Scilab Textbook Companion for Introduction To Fluid Mechanics by R. W. Fox And A. T. McDonald¹

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Book Description

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Scilab numbering policy used in this document and the relation to the above book.

Exa Example (Solved example)

Eqn Equation (Particular equation of the above book)

AP Appendix to Example(Scilab Code that is an Appednix to a particular Example of the above book)

For example, Exa 3.51 means solved example 3.51 of this book. Sec 2.3 means a scilab code whose theory is explained in Section 2.3 of the book.

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Introduction

```
check Appendix AP 79 for dependency: 1_01.sci
```

Scilab code Exa 1.01 Head addition

```
//Heat addition//
filename=pathname+filesep()+'1.01-data.sci'
exec(filename)
//Heat added during the process(in kJ):
Q12=m*cp*(T2-T1)
printf("\n\nRESULTS\n\n")
printf("\n\nHeat added during the process: %f kJ\n\n",Q12/1000)
check Appendix AP 78 for dependency:
1_02.sci
```

Scilab code Exa 1.02 Head addition

```
//speed and actual speed//
pathname=get_absolute_file_path('1.02.sce')
filename=pathname+filesep()+'1.02-data.sci'
exec(filename)
//Speed at which the ball hits the ground(in m/sec):
V=sqrt(m*g/k*(1-%e^(2*k/m*(-y0))))
//Terminal speed(in m/sec):
Vt=sqrt(m*g/k)
//Ratio of actual speed to the terminal speed:
r=V/Vt;
printf("\n\nRESULTS\n\n")
printf("\n\nSpeed at which the ball hits he ground:
%f m/sec\n\n",V)
rintf("\n\nRatio of actual speed to the terminal speed:
```

Fundamental Concepts

```
check Appendix AP 77 for dependency:
```

```
2_02.sci
```

Scilab code Exa 2.02 Viscosity and stress

```
1 // Viscosity and stress//
2 pathname=get_absolute_file_path('2.02.sce')
3 filename=pathname+filesep()+'2.02-data.sci'
4 exec(filename)
5
6 // Viscosity in units of lbf-s/ft^2:
7 u1=u/100/454/32.2*30.5
8 // Kinematic viscosity (in m/sec^2):
9 v=u1/SG/d*(0.305)^2
10 // Shear stress on the upper plate(lbf/ft^2):
11 tu=u1*U/D*1000
12 // Shear stress on the lower plate(in Pa)
13 tl=tu*4.45/0.305^2
14 printf("\n\nRESULTS\n\n")
15 printf("\n\nNiscosity in units of lbf-s/ft^2: %1.8f $lbf-s/ft^2\n\n",u1)
```

- 16 printf(" $\n\n$ Kinematic viscosity: %1.8 f m/sec^2 \n' n", v)
- 17 printf("\n\nShear stres on the upeer plate: %f lbf/ ft^2\n\n",tu)
- 18 printf("\n\nSear stress on the lower plate: %f Pa\n\n",tl)

Fluid Statics

```
check Appendix AP 76 for dependency:
```

```
3_01.sci
```

${\bf Scilab} \ {\bf code} \ {\bf Exa} \ {\bf 3.01} \ {\bf liquid} \ {\bf level}$

```
1 //liquid level//
2 pathname=get_absolute_file_path('3.01.sce')
3 filename=pathname+filesep()+3.01-data.sci
4 exec(filename)
5 //Tube diameter (in mm):
6 D=1:25;
7 D1 = D/1000
8 [m n] = size(D1)
9 for i=1:n
10 //Change in liquid level for water (in mm):
11 dhw(i)=4*STw*cosd(thetaw)/dw/g/D1(i);
12 //Change in liquid level for mercury (in mm):
13 dhm(i)=4*STm*cosd(thetam)/dm/g/D1(i);
14 end;
15
16 // Plotting tube daimeter and water level:
17 plot (D1*1000, dhw, '-o')
```

```
18 // Plotting tube daimeter and mercury level:
19 plot (D1*1000, dhm, '-*')
20 legend(['Water'; 'Mercury']);
21 xtitle ('Liquid level vs Tube diameter', 'Liquid level
      (in mm)', 'Tube diameter (in mm)')
     check Appendix AP 75 for dependency:
     3_03.sci
   Scilab code Exa 3.03 pressure difference
1 //pressure difference//
2 pathname=get_absolute_file_path('3.03.sce')
3 filename=pathname+filesep()+3.03-data.sci
4 exec(filename)
5 // Pressure difference (in lbf/in^2):
6 dp = g*d*(-d1+SGm*d2-SGo*d3+SGm*d4+d5)/12/144
7 printf("\n\nESULTS\n\n")
8 printf("\n\nPressure difference between A and B: %f
      lbf/in^2\n'n, dp)
     check Appendix AP 74 for dependency:
     3_04.sci
   Scilab code Exa 3.04 temperature and pressure
1 //temperature and pressure//
2 pathname=get_absolute_file_path('3.04.sce')
3 filename=pathname+filesep()+'3.04-data.sci'
4 exec(filename)
5 // Assuming temperature varies linearly with altitude
```

```
6 //Temperature gradient(in F/ft):
7 m = (T1-T2)/(z2-z1)
8 //Value of g/(m*R):
9 \text{ v=g/m/R/32.2}
10 // Pressure at Vail Pass (in inches of Hg):
11 p12=p1*((T2+460)/(T1+460))^v
12 // Percentage change in density:
13 pc1=(p12/p1*(T1+460)/(T2+460)-1)*100
14 //Assuming density is constant:
15 // Pressure at Vail Pass (in inches of Hg):
16 p22=p1*(1-(g*(z2-z1)/(R*32.2)/(T1+460)))
17 // Percentage change in density:
18 \text{ pc2=0};
19 //Assuming temperature is constant:
20 //Pressure at Vail Pass(in inches of Hg):
21 p32=p1*%e^{(-g*(z2-z1)/(R*32.2)/(T2+460))}
22 // Percentage change in density:
23 pc3=(p32/p1*(T1+460)/(T1+460)-1)*100
24 //For an adiabatic atmosphere:
p42=p1*((62+460)/(80+460))^(k/(k-1))
26 // Percentage change in density:
27 \text{ pc4} = (p42/p1*(T1+460)/(T2+460)-1)*100
28 printf("\n\nRESULTS\n\n")
29 printf("\n\n1) If temperature varies linearly with
      altitude \n\n")
30 printf("\n\tAtmospheric pressure at Vail Pass: %f
      inches of Hg \setminus n \setminus n",p12)
31 printf("\n\tPercentage change in density wrt
      Denver: \%f percent\n\n",pc1)
32 printf("\n\n2) If density is constant\n\n")
33 printf("\n\n\tAtmospheric pressure at Vail Pass: %f
      inches of Hg \ n \ , p22)
34 printf("\n\tPercentage change in density wrt
      Denver: \%f percent \n\n",pc2)
35 printf("\n\n3) If temperature is constant\n\n")
36 printf("\n\tAtmospheric pressure at Vail Pass: %f
      inches of Hg\n\n",p32)
```

check Appendix AP 73 for dependency:

3_05.sci

Scilab code Exa 3.05 force and pressure

```
1 //force and pressure//
2 pathname=get_absolute_file_path('3.05.sce')
3 filename=pathname+filesep()+3.05-data.sci
4 exec(filename)
5 //Net force on the gate(in kN):
6 Fr=d*g*w*(D*L+L^2/2*sind(theta))
7 // Centre of pressure:
  //Calculation for y coordinate:
      yc=D/sind(theta)+L/2
9
10
      //Area(in m^2):
11
      A = L * w
12
      //Moment of inertia of rectangular gate(in m<sup>4</sup>):
13
      Ixx=w*L^3/12
      //y coordinate(in m):
14
      y = yc + Ixx/A/yc
15
16
  //Calculation for x coordinate:
      Ixy=0
17
18
      xc = w/2
19
      //x coordinate(in m):
      x = xc + Ixy/A/xc
20
21 printf("\n\nESULTS\n\n")
```

```
22 printf("\n \in force on the gate: \%f k\n \in , Fr
      /1000)
23 printf("\n nCoordinate of centre of pressure:(\%0.1f,
     \%0.1 f) \n\n", x, y)
     check Appendix AP 72 for dependency:
     3_06.sci
  Scilab code Exa 3.06 force
1 //force//
2 pathname=get_absolute_file_path('3.06.sce')
3 filename=pathname+filesep()+3.06-data.sci
4 exec(filename)
5 //Force required to keep the door shut(in lbf):
6 function y=f(z), y=b/L*p0*z+d*b/L*(L*z-z^2),
      endfunction
7 Ft=intg(0,L,f)
8 printf("\n\nESULTS\n\n")
9 printf("\n\nForce required to kep the door shut: %.1f
       lbf \n \", Ft)
     check Appendix AP 71 for dependency:
     3_07.sci
  Scilab code Exa 3.07 force at equilibrium
1 //force at equilibrium//
2 pathname=get_absolute_file_path('3.07.sce')
3 filename=pathname+filesep()+3.07-data.sci
4 exec(filename)
5 // Horizontal component of resultant force (in kN):
```

Basic Equations in Integral form for a Control Volume

check Appendix AP 70 for dependency:

```
4_01.sci
```

Scilab code Exa 4.01 Velocity

Scilab code Exa 4.02 Mass flow

4_02.sci

```
1 //Mass flow//
2 pathname=get_absolute_file_path('4.02.sce')
3 filename=pathname+filesep()+^{\prime}4.02-data.sci
4 exec(filename)
5 //If I = integral of(pV.dA):
6 //For system: ICS=Iab+Ibc+Icd+Ida
7 / But ICS=0
9 //For Aab:
10 function p=f(y),p=-d*U*w*y^0,endfunction
11 IAab=intg(0,t,f)
12
13 // For Acd:
14 function q=g(y), q=d*U*w*(2*y/t-(y/t)^2), endfunction
15 IAcd=intg(0,t,g)
16
17 // Mass flow rate across surface bc(in kg/sec):
18 mbc = (-IAab - IAcd)/1000
19 printf("\n\nESULTS\n\n")
20 printf("\n\nMass flow rate across surface bc: %.4f
     kg/sec n ", mbc)
```

check Appendix AP 68 for dependency:

4_03.sci

Scilab code Exa 4.03 density

```
1 // density //
2 pathname=get_absolute_file_path('4.03.sce')
3 filename=pathname+filesep()+^{\prime}4.03-data.sci
4 exec(filename)
5 //Rate of change of air density in tank(in (kg/m<sup>3</sup>)/
     s):
6 r = -d * v * A / V / 10^6
7 printf("\n\nESULTS\n\n")
8 printf("\n\nRate of change of air density in tank: %
     .3 f kg/m^3 n n",r)
9 printf("\n\nThe density decreases as is indicated by
      the negative sign n ")
```

check Appendix AP 67 for dependency:

4_04.sci

Scilab code Exa 4.04 Horizontal force

```
1 // Horizontal force //
2 pathname=get_absolute_file_path('4.04.sce')
3 filename=pathname+filesep()+^{\prime}4.04-data.sci
4 exec(filename)
5 //1) Control Volume selected so that area of left
      surface is equal to the area of the right surface
6 u1=15;
7 //Force of support on control volum(in kN):
8 function y=f(A),y=-u1*d*V,endfunction
9 \text{ Rx1} = intg(0,0.01,f)
10 // Horizontal force on support (in kN):
```

```
11 \quad Kx = -Rx1
12 / 2 Control volumes are selected do that the area
      of the left and right surfaces are equial to the
      area of the plate
13
14 function z=g(A),z=-u1*d*V,endfunction
15 Fsx=intg(0,0.01,g)
16 //Net force on plate:Fx=0=-Bx-pa*Ap+Rx
17 //
                          Rx=pa*Ap+Bx
18 //From the above, it is obtained that:
19 \text{ Rx} 2 = -2.25
20 // Horizontal force on support (in kN):
21 \text{ Kx}2 = -\text{Rx}2
22 printf("\n\nRESULTS\n\n")
23 printf("\nnHorizontal force on support: \%.3 f kN\nn
      ", Kx/1000)
```

check Appendix AP 66 for dependency:

4_05.sci

Scilab code Exa 4.05 Scale

```
1 //Scale//
2 pathname=get_absolute_file_path('4.05.sce')
3 filename=pathname+filesep()+^{\prime}4.05-data.sci
4 exec(filename)
5 //Weight of water in the tank(in lbf):
6 d1 = 62.4;
7 WH20=d1*A*h
8 v = -5;
9 //Total body force in negative y direction(lbf):
10 function y=f(A),y=-v*d2*V1,endfunction
11 F=intg(0,A1,f)
12 //Force of scale on control volume(in kN):
13 Ry = W + WH20 - F
```

```
14 printf("\n\nRESULTS\n\n")
15 printf("\n\nScale Reading: %.3f lbf\n\n",Ry)
     check Appendix AP 65 for dependency:
     4_06.sci
   Scilab code Exa 4.06 force exerted per unt
1 //force exerted per unt//
2 pathname=get_absolute_file_path('4.06.sce')
3 filename=pathname+filesep()+^{\prime}4.06-data.sci
4 exec(filename)
5 //X-component of reaction force per unit width of
      the gate (in N/m):
6 Rxw = (d*(V2^2*D2-V1^2*D1))-(d*g/2*(D1^2-D2^2))
7 // Horizontal force exerted per unt width on the gate
      (in N/m):
8 \text{ Kxw} = -\text{Rxw}
9 printf("\n\nESULTS\n\n")
10 printf("\n\nHorizontal force exerted per unt width
      on the gate: \%.3 \text{ f kN/m/n'}, \text{Kxw/1000})
     check Appendix AP 64 for dependency:
     4_07.sci
   Scilab code Exa 4.07 Force to hold
1 //Force to hold//
2 pathname=get_absolute_file_path('4.07.sce')
3 filename=pathname+filesep()+^{\prime}4.07-data.sci
4 exec(filename)
5 // Velocity at section 1(in m/sec):
```

```
6 V1 = V2 * A2 / A1
7 //Gauge pressure(in kPa):
8 p1g=p1-patm
9 u1=V1; u2=-V2;
10 //Reaction force component in the x direction (in N):
11 Rx = -p1g * A1 - u1 * d * V1 * A1
12 //Reaction force component in the y direction (in N):
13 Ry = u2 * d * V2 * A2
14 printf ("\n\nRESULTS\n\n")
15 printf("\n nForce to hold elbow acting to the left:
      \%.3 f kN n n", Rx/1000)
16 printf("\n\nForce to hold elbow acting downwards: %
      .3 f N n n, Ry)
     check Appendix AP 63 for dependency:
      4_08.sci
   Scilab code Exa 4.08 Tension
1 //Tension//
2 filename=pathname+filesep()+^{\prime}4.08-data.sci
3 exec(filename)
4 //Tension required to pull the belt(in lbf):
5 \text{ T=Vbelt*m/32.2}
6 printf("\n\nRESULTS\n\n")
7 printf("\n\nTension required to pull the belt: %.3f
      lbf \n \n",T)
      check Appendix AP 62 for dependency:
      4_09.sci
```

