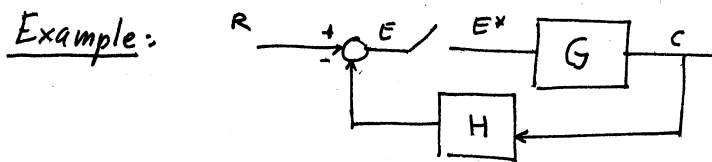


CLOSED LOOP SYSTEMS (chapter 5)

So far (chapter 4) we have considered only open-loop systems. The next step is to look into what happens when you close the loop.



Want to find closed loop transfer function: \Rightarrow

$$E = R - HC = R - (HG)E^* \Rightarrow E^* = R^* - (HG)^* E^* \Rightarrow$$

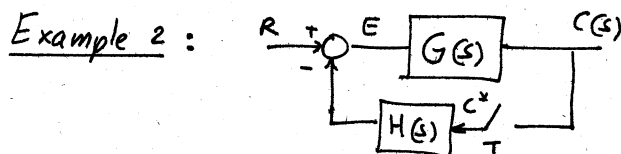
$$E^* = \frac{R^*}{1 + [HG]^*} \quad \text{and} \quad C = \frac{GR^*}{1 + (HG)^*}$$

However, if we had selected C instead of E as variable we get

$$\begin{aligned} C &= GE^* \\ E &= R - HC \Rightarrow E^* = R^* - [HC]^* \Rightarrow C = GR^* - G[HC]^* \\ C^* &= G^* R^* - G^* (HC)^* \end{aligned}$$

Now we are stuck!! we can't proceed because we can't factor C^* out of $[HC]^*$.

Need a systematic way to avoid these problems. (even if a TF does not exist, we'd like to be able to compute the output)



$$\begin{aligned} E &= R - HC^* \\ C &= GR - GH C^* \\ C^* &= (GR)^* - (GH)^* C^* \end{aligned}$$

$$\Rightarrow C^* = \frac{(GR)^*}{1 + (GH)^*} \quad \text{or} \quad C(z) = \frac{[GR](z)}{1 + (GH)(z)}$$

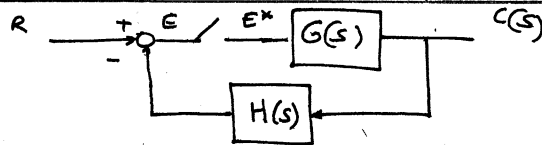
On the other hand, if we select E as a variable we have:

$$\begin{aligned} E &= R - HC^*, \quad C = GE \\ C^* &= (GE)^* \end{aligned}$$

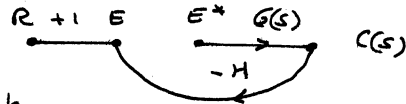
$$\Rightarrow E = R - H[GE]^* \quad \text{or} \quad E^* = R^* - H^* [GE]^* \quad \text{and}$$

stuck again!! (can't solve for E^*)

General Procedure



- (1) Find the "original" flow graph:



Note that since the sampler does not have a T.F., it is not in the graph.

- (2) Assign a variable to each sampler output
- (3) Consider each sampler output as a source. Find the sampler inputs and the systems outputs in terms of each sampler output and the system input
- (4) Take the starred transform of these equations and solve

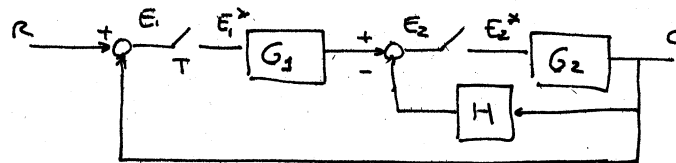
Example:

- (2) sampler output: E^*
- (3) sampler input: $E = R - (HG) E^*$
system output: $C = G(s) E^*$

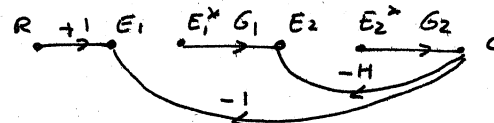
$$(4) E^* = R^* - (HG)^* E^* \Rightarrow E^* = \frac{R^*}{1 + (GH)^*}$$

$$C^* = G^* E^* \Rightarrow C^* = \frac{G^*}{1 + (GH)^*} R^*$$

Example 2:



- (1) "original" flow graph:

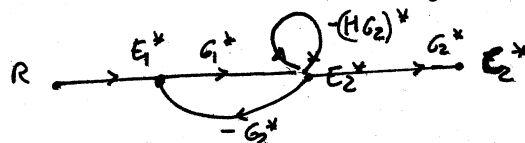


- (2) variables: E_1^*, E_2^*
- (3) equations: $E_1 = R - G_2 E_2^*$
 $E_2 = G_1 E_1^* - H G_2 E_2^*$
 $C = G_2 E_2^*$
- $$\Rightarrow \left. \begin{aligned} E_1^* &= R^* - G_2^* E_2^* \\ E_2^* &= G_1^* E_1^* - (H G_2)^* E_2^* \\ C^* &= G_2^* E_2^* \end{aligned} \right\} \text{need to solve these}$$

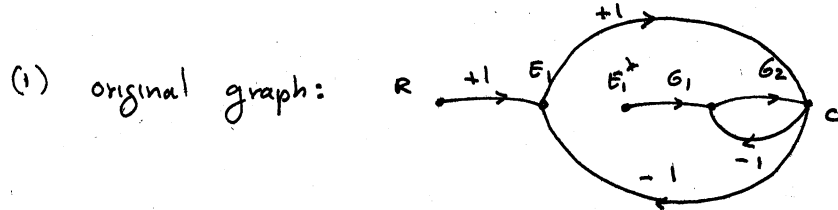
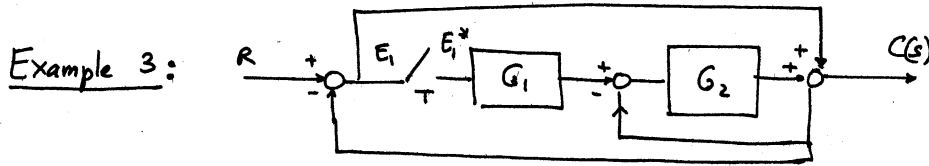
How do we solve these equations?

- (1) use Cramer's rule (tedious)
- (2) Use Mason's formula

To use Mason's formula we need to find the corresponding flow graph diagram: the sampler flow graph



$$\Delta = 1 + G_1^* G_2^* + (H G_2)^* \Rightarrow \boxed{\frac{C^*}{R^*} = \frac{G_1^* G_2^*}{1 + G_1^* G_2^* + (G_2 H)^*}}$$



(2) variables: E_1^*

(3) need to find E_1, C as functions of $R, E_1^* \Rightarrow$ use Mason's formula on the "original" graph:

$$\Delta = 1 + 1 + G_2 = 2 + G_2$$

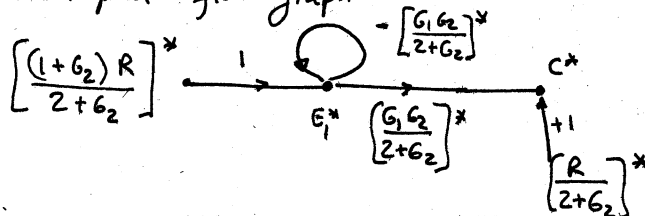
$$\frac{E_1}{R} = \frac{1 \cdot (1 + G_2)}{2 + G_2}, \quad \frac{E_1}{E_1^*} = \frac{-G_1 G_2}{2 + G_2} \Rightarrow \boxed{E_1 = \frac{(1 + G_2)}{2 + G_2} R - \frac{G_1 G_2}{2 + G_2} E_1^*} \quad (1)$$

$$\frac{C}{R} = \frac{1}{2 + G_2}; \quad \frac{C}{E_1^*} = \frac{G_1 G_2}{2 + G_2} \Rightarrow \boxed{C = \frac{1}{(2 + G_2)} R + \frac{G_1 G_2}{2 + G_2} E_1^*} \quad (2)$$

(4) Take starred transforms of (1) and (2): $E_1^* = \left[\frac{(1 + G_2)R}{2 + G_2} \right]^* - \left[\frac{G_1 G_2}{2 + G_2} \right]^* E_1^*$

$$C^* = \left[\frac{R}{2 + G_2} \right]^* + \left[\frac{G_1 G_2}{2 + G_2} \right]^* E_1^*$$

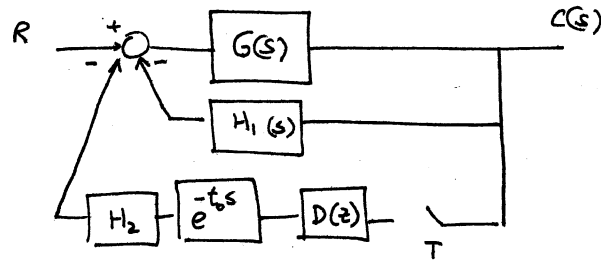
(5) sampled flow graph:



$$\Rightarrow \boxed{C^* = \left[\frac{R}{2 + G_2} \right]^* + \frac{\left[\frac{G_1 G_2}{2 + G_2} \right]^*}{1 + \left[\frac{G_1 G_2}{2 + G_2} \right]^*} \left[\frac{(1 + G_2)R}{2 + G_2} \right]^*}$$

Note: No transfer function exists from $R(z)$ to $C(z)$ since you can't factor R^* out. This was expected since the continuous time input $R(s)$ goes into the block $G_2(s)$ without going through a sampler

Example 3 :



A system containing a digital controller and non-negligible computation time:

- (1) (Assume $0 \leq t_0 < T$)

- (2) variable: C^*

$$(3) \quad C = \left(\frac{G}{1+GH_1} \right) R - \frac{GH_2 e^{-t_0 s} D^*}{1+GH_1} C^*$$

$$(4) \quad C^* = \left[\frac{GR}{1+GH_1} \right]^* - \left(\frac{GH_2 e^{-t_0 s}}{1+GH_1} \right)^* D^* C^*$$

modified z transform

$$C(z) = \left[\frac{GR}{1+GH_1} \right](z) - \left[\frac{GH_2}{1+GH_1} \right](z, m) \cdot D(z) C(z)$$

with $t_0 = \Delta T$
 $m = 1 - \Delta$
 $mT = T - t_0$

Solving this equation for $C(z)$ yields:

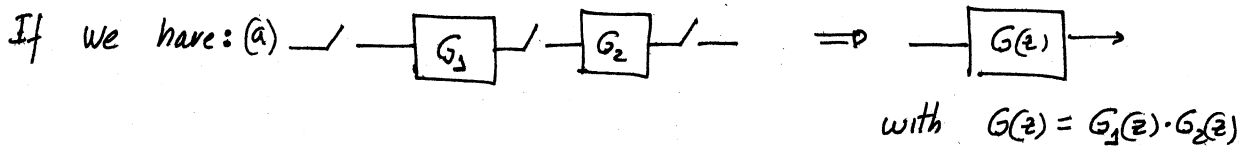
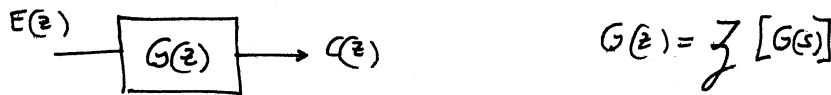
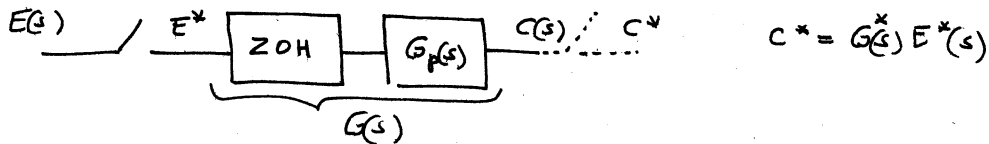
$$C(z) = \frac{\left[\frac{GR}{1+GH_1} \right](z)}{1 + \left[\frac{GH_2}{1+GH_1} \right](z, m) D(z)}$$

Idea of the system: wrap a stabilizing (continuous time) controller around the plant to guarantee stability.

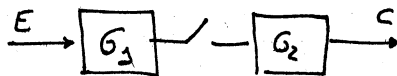
Use the digital filter to recover performance

Summary

Pulse Transfer function for sample data systems:



- Not all systems have a pulse transfer function:



This system does not have a pulse transfer function

- To get pulse T.F. you need to select as variables the inputs to the ideal samplers.

