
STATISTICAL MECHANICS: A COMPLETE GUIDE

PHYS 449

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Solo Pursuit of Learning



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Part I

Thermodynamics

Chapter 1

Energy in Thermal Physics

1.1.0 Basic Notation and Work

Definition 1.1.1. *Thermodynamics is a phenomenological description of properties of macroscopic systems in thermal equilibrium.*

By a phenomenological description we mean a discription based on observations and direct experience of the experimenter with the system, considered as a “black box” (a system whose internal structure is unknown, or is just not considered). The task of thermodynamics is to define appropriate physical quantities, state quantities, which characterize macroscopic properties of matter, that is macrostates, in a way which is as unambiguous as possible, and to relate these quantities by means of universally valid equations.

Definition 1.1.2 (Systems). *There are a number of different thermodynamic systems. In particular we define a thermodynamic system, in general, to be an arbitrary amount of matter, the properties of which can be uniquely and completely described by specifying certain macroscopic parameters. We summarize them as follows:*

- **Thermodynamic or Macroscopic System:** *A system consisting of a large number of constituents. For example, a mole of gas (approximately 10^{23} particles) can be considered as a macroscopic system.*
- **Isolated Thermodynamic System:** *A system which exhibits no exchange of any type with the surroundings; no exchange of work, heat, matter, etc. The total energy (mechanical, electrical, etc.) is a conserved quantity for such a system, and can thus be used to characterize the macrostate.*
- **Closed Theormodynamic System:** *A system which exhibits no exchange of matter with its surroundings. Hence, energy exchange is allowed, so energy is no longer a conserved quantity and can fluctuate due to exchange with the surroundings. The temperature, particle number, and volume of the system can characterize the macrostate.*
- **Open Thermodynamic System:** *A system for which it is possible for exchange of any*

type with the surroundings (work, heat, matter, etc.). Energy and particle number are both not conserved. But, temperature and chemical potential can still be used to characterize a macrostate.

If the properties of a system are the same for any part of it, one calls such a system homogeneous. On the other hand, if the properties change discontinuously at certain marginal surfaces, the system is heterogeneous, with the homogeneous portions of the system called phases and the separating surfaces phase boundaries.

Definition 1.1.3. *The macroscopic quantities which describe a system are called state quantities.*

Example 1.1.1. Examples of state quantities are the system's energy E , its volume V , its particle number N , its entropy S , its temperature T , the pressure P , the chemical potential μ , the charge q , the dipole momentum, the refractive index, the viscosity, the chemical composition, and the size of phase boundaries.

However, microscopic quantities do not fall under the umbrella of state quantities.

Definition 1.1.4 (Equilibrium). *Two thermodynamic systems are in equilibrium if and only if they are in contact such that they can exchange a given conserved quantity (for example particles) and they are relaxed to a state in which there is no average net transfer of that quantity between them anymore. A thermodynamic system S is in equilibrium with itself, if and only if, all its subsystems are in equilibrium with each other. In this case, S is called an equilibrium system.*

From this definition we find that different types of exchanged quantities can lead to different types of equilibria:

Exchanged Quantity	Type of Equilibrium
Particles/Matter	Diffusive Equilibrium
Work	Mechanical Equilibrium
Heat	Thermal Equilibrium

Definition 1.1.5. Complete Thermodynamic Equilibrium *corresponds to a state where all the conserved fluxes between two coupled thermodynamic systems vanish.*

A way of testing if a given system is in a complete thermodynamic equilibrium is if the properties of the system do not change appreciably over the observation time, which is to say the properties reflect the true asymptotic long-term properties after any initial relaxation time is over.

The state of thermodynamic systems in complete thermodynamic equilibrium can be described by a set of independent thermodynamic coordinates or state variables; this fact is based on empirical observations.

1.1.1 Boyle-Mariotte's Experiment

Law. For a given mass of gas at a constant temperature T , the volume V is inverseley proportional to the pressure P : $V \propto P^{-1}$.

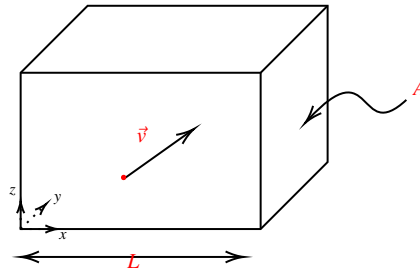
We consider Robert Boyle's (1627-1691) experiment, conducted at room temperature, which should remain constant during the time of the experiment. We use a vertical tube with markings to indicate the volume of gas, and oil at the bottom. By applying pressure on the oil, we also exert a pressure on the air in the tube above the oil, causing the volume to decrease. Drawing the graph of volume versus P^{-1} we obtain a straight line, so $V \cdot P = C$ for some constant C , given a fixed temperature. As further measurements show, the constant is proportional to the temperature T , so $V \cdot P \propto T$. More precisely, the full equation of a state of simple low-density gas is given by

$$PV = Nk_B T \quad (1.1.1)$$

where N is the number of gas particles and $k_B \approx 1.381 \times 10^{-23} \text{ J/K}$ is a natural constant called the **Boltzmann's constant**. The above equation is called the **ideal gas law** or the **equation of state for an ideal gas** since it relates the three state variables, or thermodynamic coordinates, P , V , and T at equilibrium.

Mechanical Derivation

We now sketch a derivation of the ideal gas law using an atomistic theory governed by Newton's Laws. First assume there is a single molecule or atom bouncing around in a volume $V = AL$, where L is the length along the x -direction and A is the area of a side parallel to the yz -plane:



After many perfectly elastic collisions against the wall, the average pressure directly on the wall is

$$\bar{p} = \frac{\overline{F_{x, \text{on wall}}}}{A} = -\frac{\overline{F_{x, \text{on molecule}}}}{A} = -\frac{m \overline{\frac{\Delta v_x}{\Delta t}}}{A}$$

The time it takes for a full round trip is $\Delta t = 2L/v_x$. When it undergoes one elastic collision, its change in velocity is $\Delta v_x = -2v_x$. Together these give

$$\bar{p} = -\frac{m(-2v_x/(2L/v_x))}{A} = \frac{mv_x^2}{LA} = \frac{mv_x^2}{V}$$

Now, if we extend to $N \gg 1$ non-interacting molecules, each colliding with the walls totally elastically, then we can forgoe the averageness of the pressure to obtain

$$pV = m \sum_{i=1}^N (v_x^2)_i = mN \overline{v_x^2} = Nk_B T$$

using the ideal gas law at the end, which gives the relation

$$\overline{K_x} = \frac{1}{2} m \overline{v_x^2} = \frac{1}{2} k_B T$$

Then we find that the total mean kinetic energy is

$$\overline{K} = \frac{1}{2} m \overline{v_x^2} + \frac{1}{2} m \overline{v_y^2} + \frac{1}{2} m \overline{v_z^2} = \frac{3}{2} k_B T \quad (1.1.2)$$

Definition 1.1.6. The Root-mean square speed of each atom/molecule is defined as

$$v_{RMS} = \sqrt{\overline{v^2}}$$

In general the RMS speed is often a close approximation of the average speed. In this case we have $v_{RMS} = \sqrt{3k_B T/m}$.

1.1.2 Work

Definition 1.1.7. Given a vector force field \vec{F} defined along a path γ , the work W is of \vec{F} along γ is defined to be:

$$W = \int_{\gamma} \vec{F} \cdot d\vec{r} \quad (1.1.3)$$

Recall 1.1.1. Recall that pressure is force per unit area, so we have that

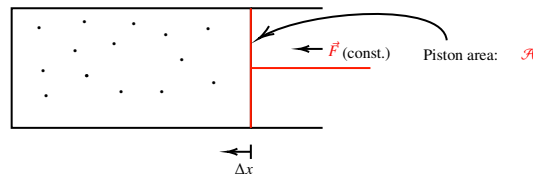
$$P = \frac{F}{A}$$

where F is the normal component of the force to the area A . More precisely, pressure is the proportionality constant that relates the force and normal vectors:

$$d\vec{F}_n = -pd\vec{A}$$

where \vec{F}_n denotes the normal component of the force vector \vec{F} .

Example 1.1.2. Consider the compression of a gas by a piston with a constant force of magnitude F .



so the work is

$$W = \int_{\gamma} \vec{F} \cdot d\vec{r} = F \int_{\gamma} dr = F\Delta x = PA\Delta x = -P\Delta V$$

where P is the pressure and ΔV is the change in volume. Since the change in volume is negative, the work W done on the system (here the gas) is positive: Energy is added to the system by a force (macroscopic) process (here the piston). $W < 0$ if energy is removed from the system.

Definition 1.1.8. *The generalized differential form for work is given by*

$$\delta W = \sum_{i=1}^m J_i dq_i \quad (1.1.4)$$

where q_i are the generalized coordinates and the J_i are the conjugate generalized forces such that $J_i dq_i$ has units of energy. This is possible when the system is undergoing an infinitesimal quasi-static transformation.

Here are a few examples of generalized coordinates and their corresponding generalized conjugate forces:

	Generalized Force J_i	Generalized Coordinate dq_i
Pressure	$-P$	dV (change in volume)
Surface tension	σ	dS (change in surface area)
Magnetic field	\vec{B}_0	$d\vec{m}$ (change in magnetic moment)
Electric field	\vec{E}	$d\vec{P}$ (change in electric dipole moment)

Definition 1.1.9. *Differential changes in a systems property are said to be **quasi-static** if the changes occur on time scales much longer than the relaxation time such that the system remains in equilibrium at all times.*

To ensure thermodynamics is a self-consistent description of macroscopic systems in thermal equilibrium we must assume that the differential changes δW are quasi-static. This also ensures that we can describe the state of such a thermodynamic system by a set of thermodynamic coordinates at all times, which is to state at any stage of the process the thermodynamic coordinates of the system exist and can in principle be computed.

Depending on the macroscopic generalized force, the work necessary to transfer a thermodynamic system in complete thermodynamic equilibrium from state A to state B might or might not depend on the path taken. For example, if γ_1 and γ_2 are two paths from state A to state B , it is possible that $\int_{\gamma_1} \delta W \neq \int_{\gamma_2} \delta W$. (Note that this justifies the use of the notation δW over dW , which would denote an exact differential)

Definition 1.1.10. *State quantities which are proportional to the amount of matter in a system are called **extensive**, and are consequently additive when looking at subsystems.*

Definition 1.1.11. *State quantities which are independent of the amount of matter in the system are called **intensive**, and are not additive for the particular phases of the system.*

Intensive quantities are indicators of equilibrium.

1.1.3 Conservative Forces

Recall 1.1.2. Recall that a conservative force is a force \vec{F} with an associated potential energy function E such that $\vec{F} = \nabla E$.

Proposition 1.1.1. *If the macroscopic generalized force \vec{J} , depending on m generalized coordinates q_i , is conservative with potential energy E_{pot} which is twice continuously differentiable and the domain of integration is simply connected, then the following are equivalent:*

- $\vec{J}(\vec{q}) = -\nabla E_{pot}(\vec{q})$
- dW is an exact differential form, so

$$\int_{\gamma} dW = \int_{\gamma} \vec{J} \cdot d\vec{r}$$

depends only on the endpoints of γ .

- For any simple closed path γ ,

$$\oint_{\gamma} dW = \oint_{\gamma} \vec{J} \cdot d\vec{r} = 0$$

- The curl of \vec{J} is trivial over the domain of integration

$$\nabla \times \vec{J} = 0$$

provided that $m = 3$

- For all $i, j \in \{1, 2, \dots, m\}$, we have that

$$\frac{\partial J_i}{\partial q_j} - \frac{\partial J_j}{\partial q_i} = 0$$

- The differential dW is exact, and we have that

$$dW = -\nabla E_{pot} \cdot d\vec{r} = -\sum_{i=1}^m \frac{\partial E_{pot}}{\partial q_i} dq_i = -dE_{pot}$$

Definition 1.1.12. For a function $A(q_1, q_2, \dots, q_m)$ the total differential or exact differential of A is given by

$$dA = \sum_{i=1}^m \frac{\partial A}{\partial q_i} dq_i$$

This corresponds to a generalized chain rule:

$$\frac{dA}{dt} = \nabla A \cdot \frac{d}{dt} \vec{q} = \sum_{i=1}^m \frac{\partial A}{\partial q_i} \frac{dq_i}{dt}$$

called the **total derivative** of A with respect to t . An exact differential corresponds to an **integrable differential form**:

$$\int_{\gamma} \sum_{i=1}^m \frac{\partial A}{\partial q_i} dq_i = \int_{\gamma} dA = A(\vec{q}_f) - A(\vec{q}_i)$$

where \vec{q}_i and \vec{q}_f are the initial and final point of the path γ , respectively.

Consequently, an integrable, or exact, differential form does not depend on the path taken and in physics we would consider A to be a potential function.

Note 1.1.3. For non-conservative forces, δW is an **inexact differential form**.

Theorem 1.1.2. A differential form

$$\delta A \equiv \sum_{i=1}^m a_i(q_1, q_2, \dots, q_m) dq_i$$

for functions $a_i : D \subseteq \mathbb{R}^m \rightarrow \mathbb{R}$ is exact if and only if

$$\frac{\partial a_i}{\partial q_j} = \frac{\partial a_j}{\partial q_i}$$

for all $i, j \in \{1, 2, \dots, m\}$.

Definition 1.1.13. An **integrating factor** μ is a factor that makes an inexact differential form exact upon multiplication.

Theorem 1.1.3. For $m = 2$, an integrating factor always exists. Specifically, for $\delta A = a_1 dx_1 + a_2 dx_2$, we can define $df := \mu \delta A = (\mu a_1) dx_1 + (\mu a_2) dx_2$, with μ determined non-uniquely by the equation

$$\frac{\partial(\mu a_1)}{\partial x_2} = \frac{\partial(\mu a_2)}{\partial x_1}$$

1.2.0 Equipartition Theorem

Theorem 1 (Equipartition Theorem).

Every degree of freedom of a system in thermodynamic equilibrium, which appear only quadratically in the total energy, contributes an average energy of $\frac{1}{2} N k_B T$ to the total energy of the system.

First, what exactly is a ‘degree of freedom’? In colloquial terms, a degree of freedom tells you about what the atom or molecule can actually do - maybe it can move around (translate), or vibrate, or rotate, or produce sound, or emit light, or a host of other things. Each of these capabilities contributes an energy of $\frac{1}{2} k_B T$ to the system’s energy.

Now, recall that the kinetic energy of a rotating body given a diagonalized inertial basis I_{ii} , is

$$K_{rot} = \frac{1}{2}(I_{xx}w_x^2 + I_{yy}w_y^2 + I_{zz}w_z^2) \quad (1.2.1)$$

and w_i are the angular frequencies associated with the angular velocity of the body in this basis. Each of these terms is quadratic, so each one corresponds to a degree of freedom.

We can conclude that the total energy of the system in some limit is

$$\frac{f}{2}Nk_B T$$

where f is the number of degrees of freedom.

1.3.0 Heat and the 1st Law of Thermodynamics

Definition 1.3.1. Recall that work corresponds to the change in energy of a thermodynamic system by a macroscopically forced process. On the other hand the heat Q is the energy added to or removed from a thermodynamic system by a spontaneous process (that is not forced).

Heat can be also stated as the amount of energy that spontaneously flows between two systems: heat moves from the system at higher temperature to the system at lower temperature (2nd law of thermodynamics to be covered later). Note we can define the temperature through the equipartition theorem as a measure of the total energy of the system E : $T \approx 2E/fk_B$, where f is the number of degrees of freedom.

We note that negative Q implies removing energy while positive Q implies adding energy.

For example, consider the energy transfer between a cooking plate and a pot of water. The origin of this type of process lies in the underlying microscopic dynamics, which we will explore using Statistical Mechanics.

