



Separation Of Acetone-Water With 3-Methylhexane As The Solvent.

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Background and Description:

Water has a high latent heat (heat of vaporization) compared to many other components. For the separation of a water-acetone mixture (50 wt-% each), it may be more energy efficient to use extraction instead of direct distillation.

In this case we use a 3-methyalhexane as a solvent for separation of water and acetone mixture, and recover at the end of operation for multi time use.

Process:

Here the feed containing Mixture of Acetone-water (50-50%) which is passed through the inlet stream (S-01) at 30 °C and 1 atm (101.325 kpa) pressure. For the easy separation 3-methyalhexane(S-02)is used as a solvent at 40 °C and 1 atm pressure.

Stream S-01 & S-02 transfer into the Extractor. Here water is separate through stream S-04 and 3-methyalhexane and acetone mixture separate through stream S-05.

Then Stream S-05 is transfer into the distillation column for further separation. here Acetone separate from the top of the column through stream S-06 and 3-methyalhexane separate from the bottom of the column through stream S-07.

Acetone Mole fraction from top of distillation column :- 1 in (S-06)

:- 0.13 in (S-07)

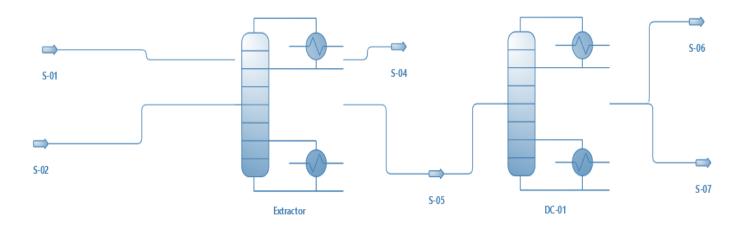
3-methyalhexane mole fraction from Bottom of distillation column: - 0.86in(s-07)

:- 1.64 x 10⁻⁹ in (S-06)





Flow sheet:



Result table:

| Master Property Table | | | | | |
|---|------------|-------------|------------|----------|-----------|
| Object | S-07 | S-06 | S-05 | S-04 | |
| Temperature | 83.9148 | 56.1396 | 30 | 30 | С |
| Pressure | 101.325 | 101.325 | 101.325 | 101.325 | kPa |
| Mass Flow | 163.673 | 100.978 | 264.651 | 35.3495 | kg/h |
| Molar Flow | 988.513 | 988.513 | 1977.03 | 1115.62 | m3/d @ SC |
| Volumetric Flow | 6.07118 | 1127.43 | 8.64153 | 0.852739 | m3/d |
| Molar Fraction (Mixture) / Acetone | 0.133789 | 1 | 0.566894 | 0 | |
| Molar Fraction (Mixture) / Water | 0.00520043 | 4.2944E-18 | 0.00260022 | 1 | |
| Molar Fraction (Mixture) / 3-methylhexane | 0.861011 | 1.64912E-09 | 0.430505 | 0 | |