

SEPARATION OF METHANOL, WATER AND DIMETHYL FORMIDE

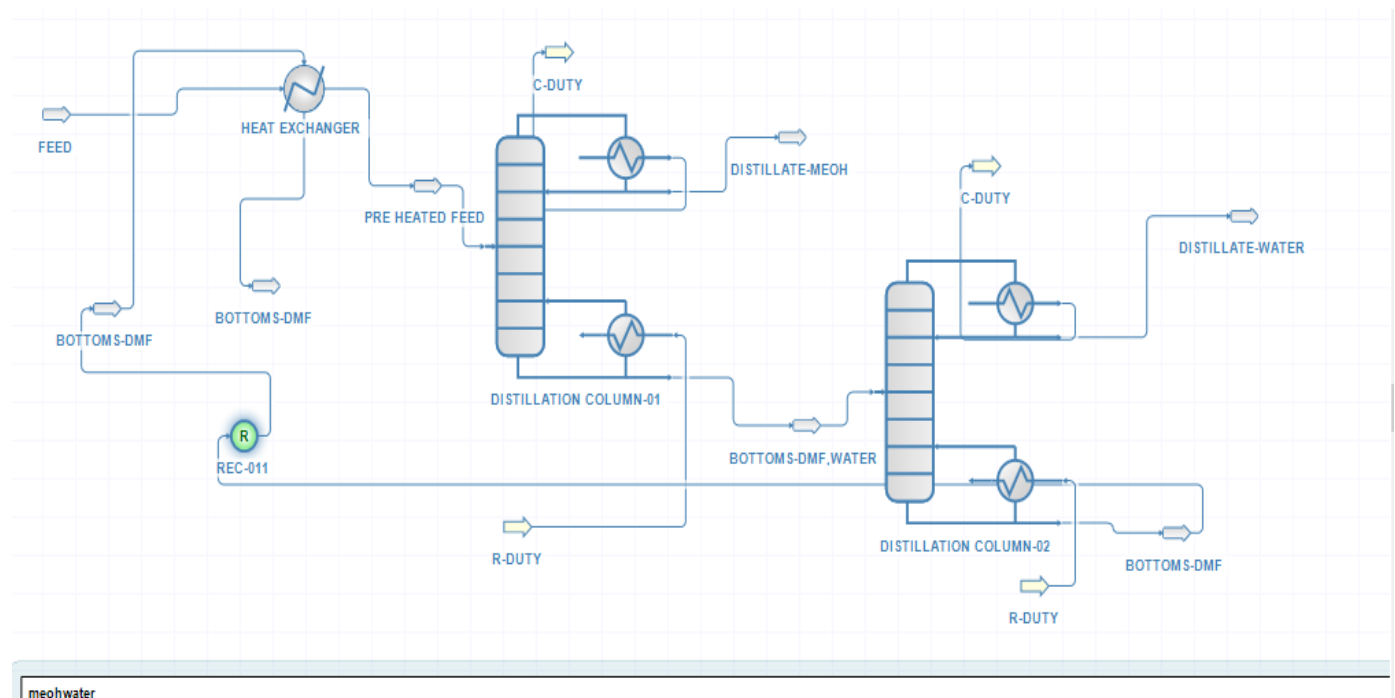
Introduction:

This flow sheet is drawn based upon my working organization. We have daily separation of 48kl of spent, In which we have 70% of methanol, 20% of water and 10% of DMF. We have to maintain the purity of methanol with not less than 95 percent. In this process I used two distillation columns, one heat exchanger and one recycle stream.

Description of flow sheet:

In this process initially Methanol, water and DMF taken with 0.7, 0.2 and 0.1 mole fractions respectively. The feed was taken as 3600 kg/hr. The initial temperature of feed was 25⁰c and it was pre heated by using the BOTTOMS-DMF. After raising the temperature it was sent to distillation column-01 in which methanol and water, DMF separated. In the distillation column-01 the distillate temperatures not maintain more than 65⁰c because methanol boiling point is 64.6⁰c .Put the temperature indicator at the top of distillation column-01. DMF and water is separated in the distillation column-02. In the distillation column-02 water and DMF are separated. BOTTOMS-DMF is used to pre heat the feed.

