Scilab Textbook Companion for Thermodynamics by K. M. Gupta¹

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Book Description

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Scilab numbering policy used in this document and the relation to the above book.

Exa Example (Solved example)

Eqn Equation (Particular equation of the above book)

AP Appendix to Example(Scilab Code that is an Appednix to a particular Example of the above book)

For example, Exa 3.51 means solved example 3.51 of this book. Sec 2.3 means a scilab code whose theory is explained in Section 2.3 of the book.

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Chapter 1

Fundamentals Concepts and Definitions of Thermodynamics

Scilab code Exa 1.2 Absolute pressure

```
1 // Exa 1.2
2 clc;
3 clear;
4 close;
5 // Given data
6 Pvacc = 700; // mm of hg
7 Patm = 760; // mm of hg
8 Pabs = Patm - Pvacc; // mm of hg
9 disp(Pabs/760, "Absolute pressure in in kg/cm^2 is :"
        ); // as 1kg/cm^2= 760 mm of Hg
10 disp(Pabs*1.01325/760, "Absolute pressure in bar is :
        "); // as 1.01325 bar = 760 mm of Hg
11 disp(Pabs*1.01325/760*10^2, "Absolute pressure in in kPa"); // as 1 bar = 10^2 kPa
```

Scilab code Exa 1.3 Tank pressure

```
1 / Exa 1.3
2 clc;
3 clear;
4 close;
5 // Given data
6 Patm = 101; // \text{kpa}
7 Rho = 13.6 * 10^3; // in kg per m^3
8 h = 250; // in cm
9 h = h*10^-2; // in m
10 g = 9.806;
11 p = Rho * g * h; // in N/m^2
12 p = p*10^-3; // in kPa
13 // Total pressure in tank
14 p = p + Patm; // in kpa
15 p = p*10^-3; // in Mpa
16 disp(p, "Total pressure in tank in Mpa");
```

Scilab code Exa 1.4 Work done by the piston

```
1 // Exa 1.4
2 clc;
3 clear;
4 close;
5 // Given data
6 m = 1.5; // in kg
7 \text{ pi} = 0.1; // \text{ in MPa}
8 pi= pi*10^6; // in Pa
9 pf = 0.7; // in MPa
10 pf= pf*10^6; // in Pa
11 rho_i = 1.16; // kg per m^3
12 vi = m/rho_i; // in m^3
13 WorkDone = pi*vi*log(pi/pf); // in J
14 disp(WorkDone*10^-3,"Work done in kJ is: ")
15 if WorkDone < 0 then
16 disp ("The -ve sign indicates work is done on the
```

```
system, hence");
17 disp((WorkDone*10^-3),"The work done by the piston
      in kJ is : ")
18 end
```

Scilab code Exa 1.5 Work done

```
1 // Exav1.5
2 clc;
3 clear;
4 close;
5 // Given data
6 p = 1.0; // in Mpa
7 p = p*10^6; // in N per m^2
8 del_v = 1.5; //m^3 per min
9 del_v = del_v*60; // m^3 per h
10 W = p * del_v; // W stands for work done in J
11 W = W*10^-6; // in MJ
12 disp(W,"Work done by the pump upon the water in an hour in MJ is:");
```

Scilab code Exa 1.6 Height from which the mass should fall

```
1 // Exa 1.6
2 clc;
3 clear;
4 close;
5 // Given data
6 // W = 2*g*h
7 // due to stirring of water
8 g = 9.81;
9 J = 4.1868*10^3;
10 m = (0.2+10*10^-3)*10^3; // in gm
```

Scilab code Exa 1.7 Power of feed pump

```
1 // Exa 1.7
2 clc;
3 clear;
4 close;
5 // Given data
6 // mass of 1 litr of water is 1 kg. so
7 \text{ m} = 5000; // \text{ in kg}
8 h = 10-1; // in m
9 g = 9.81; //
10 PE = m * g * h; // in N m
11 PE = PE*10^-3; // in kj
12 Eta = 0.85;
13 // Eta = energy output/energy input
14 E_input = PE/Eta; // in Kj
15 E_input = E_input *10^3; // in J
16 t = 45; // time in min
17 t = t*60; // in sec
18 P = E_input/t; // in J/s
19 P = P*10^-3; // in kW
20 disp(P,"Power required for the feed pump in kW is:"
      );
```

Scilab code Exa 1.11 Power of the engine

```
1 // Exa 1.11
2 clc;
3 clear;
4 close;
5 // Given data
6 V = 50; // km per hr
7 V = V * (1000/3600); // in m per sec
8 F = 900; // in N
9 P = F * V; // in watt
10 P = P *10^-3; // in kW
11 disp(P, "Power of the engine of a car in kW is : ");
12 H = P * 60; // in kJ
13 disp(H, "Heat equivalent of work per minute in kJ is");
```

Scilab code Exa 1.12 Power required

```
1 // Exa 1.12
2 clc;
3 clear;
4 close;
5 // Given data
6 E_air = 200-100; // in kJ/kg
7 E_lost = 40; // in kJ/kg
8 E_total = E_air + E_lost; // in kJ per kg
9 M = 0.5; // mass flow rate in kg per s
10 P = M * E_total; // in kJ/s
11 disp(P, "Power required for an air mass flowin kJ/s is :");
```

Scilab code Exa 1.13 Specific heat

```
1 // Exa 1.13
2 clc;
3 clear;
4 close;
5 // Given data
6 \text{ m_b} = 1; // \text{ in kg}
7 \text{ t_ib} = 80; //in degree c}
8 \text{ m_w} = 10; // \text{ in kg}
9 t_{iw} = 25; // in degree c
10 del_t = 5; // in degree c
11 S_w = 4.18; // in kJ/kg
12 t_{equ} = (t_{iw} + del_t); // in degree c
13 // Heat loss by metal = Heat gained by water
14 \, S_b = m_w * S_w * (t_equ - t_iw)/(m_b * (t_ib - t_iw))
      t_{equ}); // in kJ/kg-K
  disp(S_b, "Specific heat of metal block in kJ/kg-K is
      ");
```

Scilab code Exa 1.15 Convert reading in kPa

```
1 // Exa 1.15
2 clc;
3 clear;
4 close;
5 // Given data
6 P_gauge = 90; // in cm of hg
7 P_atm = 760; // in mm of hg
8 P_atm = 76; // in cm of hg
9 P_abs = P_gauge + P_atm; // in cm of hg
10 P_abs = P_abs * (101.32/76); // in kPa
11 disp(P_abs, "Reading of pressure in kPa");
12 // Part (b)
13 P_vacuum = 40; // in cm of hg
14 P_abs = P_atm - P_vacuum; // in cm of hg
15 P_abs = P_abs * (101.32/76); // in kpa
```

```
16 disp(P_abs, "Reading of pressure to kpa");
17 // Part (c)
18 Rho = 1000; // in kg per m^3
19 g = 9.81; //
20 h = 1.2; // in m
21 P_gauge = Rho * g * h; // in N m^2
22 P_gauge= P_gauge*10^-3; // in kPa
23 P_atm = 101.32; // in kPa
24 P_abs = P_gauge + P_atm; // in kpa
25 disp(P_abs, "Reading of pressure in kPa");
```

Scilab code Exa 1.16 Depth of atmosphere

```
1 // Exa 1.16
2 clc;
3 clear;
4 close;
5 // Given data
6 g=9.81; // in m/s^2
7 P=1.0332*10^5; // in kN/m^2
8 v='(2.3*10^4/p)^1/1.4'; // given expression
9 H= 1/g*(2.3*10^4)^(1/1.4)*integrate('(1/p)^(1/1.4)', 'p',0,P); // in m
10 disp(H*10^-3,"The value of H in km is:")
11
12 // Note: There is the calculation error in the book in this question, so the answer in the book is wrong.
```

Chapter 2

Gas Laws Ideal and Real Gases

Scilab code Exa 2.1 Air pressure in the tyre

```
1 // Exa 2.1
2 clc;
3 clear;
4 close;
5 // Given data
6 p1= 2; // in bar
7 v1= 30; // in litre
8 T1= 27+273; // in K
9 T2= -3+273; // in K
10 v2= v1; // in litre
11 // Gas law p1*v1/T1= p2*v2/T2
12 p2= p1*v1*T2/(T1*v2); // in bar
13 disp(p2,"The air pressure in the tyre in bar is:")
```

Scilab code Exa 2.2 Molar volume of the gas mixture

```
1 // Exa 2.2
2 clc;
```

```
3 clear;
4 close;
5 // Given data
6 p = 12; // in bar
7 p=p*10^5; // in N/m^2
8 v = 25; // in m^3
9 T= 30+273; // in K
10 // Part (a) Mass of each gas
11 // Formula p*v=m*R*T
12 R_U= 8314; // in J/kg-mole K
13 M_N2 = 28.016; // in mole
14 M_O2= 32; // in mole
15 M_CO2= 44; // in mole
16 R_N2= R_U/M_N2; // in J/kg K
17 R_02= R_U/M_02; // in J/kg K
18 R_CO2= R_U/M_CO2; // in J/kg K
19 m_of_N2 = p*v/(R_N2*T); // in kg
20 \text{ m\_of\_02= } p*v/(R_02*T); // in kg
21 m_of_CO2 = p*v/(R_CO2*T); // in kg
22 disp(m_of_N2, The mass of Nitrogen gas stored in the
       vessel in kg is: ")
23 disp(m_of_02,"The mass of Oxygen gas stored in the
      vessel in kg is: ")
24 disp(round(m_of_CO2), "The mass of Carbon dioxide gas
       stored in the vessel in kg is: ")
25
26 // Part (b) Molar Volume
27 // Formula v_molar= M*R*T/p= R_U*T/p
28 v_molar= R_U*T/p; // in m^3
29 disp(v_molar, "Molar volume of the gas mixture in m^3
       is : ")
30
31 // Part (c) Average density
32 // rho_avg= total mass/total volume
33 rho_avg= (m_of_N2+m_of_02+m_of_C02)/v; // in kg/m^3
34 disp(rho_avg," Average density of the gas mixture in
     kg/m^3 is : ")
```

Scilab code Exa 2.3 Value of Cp Cv and R

```
1 // Exa 2.3
2 clc;
3 clear;
4 close;
5 // Given data
6 Qp= 1230; // kJ/kg
7 Qv = 795; // kJ/kg
8 \text{ t1= } 16; // \text{ in}
                  \mathbf{C}
9 t2 = 96; // in
                   \mathbf{C}
10 R_U = 8.314;
11 delta_T= t2-t1;// in
12 Cp= Qp/delta_T;// in kJ/kg
                                   C
13 disp(Cp, "The value of Cp in kJ/kg C")
14 Cv = Qv/delta_T; // in kJ/kg
15 disp(Cv, "The value of Cv in kJ/kg C")
16 R= Cp-Cv; // in kJ/kg
                            \mathbf{C}
17 disp(R, "The value of R in kJ/kg C")
18 molecular_weight= R_U/R;
19 disp(molecular_weight, "Molecular weight of the gas
      is : ")
```

Scilab code Exa 2.4 Change in internal energy

```
1 // Exa 2.4
2 clc;
3 clear;
4 close;
5 // Given data
6 a= 0.85;
7 b= 0.00004;
```

```
8 c= 5*10^-5;
9 T1= 300; // in K
10 T2= 2300; // in K
11 gama= 1.5; // the ratio of specific heats
12 m=1; // in kg
13 delta_H= m*integrate('a+b*T+c*T^2', 'T',T1,T2); // in kJ
14 disp(delta_H*10^-3, "Change in enthalpy in MJ is:")
15 // Formula delta_U= integration of m*Cv = integration of m*Cp/gama= delta_H/gama
16 delta_U= delta_H/gama; // in kJ
17 disp(delta_U*10^-3, "The change in internal energy in MJ is:")
```

Scilab code Exa 2.5 Pressure exerted by unit mass of the gas

```
1 // Exa 2.5
2 clc;
3 clear;
4 close;
5 // Given data
6 v= 0.9/3; // in m^3/kg
7 v= 2*v; // in m^3/kg mole (as M_hydrogen = 2)
8 T=120+273; // in K
9 R=8314; // in J/kg mole K
10 a=2.51*10^4; // in Nm^4/(kg mole)^2
11 b = 0.0262;
12 // Part (a)
13 p= R*T/v; // in N/m^2
14 p= p*10^-5; // in bar
15 disp(p," Using perfect gas law the pressure for unit
     mass of hydrogen in bar is: ")
16
17 // Part (b)
18 p = R*T/(v-b)-a/v^2; // N/m^2
```

```
19 p= p*10^-5; // in bar
20 disp(p, "Using Van der waals equation, the pressure
    in bar is : ")
```

Scilab code Exa 2.6 Density of gas

```
1 // Exa 2.6
2 clc;
3 clear;
4 close;
5 // Given data
6 p1= 0.98; // in bar
7 p2= 0.6; // in bar
8 v1= 0.45; // in m^3/kg
9 // Applying Boyle's law
10 v2= p1*v1/p2; // in m^3/kg
11 rho2= 1/v2; // in kg/m^3
12 disp(rho2,"The density of the gas under the changed condition in kg/m^3 is:")
```

Scilab code Exa 2.7 Payload

```
1 // Exa 2.7
2 clc;
3 clear;
4 close;
5 // Given data
6 r=5; // in cm
7 R_U= 8314
8 T= 27+273; // in K
9 V= 4/3*%pi*r^3; // volume of balloon in cm^3
10 // atmPressure= 75 cm off mercury = 75/76*1.01325
11 atmPressure= round (75/76*1.01325); // in bar
```

Scilab code Exa 2.12 Pressure of the gas

```
1 // Exa 2.12
2 clc;
3 clear;
4 close;
5 // Given data
6 AvogadroNo= 6.023*10^23;
7 n= 5/AvogadroNo; // number of moles
8 v=10^-6; // in m^3
9 T= -270+273; // in K
10 R= 0.287;
11 p= n*R*T/v; // in kPa
12 p= p*10^18; // in aPa
13 disp("The pressure in the space is "+string(p)+" aPa
");
```

Scilab code Exa 2.13 Change in enthalpy

Scilab code Exa 2.14 Molecular weight

```
1 // Exa 2.14
2 clc;
3 clear;
4 close;
5 // Given data
6 \text{ m=12;} // \text{ in kg mol}
7 v = 723.7; // in m^3
8 T = 140; // in C
9 T=T+273; // in K
10 rho= 0.644; // in kg/m<sup>3</sup>
11 Ro= 8314; // in J/kg-mole~K
12 // \text{ rho} = \text{m/v}, where m in Kg , so \text{rho} = \text{m*M/v}
13 M = rho * v/m;
14 m = m*M; // in kg
15 disp(M, "Molecular weight is: ")
16
17 // Part (b)
18 R= Ro/M; // in J/kg K
19 disp(R*10^-3, "Gas constant in kJ/kg K")
```

```
20
21 // Part(c)
22 p= m*R*T/v; // in N/m^2
23 p=p*10^-5; // in bar
24 disp(p, "The pressure of the gas in bar is:")
```

Scilab code Exa 2.15 Load that can be lifted with the air of aerostat

```
1 // Exa 2.15
2 clc;
3 clear;
4 close;
5 // Given data
6 p = 0.98; // in bar
7 p= p*10^5; // in N/m^2
8 \text{ v=1000; // in m}^3
9 T = 27 + 273; // in K
10 \text{ g= } 9.8;
11 M=2;
12 Ro = 8314; // in J/kg-mole K
13 R=Ro/M; // in kg K
14 m= p*v/(R*T); // in kg
15 W= m*g; // in N
16 disp(W,"The load that can be lifted with the air of
      aerostat in N is : ")
```

Scilab code Exa 2.16 Change in enthalpy

```
1 // Exa 2.16
2 clc;
3 clear;
4 close;
5 // Given data
```

```
6 T1= 500; // in K
7 T2= 2000; // in K
8 m=1; // in kg
9 Cp= '11.515-172/sqrt(T)-1530/T'; // in kcal/kg mole K
10 delta_H=m* integrate('11.515-172/sqrt(T)-1530/T','T', T1,T2); // in kcal/kg mole
11 disp(delta_H,"Change in enthalpy in kcal/kg mole is: ")
```

Scilab code Exa 2.17 Value of Cv and Cp

```
1 // Exa 2.17
2 clc;
3 clear;
4 close;
5 // Given data
6 u='196+0.718*t';
7 pv= '0.278*(t+273)';
8 duBydt= 0.718;
9 Cv= duBydt;// in kJ/kg-K
10 h= u+pv;
11 h='273.351+1.005*t';
12 dhBydt= 1.005;// in kJ/kg-K
13 Cp= dhBydt;// in kJ/kg-K
14 disp(Cv, The value of Cv in kJ/kg-K is: ")
15 disp(Cp, The value of Cp in kJ/kg-K is: ")
```

Chapter 3

Zeroth Law of Thermodynamics and Temperature Scales

Scilab code Exa 3.1 Reading

```
1 // Exa 3.1
2 clc;
3 clear;
4 close;
5 // Given data
6 t_c = 303-273; // in C
7 t_f = 9/5* t_c+32; // in F
8 disp(t_f, "When the temperature is 303 K then the thermometer reading in F is:");
9 T_R = 460 + t_f; // R
10 disp(T_R, "The absolute value of the temperature in Rankine scale in R is:");
```

Scilab code Exa 3.2 Temperature of fluid

```
1 // Exa 3.2
2 clc;
3 clear;
4 close;
5 // Given data
6 T_K = '273.15 + t_C';
7 \text{ T_R} = 459.67 + \text{t_F};
8 // t_C = t_F \text{ or } T_K - T_R = -186.52
                                             (i)
9 // T_R/T_K = 1.68
                                                             (ii
10 // From eq (i) and (ii)
11 T_K = -186.52/(1-1.68); // temp. in kelvin in K
12 T_R = 1.68*T_K; // in temp. in rankine in
13 t_C = T_K - 273.15; // in
14 t_F = T_R - 459.67; // in
                              \mathbf{F}
15 disp(T_K, "Temperature in kelvin is: ")
16 disp(T_R, "Temperature in
                                  R is ")
17 disp(t_C, "Temperature in
                                  \mathbf{C}
                                    is ")
18 disp(t_F, "Temperature in
                                  F
                                    is ")
```

Scilab code Exa 3.9 Temperature

```
1 // Exa 3.9
2 clc;
3 clear;
4 close;
5 // Given data
6 p0 = 1.86;
7 p100 = 6.81;
8 T1=32;
9 T2 = 212;
10 // Relation of T in terms of p for ice point
                                                          T1
     = a * log(p0) + b
                               (i)
11 // Relation of T in terms of p for steam point
      a * log (p100) + b
                       ( i i )
```

```
12 // From eq(i) and (ii)
13 a= (T2-T1)/log(p100/p0);
14 b= T1-a*log(p0);
15 // The temp at
16 p=2.5;
17 T= a*log(p)+b;// in unit
18 disp(T,"The temperature at p=2.5 in unit is:")
```

Scilab code Exa 3.10 Reading of thermometer

```
1 // Exa 3.10
2 clc;
3 clear;
4 close;
5 // Given data
6 Tp= 'a+b*Tq+lamda*Tq^2';// relation between Tp and
     Tq
7 Tp0=0; //in C (at ice point)
8 Tq0=0; //in C (at ice point)
9 // Putting these values in relation, we get
10 \ a=0;
11 Tp100=100; //in C ( at steam point)
12 Tq100=100; //in C ( at steam point)
                                              (i)
13 // \text{Tp}100 = b*Tq100 + lamda*Tq100^2
14 Tp=45; // in C (in oil path)
15 Tq=43; // in C (in oil path)
16 // Tp = b*Tq + lamda*Tq^2
                                                       (ii)
17 b= (Tp100-Tp*Tq100^2/Tq^2)/(Tq100-Tq100^2/Tq);//
     From eq (i) and (ii)
18 lamda = (Tp-b*Tq)/Tq^2;
19 Tp = 20;
20 / \frac{1}{\text{amda}} = Tq^2 + b = Tq - Tp = 0
21 P= [lamda b -Tp];
22 Tq= roots(P); // in C
23 disp(Tq,"When P reads 20 C, then the readings of Q
```

```
in C are")
24 disp(Tq(2),"The realistic value of Tq in C is: ")
```

Chapter 4

First Law of Thermodynamics

Scilab code Exa 4.1 Work done

```
1 // Exa 4.1
2 clc;
3 clear;
4 close;
5 // Given data
6 p = 1.0; // in MPa
7 p = p * 10^6; // in N per m^2
8 del_v = 1.5; // in m^3 per min
9 del_v = del_v * 60; // in m^3 per h
10 W = p * del_v; // in J
11 W = W * 10^-6; // in MJ
12 disp(W,"Work done by the pump upon the water in MJ")
;
```

