



**higher education
& training**

Department:
Higher Education and Training
REPUBLIC OF SOUTH AFRICA

MARKING GUIDELINE

NATIONAL CERTIFICATE

FLUID MECHANICS N5

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This marking guideline consists of 11 pages.

QUESTION 1

- 1.1 The purpose of bearing lubrication is to prevent direct metallic (metal to metal) contact between different rotating and sliding components in a mechanical mechanism. (2)
- 1.2
- Eliminates rapid material expansion due to the rise in temperature
 - Increases the expected life span of the material
 - Reduction of friction and wear
 - Dissipation of friction heat
 - Prevents metal decay due to corrosion
 - Protects against harmful elements
 - Power loss due friction (Any 2 × 1) (2)
- 1.3 The tendency to resist sliding layers of fluid measured in Pa.s. ✓ The kinetic viscosity is the ratio of the absolute viscosity to the mass ✓ density measured in m²/s. ✓ (3)
- 1.4 1.4.1
- $$from, F = \frac{\mu Av}{t}$$
- $$t = \frac{D-d}{2}$$
- $$= \frac{0,1503-150}{2} \checkmark$$
- $$= 150 \times 10^{-6} m \checkmark$$
- $$A = \pi DL$$
- $$= \pi \times 0,15 \times 0,17 \checkmark$$
- $$= 80,111 \times 10^{-3} m^2 \checkmark$$
- $$v = \pi DN$$
- $$= \pi \times 0,15 \times 20 \checkmark$$
- $$= 9,425 m/s \checkmark$$
- $$F = \frac{\mu Av}{t}$$
- $$= \frac{0,02 \times 80,111 \times 10^{-3} \times 9,425}{150 \times 10^{-6}} \checkmark$$
- $$= 100,673 N \checkmark$$
- $$P = Fv$$
- $$= 100,673 \times 9,425 \checkmark$$
- $$= 0,949 kW \checkmark$$
- (8)

1.4.2
$$v = \frac{\mu}{\rho}$$

$$= \frac{0,02}{830} \quad \checkmark$$

$$= 24,096 \times 10^{-6} \text{ m}^2 / \text{s} \quad \checkmark \quad (2)$$

1.4.3
$$\text{from, } P = Fv$$

$$t = 150,3 - 150 \quad \checkmark$$

$$= 300 \times 10^{-6} \text{ m} \quad \checkmark$$

$$P = \frac{0,02 \times 80,111 \times 10^{-3} \times 5}{300 \times 10^{-6}}$$

$$= 0,0267 \text{ kW} \quad \checkmark \quad (3)$$

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QUESTION 2

2.1 2.1.1
$$P_c = P_p \dots \text{Pascal's law}$$

$$\frac{F_c}{A_c} = \frac{F_p}{A_p} \quad \checkmark$$

$$F_p = \frac{d_c^2}{d_p^2} F_c \quad \checkmark$$

$$= \frac{0,68^2}{0,0425^2} \times (2550) \quad \checkmark$$

$$= 652,8 \text{ kN} \quad \checkmark \quad (3)$$

2.1.2
$$SV_c = SV_p$$

$$A_c \times SL_c = n A_p \times SL_p \quad \checkmark$$

$$n = \frac{d_c^2}{d_p^2} \times \frac{SL_c}{SL_p} \quad \checkmark$$

$$= \frac{0,68^2}{0,0425^2} \times \frac{3,4}{0,425} \quad \checkmark$$

$$= 2048 \text{ strokes} \quad \checkmark \quad (3)$$

2.1.3
$$WD = F_p \times sl$$

$$= 652,8 \times 3,4 \quad \checkmark$$

$$= 2219,52 \text{ J} \quad \checkmark \quad (2)$$

$$\begin{aligned}
 2.1.4 \quad P &= \frac{WD}{\text{time}} \\
 &= \frac{2219,5}{51} \checkmark \\
 &= 43,52W \checkmark
 \end{aligned}
 \tag{2}$$

