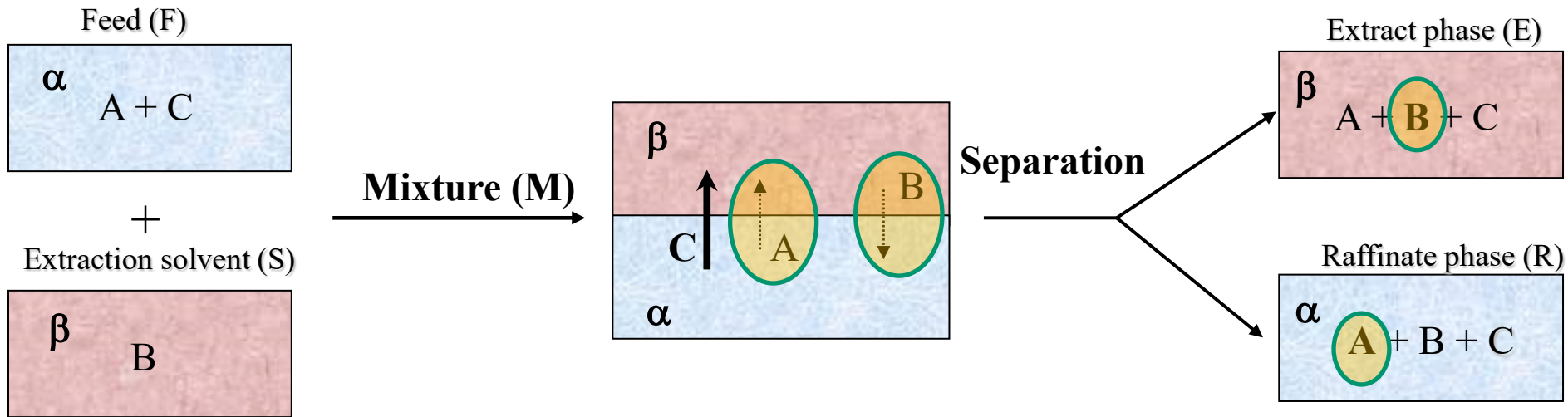


# Liquid – Liquid Extraction

Processos de Separação

LEQB

2023/2024

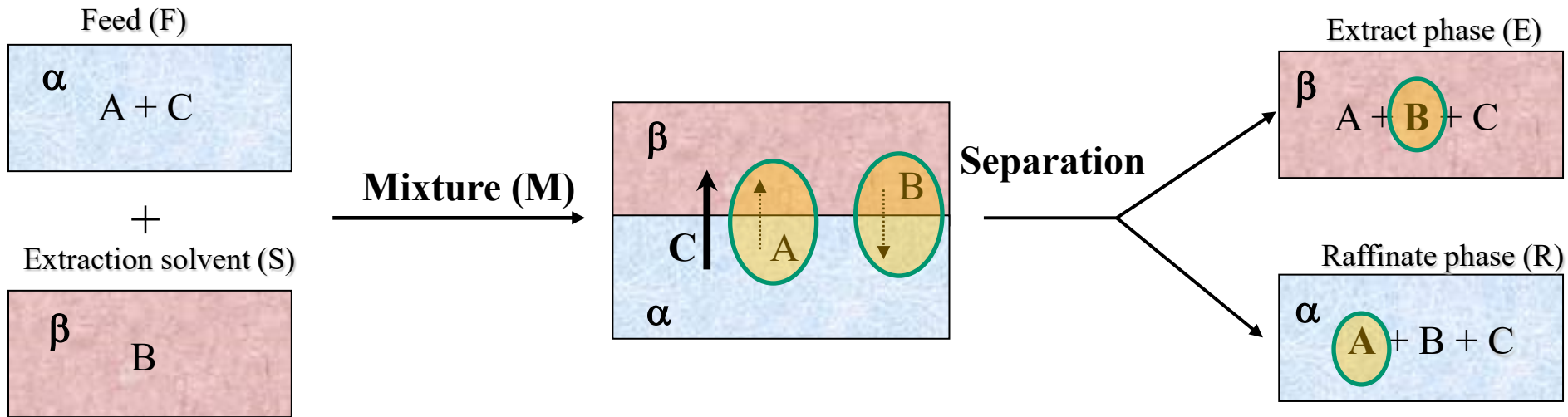


Solvents  $A$  and  $B$  are  
**partially miscible**

**A: Water** (diluent)

**C: Acetone** (solute)

**B: *n*-Hexane** (solvent)



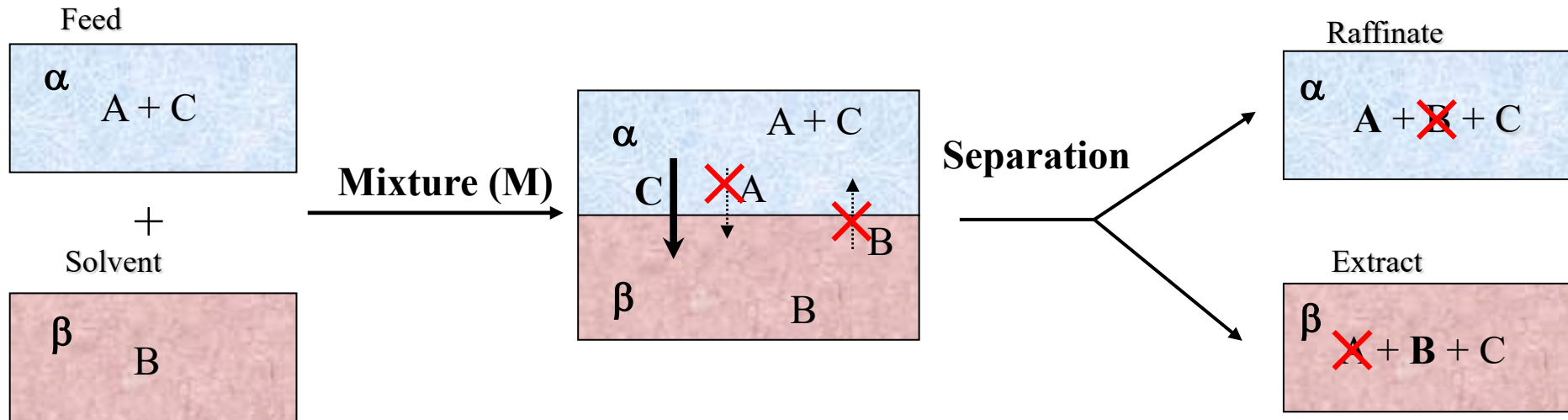
What if the solvents were  
“totally” immiscible?