Scilab code Exa 4.2 Height from which the mass should fall

```
1 // Exa 4.2
2 clc;
```

```
3 clear;
4 close;
5 // Given data
6 // w = 2*g*h
7 g = 9.81;
8 m = (0.2+10/1000)*10^3; // in gm
9 s = 1; // in cal/gm C
10 del_T = 2; // in C
11 H = m * s * del_T; // in cal
12 H = H * 10^-3; // kcal
13 J = 4.1868 * 1000;
14 // W= 2*g*h= J*H
15 h = J*H/(2 * g); // in m
16 disp(h, "Height from which the mass should fall in meter is:");
```

Scilab code Exa 4.3 Magnitude and direction of third heat transfer

```
1 // Exa 4.3
2 clc;
3 clear;
4 close;
5 // Given data
6 \text{ W1} = -25; // \text{ in kJ}
7 \text{ W2} = 45; // \text{ in kJ}
8 \ Q1 = 65; // in kJ
9 \ Q2 = -40; // in kJ
10 // del_U = Q - W and but for a cycle del_U = 0, So
11 // Q = W
12 // Q1 + Q2 + Q3 = W1 + W2
13 Q3 = W1 + W2 - Q1 - Q2; // in kJ
14 disp(Q3, "Third Heat transfer in kJ is");
15 disp("That is Third Heat transfer is of "+string(abs
      (Q3))+" kJ from the fluid");
```

Scilab code Exa 4.5 External work done

```
1 // Exa 4.5
2 clc;
3 clear;
4 close;
5 // Given data
6 \text{ m} = 1.5; // \text{ in kg}
7 \text{ T1} = 90; // \text{ in } C
8 T1 = T1 + 273; //in K
9 T2 = 225; // in C
10 \text{ T2} = \text{T2} + 273; // \text{ in } \text{K}
11 C_p = 0.24;
12 C_v = 0.17;
13 Q = (m * C_p * (T2-T1)); // in kcal
14 \text{ del}_U = (m * C_v * (T2-T1)); // in kcal
15 W = Q - del_U; // in kcal
16 disp(W,"The external work done in kcal is");
```

Scilab code Exa 4.7 Mass of the gas

```
1 //Exa 4.7
2 clc;
3 clear;
4 close;
5 // Given data
6 v1 = 0.5; // in m^3
7 v2 = 0.125; // in m^3
8 p1 = 1.5; // in bar
9 p1 = p1 * 10^5; // in N per m^2
10 p2 = 9; //in bar
11 p2 = p2 * 10^5; // in N per m^2
```

```
12 T1 = 100; // in C
13 T1 = T1 + 273; // in K
14 R = 8.31;
15 // Formula p1*v1=n*R*T1
16 n= p1*v1/(R*T1); // in mole
17 disp(n, "Mass of gas in mole is :");
18 // Part (b)
19 // Formula p1*v1/T1 = p2*v2/T2
20 \text{ T2} = (p2 * v2 * T1)/(p1 * v1); // in K
21 disp(T2-273, "Temperature at the end of compression
      in C is :");
22 // Part (c)
23 // Formula p1*v1^n = p2*v2^n
24 n1 = log(p2/p1)/log(v1/v2)
25 disp(n1," Value of index n of compression is :");
26 // Part (d)
27 F = 3;
28 C_v = 1/2*R*F;
29 \text{ del}_U = (n * C_v * (T2-T1)); // in J
30 disp(del_U*10^-3, "Increase in internal energy of gas
       in kJ is : ");
31 // Part (e)
32 \text{ Gamma} = 1.67;
33 Q_{12} = n*(Gamma-n1)/(1-n1)*R*(T2-T1)/(Gamma-1); // in
34 Q_{12} = Q_{12} * 10^{-3}; // in kJ
35 disp(Q_12,"Heat interaction in kJ is:");
36 if Q_12<0 then
       disp("The -ve sign indicates heat rejection
37
          during the process")
38 end
39
40 // Note: There is some difference between the answer
       of book and coding. Both the answer is right
      but accurate answer is of coding.
41 //
                Because in the book, the taken values
      are appox. and in the coding the values are
      accurate
```

Scilab code Exa 4.8 Law of the process

```
1 / Exa 4.8
2 clc;
3 clear;
4 close;
5 // Given data
6 \text{ p1} = 0.01; // \text{ in } \text{N/mm}^2
7 p1 = p1 * 10^3; // in kN/m^2
8 p2 = 50; // in kN/m^2
9 \text{ v1} = 5; // \text{ in } \text{m}^3
10 v2 = 1.5; // in m<sup>3</sup>
11 \text{ Gamma} = 1.4;
12 // Formula p1*v1^n = p2*v2^n
13 n= log(p2/p1)/log(v1/v2);
14 disp(n, "Part (a)
                       The value of n is: ")
15 disp("The process followed during air compression is
       POLYTROPIC");
16 // Part (b)
17 disp("Part (b)
                   The law of the process is p*v^"+
      string(n)+" = constant");
  // Part (c)
18
19 W= (p1*v1-p2*v2)/(n-1); // in kNm or (kJ)
20 disp(W, "Part (c)
                       Work done during the process in
      kJ is : ");
21 disp("The -ve sign indicates that the work has been
      done on the system")
22 // Part (d)
23 Q = ((Gamma - n)/(Gamma - 1) * W); // in kJ
24 disp(Q, "Part (d)
                         Heat transfer during the process
       in kJ is :");
25 disp ("The -ve sign indicates that the heat is
      rejected from the system")
```

Scilab code Exa 4.9 Change in internal energy

```
1 // Exa 4.9
2 \text{ clc};
3 clear;
4 close;
5 // Given data
6 // Relation of specific internal energy of the gas
7 // U = 1.5 * p * v - 85 kJ/kg
8 p1 = 1000; // in kpa
9 p2 = 200; // in pa
10 v1 = 0.20; // in m<sup>3</sup>
11 v2 = 1.20; // in m<sup>3</sup>
12 m = 1.5; // in kg
13 U1= 1.5*p1*v1-85;//
                         kJ/kg
14 U2= 1.5*p2*v2-85; //
                          kJ/kg
15 delU= U2-U1; // in kJ
16 disp(delU, "Change in internal energy in kJ is");
17 // p1 = a + b * v1
                            ( i )
18 // p2 = a+b*v2
                            ( i i )
19 // From eq(i) and (ii)
20 b= (p1-p2)/(v1-v2); // in kN/m^2
21 a= p1-b*v1; // in kN/m^2
22 disp(a, "The value of a in kN/m^2 is ")
23 disp(b, "The value of b in kN/m^2 is ")
24 // Part (c)
25 // Work done = integration of p w.r.t. v and p = a+b
      *v1
26 W= integrate('a+b*v','v',v1,v2);// in kJ
27 disp(W,"Work done in kJ is :")
28 // Part (d)
29 Q= delU+W; // in kJ
30 disp(Q,"The net heat transfer in kJ is: ")
```

Scilab code Exa 4.10 Maximum internal energy

```
1 // Exa 4.10
2 clc;
3 clear;
4 close;
5 // Given data
6 a= 1160; // in kN/m^2
7 b= -800; // in kN/m^2
8 v= -a/(2*b)
9 Umax= 1.5*(a*v+b*v^2)-85; // in kJ/kg
10 // For 1.5 kg mass of gas it is
11 Umax= Umax*1.5; // in kJ/kg
12 disp(Umax, "The maximum internal energy of the gas in kJ/kg is:")
```

Scilab code Exa 4.11 Exit velocity of air

```
1  // Exa 4.11
2  clc;
3  clear;
4  close;
5  // Given data
6  T1 = 127; // in   C
7  T1 = T1 + 273; // in   K
8  R = 287;
9  V1 = 300; // in   m/s
10  p1 = 2; // in   MPa
11  p2 = 0.5; // in   MPa
12  p1 = p1 * 10^6; // in   Pa
13  p2 = p2 * 10^6; // in   Pa
14  C_P = 1.005*10^3; // in   J/ kg-K
```

```
15 \text{ Gamma} = 1.4;
16 V2 = sqrt(2 * C_P *T1 *{1-(p2/p1)^((Gamma-1)/Gamma)}
       + V1^2; // in m/s
17 disp(V2, "The exit velocity of air in m/s is: ");
18 m = 600; // in kg/hr
19 m = m / 3600; // in kg/sec
20 v1 = (R * T1)/p1; // in m^3 per kg
21 / m = (A1*V1)/v1 = (A2*V2)/v2
22 A1 = (m * v1)/V1; // in m^2
23 A1 = A1 * 10^6; // in mm^2
24 disp(A1," Inlet area of the nozzle in square
      milimeter is : ");
25 T2 = T1*(p2/p1)^((Gamma-1)/Gamma); // in K
26 \text{ v2} = (R * T2)/(p2); // \text{ in } m^3/\text{kg}
27 \text{ A2} = (m * v2)/V2; // in m^2
28 \text{ A2} = \text{A2} * 10^6; // \text{ in mm}^2
29 disp(A2, Exit area of nozzel in square milimeter is
      : ");
```

Scilab code Exa 4.17 Net heat transfer

```
1 // Exa 4.17
2 clc;
3 clear;
4 close;
5 // Given data
6 W = -1; // in kWh
7 W = W * 10^3 * 3600; // in J
8 del_U = -5000; // in kj
9 del_U = del_U * 10^3; // in J
10 Q = del_U + W; // in J
11 Q = Q * 10^-6; // in MJ
12 disp(Q,"Net heat transfer for the system in MJ is:
");
```

Scilab code Exa 4.20 Heat flows into the system

```
1 / \text{Exa} \ 4.20
2 clc;
3 clear;
4 close;
5 // Given data
6 \quad Q_acb = 84; //in \quad kJ
7 \text{ W_acb} = 32; // in kJ
8 //Formula Q_{acb} = del_{U}+W_{acb} where del_{U} = U_{b}
      U_a;
9 \text{ del_U} = Q_acb - W_acb; // in kJ
10 // Part (a) Path a b d
11 W_abd = 10.5; // in kJ
12 Q_abd = del_U + W_abd; // in kJ
13 disp(Q_abd," Heat flows into the system along the
      path a b d in kJ is : ");
14 // Part (b) curved path b a
15 W_ba = -(21); // in kJ
16 Q_ba = -(del_U) + W_ba; // in kJ
17 disp(abs(Q_ba),"Heat liberated by the system in kJ
      is : ");
18 // Part (c) process a b and d b
19 W_ad = 10.5; // in kJ
20 \text{ del}_U1 = 42; // \text{ in } kJ
21 Q_ad = del_U1 + W_ad; // in kJ
22 disp(Q_ad,"Heat absorbed in processes a d in kJ is
      : ");
23 \text{ W_db} = -(42); // \text{ in kJ}
24 \text{ del}_U2 = 52; // \text{ in } kJ
25 Q_bd = del_U2 + W_db; // in kJ
26 disp(Q_bd,"Heat absorbed in processes b d in kJ is:
       ");
27 \text{ W\_db} = 0;
```

Scilab code Exa 4.21 Net work

```
1 / Exa 4.21
2 clc;
3 clear;
4 close;
5 // Given data
6 \text{ v1} = 5; // \text{ in } \text{m}^3
7 p1 = 2; // in bar
8 p2 = 6; // in bar
9 p3 = 2; // in bar
10 p1 = p1 * 10^5; // in N/m^2
11 p2 = p2 * 10^5; // in N/m^2
12 p3 = p3 * 10^5; // in N/m^2
13 n = 1.3;
14 v2 = v1 * ((p1/p2)^(1/1.3)); // in m^3
15 W1_2 = ((p2 * v2) - (p1 * v1))/(1-n); // in J
16 \text{ Gamma} = 1.4;
17 v3 = v2 * ((p2/p3)^(1/Gamma)); // in m^3
18 W2_3 = ((p3 * v3) - (p2 * v2))/(1-Gamma); // in J
19 W_net = W1_2 + W2_3; // in J
20 W_{net} = W_{net} * 10^{-3}; // in kJ
21 disp(W_net, "net work done in kJ is : ");
```

Chapter 5

First Law of Thermodynamics

Scilab code Exa 5.1 Mass flow rate of air

```
1 // Exa 5.1
2 clc;
3 clear;
4 close;
5 // Given data
6 v1_total = 7;// \text{ in } \text{m}^3/\text{min}
7 \text{ v\_s1} = 0.35; // in m^3/kg
8 \text{ v_s2} = 0.12; // \text{ in m}^3/\text{kg}
9 p1 = 1; // in bar
10 p1 = p1 * 10^5; // in N/m^2
11 p2 = 6; // \text{ in bar}
12 p2 = p2 * 10^5; // in N/m^2
13 D1 = 110; // in mm
14 D1 = D1 * 10^-3; // in m
15 D2 = 65; // in mm
16 D2 = D2 * 10^-3; // in m
17 Af1 = \%pi/4*D1^2; // in m^2
18 Af2 = \%pi/4*D2^2;// in m^2
19 // v1_{total} = m1 * v_{s1}
20 m1 = v1_total / v_s1; //in kg/min
21 disp(m1, "The mass flow rate of air in kg/min is:");
```

Scilab code Exa 5.2 Rate of heat transfer

```
1 //Exa 5.2
2 clc;
3 clear;
4 close;
5 // Given data
6 m = 2; // in kg per min
7 m = m / 60; // in kg per sec
8 W = 20; // in kW
9 h1 = 1400; // in kJ/kg
10 h2 = 1300; // in kJ/kg
11 Q = (m * (h2 - h1)) + W; // in kJ/s
12 disp(Q, "Rate of heat transfer to the water jacket in kJ/sec");
```

Scilab code Exa 5.3 Power output of the turbine

```
1 // Exa 5.3
2 clc;
3 clear;
```

```
4 close;
5 // Given data
6 g = 9.81;
7 p1 = 3; // in Mpa
8 p2 = 10; // in kPa
9 T1 = 350; // in
10 T1 = T1 + 273; // in K
11 m = 1; // in kg per sec
12 v1 = 50; // in m per sec
13 v2 = 120; // in m per sec
14 z1 = 2; // in m
15 	 z2 = 5; // in m
16 \text{ C_p} = 1.005; // \text{ in kJ per sec}
17 Q = 5; // in kJ per sec
18 Q = -(Q) * 10^3; // in J per sec
19 T2 = (p2 * T1)/p1; // in K
20 del_h = C_p * (T2-T1); // in kJ
21 \text{ del_h} = \text{del_h} * 10^3; // \text{ in } J
22 t = m * (del_h + (v2^2-v1^2)/2 + (g * (z2 - z1))); //
       t is variable taken for calculation
23 W_s = Q - t; // in J per sec
24 \text{ W_s} = \text{W_s} * 10^-6; // in MW
25 disp(W_s,"The power output of the turbine in MW");
26 // If kinetic and potential energy are ignored then
27 \text{ W}_{s2} = Q -(m * del_h); // in J per sec
28 \text{ W}_{s2} = \text{W}_{s2} * 10^{-6}; // \text{ in MW}
29 errorIntroduced= (abs(W_s)-abs(W_s2))/abs(W_s)*100;
      // in \%
30 disp(errorIntroduced, "Total error introduced in % is
       :");
```

Scilab code Exa 5.4 Quantity of water circulated

```
1 //Exa 5.4
2 clc;
```

```
3 clear;
4 close;
5 //Given data
6 \text{ h1} = 246.6; // \text{ in } \text{kJ/kg}
7 h2 = 198.55; // in kJ/kg
8 W = 0;
9 g = 9.8;
10 Q = -(105000); // in kJ per hr
11 // m * (h1 + ((v1*^2)/(2*1000)) + ((g * z1)/1000)) +
      Q = m * (h2 + ((v2^2)/(2*1000)) + ((g * z2))
      /1000) + W
12 // v1 and v2 is change in velocity is neglected and
     z2 = z1 + 10
13 m = Q/((h2-h1) + ((g * 10)/1000)); // kg per hr
14 disp(m, "Quantity of water circulated through the
      pipe in kg/hr is");
```

Scilab code Exa 5.5 Power of motor required

```
1 / Exa 5.5
2 clc;
3 clear;
4 close;
5 // Given data
6 \text{ m=15}; // in kg/min
7 m= m/60; // in kg/sec
8 H1= 5; // in kJ/kg
9 H1= H1*10^3; // in J/kg
10 H2= 173; // in kJ/kg
11 H2= H2*10^3; // in J/kg
12 V1= 5; // in m/s
13 V2= 7.5; // in m/s
14 Q= 760; // in kJ/min
15 Q= Q*10^3/60; // \text{ in } J/s
16 // Formula (H1+V1^2/2)+(-Q)=(H2+V2^2/2)+W
```

```
17 W= (H1+V1^2/2)+(-Q)-(H2+V2^2/2); // in W/kg
18 W= W*10^-3; // in kW/kg
19 // The work done will be
20 W= m*W; // in kW
21 P= abs(W); // in kW
22 disp(P, "Power of the motor required to drive the compressor in kW is:")
23 // Part (b)
24 v1= 0.5; // in m^3/kg
25 v2= 0.15; // in m^3/kg
26 // A1/A2= rho2*V2/(rho1*V1) = v1*V2/(v2*V1)
27 ratio0FA1andA2= v1*V2/(v2*V1);
28 radio0Fd1andd2= sqrt(ratio0FA1andA2);
29 disp(radio0Fd1andd2,"Ratio of inlet pipe diameter to outlet pipe diameter is:")
```

Chapter 6

Second Law of Thermodynamics

Scilab code Exa 6.1 Temperature of the source and the sink

```
1 // Exa 6.1
2 clc;
3 clear;
4 close;
5 // Given data
6 // In first case (T1-T2)/T1=1/6
                                                or
     T1 = 1.2 * T2
7 // In seond case (T1-(T2-62))/T1=2/6 or
                                                2*T1
     -3*(T2-62)=0
8 // From eq (i) and (ii)
9 T2= 186/0.6; // in K
10 T1= 1.2*T2; // in K
11 disp(T2-273, "Temperature of the source in C is: "
12 disp(T1-273, "Temperature of the sink in C is: ")
```

Scilab code Exa 6.2 Minimum power required

```
1 // Exa 6.2
2 clc;
3 clear;
4 close;
5 // Given data
6 	ext{ T1 = 25; // in}
7 T2 = 1; // in
8 T1 = T1 + 273; // in K
9 T2 = T2 + 273; // in K
10 HT = 2; // heat transfer across the wall and the roof
     in MJ/hr
11 HT= HT*10^6; // in J/hr
12 Q = HT* (T1-T2); // in J/hr
13 COP_heat = T1/(T1-T2);
14 W_net = Q/COP_heat; // in J/hr
15 disp(W_net*10^-3/3600, "Power rquired for operating
      the pump in kW");
  // Part (b)
16
17 T2= 25; // in
18 T2=T2+273; // in K
19 // COP= T2/(T1-T2)
                                ( i )
20 // COP = HT*(T1-T2)/W_net
                                    (ii)
21 // From (i) and (ii)
22 T1= sqrt(W_net*T2/HT)+T2;// in K
23 T1= T1-273; // in C
24 disp(T1, "The value of T1 in C is: ")
```

Scilab code Exa 6.3 Ratio of heat transfer to circulating water to the engine

```
1 //Exa 6.3
2 clc;
3 clear;
```

```
d close;
    //Given data
    heatEngineEffi= 32/100; // heat engine efficiency
    COP= 5; // COP of heat pump
    // heat engine efficiency = Wnet/Q1 = (Q1-Q2)/Q1
    Q1byWnet= 1/heatEngineEffi;
    Q2byWnet= (1-heatEngineEffi)*Q1byWnet;
    // COP = Q4/Wnet = Q4/(Q4-Q3)
    Q4byWnet= COP;
    ratio= (Q2byWnet+Q4byWnet)/Q1byWnet; // ratio of heat transferred to the circulating water to heat trasferred to the engine
    disp(ratio,"Ratio of heat trasferred to the circulating water to heat trasferred to the engine is: ")
```

Scilab code Exa 6.4 Claim of inventor is true or not

```
1 / Exa 6.4
2 clc;
3 clear;
4 close;
5 //Given data
6 Q = 88; // in MJ
7 Q=Q*10^3; // in kJ
8 T1 = 190; // in
9 T1 = T1 + 273; // in K
10 \text{ T3} = -15; // \text{ in } C
11 T3 = T3 + 273; // in K
12 Eta_carnot = (T1 - T3)/T1;
13 Wnet= Eta_carnot * Q; // in kJ
14 CarnotPower= Wnet/3600; // in kWh
15 disp(CarnotPower,"The value of Carnot Power in kWh
      is : ")
16 disp("As the actual power produced by the invented
```

```
engine is more than the Carnot Power, ");
17 disp("so inverter claim is ")
18 disp(" not true")
```

Scilab code Exa 6.5 Minimum power required

```
1 / Exa 6.5
2 clc;
3 clear;
4 close;
5 // Given data
6 \text{ T1} = 24; // in
7 \text{ T1} = \text{T1} + 273; // \text{ in } \text{K}
8 T2 = 2; // in C
9 T2 = T2 + 273; // in K
10 Q = 100; // in MJ/h
11 Q = Q * 10^3; // in kJ/h
12 COP_heatPump = T1/(T1-T2);
13 W = Q/COP_heatPump; //in kJ/h
14 W = W/3600; // in kW
15 disp(W,"The theoretical minimum power required to
      drive the heat pump in kW is: ")
16 COP_refrigerator = T2/(T1-T2);
17 W = Q/COP_refrigerator; // in kJ/h
18 W = W/3600; // in kW
19 disp(W,"The theoretical power required to drive the
      heat pump when it is used as a refrigerator in kW
       is : ");
```

Scilab code Exa 6.6 Reversible or irreversible cycle

```
1 //Exa 6.6
2 clc;
```

```
3 clear;
4 close;
5 //Given data
6 Q1= 278; // in kJ/s
7 T1= 283+273; // in K
8 T2= 50+273; // in K
9 // Let integrate of delta Q by T is V
10 disp("Part (a)")
11 Q2= 208; // in kJ/s
12 // By Clausius inequality
13 V = Q1/T1 - Q2/T2;
14 if V<0 then
15
       disp("The cycle is irreversible")
16 else
17
       if V>0 then
18
           disp("Reversible or irreversible cycle is
              not possible and the result is impossible
              ")
19
       else
20
           disp("The cycle is reversible")
21
       end
22 end
23 disp("Part (b)")
24 Q2= 139; // in kJ/s
25 V = Q1/T1 - Q2/T2;
26 if V<0 then
27
       disp("The cycle is irreversible")
28 else
       if V>0 then
29
           disp("Reversible or irreversible cycle is
30
              not possible and the result is impossible
31
       else
           disp("The cycle is reversible")
32
33
       end
34 end
35 disp("Part (c)")
36 Q2= 161.5; // in kJ/s
```

```
37 V = Q1/T1 - Q2/T2;
38 if V<0 then
       disp("The cycle is irreversible")
39
40 else
       if V>0 then
41
42
           disp("Reversible or irreversible cycle is
              not possible and the result is impossible
              ")
43
       else
           disp("The cycle is reversible")
44
45
       end
46 end
```

Scilab code Exa 6.16 Heat rejected

```
1 / Exa 6.16
2 clc;
3 clear;
4 close;
5 // Given data
6 Wnet_compresser= 3; // in kW
7 Wnet_compresser=Wnet_compresser*3600; // in kJ/h
8 Qabsorbed= 50; // in MJ/h
9 Qabsorbed=Qabsorbed*10^3; // in kJ/h
10 T1 = 46+273; // in K
11 T2 = 1+273; // in K
12 Qrejected= Wnet_compresser+Qabsorbed; // in kJ/h
13 disp(Qrejected*10^-3,"The heat rejected in MJ/h is:
      ")
14 I= -(-Qrejected/T1+Qabsorbed/T2); // in kJ/h
15 disp(I, "Irreversibility in kJ/h is : ")
```

Scilab code Exa 6.17 Entropy generated

```
1 / Exa 6.17
2 clc;
3 clear;
4 close;
5 // Given data
6 \text{ T1} = 12; // in
                      \mathbf{C}
7 T2 = 92; // in
                      \mathbf{C}
8 \text{ T1} = \text{T1} + 273; // \text{ in } \text{K}
9 T2 = T2 + 273; // in K
10 del_T = T2 - T1; // in K
11 m = 20; // in kg
12 C_v = 4.187;
13 \text{ s= 1};
14 Q = m * s * del_T; // in cal
15 Q = Q * 4.18; // in J
16 H = 2; // heat given by the heater in kw
17 \text{ H} = \text{H} * 10^3; // \text{ in } \text{J/sec}
18 t = Q/H; //time taken by the heater to raise the temp
      . in sec
19 disp(t, "Time taken by the heater to raise the
      temperature in sec is");
20 del_phi = m * C_v * log(T2/T1); // in kJ/K
21 disp(del_phi, "Entrophy generated during the process
      in kJ/K");
```

Scilab code Exa 6.18 Reversible irreversible or carnot cycle

```
1 // Exa 6.18
2 clc;
3 clear;
4 close;
5 // Given data
6 Q1 = 1000; // in kW
7 Q2 = 492; // in kW
8 T1 = 285; // in C
```

```
9 T1 = T1 + 273; // in K

10 T2 = 5; // in C

11 T2 = T2 + 273; // in K

12 Eta_carnot = (T1-T2)/T1*100; // in percentage

13 disp(Eta_carnot, "Carnot efficiency in % is : ")

14 Eta_heat = (Q1 - Q2)/Q1*100; // in percentage

15 disp(Eta_heat, "Efficiency of the heat engine in % is : ")

16 if Eta_heat > Eta_carnot then

17 disp("As the efficiency of heat engine cannot be more than Carnot efficiency, Hence engine cannot execute irreversible cycle. So engine will execute Carnot Cycle which is a reversible cycle too")

18 end
```

Scilab code Exa 6.19 Output of the engine

```
1 // Exa 6.19
2 clc;
3 clear;
4 close;
5 // Given data
6 n = 1080; // in cycle/min
7 Q_s = 57; // in J/cycle
8 T1 = 12; // in
                   \mathbf{C}
9 T1 = T1 + 273; // in K
10 T2 = 2; // in
11 T2 = T2 + 273; // in K
12 // 1 - (Q_r/Q_s) = 1 - (T2/T1)
13 Q_r = (T2/T1)*Q_s; // in J/cycle
14 W = Q_s - Q_r; // in J/cycle
15 P_o = W * n; // in J/min
16 P_o = P_o/60; // in W
17 disp(P_o, "The output of the engine in watt is");
```

Scilab code Exa 6.20 Minimum power required

```
1  // Exa 6.20
2  clc;
3  clear;
4  close;
5  // Given data
6  Q2 = 10^5; // in kJ/hr
7  T1 = -3; // in C
8  T1 = T1 + 273; // in K
9  T2 = 22; // in C
10  T2 = T2 + 273; // in K
11  COP_heat = 1/(1-T1/T2);
12  W = Q2/COP_heat; // in kJ/hr
13  W = W/3600; // in kW
14  disp(W, "Minimum power required in kW is");
```

Scilab code Exa 6.21 Engine efficiency

```
13  // Dividing (iii) by (ii)
14  WbyQ_A= (T_A/T_B-1)/(T_A/T_B);
15  disp(WbyQ_A*100, "The engine efficiency in % is : ")
```

Scilab code Exa 6.22 Heat rejected

```
1 / Exa 6.22
2 clc;
3 clear;
4 close;
5 // Given data
6 \text{ T_A} = 700; // \text{ in } K
7 \text{ T_B= } 600; // \text{ in } K
8 \text{ T_C= 500; // in } K
9 Q_A = 1200; // in kJ
10 // Q_B+Q_C= Q_A-200
                                                               ( i )
11 // Q_A/T_A = Q_B/T_B+Q_C/T_C
                                           (ii)
12 // \text{From eq}(i) \text{ and } (ii)
13 Q_B = (Q_A * (1/T_B - 1/T_A) - 200/T_B) / (1/T_B - 1/T_C); // in
        kJ
14 Q_C = Q_A - Q_B - 200; // in kJ
15 disp(Q_B, "The heat rejected at B in kJ is: ")
16 disp(Q_C, "The heat rejected at C in kJ is: ")
```

Scilab code Exa 6.23 Intermediate temperature

```
1 //Exa 6.23
2 clc;
3 clear;
4 close;
5 // Given data
6 T1= 180+273; // in K
7 T2= 20+273; // in K
```

```
8  // WA/Q1= 1-T3/T1 (i)
9  // WB/QB= 1-T2/T3 (ii)
10  // WA= WB (iii)
11  // Q1= Q_B+WA (iv)
12  // From eq(i),(ii),(iii) and (iv)
13  T3= (T1+T2)/2; // in K
14  disp(T3-273,"The intermediate temperature in C is : ")
```

Scilab code Exa 6.24 Least power necessary to pump

```
1 //Exa 6.24
2 clc;
3 clear;
4 close;
5 // Given data
6 Q2 = 1.75; // in kJ/sec
7 T1 = -15; // in C
8 T1 = T1 + 273; // in K
9 T2 = 30; // in C
10 T2 = T2 + 273; // in K
11 del_T = T2 - T1; // in K
12 // Q2/W_net = T2/(del_T)
13 W_net = Q2 * del_T/T1; // in kW
14 disp(W_net," Least power required in kW is");
```

Chapter 7

Entropy

Scilab code Exa 7.2 Change in entropy of air

```
1 //Exa 7.2
2 clc;
3 clear;
4 close;
5 // Given data
6 \text{ v1} = 0.05; // \text{ in } \text{m}^3
7 v2 = 8 * v1; // in m^3
8 T1 = 280; // in C
9 \text{ T1} = \text{T1} + 273; // \text{ in } \text{K}
10 T2 = 25; // in C
11 T2 = T2 + 273; // in K
12 p1 = 8; // \text{ in bar}
13 C_p = 1.005; // in kJ/kgK
14 C_v = 0.712; // in kJ/kgK
15 R = C_p - C_v; // in kJ/kgK
16 del_phi = (R * (log(v2/v1))) + (C_v * (log(T2/T1)))
       ); // in kJ/kgK
17 disp(del_phi,"The change in entrophy of air during
      the process in kJ/kgKis");
```

Scilab code Exa 7.3 Overall change in entropy

```
1 // Exa 7.3
2 clc;
3 clear;
4 close;
5 // Given data
6 m = 5; // in kg
7 \text{ T1 = 50; // in } C
8 T1 = T1 + 273; // in K
9 T2 = 250; // in C
10 \text{ T2} = \text{T2} + 273; // \text{ in } \text{K}
11 C_p = 1.0;
12 \quad C_v = 0.72;
13 T3 = 50; // in C
14 \text{ T3} = \text{T3} + 273; // \text{ in } \text{K}
15 del_phi = m * C_p * (log(T2/T1)); // in kJ/K (this)
      is increase in entrophy)
16 del_phi1 = m * C_v * (\log(T3/T2)); // in kJ/K (this
      is decrease in entrophy)
17 phi_net = del_phi - abs(del_phi1); // in kJ/K
18 disp(phi_net,"The net change in entrophy in kJ/K is")
      );
```

Scilab code Exa 7.6 Entropy generated during the process

```
1 // Exa 7.6
2 clc;
3 clear;
4 close;
5 // Given data
6 Q1 = 1600; // in kJ
```

```
7 Q2 = 1600; // in kJ
8 T1 = 800; // in K
9 T2 = 127; // in C
10 T2 = T2 + 273; // in K
11 d1_phi = Q1/T1; // in kJ per K
12 d2_phi = Q2/T2; // in kJ per K
13 net_phi = d2_phi - d1_phi; // in kJ per K
14 disp(net_phi, "Total entrophy generated during the process in kJ/K is : ");
```

Scilab code Exa 7.8 The flow of air

```
1 // Exa 7.8
2 clc;
3 clear:
4 close;
5 // Given data
6 \text{ T_A= } 50+273; // \text{ in } K
7 \text{ T_B= } 13+273; // in K
8 P_A = 130; // in kPa
9 P_B = 100; // in kPa
10 Cp= 1.005; // in kJ/kg-K
11 pvByT= 0.287;// p in kPa, v in m^3/kg, T in K
12 del_S_system = Cp*log(T_B/T_A) - pvByT*log(P_B/P_A); //
      in kJ/kg-K
13 del_S_surrounding=0;
14 del_S_universe= del_S_system+del_S_surrounding;// in
       kJ/kg-K
15 disp(del_S_universe, The change in entropy in kJ/kg-
     K is : ")
16 disp("But a negative change in entropy is not
      possible,");
17 disp("hence the flow of air must be from B to A")
```

Scilab code Exa 7.9 Change in entropy

```
1 // Exa 7.9
2 clc;
3 clear;
4 close;
5 // Given data
6 m = 5; // in kg
7 s = 4.18;
8 T1 = 0; // in C
9 T2 = 20; // in C
10 dt = T2 - T1; // in
11 Q = m * s * dt; // in kJ
12 L = 335; // in kJ/kg
13 // Q = m_i * 1
14 \text{ m_i} = Q/L; // \text{ in kg}
15 T1 = T1 + 273; // in K
16 \text{ T2} = \text{T2} + 273; // \text{ in } \text{K}
17 del_S = ((m_i * L)/T1) - (m * s * (log(T1/T2))); //
      in kJ per K
18 disp(del_S, "Change in entrophy of the adiabatic in
      kJ/K is");
```

Scilab code Exa 7.11 Net heat transfer and overall change in entropy

```
1 //Exa 7.11
2 clc;
3 clear;
4 close;
5 // Given data
6 p1 = 1 * 10^5; // in N/m^2
7 C_p = 1.005; // in kJ/kg k
```

```
8 R = 287; // in j/kg k
9 T1 = 290; // in K
10 T2 = 580; // in K
11 v1 = 1; // in m^3
12 m = (p1 * v1)/(R * T1); // in kg
13 Q = m * R * (T2-T1); // in J
14 Q = Q * 10^-3; // in kJ
15 del_phi = m * C_p * (log(T2/T1)); // in kJ per K
16 R = R * 10^-3; // in kJ/kg K
17 C_v = C_p - R; // in kJ/kg k
18 del1_phi = m * C_v * (log(T1/T2)); // in kJ/K
19 net_phi = del_phi + del1_phi; // in kJ/K
20 disp(net_phi,"Over all change in entrophy in kJ/K");
```

Chapter 8

Availability and Irreversibility

Scilab code Exa 8.1 Availability and unavailability of heat

```
1 // Exa 8.1
2 clc;
3 clear;
4 close;
5 // Given data
6 Q = 16; // in MJ
7 Q = Q * 10^3; // in kJ
8 T_H = 227; // in C
9 \text{ T_H} = \text{T_H} + 273; // in K
10 \text{ T_L} = 15; // in
11 T_L = T_L + 273; // in K
12 del_S = Q/T_H; // in kJ/K
13 A = Q - (T_L * del_S); // in kJ
14 disp(A, "The available part of heat in kJ is");
15 U_P_ofHeat = T_L * del_S; // unavailable part of heat
       in kJ
16 disp(U_P_ofHeat,"The unavailable part of heat in kJ
      is :");
```

Scilab code Exa 8.2 Availability and unavailability of system

```
1 //Exa 8.2
2 clc;
3 clear;
4 close;
5 // Given data
6 Q = 12000; // in kJ
7 T_H = 600; // in K
8 T_L = 300; // in K
9 dS = Q / T_H; // in kJ/K
10 A = Q - (T_L * dS); // available work in kJ
11 disp(A, "Available work is in kJ");
12 UA = T_L * dS; // unavailable work in kJ
13 disp(UA, "Anavailable work is in kJ");
```

Scilab code Exa 8.3 Available and unavailable energy

```
1 // Exa 8.3
2 clc;
3 clear;
4 close;
5 // Given data
6 m = 800; // in kg
7 C_p = 0.5; // in kJ/kg K
8 T2 = 500; // in K
9 \text{ T1} = 1250; // \text{ in } K
10 T_o = 300; // in K
11 del_t = T1 - T2; // in K
12 Q = m * C_p * del_t; // in kJ
13 dS = abs(m * C_p * log(T2/T1)); // in kJ/K
14 availableEnergy = Q - (T_o * dS); //in kJ
15 disp(round(availableEnergy*10^-3), "Available energy
      in MJ is :");
16 unavailableEnergy = T_o * dS; // UA stands for
```

```
unavailable energy in kJ
17 disp(round(unavailableEnergy*10^-3),"Unavailable
    energy in MJ is :");
```

Scilab code Exa 8.4 Availability per kg of steam entering and leaving the turbine

```
1 / Exa 8.4
2 \text{ clc};
3 clear;
4 close;
5 // Given data
6 h_i = 726.1;
7 h_o = 25.03;
8 \text{ T_o} = 298; // \text{ in } K
9 \text{ s_i} = 1.582;
10 \text{ s_o} = 0.087;
11 h2 = 669;
12 	 s2 = 1.677;
13 h3 = 52.17 + (0.9 * 567.7);
14 	ext{ s3} = 0.1748 + (0.9 * 1.7448);
15 sai_i = (h_i - h_o) - (T_o * (s_i - s_o)); // in kcl/
      kg
16 disp(sai_i,"The availablibity per kg of steam
      entering in kcl/kg is :");
17 sai_e = (0.25 * ((h2 - h_o) - (T_o * (s2 - s_o)))) +
       (0.75 * ((h3 - h_o) - (T_o * (s3 - s_o)))) ; //
      in kcl/kg
18 disp(sai_e,"The availablibity per kg of steam
      leaving in kcl/kg is :");
19 w_rev = sai_i - sai_e;// in kcl/kg
20 disp(w_rev,"reveseble work per kg of steam in kcl/kg
      ");
21
22 // Note: There is calculation error in evaluating
```

```
the value of availability per kg of steam leaving in kcl/kg. so the answer in the book is wrong and coding is right.
```

Scilab code Exa 8.5 Irreversibility

```
1 // Exa 8.5
2 clc;
3 clear;
4 close;
5 // Given data
6 \text{ T_o} = 298; // \text{ in } K
7 m2 = 25000;
8 	ext{ s2} = 16775;
9 m3 = 75000;
10 \text{ s3} = 17448;
11 \quad m1 = 1000000;
12 \text{ s1} = 1582;
13 Q = -16; // in MJ
14 Q = Q * 10^3; // in kJ
15 I = (T_o * ((m2 * s2) + (m3 * s3) - (m1 * s1))) - Q;
      // in cal/hr
16 I=I*10^-3; // in kcal/hr
17 disp(I,"The irreversibility in kcal/hr");
18
19 // Note: There is calculation error in evaluating
      the value of the irreversibility in kcal/hr. so
      the answer in the book is wrong and coding is
      right.
```

Scilab code Exa 8.6 Availability per kg of steam

```
1 // Exa 8.6
```

```
2 clc;
3 clear;
4 close;
5 // Given data
6 h_i = 749.2;
7 h_o = 25.03;
8 \text{ T_o} = 298; // \text{ in } K
9 \text{ s_i} = 1.6202;
10 \text{ s_o} = 0.0877;
11 phi_i = (h_i - h_o) - (T_o * (s_i - s_o)); // kcal/kg
12 disp(phi_i,"The availablibity before adiabatic
      throttling in kcal/kg is: ");
13 h_e = 749.2;
14 \text{ s_e} = 1.6936;
15 phi_e = (h_e - h_o) - (T_o * (s_e - s_o)); // in kcal
16 disp(phi_e,"The availablibity before adiabatic
      throttling in kcal/kg is: ");
17 Wrev = phi_i - phi_e; // in kcal/kg
18 disp(Wrev, "Reversible work in kcal/kg is: ");
19 \text{ Wactual} = 0;
20 i = Wrev-Wactual; // in kcal/kg
21 disp(i, "Irreversibility per kg of steam in kcal/kg
      is : ");
```

Scilab code Exa 8.7 Lost work

```
1 //Exa 8.7
2 clc;
3 clear;
4 close;
5 // Given data
6 // del_W = T * ds - del_Q;
7 T = 600; // in K
8 p_i = 7; //kgf/cm^2
```

```
9  p_e = 1.5; // kgf/cm^2
10  T_o = 298; // in K
11  R = 29.27/427;
12  del_W_lost = T * ( R *log(p_i/p_e)); // in kcal/kg
13  disp(del_W_lost,"Lost work in kcal/kg is");
14  i = T_o * (R * (log(p_i/p_e))); // in kcal/kg
15  disp(i,"Irreversebility per kg of air flow in kcal/kg is");
```

Chapter 9

Properties of Steam and Thermodynamic Cycles

Scilab code Exa 9.1 Specific volume enthalpy latent heat and entropy

```
1 // Exa 9.1
2 clc;
3 clear;
4 close;
5 // Given data
6 disp("Part (i): For dry saturated steam at 17.8 bar
7 p = 17.8; // in bar
8 p1 = 17.5; // in bar
9 p2 = 18.0; // in bar
10 Vs1= 0.1135; // in litre/kg
11 Vs2= 0.1104; // in litre/kg
12 Hs1= 2796.1; // in kJ/kg
13 Hs2= 2796.4; // in kJ/kg
14 L1= 1918; // in kJ/kg
15 L2= 1912; // in kJ/kg
16 phi_s1= 6.389; // in kJ/kg K
17 phi_s2= 6.379; // in kJ/kg K
18 Vs= Vs1-(Vs2-Vs1)/(p2-p1)*(p-p1);// in litre/kg
```

```
19 Hs= Hs1+(Hs2-Hs1)/(p2-p1)*(p-p1);// in kJ/kg
20 L= L1- (L1-L2)/(p2-p1)*(p-p1); // in kJ/kg
21 phi_s = phi_s1 - (phi_s1 - phi_s2)/(p2-p1)*(p-p1); // in
     kJ/kg K
22 disp("Part (i): For dry saturated steam at 17.8 bar
23 disp(Vs,"The specific volume in litre/kg is: ");
24 disp(Hs," The enthalpy in kJ/kg is: ");
25 disp(L,"The latent heat in kJ/kg is: ");
26 disp(phi_s, "The entropy in kJ/kg K")
27 disp("Part (ii): For superheated steam at 16 bar
     and 340 C")
28 T = 340; // in K
29 T1= 300; // in K
30 T2= 350; // in K
31 Vsup1= 0.1585; // in m^3/kg
32 Vsup2= 0.1743; // in m<sup>3</sup>/kg
33 Hsup1= 3030; // in kJ/kg
34 Hsup2= 3142; // in kJ/kg
35 phi_sup1= 6.877; // in kJ/kg K
36 phi_sup2= 7.063; // in kJ/kg K
37 Vsup= Vsup1+(Vsup2-Vsup1)/(T2-T1)*(T-T1); // in m^3/
     kg
38 Hsup= Hsup1+(Hsup2-Hsup1)/(T2-T1)*(T-T1); // in kJ/kg
39 phi_sup= phi_sup1+(phi_sup2-phi_sup1)/(T2-T1)*(T-T1)
     ; // in kJ/kg
40 disp(Vsup, "The specific volume in m<sup>3</sup>/kg is: ");
41 disp(Hsup, "The enthalpy in kJ/kg is: ");
42 disp(phi_sup,"The entropy in kJ/kg K is : ")
```