$$\begin{aligned}
 2.2 \quad 2.2.1 \quad SV &= A \times SL \\
 &= \frac{\pi}{4} \times 0,06^2 \times 0,17 \checkmark \\
 &= 480,664 \times 10^{-3} m^3 \checkmark
 \end{aligned}
 \tag{2}$$

$$\begin{aligned}
 2.2.2 \quad P &= \frac{F}{A} \\
 &= \frac{4 \times 3,4 \times 10^3}{\pi \times 0,06^2} \checkmark \\
 &= 1,203 MPa \checkmark
 \end{aligned}
 \tag{2}$$

$$\begin{aligned}
 2.2.3 \quad K_{air} &= P\gamma \\
 &= 1,203 \times 1,4 \checkmark \\
 &= 1,684 MPa \checkmark
 \end{aligned}
 \tag{1}$$

$$\begin{aligned}
 2.2.4 \quad \text{from, } \frac{1}{K_e} &= \frac{1}{K_l} + \frac{1}{K_c} + \frac{V_{air}}{V_{total} K_{air}} \checkmark \\
 &= \frac{1}{2,035 \times 10^9} + \frac{2,5}{8,8 \times 10^9} + \frac{3,44 \times V_{total}}{100 V_{total} \times 1,684 \times 10^6} \checkmark \\
 &= 491,40049 \times 10^{-12} + 284,09091 \times 10^{-12} + 20,427553 \times 10^{-9} \checkmark \\
 \frac{1}{K_e} &= 21,203044 \times 10^{-9} \checkmark \\
 K_e &= 47,143 MPa \checkmark
 \end{aligned}
 \tag{3}$$

$$\begin{aligned}
 2.2.5 \quad \text{from, } P &= K_e \times \frac{\Delta V}{V_{total}} \\
 P &= K_e \times \frac{A \times \Delta L}{A \times SL} \checkmark \\
 \Rightarrow \Delta L &= \frac{1,203 \times 10^6}{47,143 \times 10^6} \times 0,17 \checkmark \\
 &= 4,336 mm \checkmark
 \end{aligned}
 \tag{2}$$

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QUESTION 3

- 3.1 3.1.1 $\bar{y} = \frac{d}{2}$
 $= \frac{1,45}{2} \quad \checkmark$
 $= 0,725m \quad \checkmark$
 $P = \rho g \bar{y}$
 $= 0,963 \times 1000 \times 9,81 \times 0,725 \quad \checkmark$
 $= 6,849kPa \quad \checkmark$ (3)
- 3.1.2 $F = PA$
 $= 6,849 \times \frac{\pi}{4} \times 1,45^2 \quad \checkmark$
 $= 11,31kN \quad \checkmark$ (2)
- 3.1.3 $I_G = \frac{\pi D^4}{64}$
 $= \frac{\pi \times 1,45^4}{64} \quad \checkmark$
 $= 216,991 \times 10^{-3} m^4 \quad \checkmark$ (2)
- 3.1.4 $\bar{h} = \bar{y} + \frac{I_G \sin^2 \theta}{A \bar{y}}$
 \checkmark
 $= 0,75 + \frac{216,991 \times 10^{-3}}{\frac{\pi \times 1,45^2}{4} \times 0,75} \quad \checkmark$
 $= 0,75 + 0,175208 \quad \checkmark$
 $= 925mm \quad \checkmark$ (3)
- 3.2 3.2.1 $F_b = W_m$
 $\rho g V_{displaced} = W_m \quad \checkmark$
 $as, V_{displaced} = 0,925 \times \frac{\pi}{6} \times 0,05^3 \quad \checkmark$
 $= 60,54111 \times 10^{-6} m^3 \quad \checkmark$
 $thus, W_m = 1260 \times 9,81 \times 60,54111 \times 10^{-6} \quad \checkmark$
 $= 784,324 \times 10^{-3} N \quad \checkmark$ (4)