A: **Water** (diluent)

C: **Acetone** (solute)

B: ***n*-Hexane** (solvent)

# Solvents "totally" immiscible



A – **Water** (diluent)

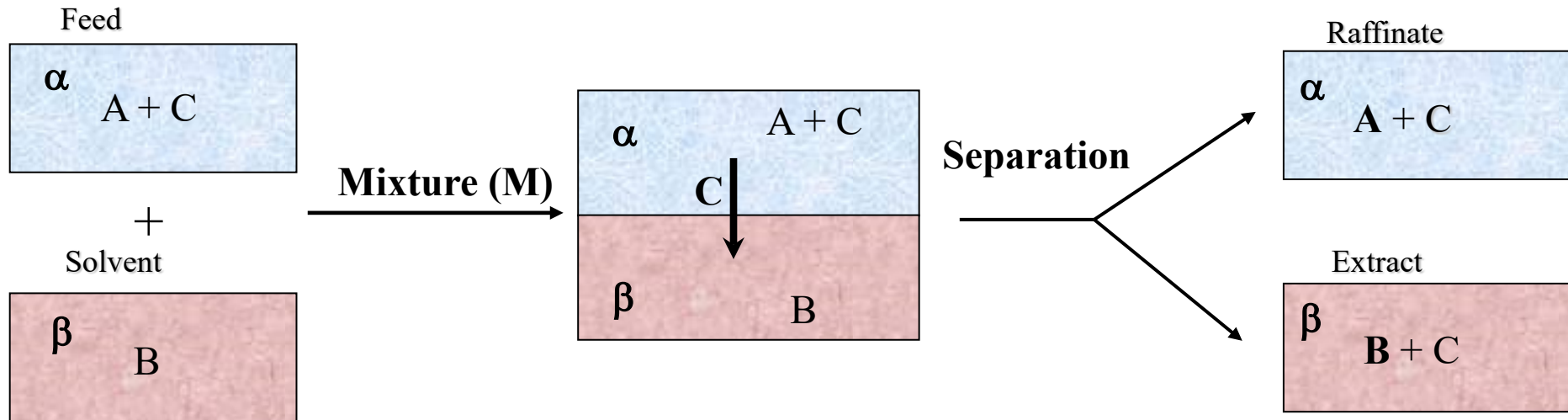
C – **Nicotine** (solute)

B – **Kerosene** (solvent)

Water / kerosene: **immiscible**

The generic term "kerosene" is used to describe the fraction of crude oil that boils approximately in the range of 302 to 554 °F (150 to 290°C) and consists of hydrocarbons approximately in the range of C9-C16

# Solvents "totally" immiscible



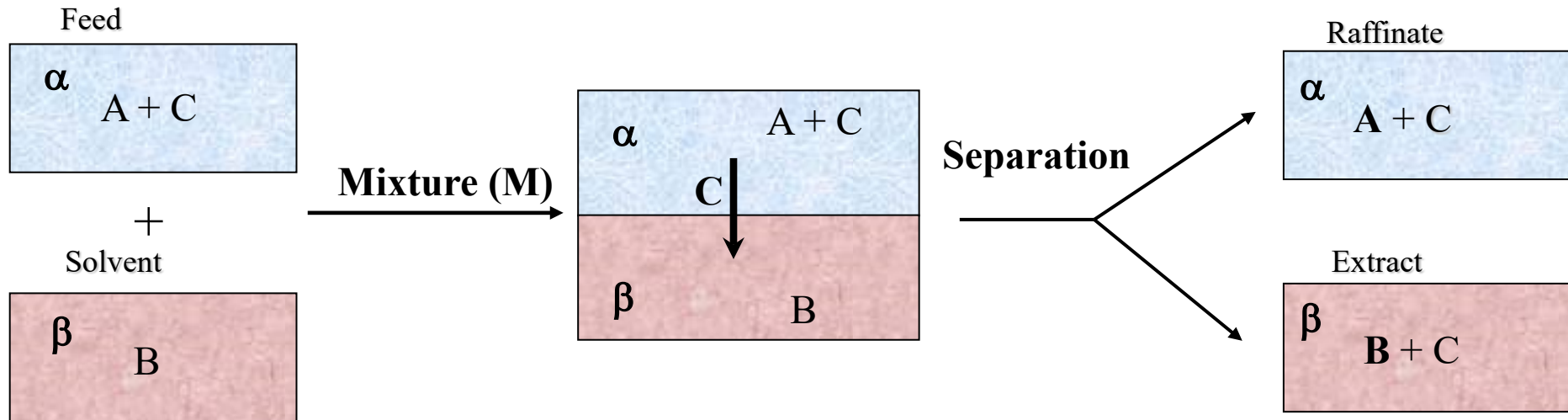
**A – Water (diluent)**

**C – Nicotine (solute)**

**B – Kerosene (solvent)**

Water / kerosene: **immiscible**

# Solvents "totally" immiscible



**A – Water (diluent)**

**C – Nicotine (solute)**

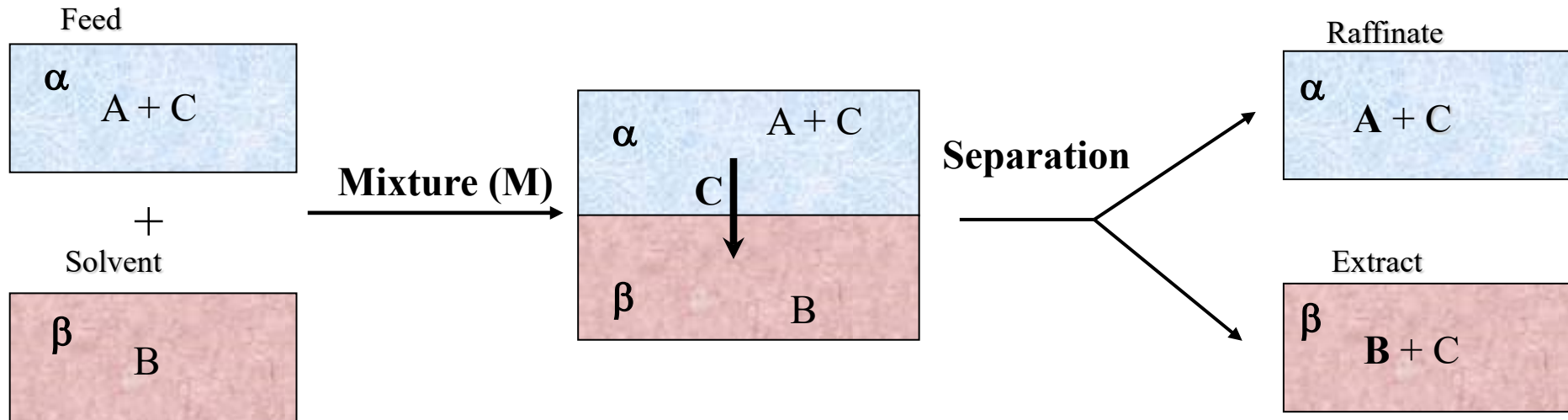
**B – Kerosene (solvent)**

Solute-free compositions

$$x', y' = \frac{m_C}{(m_A + m_B)}$$

Solute-free flowrates

# Solvents "totally" immiscible



A – Water (diluent)

C – Nicotine (solute)

B – Kerosene (solvent)

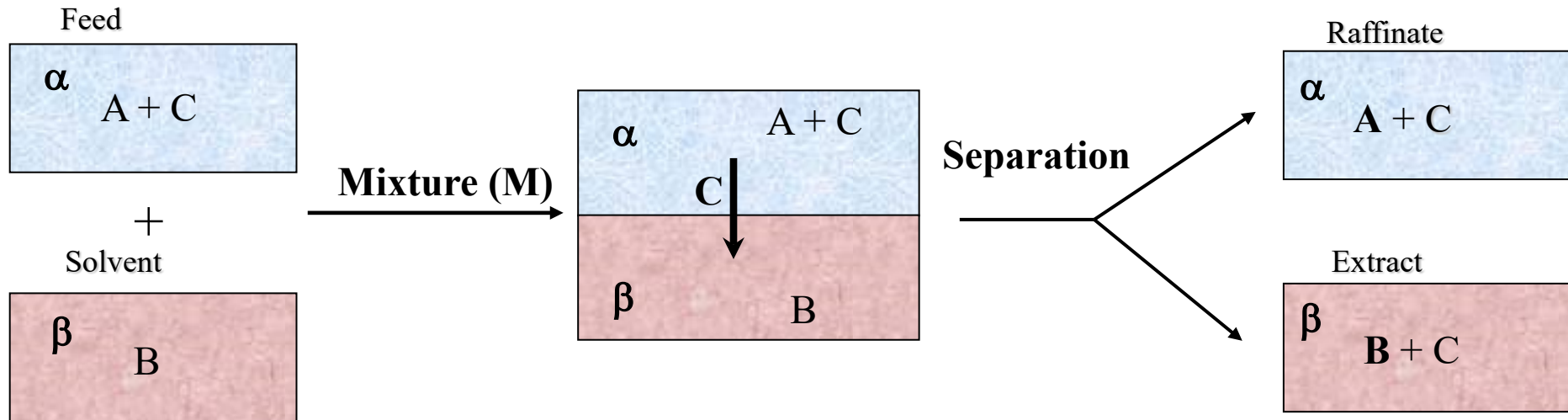
Solute-free compositions

$$x' = \frac{m_C}{(m_A + \cancel{m_B})} \Big|_{\text{raffinate}} \quad y' = \frac{m_C}{(\cancel{m_A} + m_B)} \Big|_{\text{extract}}$$

$\underset{=0}{\quad}$        $\underset{=0}{\quad}$

Solute-free flowrates

# Solvents "totally" immiscible



**A – Water (diluent)**

**C – Nicotine (solute)**

**B – Kerosene (solvent)**

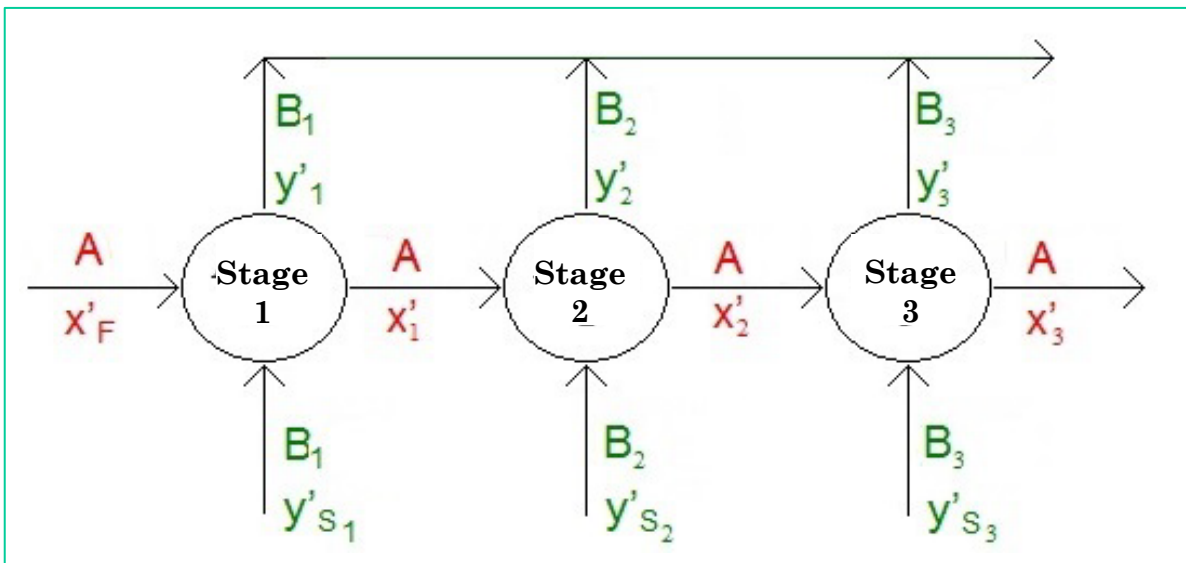
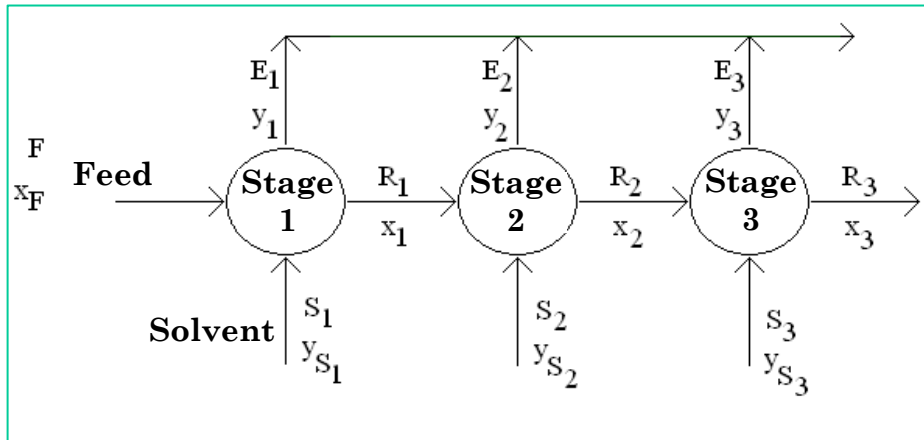
Solute-free compositions

$$x' = \left. \frac{m_C}{m_A} \right|_{\text{raffinate}} \quad y' = \left. \frac{m_C}{m_B} \right|_{\text{extract}}$$

Solute-free flowrates



# Cross flow extraction - A and B totally immiscible

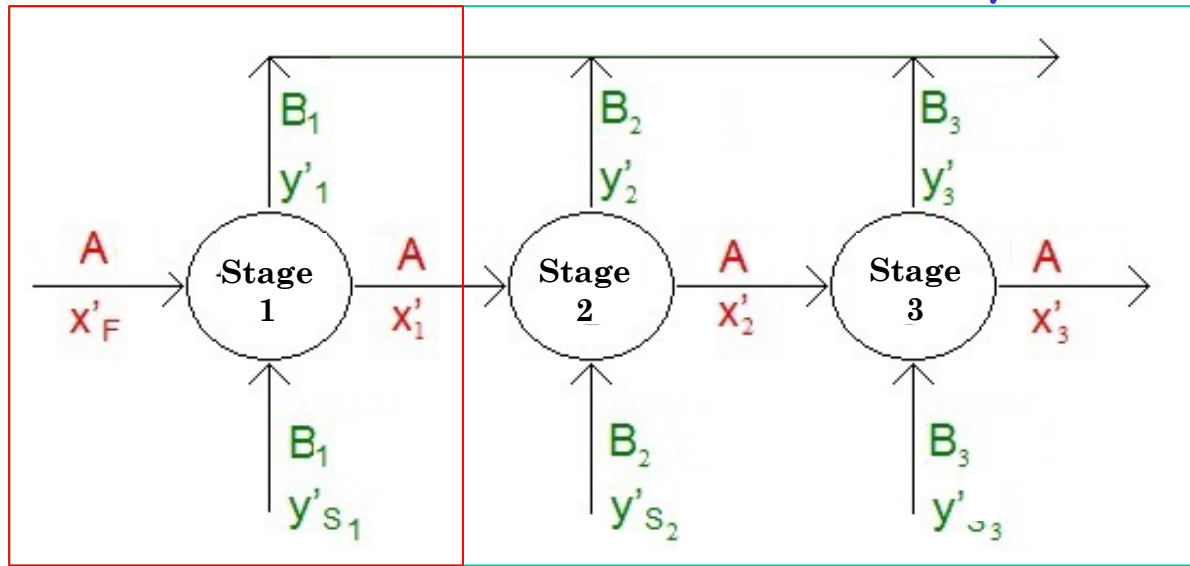


A: solute-free raffinate phase flowrates (kg<sub>A</sub>/h)

B<sub>n</sub>: solute-free extract phase flowrates (kg<sub>B</sub>/h)

$$x' = \frac{m_C}{m_A} \quad y' = \frac{m_C}{m_B}$$

# Cross flow extraction - A and B totally immiscible



$$x' = \frac{m_C}{m_A}$$

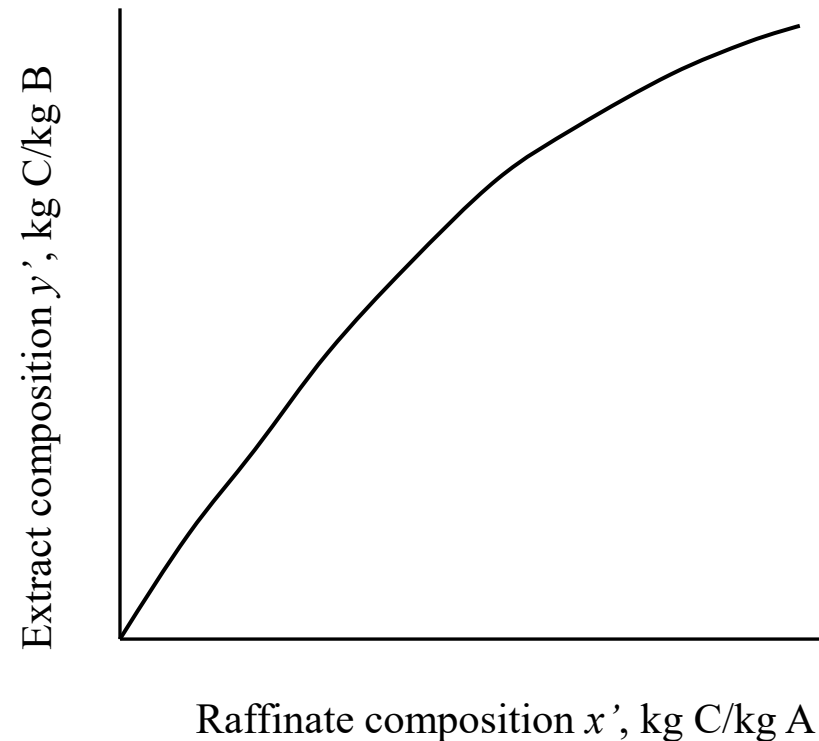
$$y' = \frac{m_C}{m_B}$$

## Material balance to solute (stage 1)

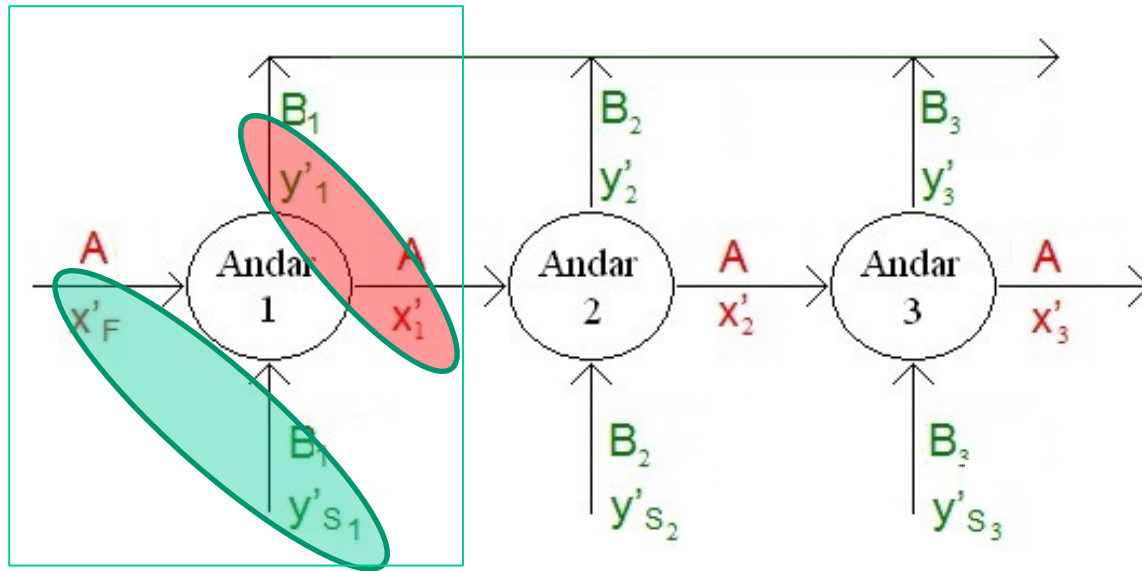
Solute-free compositions:

$$A x'_F + B_1 y'_{S1} = A x'_1 + B_1 y'_1$$

$$\Rightarrow \boxed{-\frac{A}{B_1} = \frac{y'_S - y'_1}{x'_F - x'_1}} \quad \text{Operating line}$$



