ( $z \leq z_{ox}$ )

$$\frac{\partial PO_4^I}{\partial t} = \frac{D_{PO_4}}{1 + K_{PO_4}^I} \frac{\partial^2 PO_4^I}{\partial z^2} - w \frac{\partial PO_4^I}{\partial z} + \frac{1 - \phi}{\phi \cdot (1 + K_{PO_4}^I)} \sum_i (PO_4 C_i \cdot k_i \cdot C_i(z)) - \frac{k_s}{1 + K_{PO_4}^I} (PO_4^I - PO_4^s) \quad (13)$$

$$\frac{\partial M^I}{\partial t} = D_M \frac{\partial^2 M^I}{\partial z^2} - w \frac{\partial M^I}{\partial z} + k_s \frac{\phi}{1 - \phi} (PO_4^I - PO_4^s) \quad (14)$$

2. Layer ( $z_{ox} < z$ )

$$\frac{\partial M^{II}}{\partial t} = D_M \frac{\partial^2 M^{II}}{\partial z^2} - w \frac{\partial M^{II}}{\partial z} - k_m (M^{II} - M^\infty) \quad (15)$$

$$\frac{\partial PO_4^{II}}{\partial t} = \frac{D_{PO_4}^{II}}{1 + K_{PO_4}^{II}} \frac{\partial^2 PO_4^{II}}{\partial z^2} - w \frac{\partial PO_4^{II}}{\partial z} + \frac{1 - \phi}{\phi \cdot (1 + K_{PO_4}^{II})} \sum_i (PO_4 C_i \cdot k_i \cdot C_i(z)) - \frac{k_a}{1 + K_{PO_4}^{II}} (PO_4^{II} - PO_4^a) + \frac{(1 - \phi) k_m}{\phi (1 + K_{PO_4}^{II})} (M^{II} - M^\infty) \quad (16)$$

$$(17)$$

Explain boundary conditions in Table 5.

**Table 5.** Boundary conditions for phosphate and Fe-bound P (M). As in MATLAB (in red my suggestions).

Boundary	Condition	
$z = 0$	known concentration	1) $PO_4(0) = PO_{40}$
$z = z_{bio}$	continuity	2) $PO_4(z_{bio}^-) = PO_4(z_{bio}^+)$
	flux	3) $(D_{PO_4,0} + D_{bio}) \cdot \frac{\partial PO_4}{\partial z} \Big _{z_{bio}^-} = D_{PO_4,0} \cdot \frac{\partial PO_4}{\partial z} \Big _{z_{bio}^+}$
$z = z_{ox}$	continuity	4) $PO_4(z_{ox}^-) = PO_4(z_{ox}^+)$
	flux	5) $-\frac{D_{PO_4}}{1+K_{PO_4}^I} \cdot \frac{\partial PO_4}{\partial z} \Big _{z_{ox}^-} = -\frac{D_{PO_4}}{1+K_{PO_4}^{II}} \cdot \frac{\partial PO_4}{\partial z} \Big _{z_{ox}^+}$
$z = z_{\infty}$	flux	10) $\frac{\partial PO_4}{\partial z} \Big _{z_{\infty}} = 0$
$z = 0$	known concentration	1) $M(0) = M_0$
$z = z_{bio}$	continuity	2) $M(z_{bio}^-) = M(z_{bio}^+)$
correct???	flux	3) $\frac{\partial M}{\partial z} \Big _{z_{bio}^-} = \frac{\partial M}{\partial z} \Big _{z_{bio}^+}$
$z = z_{ox}$	continuity	4) $M(z_{ox}^-) = M(z_{ox}^+)$
correct???	flux	5) $\frac{\partial M}{\partial z} \Big _{z_{ox}^-} = \frac{\partial M}{\partial z} \Big _{z_{ox}^+}$
$z = z_{\infty}$	flux	10) $M(z_{\infty}) = M_{\infty}$

## 2.4 Model Parameters

### 2.4.1 Transport Parameters

Sedimentation rate

Diffusion coefficients

Bio-irrigation coefficients

### 2.5 Reaction Parameters

short description

### 2.6 Module Structure

technical description, e.g. how is it implemented and how can it be coupled to model

## 3 Test Cases

### 3.1 Benthic fluxes on a global scale

Application to Seitert, 2004 OM, burwicz see rate data and evaluation based on global data (Archer)

### **3.2 HILDA-like test**

### **3.3 GENIE-Cretaceous test?**

## **4 Scope of applicability and model limitations**

## **5 Conclusions**

TEXT

## **6 Code Availability**

## **Appendix A**

### **A1**

*Acknowledgements.* TEXT

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