Law (First Law of Thermodynamics). For an isolated thermodynamic system, the total internal energy U is a constant and $dU = 0$. By the definition of internal energy, dU is an exact differential; consequently, U should be unique for a given state. For various systems we have the following:

- For a closed system, $dU = \delta Q + \delta W$.
- For an open system, $dU = \delta Q + \delta W + \delta E_c$, with

$$\delta E_c := \sum_{i=1}^{\alpha} \mu_i dN_i$$

where N_i is the number of particles of type i and μ_i is the chemical potential associated with particles of type i for all $1 \leq i \leq \alpha$ with α being the number of different particle

types. The chemical potential corresponds to the energy needed to add a particle of type i to a given thermodynamic system while no other type of energy is exchanged, which is to say $\delta W = 0$ and $\delta Q = 0$.

In summary, the empirical first law is a reformulation of the conservation of energy and requires the inclusion of heat.

Chapter 2

Thermodynamical Systems

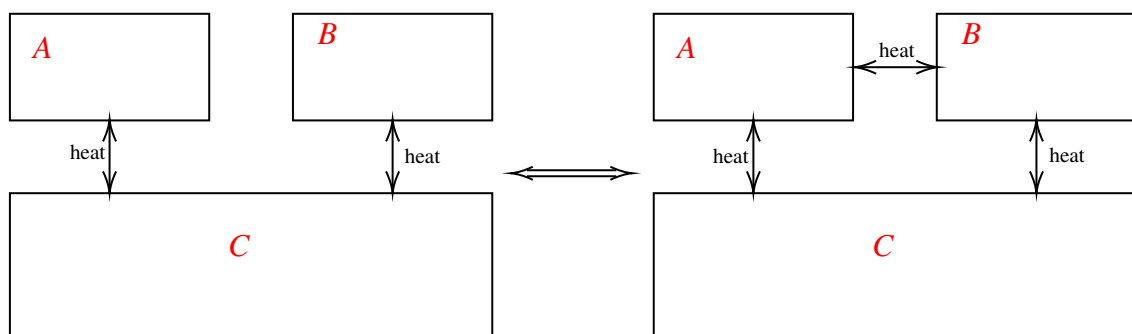
2.1.0 The 0th Law of Thermodynamics

We now wish to define the concept of temperature from a macroscopic perspective, to ensure our theoretical framework of thermodynamics is a self-consistent description of macroscopic systems in thermal equilibrium. The empirical principal we proceed with in our construction is that two systems which are in thermal equilibrium with one another should share the same “temperature.” Before we showed a derivation of the temperature in terms of kinetic energy from a microscopic perspective of sparse (non-dense) gas - this belongs to the area of Statistical mechanics.

Now, the 0th law of thermodynamics describes the transitivity of the equilibrium relation for systems:

Law (0th Law of Thermodynamics). *If two systems, A and B, are separately in equilibrium with a third system, C, then they are also in thermal equilibrium with one another.*

Indeed we can depict this as follows:



where the double-sided arrows labeled “heat” correspond to equilibrium between the systems. This law leads to existence of the state function Θ , known as the empirical temperature, such that systems in equilibrium are at the same temperature:

Corollary 2.1.1. *The 0th law of thermodynamics (transitivity of equilibria) implies the existence of temperature (state function).*

Proof. Assume that systems A and C are allowed to exchange heat and that they are in thermal equilibrium with each other. The state of system A is described by thermodynamic coordinates A_1, A_2, \dots and that of C by C_1, C_2, \dots . If now, for example, A_1 is changed, then this will potentially lead to changes in A_2, A_3, \dots and C_1, C_2, \dots . Mathematically, this means that a function f_{AC} exists such that

$$f_{AC}(A_1, A_2, \dots, C_1, C_2, \dots) = 0,$$

which is to say the function is constant for all thermodynamic coordinates that correspond to a thermal equilibrium between A and C . This has the form of a **constraint**. Similarly, we have another function f_{BC} with

$$f_{BC}(B_1, B_2, \dots, C_1, C_2, \dots) = 0,$$

describing the thermal equilibrium between systems B and C , where the state coordinates of B are B_1, B_2, \dots . For such physical constraints, the implicit function theorem applies and we can solve the above equations for any specific parameter, for example

$$C_1 = F_{AC}(A_1, A_2, \dots, C_2, C_3, \dots)$$

and

$$C_1 = F_{BC}(B_1, B_2, \dots, C_2, C_3, \dots)$$

for thermodynamic coordinates $A_1, A_2, \dots, B_1, B_2, \dots, C_2, C_3, \dots$ such that the constraints hold, so the systems are in thermodynamic equilibrium. Thus, as C is separately in equilibrium with A and B , this implies that

$$F_{AC}(A_1, A_2, \dots, C_2, \dots) = F_{BC}(B_1, B_2, \dots, C_2, \dots)$$

Now the 0th law ensures that A and B are also in thermal equilibrium so there is a function f_{AB} such that

$$f_{AB}(A_1, A_2, \dots, B_1, B_2, \dots) = 0$$

is the constraint describing the equilibrium. For any set of state parameters satisfying this equation, when substituting into $F_{AC} = F_{BC}$ the equality must hold quite independently of the state variables for C . Moving along the level surface described by this constraint, $F_{AC} = F_{BC}$ will remain valid irrespective of the state of C . This implies that we can cancel the C_2, C_3, \dots state variables in the equation $F_{AC} = F_{BC}$ on the manifold described by $f_{AB} = 0$. Hence, we have after cancelling the C_2, C_3, \dots 's out of the equation,

$$\Theta_A(A_1, A_2, \dots) = \Theta_B(B_1, B_2, \dots)$$

and this characterizes the equilibrium previously characterized by $f_{AB} = 0$. Thus, we have the existence of a universal property of systems in thermal equilibrium, namely the existence of a state function Θ that takes on identical values if systems are in thermal equilibrium, and this function specifies the **equation of state**. Hence, it fulfils the basic property of what one would naturally consider a temperature. We define Θ as the **empirical temperature**, which is scalar and not unique - we have many possible choices for Θ at this point. For a given fixed temperature Θ , all allowed thermodynamic states of a system, say A , can be obtained by $\Theta_A(A_1, A_2, \dots) = \Theta$. These states are called the **isotherms**. ■

We note that due to this, the zeroth law constrains the form of the constraint equation describing the equilibrium between two bodies such that it can be organized into an equality of two empirical temperature functions.

Remark 2.1.1. *Isotherms* can be considered as manifolds, or level-surfaces, of the empirical temperature function in the space of state variables for a system.

Definition 2.1.1. A **thermometer** is a system with some convenient macroscopic property that changes in a simple way as the equilibrium macrostate changes.

2.2.0 Heat Capacities

We move to the question of how much heat (energy added through a spontaneous not-forced process) is needed to raise the temperature of a system by a given amount. Heat is often an inexact differential, δQ , (which is to say it is not-path independent), and hence not a function of the state variables (i.e. not a **state function**). Consequently, one needs to specify the path by which heat is supplied:

Definition 2.2.1. The **heat capacities** are defined as $C_{\vec{X}} = \left(\frac{\partial Q}{\partial T}\right)_{\vec{X}}$, where \vec{X} is the set of thermodynamic coordinates which are held constant during the heat supply δQ . The **specific heats** are defined as $c_{\vec{X}} = \left(\frac{\delta Q}{M dT}\right)_{\vec{X}}$ where M is the mass of the system.

Consequently, the heat capacity of a system is how much heat energy is needed to raise its temperature by one degree. The specific heat is the heat capacity per unit mass.

Example 2.2.1. Examples of common specific heats are as follows:

- Water: $c_P \approx 4180 \text{ J/(kg K)}$ and $c_V \approx c_P$ at $T = 25^\circ\text{C}$, $p = 100 \text{ kPa}$, and N fixed.
- Air: $c_P \approx 1010 \text{ J/(kg K)}$ and $c_V \approx 720 \text{ J/(kg K)}$ at $T = 25^\circ\text{C}$, $p = 100 \text{ kPa}$, and N fixed.

2.2.1 Closed Systems (Heat Capacities)

Assume that the internal energy of a system is given by $U = U(T, q_1, \dots, q_m)$, which is to say the state of the system can be uniquely determined by the temperature and \vec{q} . Starting from the 1st law we have that

$$\delta Q = dU - \delta W = dU - \sum_{i=1}^m J_i dq_i = \frac{\partial U}{\partial T} dT + \sum_{i=1}^m \left[\frac{\partial U}{\partial q_i} - J_i \right] dq_i$$

We consider as a first special case the absence of any external work, so $\delta W = 0$ and equivalently \vec{q} is constant (for example, the volume for a gas being constant), so we have that

$$C_{\vec{q}} = \left(\frac{\delta Q}{dT}\right)_{\vec{q}} = \left(\frac{\partial U}{\partial T}\right)_{\vec{q}}$$

As a second special case let us consider when all macroscopic generalized forces are constant, so \vec{J} is constant (for example, the pressure for a gas is constant). We use the state functions $J_i = J_i(q_1, \dots, q_m, T)$, for $1 \leq i \leq m$, and we invert them to obtain $q_i = q_i(J_1, \dots, J_m, T)$ for $1 \leq i \leq m$ and make a change of variables:

$$dq_i = \sum_{j=1}^m \frac{\partial q_i}{\partial J_j} dJ_j + \frac{\partial q_i}{\partial T} dT = \frac{\partial q_i}{\partial T} dT$$

using the fact that \vec{J} is constant. Thus, for this special case of constant generalized force we have the heat capacity:

$$\begin{aligned} C_{\vec{J}} &= \left(\frac{\delta Q}{dT} \right)_{\vec{J}} \\ &= \left(\frac{\partial U}{\partial T} \right)_{\vec{q}} + \sum_{i=1}^m \left[\frac{\partial U}{\partial q_i} - J_i \right] \left(\frac{dq_i}{dT} \right)_{\vec{J}} \\ &= \left(\frac{\partial U}{\partial T} \right)_{\vec{q}} + \sum_{i=1}^m \left[\frac{\partial U}{\partial q_i} - J_i \right] \left(\frac{\partial q_i}{\partial T} \right)_{\vec{J}} \end{aligned}$$

using the expressions for δQ and dq_i from above.

Example 2.2.2 (Gas). For a simple dilute gas, we have $m = 1$ with state variable $q = V$ and generalized force $J = -p$. Hence:

$$C_V = \left(\frac{\partial U}{\partial T} \right)_V$$

and

$$C_p = \left(\frac{\partial U}{\partial T} \right)_V + \left[\left(\frac{\partial U}{\partial V} \right)_T + p \right] \left(\frac{\partial V}{\partial T} \right)_p$$

Thus, we have

$$C_p - C_V = \left[\left(\frac{\partial U}{\partial V} \right)_T + p \right] \left(\frac{\partial V}{\partial T} \right)_p$$

For an ideal gas, we can simplify further by using the equation of state $pV = Nk_B T$. Specifically, we have $\frac{\partial V}{\partial T} = \frac{Nk_B}{p}$. From experiments, we also have $U = U(T)$. Thus, $C_p - C_V = Nk_B$.

Remark 2.2.1. Most real-world objects prefer to expand when heated, keeping their pressure constants (this effect is less noticable in solids and liquids, and quite important in gases).

Example 2.2.3 (Magnet). For a magnet we have $m = 1$ generalized coordinate, the magnetic moment m , and we have the generalized force $J = B_0 = \mu_0 H$. Hence,

$$C_m = \left(\frac{\partial U}{\partial T} \right)_m$$

and

$$C_H = C_m + \left[\left(\frac{\partial U}{\partial m} \right)_T - \mu_0 H \right] \left(\frac{\partial m}{\partial T} \right)_H$$

2.3.0 Adiabats and Isotherms

2.3.1 Fire Syringe

A syringe with air and cotton wool at the bottom is the setup for the experiment. When the Piston is pushed down quickly, the compression of the air on top of the wool ignites it. Compressing the air forces the particles to collide closer together, causing the kinetic energy of the particles to quickly increase.

From the quick compression we reach the auto-ignition temperature for cotton, which is in the range of 400°C . If the compression is done too slowly, there is time for heat to escape into the air so there won't be enough to ignite the cotton. The compression in which no/minimal heat loss occurs due to how rapid the compression is is called an adiabatic compression. These observations lead to the following definition

Definition 2.3.1. An **adiabat** is a change in the state of a system such that $\delta Q = 0$. Hence, the 1st law simplifies to $dU = \delta W$ for adiabats.

2.3.2 Closed Systems (Adiabats)

We now consider the properties of adiabats for closed systems. In the case that $U = U(T, q_1, \dots, q_m)$, we can use the formulation of the first law $dU = \delta W + \delta Q$ and apply $\delta Q = 0$ to obtain

$$\frac{\partial U}{\partial T}(dT)_{ad} = \sum_{i=1}^m \left[J_i - \frac{\partial U}{\partial q_i} \right] (dq_i)_{ad}$$

where the subscript ad indicates that this expression is only valid for adiabats.

Example 2.3.1 (Gas). For a simple gas, we have $m = 1$ with generalized coordinate $q = V$ and generalized force $J = -p$. Hence:

$$\frac{\partial U}{\partial T}(dT)_{ad} = \left[-p - \frac{\partial U}{\partial V} \right] (dV)_{ad}$$

This implies that

$$\left(\frac{dT}{dV} \right)_{ad} = -\frac{p + \frac{\partial U}{\partial V}}{C_V}$$

recalling that

$$C_V = \frac{\partial U}{\partial T}$$

so this expression represents the change in temperature during an adiabatic process with respect to the change in volume. For an ideal gas, which has $U = U(T)$, this expression simplifies further to

$$\left(\frac{dT}{dV} \right)_{ad} = -\frac{p}{C_V} = -\frac{Nk_B T}{C_V V} = -\frac{(C_p - C_V) T}{C_V V} = -(\gamma - 1) \frac{T}{V}$$

where we define $\gamma := \frac{C_p}{C_v} \geq 1$, and where we have used the previously derived equality $C_p - C_v = Nk_B$ for an ideal gas. Under the assumption that γ is constant, this ordinary differential equation can be easily solved to obtain

$$TV^{\gamma-1} = \text{const.}$$

Using the equation of state for an ideal gas one can get the following two equivalent formulations:

$$\begin{aligned} pV^\gamma &= \text{const.} \\ T^\gamma p^{1-\gamma} &= \text{const.} \end{aligned}$$

We can then draw the following graphs:

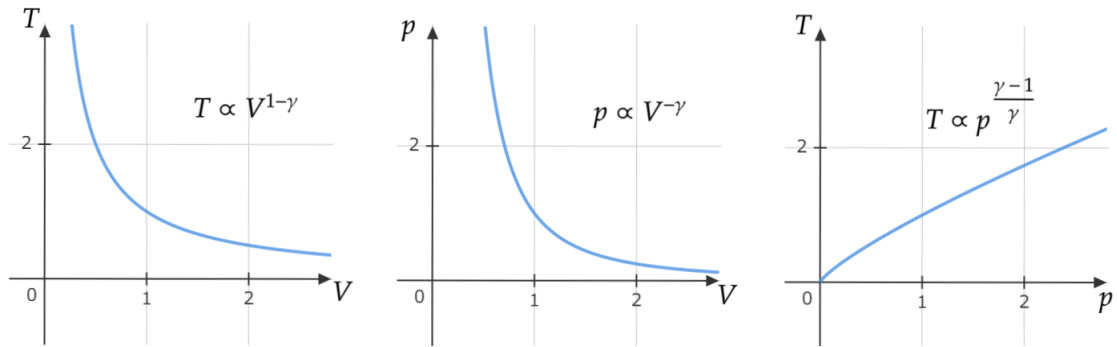
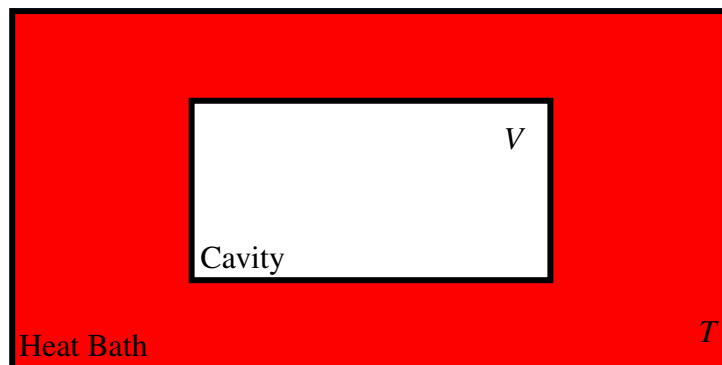


Figure 2.1: Relationships for temperature, pressure, and volume for an adiabatic process involving an ideal gas.

Some specific applications of adiabatic processes are as follows:

- Diesel engine (spontaneous explosion due to heating; no spark plugs)
- Chinooks (air pressure increases due to lower altitude)

Example 2.3.2 (Black-body radiation). We now deal with electromagnetic radiation in a cavity in thermal equilibrium, which is emitted by black walls. Here “black” means all radiation is absorbed:



Experiments show that $U = U(T, V) = V\epsilon(T)$, where ϵ is the energy density per volume. From classical electromagnetism, we also have $p = \frac{1}{3}\epsilon(T)$ for isotropic radiation (uniform radiation). The existence of a pressure from the classical perspective is similar to what we have for a gas. We can also borrow the wave-particle dualism from Quantum Mechanics. This suggests that we might be able to interpret or model black-body radiation as a **photon gas** (at least in a first approximation). Using our previous derivation for a gas we have

$$C_V = \frac{\partial U}{\partial T} = V \frac{d\epsilon}{dT}$$

and for adiabats we find then

$$\left(\frac{dT}{dV}\right)_{ad} = -\frac{p + \frac{\partial U}{\partial V}}{C_V} = -\frac{\frac{4}{3}\epsilon(T)}{V \frac{d\epsilon}{dT}}$$

We can rewrite this to obtain the simple ODE

$$-\frac{d\epsilon}{\epsilon} = \frac{4}{3} \frac{dV}{V}$$

The solution of this ODE can be written as

$$\epsilon V^{4/3} = \text{const.}$$

which has the equivalent form

$$p V^{4/3} = \text{const.}$$

given the relationship between p and ϵ for black-body radiation from above.

Since no heat is flowing in or out of the system in an adiabatic process, in the absence of any friction we can completely recover the original state of the system by reversing the procedure. Such a process also conserves entropy, as we will see later.

Definition 2.3.2. A thermodynamic process which is both adiabatic and reversible is said to be an **isentropic process**.

2.3.3 Isotherms

Definition 2.3.3. An **isotherm** is a change in the state of a system such that $dT = 0$.

This is not to be confused with an adiabatic process in which there is no heat transfer between the surroundings and the system. $dT = 0$ relates to a level surface, or manifold, associated to a constant empirical temperature Θ , which we use to define T .

Chapter 3

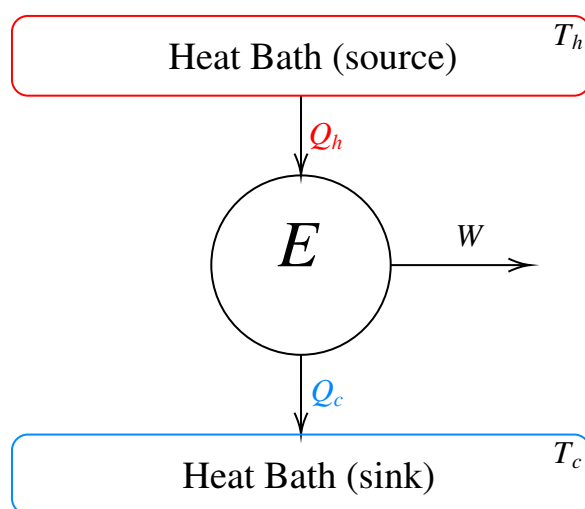
Thermodynamical Engines and Refrigerators

3.1.0 The 2nd Law of Thermodynamics

Recall from the first law we know that energy is conserved during all thermodynamic processes. This leaves the question as to whether all thermodynamic processes that conserve energy can actually occur. To answer this we focus on the conversion of heat to work in terms of engines:

Definition 3.1.1. An idealized heat engine is a thermodynamic system that runs in a cycle (i.e. it returns to the same internal thermodynamic states) taking in a certain amount of heat Q_h from a heat bath with temperature T_h , converting a portion of it to work $W > 0$ and dumping the remaining heat Q_c into a heat bath with $T_c < T_h$. The efficiency of a heat engine is given by

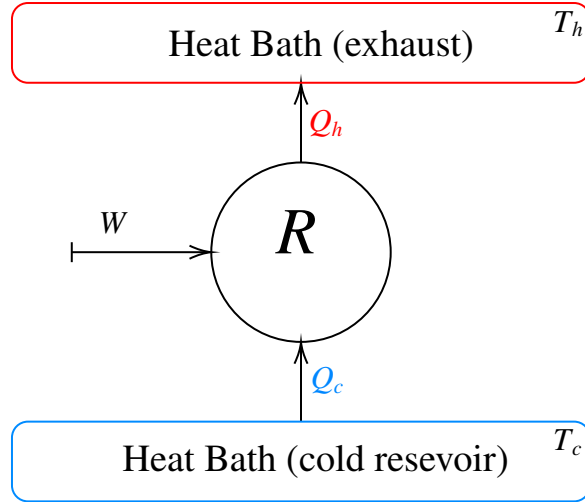
$$\eta = \frac{W}{Q_h} = \frac{Q_h - Q_c}{Q_h} = 1 - \frac{Q_c}{Q_h} \leq 1 \quad (3.1.1)$$



Definition 3.1.2. An idealized refrigerator can be considered as an idealized heat engine

running backwards, such that it uses work W to extract heat Q_c (e.g. from an ice box) and dump the heat Q_h at higher T_h (e.g. through an exhaust). The performance of a refrigerator is given by

$$w = \frac{Q_c}{W} = \frac{Q_c}{Q_h - Q_c} \quad (3.1.2)$$



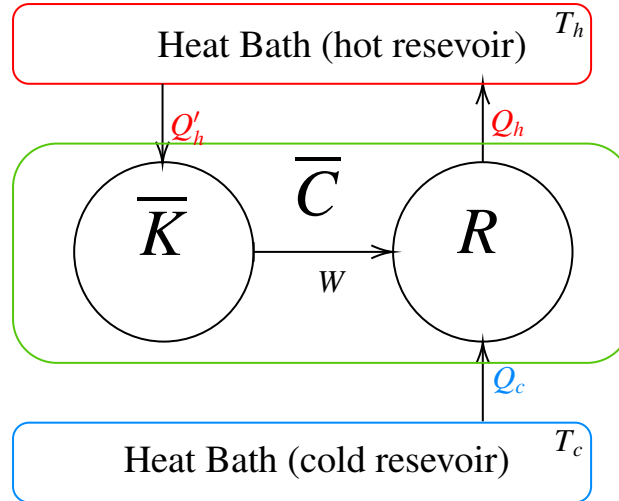
We will now give two formulations of the second law of thermodynamics:

Law (2nd Law of Thermodynamics (Kelvin)). *A thermodynamic machine or process that runs in a cycle and whose sole result is the complete conversion of heat from a single heat bath or reservoir into work is not possible.*

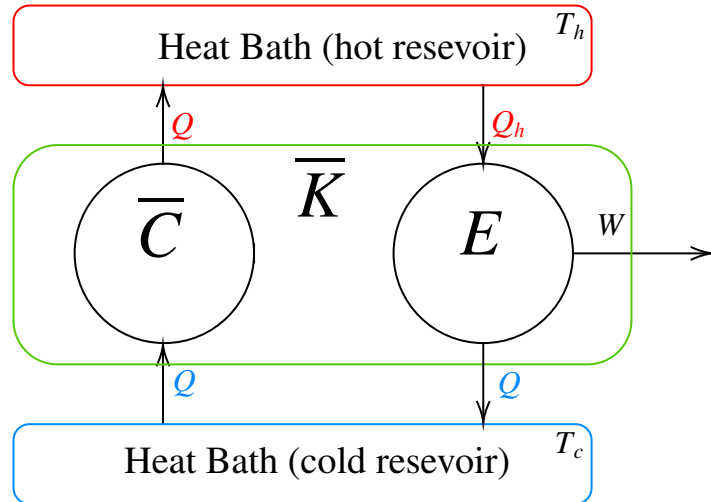
Law (2nd Law of Thermodynamics (Clausius)). *There is no thermodynamics machine or process that runs in a cycle and whose sole result is the transfer of heat from a colder to a hotter body.*

These two formulations are in fact equivalent, as we shall now prove:

Proof. To prove their equivalence, we shall show “not Kelvin” implies “not Clausius” and vice-versa. First, suppose that there exists a thermodynamic machine that runs in a cycle and whose sole result is the complete conversion of heat from a single heat bath or reservoir into work. Let T_h correspond to the reservoir of interest. Then, consider a refrigerator from a reservoir $T_c < T_h$ to T_h , and have the work come from our engine. Then, after the system as balanced, looking at the engine and refrigerator as a single machine we have that heat Q_c comes from the cold reservoir, and heat $Q_h - Q'_h$ is deposited in the hot reservoir, without any external work. Thus, such a machine violates Clausius, as desired, and as shown in the following diagram:



Next, suppose there exists a thermodynamic machine that runs in a cycle and whose sole result is the transfer of heat, Q , from a colder to a hotter body. Then, connect an engine that takes heat Q_h from the hotter body, does work W , and deposits heat Q_c to the colder body. It follows that the combined machine has input $Q_h - Q$ from the hot body, work output W , and heat output $Q_c - Q$. We then adjust the output of the heat engine such that $Q_c = Q$. Then we have obtained a machine violating Kelvin, as seen in the diagram:



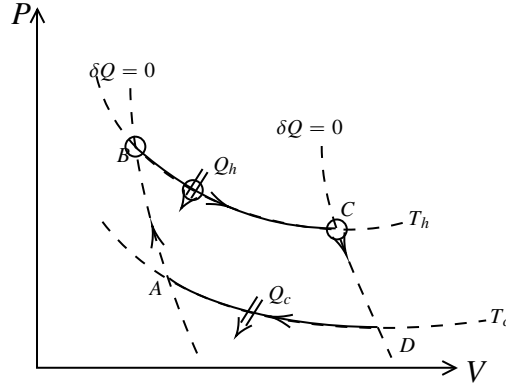
■

3.2.0 Carnot Engines

We now investigate the idea of the most efficient heat engine.

Definition 3.2.1. A Carnot engine is any heat engine that is reversible and runs in a cycle along two isotherms at temperatures T_h and T_c and adiabats. A reversible process is one that can be run backward in time by simply reversing its inputs and outputs.

Example 3.2.1 (Carnot Engine with an Ideal Gas as the Internal Working Substance). Here we have adiabatic compression of the gas, causing $\Delta T = T_h - T_c > 0$ ($A \rightarrow B$), then we have isothermal expansion with $\Delta Q_1 = Q_h > 0$ ($B \rightarrow C$), next we have adiabatic expansion which causes $\Delta T = T_c - T_h < 0$ ($C \rightarrow D$), and finally isothermal compression with $\Delta Q_2 = -Q_c < 0$ ($D \rightarrow A$).



Over one cycle, the 1st law gives us

$$0 = \oint dU = \Delta Q_1 + \Delta Q_2 + \Delta W$$

We calculate ΔW by considering the individual contributions:

- $A \rightarrow B$: adiabatic process, so $\delta Q = 0$, and $\delta W = dU$. Hence, $\Delta W_{AB} = U(T_h) - U(T_c)$, where we have used that $U = U(T)$ for an ideal gas.
- $B \rightarrow C$: isothermal process, so $dT = 0$. Hence, $p = p(V)$ for an ideal gas in a closed system setting ($pV = Nk_B T$) as temperature is a constant, and so

$$\Delta W_{BC} = - \int_B^C p(V) dV = -Nk_B T_h \int_{V_B}^{V_C} \frac{dV}{V} = -Nk_B T_h \ln \frac{V_C}{V_B}$$

- $C \rightarrow D$: another adiabatic process, so $\Delta W_{CD} = U(T_c) - U(T_h)$ as in $A \rightarrow B$
- $D \rightarrow A$: another isothermal process, so $\Delta W_{DA} = -Nk_B T_c \ln \frac{V_A}{V_D}$ as in $B \rightarrow C$

This gives the total work:

$$\Delta W = \Delta W_{AB} + \Delta W_{BC} + \Delta W_{CD} + \Delta W_{DA} = -Nk_B \left(T_h \ln \frac{V_C}{V_B} + T_c \ln \frac{V_A}{V_D} \right)$$

Recall that since we are dealing with adiabats, we have $TV^{\gamma-1} = \text{const}$, where the constant is the same along a given adiabat. This implies that $T_h V_B^{\gamma-1} = T_c V_A^{\gamma-1}$ and $T_h V_C^{\gamma-1} = T_c V_D^{\gamma-1}$. Dividing the first equation by the second and simplifying slightly gives $\frac{V_B}{V_C} = \frac{V_A}{V_D}$. Using this in the above equation we find

$$\Delta W = -Nk_B \ln \frac{V_D}{V_A} (T_h - T_c) < 0$$

Now, by definition the efficiency of a Carnot engine for an ideal gas is

$$\eta_{C,ideal\ gas} = \frac{W}{Q_h} = \frac{-\Delta W}{\Delta Q_1}$$

Now, since $U = U(T)$ for an ideal gas in a closed system, we have $\Delta U = 0$ for any isothermal process. Thus, during the isothermal expansion the 1st law gives us

$$\Delta Q_1 = -\Delta W_{BC} = Nk_B T_h \ln \frac{V_D}{V_A} > 0$$

using the identity between volume ratios $\frac{V_B}{V_C} = \frac{V_A}{V_D}$. Using the expressions for ΔW and ΔQ_1 , we obtain the efficiency

$$\eta_{C,ideal\ gas} = \frac{W}{Q_h} = \frac{-\Delta W}{\Delta Q_1} = 1 - \frac{T_c}{T_h}$$

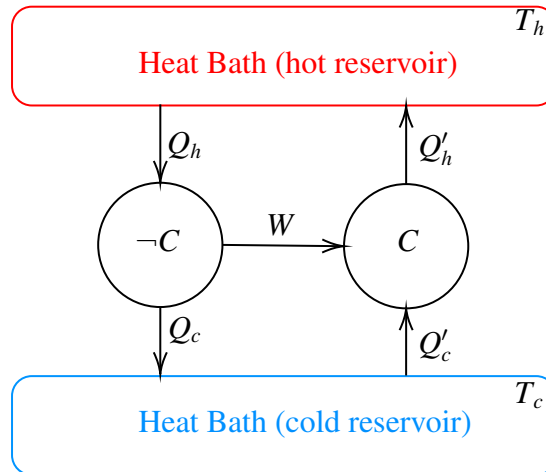
3.2.1 Carnot's Theorem

We can now address the question of which heat engine is the most efficient:

Theorem 2 (Carnot's Theorem).

No heat engine operating between two heat reservoirs (at temperatures T_h and T_c) is more efficient than a Carnot engine operating between them.