# Cross flow extraction - A and B totally immiscible



$$x' = \frac{m_C}{m_A}$$

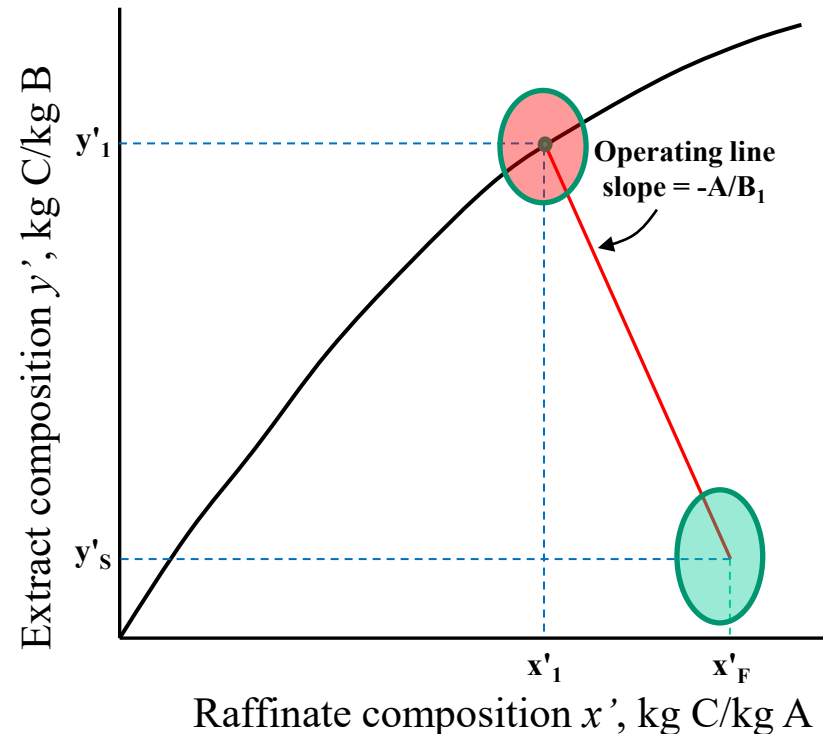
$$y' = \frac{m_C}{m_B}$$

## Material balance to solute (stage 1)

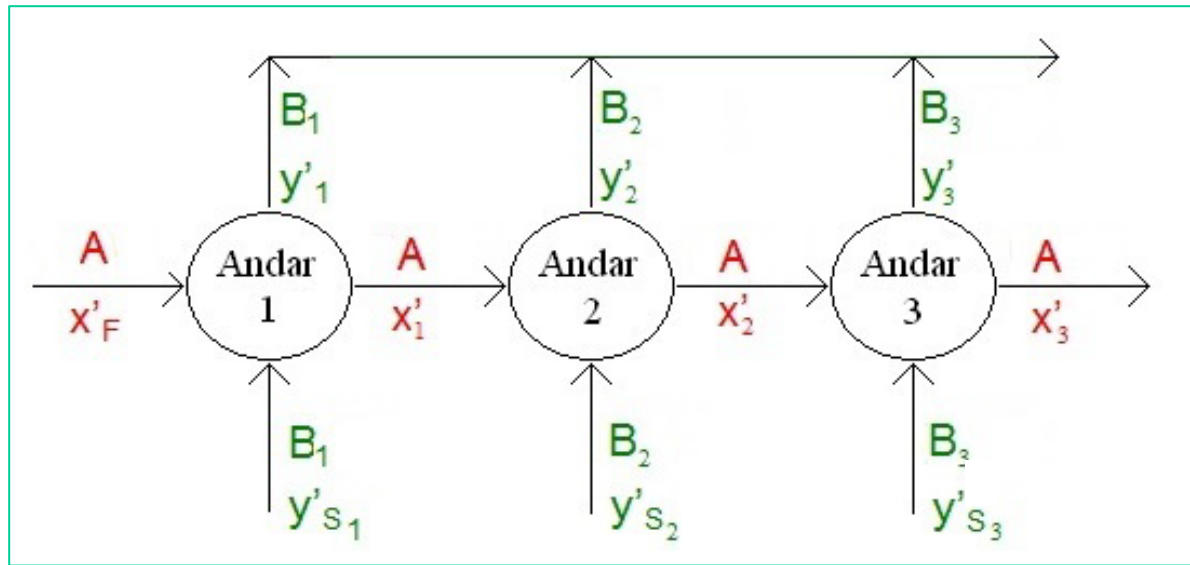
Solute-free compositions:

$$A x'_F + B_1 y'_S = A x'_1 + B_1 y'_1$$

$$\Rightarrow -\frac{A}{B_1} = \frac{y'_S - y'_1}{x'_F - x'_1} \quad \text{Operating line}$$



# Cross flow extraction - A and B totally immiscible



$$x' = \frac{m_C}{m_A}$$

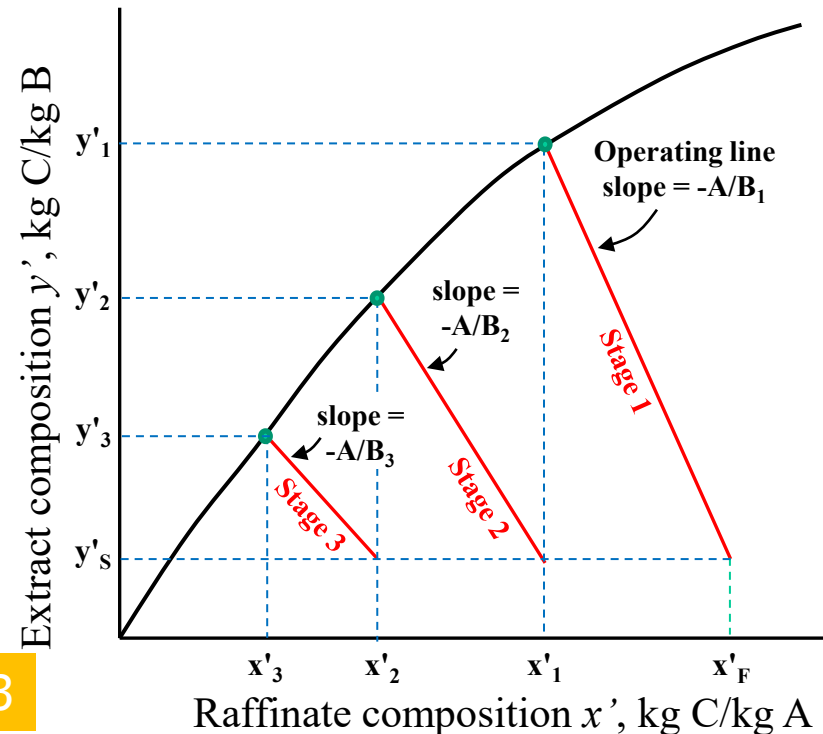
$$y' = \frac{m_C}{m_B}$$

## Material balance to solute (stage 1)

Solute-free compositions:

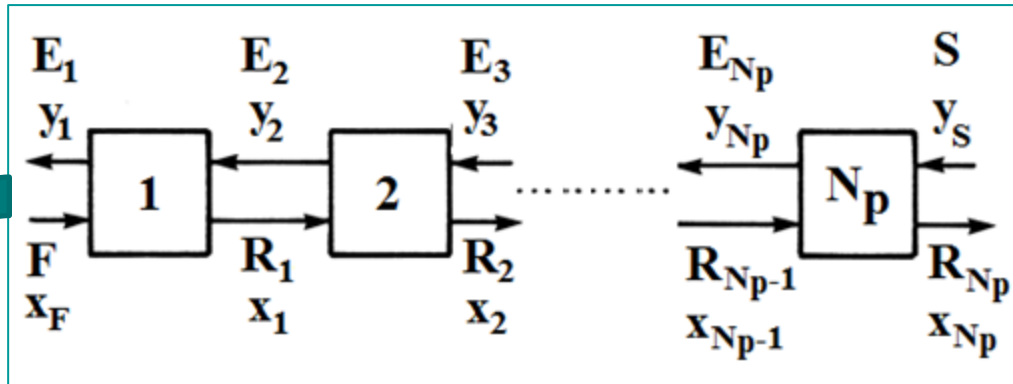
$$A x'_F + B_1 y'_S = A x'_1 + B_1 y'_1$$

$$\Rightarrow \boxed{-\frac{A}{B_1} = \frac{y'_S - y'_1}{x'_F - x'_1}} \quad \text{Operating line}$$