Scilab code Exa 9.2 Condition of steam

```
1 // Exa 9.2
2 clc;
3 clear;
```

```
4 close;
5 // Given data
6 \text{ h\_sen} = 798.43; // in kJ/kg
7 L = 1984.3; // in kJ/kg
8 H_total_wet = 2665.7;
9 // H_{total_wet} = h_{sen} + x * L
10 x = (H_total_wet - h_sen)/L;
11 disp(x,"The value of x is :");
12 // Part (b)
13 h_total_sup= 2961; // in kJ/kg
14 Cps= 2.112; // in kJ/kg
15 H_total_dry= 2782.7; // in kJ/kg
16 // Let deltaT= T_sup-T_sat
17 // h_total_sup = h_sen+L+h_sup = H_total_dry +Cps*
     deltaT
18 deltaT= (h_total_sup-H_total_dry)/Cps;// in C
19 disp(deltaT, "Degree of superheat in C is:")
```

Scilab code Exa 9.3 Change in enthalpy and entropy

```
1  // Exa 9.3
2  clc;
3  clear;
4  close;
5  // Given data
6  H2 = 3055; // in kj per kg
7  H3 = 2550; // in kj per kg
8  fie_1 = 7.15; // kj per kg k
9  fie_2 = 7.57; // kj per kg k
10  d_fie= fie_2 - fie_1; // in kj per kg k
11  disp(d_fie, "Change in entropy during throttling process in kJ/kg-K is:");
12  dH = H2 - H3; // in kj per kg
13  disp(dH, "Change in enthalpy during isentropic process in kJ/kg is:");
```

Scilab code Exa 9.4 Quantity of heat

```
1 // Exa 9.4
2 clc;
3 clear;
4 close;
5 // Given data
6 \text{ H}_{w} = 670.4; // \text{ in } \text{kJ/kg}
7 L = 2085; // kJ per kg
8 T_sat = 158.8; // in degree c
9 m = 4; // in kg
10 x = 0.5;
11 h_sen = 670.4; // in kJ/kg
12 H_totalwet = m * ( h_sen + (x *L)); // in kJ
13 \times 1 = 0.95
14 H_totalwet1 = m *( h_sen + (x1 *L)); // in kJ
15 Q1 = H_{totalwet1} - H_{totalwet}; // in kJ
16 disp(Q1," Part (i) The quantity of heat in case first
       in kJ is : ");
17 // Part (b)
18 \times 2 = 1;
19 H_totaldry = m *( h_sen + (x2 *L)); // in kJ
20 Q2 = H_totaldry - H_totalwet; // in kJ
21 disp(Q2," Part (ii) The quantity of heat in case
      second in kJ is: ");
22 // Part (c)
23 H_totalsup = 3062.3; // in kJ per kg
24 H_totalsup = m * H_totalsup; // in kJ
25 Q3 = H_totalsup - H_totalwet; // in kJ
26 disp(Q3," Part (iii) The quantity of heat in case
      third in kJ is : ");
27 // Part (d)
28 H_totalsup = 2950.4; // in kj per kg
29 H_totalsup = m * H_totalsup; // in kj
```

```
30 Q4 = H_totalsup - H_totalwet; // in kj
31 disp(Q4, "Part (iv) The quantity of heat in case forth in kJ is: ");
```

Scilab code Exa 9.5 Isentropic efficiency of turbine

```
1 // Exa 9.5
2 clc;
3 clear;
4 close;
5 // Given data
6 p1 = 2.5; // Mpa
7 p1 = p1 * 10^6; // in pa
8 p1 = p1 * 10^-5; // in bar
9 p2 = 10; // in kpa
10 p2 = p2 * 10^3; // in pa
11 p2 = p2 * 10^-5; // in bar
12 H1 = 2878; // in kJ/kg at 25 bar and 250 C
13 H2 = 2583.9; // in kJ/kg at 0.1 bar for dry saturated
      steam
14 AHD= H1-H2; // actual heat drop in kJ/kg
15 H2_desh = 2110; // in kj per kg
16 IHD = H1 - H2_desh; // Isentropic heat drop in kJ/kg
17 Eta_Isentropic = (AHD/IHD) * 100; // in \%
18 disp(Eta_Isentropic, "Isentropic efficiency in % is")
19 // H1 + v1^2/2 + g*z1 + Q = H2 + v2^2/2 + g*z2 + W
20 W = H1 - H2; // in kJ/kg (as v1=v2, z1=z2 and Q=0)
21 disp(W, "Turbine work is in kJ/kg is :");
```

Scilab code Exa 9.6 Dryness fraction of steam

```
1 / Exa 9.6
```

```
2 clc;
3 clear;
4 close;
5 // Given data
6 p1 = 11; // in bar
7 p2 = 1.2; // in bar
8 \text{ H}_{\text{w}1} = 781.1; //\text{in kJ/kg}
9 L1 = 2000; // in kJ/kg
10 t1 = 120; // in degree c
11 t1 = t1 + 273; // in K
12 t2 = 104.81; // in degree c
13 t2 = t2 + 273; // in K
14 H_dry2 = 2683.4; // in kJ/kg
15 C_p = 2.607; // in kJ/kgK
16 // From Hw1+x*L1 = H_dry2+Cp*(t1-t2)
17 x = (H_dry2 + (C_p * (t1 - t2)) - H_w1) / L1;
18 disp(x,"Dryness fraction of steam is:");
19 x1 = (H_dry2 - H_w1)/L1;
20 disp(x1, "Maximum dryness fraction of steam is:");
```

Scilab code Exa 9.7 Dryness fraction of sample steam

```
1 //Exa 9.7
2 clc;
3 clear;
4 close;
5 // Given data
6 W = 21; // in kg
7 w_wp = 2; // in kg
8 h1 = 781.15; // in kJ/kg
9 L1 = 1998.5; // in kJ/kg
10 m = 2; // in kg
11 h2 = 420.5; // in kJ/kg
12 L = 2255.9; // in kJ/kg
13 t_sat = 100.4; // in degree c
```

```
14 t1 = 110; // in degree c
15 C_ps = 2; // in kJ/kgK
16 x1 = W / (W + w_wp);
17 x2 = (h2 + L + m * (t1-t_sat) - h1) / L1;
18 x = x1 * x2;
19 disp(x, "The dryness fraction for sample steam is");
```

Scilab code Exa 9.8 Heat transfer during the process

```
1 //Exa 9.8
2 clc;
3 clear;
4 close;
5 // Given data
6 h_sen = 417.4; // in kJ/kg
7 h_totaldry = 2675.4; // in kJ/kg
8 L = 2258; // in kJ/kg
9 v = 5; // in m^3
10 v_v = 4.95; // in m^3
11 x = v_v/v;
12 Q = h_totaldry -(h_sen +x*L); // in kJ/kg
13 disp(Q,"Heat transferred per kg in kJ/kg is:");
```

Scilab code Exa 9.9 Work done during evaporation

```
1 // Exa 9.9
2 clc;
3 clear;
4 close;
5 // Given data
6 m = 1; // in kg
7 p = 10; // in bar
8 p = p * 10^2; // in kpa
```

```
9  x = 0.94;
10  h_sen = 762.61; // in kJ/kg
11  L = 2013.6; // in kJ/kg
12  v_s = 0.1942; // in m^3 per kg
13  w_ext = p * x * v_s * m; // in kJ/kg
14  disp(w_ext, "The work done during evaporation in kJ/kg is");
15  // Part (b)
16  L_internal = (x * L) - w_ext; // in kJ/kg
17  disp(L_internal, "Internal latent heat in kJ/kg is");
18  // Part (c)
19  U_wet = h_sen+x*L-p*x*v_s; // in kJ/kg
20  disp(U_wet, "Internal energy in kJ/kg is");
```

Scilab code Exa 9.10 Entropy

```
1 // Exa 9.10
2 clc;
3 clear;
4 close;
5 // Given data
6 \text{ T_sat} = 179.88; // \text{ in degree c}
7 \text{ T_sat} = \text{T_sat} + 273; // in k
8 \text{ T_sup} = 200; // \text{ in degree c}
9 \text{ T_sup} = \text{T_sup} + 273; // in k
10 L = 2013.6; // in kJ/kg
11 C_{ps} = 2.326;
12 C_pw = 1;
13 x = 0.8;
14 phi_wet = C_{pw} * log(T_{sat}/273) + ((x * L)/T_{sat}); //
       in kJ/kg-K
15 disp(phi_wet, "Entropy of wet steam in kJ/kg-K is");
16 // Part (b)
17 phi_dry = C_pw * log(T_sat/273) + L/T_sat; // in kJ/kg
18 disp(phi_dry, "Entropy of dry and saturated steam in
```

```
kJ/kg-K~is");\\ 19~//~Part~(c)\\ 20~phi\_sup = phi\_dry+C\_ps~*log(T\_sup/T\_sat);//~in~kJ/kg\\ 21~disp(phi\_sup,"Entropy~at~200~C~in~kJ/kg-K~is~:");
```