Scilab code Exa 4.09 pressure required

```
1 //pressure required//
2 pathname=get_absolute_file_path(^{\prime}4.09.sce^{\prime})
3 filename=pathname+filesep()+^{\prime}4.09-data.sci
4 exec(filename)
5 //Minimum gauge pressure required (in lbf/in^2):
6 pg=8/%pi^2*d/D1^4*Q^2*((D1/D2)^4-1)*144
7 printf("\n\nESULTS\n\n")
8 printf ("Minimum gauge pressure required: %.3 f lbf/in
      ^2",pg)
     check Appendix AP 61 for dependency:
     4_10.sci
   Scilab code Exa 4.10 Net force
1 //Net force//
2 pathname=get_absolute_file_path('4.10.sce')
3 filename=pathname+filesep()+^{\prime}4.10-data.sci
4 exec(filename)
5 u1=V-U
6 u2=(V-U)*cosd(theta)
7 v2=(V-U)*sind(theta)
8 V1 = V - U
9 V2 = V1
10 //X component of moment equation (in N):
11 function y=f(A),y=u1*-(d*V1),endfunction
12 function z=g(A),z=u2*d*V2,endfunction
13 Rx=intg(0,A,f)+intg(0,A,g)
14
15 //Y component of moment equation (in N):
16 function a=h(A),a=v2*d*V1,endfunction
17 Ry=intg(0,A,h) //This is after neglecting weight of
      vane and the water.
18 printf ("\n\nRESULTS\n\n")
19 printf("\n nNet force on the vane: %.3 f i+%.2 f j kN\n
```

 $n \ n$ ", Rx/1000, Ry/1000)

```
check Appendix AP 60 for dependency:
```

```
4_11.sci
```

Scilab code Exa 4.11 PLOTTING

```
1 //PLOTTING//
2 pathname=get_absolute_file_path('4.11.sce')
3 filename=pathname+filesep()+^{\prime}4.11-data.sci
4 exec(filename)
5 //Evaluating the value of Vb:
6 Vb=V*(1-cosd(theta))*d*A/M
7 // Value of U/V for various values of t
8 t=0:20;
9 [m n] = size(t)
10 for i=1:n
     U_V(i) = Vb*t(i)/(1+Vb*t(i));
11
12 end
13
14 // Plotting U/V vs t:
15 plot(t,U_V)
16 xtitle('U/V vs t', 't (in sec)', 'U/V')
```

check Appendix AP 59 for dependency:

```
4_12.sci
```

Scilab code Exa 4.12 Velocity of rocket

```
//Velocity of rocket//
pathname=get_absolute_file_path('4.12.sce')
filename=pathname+filesep()+'4.12-data.sci'
exec(filename)
```

```
5 // Acceleration of rocket at t=0(in m/sec^2):
6 \text{ Ve*me/MO-g}
7 // Velocity of rocket at t=10 (in m/sec):
8 function y=f(t),y=Ve*me/(MO-me*t)-g,endfunction
9 Vcv=intg(0,t,f)
10 printf ("\n\nESULTS\n\n")
11 printf("\n\nVelocity of rocket at t=10: %.1 f m/sec\n
      \n", \ncv)
     check Appendix AP 58 for dependency:
     4_14.sci
   Scilab code Exa 4.14 Relative speed and friction
1 //Relative speed and friction//
2 pathname=get_absolute_file_path('4.14.sce')
3 filename=pathname+filesep()+'4.14-data.sci'
4 exec(filename)
5 //Area of jet(in mm^2):
6 Ajet=\%pi/4*D^2
7 // Jet speed relative to the nozzle (in m/sec):
8 Vrel=Q/2/Ajet*10^6/60/1000
9 //Value of w*R in m/sec:
10 \text{ wR} = \text{w*R*2*\%pi/60/1000}
11 // Friction torque at pivot (in N-m):
12 Tf = R*(Vrel*cosd(alpha) - wR)*d*Q/1000/60/1000
13 printf("\n\nESULTS\n\n")
14 printf("\n nJet speed relative to each nozzle: \%.2 f
     m/\sec nn", Vrel)
15 printf("\n nFriction torque at pivot: \%.5 f N-m\n",
```

check Appendix AP 57 for dependency:

4_16.sci

Tf)

Scilab code Exa 4.16 Rate of heat

Scilab code Exa 4.17 Mass flow rate

```
//Mass flow rate//
pathname=get_absolute_file_path('4.17.sce')
filename=pathname+filesep()+'4.17-data.sci'

exec(filename)
//Density of tank(in kg/m^3):
d=(p1+patm)/R/T
//Mass flow rate of air into the tank(in kg/sec):
m=d*V*cv*r/R/T*1000
printf("\n\nRESULTS\n\n")
printf("\n\nMass flow rate of air into the tank: %.3
f g/sec\n\n",m)
```

Introducton to Differential Analysis of Fluid Motion

```
check Appendix AP 55 for dependency: 5_02.sci
```

Scilab code Exa 5.02 Rate of change

5_07.sci

Scilab code Exa 5.07 angular and rotation

```
1 //angular and rotation//
2 pathname=get_absolute_file_path('5.07.sce')
3 filename=pathname+filesep()+^{\prime}5.07-data.sci
4 exec(filename)
5 //At point b, u=3 mm/sec
6 u=3;
7 // Displacemet of b(in mm):
8 \text{ xb=u*t}
9 //Rate of angular deformation (in s^-1):
10 \, \text{def} = \text{U/h}
11 //Rate of rotation (in s^-1):
12 \text{ rot} = -0.5*U/h
13 printf("\n\nRSULTS\n\n")
14 printf("\nnRate of angular deformation: %.1 f /sec\n
      \n", def)
15 printf("\nnRate of rotation: %.1f /sec\n",rot)
      check Appendix AP 53 for dependency:
      5_08.sci
```

Scilab code Exa 5.08 Rates and area

```
//Rates and area//
pathname=get_absolute_file_path('5.08.sce')
filename=pathname+filesep()+'5.08-data.sci'
exec(filename)
//Value of T:
T=log(3/2)/A
x0=1:2;
y0=1:2;
for i=1:2
//For X coordinate:
```

```
12
     X(i)(j)=x0(i)*%e^{(A*T)}
     //For Y coordinate:
13
     Y(i)(j) = y0(j) * %e^{(-A*T)}
14
15
     end
16 \text{ end}
17 plot(X,Y)
18 //Rates of linear deformation in X direction:
19 Ax = 0.3;
20 //Rate of linear deformation in the y direction:
21 Ay = -0.3;
22 //Rate of volume dilation (s^-1):
23 v=A-A
24 // Area of abcd:
25 \quad A1 = 1;
26 // Area of a'b'c'd':
27 \quad A2 = (3-3/2) * (4/3-2/3)
28 printf ("\n\nRESULTS\n\n")
29 printf("\n nRates of linear deformation in X and Y
       direction: \%.1 f / s, \%.1 f / s \setminus n \setminus n, Ax, Ay)
30 printf("\nnRate of volume dilation: %.0 f /sec\n",
      v)
31 printf("\n nArea of abcd and a,b,c,d:%.1f m<sup>2</sup>, %.1f
      m^n n^n, A1, A2)
      check Appendix AP 52 for dependency:
      5_09.sci
```

Scilab code Exa 5.09 Volume flow rate

```
1 //Volume flow rate//
2 pathname=get_absolute_file_path('5.09.sce')
3 filename=pathname+filesep()+'5.09-data.sci'
4 exec(filename)
5 //Volume flow rate(in m^3/sec):
6 Q=d*g*sind(theta)*b*(h/1000)^3*1000/u/3
```

```
7 printf("RESULTS")
8 printf("\n\nVolume flow rate: \%.4 \, f \, m^3/\sec n^n,Q)
```

Incompressible Inviscid Flow

```
check Appendix AP 51 for dependency:
```

```
6_01.sci
```

Scilab code Exa 6.01 Volume flow rate

```
//Volume flow rate//
pathname=get_absolute_file_path('06.01.sce')
filename=pathname+filesep()+'06.01-data.sci'
exec(filename)
//Velocity of flow(in m/sec):
V=sqrt(dw/log((r+w)/r)*g/da*p/1000)
//Volume flow rate(in m^3/sec):
Q=V*(d*w)
printf("\n\nRESULTS\n\n")
printf("\n\nVolume flow rate: %.3f m^3/sec\n\n",Q)
```

check Appendix AP 50 for dependency:

6_02.sci

Scilab code Exa 6.02 Velocity of flow

```
1 // Velocity of flow //
2 pathname=get_absolute_file_path('06.02.sce')
3 filename=pathname+filesep()+^{\prime}06.02-data.sci
4 exec(filename)
5 // Velocity of flow(in m/sec):
6 V = sqrt(2*dw*g*p/1000*SG/da)
7 printf("\n\nESULTS\n\n")
8 printf("\n \ n \ velocity of flow: \%.3 f m/sec \n', V)
     check Appendix AP 49 for dependency:
     6_03.sci
  Scilab code Exa 6.03 prssure required
1 //prssure required//
2 filename=pathname+filesep()+^{\prime}06.03-data.sci
3 exec(filename)
4 // Velocity of flwat the inlet (in m/sec):
5 V1=Ae/Ai*V2
6 //Gauge pressure required at the inlet(in kPa):
7 p=0.5*da*(V2^2-V1^2)
```

9 printf("\n\nGauge prssure required at the inlet: %.3

check Appendix AP 48 for dependency:

8 printf(" $\n\n$ ESULTS $\n\n$ ")

f $kPa \n\n$ ",p/1000)

6_04.sci

Scilab code Exa 6.04 Speed and pressure

```
1 //Speed and pressure//
2 pathname=get_absolute_file_path('06.04.sce')
3 filename=pathname+filesep()+^{\prime}06.04-data.sci
4 exec(filename)
5 //Speed of water at exit(in m/sec):
6 V2=sqrt(2*g*z)
7 // Pressure at point A in the flow (kPa):
8 pA=p1+d*g*(0-1)-0.5*d*V2^2
9 printf("\n\nESULTS\n\n")
10 printf("\n nSpeed of water at exit: %.3 f m/sec\n",
      V2)
11 printf("\n\nPressure at point A in the flow: %3f kPa
      \n\n", pA/1000)
     check Appendix AP 47 for dependency:
     6_05.sci
   Scilab code Exa 6.05 flow
1 //flow//
2 pathname=get_absolute_file_path('06.05.sce')
3 filename=pathname+filesep()+^{\prime}06.05-data.sci
4 exec(filename)
5 // Velocity of flow at the exit(in ft/sec):
6 V2 = sqrt(2*g*(Du-Dd/12))
7 //Volume flow rate/width(ft^2/sec):
8 \ Q = V2 * Dd / 12
9 printf("\n\nESULTS\n\n")
10 printf("\n velocity of flow at the exit: %.3 f ft/
      \sec \langle n \rangle n", V2)
11 printf("\n\nVolume flow rate/width: %.3 f ft^2/sec\n\
      n",Q)
```

check Appendix AP 46 for dependency:

6_06.sci

Scilab code Exa 6.06 pressure

```
1 //pressure//
2 pathname=get_absolute_file_path('06.06.sce')
3 filename=pathname+filesep()+^{\prime}06.06-data.sci
4 exec(filename)
5 // Pressure of air at 1000 \text{ m(in N/m}^2):
6 p=P1*pa
7 // Density of air at 1000m(in kg/m^3):
8 d=D1*da
9 //Stagnation pressure at A(in kPa):
10 p0A=p+0.5*d*(V*1000/3600)^2
11 //Static pressure at B(in kPa):
12 pB=p+d/2*((V*1000/3600)^2-Vb^2)
13 printf("\n\nRESULTS\n\n")
14 printf("\n nStagnation pressure at A: \%.3 f kPa\n",
      p0A/1000)
15 printf("\nnStatic pressure at B: %.3f kPa\nn",pB
      /1000)
     check Appendix AP 45 for dependency:
     6_08.sci
```

Scilab code Exa 6.08 temperature

```
//temperature//
pathname=get_absolute_file_path('06.08.sce')
filename=pathname+filesep()+'06.08-data.sci'
exec(filename)
//Velocity of flow at exit(in ft/sec):
V4=sqrt(2*g*(z3-0))
```

```
7 //Mass flow rate of water (in slug/sec):
8 m = d * V4 * A4 / 144
9 // Rise in temperature between points 1 and 2(in R):
10 T=Q*3413/3600/m/32.2
11 printf ("\n\nRESULTS\n\n")
12 printf("\n\nRise in temperature between points 1 and
       2: \%.3 f R n n, T)
     check Appendix AP 44 for dependency:
     6_09.sci
   Scilab code Exa 6.09 Streamline flow
1 //Streamline flow//
2 pathname=get_absolute_file_path('06.09.sce')
3 filename=pathname+filesep()+^{\prime}06.09-data.sci
4 exec(filename)
5 t=0:5
6 // Value of sqrt(2gh):
7 x = sqrt(2*g*h)
8 //Value of 1/2L*sqrt(2gh):
9 y = 1/2/L * x
10 [m n] = size(t)
11 i=1:n;
```

15 xtitle('Streamline flow from 1 to 2', 'Time(in s)', '

12 // Velocity (in m/sec):

V2(in m/sec)')

13 V2=x*tanh(y*t(i))

14 plot(t, V2);

Chapter 7

Dimensional Analysis and Simlitude

```
check Appendix AP 43 for dependency:
```

7_04.sci

Scilab code Exa 7.04 speed and force

```
//speed and force//
pathname=get_absolute_file_path('7.04.sce')
filename=pathname+filesep()+'7.04-data.sci'
exec(filename)
//Velocity of prototype in ft/sec
Vp1=Vp*6080/3600
//Reynolds number of prototype:
Rep=Vp1*Dp/vp
//Rep=Rem
//Therefore:
Rem=Rep;
//Velocity of air for wind tunnel(in ft/sec):
Wm=Rem*vm/(Dm/12)
//Drag force on prototype(in lbf):
Fp=Fm*(dp/dm)*(Vp1/Vm)^2*(Dp/(Dm/12))^2
```

```
16 printf("\n\nRESULTS\n\n")
17 printf("\n\nTest speed in air: \%.3 \, f \, ft/sec \cdot n \cdot n", Vm)
18 printf("\n\nDrag force on prototype: \%.3 \, f \, lbf \cdot n \cdot n",
Fp)
```

check Appendix AP 42 for dependency:

7_05.sci

Scilab code Exa 7.05 speed force and power

```
1 //speed force and power//
2 pathname=get_absolute_file_path('7.05.sce')
3 filename=pathname+filesep()+^{\prime}7.05-data.sci
4 exec(filename)
5 //Width of the model(in m):
6 \text{ wm} = S*wp*0.3048
7 //Area of model (in m<sup>2</sup>):
8 Am = S^2 * Ap * 0.305^2
9 [m n] = size(V)
10 i = 1:n
11 //Aerodynamic drag coefficient():
12 Cd=2.*Fd(i)/d./(V(i))^2/0.0305
13 //Reynolds number:
14 Re=V(i)*wm/v
15 plot (Re, Cd);
16 \quad a = gca()
17 a.data_bounds = [100000, 0.4; 500000, 0.6]
18 xtitle ('Aerodynamic drag coefficient vs drag force',
      'Reynolds number', 'Model Drag Coeff.')
19 //It is seen that drag coefficient becomes constant
      at CD=0.46 above Re=4*10^5 at which speed of air
      is 40 \text{m/s}
20 \text{ CDc} = 0.46;
21 \text{ Va} = 40;
22 //Drag force (in N):
```

```
23 FDp=CDc/2*d*(Vp*5/18)^2*Ap*0.305^2
24 //Power required to pull prototype at 100 kmph(in W)
25 Pp=FDp*Vp*5/18
26 printf("\n\nRESULTS\n\n")
27 printf("\n\nSpeed above which Cd is constant: %.3 f m / sec\n\n", Va)
28 printf("\n\nDrag Force: %.3 f kN\n\n", FDp/1000)
29 printf("\n\nPower required to pull prototype at 100 kmph: %.3 f kW\n\n", Pp/1000)
```

check Appendix AP 41 for dependency:

7_06.sci

Scilab code Exa 7.06 power and speed

```
1 //power and speed//
2 pathname=get_absolute_file_path('7.06.sce')
3 filename=pathname+filesep()+^{\prime}7.06-data.sci
4 exec(filename)
5 //The same pump is used for both the conditions.
      Hence:
6 D2=D1:
7 //The same water is used for both the conditions.
      Hence:
8 d2=d1;
9 //Flow rate at condition 2(in gpm):
10 Q2=Q1*N2/N1*(D2/D1)^3
11 //Head at condition 1(in ft):
12 H1 = (N1 * sqrt(Q1) / Nscu1)^(4/3)
13 //Head at condition 1(in ft):
14 \text{ H2=H1*(N2/N1)^2*(D2/D1)^2}
15 //Pump output power at condition 1(in hp):
16 \text{ P1}=d1*g*Q1*H1/7.48/60/550
17 //Pump output power at condition 2(in hp):
18 P2=P1*(d2/d1)*(N2/N1)^3*(D2/D1)^5
```

Chapter 8

Internal Incompressible Viscous Flow

```
check Appendix AP 40 for dependency:
```

```
8_01.sci
```

Scilab code Exa 8.01 Leakage flow rate

```
//Leakage flow rate//
pathname=get_absolute_file_path('8.01.sce')
filename=pathname+filesep()+'8.01-data.sci'

exec(filename)
//Leakage flow rate (in mm^3/sec):
Q=%pi/12*D*a^3*(p1-p2)*10^3/u/L
//Velocity of flow(in m/sec):
V=Q/%pi/D/a/1000
//Specific gravity of SAE 10W oil:
SG=0.92;
//Reynolds Number:
Re=SG*dw*V*a/u/1000
//As Re<1400, flow is laminar.
printf("\n\nRESULTS\n\n")
printf("\n\nLeakage flow rate: %.3 f mm^3/sec\n\n",Q)</pre>
```

```
check Appendix AP 39 for dependency:
     8_02.sci
   Scilab code Exa 8.02 Torque and power
1 //Torque and power//
2 pathname=get_absolute_file_path('8.02.sce')
3 filename=pathname+filesep()+^{\prime}8.02-data.sci
4 exec(filename)
5 // Shear stres (in lbf/ft^2):
6 Tyx=u*N*2*\%pi/60*D/2/(a/2)
7 //Torqe(in inches-lbf):
8 T = \%pi/2 * Tyx * D^2 * L/144
9 //Power dissipated in the bearing (in hp):
10 P=T*N/60*2*\%pi/12/550
11 //Reynolds number:
12 Re=SG*p*N*2*%pi/60*1.5*a/2/u/144
13 printf ("\n\nRESULTS\n\n")
14 printf("\nnTorque: %.3f inches-lbf\n",T)
15 printf("\n\nPower dissipated in the bearing: %.3f hp
      \n\n",P)
     check Appendix AP 38 for dependency:
     8_04.sci
   Scilab code Exa 8.04 Viscosity of fluid
1 // Viscosity of fluid //
2 pathname=get_absolute_file_path('8.04.sce')
```

3 filename=pathname+filesep()+ $^{\prime}8.04-data.sci$

4 exec(filename)

```
5 // Viscosity of the liquid (in N-s/m^2):
6 u = \pi / 128 * p * 1000 * D^4 / Q/L / 1000
7 // Velocity (in m/sec)
8 V=Q/(\%pi/4*D^2)/1000
9 //Reynolds number:
10 Re=d*V*D/u/1000
11 printf("\n\nRESULTS\n\n")
12 printf("\n \in V is cosity of fluid %.3 f N-s/m^2 \in n \in M", u)
     check Appendix AP 37 for dependency:
     8_05.sci
   Scilab code Exa 8.05 required
1 //required//
2 pathname=get_absolute_file_path('8.05.sce')
3 filename=pathname+filesep()+^{\prime}8.05-data.sci
4 exec(filename)
5 // Reservoir depth required to maintain flow (in m):
6 D1=8*Q^2/(\%pi)^2/D^4/g*(f*L/D+K+1)
7 //Reynolds number:
8 Re=4*d*Q/((\%pi)*u*D)
9 printf("\n\nESULTS\n\n")
10 printf("\n\nReservoir depth required to maintain
      flow: \%.3 f m n n", D1)
     check Appendix AP 36 for dependency:
```

Scilab code Exa 8.06 Maximum and power

8_06.sci

```
1 //Maximum and power//
2 pathname=get_absolute_file_path('8.06.sce')
3 filename=pathname+filesep()+^{\prime}8.06-data.sci
4 exec(filename)
5 // Velocity of flow (in ft/sec):
6 V=Q/24/3600/(\%pi/4*(D/12)^2)*42/7.48
7 //Maximum spacing (in ft):
8 L=2/f*D/12*(p2-p1)/(SG*d)/V^2*144
9 //Power needed at each pump(in hp):
10 Win=1/Effp*V*%pi/4*(D/12)^2*(p2-p1)/550*144
11 printf("\n\nESULTS\n\n")
12 printf("\n)nMaximum spacing: %.3 f feet\n,",L)
13 printf("\nnPower needed at each pump: %.3 f hp\nn",
     Win)
     check Appendix AP 35 for dependency:
     8_07.sci
  Scilab code Exa 8.07 Volume low
1 //Volume low//
2 pathname=get_absolute_file_path('8.07.sce')
3 filename=pathname+filesep()+^{\prime}8.07-data.sci
4 exec(filename)
5 // Velocity (in ft/sec):
6 V2=sqrt(2*g*1/(f*((L+1)/D*12+8)+1))
7 //Volume flow rate(in gpm):
8 Q=V2*\%pi*(D/12)^2/4*7.48*60
9 printf("\n\nESULTS\n\n")
10 printf("\n\nVolume low rate: \%.3 f\n\n",Q)
     check Appendix AP 34 for dependency:
```

8_08.sci

Scilab code Exa 8.08 Minimum diameter

```
1 //Minimum diameter//
2 pathname=get_absolute_file_path('8.08.sce')
3 filename=pathname+filesep()+^{\prime}8.08-data.sci
4 exec(filename)
5 // Value of dPmax(in psi):
6 \text{ dPmax}=p1-p2
7 //Q in cubic feet/sec:
8 \quad Q1 = 1500/60/7.48;
9 //Initially assume diameter to be 4inches:
10 D=4;
11 //Reynolds number:
12 Re=4*Q1/\%pi/v/D*12
13 //For this value,
14 f=0.012;
    dP=8*f*L*p*Q1^2/(%pi)^2/D^5*1728;
15
16 while (dP>dPmax)
      dP=8*f*L*p*Q1^2/(\%pi)^2/D^5*1728;
17
      if (dP < dPmax)</pre>
18
19
      break
20
      else
21
      D=D+1;
22
    end
23 end
24 printf("\n\nRESULTS\n\n")
25 printf ("Minimum diameter that can be used: %.1 f
      inches \n\n",D)
     check Appendix AP 33 for dependency:
      8_09.sci
```

Scilab code Exa 8.09 Loss Coefficient

```
1 //Loss Coefficient//
```

```
2 pathname=get_absolute_file_path('8.09.sce')
3 filename=pathname+filesep()+^{\prime}8.09-data.sci
4 exec(filename)
5 //Average velocity (in ft/s):
6 V2=4/\%pi*Q/D^2*144
7 //Reynolds number:
8 \text{ Re} = V2 * D/v/12
9 //For this value,
10 f = 0.013;
11 //Power law exponent:
12 n = -1.7 + 1.8 * log10 (Re)
13 //Value of V/U:
14 v_u=2*n^2/(n+1)/(2*n+1)
15 // Value of alpha:
16 alpha=(1/v_u)^3*2*n^2/(3+n)/(3+2*n)
17 //Loss Coefficient for a square edged entrance:
18 K=2*g*h/V2^2-f*L/D*12-alpha;
19 printf("\n\nESULTS\n\n")
20 printf("\n\nLoss Coefficient for a square edged
      entrance: \%.3 f \setminus n \setminus n", K)
      check Appendix AP 32 for dependency:
```

8_10.sci

Scilab code Exa 8.10 Volume and increase

```
1 //Volume and increase//
2 pathname=get_absolute_file_path('8.10.sce')
3 filename=pathname+filesep()+^{\prime}8.10-data.sci
4 exec(filename)
5 // Velocity V1(in m/s):
6 V1 = sqrt(2*g*z0/1.04)
7 //Volume flow rate(in m<sup>3</sup>/sec):
8 \ Q=V1*\%pi*D^2/4
9 Kdiff=1-1/A_R^2-Cp
```

```
//For 2nd case:
//Velocity(in m/s):
V1=sqrt(2*g*z0/0.59)
//Volume flow rate(in m^3/s):
Qd=V1*%pi*D^2/4
//Increase in discharge after addition of diffuser is:
dQ=(Qd-Q)/Q*100
printf("\n\nRESULTS\n\n")
printf("\n\nVolume flow rate in case1: %.3 f m^3/sec\n\n",Q)
printf("\n\nVolume flow rate in case 2: %.3 f m^3/sec\n\n",Qd)
printf("\n\nIncrease in discharge after addition of diffuser is: %.3 f percent\n\n",dQ)
```

check Appendix AP 31 for dependency:

8_11.sci

Scilab code Exa 8.11 Diameter and head

```
//Diameter and head//
pathname=get_absolute_file_path('8.11.sce')
filename=pathname+filesep()+'8.11-data.sci'
exec(filename)

//Value of K*B^2:
K_B=Q/(%pi/4*D^2)*sqrt(0.5*d1/g/d2/h)
//Reynods number:
ReD1=4/%pi*Q/D/v
//By trial and error method, the value of beta is fixed at:
betta=0.66;
//K is then:
K=K_B/betta^2
```

```
14  //Diameter of orifice plate(in m):
15  Dt=betta*D
16  //Value of p3-p2(in N/m^2):
17  P1=d1*Q^2/(%pi/4*D^2)^2*(1/0.65/betta^2-1)
18  //Value of p1-p2(in N/m^2):
19  P2=d2*g*h
20  //Head loss between sections 1 and 3(in N-m/kg):
21  hLT=(P2-P1)/d1
22  //Expressing the permanent pressure as a fractio of the meter differential:
23  C=(P2-P1)/P2
24  printf("\n\n\nRESULTS\n\n")
25  printf("\n\nDiameter of the orifice: %.3f m\n\n",Dt)
26  printf("\n\nHead loss between secions 1 and 3: %.3f N-m/kg\n\n",hLT)
```

Chapter 9

External Incompressible Viscous Flow

```
check Appendix AP 30 for dependency:
   9_01.sci
```

Scilab code Exa 9.01 static pressure

```
1 //static pressure//
2 pathname=get_absolute_file_path('9.01.sce')
3 filename=pathname+filesep()+^{\prime}9.01-data.sci
4 exec(filename)
5 //Change in static pressure between sections 1 and
     2:
6 C=(((L-2*d1)/(L-2*d2))^4-1)*100;
7 printf("\n\nESULTS\n\n")
8 printf("\n\nChange in static pressure between the
     sections 1 and 2: \%.3f percent \n\n",C)
    check Appendix AP 29 for dependency:
```

9_04.sci

Scilab code Exa 9.04 Displacement thickness and stress

```
1 //Displacement thickness and stress//
2 pathname=get_absolute_file_path('9.04.sce')
3 filename=pathname+filesep()+'9.04-data.sci'
4 exec(filename)
5 //Reynolds number:
6 \text{ ReL=U*L/v}
7 //FOR TURBULENT FLOW
8 // Disturbance thickness (in m):
9 dL1=0.382/ReL^0.2*L
10 // Displacement thickness (in m):
11 function y=f(n), y=dL1*(1-n^(1/7))
12 endfunction
13 dl1=intg(0,1,f)
14 //Skin friction coefficient:
15 Cf1=0.0594/ReL^0.2
16 //Wall shear stress(in N/m<sup>2</sup>):
17 \text{ tw1} = \text{Cf1} * 0.5 * d * U^2
18 // For LAMINAR FLOW:
19 // Disturbance thickness (in m)
20 \text{ dL}2=5/\text{sqrt}(\text{ReL})*L
21 // Displacement thickness (in m):
22 d12 = 0.344 * dL2
23 //Skin friction coefficient:
24 Cf2=0.664/sqrt(ReL)
25 //Wall shear stress(in N/m<sup>2</sup>):
26 \text{ tw2} = \text{Cf2} * 0.5 * d * U^2
27 //COMPARISON OF VALUES WITH LAMINAR FLOW
28 // Disturbance thickness
29 D=dL1/dL2
30 // Displacement thickness
31 DS = dl1/dl2
32 //Wall shear stress
33 \text{ WSS}=\text{tw1/tw2}
34 printf ("\n\nRESULTS\n\n")
35 printf("\n\nDisturbace thickness: \%.3 f m\n\n",dL1)
36 printf("\n\nDisplacement thickness: \%.3 f m\n\n",dl1)
```

```
37 printf("\n\nWall shear stress: %f N/m^2\n\n",tw1)
38 printf ("\n \nCOMPARISON WIH LAMINAR FLOW\n \n'")
39 printf("\n\ Disturbance thicknes: \%.3 f \n\,D)
40 printf("\n\nDisplacement thickness: \%.3 f\n\n",DS)
41 printf("\n\nWall shear stress: %.3f \n\n", WSS)
```

check Appendix AP 28 for dependency:

9_05.sci

Scilab code Exa 9.05 force and power

```
1 //force and power//
2 pathname=get_absolute_file_path('9.05.sce')
3 filename=pathname+filesep()+^{\prime}9.05-data.sci
4 exec(filename)
5 //Speed in m/s:
6 U=s*6076*0.305/3600
7 //Reynolds number:
8 Re=U*L/v
9 //Drag coefficient:
10 Cd=0.455/log10(Re)^2.58-1610/Re
11 / Area(in m^2):
12 A = L * (W+D)
13 //Drag force (in N)
14 Fd=Cd*A*0.5*d*U^2
15 //Power required to overcome skin friction drag(in W
      ):
16 P=Fd*U
17 printf ("\n\nRESULTS\n\n")
18 printf("\n\nDrag force: %f N\n\n,Fd)
19 printf("\n\nPower required to overcome skin friction
       drag: \%.3 f W n n, P)
```

check Appendix AP 27 for dependency:

9_06.sci

Scilab code Exa 9.06 Bending moment

```
1 //Bending moment//
2 pathname=get_absolute_file_path('9.06.sce')
3 filename=pathname+filesep()+^{\prime}9.06-data.sci
4 exec(filename)
5 // Velocity in m/sec:
6 \ V=s*5/18
7 //Reynolds number:
8 Re=d*V*D/u
9 // Value of Cd is obtained as:
10 \text{ Cd} = 0.35;
11 // Area(in m^2):
12 A=L^2;
13 //Moment about the chimney base (in N-m):
14 MO = Cd * A * D / 4 * d * V^2
15 printf("\n\nRESULTS\n\n")
16 printf("\n\nBending moment at the bottom of the
      chimney: \%.3 f N-m n n, MO)
     check Appendix AP 26 for dependency:
     9_07.sci
```

Scilab code Exa 9.07 Time required

```
1 //Time required//
2 pathname=get_absolute_file_path('9.07.sce')
3 filename=pathname+filesep()+'9.07-data.sci'
4 exec(filename)
5 //Time required to decelerate to 100 mph(in seconds)
:
```

```
6 t=(s1-s2)*2*w/(s1*s2)/Cd/d/A/g*3600/5280
7 printf("\n\nRESULTS\n\n")
8 printf("\n\nTime required to decelerate to 100 mph:

%.3 f seconds\n\n",t)

check Appendix AP 25 for dependency:
```

9_08.sci

Scilab code Exa 9.08 Optimum cruise speed

```
1 //Optimum cruise speed//
2 pathname=get_absolute_file_path('9.08.sce')
3 filename=pathname+filesep()+^{\prime}9.08-data.sci
4 exec(filename)
5 //Plotting velocity with drag force
6 V = 175 : 25 : 455;
7
8 [m n] = size(V);
9 for i=1:n
     CL(i) = 2*W/p*(3600/V(i)/5280)^2/A;
10
     Cd(i)=Cd0+CL(i)^2/\%pi/ar;
11
12
     Fd(i) = Cd(i)/CL(i)*W;
13
     FD(i) = Fd(i) / 1000;
14 end
15 plot(V,FD)
16 xtitle('Flight speed vs thrust', 'Flight Speed(in mph
      )', 'Drag Force (in 1000 lbf)')
17 //Optimum cuise speed at speed level is obtained to
      be 320 mph from the graph.
18 Vosl=320;
19 //Ratio of speeds at 30000 ft and at sea level is
      given by:
20 r = sqrt(1/0.375);
21 / Stall speed at 30000 ft is (in mph):
22 \text{ Vs3=Vssl*r};
```

Scilab code Exa 9.09 Aerodynamic and Radius

```
1 //Aerodynamic and Radius//
2 pathname=get_absolute_file_path('9.09.sce')
3 filename=pathname+filesep()+^{\prime}9.09-data.sci
4 exec(filename)
5 //Reynolds number:
6 // Value of wD/2V:
7 W=0.5*N*D/1000/V*2*\%pi/60
8 Red=V*D/v;
9 //For this value, CL is obtained as:
10 CL=0.3;
11 //Aerodynamic lift(in N):
12 FL = \%pi/8*CL*(D/1000)^2*d*V^2;
13 //Radius of curvature of the path in the vertical
      plane (in m) with topspin:
14 Rts=V^2/(g+FL/(m/1000));
15 //Radius of curvature without topspin(in m):
16 Rwts=V^2/g;
17 printf("\n\nRESULTS\n\n")
18 printf("\n\nAerodynamic lift acting on the ball:%.3f
      N n n, FL)
```

- 19 printf(" $\n\$ nRadius of curvature of the path when ball has topspin: $\%.3 \ fm\$ n", Rts)
- 20 printf(" $\n\n$ Radius of curvature of the path when ball has topspin: %.3f m $\n\n$, Rwts)

Chapter 10

Fluid Machinery

```
check Appendix AP 23 for dependency:

10_01.sci

check Appendix AP 17 for dependency:

10_11.sci
```

Scilab code Exa 10.01 input and power

```
//input and power//
pathname=get_absolute_file_path('10.01.sce')
filename=pathname+filesep()+'10.01-data.sci'
exec(filename)
//Impeller exit width b2(in feet):
b2=Q*12/(2*%pi*R2*Vrb2*7.48*60)
//Torque of the Shaft, Tshaft(in ft-lbf):
Tshaft=w*R2^2*p*Q*2*%pi/3600/7.48/144
//Power, Wm(in hp):
Wm=w*Tshaft*2*%pi/60/550
printf("\n\nRESULTS\n\n")
printf("\n\nImpeller exit width: %.3 f feet\n\n",b2)
printf("\n\nTorque input: %.3 f ft-lbf\n\n",Tshaft)
printf("\n\nPower: %.3 f hp\n\n", Wm)
```

Scilab code Exa 10.1 Performance curves

```
1 //Performance curves//
2 pathname=get_absolute_file_path('10.11.sce')
3 filename=pathname+filesep()+^{\prime}10.11-data.sci
4 exec(filename)
5 [nQ mQ] = size(Q1);
6 [np mp] = size(p1);
7 [nP mP] = size(P1);
8 //Volume flow rate for fan 2(in cfm):
9 j=1:mQ;
10 Q2=Q1(j)*(N2/N1)*(D2/D1)^3
11 // Pressure values for fan 2(in inches of H2O):
12 j = 1 : mp;
13 p2=p1(j)*(d2/d1)*((N2/N1)^2)*((D2/D1)^2)
14 //Power values for fan 2(in hp):
15 j=1:mP;
16 P2=P1(j)*(d2/d1)*((N2/N1)^3)*((D2/D1)^5)
17 plot(Q2,p2)
18 xtitle('Performance curves', 'Volume flow rate(in cfm
      )', 'Pressure head(in inches of water)')
19 printf("\n\nType (resume) to continue or (abort) to
      exit \n n")
20 pause
21 clf
22 plot(Q2,P2)
23 xtitle ('Performance curves', 'Volume flow rate (in cfm
     )', 'Power(in hp)')
24 printf("\nType (resume) to continue or (abort) to
      exit \n\n")
25 pause
26 clf
27 plot(Q2, Eff)
28 xtitle('Performance curves', 'Volume flow rate(in cfm
```

```
)', 'Eficiency (in percentage)')

29 // Specific speed of fan (in US customary units) at operating point:

30 Nscu= 1150*110000^0.50*0.045^0.75/7.4^0.75

31 // Specific speed of fan (in SI units) at operating point:

32 Nssi=120*3110^0.5*0.721^0.75/1.84e3^0.75

check Appendix AP 22 for dependency:

10_02.sci
```

Scilab code Exa 10.02 volume and power

```
1 //volume and power//
2 pathname=get_absolute_file_path('10.02.sce')
3 filename=pathname+filesep()+^{\prime}10.02-data.sci
4 exec(filename)
5 U=0.5*(Dh+Dt)/2*1200*2*%pi/60
6 k=tand(alpha1)+cotd(betta1)
7 \text{ Vn1}=U/k
8 V1=Vn1/cosd(alpha1)
9 Vt1=V1*sind(alpha1)
10 Vrb1=Vn1/sind(betta1)
11 //Volume flow rate (in m^3/sec):
12 Q = \%pi/4 * Vn1 * (Dt^2 - Dh^2)
13 k=(U-Vn1*cotd(betta2))/Vn1
14 alpha2= atand(k)
15 V2=Vn1/cosd(alpha2)
16 Vt2=V2*sind(alpha2)
17 //Rotor Torque (in N-m):
18 Tz=p*Q*(Dh+Dt)/4*(Vt2-Vt1)
19 //Power required (in W):
20 \text{ Wm} = \text{w} * 2 * \% \text{pi} / 60 * \text{Tz}
21 printf("\n\nESULTS\n\n")
22 printf("\n\nVolume flow rate: \%.3 \, \text{f m}^3/\sec \n\",Q)
```

```
printf("\n\nRotor Torque: %.3 f N-m\n', Tz)
printf("\n'nPower required: %.3 f W\n'n", Wm)
```

check Appendix AP 21 for dependency:

10_03.sci

Scilab code Exa 10.03 Pump Power

```
1 //Pump Power//
2 pathname=get_absolute_file_path('10.03.sce')
3 filename=pathname+filesep()+^{\prime}10.03-data.sci
4 exec(filename)
5 [nQ mQ] = size(Q);
6 [nps mps]=size(ps);
7 [npd mpd] = size(pd);
8 [nI mI] = size(I);
9 //Correct measured static pressures to he pump
      centreline p1, p2(in psig):
10
    j=1:mps;
11
     p1=ps(j)+px*g*zs/144
12
      j=1:mpd;
     p2=pd(j)+px*g*zd/144
13
     //The value of Pump head(in feet):
14
15
     j=1:mps;
     Hp = (p2(j)-p1(j))/(px*g)*144
16
17
     //Values of Hydraulic Power delivered (in hp):
18
      j=1:mps;
      Wh=Q(j).*(p2(j)-p1(j))/7.48/60*144/550
19
      //Values of motor power output (in hp):
20
21
     j=1:mI;
     Pin=Effm*sqrt(3)*PF*E*I(j)/746
22
     //Values of Pump Efficiecy:
23
24
      j=1:mI;
25
     Effp= Wh(j)./Pin(j)*100
     //Plotting pump characteristics:
26
```

```
plot(Q,Hp,"-o")
plot(Q,Pin,"-+")
plot(Q,Effp,"-*")

xtitle('Pump Characteristics','Volume flow rate(in gpm)',['Pump Efficincy(%)',' Pump Head(in feet)',' Pump Power input(in hp)'])

legend('Hp','Pin','Effp')
```

check Appendix AP 20 for dependency:

10_06.sci

Scilab code Exa 10.06 Specific and relation

```
1 //Specific and relation//
2 pathname=get_absolute_file_path('10.06.sce')
3 filename=pathname+filesep()+^{\prime}10.06-data.sci
4 exec(filename)
5 //Specific speed in Us customary units:
6 \text{ Nscu=N*Qus}^0.5/\text{Hus}^0.75
7 //Conversion to SI units:
8 \text{ w=} 1170*2*\%\text{pi/}60;
9 Qsi=Qus/7.48/60*0.305<sup>3</sup>;
10 Hsi=Hus*0.305;
11 //Energy per unit mass is:
12 h=g*Hsi;
13 // Specific speed in SI units:
14 Nssi=w*Qsi^0.5/h^0.75
15 // Conversion to hertz:
16 whz=N/60;
17 // Specific speed in European units:
18 Nseu=whz*Qsi^0.5/65.5^0.75
19 // Relation between specific speeds in Us customary
      units and European units:
20 Conversionfactor1=Nscu/Nseu
```

```
21 //Relation between specific speeds in Us customary
      units and SI units:
22 Conversionfactor2=Nscu/Nssi
23 printf("\n\nRESULTS\n\n")
24 printf("\n\nSpecific speed in US customary units: %
      .3 f \setminus n \setminus n", Nscu)
25 printf("\n\nSpecific speed in SI units: %.3f \n\n",
      Nssi)
26 printf("\n nSpecific speedin European units: \%.3 f \n
      \n", Nseu)
27 printf("\n\nRelation between specific speeds in Us
      customary units and European units: \%.3 f \n\n",
      Conversionfactor1)
28 printf("\n\nRelation between specific speeds in Us
      customary units and SI units: \%.3 f \ln n,
      Conversionfactor2)
     check Appendix AP 19 for dependency:
     10_07.sci
```

Scilab code Exa 10.07 Comparison of head

```
//Comparison of head//
pathname=get_absolute_file_path('10.07.sce')
filename=pathname+filesep()+'10.07-data.sci'
exec(filename)
//Volume flow rate(in gpm) at shut off condition for N2:
Q2so=N2/N1*Q1so
//Volume flow(in gpm) rate at best efficiency for N2:
Q2be=N2/N1*Q1be
//Relation between pump heads:
head_relation=(N2/N1)^2
//Head(in feet) at shut off condition for N2:
```

Scilab code Exa 10.08 NPSHA and NPSHR

10_08.sci

```
1 //NPSHA and NPSHR//
2 pathname=get_absolute_file_path('10.08.sce')
3 filename=pathname+filesep()+^{\prime}10.08-data.sci
4 exec(filename)
5 // Diameter of pipe (in feet):
6 \text{ Df} = \text{Di}/12
7 // Area of crossection of pipe (in ft^2):
8 A = \%pi/4*Df^2
9 // Velocity of flow (in ft/sec):
10 \quad V = Q/7.48/A/60
11 //For water at T=80F, viscosity=0.927e-5 ft ^2/sec,
      Reynolds number:
12 Re=V*Df/v
13 // Friction loss Coefficient for this value of Re:
14 f=0.0237;
15 //For cast iron, roughness(in feet):
16 e = 0.00085
```

```
17 / e/D is:
18 \text{ e/Df}
19 //Total head loss (in feet):
20 HL=K+f*(SE+OGV)+f*(L/Df)+1
21 //The heads are(in feet):
22 \text{ H1=patm}*144/(p*g)
23 \text{ Vh=V}^2/2/g
24 //Suction head(in feet):
25 \text{ Hs} = \text{H1} + \text{h} - \text{HL} * \text{Vh}
\frac{26}{NPSHA} (in feet):
27 \text{ NPSHA} = \text{Hs} + \text{Vh} - \text{Hv1}
28 //For a flow rate of 1000 gpm, NPSHR(in feet) for
       water at 80 F
29 NPSHR=10
30 //PLOTTING NPSHA AND NPSHR VERSUS VOLUME FLOW RATE:
31 / \text{For } 80 \text{ F}
32 \quad Qp = 0:100:1500;
33 [nQp mQp] = size(Qp);
34
   for j=1:mQp;
35
   Vp(j) = Qp(j) / (7.48 * A * 60);
    Vhp(j) = (Vp(j))^2/2/g;
36
37
    Hs(j)=H1+h-HL*Vhp(j);
38
    end
39
40 for j=1:mQp;
     NPSHAp1(j)=Hs(j)+(Vhp(j))-Hv1;
41
42 end
43
44 plot (Qp, NPSHAp1,"-+")
45 plot (Qh, NPSHRp, "-0")
46 xtitle ('Suction head vs Flow rate', 'Volume flow rate
       (gpm)', 'Suction Head(feet)');
47 printf("\n\nType (Resume) to continue or (abort) to
       end \n "
48 legend('NPSHA', 'NPSHR')
49 pause
50 clf
51
```

check Appendix AP 16 for dependency:

10_12.sci

Scilab code Exa 10.12 Power required

```
//Power required//
pathname=get_absolute_file_path('10.12.sce')
filename=pathname+filesep()+'10.12-data.sci'
exec(filename)
//From given graph, for maximum delivery condition,
Q=48.5gpm.
//Volume of oil per revolution delivered by the pump
(in in^3/rev):
vc=Qe/N*231
//Volumetric Effciency of pump at max flow:
Effv=vc/va
//Operating point of the pump is found to be at 1500
psig,Q=46.5gpm
```

```
11 //Power delivered by the fluid (in hp):
12 Pf=Qo*po1/7.48/60*144/550
13 //Input power(in hp):
14 Pi=Pf/Effp
15 //The power delivered to the load (in hp):
16 \text{ Pl} = \mathbb{Q} * (po1) / 7.48 / 60 * 144 / 550
17 //Power dissipated by throttling (in hp):
18 \text{ Pd=Pf-Pl}
19 //The dissipation with the variable displacement
      pump(in hp):
20 Pvd=Q*(po2-po1)/7.48/60*144/550
21 //Power required for te load sensing pump if pump
      pressure is 100 psi above that required by the
      load (in hp):
22 Pls=Q*100/7.48/60*144/550
23 printf("\n\nRESULTS\n\n")
24 printf("\n\nVolume of oil per revolution delivered
      by the pump: \%.3 \, \text{f in} \, 3/\text{rev} \, \text{n} \, \text{",vc}
25 printf("\n\nRequired pump power input: \%.3 f hp\n\n",
      Pi)
26 printf("\nnPower deliverd to the load: \%.3 f hp\n"
  printf("\n nPower dissipated by throttling: %.3f hp
27
      n \setminus n", Pd)
28 printf("\n nThe dissipation with the variable
      displacement pump: \%.3 f hp \n\n", Pvd)
29 printf("\nnPower required for te load sensing pump
      if pump pressure is 100 psi above that required by
       the load: \%.3 f hp n n, Pls)
      check Appendix AP 15 for dependency:
      10_14.sci
```