PROBLEM 3

### 3. Countercurrent extraction

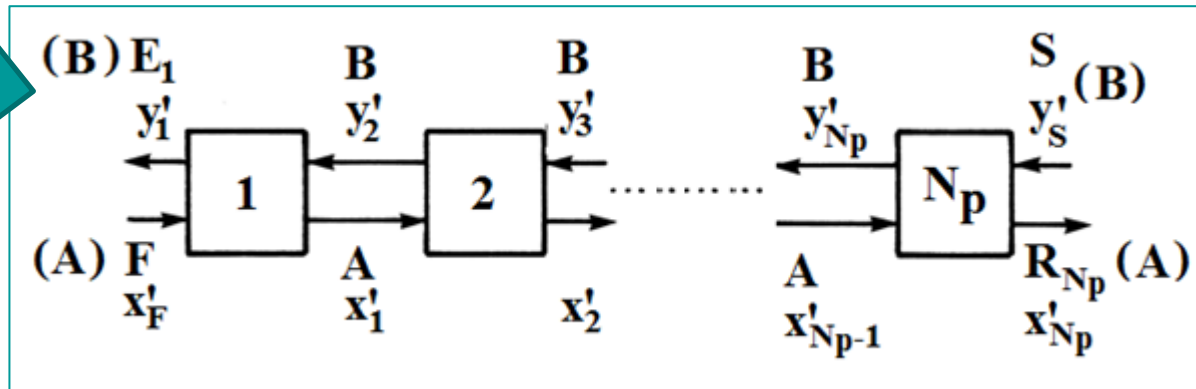


Solvents partially miscible

$A$ : solute-free raffinate phase flowrates ( $\text{kg}_A/\text{h}$ )

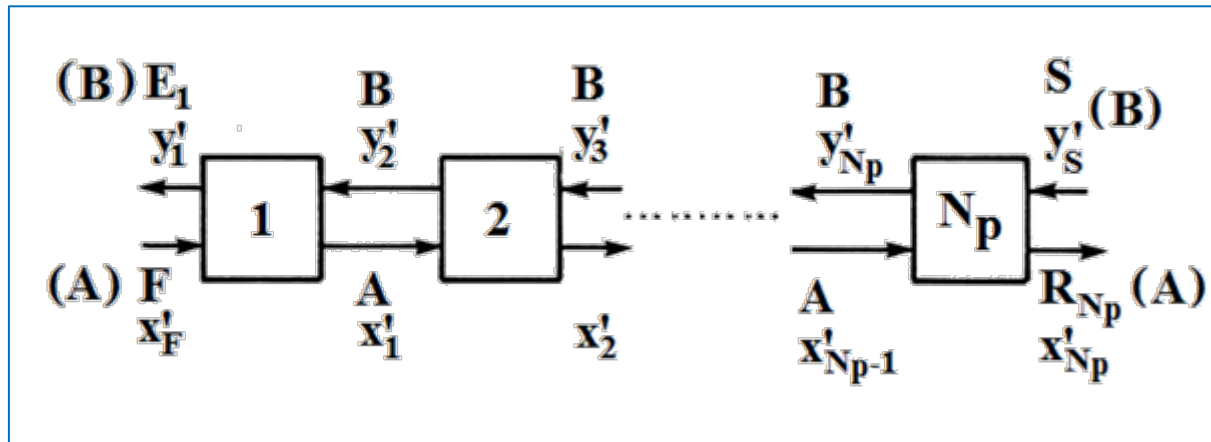
$B_n$ : solute-free extract phase flowrates ( $\text{kg}_B/\text{h}$ )

Solute-free compositions



Solvents  
"totally"  
immiscible

### 3. Countercurrent extraction



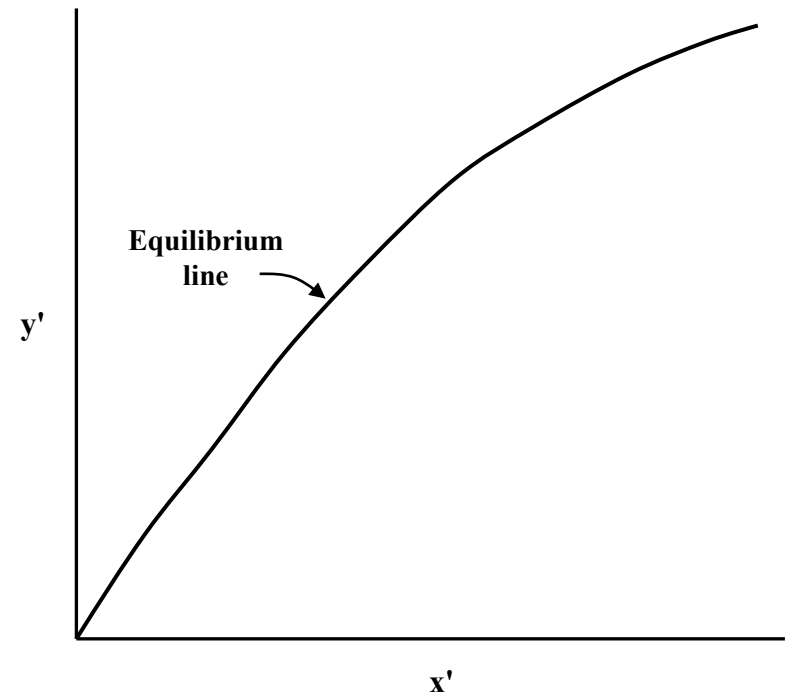
#### Overall material balance to solute

Solute-free compositions:

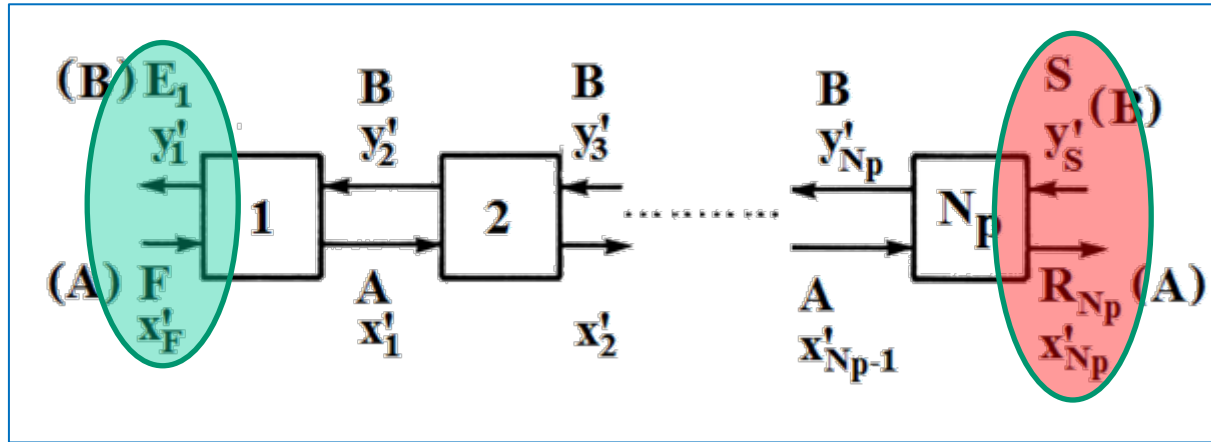
$$A x'_F + B y'_S = A x'_N + B y'_1$$

=> Operating line

$$\frac{A}{B} = \frac{y'_1 - y'_S}{x'_F - x'_N}$$



### 3. Countercurrent extraction



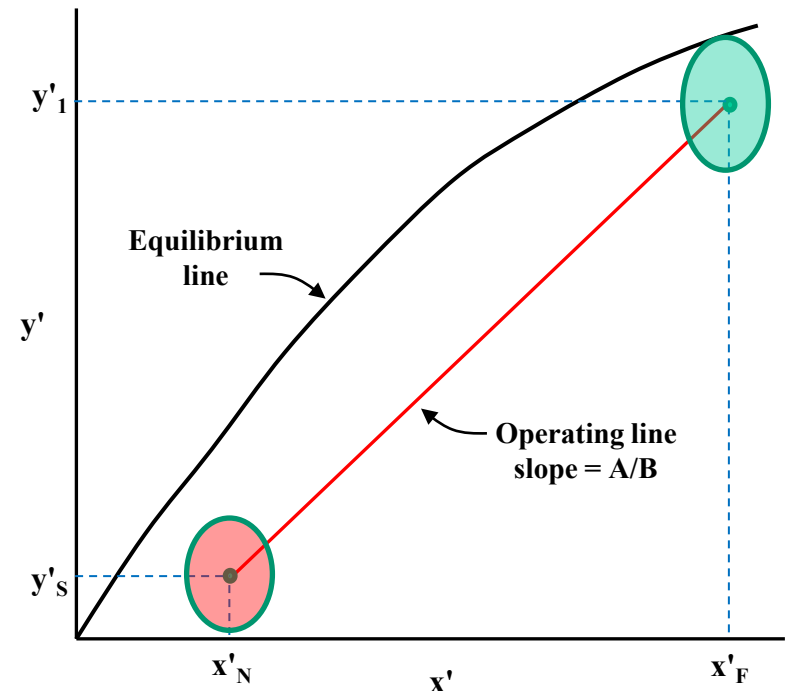
#### Overall material balance to solute

Solute-free compositions:

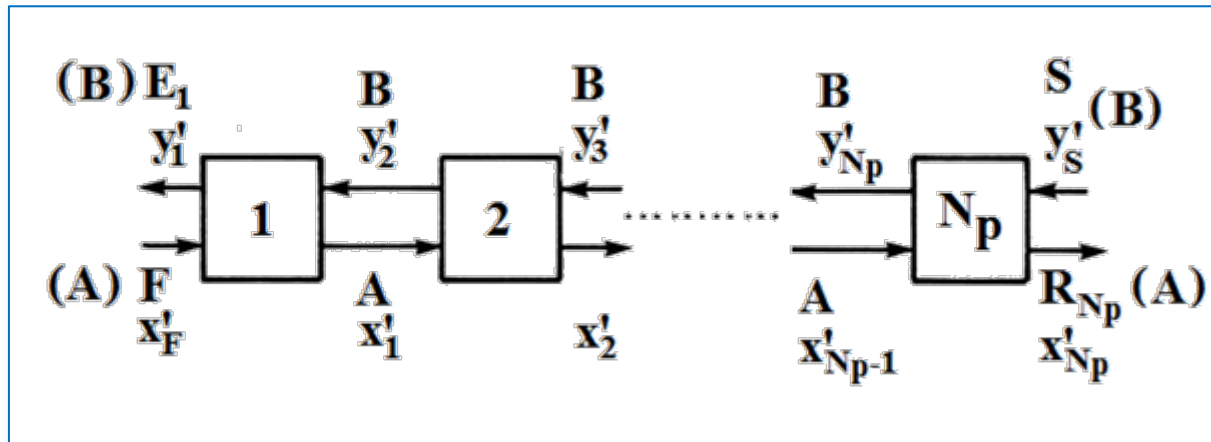
$$A x'_F + B y'_S = A x'_N + B y'_1$$

=> Operating line

$$\frac{A}{B} = \frac{y'_1 - y'_S}{x'_F - x'_N}$$



### 3. Countercurrent extraction



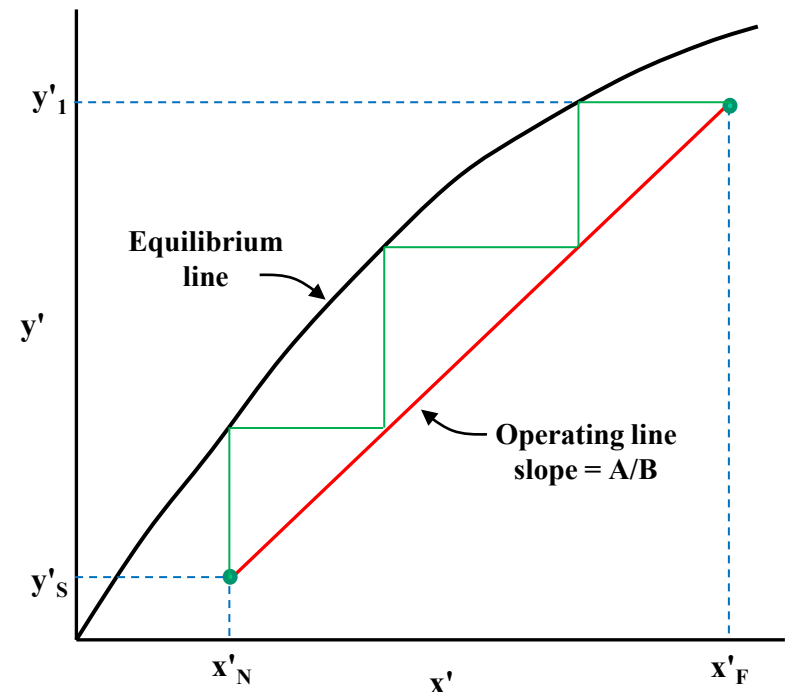
#### Overall material balance to solute

Solute-free compositions:

$$A x'_F + B y'_S = A x'_N + B y'_1$$

=> Operating line

$$\frac{A}{B} = \frac{y'_1 - y'_S}{x'_F - x'_N}$$

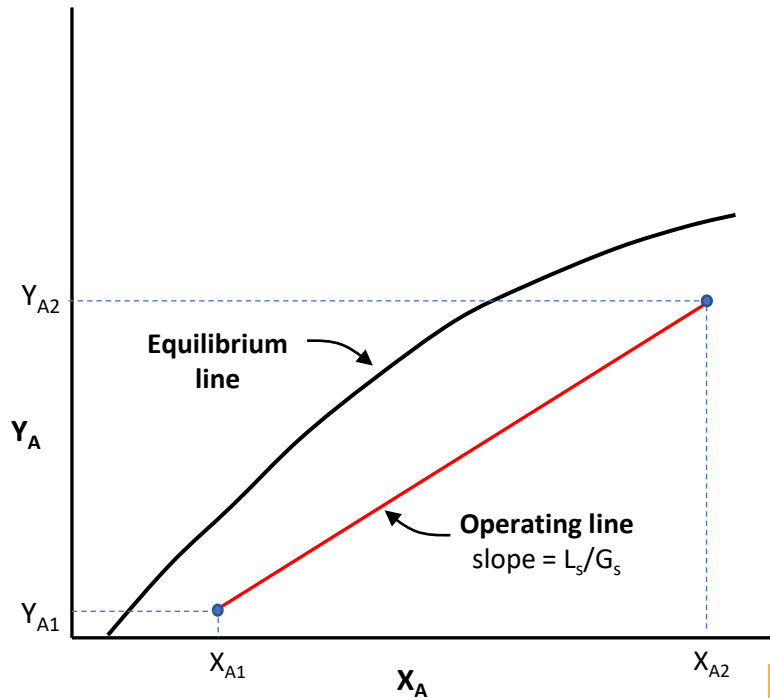
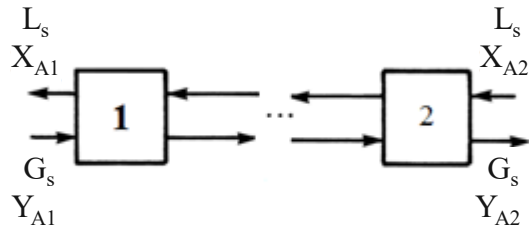