$$3.2.2 \quad W_m = \rho g V_m$$

$$748,324 \times 10^{-3} = \rho \times 9,81 \times \frac{\pi \times 0,05^3}{6} \quad \checkmark$$

$$\rho = 1165,499 \text{ kg / m}^3 \quad \checkmark \quad (2)$$

$$3.2.3 \quad F_b = W_m + W_{added}$$

$$\rho g V_{\text{fully displaced}} = W_m + W_{added} \quad \checkmark$$

$$1260 \times 9,81 \times \frac{\pi}{6} \times 0,05^3 = 784,324 \times 10^{-3} + 9,81 m_{added} \quad \checkmark$$

$$808,999378 \times 10^{-3} - 748,324 \times 10^{-3} = 9,81 m_{added} \quad \checkmark$$

$$m_{added} = \frac{60,675378 \times 10^{-3}}{9,81}$$

$$m_{added} = 6,185 \times 10^{-3} \text{ kg} \quad \checkmark \quad (4)$$

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QUESTION 4

- 4.1 4.1.1 It is the path line or route followed by the fluid particles in motion which may never intersect each other,✓ where the line is instantaneous tangent to the velocity vector in the streamline at that particular point.✓
- 4.1.2 It is the imaginary boundary✓ or region of the fluid in motion restricted or confined by streamlines that are drawn to form a tubular region of fluid called a tube of flow, of which the fluid flowing never intersects these lines.✓
- 4.1.3 It is the path or route which a fluid particle follows in a fluid flow, where the path of each particle will be determined by the streamline route over a period of time.✓
- 4.1.4 This is the type of flow that is accompanied by indiscriminate✓ eddy currents causing the fluid particles to flow in a disorderly manner in relation to its path line.✓
- 4.1.5 This is the type of flow that is not accompanied by indiscriminate eddy currents,✓ causing the fluid particles to flow in an orderly manner without interfering with their adjacent path line.✓
- (5 × 2) (10)

4.2 4.2.1 $Q = \frac{\text{volume}}{\text{time}}$
 $= \frac{93,45 \times 10^{-3}}{21,96} \quad \checkmark$
 $= 4,256 \times 10^{-3} m^3 / s \quad \checkmark$ (1)

4.2.2 $Q = Av$
 $4,256 \times 10^{-3} = \frac{\pi}{4} \times 0,0549^2 v \quad \checkmark$
 $v = \frac{4,256 \times 10^{-3}}{2,367198 \times 10^{-3}} \quad \checkmark$
 $= 1,798 m / s \quad \checkmark$ (2)

4.3 4.3.1 *from, $Q = Av$*
 $v_{\phi 425} = \frac{4 \times \frac{10540 \times 10^{-3}}{60}}{\pi \times 0,425^2} \quad \checkmark$
 $= 1,238 m / s \quad \checkmark$ (2)

4.3.2 $v_{\phi 425} = \frac{4 \times \frac{10540 \times 10^{-3}}{60}}{\pi \times 0,2125^2} \quad \checkmark$
 $= 4,953 m / s \quad \checkmark$ (2)

4.3.3 $\frac{P_1}{\rho g} + \frac{v_1^2}{2g} + Z_1 - \sum h_{losses} = \frac{P_2}{\rho g} + \frac{v_2^2}{2g} + Z_2$
 $\frac{1351,5 \times 10^3}{9810} + \frac{1,238^2}{19,62} + 0 = \frac{P_2}{\rho g} + \frac{4,953^2}{19,62} + (-6,8)$
 $\frac{P_2}{9810} = 137,76758 + 0,0781164 + 6,8 - 1,250367 \quad \checkmark$
 $P_2 = 1,407 MPa \quad \checkmark$ (3)