Proof. We start with any given heat engine and couple it with a Carnot engine, which is run in reverse as a refrigerator and powered by the other engine:



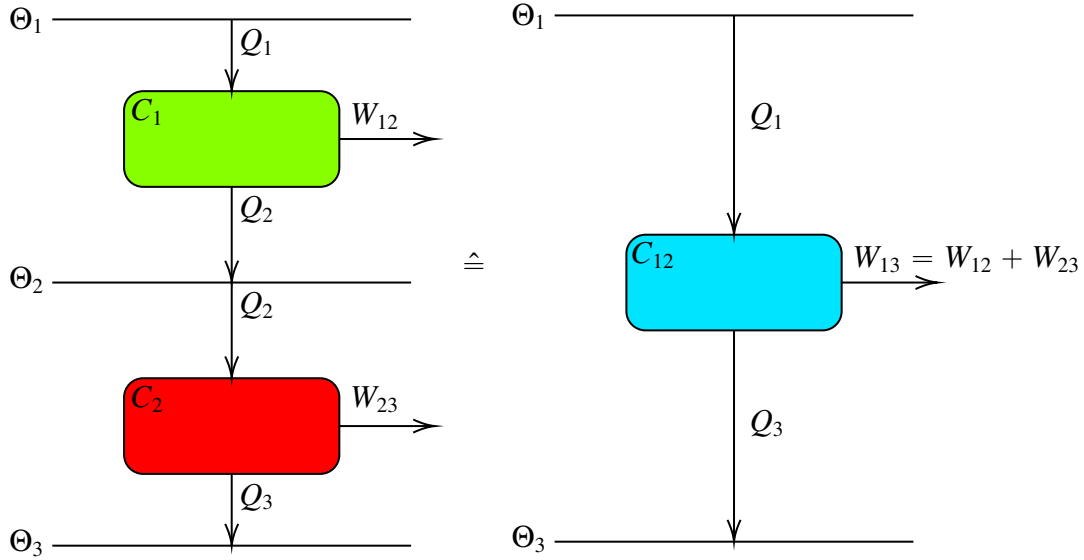
Instead of considering both engines in isolation, we can equivalently consider them as a combined engine, taking in heat $Q_h - Q'_h$, and outputting heat $Q_c - Q'_c$. As this combined machine runs in a cycle, so $\Delta U = 0$ over a cycle, and only exchanges heat with the outside world without doing any external work, we have $Q_h + Q'_c = Q_c + Q'_h$ based on the first law of thermodynamics. Moreover, the combined machine falls under the 2nd law of thermodynamics. Using the formulation by Clausius, we have $Q_h - Q'_h \geq 0$, so $Q_h \geq Q'_h$, and hence $\frac{W}{Q_h} \leq \frac{W}{Q'_h}$. This implies that $\eta \leq \eta_C$ (where the last implication uses the fact that Carnot engines are exactly reversible). ■

Corollary 3.2.1. *All reversible engines have the same universal efficiency $\eta = \eta_C(T_h, T_c) = 1 - \frac{T_c}{T_h}$.*

Proof. Each reversible Carnot engine can be used to run any other reversible heat engine backwards. ■

3.3.0 Thermodynamic Temperature Scale

Recall the 0th law ensures the existence of a temperature. For the ideal gas we can use the equation of state to define T , but this does not usually generalize to other systems. We now use the universal efficiency η_C of Carnot engines to establish a more general thermodynamic temperature scale. Consider two coupled Carnot engines with some empirical temperature scale Θ :



with $\Theta_1 > \Theta_2 > \Theta_3$. For the three efficiencies we have

$$\begin{aligned}\eta_C(\Theta_1, \Theta_2) &= 1 - \frac{\Theta_2}{\Theta_1} \\ \eta_C(\Theta_2, \Theta_3) &= 1 - \frac{\Theta_3}{\Theta_2} \\ \eta_C(\Theta_1, \Theta_3) &= 1 - \frac{\Theta_3}{\Theta_1}\end{aligned}$$

These can be rewriting to obtain

$$\Theta_2 = \Theta_1(1 - \eta_C(\Theta_1, \Theta_2))$$

$$\Theta_3 = \Theta_2(1 - \eta_C(\Theta_2, \Theta_3)) = \Theta_1(1 - \eta_C(\Theta_1, \Theta_2))(1 - \eta_C(\Theta_2, \Theta_3))$$

and

$$\Theta_3 = \Theta_1(1 - \eta_C(\Theta_1, \Theta_3))$$

Equating the last two equations and dividing out the empirical temperature we have that

$$(1 - \eta_C(\Theta_1, \Theta_2))(1 - \eta_C(\Theta_2, \Theta_3)) = (1 - \eta_C(\Theta_1, \Theta_3))$$

Defining the function $f \equiv 1 - \eta_C$, this can be written as $f(\Theta_1, \Theta_2)f(\Theta_2, \Theta_3) = f(\Theta_1, \Theta_3)$. To investigate the functional form of f let us take the logarithm to find

$$\ln f(\Theta_1, \Theta_2) + \ln f(\Theta_2, \Theta_3) = \ln f(\Theta_1, \Theta_3)$$

Taking the partial with respect to Θ_1 we obtain

$$\frac{\partial}{\partial \Theta_1} \ln f(\Theta_1, \Theta_2) = \frac{\partial}{\partial \Theta_1} \ln f(\Theta_1, \Theta_3)$$

For this equality to hold, the Θ_2 dependence on the left and the Θ_3 dependence on the right must both vanish. The only functional form of f that allows this is $f(\Theta_1, \Theta_2) = \alpha(\Theta_1)\beta(\Theta_2)$. Further, we have that

$$\alpha(\Theta_1)\beta(\Theta_2)\alpha(\Theta_2)\beta(\Theta_3) = \alpha(\Theta_1)\beta(\Theta_3)$$

which gives $\alpha(\Theta_2) = \beta^{-1}(\Theta_2)$. With this we find that

$$\eta_C(\Theta_1, \Theta_2) = 1 - \frac{\beta(\Theta_2)}{\beta(\Theta_1)}$$

Then, our new thermodynamic temperature scale is β , which can be fixed by setting $T^* \equiv \beta(\Theta^*)$ for a single heat bath. For example, we can use the triple point of water, ice and steam and set T^* to 273.15 K. Thus, rewriting the previous equation we have

$$T = T^*(1 - \eta_C(T^*, T))$$

Hence, using a heat bath at T^* as a reference point and operating a Carnot engine between the heat bath and any system of interest, the temperature of that system is given by the above expression, which requires the measurement of the efficiency of the Carnot engine in that arrangement.

3.4.0 Clausius' Teorem and Thermodynamic Entropy

Question 3.4.1. How does the efficiency limit of η_C affect the allowed heat exchanges for heat engines? More generally, what can we say about the heat increment supplied to a system during a cyclic process or transformation?

For a Carnot engine operating between $T_1 > T_2$, we have

$$1 - \frac{Q_c}{Q_h} \equiv \eta_C = 1 - \frac{T_2}{T_1},$$

where $Q_c > 0$ is the heat leaving the Carnot engine and Q_h is the heat entering the Carnot engine. From the perspective of the Carnot engine, its change in energy has a positive contribution $\Delta Q_1 = Q_h$ and a negative one $\Delta Q_2 = -Q_c$. Then we can rewrite our last equation as

$$1 + \frac{\Delta Q_2}{\Delta Q_1} = 1 - \frac{T_2}{T_1}$$

or equivalently

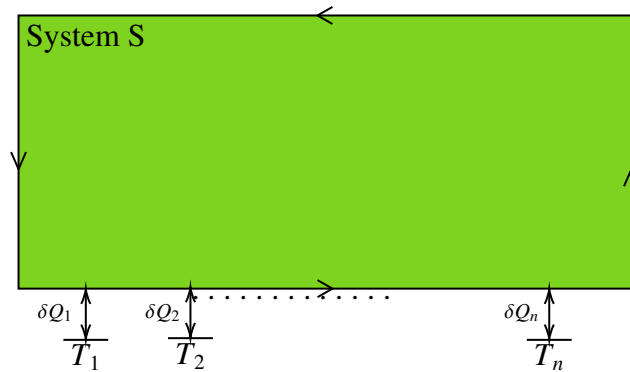
$$\frac{\Delta Q_2}{T_2} + \frac{\Delta Q_1}{T_1} = 0$$

which has the form of a **conservation law**: over one cycle, the sum over all heat exchanges, divided by the respective temperature, is zero for the Carnot engine.

Theorem 3 (Clausius' Theorem).

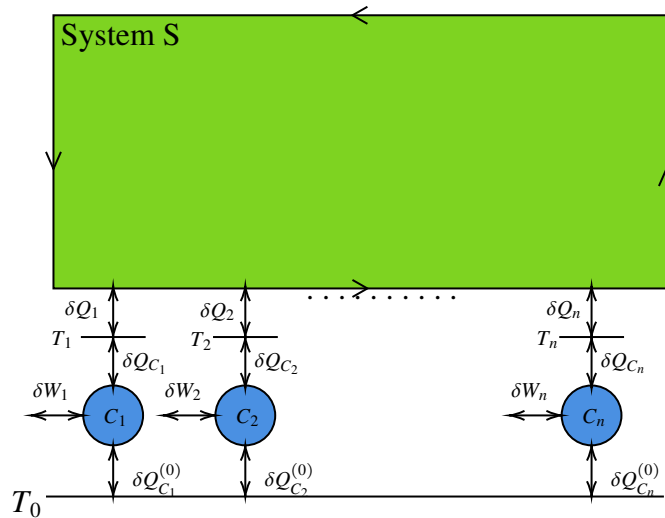
For any cyclic transformation (reversible or not), $\oint \frac{\delta Q}{T} \leq 0$, where δQ is the heat increment supplied to the system at temperature T .

Proof. Consider a system S that follows a general cyclic, quasi-static, process involving n heat exchanges δQ_i , positive or negative, with heat baths at temperatures T_i .



Over one cycle we necessarily have $\Delta U_S = 0$. The system might also perform a total amount of work ΔW_S over one cycle. Thus, the first law gives us $\Delta W_S = -\sum_{i=1}^n \delta Q_i$.

Next we can couple each heat bath to a Carnot engine, which operates between the given heat bath and a general heat bath at temperature T_0 with $T_0 > T_i$ for all $1 \leq i \leq n$.



Since we can operate each Carnot engine also as a refrigerator, we can require that $\delta Q_{C_i} = -\delta Q_i$ for all i . Thus, we have effectively removed the heat baths from the picture since the Carnot

engines either directly provide or receive the heat from the system in each step. Further, the combined system is effectively coupled to a single heat bath at T_0 , which will allow us to invoke the 2nd law. Given that we are dealing with Carnot engines, we can use the conservation law we established above. Specifically, we have

$$\delta Q_{C_i}^{(0)} = -\frac{T_0}{T_i} \delta Q_{C_i} = \frac{T_0}{T_i} \delta Q_i$$

Thus, for the total heat exchanged with the heat bath at T_0 over one cycle we have

$$\Delta Q^{(0)} = \sum_{i=1}^n \delta Q_{C_i}^{(0)} = T_0 \sum_{i=1}^n \frac{\delta Q_i}{T_i}$$

Considering now the combined system, its internal energy does not change over one cycle since it is a cyclic process. Thus, the first law gives us

$$-\Delta Q^{(0)} = \Delta W$$

over once cycle, where $\Delta W = \Delta W_S + \sum_{i=1}^n \delta W_i$ is the total external work done by the combined system over one cycle. Since the combined system is coupled to a single heat bath, Kelvin's formulation of the second law applies giving $\Delta W \geq 0$ (the system is not doing work on the surroundings). Combining the last three equations we can eliminate all reference to the Carnot engines and obtain

$$-T_0 \sum_{i=1}^n \frac{\delta Q_i}{T_i} \geq 0$$

Since $T_0 > 0$, this is equivalent to

$$\sum_{i=1}^n \frac{\delta Q_i}{T_i} \leq 0$$

In the limit as $n \rightarrow \infty$, this takes on the integral form given in Clausius' theorem. ■

3.4.1 Reversible Processes

We now investigate consequences of Clausius' theorem for reversible processes. For a reversible process any path γ in state space can be traced in reverse, $-\gamma$. For a cyclic process, this means that $\oint_{\gamma} \frac{\delta Q}{T} \leq 0$ and $\oint_{-\gamma} \frac{\delta Q}{T} \leq 0$, implying that

$$\oint_{\gamma} \frac{\delta Q}{T} = 0$$

Then, for reversible processes we find that $\frac{\delta Q}{T}$ is an exact differential, and it allows us to construct a new function of state

$$S(B) - S(A) \equiv \int_A^B \frac{\delta Q}{T}$$

where A and B are specific thermodynamic states and the integral is path-independent. S is called the thermodynamic entropy. In differential form this reads

$$dS = \frac{\delta Q}{T} \text{ or } \delta Q = T dS$$

The latter expression shows that adiabatic curves can be constructed for a general system from the condition of constant S , and it also allows us to reformulate the first law for reversible processes: in the case of a closed system

$$dU = \delta Q + \delta W = TdS + \sum_{i=1}^m J_i dq_i$$

3.4.2 Irreversible Processes

Consider two states A and B , and suppose we take one path from A to B , and one arbitrarily chosen reversible path from B back to A . Then by Clausius' theorem

$$\int_A^B \frac{\delta Q}{T} + \int_A^B \frac{\delta Q_{rev}}{T} \leq 0 \implies \int_A^B \frac{\delta Q}{T} \leq \int_A^B \frac{\delta Q_{rev}}{T} = \int_A^B dS = S(B) - S(A)$$

In differential form this reads

$$\frac{\delta Q}{T} \leq dS$$

for any transformation.

Note 3.4.2. Entropy has to be calculated along a reversible path.

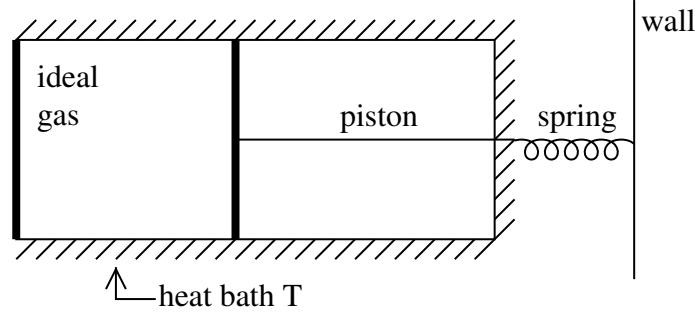
Hence, for irreversible processes $\frac{\delta Q}{T}$ is not exact so we can't use it to define the entropy. Further, for an isolated system there is no exchange of heat, so the above equation reduces to $\delta S \geq 0$ for all internal processes (entropy always increases in isolated systems). This implies that an isolated system attains a maximum value of entropy in equilibrium since spontaneous internal changes can only increase S . Hence, the direction of increasing entropy points out the arrow of time and the path to equilibrium.

Law (Second Law of Thermodynamics (Planck)). *If A and B are two isolated systems with fixed internal energies U_A and U_B and fixed entropies $S_A(U_A)$ and $S_B(U_B)$ before coupling, then the entropy of the compound system after coupling, $S(U_A + U_B)$, must be at least as large as the sum of the initial entropies*

$$S(U_A + U_B) \geq S_A(U_A) + S_B(U_B)$$

3.4.3 Example of Thermodynamic Entropy

We consider the isothermal expansion of an ideal gas. We first consider a reversible version:



The work done by the gas will be stored in the spring, making the process reversible (assuming an idealized frictionless spring). For an isothermal process, $T = \text{const}$. Since for an ideal gas we also have $U = U(T)$, this means that there is no change to the internal energy during this process. This fact together with the first law as our starting point, we have:

$$\Delta Q = -\Delta W = \int_{V_1}^{V_2} p dV = Nk_B T \int_{V_1}^{V_2} \frac{1}{V} dV = Nk_B T \ln \frac{V_2}{V_1}$$

where we have used the equation of state for an ideal gas and the fact that T and N are constant. For the change in entropy of the gas, this gives us

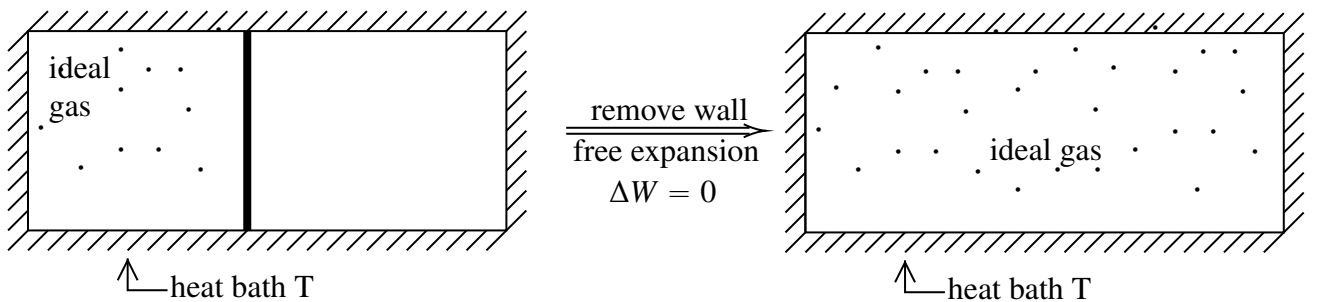
$$(\Delta S)_{gas} = \int_1^2 \frac{\delta Q}{T} = \frac{1}{T} \int_1^2 \delta Q = \frac{1}{T} \Delta Q = Nk_B \ln \frac{V_2}{V_1} > 0$$

Similarly, we can obtain the change in entropy for the heat bath:

$$(\Delta S)_{hb} = \int_1^2 \frac{\delta Q_{hb}}{T} = \frac{1}{T} \int_1^2 \delta Q_{hb} = \frac{\Delta Q_{hb}}{T} = \frac{-\Delta Q}{T} = -(\Delta S)_{gas}$$

Consequently, there is an entropy increase for the gas and an entropy decrease for the heat bath such that the combined change of entropy adds up to zero, $(\Delta S)_{total} = (\Delta S)_{gas} + (\Delta S)_{hb} = 0$.

Now, let us consider an irreversible process:



This process is irreversible since reintroducing the wall will not lead back to the original state. As for the reversible case, $\Delta U = 0$. Yet, no work is done, $\Delta W = 0$, and the first law gives $\Delta Q = 0$. To calculate the change in entropy we need a reversible process that has the same initial and final state as the irreversible one. The reversible version above can be used for that purpose. Thus

$$(\Delta S)_{gas} = Nk_B \ln \frac{V_2}{V_1} > 0$$

However, for the heat bath we have to take into account that $\Delta Q = 0 = \Delta Q_{hb}$ — the state of the heat bath did not change at all — which leads to

$$(\Delta S)_{hb} = \int_1^2 \frac{\delta Q_{hb}}{T} = 0$$

Consequently, there is an entropy increase for the gas and no change in entropy for the heat bath such that the combined change of entropy of the system is positive, $(\Delta S)_{total} = (\Delta S)_{gas} + (\Delta S)_{hb} = Nk_B \ln \frac{V_2}{V_1} > 0$. Multiplying this expression by T , we obtain

$$T(\Delta S)_{total} = Nk_B T \ln \frac{V_2}{V_1} > 0$$

where the left hand side is equivalent to the work done in the reversible case. Thus, the irreversible process wastes usable energy.

Chapter 4

Thermodynamical Potentials and Equilibrium

4.1.0 Thermodynamic Potentials

Recall that we have introduced thermodynamic entropy as a new state variable based on reversible processes. Now we answer the question

Question 4.1.1. How can we uniquely determine all equilibrium properties of a given system?

First, for reversible processes the 1st law reads

$$dU = \delta Q + \delta W + \delta E_{chem} = TdS + \sum_{i=1}^m J_i dq_i + \sum_{j=1}^{\alpha} \mu_j dN_j$$

so we have that $U = U(S, \vec{q}, \vec{N})$. Hence, the number of independent thermodynamic coordinates is $1 + m + \alpha$, assuming that there are no additional constraints between these coordinates. From this expression for the first law we have that

$$\begin{aligned} \left(\frac{\partial U}{\partial S} \right)_{\vec{q}, \vec{N}} &= T, \\ \left(\frac{\partial U}{\partial q_i} \right)_{S, q_{j \neq i}, \vec{N}} &= J_i \\ \left(\frac{\partial U}{\partial N_j} \right)_{S, \vec{q}, N_{i \neq j}} &= \mu_j \end{aligned}$$

Similarly, the function $U(S, \vec{q}, \vec{N})$ “generates” all other dependent thermodynamic quantities of interest through partial derivatives, including heat capacities, compressibilities, etcetera.

Definition 4.1.1. A function that uniquely determines all equilibrium properties of a given system is called a thermodynamic potential

Remark 4.1.2. The goal of thermodynamics is to do measurements such that one can construct a thermodynamic potential as a function of its arguments for a given system.

Statistical Mechanics aims to derive these thermodynamic potentials from the underlying microscopic dynamics.

4.1.1 Maxwell Relations

Requiring U to be a two time continuously differentiable function, using the relations derived above and the fact that the mixed partials will be equal we have the following:

Proposition 4.1.1. *Using the commutativity of mixed partials for two time continuously differentiable functions, we have the following Maxwell relations:*

$$\frac{\partial^2 U}{\partial q_i \partial S} = \frac{\partial^2 U}{\partial S \partial q_i} \iff \frac{\partial T}{\partial q_i} = \frac{\partial J_i}{\partial S} \quad (4.1.1)$$

and

$$\frac{\partial^2 U}{\partial N_j \partial S} = \frac{\partial^2 U}{\partial S \partial N_j} \iff \frac{\partial T}{\partial N_j} = \frac{\partial \mu_j}{\partial S} \quad (4.1.2)$$

4.1.2 Thermodynamic Entropy

Rewriting the first law for reversible processes we have

$$dS = \frac{1}{T} \left(dU - \sum_{i=1}^m J_i dq_i - \sum_{j=1}^{\alpha} \mu_j dN_j \right)$$

Hence, we can express entropy as $S = S(U, \vec{q}, \vec{N})$. Moreover, we can obtain all other thermodynamic quantities of interest through partials:

$$\begin{aligned} \left(\frac{\partial S}{\partial U} \right)_{\vec{q}, \vec{N}} &= \frac{1}{T}, \\ \left(\frac{\partial S}{\partial q_i} \right)_{U, q_{j \neq i}, \vec{N}} &= -\frac{J_i}{T}, \\ \left(\frac{\partial S}{\partial N_j} \right)_{U, \vec{q}, N_{i \neq j}} &= -\frac{\mu_j}{T} \end{aligned}$$

Thus, the thermodynamic entropy is a thermodynamic potential. If the arguments U, \vec{q}, \vec{N} are fixed there is no change in internal energy, no mechanical work is done, no chemical work is done, and there is no exchange of heat by the first law so we have an isolated system. Further, for an isolated system the thermodynamic entropy is maximal in equilibrium, so if entropy is expressed as a function of its natural variable U, \vec{q} and \vec{N} it is a thermodynamic potential with extremal properties.

4.1.3 Legendre Transformation

Consider an arbitrary smooth real valued function $f(x, y)$ defined on the plane, and consider its total differential $df = \frac{\partial f}{\partial x}dx + \frac{\partial f}{\partial y}dy$. We wish to replace the variable x with its conjugate variable $u = \frac{\partial f}{\partial x}$. First, consider the function $g(x, y, u) = ux - f(x, y)$. Its exact differential is

$$dg = d(ux) - df = xdu + udx - \frac{\partial f}{\partial x}dx - \frac{\partial f}{\partial y}dy$$

So that the dx terms cancel out we choose $u(x, y) = \frac{\partial f}{\partial x}$, which gives

$$dg = xdu - \frac{\partial f}{\partial y}dy \text{ and } g = g(u, y) = ux(u, y) - f(x(u, y), y)$$

where we have made the assumption that $u(x, y) = \frac{\partial f}{\partial x}$ is suitably nice (is an increasing function, and hence invertible) such that we can write x as a function of u and y . Under these assumptions g is the **Legendre transformation** of f with respect to x . We will now use the Legendre transformation to derive different thermodynamic potentials starting from the expression for the total differential of the internal energy for reversible processes

$$dU = TdS + \sum_{i=1}^m J_i dq_i + \sum_{j=1}^{\alpha} \mu_j dN_j$$

so $\partial_S U = T$, $\partial_{q_i} U = J_i$, and $\partial_{N_j} U = \mu_j$. Thus, T , \vec{J} and $\vec{\mu}$ fulfill the requirements to be used as new thermodynamic coordinates in a Legendre transformation of the internal energy provided the invertibility conditions hold.

4.1.4 Helmholtz Free Energy

Given that $\partial_S U = T$ we can replace S by T through a Legendre transformation of the internal energy. The new function is defined as follows:

Definition 4.1.2. The **Helmholtz free energy** is defined as

$$F(T, \vec{q}, \vec{N}) = U - TS$$

which is the negative of the standard Legendre transformation, and has total differential

$$dF = dU - d(TS) = dU - SdT - TdS = \sum_{i=1}^m J_i dq_i + \sum_{j=1}^{\alpha} \mu_j dN_j - SdT$$

such that

$$\begin{aligned} J_i &= \left(\frac{\partial F}{\partial q_i} \right)_{q_{j \neq i}, \vec{N}, T} \\ \mu_j &= \left(\frac{\partial F}{\partial N_j} \right)_{\vec{q}, N_{i \neq j}, T} \\ S &= - \left(\frac{\partial F}{\partial T} \right)_{\vec{q}, \vec{N}} \end{aligned}$$

Note that $U = F + TS = F - T \frac{\partial F}{\partial T}$, so we can derive all thermodynamic properties of a given system from the Helmholtz free energy making it a thermodynamic potential. From the partials we have the following:

Proposition 4.1.2. *Using the relations above for the Helmholtz free energy, we have the Maxwell relation*

$$\frac{\partial^2 F}{\partial q_i \partial T} = \frac{\partial^2 F}{\partial T \partial q_i} \iff -\frac{\partial S}{\partial q_i} = \frac{\partial J_i}{\partial T}$$

Example 4.1.1 (Ideal Gas). For an ideal gas, the Maxwell relation takes the form $-\frac{\partial S}{\partial V} = -\frac{\partial p}{\partial T}$, so $\frac{\partial S}{\partial V} = \frac{\partial p}{\partial T}$. Using the equation of state for an ideal gas we have

$$\frac{\partial S}{\partial V} = \frac{Nk_B}{V}$$

Integration of this partial differential equation gives

$$S(T, V, N) = S_0 + Nk_B \ln \frac{V}{V_0} + f(T, N)$$

where S_0 and V_0 are constants of integration and f is a function is an arbitrary function to be specified by other partials of S .

4.1.5 Enthalpy

Given that $\partial_{q_i} U = J_i$, we can replace \vec{q} by \vec{J} through a sequence of Legendre transformations of the internal energy. The new function is defined as follows:

Definition 4.1.3. The enthalpy of a thermodynamic system is defined by

$$\mathcal{H}(S, \vec{J}, \vec{N}) = U - \sum_{i=1}^m J_i q_i$$

(The negative of a sequence of Legendre transforms) with the exact differential

$$d\mathcal{H} = dU - \sum_{i=1}^m (J_i dq_i + q_i dJ_i) = TdS - \sum_{i=1}^m q_i dJ_i + \sum_{j=1}^{\alpha} \mu_j dN_j$$

with the partials

$$\begin{aligned} T &= \left(\frac{\partial \mathcal{H}}{\partial S} \right)_{\vec{J}, \vec{N}} \\ q_i &= - \left(\frac{\partial \mathcal{H}}{\partial J_i} \right)_{S, J_{j \neq i}, \vec{N}} \\ \mu_j &= \left(\frac{\partial \mathcal{H}}{\partial N_j} \right)_{S, \vec{J}, N_{i \neq j}} \end{aligned}$$

Consequently, enthalpy is also a thermodynamic potential. Then we obtain the Maxwell relations:

Proposition 4.1.3. *Using the mixed partials of the Enthalpy we have*

$$\frac{\partial^2 \mathcal{H}}{\partial S \partial J_i} = \frac{\partial^2 \mathcal{H}}{\partial J_i \partial S} \iff -\frac{\partial q_i}{\partial S} = \frac{\partial T}{\partial J_i}$$

4.1.6 Gibbs Free Energy

Performing a Legendre transformation on the Enthalpy by replacing S by T , we obtain the following function:

Definition 4.1.4. *The Gibbs free energy is defined by*

$$G(T, \vec{J}, \vec{N}) = U - TS - \sum_{i=1}^m J_i q_i$$

with the exact differential

$$dG = dU - TdS - SdT - \sum_{i=1}^m (J_i dq_i + q_i dJ_i) = -SdT - \sum_{i=1}^m q_i dJ_i + \sum_{j=1}^{\alpha} \mu_j dN_j$$

and the partials

$$\begin{aligned} S &= - \left(\frac{\partial G}{\partial T} \right)_{\vec{J}, \vec{N}} \\ q_i &= - \left(\frac{\partial G}{\partial J_i} \right)_{T, J_{j \neq i}, \vec{N}} \\ \mu_j &= \left(\frac{\partial G}{\partial N_j} \right)_{T, \vec{J}, N_{i \neq j}} \end{aligned}$$

Hence, the Gibbs free energy is also a thermodynamic potential. We also obtain the Maxwell relations:

Proposition 4.1.4. *Using the mixed partials of the Gibbs free energy we have*

$$\frac{\partial^2 G}{\partial T \partial J_i} = \frac{\partial^2 G}{\partial J_i \partial T} \iff \frac{\partial q_i}{\partial T} = \frac{\partial S}{\partial J_i}$$

4.1.7 Grand Potential

Finally, we use $\partial_{N_j} U = \mu_j$ to replace \vec{N} by $\vec{\mu}$ through a Legendre transformation, while also replacing S by T .

Definition 4.1.5. The grand potential is defined by

$$\mathcal{G}(T, \vec{q}, \vec{\mu}) = U - TS - \sum_{j=1}^{\alpha} N_j \mu_j$$

with the exact differential

$$d\mathcal{G} = -S dT + \sum_{i=1}^m J_i dq_i - \sum_{j=1}^{\alpha} N_j d\mu_j$$

$$S = - \left(\frac{\partial \mathcal{G}}{\partial T} \right)_{\vec{q}, \vec{\mu}}$$

$$J_i = \left(\frac{\partial \mathcal{G}}{\partial q_i} \right)_{T, q_{j \neq i}, \vec{\mu}}$$

$$N_j = \left(\frac{\partial \mathcal{G}}{\partial \mu_j} \right)_{T, \vec{q}, \mu_{i \neq j}}$$

Thus, the grand potential is also a thermodynamic potential. We also obtain the Maxwell relations:

Proposition 4.1.5. Using the mixed partials of the Gibbs free energy we have

$$\frac{\partial^2 \mathcal{G}}{\partial T \partial q_i} = \frac{\partial^2 \mathcal{G}}{\partial q_i \partial T} \iff \frac{\partial J_i}{\partial T} = - \frac{\partial S}{\partial q_i}$$

4.1.8 Example: Surface Tension of a Liquid

Consider the situation where the surface area of a liquid is increased from A to $A + dA$ at fixed volume V . The associated work due to surface tension σ is given by $\delta W_A = \sigma dA$. Experimentally, it has been established that $\sigma = \sigma(T) = \alpha(1 - T/T_c)$ with $\alpha > 0$ for $T < T_c$.