Scilab code Exa 10.14 propeller

```
1 //propeller//
2 pathname=get_absolute_file_path('10.14.sce')
3 filename=pathname+filesep()+^{\prime}10.14-data.sci
4 exec(filename)
5 // Propeller Thrust (in MN) :
6 \text{ Ft=P/V}
7 // Required power input to the propeller (in MW):
8 Pin=P/Eff
9 // Calculating value of D(in m):
10 \text{ nD=V/J}
11 D=(Ft*10^6/p/(nD)^2/Cf)^0.5
12 //Operating speed (in rpm) is given by:
13 n=nD/D*60
14 printf("\n\nESULTS\n\n")
15 printf("\n\nDiameter of the single propeller
      required to pwer the ship:\%.3 \text{ f m/n/n},D)
16 printf("\n nOperating speed of the propeller: \%.3 f
      rpm \ n \ n", n)
     check Appendix AP 14 for dependency:
     10_16.sci
```

Scilab code Exa 10.16 Actual

```
//Actual//
pathname=get_absolute_file_path('10.16.sce')
filename=pathname+filesep()+'10.16-data.sci'
exec(filename)
//Tip speed ratio of windmill:
X=N*2*%pi/60*D/2/(V*5/18)
//Accounting for whirl, max attainable efficiency is:
Efw=0.53;
//Kinetic energy flux(in W) is given by:
KEF=0.5*p*(V*5/18)^3*%pi*(D/2)^2
//Actual Efficiency:
```

Chapter 11

Introduction to Compressible Flow

```
check Appendix AP 13 for dependency:
```

```
11_01.sci
```

Scilab code Exa 11.01 Change

```
//Change//
pathname=get_absolute_file_path('11.01.sce')
filename=pathname+filesep()+'11.01-data.sci'
exec(filename)
//Density of air at entry:
d1=p1*10^3/R/T1
//Area(in m^2):
A=m/d1/V1
//Change in enthalpy of air(in kJ/kg):
dh=cp*(T2-T1)
//Change in internal energy of air(in kJ/kg):
du=cv*(T2-T1)
//Change in entropy(in kJ/(kg-K)):
ds=cp*log(T2/T1)-R/1000*log(p2/p1)
printf("\n\nRESULTS\n\n")
```

```
printf("\n\nDuct Area: %.3 f m^2\n\n",A)
printf("\n\nChange in enthalpy of air: %.3 f kJ/kg\n\
n",dh)
printf("\n\nChange in internal energy of air:%.3 f kJ/kg\n\n",du)
printf("\n\nChange in entropy: %.3 f kg-K\n\n",ds)

check Appendix AP 12 for dependency:
11_03.sci
```

Scilab code Exa 11.03 Speed of sound

```
1 //Speed of sound//
2 pathname=get_absolute_file_path('11.03.sce')
3 filename=pathname+filesep()+'11.03-data.sci'
4 exec(filename)
5 // Values of altitude (in m):
6 Al=0:1000:15000
7 [nAl mAl] = size(Al);
8 // Values of temperature at given altitudes (in K):
9 T=[288.2 281.7 275.2 268.7 262.2 255.7 249.2 242.7
      236.2 229.7 223.3 216.8 216.7 216.7 216.7 216.7];
10 [nT mT] = size(T);
11 //Values of speed of sound at these altitudes (in m/
      sec):
12 j = 1 : mT;
13 c=sqrt(k*R*T(j))
14 //Speed of sound at sea level(in m/sec):
15 c1 = sqrt(k*R*T(1))
16 plot(c, A1)
17 xtitle ('Variation of sound speed with altitude','
      Speed of sound (m/sec)', 'Altitude (m)')
18 printf ("\n\nRESULTS\n\n")
19 printf("\n speed of sound at sea level: %.3 f m/sec\
      n \setminus n", c1)
```

```
check Appendix AP 11 for dependency:
```

11_04.sci

Scilab code Exa 11.04 pressure and change

```
1 //pressure and change//
2 pathname=get_absolute_file_path('11.04.sce')
3 filename=pathname+filesep()+'11.04-data.sci'
4 exec(filename)
5 //Mach number at entry:
6 M1=V1/sqrt(k*R*T1)
7 //Stagnation pressure at entry (in kPa):
8 p01=p1*(1+(k-1)/2*M1^2)^(k/(k-1))
9 //Stagnation temperature at entry (in K):
10 T01=T1*(1+(k-1)/2*M1^2)
11 //Static pressure at exit(in kPa):
12 p2=p02/(1+(k-1)/2*M2^2)^(k/(k-1))
13 //Temperature at exit(in K):
14 T2=T02/(1+(k-1)/2*M2^2)
15 //Change in entropy (in kJ/kg-K):
16 ds=cp*log(T2/T1)-R/1000*log(p2/p1)
17 printf ("\n\nRESULTS\n\n")
18 printf("\n nStagnation pressure at entry: %.3 f kPa\n
     \n",p01)
19 printf("\n Stagnation temperature at entry: %.3 f K\n
     n \ n", T01)
20 printf("\n\nStatic pressure at exit: \%.3f kPa\n\n",
21 printf("\nnTemperature at exit: %.3 f K\nn", T2)
22 printf("\n\nChange in entropy: \%.3 f kJ/kg-K\n\n", ds)
```

Chapter 12

Steady One Dimensional Compressible Flow

```
check Appendix AP 10 for dependency:
```

```
12_01.sci
```

Scilab code Exa 12.01 pressure and area

```
//pressure and area//
pathname=get_absolute_file_path('12.01.sce')
filename=pathname+filesep()+'12.01-data.sci'
exec(filename)
// Here the stagnation quantities are constant.
// Stagnation temperature(in K):
T0=T1*(1+(k-1)/2*M1^2)
//Stagnation pressure(in kPa):
p0=p1*((1+(k-1)/2*M1^2)^(k/(k-1)))
// Finding T2/T1:
T=t2/t1
// Temperature at exit(in K):
T2=T*T1
// Finding p2/p1:
P=P2/P1
```

```
16 // Pressure at exit(in kPa):
17 p2 = P2 * p1
18 // Density of air at exit(in kg/m^3):
19 d2=p2*10^3/R/T2
20 // Velocity of air at exit(in m/sec):
21 \quad V2=M2*sqrt(k*R*T2)
22 // Finding A2/A1:
23 = a^2/a^1
24 //Area at exit(in m^2):
25 \quad A2 = a * A1
26 printf ("\n\nRESULTS\n\n")
27 printf("\n\nStagnation temperature: %.3 f K\n\n", T0)
28 printf("\n\nStagantion pressure: %.3f kPa\n\n",p0)
29 printf("\n\nTemperature a exit %.3 f K\n\n",T2)
30 printf("\n Pressure at exit: %.3 f kPa\n",p2)
31 printf("\nnDensity of air at exit: \%.3 f kg/m^3n\n"
      ,d2)
32 printf("\n\nVelocity of air at exit: %.3 f m/sec\n\"
33 printf("\n nArea at exit: \%.3 f \n , A2)
     check Appendix AP 9 for dependency:
```

Scilab code Exa 12.02 Mass flow

12_02.sci

```
1 //Mass flow//
2 pathname=get_absolute_file_path('12.02.sce')
3 filename=pathname+filesep()+'12.02-data.sci'
4 exec(filename)
5 //Checking for chocking:
6 c=pb/p0;
7 if(c<=0.528)
8 //choked
9 else</pre>
```

```
10
     //Not choked
     //Therefore pressure at exit = back pressure
11
12
     pe=pb;
     //Mach number at exit:
13
14
     Me = (((p0/pe)^((k-1)/k)-1)*(2/(k-1)))^0.5
15
     //Temperature at exit(in K):
     Te=T0/(1+(k-1)/2*Me^2)
16
     //Velocity at exit(in m/sec):
17
     Ve=Me*sqrt(k*R*Te)
18
     //Density at exit(in kg/m^3):
19
20
     de=pe*10^3/R/Te
21
     //Mass flow rate of air(kg/sec):
22
     m = de * Ve * Ae
23 end:
24 printf("\n\nRESULTS\n\n")
25 printf("\n\n nMach number at exit: \%.3 f\n\n", Me)
26 printf("\n\n mass flow rate of air: %.3 f kg/sec\n\n",
     m)
```

check Appendix AP 8 for dependency:

12_03.sci

Scilab code Exa 12.03 mass and area

```
1 //mass and area//
2 pathname=get_absolute_file_path('12.03.sce')
3 filename=pathname+filesep()+'12.03-data.sci'
4 exec(filename)
5 //Saturation pressure(in psia):
6 p0=p1*(1+(k-1)/2*M1^2)^(k/(k-1))
7 // Checking for choking:
8 x=pb/p0;
9 \text{ if}(x>0.528)
     //Not choked
10
11 else
```

```
12
     //choked
13 end
14 //As there is choking:
15 Mt = 1;
16 // Velocity at entry:
17 V1=M1*sqrt(k*R*(T1+460)*32.2)
18 // Density at the entry (in lbm/ft<sup>3</sup>):
19 d1=p1/(R*(T1+460))*144
20 //Mass flow rate(in lbm/sec):
21 m = d1 * V1 * A1
22 //Finding the value of A1/A*;
23 A=1/M1*((1+(k-1)/2*M1^2)/(1+(k-1)/2))^((k+1)/(2*(k-1)/2))^2
      -1)))
24 //For choked flow, At=A*
25 \text{ At} = \text{A1/A}
26 printf ("\n\nRESULTS\n\n")
27 printf("\nnMach number at throat: \%.3 f\n", Mt)
28 printf("\n \n sec\n \n",m)
29 printf("\n\nArea at throat: %.3 f ft^2\n\n", At)
     check Appendix AP 7 for dependency:
```

12_04.sci

Scilab code Exa 12.04 throat

```
//throat//
pathname=get_absolute_file_path('12.04.sce')
filename=pathname+filesep()+'12.04-data.sci'
exec(filename)
//Temperature at the throat(in K):
Tt=T0/(1+(k-1)/2*Mt^2)
//Pressure at throat(in kPa):
pt=p0*(Tt/T0)^(k/(k-1))
//Density at throat(in kg/m^3):
dt=pt*1000/R/Tt
```

```
11 // Velocity at the throat (in m/s):
12 Vt=Mt*sqrt(k*R*Tt)
13 //Value of At/A*:
14 \text{ Ax}=1/\text{Mt}*((1+(k-1)/2*\text{Mt}^2)/(1+(k-1)/2))^((k+1)/(2*(k-1)/2))^2
      -1)))
15 //Stagnation properties are constant
16 //As a result pressure at exit,
17 pe=pb;
18 //The Mach number at the exit is therefore given by
19 Me=sqrt(((p0/pe)^((k-1)/k)-1)*2/(k-1))
20 // Calculating the value of Ae/A*:
21 Ay=1/Me*((1+(k-1)/2*Me^2)/(1+(k-1)/2))^((k+1)/(2*(k-1)/2))
      -1)))
22 //Value of A*(in m<sup>2</sup>):
23 \quad A_star=Ae/Ay
24 //Area at throat (in m^2):
25 \text{ At}=\text{Ax}*\text{A_star}
26 printf("\n\nRESULTS\n\n")
27 printf("\nnTemperature at the throat: \%.3 f K\nn",
      Tt)
28 printf("\n\nPressure at throat: \%.3 f kPa\n\n",pt)
29 printf("\n \nDensity at throat: \%.3 f \kg/m^3 \n', dt)
30 printf("\n\nVelocity at the throat: %.3 f m/sec\n\n",
      Vt)
31 printf("\nnMach number at the exit: \%.3 f \n", Me)
32 printf("\nnArea at throat: %.3 f m<sup>2</sup>\nn", At)
      check Appendix AP 6 for dependency:
      12_05.sci
```

Scilab code Exa 12.05 number and flow

```
1 //number and flow//
2 pathname=get_absolute_file_path('12.05.sce')
3 filename=pathname+filesep()+'12.05-data.sci'
```

Scilab code Exa 12.06 mass and volume

```
1 //mass and volume//
2 pathname=get_absolute_file_path('12.06.sce')
3 filename=pathname+filesep()+^{\prime}12.06-data.sci
4 exec(filename)
5 //Mach umber at section 1:
6 M1 = sqrt((2/(k-1)*((p0/p1)^((k-1)/k)-1)))
7 //Temperature at section 1(in K):
8 T1=T0/(1+(k-1)/2*M1^2)
9 // Density at section 1(in kg/m^3):
10 d1 = p1 * 1000 / R / T1
11 // Velocity at section1 (in m/sec):
12 V1=M1*sqrt(k*R*T1)
13 //Area at section 1(in m<sup>2</sup>):
14 \quad A1 = \%pi/4*D^2
15 //Mass flow rate(in kg/sec):
16 \text{ m} = d1 * A1 * V1
17 //Mach number at section 2:
18 M2 = sqrt((2/(k-1))*((T0/T2)-1))
19 // Velocity at section 2(in m/sec):
```

```
20 \quad V2=M2*sqrt(k*R*T2)
21 // Density at section 2(in kg/m^3):
22 d2=d1*V1/V2
23 // Pressure at section 2(in kPa):
24 p2=d2/1000*R*T2
25 //Stagnation pressure at section 2(in kPa):
26 p02=p2*(1+(k-1)/2*M2^2)^(k/(k-1))
27 //Force exerted on control volume by duct wall(in N)
28 F = (p2-p1)*1000*A1+m*(V2-V1)
29 printf("\n\nESULTS\n\n")
30 printf("\n \n mass flow rate: %.3 f kg/sec\n \n",m)
31 printf("\n\nLocal isentropic stagnation pressure at
      section 2:\%.3 f kPa\n\n",p02)
32 printf("\n\nForce exerted on control volume by duct
      wall:\%.3f N\n\n",F)
     check Appendix AP 4 for dependency:
     12_07.sci
```

Scilab code Exa 12.07 length

```
1 //length//
2 pathname=get_absolute_file_path('12.07.sce')
3 filename=pathname+filesep()+'12.07-data.sci'
4 exec(filename)
5 //Mach number at section 1:
6 M1= sqrt(2/(k-1)*((p0/(p0+p1))^((k-1)/k)-1))
7 //Temperature at section 1(in K):
8 T1=T0/(1+(k-1)/2*(M1)^2)
9 V1=M1*sqrt(k*R*T1)
10 //Pressure at section 1(in kPa):
11 p1=g*dHg*(760-18.9)*10^-3
12 //Density at section 1(in kg/m^3):
13 d1=p1/R/T1
```

```
14 / At M1 = 0.190,
15 //(p/p*) 1:
16 P1=5.745
17 // (fLmax/Dh) 1:
18 F1=16.38
19 //Value of L13(in m):
20 L13=F1*D/f
21 //Value of (p/p*) 2:
22 P2=p2/p1*P1
23 //For this value, Value of M2 is obtained as 0.4
24 \quad M2 = 0.4;
25 / \text{For M} = 0.4, fLmX/D = 2.309
26 F2=2.309
27 //Value of L23(in m):
28 L23=F2*D/f
29 //Length of duct between section 1 and 2(in m):
30 L12=L13-L23
31 printf("\n\nESULTS\n\n")
32 printf("\n\nLength of duct required for choking from
       section 1: \%3f \text{ m} \text{ n} \text{ n}, L13)
33 printf("\n\n number section 2: %.3 f \n\n, M2)
34 printf("\n\Length of duct between section 1 and 2: \%
      .3 f m n n", L12)
      check Appendix AP 3 for dependency:
      12_08.sci
```

