

6.6

a) Calculate the range of temperatures within which the vapor-air mixture above the liquid surface in a can of n-hexane at atmospheric pressure will be flammable. Data are found in Table 4.5.

a) The boiling temperature at 1 atmosphere is shown below.

$$T_b := 342 \quad P_{kpa} := 101000$$

The lower and upper flammability limits and the latent heat are:

$$x_l := 0.012 \quad x_u := 0.074 \quad h_{fg} := 0.35 \cdot 1000$$

The universal gas constant and themolecular weight are found.

$$R_{gas} := 8.314 \quad M1 := 12 \cdot 6 + 14 \quad M1 = 86$$

Invert C-C for the temperature in terms of the mole fraction.

$$T_l := \left(\frac{1}{T_b} - \frac{R_{gas} \cdot \ln(x_l)}{h_{fg} \cdot M1} \right)^{-1} \quad T_l = 241.218 \text{ K}$$

$$T_u := \left(\frac{1}{T_b} - \frac{R_{gas} \cdot \ln(x_u)}{h_{fg} \cdot M1} \right)^{-1} \quad T_u = 274.488 \text{ K}$$

b) Calculate the range of ambient pressures within which the vapor-air mixture above the liquid surface in a can of n-hexane or n-decane will be flammable at 25C.

We first need to get the vapor pressure at 25C. Once we know the vapor pressure we then find the atmospheric pressure that allows the vapor pressure divided by atmospheric pressure to equal the mole fraction.

If we are looking for n-hexane results we get: $T_e := 25 + 273$

$$P_{vap} := \exp\left[-hfg \cdot \frac{M1}{R_{gas}} \cdot \left(\frac{1}{T_e} - \frac{1}{T_b}\right)\right] \cdot P_{kpa} \quad P_{vap} = 2.116 \times 10^4$$

$$P_{low} := \frac{P_{vap}}{x_l} \quad P_{up} := \frac{P_{vap}}{x_u} \quad P_{low} = 1.763 \times 10^6 \text{ Pa} \quad P_{up} = 2.859 \times 10^5 \text{ Pa}$$

For n-decane

The boiling temperature at 1 atmosphere is shown below.

$$T_b := 447 \quad P_{kpa} := 101000$$

The lower and upper flammability limits and the latent heat are:

$$x_l := 0.006 \quad x_u := 0.054 \quad hfg := 0.28 \cdot 1000$$

The universal gas constant and themolecular weight are found.

$$R_{gas} := 8.314 \quad M1 := 12 \cdot 10 + 22 \quad M1 = 142$$

$$P_{vap} := \exp\left[-hfg \cdot \frac{M1}{R_{gas}} \cdot \left(\frac{1}{T_e} - \frac{1}{T_b}\right)\right] \cdot P_{kpa} \quad P_{vap} = 479.888 \text{ Pa}$$

$$P_{low} := \frac{P_{vap}}{x_l} \quad P_{low} = 7.998 \times 10^4 \text{ Pa} \quad \frac{P_{low}}{101000} = 0.792 \text{ atm}$$

$$P_{up} := \frac{P_{vap}}{x_u} \quad P_{up} = 8.887 \times 10^3 \text{ Pa} \quad \frac{P_{up}}{101000} = 0.088 \text{ atm}$$

$$x_{u1} := 6.5 \cdot (0.6)^{.5} \quad x_{u1} = 5.035$$