Based on the 1st law we have

$$dU = \delta Q + \delta W = \delta Q + \delta W_V + \delta W_A = TdS - pdV + \sigma dA$$

for reversible processes. Thus, $U = U(S, V, A)$.

Question 4.1.3. How does the temperature change if A changes?

To answer this we find $\frac{\partial T}{\partial A}$, which corresponds to an adiabatic ($\delta Q = 0 \iff dS = 0$) and isochoric ($dV = 0$) reversible process. Looking at the expression for U we can use a Maxwell relation

$$\frac{\partial T}{\partial A} = \frac{\partial \sigma}{\partial S} = \frac{\partial \sigma}{\partial T} \frac{\partial T}{\partial S} = \frac{d\sigma}{dT} \left(\frac{\partial S}{\partial T} \right)^{-1}$$

where we have used the chain rule together with the fact that $\sigma = \sigma(T)$. From the experimental form of σ above we have $\frac{d\sigma}{dT} = -\frac{\alpha}{T_c}$. From the expression for the internal energy $dU = TdS - pdV + \sigma dA$ we have

$$\begin{aligned} dS &= \frac{1}{T}(dU + pdV - \sigma dA) = \frac{1}{T} \left[\frac{\partial U}{\partial T} dT + \frac{\partial U}{\partial V} dV + \frac{\partial U}{\partial A} dA + pdV - \sigma dA \right] \\ &= \frac{1}{T} \left[\frac{\partial U}{\partial T} dT + \left(\frac{\partial U}{\partial V} + p \right) dV + \left(\frac{\partial U}{\partial A} - \sigma \right) dA \right] \end{aligned}$$

Hence, we can read off

$$\frac{\partial S}{\partial T} = \frac{1}{T} \frac{\partial U}{\partial T} = \frac{1}{T} C_{V,A}$$

Combining all of the above we get

$$\frac{\partial T}{\partial A} = \frac{d\sigma}{dT} \frac{T}{C_{V,A}} = \frac{-\alpha T}{C_{V,A} T_c} < 0$$

Thus, the temperature decreases with increasing surface area. Provided $C_{V,A} = \text{const}$, we find that $T = T_0 \exp \{-\gamma(A - A_0)\}$ with $\gamma \equiv \frac{\alpha}{C_{V,A} T_c} > 0$.

Question 4.1.4. How does the entropy change if A changes?

To ensure we don't have overlapping changes with other types of work, we need $V = \text{const}$ and since $\sigma = \sigma(T)$ we need $T = \text{const}$ to avoid having some changes in S arising from changes in σ . So we need to find $\left(\frac{\partial S}{\partial A}\right)_{T,V}$. Since we are considering the thermodynamic coordinates A, T, V we need to consider the Helmholtz free energy. Using $dU = TdS - pdV + \sigma dA$ we find

$$dF = d(U - TS) = -SdT - pdV + \sigma dA$$

Then we can read off the Maxwell relation

$$\frac{\partial S}{\partial A} = -\frac{\partial \sigma}{\partial T} = \frac{\alpha}{T_c} > 0$$

using the experimental expression for σ . Thus, for constant temperature and volume the thermodynamic entropy increases linearly with A .

Question 4.1.5. How does the internal energy change if A changes for an isothermal and isochoric reversible process?

We need to find $\left(\frac{\partial U}{\partial A}\right)_{T,V}$. From the expression for the internal energy we have that

$$\left(\frac{\partial U}{\partial A}\right)_{T,V} = T \left(\frac{\partial S}{\partial A}\right)_{T,V} + \sigma = \alpha \frac{T}{T_c} + \alpha(1 - T/T_c) = \alpha > 0$$

where we have used the result of the previous question and the given expression for σ . Thus, again we have a linear increase.

Question 4.1.6. How much heat is necessary to change the surface area from A_1 to A_2 for an isothermal and isochoric reversible process?

For a reversible process we have that $\delta Q = TdS$. For an isothermal process we only need to investigate the changes in entropy. Specifically, we need to find $S(T, A, V)$. We start with the Helmholtz free energy:

$$dF = -SdT - pdV + \sigma dA$$

Specifically, we can see that

$$\frac{\partial F}{\partial A} = \sigma = \sigma(T)$$

Integrating this expression gives

$$F(T, V, A) = \sigma(T)A + F_V(T, V)$$

such that the Helmholtz free energy is the sum of a surface term $F_A(T, V) \equiv \sigma(T)A$, and a volume term $F_V(T, V)$. Using this expression we can obtain S :

$$S = -\frac{\partial F}{\partial T} = -\frac{\partial F_A}{\partial T} - \frac{\partial F_V}{\partial T} = -A\frac{d\sigma}{dT} - \frac{\partial F_V}{\partial T}$$

Note only the first term depends on A , and the second term only depends on V and T which we are holding constant. Then, we have

$$\begin{aligned} \Delta Q &= T(S(T, V, A_2) - S(T, V, A_1)) = -T \left[\frac{\partial F_A}{\partial T}(T, A_2) - \frac{\partial F_A}{\partial T}(T, A_1) \right] \\ &= -T \left(A_2 \frac{d\sigma}{dT} - A_1 \frac{d\sigma}{dT} \right) = \alpha \frac{T}{T_c} (A_2 - A_1) \end{aligned}$$

using the given expression for σ .

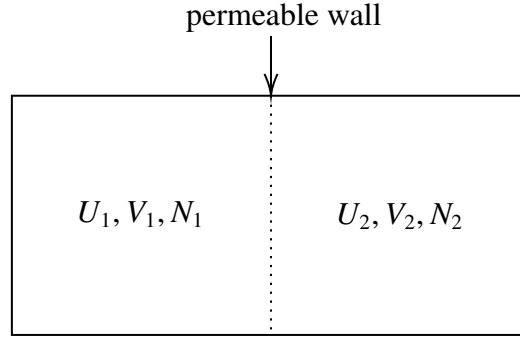
4.2.0 Approach to Equilibrium and Equilibrium Conditions

We aim to show that each thermodynamic potential takes on an extremal value in equilibrium in situations where their natural variables are held constant. This is a consequence of the 2nd law.

4.2.1 Isolated System

In this case we have $dU = 0$, $dq_i = 0$, and $dN_j = 0$, which implies that $\delta Q = 0$ based on the first law. It follows that $dS \geq \frac{\delta Q}{T} = 0$ and $dS = 0$ in equilibrium. Thus, entropy is maximal in equilibrium, given by $S = S(U, \vec{q}, \vec{N})$.

Now, let us consider a gas with a single particle type in a container that is subdivided into two compartments:



Since we are dealing with an isolated system we have $U \equiv U_1 + U_2 = \text{const}$, $V \equiv V_1 + V_2 = \text{const}$, $N \equiv N_1 + N_2 = \text{const}$, $S \equiv S_1(U_1, V_1, N_1) + S_2(U_2, V_2, N_2)$ such that different changes need to compensate, i.e., $dU_1 = -dU_2$, $dV_1 = -dV_2$, $dN_1 = -dN_2$. In equilibrium we also have

$$\begin{aligned} 0 &= dS = dS_1 + dS_2 \\ &= \left[\frac{\partial S_1}{\partial U_1} - \frac{\partial S_2}{\partial U_2} \right] dU_1 + \left[\frac{\partial S_1}{\partial V_1} - \frac{\partial S_2}{\partial V_2} \right] dV_1 + \left[\frac{\partial S_1}{\partial N_1} - \frac{\partial S_2}{\partial N_2} \right] dN_1 \\ &= \left(\frac{1}{T_1} - \frac{1}{T_2} \right) dU_1 + \left(\frac{p_1}{T_1} - \frac{p_2}{T_2} \right) dV_1 - \left(\frac{\mu_1}{T_1} - \frac{\mu_2}{T_2} \right) dN_1 \end{aligned}$$

For this expression to be true, all prefactors of the infinitesimal changes need to vanish since U_1 , V_1 , and N_1 are independent variables. Thus, we obtain that

$$T_1 = T_2, \quad p_1 = p_2, \quad \mu_1 = \mu_2,$$

meaning that temperature, pressure, and chemical potential are identical in both compartments in equilibrium. Inductively continuing this process of splitting the compartments into smaller parts, and repeating the argument, we find that in an isolated system in equilibrium, temperature, pressure, and chemical potential are the same everywhere.

4.2.2 Isolated System Coupled to a Heat Bath

In this case, we have $dT = 0$, $dq_i = 0$, and $dN_j = 0$, which corresponds to the natural variables of the Helmholtz free energy. Note that the heat bath is assumed to be sufficiently large such that its temperature fully controls the temperature of the system of interest. Starting from the second law and using the 1st law for this case we have

$$TdS \geq \delta Q = dU - \sum_{i=1}^m J_i dq_i - \sum_{j=1}^{\alpha} \mu_j dN_j = dU,$$

Since we also have $dT = 0$, we can rewrite this inequality as

$$d(TS) = TdS \geq dU \iff d(U - TS) \leq 0 \iff dF \leq 0$$

Hence, for all irreversible processes under the condition that $T = \text{const}$, $\vec{q} = \text{const}$, $\vec{N} = \text{const}$, the Helmholtz free energy decreases. In equilibrium $dF = 0$ and F is minimal.

Using a similar line of argument as the last case, we can show that pressure and chemical potential are everywhere the same in equilibrium in this case.

4.2.3 Isolated System Coupled to a Heat Bath and Exchanging Work with Constant External Forces

In this case we have $dT = 0$, $dJ_i = 0$, and $dN_j = 0$, which corresponds to the natural variables of the Gibbs free energy. Starting from the second law and then using the 1st we have

$$d(TS) = TdS \geq \delta Q = dU - \sum_{i=1}^m J_i dq_i - \sum_{j=1}^{\alpha} \mu_j dN_j = dU - d\left(\sum_{i=1}^m J_i q_i\right)$$

Rewriting this expression we obtain

$$dG = d\left(U - \sum_{i=1}^m J_i q_i - TS\right) \leq 0$$

Hence, for all irreversible processes under the condition that $T = \text{const}$, $\vec{J} = \text{const}$, $\vec{N} = \text{const}$, the Gibbs free energy decreases. In equilibrium, $dG = 0$ and G is minimal.

Again we can show that the chemical potential is everywhere the same in equilibrium in this case.

4.2.4 Closed System Exchanging Work with Constant External Forces and Heat at Constant Entropy

In this case we have $dS = 0$, $dJ_i = 0$ and $dN_j = 0$, which corresponds to the natural variables of the enthalpy. Starting from the 2nd law and then using the 1st law we have

$$0 = TdS \leq \delta Q = dU - \sum_{i=1}^m J_i dq_i - \sum_{j=1}^{\alpha} \mu_j dN_j = d\left(U - \sum_{i=1}^m J_i q_i\right) = d\mathcal{H}$$

Hence, for all irreversible processes under the condition that $S = \text{const}$, $\vec{J} = \text{const}$, $\vec{N} = \text{const}$, the enthalpy decreases. In equilibrium $d\mathcal{H} = 0$ and \mathcal{H} is minimal.

4.3.0 The Third Law of Thermodynamics

Recall our definition of thermodynamic entropy is only specified up to an additive constant. Empirical observations indicate that this constant is indeed constrained.

Law (Third Law of Thermodynamics (Nernst)). *The entropy of all systems at absolute zero temperature is a universal constant that can be taken to be 0, independent of the specific choice and value of the other state variables, for example $\lim_{T \rightarrow 0} S(T, \vec{q}, \vec{N}) = 0$ and $\lim_{T \rightarrow 0} S(T, \vec{J}, \vec{N}) = 0$.*

There are a number of consequences to this formulation of the third law:

Corollary 4.3.1. *All partial derivatives of the entropy with respect to any thermodynamic coordinate other than T vanish at zero temperature.*

Proof. Since $S(T = 0, \vec{X}) = 0$, $\lim_{T \rightarrow 0} \left. \frac{\partial S}{\partial \vec{X}} \right|_T = 0$ for all thermodynamic coordinates \vec{X} . ■

Corollary 4.3.2. *All heat capacities vanish at zero temperature.*

Proof. $C_{\vec{X}} = \left(\frac{\delta Q}{dT} \right)_{\vec{X}} = \left(T \frac{\partial S}{\partial T} \right)_{\vec{X}}$ implies that

$$S(T, \vec{X}) - S(0, \vec{X}) = \int_0^T dT' \frac{C_{\vec{X}}(T')}{T'} + f(\vec{X})$$

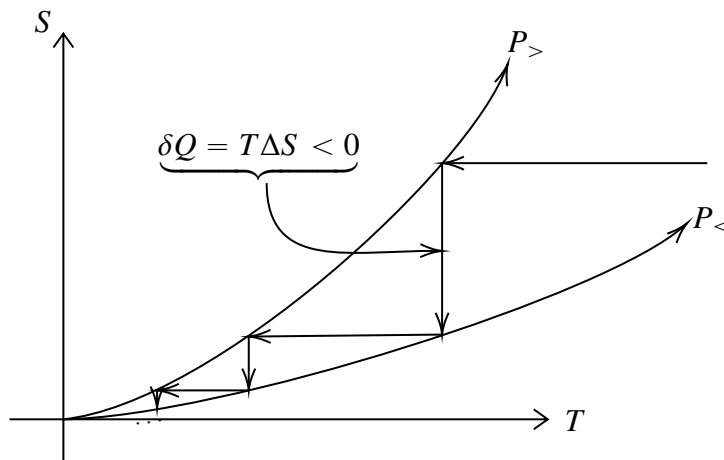
Due to the third law, $S(0, \vec{X}) = 0$ and due to the first consequence above $f(\vec{X}) = 0$. To ensure that $S(T, \vec{X})$ is finite, the integral needs to be finite, which requires that $\lim_{T \rightarrow 0} C_{\vec{X}}(T) = 0$. ■

Corollary 4.3.3. *All thermal expansivities vanish at zero temperature.*

Proof. $\beta_J \equiv \left. \frac{1}{q} \frac{\partial q}{\partial T} \right|_J = \left. \frac{1}{q} \frac{\partial S}{\partial J} \right|_T$, where we have used a Maxwell relation to obtain the last equality. Given the first consequence above, this implies that $\lim_{T \rightarrow 0} \beta_J = 0$. ■

Corollary 4.3.4. *It is impossible to cool any system to absolute zero temperature.*

We explore an example since the general proof is beyond the scope of this course. Consider the situation when we cool a gas by alternating between an adiabatic reduction in pressure ($dS = 0$) and an isothermal compression ($dT = 0$). As the sketch shows, it would require infinitely many steps to cool the system to absolute zero.



Part II

Statistical Mechanics

Chapter 5

Microstates and Entropy

Chapter 6

Ensemble Theory and Free Energy

Chapter 7

Boltzmann Statistics and the Canonical Ensemble

Chapter 8

Breakdown of Classical Statistical Mechanics

Part III

Probability Theory

Chapter 9

Characteristics of Probability Theory

9.1.0 Measure Theory

We first formalize the notion of a probability space:

Definition 9.1.1. A probability space (Ω, \mathcal{F}, P) is a measure space with a measure P that satisfies the probability axioms. Here, Ω is the non-empty set of all possible outcomes, \mathcal{F} is the σ -algebra of subsets of Ω , its elements are called events, and P is a function from \mathcal{F} to \mathbb{R} that assigns to each event a probability between 0 and 1.

The probability axioms are (Kolmogorov):

1. $P(E) \geq 0$ for all $E \in \mathcal{F}$ (positivity)
2. $P(\Omega) = 1$ (normalization)
3. $P(E_1 \cup E_2) = P(E_1) + P(E_2) - P(E_1 \cap E_2)$ for all $E_1, E_2 \in \mathcal{F}$ (additivity), so $P(E_1 \cup E_2) = P(E_1) + P(E_2)$ if $E_1 \cap E_2 = \emptyset$.