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QUESTION 5

5.1 An orifice is an opening or hole in the bottom side of the tank used to discharge fluid at a given unit of time. (2)

5.2 5.2.1 *with the aid of Bernoulli's theorem :*

$$\begin{aligned} v_{\text{orifice}} &= \sqrt{2gh} \\ &= \sqrt{19,62 \times 59,4} \quad \checkmark \\ &= 34,138 \text{ m/s} \quad \checkmark \end{aligned} \quad (2)$$

5.2.2

$$\begin{aligned} \text{from, } Q &= Av_{\text{jet}} \\ v_{\text{jet}} &= \frac{4 \times 4,774 \times 10^{-3}}{\pi \times 0,0134^2} \quad \checkmark \\ &= 33,852 \text{ m/s} \quad \checkmark \end{aligned} \quad (2)$$

5.2.3

$$\begin{aligned} C_c &= \frac{A_j}{A_t} \\ &= \frac{d_j^2}{d_o^2} \quad \checkmark \\ &= \left(\frac{0,0134}{0,0145} \right)^2 \quad \checkmark \\ &= 0,854 \quad \checkmark \end{aligned} \quad (2)$$

5.2.4

$$\begin{aligned} C_v &= \frac{v_j}{v_o} \\ &= \frac{33,852}{34,138} \quad \checkmark \\ &= 0,992 \quad \checkmark \end{aligned} \quad (2)$$

5.2.5

$$\begin{aligned} C_q &= C_v \times C_c \\ &= 0,992 \times 0,854 \quad \checkmark \\ &= 0,847 \quad \checkmark \\ \text{Alternatively:} \\ C_q &= \frac{Q_j}{Q_o} \\ &= \frac{4,774}{\frac{34,138 \times \pi \times 0,0145^2}{4}} \quad \checkmark \\ &= 0,847 \quad \checkmark \end{aligned} \quad (2)$$

$$\begin{aligned}
 5.2.6 \quad h_{loss} &= h(1 - C_v^2) \\
 &= 59,4(1 - 0,992^2) \quad \checkmark \\
 &= 0,947m \quad \checkmark
 \end{aligned}$$

Alternatively :

$$\begin{aligned}
 h_{loss} &= h - \frac{v_j^2}{2g} \quad \checkmark \\
 &= 59,4 - \frac{33,852^2}{19,62} \\
 &= 0,992m \quad \checkmark
 \end{aligned}$$

(3)

5.3 with the aid of Bernoulli's equation :

$$\begin{aligned}
 \Delta h &= \frac{P_1 - P_2}{\rho g} \\
 &= \frac{6,8 \times 10^3}{9,81 \times 880} \quad \checkmark \\
 &= 787,69345mm \quad \checkmark \\
 \text{from, } Q &= C_Q \times a \frac{\sqrt{2g\Delta h}}{\sqrt{1 - \frac{a^2}{A^2}}} \\
 &= 0,715 \times \frac{\pi}{4} \times 0,2135^2 \times \frac{\sqrt{19,62 \times 787,69345 \times 10^{-3}}}{\sqrt{1 - \frac{\left(\frac{\pi \times 0,2135^2}{4}\right)^2}{\left(\frac{\pi \times 0,34^2}{4}\right)^2}}} \quad \checkmark \\
 &= \frac{0,0255972 \times 3,931227}{0,8445195} \quad \checkmark \\
 &= 120,899l/s \quad \checkmark
 \end{aligned}$$

(5)
[20]

QUESTION 6

6.1 $\overset{0}{from}, \overset{0}{W} = \overset{0}{m} g$
 as, $\overset{0}{Q}_{system} = \overset{0}{Q}_{in} = \overset{0}{Q}_{out} \dots \text{continuity of flow}$
 $\overset{0}{W} = \rho Q g$
 $= 820 \times \frac{\pi}{4} \times 0,22^2 \times 2,356 \times 9,81 \quad \checkmark$
 $= 720,433 N / s \quad \checkmark \quad (2)$