## Gas absorption - Stripping

Operating line

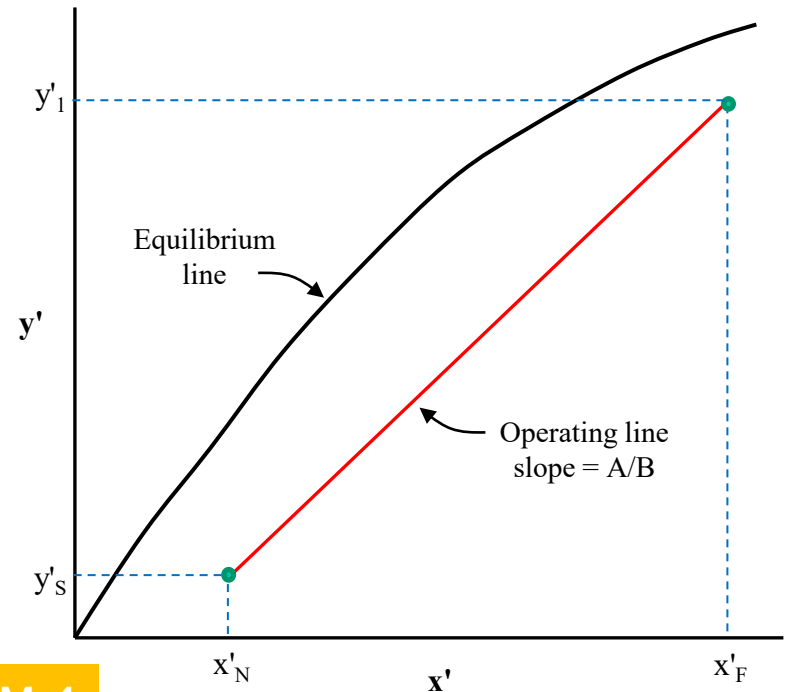
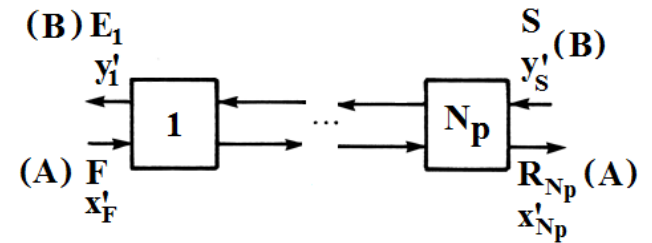
$$\frac{L_s}{G_s} = \frac{Y_{A1} - Y_{A2}}{X_{A1} - X_{A2}}$$



## Countercurrent extraction

Operating line

$$\frac{A}{B} = \frac{y'_1 - y'_S}{x'_F - x'_N}$$

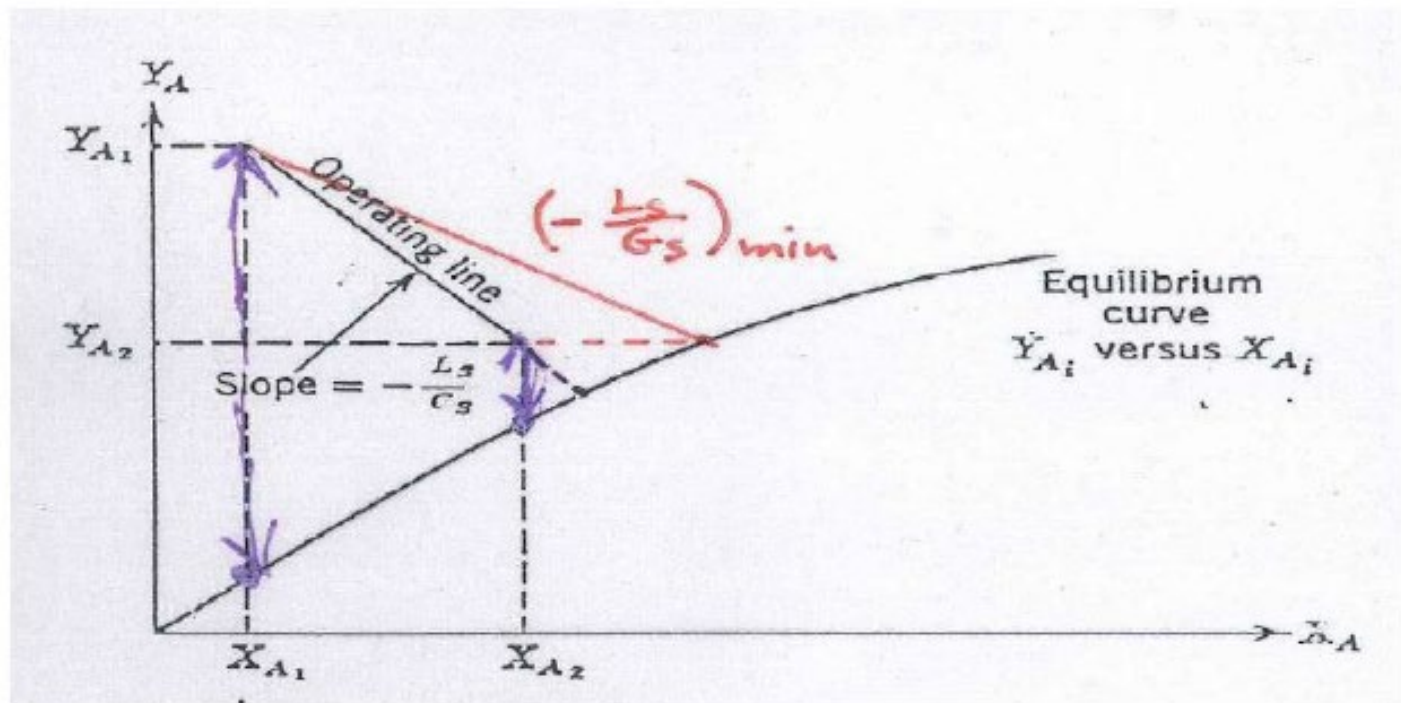


PROBLEM 4



# Absorção - Caudal mínimo

Fluxo em cocorrente



# Absorção Gasosa

## Fluxo em contracorrente