To deconstruct this formal definition we pursue certain measure theoretic terms:

Definition 9.1.2. A class of sets $\mathcal{A} \subseteq 2^\Omega$, for $\Omega \neq \emptyset$ a nonempty set, is called

- \cap -closed (closed under intersections) or a π -system if $A \cap B \in \mathcal{A}$ whenever $A, B \in \mathcal{A}$
- $\sigma - \cap$ -closed (closed under countable intersections) if $\bigcap_{n=1}^{\infty} A_n \in \mathcal{A}$ for any countable collection $\{A_n\}_{n=1}^{\infty} \subseteq \mathcal{A}$
- \cup -closed (closed under unions) if $A \cup B \in \mathcal{A}$ whenever $A, B \in \mathcal{A}$.
- $\sigma - \cup$ -closed (closed under countable unions) if $\bigcup_{n=1}^{\infty} A_n \in \mathcal{A}$ for any countable collection $\{A_n\}_{n=1}^{\infty} \subseteq \mathcal{A}$
- \setminus -closed (closed under differences) if $A \setminus B \in \mathcal{A}$ whenever $A, B \in \mathcal{A}$

- closed under complements if $A^c := \Omega \setminus A \in \mathcal{A}$ for any set $A \in \mathcal{A}$.

Definition 9.1.3 (σ -algebra). A class of sets $\mathcal{A} \subseteq 2^\Omega$ is called a σ -algebra if it fulfills the following three conditions:

- (i) $\Omega \in \mathcal{A}$
- (ii) \mathcal{A} is closed under complements
- (iii) \mathcal{A} is closed under countable unions

σ -algebras are the natural classes of sets to be considered as events in probability theory.

Definition 9.1.4. A class of sets $\mathcal{A} \subseteq 2^\Omega$ is called an algebra if the following three conditions are fulfilled:

- (i) $\Omega \in \mathcal{A}$
- (ii) \mathcal{A} is \setminus -closed
- (iii) \mathcal{A} is \bigcup -closed

Definition 9.1.5. A class of sets $\mathcal{A} \subseteq 2^\Omega$ is called a ring if the following three conditions hold:

- (i) $\emptyset \in \mathcal{A}$
- (ii) \mathcal{A} is \setminus -closed
- (iii) \mathcal{A} is \bigcup -closed

If it is also $\sigma - \bigcup$ -closed, then \mathcal{A} is called a σ -ring.

Definition 9.1.6. A class of sets $\mathcal{A} \subseteq 2^\Omega$ is called a semiring if

- (i) $\emptyset \in \mathcal{A}$
- (ii) for any two sets $A, B \in \mathcal{A}$ the difference $B \setminus A$ is a finite union of mutually disjoint sets in \mathcal{A}
- (iii) \mathcal{A} is \bigcap -closed

Definition 9.1.7. A class of sets $\mathcal{A} \subseteq 2^\Omega$ is called a λ -system (or Dynkin's λ -system) if

- (i) $\Omega \in \mathcal{A}$
- (ii) for any two sets $A, B \in \mathcal{A}$ with $A \subseteq B$, the difference $B \setminus A$ is in \mathcal{A}
- (iii) $\bigcup_{n=1}^{\infty} A_n \in \mathcal{A}$ for any countable collection of pairwise disjoint sets $\{A_n\}_{n=1}^{\infty} \subseteq \mathcal{A}$

Theorem 9.1.1.

- (i) Every σ -algebra is a λ -system, an algebra, and a σ -ring
- (ii) Every σ -ring is a ring, and every ring is a semiring
- (iii) Every algebra is a ring. An algebra on a finite set Ω is a σ -algebra.

Definition 9.1.8. Let A_1, A_2, \dots be subsets of Ω . The sets

$$\liminf_{n \rightarrow \infty} A_n := \bigcup_{n=1}^{\infty} \bigcap_{m=n}^{\infty} A_m \quad \text{and} \quad \limsup_{n \rightarrow \infty} A_n := \bigcap_{n=1}^{\infty} \bigcup_{m=n}^{\infty} A_m$$

are called **limes inferior** and **limes superior**, respectively, of the sequence $(A_n)_{n \in \mathbb{N}}$.

Equivalently these sets can be formulated as

$$\liminf_{n \rightarrow \infty} A_n = \{\omega \in \Omega : |\{n \in \mathbb{N} : \omega \notin A_n\}| < \infty\} \quad \limsup_{n \rightarrow \infty} A_n = \{\omega \in \Omega : |\{n \in \mathbb{N} : \omega \in A_n\}| = \infty\}$$

Thus, limes inferior is the event where eventually all of A_n occur, while limes superior is the event where infinitely many of the A_n occur.

Definition 9.1.9. The **indicator function** on the set A is defined by

$$\mathbb{I}_A(x) := \begin{cases} 1, & \text{if } x \in A, \\ 0, & \text{if } x \notin A, \end{cases}$$

Theorem 9.1.2. Let I be an arbitrary index set, and assume \mathcal{A}_i is a σ -algebra for every $i \in I$. Hence the intersection

$$\mathcal{A}_I := \bigcap_{i \in I} \mathcal{A}_i$$

is a σ -algebra. The analogous statement holds for rings, σ -rings, algebras, and λ -systems.

Theorem 9.1.3. Let $\mathcal{E} \subseteq 2^\Omega$. Then there exists a smallest σ -algebra $\sigma(\mathcal{E})$ with $\mathcal{E} \subseteq \sigma(\mathcal{E})$:

$$\sigma(\mathcal{E}) := \bigcap_{\substack{\mathcal{A} \subseteq 2^\Omega \\ \mathcal{E} \subseteq \mathcal{A} \\ \mathcal{A} \text{ is a } \sigma\text{-algebra}}} \mathcal{A}$$

$\sigma(\mathcal{E})$ is called the σ -algebra **generated by** \mathcal{E} . \mathcal{E} is called a **generator** of $\sigma(\mathcal{E})$. Similarly, we define $\delta(\mathcal{E})$ as the λ -system generated by \mathcal{E} .

Theorem 9.1.4. Let $\mathcal{D} \subseteq 2^\Omega$ be a λ -system. Then

$$\mathcal{D} \text{ is a } \pi\text{-system} \iff \mathcal{D} \text{ is a } \sigma\text{-algebra}$$

Theorem 4 (Dynkin's $\pi - \lambda$ theorem).

If $\mathcal{E} \subseteq 2^\Omega$ is a π -system, then $\sigma(\mathcal{E}) = \delta(\mathcal{E})$.

We are often interested in σ -algebras generated by topologies.

Definition 9.1.10. Let $\Omega \neq \emptyset$ be an arbitrary set. A class of sets $\tau \subseteq \Omega$ is called a **topology** on Ω if it has the following three properties:

- (i) $\emptyset, \Omega \in \tau$
- (ii) $A \cap B \in \tau$ for any $A, B \in \tau$
- (iii) $(\bigcup_{A \in \mathcal{F}} A) \in \tau$ for any $\mathcal{F} \subseteq \tau$

The pair (Ω, τ) is called a **topological space**. The sets $A \in \tau$ are called **open**, and the sets $A \subseteq \Omega$ with $A^c \in \tau$ are called **closed**.

Definition 9.1.11 (Borel σ -algebra). Let (Ω, τ) be a topological space. The σ -algebra

$$\mathcal{B}(\Omega) := \mathcal{B}(\Omega, \tau) := \sigma(\tau)$$

that is generated by the open sets is called the **Borel σ -algebra** on Ω . The elements $A \in \mathcal{B}(\Omega, \tau)$ are called **Borel sets** or **Borel measurable sets**.

Definition 9.1.12. Let $\mathcal{A} \subseteq 2^\Omega$ be an arbitrary class of subsets of Ω and let $A \in 2^\Omega \setminus \{\emptyset\}$. The class

$$\mathcal{A}|_A := \{A \cap B : B \in \mathcal{A}\} \subseteq 2^A$$

is called the **trace** of \mathcal{A} on A or the **restriction** of \mathcal{A} to A .

9.1.1 Set Functions

Definition 9.1.13. Let $\mathcal{A} \subseteq 2^\Omega$ and let $\mu : \mathcal{A} \rightarrow [0, \infty]$ be a set function. We say that μ is

- (i) **monotone** if $\mu(A) \leq \mu(B)$ for any two sets $A, B \in \mathcal{A}$ with $A \subseteq B$,
- (ii) **additive** if $\mu(\bigsqcup_{i=1}^n A_i) = \sum_{i=1}^n \mu(A_i)$ for any choice of finitely many mutually disjoint sets $A_1, \dots, A_n \in \mathcal{A}$ with $\bigsqcup_{i=1}^n A_i \in \mathcal{A}$
- (iii) **σ -additive** if $\mu(\bigsqcup_{i=1}^\infty A_i) = \sum_{i=1}^\infty \mu(A_i)$ for any choice of countably many mutually disjoint sets $A_1, A_2, \dots \in \mathcal{A}$ with $\bigsqcup_{i=1}^\infty A_i \in \mathcal{A}$
- (iv) **subadditive** if for any choice of finitely many sets $A, A_1, \dots, A_n \in \mathcal{A}$ with $A \subseteq \bigcup_{i=1}^n A_i$, we have $\mu(A) \leq \sum_{i=1}^n \mu(A_i)$,
- (v) **σ -subadditive** if for any choice of countably many sets $A, A_1, A_2, \dots \in \mathcal{A}$ with $A \subseteq \bigcup_{i=1}^\infty A_i$, we have $\mu(A) \leq \sum_{i=1}^\infty \mu(A_i)$,

Definition 9.1.14. Let \mathcal{A} be a semiring and let $\mu : \mathcal{A} \rightarrow [0, \infty]$ be a set function with $\mu(\emptyset) = 0$. μ is called a

- **content** if μ is additive,
- **premeasure** if μ is σ -additive
- **measure** if μ is a premeasure and \mathcal{A} is a σ -algebra,
- **probability measure** if μ is a measure and $\mu(\Omega) = 1$

Definition 9.1.15. Let \mathcal{A} be a semiring. A content μ on \mathcal{A} is called

- (i) **finite** if $\mu(A) < \infty$ for every $A \in \mathcal{A}$
- (ii) **σ -finite** if there exists a sequence of sets $\Omega_1, \Omega_2, \dots \in \mathcal{A}$ such that $\Omega = \bigcup_{n=1}^{\infty} \Omega_n$ and such that $\mu(\Omega_n) < \infty$ for all $n \in \mathbb{N}$.

Definition 9.1.16. For any $\omega \in \Omega$, δ_ω defined by $\delta_\omega(A) = \mathbb{1}_A(\omega)$ is a probability measure on any σ -algebra $\mathcal{A} \subseteq 2^\Omega$, and is called the **Dirac measure** for the point ω .

Definition 9.1.17. Let Ω be a finite nonempty set. The set function defined by

$$\mu(A) := \frac{|A|}{|\Omega|}$$

for all $A \subseteq \Omega$ defines a probability measure on $\mathcal{A} = 2^\Omega$. μ is called the **uniform distribution** on Ω . The resulting triple $(\Omega, \mathcal{A}, \mathcal{U}_\Omega)$ is called a **Laplace space** where $\mathcal{U}_\Omega := \mu$.

We remark that a countable linear combination of measures (resp. premeasures, contents) is once again a measure (resp. premeasure, content).

Definition 9.1.18. Let Ω be an at most countable nonempty set and let $\mathcal{A} = 2^\Omega$. Further, let $(p_\omega)_{\omega \in \Omega}$ be nonnegative numbers. Then $A \mapsto \mu(A) := \sum_{\omega \in A} p_\omega$ defines a σ -finite measure on 2^Ω . We call $p = (p_\omega)_{\omega \in \Omega}$ the **weight function** of μ . The number p_ω is called the weight of μ at point ω . If the sum over Ω , $\sum_{\omega \in \Omega} p_\omega$, equals one, then μ is a probability measure, and we call the weight function, $p = (p_\omega)_{\omega \in \Omega}$, a **probability vector**.

Lemma 9.1.5 (Properties of Contents). Let \mathcal{A} be a semiring and let μ be a content on \mathcal{A} . Then the following statements hold:

- (i) If \mathcal{A} is a ring, then $\mu(A \cup B) + \mu(A \cap B) = \mu(A) + \mu(B)$ for any two sets $A, B \in \mathcal{A}$
- (ii) μ is monotone. If \mathcal{A} is a ring, then $\mu(B) = \mu(A) + \mu(B \setminus A)$ for any two sets $A, B \in \mathcal{A}$ with $A \subseteq B$.
- (iii) μ is subadditive. If μ is σ -additive, then μ is also σ -subadditive.
- (iv) If \mathcal{A} is a ring, then $\sum_{n=1}^{\infty} \mu(A_n) \leq \mu\left(\bigcup_{n=1}^{\infty} A_n\right)$ for any choice of countably many mutually disjoint sets $A_1, A_2, \dots \in \mathcal{A}$ with $\bigcup_{n=1}^{\infty} A_n \in \mathcal{A}$

Theorem 9.1.6. Let \mathcal{A} be a ring and let μ be a content on \mathcal{A} . Let $n \in \mathbb{N}$ and $A_1, \dots, A_n \in \mathcal{A}$. Then the following inclusion and exclusion formulas hold:

$$\begin{aligned}\mu(A_1 \cup \dots \cup A_n) &= \sum_{k=1}^n (-1)^{k-1} \sum_{\{i_1, \dots, i_k\} \subseteq \{1, \dots, n\}} \mu(A_{i_1} \cap \dots \cap A_{i_k}), \\ \mu(A_1 \cap \dots \cap A_n) &= \sum_{k=1}^n (-1)^{k-1} \sum_{\{i_1, \dots, i_k\} \subseteq \{1, \dots, n\}} \mu(A_{i_1} \cup \dots \cup A_{i_k})\end{aligned}$$

where the second summation is over all subsets of $\{1, \dots, n\}$ with k elements.

Definition 9.1.19. Let A, A_1, A_2, \dots be sets. We write

- $A_n \uparrow A$ and say that $(A_n)_{n \in \mathbb{N}}$ increases to A if $A_1 \subseteq A_2 \subseteq \dots$ and $\bigcup_{n=1}^{\infty} A_n = A$
- $A_n \downarrow A$ and say that $(A_n)_{n \in \mathbb{N}}$ decreases to A if $A_1 \supseteq A_2 \supseteq \dots$ and $\bigcap_{n=1}^{\infty} A_n = A$

Definition 9.1.20 (Continuity of Contents). Let μ be a content on the ring \mathcal{A} .

- (i) μ is called lower semicontinuous if $\mu(A_n) \xrightarrow[n \rightarrow \infty]{\mu} \mu(A)$ for any $A \in \mathcal{A}$ and any sequence $(A_n)_{n \in \mathbb{N}}$ in \mathcal{A} with $A_n \uparrow A$
- (ii) μ is called upper semicontinuous if $\mu(A_n) \xrightarrow[n \rightarrow \infty]{\mu} \mu(A)$ for any $A \in \mathcal{A}$ and any sequence $(A_n)_{n \in \mathbb{N}}$ in \mathcal{A} with $\mu(A_n) < \infty$ for some (and then eventually all) $n \in \mathbb{N}$ and $A_n \downarrow A$.
- (iii) μ is called \emptyset -continuous if (ii) holds for $A = \emptyset$.

Theorem 9.1.7 (Continuity and Premeasure). Let μ be a content on the ring \mathcal{A} . Consider the following properties:

- μ is σ -additive
- μ is σ -subadditive
- μ is lower semicontinuous
- μ is \emptyset -continuous
- μ is upper semicontinuous

Then the following implications hold:

$$(i) \iff (ii) \iff (iii) \implies (iv) \iff (v)$$

If μ is finite, then we also have $(iv) \implies (iii)$.

Definition 9.1.21.

- A pair (Ω, \mathcal{A}) consisting of a nonempty set Ω and a σ -algebra $\mathcal{A} \subseteq 2^\Omega$ is called a **measurable space**. The sets $A \in \mathcal{A}$ are called **measurable sets**. If Ω is at most countably infinite and if $\mathcal{A} = 2^\Omega$, then the measurable space $(\Omega, 2^\Omega)$ is called **discrete**.
- A triple $(\Omega, \mathcal{A}, \mu)$ is called a **measure space** if (Ω, \mathcal{A}) is a measurable space and if μ is a measure on \mathcal{A} .
- If in addition $\mu(\Omega) = 1$, then $(\Omega, \mathcal{A}, \mu)$ is called a **probability space**. In this case, the sets $A \in \mathcal{A}$ are called **events**.
- The set of all finite measures on (Ω, \mathcal{A}) is denoted $\mathcal{M}_f(\Omega) := \mathcal{M}_f(\Omega, \mathcal{A})$. The subset of probability measures is denoted by $\mathcal{M}_1(\Omega) := \mathcal{M}_1(\Omega, \mathcal{A})$. Finally, the set of σ -finite measures on (Ω, \mathcal{A}) is denoted by $\mathcal{M}_\sigma(\Omega, \mathcal{A})$.

9.1.2 The Measure Extension Theorem

9.1.3 Measurable Maps

9.2.0 Random variables

We wish to model one or more random experiments as a probability space $(\Omega, \mathcal{A}, \mathbf{P})$. The sets $A \in \mathcal{A}$ are called **events**. Random observations, or variables, are measurable maps. The probabilities of the possible random observations are described in terms of the distribution of the corresponding random variable, which is the image measure of \mathbf{P} under X .

Definition 9.2.1 (Random Variables). Let (Ω', \mathcal{A}') be a measurable space and let $X : \Omega \rightarrow \Omega'$ be measurable.

- X is called a **random variable** with values in (Ω', \mathcal{A}') . If $(\Omega', \mathcal{A}') = (\mathbb{R}, \mathcal{B}(\mathbb{R}))$, then X is called a **real random variable** or simply a **random variable**.
- For $A' \in \mathcal{A}'$, we denote $\{X \in A'\} := X^{-1}(A')$ and $\mathbf{P}[X \in A'] := \mathbf{P}[X^{-1}(A')]$. In particular, we let $\{X \geq 0\} := X^{-1}([0, \infty))$ and define $\{X \leq b\}$ similarly, and so on.

Definition 9.2.2 (Distributions). Let X be a random variable.

- The probability measure $\mathbf{P}_X := \mathbf{P} \circ X^{-1}$ is called the **distribution** of X .
- For a real random variable X , the map $F_X : x \mapsto \mathbf{P}[X \leq x]$ is called the **distribution function of X** (or, more accurately, of \mathbf{P}_X). We write $X \sim \mu$ if $\mu = \mathbf{P}_X$ and say that X has **distribution μ** .
- A family $(X_i)_{i \in I}$ of random variables is called **identically distributed** if $\mathbf{P}_{X_i} = \mathbf{P}_{X_j}$ for all $i, j \in I$. We write $X \stackrel{\mathcal{D}}{=} Y$ if $\mathbf{P}_X = \mathbf{P}_Y$ (\mathcal{D} for distribution).

Theorem 9.2.1. For any distribution function F , there exists a real random variable X with $F_X = F$.

We now present prominent distributions of real random variables, before going into the specifics for thermodynamics:

Example 9.2.1.

- i Let $p \in [0, 1]$ and let $\mathbf{P}[X = 1] = p, \mathbf{P}[X = 0] = 1 - p$. Then $\mathbf{P}_X =: \text{Ber}_p$ is called the **Bernoulli distribution** with parameter p ; formally,

$$\text{Ber}_p = (1 - p)\delta_0 + p\delta_1$$

Its distribution function is

$$F_X(x) = \begin{cases} 0, & \text{if } x < 0, \\ 1 - p, & \text{if } x \in [0, 1) \\ 1, & \text{if } x \geq 1 \end{cases}$$

- ii Let $p \in [0, 1]$ and $n \in \mathbb{N}$, and let $X : \Omega \rightarrow \{0, \dots, n\}$ be such that

$$\mathbf{P}[X = k] = \binom{n}{k} p^k (1 - p)^{n-k}$$

Then $\mathbf{P}_X =: b_{n,p}$ is called the **binomial distribution** with parameters n and p ; formally

$$b_{n,p} = \sum_{k=0}^n \binom{n}{k} p^k (1 - p)^{n-k} \delta_k$$

- iii Let $p \in (0, 1]$ and $X : \Omega \rightarrow \mathbb{N}_0$ with

$$\mathbf{P}[X = n] = p(1 - p)^n \text{ for any } n \in \mathbb{N}_0$$

Then $\gamma_p := b_{1,p}^- := \mathbf{P}_X$ is called the **geometric distribution** with parameter p ; formally

$$\gamma_p = \sum_{n=0}^{\infty} p(1 - p)^n \delta_n$$

Its distribution function is $F(x) = 1 - (1 - p)^{\lfloor x+1 \rfloor \vee 0}$ for $x \in \mathbb{R}$.

- iv Let $r > 0$ and let $p \in (0, 1]$. We denote

$$b_{r,p}^- := \sum_{k=0}^{\infty} \binom{-r}{k} (-1)^k p^r (1 - p)^k \delta_k$$

the **negative binomial distribution** with parameters r and p , and where $\binom{x}{k} = \frac{x(x-1)\dots(x-k+1)}{k!}$ is the generalized binomial coefficient.

- v Let $\lambda \in [0, \infty)$ and let $X : \Omega \rightarrow \mathbb{N}_0$ be such that

$$\mathbf{P}[X = n] = e^{-\lambda} \frac{\lambda^n}{n!} \text{ for any } n \in \mathbb{N}_0$$

Then $\mathbf{P}_X =: \text{Poi}_\lambda$ is the **Poisson distribution** with parameter λ .

- vi Consider an urn with $B \in \mathbb{N}$ black balls and $W \in \mathbb{N}$ white balls. Draw $n \in \mathbb{N}$ balls from the urn without replacement. The probability of drawing exactly $b \in \{0, \dots, n\}$ black balls is given by the **hypergeometric distribution** with parameters $B, W, n \in \mathbb{N}$:

$$\text{Hyp}_{B,W,n}(\{b\}) = \frac{\binom{B}{b} \binom{W}{n-b}}{\binom{B+W}{n}}, \quad b \in \{0, \dots, n\}$$

Generally, the probability of drawing out of n balls exactly b_i of which of colour i for each $i = 1, \dots, k$, with the restriction $b_1 + \dots + b_k = n$ and $b_i \leq B_i$ for all i , is given by the **generalized hypergeometric distribution**

$$\text{Hyp}_{B_1, \dots, B_k, n}(\{(b_1, \dots, b_k)\}) = \frac{\binom{B_1}{b_1} \dots \binom{B_k}{b_k}}{\binom{B_1 + \dots + B_k}{n}},$$

- vii Let $\mu \in \mathbb{R}$, $\sigma^2 > 0$ and let X be a real random variable with

$$\mathbf{P}[X \leq x] = \frac{1}{\sqrt{2\pi\sigma^2}} \int_{-\infty}^x e^{-\frac{(t-\mu)^2}{2\sigma^2}} dt \quad \text{for } x \in \mathbb{R}$$

Then $\mathbf{P}_X =: \mathcal{N}_{\mu, \sigma^2}$ is called the **Gaussian normal distribution** with parameters μ and σ^2 . In particular, $\mathcal{N}_{0,1}$ is called the standard normal distribution.

- viii Let $\theta > 0$ and let X be a nonnegative random variable such that

$$\mathbf{P}[X \leq x] = \mathbf{P}[X \in [0, x]] = \int_0^x \theta e^{-\theta t} dt \quad \text{for } x \geq 0$$

Then \mathbf{P}_X is called the **exponential distribution** with parameter θ .

Definition 9.2.3. If the distribution function $F : \mathbb{R}^n \rightarrow [0, 1]$ is of the form

$$F(x) = \int_{-\infty}^{x_1} dt_1 \dots \int_{-\infty}^{x_n} dt_n f(t_1, \dots, t_n) \quad \text{for } x = (x_1, \dots, x_n) \in \mathbb{R}^n$$

for some integrable function $f : \mathbb{R}^n \rightarrow [0, \infty)$, then f is called the **density** of the distribution.

Example 9.2.2.

- i Let $\theta, r > 0$ and let $\Gamma_{\theta, r}$ be the distribution on $[0, \infty)$ with density

$$x \mapsto \frac{\theta^r}{\Gamma(r)} x^{r-1} e^{-\theta x}$$

where $\Gamma(r) = \int_0^\infty \theta^r x^{r-1} e^{-\theta x} dx$ is the gamma function. Then $\Gamma_{\theta, r}$ is called the **Gamma distribution** with scale parameter θ and shape parameter r .

- ii Let $r, s > 0$ and let $\beta_{r,s}$ be the distribution on $[0, 1]$ with density

$$x \mapsto \frac{\Gamma(r+s)}{\Gamma(r)\Gamma(s)} x^{r-1} (1-x)^{s-1}$$

Then $\beta_{r,s}$ is called the **Beta distribution** with parameters r and s .

9.3.0 States and Combined Events

Definition 9.3.1. A microstate is a specific outcome or elementary event.

Definition 9.3.2. A macrostate is a collection or union of microstates with some common property.

Consider the example of a gas. In this case, a microstate would correspond to a specific initial condition of all particles and a macrostate could correspond to all those microstates with the same U , N , and V .

For the Bernoulli process, we have

$$P_{micro,N} = P_H^{n_H} P_T^{n_T} = P_H^{n_H} (1 - P_H)^{N-n_H} = P_{micro,N}(n_H)$$

$$P_{macro,N} = \binom{N}{n_H} P_H^{n_H} P_T^{n_T} = \binom{N}{n_H} P_H^{n_H} (1 - P_H)^{N-n_H} = P_{macro,N}(n_H)$$

where n_H is the number of times heads occurs, n_T is the number of times tails occurs, and we have used $N = n_H + n_T$ and $P_H + P_T = 1$. Observe that

$$\sum_{n_H=0}^N P_{macro,N}(n_H) = \sum_{n_H=0}^N \binom{N}{n_H} P_H^{n_H} (1 - P_H)^{N-n_H} = (P_H + (1 - P_H))^N = 1$$

so $P_{macro,N}$ is normalized, as required. For a collection of independent identically distributed Bernoulli processes, we have the binomial distribution

$$P_N(n) = \binom{N}{n} P^n (1 - P)^{N-n}$$

Now, we look at the construction of probabilities of events from other events:

- i $P(E_1 \cup E_2) = P(E_2 \cup E_1) = P(E_1) + P(E_2)$ provided $E_1 \cap E_2 = \emptyset$
- ii If E_1 and E_2 are independent events, then $P(E_1 \cap E_2) = P(E_2 \cap E_1) = P(E_1)P(E_2)$
- iii $P(E_1 \cup E_2) = P(E_1) + P(E_2) - P(E_1 \cap E_2)$
- iv The conditional probability $P(E_2|E_1)$ corresponds to the probability that E_2 occurs given that E_1 occurred. By definition, this means that $P(E_2|E_1) = \frac{P(E_2 \cap E_1)}{P(E_1)}$.
- v We say that E_1 and E_2 are independent events if and only if $P(E_2|E_1) = P(E_2)$ and $P(E_1|E_2) = P(E_1)$.

9.4.0 Characteristics of Probability Distributions

We often wish to investigate certain key parameters related to the probability distributions associated with the events we are observing. We first introduce these for the case of discrete random variables:

Definition 9.4.1. The mean (or average or expectation value) for a discrete random variable X is

$$E[X] := \langle n \rangle := \sum_{n=0}^N n P_N(n)$$

where P_N is the probability distribution of X .

For the Binomial distribution we have a mean of

$$\begin{aligned} \langle n \rangle &= \sum_{n=0}^N n \binom{N}{n} P^n (1-P)^{N-n} \\ &= \sum_{n=0}^N n \frac{N!}{n!(N-n)!} P^n (1-P)^{N-n} \\ &= N \sum_{n=1}^N \frac{(N-1)!}{(n-1)!(N-n)!} P^n (1-P)^{N-n} \\ &= N \sum_{n=0}^{N-1} \binom{N-1}{n} P^{n+1} (1-P)^{N-n-1} \\ &= NP \sum_{n=0}^{N-1} \binom{N-1}{n} P^n (1-P)^{N-1-n} \\ &= NP \end{aligned}$$

Definition 9.4.2. The variance of a discrete random variable X is defined as follows

$$\begin{aligned} E[(X - E[X])^2] &:= \langle \Delta n^2 \rangle := \langle (n - \langle n \rangle)^2 \rangle := \sum_{n=0}^N (n - \langle n \rangle)^2 P_N(n) \\ &= \sum_{n=0}^N (n^2 + \langle n \rangle^2 - 2n\langle n \rangle) P_N(n) = \sum_{n=0}^N n^2 P_N(n) + \langle n \rangle^2 - 2\langle n \rangle^2 \\ &= \sum_{n=0}^N n^2 P_N(n) - \langle n \rangle^2 =: E[X^2] - E[X]^2 \end{aligned}$$

where we have used the fact that $P_N(n)$ is normalized and the definition of the mean.

For a binomial distribution we have the following variance:

$$\begin{aligned} E[X]^2 - E[X]^2 &= \sum_{n=0}^N n^2 \binom{N}{n} P^n (1-P)^{N-n} - N^2 P^2 \\ &= N \sum_{n=1}^N n \frac{(N-1)!}{(n-1)!(N-n)!} P^n (1-P)^{N-n} - N^2 P^2 \\ &= NP \sum_{n=0}^{N-1} (n+1) \binom{N-1}{n} P^n (1-P)^{N-1-n} - N^2 P^2 \end{aligned}$$

$$\begin{aligned}
 &= NP \left[\sum_{n=0}^{N-1} n \frac{(N-1)!}{n!(N-1-n)!} P^n (1-P)^{N-1-n} + \sum_{n=0}^{N-1} \binom{N-1}{n} P^n (1-P)^{N-1-n} \right] - N^2 P^2 \\
 &= NP \left[\sum_{n=1}^{N-1} \frac{(N-1)!}{(n-1)!(N-1-n)!} P^n (1-P)^{N-1-n} + 1 \right] - N^2 P^2 \\
 &= NP \left[(N-1)P \sum_{n=0}^{N-2} \frac{(N-2)!}{n!(N-2-n)!} P^n (1-P)^{N-2-n} + 1 \right] - N^2 P^2 \\
 &= NP [(N-1)P + 1] - N^2 P^2 \\
 &= N^2 P^2 - NP^2 + NP - N^2 P^2 = NP(1-P)
 \end{aligned}$$

Definition 9.4.3. The standard deviation of a random variable X is the square root of its variance:

$$SD[X] := \sqrt{E[(X - E[X])^2]} := \sigma := \sqrt{\langle \Delta n^2 \rangle}$$

Evidently the standard deviation of a binomial distribution is $\sigma = \sqrt{NP(1-P)}$.

Definition 9.4.4. The relative uncertainty of a random variable X is the ratio $\frac{SD[X]}{E[X]} = \frac{\sigma}{\langle n \rangle}$.

Chapter 10

Continuous Random Variables and the Gaussian Distribution

Chapter 11

Information and Entropy

Part IV

Real Gases and Phase Transitions

Chapter 12

Kinetic Theory of Gases

Chapter 13

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Part V

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Appendices