6.2 $\overset{0}{Q}_{system} = \overset{0}{Q}_{in} = \overset{0}{Q}_{out} \dots \text{continuity of flow}$
 $A_{in} v_{in} = A_{out} v_{out}$
 $v_{out} = \frac{d_{in}^2}{d_{out}^2} \times v_{in} \quad \checkmark$
 $= \frac{0,22^2}{0,125^2} \times 2,356 \quad \checkmark$
 $= 7,298 m / s \quad \checkmark \quad (2)$

6.3 $\overset{0}{from}, \overset{0}{m}_{system} = \overset{0}{m}_{in} = \overset{0}{m}_{out} \dots \text{continuity of flow}$
 as, $\overset{0}{m} = \rho Q$
 $= 820 \times \pi \times \frac{0,22^2}{4} \times 2,356 \quad \checkmark$
 $= 73,439 kg / s \quad \checkmark \quad (2)$

6.4 *Applying Bernoulli's equation between the bend inlet and outlet :*
 $E_1 - H_{loss} = E_2$
 $\frac{P_{in}}{\rho g} + \frac{v_{in}^2}{2g} + Z_{in} - H_{loss} = \frac{P_{out}}{\rho g} + \frac{v_{out}^2}{2g} + Z_{out} \quad \checkmark$
 $\Rightarrow \frac{P_{out}}{\rho g} = \frac{P_{in}}{\rho g} + \frac{v_{in}^2}{2g} + Z_{in} - \frac{v_{out}^2}{2g} - Z_{out} - H_{loss} \quad \checkmark$
 $\frac{P_{out}}{820 \times 9,81} = \frac{86,856 \times 10^3}{820 \times 9,81} + \frac{2,356^2}{19,62} + 0 - 1,35 - \frac{7,298^2}{19,62} - 1,063 \quad \checkmark$
 $P_{out} = 820 \times 9,81 \times 5,952639 \quad \checkmark$
 $= 47,884 kPa \quad \checkmark \quad (4)$

6.5 $\overset{0}{F}_{in} = \overset{0}{m}_{in} v_{in}$
 $= 73,439 \times 2,356 \quad \checkmark$
 $= 173,022 N \quad \checkmark \quad (1)$

$$\begin{aligned}
 6.6 \quad F_{in} &= P_{in} A_{in} \\
 &= 86,856 \times 10^3 \times \frac{\pi}{4} \times 0,22^2 \sqrt{} \\
 &= 3301,681 N \sqrt{}
 \end{aligned}
 \tag{1}$$

$$\begin{aligned}
 6.7 \quad F_{out} &= m_{out}^0 v_{out} \\
 &= 73,439 \times 7,298 \sqrt{} \\
 &= 535,956 N \sqrt{}
 \end{aligned}
 \tag{1}$$

$$\begin{aligned}
 6.8 \quad F_{out} &= P_{out} A_{out} \\
 &= 47,884 \times 10^3 \times \frac{\pi}{4} \times 0,125^2 \sqrt{} \\
 &= 587,625 N \sqrt{}
 \end{aligned}
 \tag{1}$$

$$\begin{aligned}
 6.9 \quad F_x &= F_{in} - F_{out} \cos \theta \\
 &= (173,022 + 3301,681) - (535,956 + 587,625) \cos 52^\circ \sqrt{} \\
 &= 2782,95 N \checkmark \\
 F_y &= (535,956 + 587,625) \sin 52^\circ \sqrt{} \\
 &= 885,394 N \sqrt{} \\
 \text{from, } F_r^2 &= F_x^2 + F_y^2 \\
 F_r &= \sqrt{2782,95^2 + 885,394^2} \sqrt{} \\
 &= 2920,4 N \sqrt{}
 \end{aligned}
 \tag{4}$$

$$\begin{aligned}
 6.10 \quad \tan \theta &= \frac{F_y}{F_x} \\
 &= \tan^{-1} \left(\frac{885,394}{2782,95} \right) \checkmark \\
 &= 17,648^\circ \checkmark
 \end{aligned}
 \tag{2}$$

[20]**TOTAL: 100**