Example 1 - A Rankine cycle with CoolProp

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1 Example 1. A Rankine cycle with CoolProp.

First, take an initial look this notebook. Then, use "Kernel-> Restart & Run All" to re-evaluate the entire notebook. Running this notebook is a good test for your Python installation.

As a test for CoolProp, we plot the water saturation curve on a T-s diagram, as well as a classic Rankine cycle, between 80 bar and 80 mbar.

No more details will be given here. This will be done in the *Thermodynamique & Phénomènes de transport* course!

```
[1]: import numpy as np
  import matplotlib.pyplot as plt
  import CoolProp
  from CoolProp.CoolProp import PropsSI
  print('CoolProp version:', CoolProp.__version__)
```

CoolProp version: 6.3.0

```
[2]: Npts=400
```

```
[3]: pcrit = PropsSI('water', 'Pcrit')
  Tcrit = PropsSI('water', 'Tcrit')
  vcrit = 1./PropsSI('water', 'RHOCRIT')
  ptriple = PropsSI('water', 'ptriple')
  Ttriple = PropsSI('water', 'Ttriple')
```

```
[4]: Tstart = 283.15
Tend = Tcrit
sat_T = np.linspace(Tstart,Tend,Npts)[:-1]
```

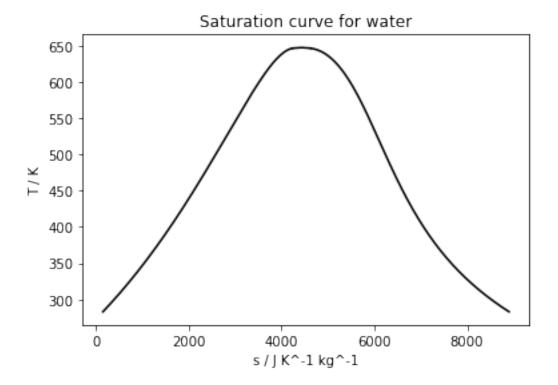
```
[5]: sat_s0 = PropsSI('S','T',sat_T,'Q',0.0,'water')
sat_s1 = PropsSI('S','T',sat_T,'Q',1.0,'water')
```

```
[6]: Scrit = (sat_s0[-1]+sat_s1[-1])/2.0
```

```
[7]: plt.plot(sat_s0,sat_T,'k')
plt.plot(sat_s1,sat_T,'k')
```

```
plt.plot([sat_s0[-1],Scrit,sat_s1[-1]],[sat_T[-1],Tcrit,sat_T[-1]],'k')
plt.ylabel('T / K')
plt.xlabel('s / J K^-1 kg^-1')
plt.title('Saturation curve for water')
```

[7]: Text(0.5, 1.0, 'Saturation curve for water')



```
[8]: # fix states
# state 1
p1=8.0e6
# version with sat. vapour ("real Rankine")
x1 = 1.0
h1=PropsSI('H','P',p1,'Q',x1,'water')
s1=PropsSI('S','P',p1,'Q',x1,'water')
T1=PropsSI('T','P',p1,'Q',x1,'water')

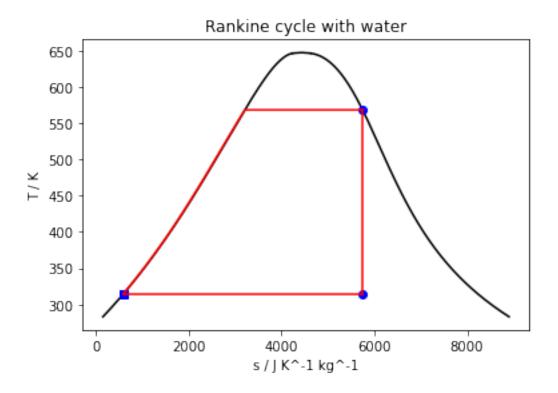
# state 2
p2=8.0e3
s2=s1
h2=PropsSI('H','P',p2,'S',s2,'water')
T2=PropsSI('T','P',p2,'S',s2,'water')
x2=PropsSI('Q','P',p2,'S',s2,'water')
```

```
# state 3
p3=p2
x3=0.0
h3=PropsSI('H','P',p3,'Q',x3,'water')
s3=PropsSI('S','P',p3,'Q',x3,'water')
T3=PropsSI('T','P',p3,'Q',x3,'water')

# state 4
p4=p1
s4=s3
h4=PropsSI('H','P',p4,'S',s4,'water')
T4=PropsSI('T','P',p4,'S',s4,'water')
x4=PropsSI('Q','P',p4,'S',s4,'water')
```

```
[9]: # plot saturation curve again
     plt.plot(sat_s0,sat_T,'k')
     plt.plot(sat s1,sat T,'k')
     plt.plot([sat_s0[-1],Scrit,sat_s1[-1]],[sat_T[-1],Tcrit,sat_T[-1]],'k')
     plt.ylabel('T / K')
     plt.xlabel('s / J K^-1 kg^-1')
     # plot states
     plt.plot(s1,T1,'bo')
     plt.plot(s2,T2,'bo')
     plt.plot(s3,T3,'bs')
     plt.plot(s4,T4,'bo')
     # plot processes
     ##isentrope s1-s2
     plt.plot([s1,s2],[T1,T2],'r')
     ##isobar s2-s3
     s isobar = np.linspace(s2,s3,Npts)
     T_isobar = PropsSI('T', 'S', s_isobar, 'P', p3, 'water')
     plt.plot(s_isobar,T_isobar,'r')
     ##isobar s4->s1
     s_isobar = np.linspace(s4,s1,Npts)
     T_isobar = PropsSI('T', 'S', s_isobar, 'P', p4, 'water')
     plt.plot(s_isobar,T_isobar,'r')
     plt.title('Rankine cycle with water')
```

[9]: Text(0.5, 1.0, 'Rankine cycle with water')



```
[10]: # calculate thermodynamic efficiency
eta = (-(h2-h1)-(h4-h3))/(h1-h4)
print("heat-to-work conversion efficiency: {0:4.1f} %".format(eta*100))
```

heat-to-work conversion efficiency: 37.1 %

1.1 End.

[]: