

PHYSICS

21. 1cm of the scale at
- 30°C

$$= \{1 + (18 \times 10^{-6} \times 20)\} \text{ cm}$$

\therefore 60cm of the scale at 30°C

$$= 60 \{1 + 36 \times 10^{-5}\} = 60.02 \text{ cm}$$

- 22.
- $-\frac{dT}{dt} = \frac{K_2 A}{CL}(T - T_a)$
- through radiation &
- $-\frac{dT}{dt} = \frac{K_2 A}{CL}(T - T_a)$
- through conduction net rate of fall of temperature is

$$\left(-\frac{dT}{dt}\right)_{\text{net}} = \left(R_1 + \frac{K_2 A}{CL}\right)(T - T_a)$$

$$-\int \frac{dT}{(T - T_a)} = \int K_1 + \frac{K_2 A}{CL} dt$$

$$-\ln(T - T_a) \Big|_{400}^T = \left(K_1 + \frac{K_2 A}{CL}\right)t$$

$$\ln\left(\frac{T - T_a}{400 - T_a}\right) = -t\left(K_1 + \frac{K_2 A}{CL}\right)$$

$$\frac{T - 300}{100} = e^{-t\left[K_1 + \frac{K_2 A}{CL}\right]}$$

$$T(t) = 300 + 100e^{-t\left[K_1 + \frac{K_2 A}{CL}\right]}$$

23. At the interface between ice and water
- $T_x = 0^\circ\text{C}$
- . Then
- $R_1 T_2 + R_2 T_1 = 0$
- , or

$$k_1 T_1 / L_1 + k_2 T_2 / L_2 = 0. \text{ Not only that, } L_1 + L_2 = L, \text{ so}$$

$$k_1 T_1 L_2 + (L - L_2) k_2 T_2 = 0,$$

$$\text{So } L_2 = \frac{(1.42 \text{ m})(1.67 \text{ W / m.K})(-5.20^\circ\text{C})}{(1.67 \text{ W / m.K})(-5.20^\circ\text{C}) - (0.502 \text{ W / m.K})(3.98^\circ\text{C})} = 1.15 \text{ m}.$$

24. a.
- $6T_1 = 3T_2 = 2T_4 = T_3 = 1800 \text{ K}$

$$T_1 = 300 \text{ K}; T_2 = 600 \text{ K}$$

$$T_4 = 900 \text{ K}; T_3 = 1800 \text{ K}$$

$4 \rightarrow 1$ and $2 \rightarrow 3$ are isochoric processes in which work done = 0

$$W_{12} = P(V_2 - V_1) = nR(T_2 - T_1) = 2 \times R(600 - 300) = 600R$$

$$W_{34} = P(V_4 - V_3) = nR(T_4 - T_3) = 2 \times R(900 - 1800) = -1800R$$

$$W_{\text{Total}} = 600R - 1800R = -1200R = -10000 \text{ J}$$

25. c.

$$\frac{\Delta Q}{\Delta t} = \frac{KA\Delta T}{\Delta x} \quad \Delta Q = KA\left(\frac{\Delta T}{\Delta x}\right)\Delta t$$

Assuming the thickness of the spheres to be small, we have for smaller sphere:

(rate of heat flow) (time) = (volume of ice melted) (ρL)

$$\text{i.e., } K_1(4\pi r^2)\frac{\Delta\theta}{d}.16 = \frac{4}{3}\pi r^3 \rho L \quad (i)$$

For larger sphere:

$$K_2 \left[4\pi (2r)^2 \right] \frac{\Delta\theta}{d/4} \cdot 25 = \frac{4\pi}{3} (2r)^3 \rho L \quad (ii)$$

Dividing Eq. (ii) by Eq. (i),

$$K_2 / K_1 = 8/25.$$

26. b. Evidently the initial temperature of the water contained in the vessel (Mg) is 80°C , and the temperature of the water passed into it is 60°C , as the final temperature of the mixture tends to attain a value of 60°C .

$$M \times 1(80 - 70) = m \times 10 \times 1(70 - 60)$$

or,

$$M / m = 10$$

since the heat exchanged after a long time is 800 cal.