Scilab code Exa 12.08 velocity and entropy

```
// velocity and entropy//
pathname=get_absolute_file_path('12.08.sce')
filename=pathname+filesep()+'12.08-data.sci'
exec(filename)
// Density at section 1(in lbm/ft^3):
d1=p1*144/R/T1
```

```
7 // Velocity at section 2(in ft/sec):
8 V2=(p1-p2)*144/d1/V1*32.2+V1
9 //Density at section 2(in lbm/ft3):
10 d2 = d1 * V1 / V2
11 / Temperature at section 2(in R):
12 T2=p2/d2/R*144
13 //Mach number at section 2:
14 M2=V2/sqrt(k*R*32.16*T2)
15 //Stagnation Temperature at section 2(in R):
16 \quad T02=T2*(1+(k-1)/2*M2^2)
17 //Stagnation pressure at section 2 (in psia):
18 p02=p2*(T02/T2)^(k/(k-1))
19 //Mach Number at section 1:
20 M1=V1/sqrt(k*R*32.16*T1)
21 //Stagnation temperature at section 1(in R):
22 T01=T1*(1+(k-1)/2*M1^2)
23 //Energy added(in Btu/lbm):
24 E = Cp * (T02 - T01)
25 //Change in entropy (in Btu/(lbm-R)):
26 \text{ dS} = \text{Cp} * \log (T2/T1) - (\text{Cp} - \text{Cv}) * \log (\text{p2/p1})
27 printf("\n\nRESULTS\n\n")
28 printf("\n\nVelocity at section 2: %.3f ft/sec\n\",
      V2)
29 printf("\nnDensity at section 2: %.3 f lbm/ft^3n^"
30 printf("\nnTemperature at section 2: %.3 f R\nn", T2
31 printf("\n nStagnation Temperature at section 2: \%.3
      f R n n, T02)
32 printf("\n nStagnation pressure at section 2: \%.3 f
      psia \n\n", p02)
33 printf("\nnEnergy added: %.3f Btu/lbm\nn",E)
34 printf("\n\nChange in entropy: %.3 f Btu/(lbm-R)\n'"
      ,dS)
     check Appendix AP 2 for dependency:
```

12_09.sci

Scilab code Exa 12.09 Temperature and entropy

```
1 //Temperature and entropy//
2 pathname=get_absolute_file_path('12.09.sce')
3 filename=pathname+filesep()+^{\prime}12.09-data.sci
4 exec(filename)
5 //Mach nuber at section 1:
6 M1=V1/sqrt(k*R*T1)
7 //For these value of M1 and M2, the following values
      are obtained:
8 // (To/T0*) 1:
9 \text{ t01=0.7934};
10 // (T0/T0*) 2:
11 t02=0.9787;
12 //(p0/p0*)1:
13 P01=1.503;
14 //(p0/p0*) 2:
15 P02=1.019;
16 //(T/T*) 1:
17 t1=0.5289;
18 // (T/T*) 2:
19 t2=0.9119;
20 //(p/p*) 1:
21 P1 = 0.3636;
22 //(p/p*) 2:
23 P2=0.7958;
24 / (V/V*) 1:
25 \text{ v1}=1.455;
26 / (V/V*) 2:
27 \text{ v} 2 = 1.146;
28 //Value of T2/T1:
29 t=t2/t1
30 //Temperature at section 2(in K):
31 T2=t*T1
```

```
32 //Value of p2/p1:
33 p = P2/P1
34 // Pressure at section 2(in kPa):
35 p2=p*p1
36 //Value of V2/V1:
37 v = v2/v1
38 // Velocity at section 2(in m/sec):
39 \ V2 = v * V1
40 // Density at section 2(in kg/m^3):
41 d2=p2*1000/R/T2
42 //At M1, T/T0=0.5556
43 T01=T1/0.5556
44 //At M2, T/T0=0.7764
45 \quad T02 = T2/0.7764
46 //Heat added(in kJ/kg):
47 E = Cp * (T02 - T01)
48 //Change in entropy(kJ/kg-K):
49 dS = Cp * log(T2/T1) - R * log(p2/p1)/1000
50 printf("\n\nRESULTS\n\n")
51 printf("\nnTemperature at section 2: %.3 f K\nn", T2
      )
52 printf("\n\nPressure at section 2: %.3f kPa\n\n",p2)
53 printf("\n\nVelocity at section 2: %.3 f m/sec\n\n",
      V2)
54 printf("\n\nDensity at section 2: %.3 f kg/m<sup>3</sup>\n\n",
      d2)
55 printf("\nstagnation temperature at section 2: \%.3
      f K n n, T02)
56 printf("\nnHeat added: %.3 f kJ/kg\n",E)
57 printf("\n\nChange in entropy: %.3 f kJ/kg\n\n",dS)
     check Appendix AP 1 for dependency:
     12_10.sci
```

Scilab code Exa 12.10 Temperature

```
1 //Temperature//
2 pathname=get_absolute_file_path('12.10.sce')
3 filename=pathname+filesep()+^{\prime}12.10-data.sci
4 exec(filename)
5 // Density at section 1(in kg/m^3):
6 d1=p1*1000/R/T1
7 //Mach number at section 1:
8 M1=V1/sqrt(k*R*T1)
9 //Stagnation temperature at section 1(in K):
10 T01=T1*(1+(k-1)/2*M1^2)
11 //Stagnation pressure at section 1(in kPa):
12 p01=p1*(1+(k-1)/2*M1^2)^(k/(k-1))
13 //The following values are obtained from the
      appendix:
14 //po2/p01:
15 p0=0.7209;
16 / T2/T1:
17 T=1.687;
18 / p2/p1:
19 p=4.5;
20 //V2/V1:
21 \quad V = 0.3750;
22 //Temperature at section 2 (in K):
23 T2=T*T1
24 // Pressure at section 2(in kPa):
25 p2=p*p1
\frac{26}{\sqrt{\text{Velocity}}} at section 2(\text{in m/sec}):
27 V2 = V * V1
28 // Density at section 2 (in kg/m^3):
29 	 d2=p2*1000/R/T2
30 //Stagnation pressure at section 2(in kPa):
31 p02=p0*p01
32 //Stagnation temperature at section 2(in K):
33 T02=T01;
34 //Change in entropy (in kJ/(kg-K)):
35 \text{ dS} = -R/1000 * \log(p0)
36 printf("\n\nESULTS\n\n")
```

42 printf(" $\n\$ nChange in entropy: %.3 f kg-K $\n\$ n",dS) 43 printf(" $\n\$ nStagnation temperature at section 2: %.3

f K n n", T02)

Appendix

Scilab code AP 1 data

```
1 //Temperature at section 1(in K):
2 T1=278;
3 //Pressure at section 1(in kPa):
4 p1=65;
5 //Velocity at section 1(in m/sec):
6 V1=668;
7 //Value of gas constant(in N-m/kg-K):
8 R=287;
9 //Value of k:
10 k=1.4;
```

Scilab code AP 2 data

```
14 Cp=1;
```

Scilab code AP 3 data

```
1 //Temperature at section 1(in R):
2 T1 = 600;
3 //Pressure at section 1(in psia):
4 p1=20;
5 // Pressure at section 2(in psia):
6 p2=10;
7 // Velocity at section 1(in ft/s):
8 V1 = 360;
9 // \text{Cross-sectional} area of the duct(in ft<sup>2</sup>):
10 A = 0.25;
11 //Gas Constant (in ft-lbf/lbm-R):
12 R=53.3;
13 //Value of k:
14 k = 1.4;
15 // Specific heat at constant presure (in Btu/lbm-R):
16 \text{ Cp} = 0.24;
17 // Specific heat at constant volume (in Btu/lbm-R):
18 Cv = 0.171;
```

Scilab code AP 4 data

```
//Stagnation temperature(in K):
T0=296;
//Stagnation pressure(in mm of Hg):
p0=760;
//Gauge pressure at section 1(in mm of Hg):
p1=-18.9;
//Gauge pressure at section2(in mm of Hg):
p2=-412;
//Mach number at 3:
M3=1;
//Gas constant:
R=287;
//Density of mercury(kg/m^3):
```

```
14 \text{ dHg} = 13500;
15 // Acceleration due to gravity (in m/sec^2):
16 \text{ g=9.8};
17 // Friction factor:
18 f = 0.0235;
19 // Diameter of tube (in m):
20 D=7.16*10^{-3};
21 // Value of k:
22 k=1.4;
   Scilab code AP 5 data
1 //Diameter of pipe(in m):
2 D=7.16*10^-3;
3 //Stagnation pressure (in kPa):
4 p0=101;
5 //Stagnation temperature(in K):
6 T0 = 296;
7 // Pressure at section 1(in kPa):
8 p1=98.5;
9 //Temperature at section 2(in K):
10 T2 = 287;
11 //Gas constant (in N-m/kg-K):
12 R = 287;
13 //Value of k:
14 k = 1.4;
   Scilab code AP 6 data
1 //Stagnation temperature(in K):
2 T0 = 350;
3 //Stagnation pressure(in kPa)\
4 p0=1000;
5 //Pressure at exit(in kPa)
6 pe=87.5;
7 //Back Pressure(in kPa):
8 \text{ pb=50};
9 //Area at exit(in m^2):
```

```
10 Ae=0.001;
11 //Gas Constant (in N-m/kg-K)
12 R = 287;
13 //Value of k:
14 k=1.4;
   Scilab code AP 7 data
1 //Stagnation temperature(in K):
2 T0 = 350;
3 //Stagnation pressure(in kPa):
4 p0=1000;
5 //Back Pressure(in kPa):
6 pb = 954;
7 //Mach number at throat:
8 \text{ Mt} = 0.68;
9 //Area at exit(in m^2):
10 Ae=0.001;
11 //Value of k:
12 k=1.4;
13 //Gas Constant (in N-m/kg-K):
14 R = 287;
   Scilab code AP 8 data
1 //Mach number at entry:
2 M1 = 0.52;
3 //Temperature at entry (in F):
4 T1 = 40;
5 // Pressure at entry (in psia):
6 p1 = 60;
7 // Area at entry (in ft ^2):
8 \quad A1 = 0.013;
9 //Back pressure(in psia):
10 pb=30;
11 //Gas Consant (in ft-lbf/lbm-R)
12 R=53.3;
13 //Value of k:
```

```
14 k=1.4;
```

Scilab code AP 9 data

```
//Throat area of nozzle(in m^2):
2 Ae=0.001;
3 //Back pressure of air(in kPa):
4 pb=591;
5 //Stagnation pressure(in kPa):
6 p0=1000;
7 //Stagnation temperature(in K):
8 T0=333;
9 //Gas Constant(in N-m/kg-K):
10 R=287;
11 //Value of k:
12 k=1.4;
```

Scilab code AP 10 data

```
1 //Mach number at entry:
2 M1 = 0.3;
3 //Temperature at entry (in K):
4 T1 = 335;
5 // Pressure at entry(in kPa):
6 p1 = 650;
7 // Area at entry (in m^2):
8 \quad A1 = 0.001;
9 //Mach number at exit:
10 M2 = 0.8;
11 ///Value of k:
12 k=1.4;
13 //For the Mach no:0.3:
14 //T/T0:
15 t1=0.9823,
16 //p/p0:
17 P1=0.9395;
18 //d/d0:
19 den1=0.9564;
```

```
20 //A/A*:
21 \quad a1=2.035;
22 // For the Mach no:0.8:
23 // T/T0:
24 t2=0.8865;
25 //p/p0:
26 P2 = 0.6560;
27 //d/d0:
28 \text{ den2=0.7400};
29 //A/A*:
30 \quad a2=1.038;
31 //Gas Constant (in N-m/kg-K):
32 R = 287;
   Scilab code AP 11 data
1 // Pressure at entry (in kPa):
2 p1 = 350;
3 //Temperature at entry (in K)
4 T1 = 333;
5 // Velocity at entry (in m/s):
6 V1 = 183;
7 //Mach no. at exit:
8 M2=1.3;
9 //Stagnation pressure at exit(in kPa):
10 p02=385;
11 //Stagnation temperature at exit(in K):
12 \quad T02 = 350;
13 //Value of k:
14 k=1.4;
15 //Gas constant (in N-m/kg-K)
16 R = 287;
17 // Specific heat at constant pressure (kJ/(kg-K):
18 \text{ cp=1};
   Scilab code AP 12 data
```

1 // Value of k:

```
2 k=1.4;
3 //Gas Constant(in Kj/(kg-K)):
4 R = 287;
   Scilab code AP 13 data
1 //Temperature of air entering the cold section (in K)
2 T1=440:
3 // Absolute pressure of air entering the cold section
      (in kPa):
4 p1=188;
5 // Velocity of air entering the cold section (in m/sec
      ):
6 V1 = 210;
7 //Temperature of air at outlet:(in K)
8 T2 = 351;
9 // Absolute pressure of air at outlet (in kPa):
10 p2 = 213;
11 //Rate of heat loss in the section (in kJ/sec):
12 //Gas Constant (in N-m):
13 R = 287;
14 //Mass flow rate of air(in kg/sec):
15 \text{ m=0.15};
16 // Specific heat at constant pressue (in kJ/(kg-K)):
17 \text{ cp=1};
18 //Specific energy at constant volume(in kJ/(kg-K)):
19 cv = 0.717;
   Scilab code AP 14 data
1 // Diameter of windmill (in m):
2 D=26;
3 //Operating speed(in rpm):
4 N = 20;
5 //Wind speed (in km/hr):
6 V = 36;
7 //Power Output(in W):
```

```
8 Po=41000;
9 //Maximum efficiency occurs in following conditions:
10 // Efficiency:
11 Eff=0.593;
12 //Inteference Factor:
13 \ a=1/3;
14 // Density of air (in kg/m^3):
15 p=1.23;
   Scilab code AP 15 data
1 //Total propulsion power requirement (in MW):
2 P = 11.4;
3 //From the given curves, Value of coefficients
      atoptimum efficiency are as follows:
4 //Speed of advance coefficient:
5 J = 0.85;
6 //Thrust Coefficient:
7 Cf = 0.1;
8 //Torque Coefficint:
9 \text{ Ct} = 0.02;
10 // Efficiency:
11 Eff=0.66;
12 // Velocity of ship (in m/sec):
13 V=6.69;
14 // Density of water (in kg/m^3):
15 p=1025;
   Scilab code AP 16 data
1 //Operation speed(in rpm):
2 N = 2000;
3 //Volume flow rate(in gpm):
4 Q = 20;
5 // Pressure (in psig):
6 p=1500;
7 // Actual Pump Displacement (in ^3/rev):
8 \text{ va} = 5.9;
```

```
9 //Volume flow rate at operating condition (in gpm):
10 Qo = 46.5;
11 //Volume flow rate at maximum delivery (in gpm):
12 Qe = 48.5;
13 // Pressure at operation condition (in psi):
14 po1=1500;
15 // Efficiency of pump at operating condition:
16 Effp=0.84;
17 //Pressure at operating condition case 2(in psig):
18 \text{ po2} = 3000;
   Scilab code AP 17 data
1 //Diameter of fan 1 (in inches):
2 D1=36;
3 //Operating speed of fan 1(in rpm):
4 N1 = 600
5 // Density of air used in fan 1(in lbm/ft<sup>3</sup>):
6 	 d1 = 0.075;
7 // Diameter of fan 2(in inches):
8 D2 = 42;
9 //Operating speed of fan 2(in rpm):
10 N2 = 1150;
11 // Density of aif usd in fan 2(in lbm/ft^3):
12 d2 = 0.045;
13 //The following values are obtained from the given
      graph
14 // Values of volume flow rate (in cfm) through fan 1:
15 Q1= [0 10000 20000 30000 40000 50000 60000];
16 // Values of pressure (in inches of H2O):
17 p1=[ 3.68 3.75 3.50 2.96 2.12 1.02 0];
18 // Values of power (in hp):
19 P1=[ 11.1 15.1 18.6 21.4 23.1 23.1 21.0];
20 // Efficiency (in %):
21 Eff=[0 37 59 65 57 34 0];
```