Scilab code Exa 9.11 Volume of steam

```
1 // Exa 9.11
2 clc;
3 clear;
4 close;
5 // Given data
6 m = 1; // in kg
7 x = 0.9;
8 p = 1; // N/mm^2
9 p = p * 10^1; // in bar
10 p = p * 10^2; // in kPa
11 h_sen = 762.61; // in kJ/kg
12 L = 2013.6; // in kJ/kg
13 v_s = 0.1944; // in m^3 per kg
14 H_totalwet = h_sen + x*L; // in kJ/kg
15 U_wet = H_totalwet - (p * x * v_s); // in kJ/kg
16 I = U_wet / H_totalwet; // internal energy as a
      fraction of total heat
17 I = I * 10^2; // in \%
18 disp(I,"The internal energy in % is");
19 // Part (b)
20 \text{ v_s} = 0.1542; // \text{ in } \text{m}^3/\text{kg}
21 h_sen = 815; // in kJ/kg
22 L = 1972; // in kJ/kg
23 H_totaldry = 2787; // in kJ/kg
24 \text{ C_ps} = 2.199;
25 t_{sup} = 250; // in
26 t_{sup} = t_{sup} + 273; // in K
27 \text{ t_sat} = 190.74; // in C
```

Scilab code Exa 9.12 Condition of steam

```
1 // Exa 9.12
2 \text{ clc};
3 clear;
4 close;
5 // Given data
6 m = 0.5; // in kg
7 M = 6.6; // in kg
8 x1 = M / (M+m);
9 \text{ h_dry} = 2683; //in kJ/kg}
10 \ C_p = 2.1;
11 h_sen = 814.5; //in kJ/kg
12 L = 1973; // in kJ/kg
13 t_{sup} = 120; // in C
14 \text{ t_sat} = 104.8; // in C
15 x2 = (h_dry+C_p*(t_sup - t_sat)-h_sen)/L;
16 x = x2 * x1;
17 disp(x," the dryness fraction of steam is");
```

Chapter 10

Steam Power Plant and Rankine Cycle

Scilab code Exa 10.1 Carnot efficiency

```
1 //Exa 10.1
2 clc;
3 clear;
4 close;
5 // Given data
6 p1 = 10; // in bar
7 p2 = 0.5; // in bar
8 \text{ T1} = 179.9; // in
9 T1 = T1 + 273; // in K
10 \text{ T2} = 81.4; // in
                       C
11 T2 = T2 + 273; // in K
12 Eta_carnot = (T1 - T2)/T1*100; // in \%
13 disp(Eta_carnot,"Carnot efficiency of an engine when
       the steam is 0.87 dry in % is");
14 disp(Eta_carnot," Carnot efficiency of an engine when
       the steam is dry saturated in % is");
15 \text{ T1} = \text{T1} + 50; // \text{ in } \text{K}
16 Eta_carnot1 = (T1 - T2) / T1*100; // in %
17 disp(Eta_carnot1, "Carnot efficiency of an engine
```

Scilab code Exa 10.2 Heat supplied to the boiler

```
1 // Exa 10.2
2 clc;
3 clear;
4 close;
5 // Given data
6 \text{ h1} = 3015; // \text{ in } \text{kJ/kg}
7 h2 = 2326; // in kJ/kg
8 h3 = 113; // in kJ/kg
9 h4 = 114.95; // in kJ/kg
10 Q = h1 - h4; // in kJ/kg
11 disp(Q,"Heat supplied to the boiler in kJ/kg is");
12 W_T = h1 - h2; /// in kJ/kg
13 disp(W_T, "Work developed by turbine in kJ/kg is:")
14 W_P = ( h1 - h3) - Q; // in kJ/kg
15 disp(W_P, "Work absorbed by pump in kJ/kg is : ");
16 Eta = (W_T - W_P)/Q*100; // in \%
17 disp(Eta, "Efficiency of flow system in % is:");
```

Scilab code Exa 10.3 Percentage increse in Rankine efficiency

```
1 // Exa 10.3
2 clc;
3 clear;
4 close;
5 // Given data
6 phi_s = 6.583;
7 phi_w = 1.091;
8 phi_s1 = 6.504;
```

```
9 C_p = 2.25;
10 T_{sat} = 179.9; // in C
11 T_{sat} = T_{sat} + 273; // in K
12 T_{sup} = T_{sat} + 50; // in K
13 \times 2 = (phi_s - phi_w)/phi_s1;
14 H1 = 2776.2; // \text{ in } kJ/kg
15 H_w2 = 340.6; // in kJ/kg
16 L2 = 2305;
17 H2 = H_w2 + (x2 * L2); // in kJ/kg
18 Eta_rankine = (H1 - H2)/(H1 - H_w2)*100; // in \%
19 disp(Eta_rankine, "Rankine efficiency in % is");
20 \text{ phi}_w1 = 2.138;
21 \times 1 = 0.87;
22 \text{ phi}_s1 = 4.445;
23 \text{ phi}_w2 = 1.091;
24 \text{ phi}_{s2} = 6.504;
25 	ext{ x2} = (phi_w1 + (x1 * phi_s1) - phi_w2) / phi_s2;
26 \text{ H1} = 762.6 + (x1 * 2013.6); // in kJ/kg
27 H2 = 340.6 + (x2 * 2305); // in kJ/kg
28 Eta_rankine1 = (H1 - H2) / (H1 - H_w2)*100; // in \%
29 PerDropInRankine= (Eta_rankine - Eta_rankine1)/
      Eta_rankine * 100; // in \%
30 disp(PerDropInRankine, "Percentage drop in Rankine
       efficiency in % is : ");
31 \text{ phi}_s1 = 6.583;
32 \text{ phi}_w1 = 1.091;
33 \text{ phi}_{s2} = 6.504;
34 \times 2 = (phi_s1 + C_p * log(T_sup/T_sat) - phi_w1)/
      phi_s2;
35 \text{ H\_s1} = 2776.2;
36 \text{ H1} = \text{H\_s1} + \text{C\_p} * (\text{T\_sup} - \text{T\_sat}); // \text{ in } \text{kJ/kg}
37 \text{ H2} = 340.6 + (0.88 * 2305); // \text{ in } \text{kJ/kg}
38 \text{ H}_{w2} = 340.6;
39 Eta_rankine2 = (H1 - H2) / (H1 - H_w2);
40 Eta_rankine2 = Eta_rankine2 * 10^2; // in percentage
41 PerIncInRank = ((Eta_rankine2 - Eta_rankine)/
       Eta_rankine2) * 100;// in percentage
42 disp(PerIncInRank," Percentage increase in rankine
```

Scilab code Exa 10.4 Thermal efficiency of the cycle

```
1 / Exa 10.4
2 clc;
3 clear;
4 close;
5 // Given data
6 \text{ H2} = 2776.2; // in kJ/kg
7 p1 = 10; // in bar
8 p_2 = 1; // in bar
9 p_3 = 0.25; // in bar
10 p_4 = p_3; // in bar
11 // w = (H2 - H_{-}2) + ((p_{-}2 - p_{-}3) * v_{-}2); // work done
       in kJ/kg
12 \text{ phi}_2 = 6.583;
13 \text{ phi}_d2 = 1.303;
14 L = 6.057;
15 x_2 = (phi_2 - phi_d2) / L;
16 H2_desh = 417.5 + (x_2* 2257.9); // in kJ/kg
17 \text{ v_s} = 1.694;
18 \ v_2 = x_2 * v_s; // in m^3 per kg
19 w = (H2 - H2_desh) + ((p_2 - p_3) * v_2); // in kJ/kg
20 H4 = 282.7; // in kJ/kg
21 H_w4 = H4; // in kJ/kg
22 HeatSupplied = H2 - H4; // kJ/kg
23 Eta_modifiedRankine = w / HeatSupplied*100; // in \%
24 disp(Eta_modifiedRankine,"Thermal efficiency of
      the cycle in \% is : ");
25 HeatRemoved = HeatSupplied - w; // in kJ/kg
26 disp(HeatRemoved, "Heat removed in condenser in kJ/kg
       is : ");
```

Scilab code Exa 10.13 Work output per kg

```
1 // Exa 10.13
2 \text{ clc};
3 clear;
4 close;
5 // Given data
6 Q = 1100; // in kW
7 \text{ m=1}; // \text{ in kg}
8 p1 = 15; // in bar
9 p1 = p1 * 10^5; // in Pa
10 p1 = p1 * 10^-3; // in kPa
11 p2 = 0.05 * 10^2; // in kPa
12 v1 = 0.16; // m<sup>3</sup> per kg
13 v2 = 26; // in m<sup>3</sup> per kg
14 V1 = 110; // in m per s
15 V2 = 120; // in m per s
16 \text{ u1} = 2935; // \text{ in kJ per kg}
17 u2 = 1885; // in kJ per kg
18 g = 9.8;
19 z1 = 0;
20 	 z2 = 0;
21 // Formula Q-W= m*\{(u2 - u1) + (p2*v2-p1*v1) + 1/2*(V2)\}
      ^2-V1^2)+g*(z2-z1)
22 \text{ W} = Q - m * \{(u2 - u1) + (p2 * v2 - p1 * v1) + 1/2 * (V2^2 - V1^2) + g\}
      *(z2 - z1); // in kW
23 disp(W,"Work output per kg in kW is");
24 SteamFlowRate = Q / W; // in kg/sec
25 SteamFlowRate = SteamFlowRate * 3600; // in kg per hr
26 disp(SteamFlowRate, "Steam flow rate in kg/hr is");
```

Scilab code Exa 10.14 Ratio of mass flow rate of cooling water to condensing steam

```
1 // Exa 10.14
2 clc;
3 clear;
4 close;
5 // Given data
6 \text{ h\_sen} = 191.9; // \text{ in } \text{kJ/kg}
7 L = 2392; // in kJ/kg
8 x = 0.95;
9 \text{ t_o} = 35; // in
10 t_i = 20; // in
                     \mathbf{C}
11 \ C = 4.18;
12 H_totalwet = h_sen + (x * L); //in kJ/kg
13 // m_steam * (H_totalwet - h_sen) = m_water * C * (
      t_o - t_i
14 msBYmw = (H_totalwet - h_sen) / (C * (t_o - t_i));
15 disp(msBYmw,"The Ratio of mass flow rate of cooling
      water to condensing steam is: ");
```

Chapter 11

Introduction to Working of IC Engines

Scilab code Exa 11.1 Capacity of the engine

```
1 // Exa 11.1
2 clc;
3 clear;
4 close;
5 // Given data
6 n = 3;
7 1 = 80; // in mm
8 d = 76; // in mm
9 r = 8.5;
10 V_s = (\%pi/4) * d * d * 1; // in mm^3
11 V_s = V_s * 10^-3; // in cm<sup>3</sup>
12 // r = 1 + (V_s/V_c)
13 V_c = (1/(r - 1)) * V_s; // in cm^3
14 disp(V_c*10^3, "Clearance volume of cylinder in mm^3
      is : ");
15 C = V_s * n; // C stands for capacity of engine in cm
16 \ C = C * 10^{-3}; // in litre
17 disp(C, "Capacity of the engine in litre is:");
```