$$(Mg)(1 \text{ cal} / \text{g}^\circ\text{C})(80 - 60^\circ\text{C}) = 800 \text{ cal}$$

or,

$$M = 40 \text{ g}$$

$$\Rightarrow m = 4 \text{ g}$$

27. b. Heat given to the metal

$$dQ = P dt = C_p(t) dT \quad (i)$$

At constant pressure in time interval at

$$\text{Given} \quad T = T_0 [1 + a(t - t_0)]^{1/4}$$

$$\frac{dT}{dt} = \frac{T_0}{4} [1 + a(t - t_0)]^{-3/4} \times a \quad (ii)$$

From Eqs. (i) and (ii)

$$C_p(T) = \frac{P}{\left(\frac{dT}{dt}\right)} = \frac{4P[1 + a(t - t_0)]^{3/4}}{T_0 a} = \frac{4PT^3}{aT_0^4}$$

28. b. Let m be the mass of ice.

Rate of heat given by the burner is constant.

In the first 50 min

$$\frac{dQ}{dt} = \frac{mL}{t_3} = \frac{m \text{ kg} \times (80 \times 4.2 \times 10^3) \text{ J} / \text{kg}}{(50 \text{ min})} \quad (i)$$

From 50 min to 60 min

$$\begin{aligned} \frac{dQ}{dt} &= \frac{(m+5)S_{H_2O}\Delta\theta}{t_2} \\ &= \frac{(m+5) \text{ kg} (4.2 \times 10^3) \text{ J} / \text{kg} \times 2^\circ\text{C}}{10 \text{ min}} \quad (ii) \end{aligned}$$

From Eqs. (i) and (ii)

$$\frac{80m}{50} = \frac{2(m+5)}{10}$$

$$7m = 5 \Rightarrow m = \frac{5}{7} \text{ kg} = 0.7 \text{ kg}$$

29. Freezing water to ice is a process with Q being negative volume of system increases $\Rightarrow W_{\text{system}}$ is positive using $Q = \Delta U + W \Rightarrow \Delta U$ is negative.

30. $\frac{x-0}{100} = \frac{-x-32}{180} \Rightarrow x = -\frac{80}{7}^{\circ}\text{C}$ or $\frac{80}{7}^{\circ}\text{F}$

31. (A) Area under the curve is equal to number of molecules of the gas sample

$$\text{Area} = \frac{av_0}{2} = N$$

(B) $V_{\text{avg}} = \frac{\int V dN}{\int dN} = \frac{\int_0^{v_0} \frac{a}{V_0} V dV}{\int_0^{v_0} \frac{a}{V_0} V dV} = \frac{V^{\frac{2}{3}}}{\frac{V^2}{2}} \Big|_0^{v_0} = \frac{2}{3} V_0$

(C) $V_{\text{rms}}^2 = \frac{\int V^2 dN}{\int dN} = \frac{\int_0^{v_0} V^2 \frac{a}{V_0} V dV}{\int_0^{v_0} \frac{a}{V_0} V dV} = \frac{V^{\frac{4}{3}}}{\frac{V^2}{2}} \Big|_0^{v_0} = \frac{V_0^2}{2}$

(D) Area under curve from $\frac{V_0}{2}$ to V_0 is $\frac{3}{4}$ of total area

32. Conceptual

33. Rate of heat conduction through rod = rate of the heat lost from right end of the rod.

$$\frac{KA(T_1 - T_2)}{L} = eA\sigma(T_2^4 - T_s^4) \quad (i)$$

Given that $T_2 = T_s + \Delta T$

$$T_2^4 = (T_s + \Delta T)^4 = T_s^4 \left(1 + \frac{\Delta T}{T_s}\right)^4$$

Using binomial expansion, we have

$$T_2^4 = T_s^4 \left(1 + 4\frac{\Delta T}{T_s}\right) \quad (\text{as } \Delta T \ll T_s)$$

$$T_2^4 - T_s^4 = 4(\Delta T)(T_s^3)$$

Substituting in Eq. (i), we have

$$\frac{K(T_1 - T_s - \Delta T)}{L} = 4e\sigma T_s^3 \Delta T$$

$$\frac{K(T_1 - T_s)}{L} = \left(4e\sigma T_s^3 + \frac{K}{L}\right) \Delta T$$

$$\Delta T = \frac{K(T_1 - T_s)}{(4e\sigma L T_s^3 + K)}$$

Comparing with the given relation, proportionality constant

$$= \frac{K}{4e\sigma L T_s^3 + K}$$

34. Let l be side of cube at initial temperature and d the depth of cube submerged. Then according law of floatation

Weight of solid = weight of liquid displaced

$$\therefore Mg = l^2 d \rho_l g$$

But $l' = l(1 + \alpha_s \Delta T), \rho_l = \frac{\rho_l}{1 + \gamma_l \Delta T}$

Substituting these values in Eq. (iii), we get

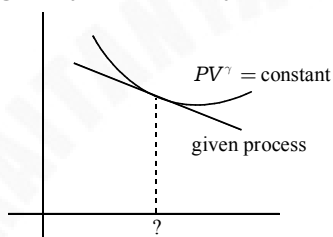
$$l^2 d\rho_l g = l^2 (1 + \alpha_s \Delta T)^2 \frac{\rho_l}{1 + \gamma_l \Delta T} g \Rightarrow 1 + \gamma_l \Delta T = (1 + \alpha_s \Delta T)^2$$

As $\alpha_s \Delta T \ll 1$, using binomial theorem

$$1 + \gamma_l \Delta T = 1 + 2\alpha_s \Delta T \Rightarrow \gamma_l = 2\alpha_s$$

35. The given process will be tangent to an adiabat as shown. We have to find that point

of tangency as it obeys $dQ = 0$. At this point dQ changes sign.



Equation of process is $\frac{P}{P_0} + \frac{V}{V_0} = 1 \Rightarrow P = P_0 \left(1 - \frac{V}{V_0}\right)$

Slope of process $= -\frac{P_0}{V_0}$

Let us assume required volume is V_1

Slope of adiabat at this volume is $-\frac{\gamma P_1}{V_1} = -\frac{\gamma P_0 \left(1 - \frac{V_1}{V_0}\right)}{V_1}$

But this should be equal to $-\frac{P_0}{V_0}$

$$\Rightarrow -\frac{P_0}{V_0} = -\frac{\gamma P_0 \left[1 - \frac{V_1}{V_0}\right]}{V_1}$$

$$\Rightarrow \frac{V_1}{V_0} = \gamma \left[1 - \frac{V_1}{V_0}\right] \Rightarrow V_1 = \frac{V_0 \gamma}{1 + \gamma} = \frac{5V_0}{8}$$

36. The heat current is given as

$$i = -KA \frac{dT}{dx}$$

Putting $K = \alpha \sqrt{T}$, where $\alpha = \text{constant}$, We have

$$i = -\alpha \sqrt{T} A \frac{dT}{dx}$$

or $idx = -\alpha A \sqrt{T} dT$

Integrating both sides

$$i \int_0^x dx = -\alpha A \int_{T_1}^T \sqrt{T} dT$$

$$\text{or } ix = -\frac{2}{3}\alpha A(T^{3/2} - T_1^{3/2})$$

$$\text{or } ix = \frac{2}{3}\alpha A(T_1^{3/2} - T^{3/2})$$

putting $x = l$ and $T = T_2$, we have

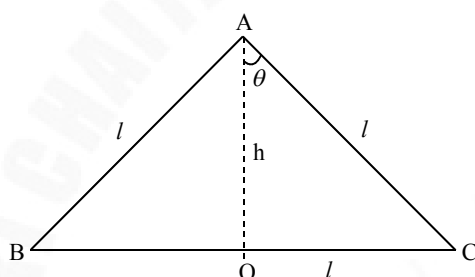
$$il = \frac{2}{3}\alpha A(T_1^{3/2} - T_2^{3/2})$$

On dividing eqn (i) by eqn. (ii),

$$\frac{x}{l} = \frac{T_1^{3/2} - T^{3/2}}{T_1^{3/2} - T_2^{3/2}}$$

$$\text{or } T = T_1 \left[1 + \frac{x}{l} \left[(T_2 / T_1)^{3/2} - 1 \right] \right]$$

37.



$$h^2 = l^2 - l^2 / 4 = \frac{3}{4}l^2$$

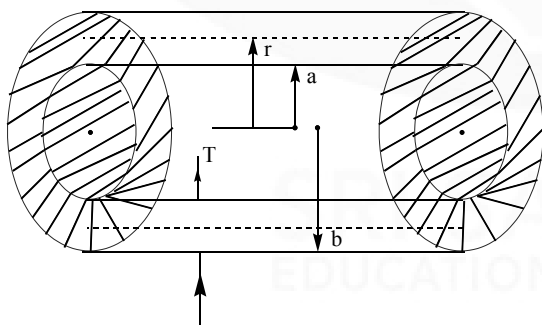
$$2h = \frac{dh}{dT} = \frac{3}{4}2l \frac{dl}{dT}$$

$$y_{cm} = \frac{1}{3}h$$

$$\frac{dy_{cm}}{dT} = \frac{1}{3} \frac{dh}{dT} = \frac{1}{3} \cdot \frac{3}{4} \cdot \frac{l}{h} \frac{dl}{dT}$$

$$= \frac{1}{4} 2 \tan 30^\circ l_0 \alpha = \frac{1}{2\sqrt{3}} 2 \times 4\sqrt{3} 10^{-6}$$

38.



At any instant let "P" be the power entered into the cylinder, $P = K 2\pi r l \left(\frac{-dT}{-dr} \right)$;

where "r" is the radius of any cylindrical layer between 'a' and 'b'.

$$P = K 2\pi l \Delta T \ln(b/a).$$

ΔT is the instantaneous temperature different of body with surroundings.

$$\text{Then } P = \pi a^2 Sl \frac{dT}{dt} = K 2\pi l \Delta T \ln\left(\frac{b}{a}\right)$$

$$\text{or } t = \frac{\pi a^2 Sl}{K 2\pi l \ln\left(\frac{b}{a}\right)} \ln\left(\frac{T_0 - T_2}{T_0 - T_1}\right)$$

$$t = \frac{Sa^2}{2K} \ln\left(\frac{b}{a}\right) \ln\left(\frac{T_0 - T_1}{T_0 - T_2}\right)$$

$$39. \quad P_1 V = N_1 k T_1$$

$$P_2 V = N_2 k T_2 \quad \text{and } N_2 = 0.8N_1 + 2(0.2N_1) = 1.2N_1$$

$$\frac{P_2}{P_1} = (1.2) \left(\frac{T_2}{T_1}\right) = (1.2)(1.01) \approx 1.21$$

$$U_1 = \frac{f_1}{2} N_1 k T_1 \quad \text{and } U_2 = \frac{f_1}{2} 0.8N_1 k T_2 + \frac{f_2}{2} (2)(0.2N_1) k T_2$$

Where $f_1 = 5$ and $f_2 = 3$ for diatomic and monoatomic gas respectively.

$$\Rightarrow \frac{U_2}{U_1} = 1.04 \frac{T_2}{T_1} = 1.05$$

$$C_v = \frac{n_1 C_{v1} + n_2 C_{v2}}{n_1 + n_2} = \frac{0.8 \left(\frac{5R}{2}\right) + 0.4 \left(\frac{3R}{2}\right)}{1.2} = \frac{13R}{6}$$

$$\% \text{ increase in } C_v = \left(\frac{\frac{13}{6}}{\frac{5}{2}} - 1 \right) \times 100 = \frac{-2}{15} \times 100$$

$$C_p = C_v + R = \frac{19R}{6}$$

$$\% \text{ increase in } C_p = \left(\frac{\frac{19}{6}}{\frac{7}{2}} - 1 \right) \times 100 = \frac{-2}{21} \times 100$$

$$\text{Difference} = \left(\frac{2}{15} - \frac{2}{21} \right) \times 100 = \frac{200 \times 6}{15 \times 21} = \frac{80}{21} \approx 4$$