



Separation of close boiling mixtures 1-butanol and 2-methyl-1-propanol

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Background & Description:

The boiling points of 2-methyl-1-propanol and butanol is 107.3 and 117.3 °C respectively. It is difficult to obtain them separately from their mixture because the boiling points of *n*-butanol and iso-butanol are very close Therefore to separate out conventional distillation process is used. Butanol has numerous applications as an automotive **fuel** and in the chemical industry. 2-methyl-1-propanol is used in lubricants and greases, coating products, adhesives and sealants, washing & cleaning products, finger paints, polishes and waxes, anti-freeze products, inks and toners, cosmetics and personal care products and perfumes and fragrances.

For the Conventional Distillation process, the feed stream flows at 5000 kg/h, composed of 55 wt% *n*-butanol and 45 wt% iso-butanol, at 130 kPa and 120 °C. The specifications for the purity of *n*-butanol and iso-butanol products are all set at 99.1 wt%. The top stage/condenser pressure is 100 kPa with the stage pressure drop of 0.75 kPa.

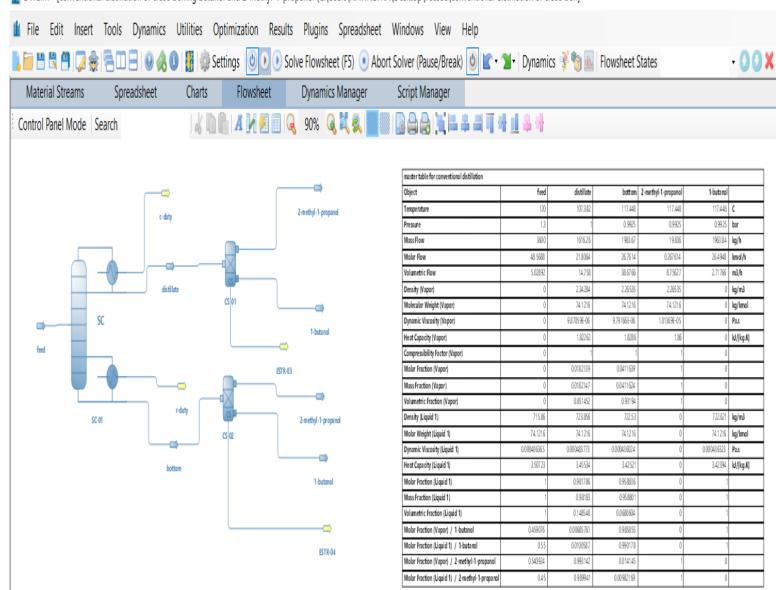
The simulation results of optimal feed stage is 27,total number of stages is 58,Condensor duty is 1683.92 kW and reboiler duty is 1676.47.98.99% of 2-methyl 1-propanol is obtained at the reflux ratio of 5.57687 which increases to about 99.1% as we increase the reflux ratio from 5.57687 to 6. 99% butanol is obtained at the reflux ratio of 5.57687. We try to keep the reflux ratio as minimum as possible as the reboiler duty increases with increase in reflux ratio. This is the main part of the distillation column that consumes energy.





Flowsheet:

👔 DWSIM - [conventional distillation of close boiling butanol and 2-methyl-1-propanol (C\Users\NAVINETRA\Desktop\Fossee\conventional distillation of close boil]







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Results:

Results		
Property	Value	Units
Minimum Reflux Ratio	4.93875	
Minimum Number of Stages	25.1971	
Actual Number of Stages	57.2277	
Optimal Feed Stage	27.3645	
Stripping Liquid	170.181	kmol/h
Rectify Liquid	121.612	kmol/h
Stripping Vapor	143.419	kmol/h
Rectify Vapor	143.418	kmol/h
Condenser Duty	1683.92	kW
Reboiler Duty	1676.47	kW

Simulation Report DWSIM 6.4

Details

Object:

Type:

distillate

Material Stream

Title: MySimulation_15

Comments:

Temperature	117.448	С
Pressure	0.9925	bar
Mass Flow	1983.67	kg/h
Molar Flow	26.7614	kmol/h
Volumetric Flow	38.6766	m3/h
Mixture Molar Fraction		
1-butanol	0.990036	
2-methyl-1-propanol	0.01	
Density (Mixture)	51.2887	kg/m3
Molecular Weight (Mixture)	74.1243	kg/kmol
Specific Enthalpy (Mixture)	-404.605	kJ/kg
Specific Entropy (Mixture)	-0.974313	kJ/[kg.K]
Molar Enthalpy (Mixture)	-29991	kJ/kmol
Molar Entropy (Mixture)	-72.2203	kJ/[kmol.k]
Thermal Conductivity (Mixture)	0.135081	W/[m.K]
Molar Fraction (Vapor)		
1-butanol	0.985855	
2-methyl-1-propanol	0.014145	
Molar Fraction (Overall Liquid)		
1-butanol	0.990178	
2-methyl-1-propanol	0.00982169	
Molar Fraction (Liquid 1)		
1-butanol	0.990178	
2-methyl-1-propanol	0.00982169	
Molar Fraction (Liquid 2)		
1-butanol	0	
2-methyl-1-propanol	0	
Molar Fraction (Aqueous)		
1-butanol	0	
2-methyl-1-propanol	0	
Molar Fraction (Solid)		
1-butanol	0	
2-methyl-1-propanol	0	

Value Property