Scilab code AP 18 data

```
1 //For 5 inch nominal pipe line, diameter D:
2 \text{ Di} = 5.047;
3 //Length of pipeline(in feet):
4 L=6;
5 //Operatng spped (in rpm):
6 N = 1750;
7 //Water level abovepump centreline (in feet):
8 h=3.5;
9 //Temperature 1 of water(in Farenheit):
10 \text{ T1=80};
11 //Temperature 2 of water (in Farenheit):
12 T2 = 180;
13 //Volume flow rate of water(in gpm):
14 \quad Q = 1000;
15 //Minor loss Coefficients:
16 \text{ K=0.5}; SE=30; OGV=8;
17 // Atmospheric pressure (in lbf/in^2):
18 \text{ patm} = 14.7;
19 // Density of air (slug/ft<sup>3</sup>):
20 p=1.93;
21 // Acceleration due to gravity (in ft/sec^2):
22 g=32.2;
23 //Head(in feet) due to vapor pressure of water for T
       =80F:
24 \text{ Hv1} = 1.17;
25 //Head(in feet) due to vapor pressure of water for T
       =180F:
26 \text{ Hv} 2 = 17.3;
27 //Kinematic viscosity of water at 80F:
28 \quad v = 0.927 e - 5;
29 //Value of discharges for plotting NPSHR(in gpm):
30 Qh = [500 700 900 1100 1300]
31 // Values of NPSHR obtained from Fig. D3 of appendix
      D:
32 \text{ NPSHRp} = [7 8 9.5 12 16]
```

Scilab code AP 19 data

```
1 //Volume flow rate (in gpm) at shut off condition for
       N1:
2 Q1so=0;
3 //Volume flow(in gpm) rate at best efficiency for N1
4 Q1be=300;
5 //Head(in feet) at shut off condition for N1:
6 \text{ H1so} = 25;
7 //Head(in feet) at best efficiency condition for N1:
8 \text{ H1be} = 21.9
9 //Operation Speed 1:
10 N1 = 1170;
11 //Operation speed 2:
12 N2 = 1750;
   Scilab code AP 20 data
1 //Head in Us customary units:
2 \text{ Hus} = 21.9;
3 //Volume flow rate in US customary units:
4 Qus=300;
5 //Working seed in rpm:
6 N = 1170;
7 // Aceleration due to graviy in m/s<sup>2</sup>
8 g=9.81;
   Scilab code AP 21 data
1 //Rate of flow in gm:
2 Q=[0 500 800 1000 1100 1200 1400 1500];
3 //Suction pressure in psig:
4 ps=[0.65\ 0.25\ -0.35\ -0.92\ -1.24\ -1.62\ -2.42\ -2.89];
5 // Discharge pressure in psig:
6 pd=[53.3 48.3 42.3 36.9 33 27.8 15.3 7.3];
7 //Motor Current in amps:
8 I=[18 26.2 31 33.9 35.2 36.3 38 39];
9 // Acceleration due to gravity in ft/s^2:
10 \text{ g=} 32.2;
```

```
11 //Value of Zs in feet
12 zs=1;
13 // Density of air in slug/ft^3:
14 \text{ px} = 1.94;
15 // Value of ZD in feet:
16 \text{ zd} = 3;
17 // Density of fluid in slug/ft^3:
18 \text{ py} = 1000;
19 //Motor Efficiency:
20 Effm=0.9;
21 //Motor Supply in volts:
22 E = 460;
23 //Power Factor:
24 PF=0.875;
   Scilab code AP 22 data
1 //Tip Diameter in metres:
2 Dt=1.1;
3 //Hub Diameter in metres:
4 Dh=0.8;
5 // Operating Speed in rpm:
6 \text{ w} = 1200;
7 //Absolute inlet angle in degrees:
8 alpha1=30;
9 //Blade inlet angle in degrees:
10 betta1=30;
11 //Blade outlet angle in degrees:
12 betta2=60;
13 // Density of air in kg/m<sup>3</sup>
14 p=1.23;
   Scilab code AP 23 data
1 //Volume flow rate in gpm:
2 Q = 150;
3 //Value of Vrb2 in ft/sec:
4 Vrb2=10;
```

```
5 //Radius of outter impeller in inches:
6 R2 = 2;
7 //Impeller Speed in rpm:
8 \quad w = 3450;
9 //Density of air in slug/ft<sup>3</sup>
10 p=1.94;
   Scilab code AP 24 data
1 //Mass of the tennis ball(in grams):
2 m = 57;
3 //Diameter of the ball (in mm):
4 D=64;
5 // Velocity with which te ball is hit(in m/s):\
6 V = 25;
7 //Topspin given on the ball(in rpm):
8 N = 7500;
9 // Acceleration due to gravity (in m/s^2):
10 g=9.81;
11 //Kinematic viscosity (in m^2/s):
12 v=1.46*10^-5
13 // Desity of air (in kg/m^3):
14 d=1.23;
   Scilab code AP 25 data
1 //Wing area(in ft^2):
2 A = 1600;
3 //Aspect ratio:
4 \text{ ar} = 6.5;
5 //Groos weight of aircraft (in lbf):
6 W = 150000;
7 // Coefficient of drag at zero lift :
8 \text{ Cd0} = 0.0182;
9 //Sonic speed at sea level(in mph):
10 c = 759;
11 // Density of air (in slug/ft^3):
12 p=0.00238;
```

```
13 //Srall speed at sea level(in mph):
14 Vssl=175;
   Scilab code AP 26 data
1 //Weight of the dragster(in lbf):
2 w = 1600;
3 //Speed of dragster(in mph):
4 s1=270;
5 // Area of drag chute (in ft^2):
6 \quad A = 25;
7 //Speed of dragster after deceleration (in mph):
8 s2=100;
9 // Acceleration due to gravity (in ft/sec^2):
10 g=32.2;
11 // Density of air (in slug/ft^3):
12 d=0.00238;
13 // Value of coefficient of drag:
14 Cd=1.42;
   Scilab code AP 27 data
1 // Diameter of chimney (in m):
2 D=1;
3 // Height of chimney (in m):
4 L=25;
5 //Speed of wind(in kmph):
6 \text{ s} = 50;
7 // Density of air (in kg/m^3):
8 d=1.23;
9 // Viscosity of air (in kg/(m-s)):
10 u=1.79*10^-5;
11 // Pressure (in kPa):
12 p = 101;
```

Scilab code AP 28 data

```
1 //Length of the supertanker(in m):
2 L=360;
3 //Width of supertanker(in m):
4 W = 70;
5 //Draft of the supertanker(in m):
6 D = 50;
7 // Cruising speed in water(in knots):
8 s = 13;
9 //Kinematic viscosity at 10 C
10 v=1.37*10^-6;
11 // Density of sea water (in kg/m^3):
12 d=1020;
  Scilab code AP 29 data
1 // Veocity of flow (in m/sec):
2 U=1;
3 //Length of flat plate(in m):
4 L=1;
5 // Density of water (in kg/m^3):
6 d = 999;
7 // Kinematic viscosity of water(in m^2/sec):
8 v = 10^{-6};
  Scilab code AP 30 data
1 //Lengh of side of the test section (in mm):
2 L=305;
3 //Freesteam speed at section 1(in m/sec):
4 U1=26;
5 // Displacement thickness at section 1(in mm):
6 d1=1.5;
7 // Displacment thickness at section 2(in mm):
8 d2=2.1;
```

Scilab code AP 31 data

```
1 //Volume flw rate of ai(in m<sup>3</sup>/sec):
2 Q = 1;
3 // Diameter of pipe (in m):
4 D=0.25;
5 // Density of air (in kg/m^3):
6 d1=1.23;
7 // Acceleration due to gravity (in m/s^2):
8 g=9.8;
9 // Density of water (in kg/m^3):
10 d2=999;
11 //Maxmum range of manometer(in m):
12 h=0.3;
13 //Kinematic viscosity (in m^2/s):
14 v=1.46*10^-5;
   Scilab code AP 32 data
1 // Nozzle exit diameter (in mm):
2 D=25;
3 //N/R1 value value:
4 N_R=3;
5 //AR value:
6 \quad A_R = 2;
7 // Static head available from the main(in m):
8 z0=1.5;
9 // Acceleration due to gravity (in m/sec^2):
10 g=9.8;
11 //Value of Cp:
12 \text{ Cp=0.45};
   Scilab code AP 33 data
1 //Length of copper wire(in ft):
2 L=10;
3 //Inner diameer of pipe(in inches):
4 D=1.5;
5 // Dischare (in ft^3/sec):
6 \quad Q = 0.566;
```

```
7 //Level of reservoir above pipe centreline (inn feet)
8 h=85.1;
9 //Kinematic viscosity at 70 F(in ft^2/s):
10 v=1.05*10^-5;
11 // Acceleration due to gravity (in ft/sec^2):
12 g=32.2;
   Scilab code AP 34 data
1 //Length of Al tubing (in ft):
2 L=500;
3 //Volume flow rate of pump output (in gpm):
4 Q = 1500;
5 // Discharge pressure (in psig):
6 p1=65;
7 //Sprinkler pressure(in psig):
8 p2=30;
9 //Kinematic viscosity (in ft^2/sec):
10 v=1.21*10^-5;
11 // Density (in slug/ft^3):
12 p=1.94;
   Scilab code AP 35 data
1 // Height of standpipe (in ft):
21=80;
3 //Length of longest pipe(in ft):
4 L=600;
5 // Diameter of pipe (in inches):
6 D=4;
7 // Friction factor:
8 f = 0.031;
9 // Acceleration due to gravity in ft/sec^2):
10 g=32.2;
```

Scilab code AP 36 data

```
1 //Flow rate of crude oil(in bbl):
2 Q=1.6*10<sup>6</sup>;
3 //Inside diamete of pipe(i inches):
4 D=48;
5 //Maximum allowable pressure(in psi):
6 p2=1200;
7 //Minimum pressure required to keep gases dissolves (
      in psi):
8 p1=50;
9 //Specific gravity of crde oil:
10 \text{ SG=0.93};
11 // Viscosity at 140 F(in lbf-s/ft^2):
12 u=3.5*10^-4;
13 // Efficincy of pump:
14 Effp=0.85;
15 // Density (in slug/ft^3):
16 d=1.94;
17 // Viscosity (in lbf-sec):
18 u=3.5*10^-4;
19 // Friction factor:
20 f = 0.017;
   Scilab code AP 37 data
1 //Volme flow rate of water(in m<sup>3</sup>/sec):
2 Q = 0.0084;
3 //Length of horizontal pipe(in m):
4 L=100;
5 // Diameter of pipe (in m):
6 D=0.075;
7 // Density of water (in kg/m^3):
8 d=999;
9 // Friction factor:
10 f=0.017;
11 //Minor lossses coefficient:
12 K = 0.5;
13 // Viscosity (in kg/m-s):
14 u=10^-3;
```

```
15 // Acceleration due to gravity (in /sec^2):
16 \text{ g=9.8};
   Scilab code AP 38 data
1 //Flow rate through capilarry viscometer (in mm<sup>3</sup>/sec
      ):
2 Q=880;
3 //Tube length (in m):
4 L=1;
5 //Tube diameter (in mm):
6 D=0.5;
7 // Pressure drop (in kPa):
8 p=1000;
9 // Density of oil (in kg/m^3):
10 d=999;
   Scilab code AP 39 data
1 //temperature fo operation (in F):
2 T = 210;
3 //Diameter of te bearing (in inches):
4 D=3;
5 // Diametral clearance (in inches):
6 a=0.0025;
7 //Length of shaft (in inhes):
8 L=1.25;
9 //Speed of rotation of the shaft(in rpm):
10 N = 3600;
11 // Viscosity of the oil (in lbf-s/ft^2):
12 u=2.01*10^-4;
13 // Specific gravity of SAE 10W:
14 SG=0.92;
15 // Density of water (in slug/ft<sup>3</sup>)
16 p=1.94;
```

Scilab code AP 40 data

```
1 // Operation pressure of hydraulic system(in kPa):
2 p1 = 20000;
3 //Operation temperature of hydraulic system(in C):
4 T=55;
5 // Piston diameter (in mm):
6 D = 25;
7 // Viscosity of SAE 10W at 55C(in kg/(m-s):
8 u=0.018;
9 //Mean radial clearance of a cylinder (in mm):
10 a=0.005;
11 //Gauge pressure on lower pressure side of piston(in
       kPa):
12 p2=1000;
13 //Lenth of piston(in mm):
14 L=15;
15 // Denity of water (in kg/m^3):
16 \, dw = 1000;
   Scilab code AP 41 data
1 // Efficinc of pump:
2 Effp=0.8;
3 //Design specific speed(in rpm):
4 Nscu1=2000;
5 //Impeller diameter(in inches):
6 D1=8;
7 // Opertion sped at esign point flow condition (in rpm
      ):
8 \text{ N1} = 1170;
9 //Flow rate at design point flow condition (in gpm):
10 \quad Q1 = 300;
11 // Density of water (in slug/ft^3):
12 d1=1.94;
13 // Acceleration due to gravity (in ft^2/sec):
14 g=32.2;
15 //Working speed 2(in rpm):
16 \text{ N2} = 1750;
```

Scilab code AP 42 data

```
1 //Width of the prototype (in ft):
2 \text{ wp=8};
3 //Frontal area of the prototype (in ft^2):
4 Ap=84;
5 //Model Scale:
6 S=1/16;
7 // Density of air (in kg/m^3):
8 d=1.23;
9 //Air speed in wind tunnel(in m/sec):
10 V = [18 \ 21.8 \ 26 \ 30.1 \ 35 \ 38.5 \ 40.9 \ 44.1 \ 46.7];
11 //Drag force (in N):
12 Fd=[3.1 4.41 6.09 7.97 10.7 12.9 14.7 16.9 18.9];
13 //Kinematic viscosity (in m<sup>2</sup>/sec):
14 \quad v=1.46*10^-5;
15 // Density of air (in kg/m^3):
16 d=1.23;
17 //Speed of prototype(in km/hr):\
18 Vp = 100;
```