Flow sheet:



Separation of methanol, water and DMF

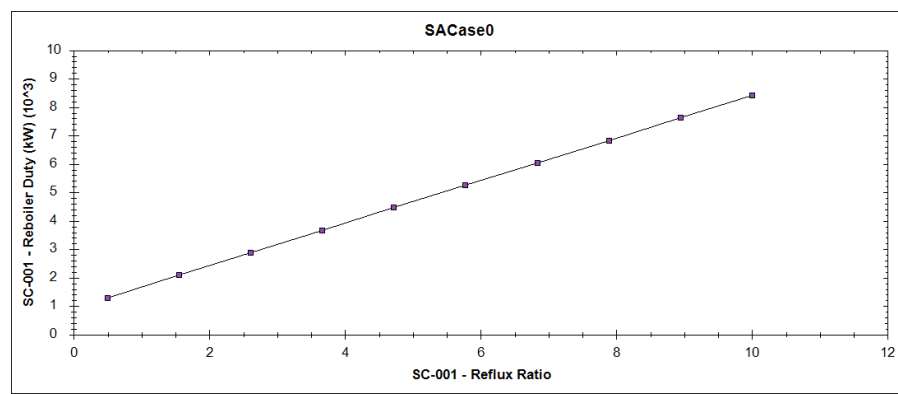
Results:

| meohwater | | | | | | | |
|--------------------------------|-----------------|-------------|------------------|-----------------|--------------------|-------------|------------------------|
| Object | PRE HEATED FEED | FEED | DISTILLATE-WATER | DISTILLATE-MEOH | BOTTOMS-DMF, WATER | BOTTOMS-DMF | |
| Temperature | 42.1946 | 25 | 97.6149 | 64.7514 | 107.861 | 45.5793 | C |
| Pressure | 1.033 | 1.033 | 1.033 | 1.033 | 1.033 | 1.033 | kgf/cm ² |
| Mass Flow | 3600 | 3600 | 399.218 | 2425.22 | 1174.78 | 775.602 | kg/h |
| Molar Flow | 62334.8 | 62334.8 | 12273.5 | 43888.8 | 18446.1 | 6173.79 | m ³ /d @ BR |
| Volumetric Flow | 4.37267 | 4.29185 | 0.421035 | 3.53084 | 1.31618 | 0.833377 | m ³ /h |
| Mixture Density | 823.295 | 838.798 | 948.184 | 686.869 | 892.572 | 930.673 | kg/m ³ |
| Mixture Molar Weight | 33.3418 | 33.3418 | 18.7784 | 31.9018 | 36.7679 | 72.5277 | kg/kmol |
| Mixture Specific Enthalpy | -1147.28 | -1200.38 | -2036.68 | -1055.07 | -987.178 | -607.852 | kJ/kg |
| Mixture Specific Entropy | -3.39643 | -3.78656 | -5.41945 | -3.08791 | -2.36621 | -1.88186 | kJ/[kg.K] |
| Mixture Molar Enthalpy | -38252.2 | -40022.7 | -38245.5 | -33658.7 | -36296.5 | -44086.1 | kJ/kmol |
| Mixture Molar Entropy | -113.243 | -126.251 | -101.769 | -98.5097 | -87.0005 | -136.487 | kJ/[kmol.K] |
| Mass Flow (Mixture) / Water | 389.025 | 389.025 | 373.44 | 13.6953 | 375.33 | 1.9265 | kg/h |
| Mass Flow (Mixture) / Methanol | 2421.76 | 2421.76 | 10.2388 | 2411.53 | 10.2378 | 2.35342E-05 | kg/h |
| Phases | Liquid Only | Liquid Only | Liquid Only | Mixed | Liquid Only | Liquid Only | |
| Energy Flow | -1147.28 | -1200.38 | -225.855 | -710.774 | -322.144 | -130.959 | kW |

Separation of methanol, water and DMF-Results

Analysis:

Reflux vs Re-boiler duty for distillation column-01



x-axis: Reflux ratio

y-axis: Re-boiler duty

Conclusion: Separation of methanol from water and DMF is very important process in so many chemical and Pharmaceutical companies. So this flow sheet give basic idea of separating the solvents for industrial purposes. Reference: Covalent laboratories pvt ltd