Scilab code AP 43 data

```
1 //Diameter of the prototype(in ft):
2 Dp=1;
3 //Speed of towing of prototype(in knots):
4 Vp=5;
5 //Diameter of model(in inches):
6 Dm=6;
7 //Drag for model at test condition(in lbf):
8 Fm=5.58;
9 //Density of seawater at 5 C for prototype(in slug/ft^3):
10 dp=1.99;
11 //Kinematic viscosity at 5 C for prototype(in ft^2/sec):
12 vp=1.69*10^-5;
13 //Density of air at STP for model(in slug/ft^3):
```

```
14 \text{ dm} = 0.00238;
15 //Kinematic viscosity of air at STP for model(in ft
      ^{2}/\sec ):
16 \text{ vm} = 1.57 * 10^{-4};
   Scilab code AP 44 data
1 //Depth to which water is filled (in m):
2 h=3;
3 //Length of pipe(in m):
4 L=6;
5 // Diameter of pipe (in mm):
6 D = 150;
7 // Acceleration due to gravity (in m/sec^2):
8 g=9.81;
   Scilab code AP 45 data
1 // Area of cross section of the nozzle(in in 2):
2 \quad A4 = 0.864;
3 // Capacity of heater (in kW):
4 Q = 10
5 // Acceleration due to gravity (in ft/sec^2):
6 g=32.2;
7 //Water level in reservoir above datum line(in ft):
8 z3=10;
9 // Density of water (In slug/ft<sup>3</sup>):
10 d=1.94;
   Scilab code AP 46 data
1 //Speed of plane(in km/hr):
2 V = 150;
3 //Speed at point B relative to the wing(in m/sec):
4 Vb = 60;
5 // Density of air (in kg/m^3):
6 da=1.23;
```

```
7 // Atmospheris pressure (in N/m^2):
8 pa=1.01*10<sup>5</sup>;
9 //At 1000m
10 //p/pSL:
11 P1=0.8870;
12 //d/dSL:
13 D1=0.9075;
   Scilab code AP 47 data
1 //Depth of water at the upstream (on feet):
2 Du = 1.5;
3 //Depth of water at the vena contracta downstream
      from the gate (in inches):
4 Dd = 2;
5 // Acceleration due to gravity (in ft/sec^2):
6 g=32.2;
   Scilab code AP 48 data
1 //Length of tube above surface (in m):
2 1 = 1;
3 //Depth of exit below water surface (in m):
4 z=7;
5 // Acceleration due to gravity (in m/sec^2):
6 g=9.81;
7 // Density of water (in kg/m^3):
8 d=999;
9 //Atmospheric pressure (in N/m^2):
10 p1=1.01*10<sup>5</sup>;
   Scilab code AP 49 data
1 //Area of nozzle at input(in m^2):
2 \text{ Ai=0.1};
3 //Area of nozzle at exit(in m^2):
4 Ae=0.02;
```

```
5 //Outlet velocity of flow(in m/sec):
6 V2=50;
7 // Density of air (in kg/m^3):
8 da=1.23;
   Scilab code AP 50 data
1 // Pressure diference (in mm of mecury):
2 p=30;
3 // Density of water (in kg/m<sup>3</sup>):
4 \, dw = 1000;
5 // Aceleration due to gravity (in m/sec^2):
6 g=9.81;
7 // Density of air (in kg/m^3):
8 da=1.23;
9 // Specific gravity of mercury:
10 \text{ SG} = 13.6;
   Scilab code AP 51 data
1 //Depth of the duct(in m):
2 d=0.3;
3 //Width of the duct(in m):
4 w = 0.1;
5 //Inner radius of the bend(in m):
6 r = 0.25;
7 // Pressure difference between the taps (in mm of Hg):
8 p=40;
9 // Density of water (in kg/m^3):
10 \text{ dw} = 999;
11 // Acceleration due to gravity (in m/sec^2):
12 g=9.8;
13 // Density of air (in kg/m^3):
14 da=1.23;
```

Scilab code AP 52 data

```
1 //Thickness of water film (in mm):
2 h = 1;
3 //Width of surface(in m):
4 b=1;
5 //Angle of inclination of surface:
6 \text{ theta=15};
7 // Density of water (in kg/m^3):
8 d=999;
9 // Acceleration du to gravity (in m/sec^2):
10 g=9.81;
11 // Viscosity (kg/m-s):
12 u=10^-3;
   Scilab code AP 53 data
1 // Value of A(in sec^-1):
2 A = 0.3;
   Scilab code AP 54 data
1 // Value of (in mm/sec):
2 U=4;
3 //Value of h(in mm):
4 h = 4;
5 //Tme at which to find position (in sec):
6 t=1.5;
   Scilab code AP 55 data
1 // Distance f piston from closed end of the cylinder
      at the give instant (in m):
2 L=0.15;
3 // Density of gas (in kg/m<sup>3</sup>):
4 d=18;
5 // Velocity of piston (in m/sec):
6 V = 12;
```

Scilab code AP 56 data

```
1 // Volume of tak(in m^3):
2 V = 0.1;
3 //Temperature of line and tank(in K):
4 T = 293;
5 //Initial tank gauge pressure(in N/m<sup>2</sup>):
6 p1=1*10^5;
7 //Absolute line pressure (in N/m^2):
8 p=2*10^6;
9 //Rate of rise of temperature after opening of the
      valve(in C/sec):
10 r = 0.05;
11 / Atmospheric pressure (in N/m^2):
12 patm=1.01*10<sup>5</sup>;
13 //Gas Constant(in N-m/(kg-K)):
14 R=287;
15 // Value of cv (in N-m/kg-K):
16 \text{ cv} = 717;
   Scilab code AP 57 data
1 // Pressure at entry (in psia):
2 p1=14.7;
3 //Temperature at entry (in F):
4 T1 = 70;
5 // Pressure at exit(in psia):
6 p2=50;
7 //Temprature a exit(in F):
8 T2 = 100;
9 //Cross sectional area of the pipe at exit(in ft^2):
10 A2=1;
11 //Mass flow rate(in lbf/sec):
12 m = 20;
13 //Power input to the compressor(in hp):
14 Ws = -600;
15 // Value of cp (in Btu/lbm-R):
16 \text{ cp=0.24};
17 // Value of gas constant (in ft-lbf/(lbm-R))
```

18 R=53.3;

Scilab code AP 58 data

```
1 //Inlet gauge pressure(in kPa):
2 p = 20;
3 //Volume flow rate of water through the sprinkler (in
       1/min):
4 Q=7.5;
5 //Speed of rotstion of sprinkler(in rpm):
6 \text{ w} = 30;
7 // Diameter of jet f sprinkle (in mm):
8 D=4;
9 //Radius of sprinkler(in mm):
10 R = 150;
11 //Supply pressure to sprinkler(in kPa):
12 p = 20;
13 //Angle at which jet is sprayed wrt horizontal:
14 alpha=30;
15 // Density of water (in kg/m^{\hat{}}):
16 d=999;
```

Scilab code AP 59 data

```
1 //Initial mass of th rocket(in kg):
2 M0=400;
3 //Rate of fuel consumption(in kg/sec):
4 me=5;
5 //Exhaust velocity(in m/sec):
6 Ve=3500;
7 //Acceleration due to gravity(in m/sec^2):
8 g=9.81;
9 //Time after which velocity is to be calculated(in sec):
10 t=10;
```

Scilab code AP 60 data

```
1 //Mass of vane and cart(in kg):
2 M = 75;
3 //Turning angle of vane:
4 theta=60;
  //Speed of water leaving nozzle horizontally (in m/
      sec):
6 V = 35;
7 //Exit area of nozzle(in m^):
8 \quad A = 0.003;
9 // Density of water (in kg/m^3):
10 d = 999;
   Scilab code AP 61 data
1 //Vane turning angle:
2 \text{ theta=60};
3 //Speed of vane(in m/sec):
4 U=10;
5 //Area of nozzle(in m2):
6 \quad A = 0.003;
7 //Flow velocity of water(in m/sec):
8 V = 30;
9 // Density of water (in kg/m^3):
10 d=999;
   Scilab code AP 62 data
1 //Nozzle inlet diameter(in inchess):
2 D1 = 3;
3 //Nozzle exit diameter(in inches):
4 D2=1;
5 // Desired volume flow rate (in ft 3/sec):
6 \quad Q = 0.7;
7 // Density of water (in slug/ft^3):
8 d=1.94;
```

Scilab code AP 63 data

```
1 // Velocity of conveyor belt(in ft/sec):
2 Vbelt=3;
3 // Velocity of sand alling onto belt(in ft/sec):
4 Vsand=5;
5 //Flow rate(in lbm/sec):
6 m = 500;
   Scilab code AP 64 data
1 //Pressure at inlet to the elbow (in N/m^2):
2 p1=2.21*10^5;
3 // Area of crosssection (in m<sup>2</sup>):
4 \quad A1 = 0.01;
5 // Velocity at secton 2(in m/sec):
6 V2 = 16;
7 // Area of cross section of section 2(in m^2):
8 \quad A2 = 0.0025;
9 //Atmospheric pressure(in kPa):
10 patm=1.012*10<sup>5</sup>;
   Scilab code AP 65 data
1 // Diameter of channel (in m):
2 D1=1.5;
3 // Velcity of flow in channel(in m/sec):
4 V1 = 0.2;
5 // Diameter at section 2(in m):
6 D2 = 0.0563;
7 // Velocity a section 2(in m/sec):
8 V2=5.33;
9 // Density of water (in kg/m^3):
10 d=999;
11 // Acceleration due to gravity (in m/sec2):
12 g=9.81;
```

Scilab code AP 66 data

```
1 // Height of the container (in ft):
2 1=2;
3 //Area of cross section (in ft^2):
4 A = 1;
5 //Weight of container (in lbf):
6 \text{ W=5};
7 //Water depth (in ft):
8 h=1.9;
9 //Area of opening 1(in ft<sup>2</sup>):
10 A1=0.1;
11 // Velocity at opening 1(in ft/sec):
12 V1 = -5;
13 //Area of opening 2(in ft ^2):
14 A2=0.1;
15 //Area of opening 1(in ft<sup>2</sup>):
16 \quad A3 = 0.1;
17 // Density of water (in slug/f<sup>3</sup>):
18 d2=1.94;
   Scilab code AP 67 data
1 // Velocity of water leaving the nozle(in m/sec):
2 V = 15;
3 / Area of nozzle(in m^2):
4 A = 0.01;
5 // Density of water (in kg/m^3):
6 d=999;
   Scilab code AP 68 data
1 //Volume of tank(in m<sup>3</sup>):
2 V = 0.05;
3 // Pressure of air (In kPa):
4 p = 800;
5 //Temperature of tank(in C):
6 T = 15;
7 // Velocity of leavig air (in m/sec):
8 v = 311;
```

```
9 // Density of air (in kg/m^3):
10 d=6.13;
11 // Area of valve exit (in mm^2):
12 A = 65;
   Scilab code AP 69 data
1 //Flow velocity ahead of the plate(in m/sec):
2 U=30;
3 //Boundary layer tckness at location d(in mm):
4 t=5;
5 // Density of fluid air (in k/m^3):
6 d=1.24;
7 // Plate wdth perpendicular to the plate(in m):
8 \quad w = 0.6;
   Scilab code AP 70 data
1 //Area of 1 (in ft<sup>2</sup>):
2 \quad A1 = 0.2;
3 //Area of 2 (in ft^2):
4 \quad A2 = 0.5;
5 //Area of 3 (in ft^2):
6 \quad A3 = 0.4;
7 // Area of 4 (in ft^2):
8 \quad A4 = 0.4;
9 //Density of water (in slug/ft<sup>3</sup>):
10 d=1.94;
11 //Mass flow rate out of section 3(in slug/sec):
12 \quad m3=3.88;
13 //Volme flow rate in section 4 (in ft^3/sec):
14 \quad Q4=1;
15 // Velocity at 1(in ft/sec):
16 V1 = 10;
```

Scilab code AP 71 data

```
1 //Width of gate(in m):
2 w = 5;
3 //Depth of water(in m):
4 D=4;
5 // Density of water (in kg/m^3);
6 d = 999;
7 // Accelration deto gravity (in m/sec^2):
8 g=9.81;
9 //Value of a (in m):
10 a=4;
11 // Point where force acts (in m):
12 \quad 1=5;
   Scilab code AP 72 data
1 //Pressure apllied on the door(in psfg):
2 p0 = 100;
3 //Length of door(in feet):
4 L=3;
5 //Breadth of the door(in feet):
6 b=2;
7 // Density of liquid (in lbf/ft^3):
8 d=100;
   Scilab code AP 73 data
1 //Length of gate(in m):
2 L=4;
3 //Width of gate(in m):
4 w = 5;
5 //Depth of gate under water(in m):
6 D=2;
7 // Density of water (in kg/m<sup>3</sup>:
8 d=999;
9 // Acceleration due to gravity (in m/sec^2):
10 g=9.81;
11 //Angle of gate with horizontal:
12 \text{ theta=30};
```

Scilab code AP 74 data

```
1 //Elevation of Denver(in ft):
2 z1 = 5280;
3 //Pressure at Denver(in mm of Hg):
4 p1=24.8;
5 //Temperature at Denver(in F):
6 T1 = 80;
7 // Elevation at Vail Pass(in ft):
8 z2=10600;
9 //Temperature at Vsil Pass(in F):
10 T2 = 62;
11 //Value of R in ft-lbf/lbm-R):
12 R=53.3;
13 // Acceleration due togravity (in ft/sec^2):
14 g=32.2;
15 // Value of adiabatic constant:
16 \text{ k=1.4};
```

Scilab code AP 75 data

```
//Acceleration due to gravity(in ft/sec^2):
g=32.2;
//Specific gravity of mercury:
SGm=13.6;
//Specific gravity of oil:
SGo=0.88;
//Specific gravity of water:
SGw=1;
//Density of water(in slug/ft^3):
d=1.94;
//Heights of liquid in various tubes(in inches):
d1=10;
d2=3;
d3=4;
d4=5;
```

```
16 	ext{ d5=8};
   Scilab code AP 76 data
1 //Surface tension of water(in mN/m):
2 STw = 72.8 * 10^{-3};
3 //Surface Tension of mercury (in mN/m):
4 STm=375*10^-3;
5 //Contact angle for water:
6 \text{ thetaw=0};
7 //COntact angle for mercury:
8 \text{ thetam=140};
9 // Density of water (in kg/m^3):
10 dw = 1;
11 // Density of mercury (in kg/m^3):
12 \, dm = 13.6;
13 // Acceleration de to gravity (in m/sec):
14 g=9.81;
   Scilab code AP 77 data
1 //Liquid Viscosity (in cp):
2 u=0.65;
3 //Specific gravity:
4 SG=0.88;
```

Scilab code AP 78 data

6 d=1.94;

8 U=0.3;

10 D=0.3;

```
1 //Mass of ball(in kg):
2 m=0.2;
3 //Height fom which ball is dropped(in m):
```

7 // Velocity with which plate is moved(in m/sec):

5 //Density of water(in slug/ft^3):

9 // Distance between the plates (in mm):

```
4 y0 = 500;
5 //Value of k:
6 k=2*10^-4;
7 // Accleration due to gravity (in m/sec^2):
8 g=9.81;
   Scilab code AP 79 data
1 //Mass of oxygen present(in kg):
2 m = 0.95;
3 //Initial temperatur(in K):
4 T1 = 300;
5 // Final temperature of oxygen(in K):
6 T2 = 900;
7 // Pressure of oxygen (in kPa):
8 p=150;
9 // Specific heat at constant pressure (in J/kg-K):
10 \text{ cp} = 909.4;
```