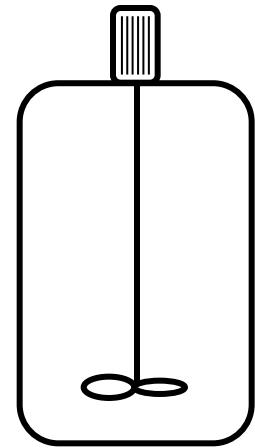


# **Dimensionamento de reactores isotérmicos**

# Dimensionamento de reactores isotérmicos

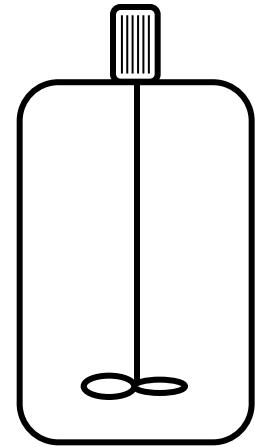
## Reactor Batch



# Dimensionamento de reactores isotérmicos

## Reactor Batch

Balanço molar     $r_A V = \frac{dN_A}{dt}$                    $N_A = N_{A0} (1 - X)$

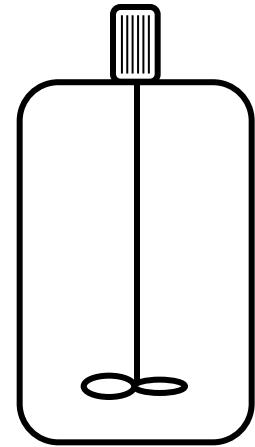


# Dimensionamento de reactores isotérmicos

## Reactor Batch

Balanço molar     $r_A V = \frac{dN_A}{dt}$                        $N_A = N_{A0} (1 - X)$

∴     $r_A V = -N_{A0} \frac{dX}{dt}$

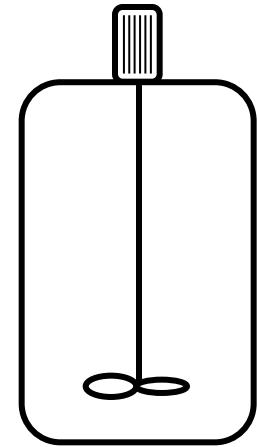


# Dimensionamento de reactores isotérmicos

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# Dimensionamento de reactores isotérmicos

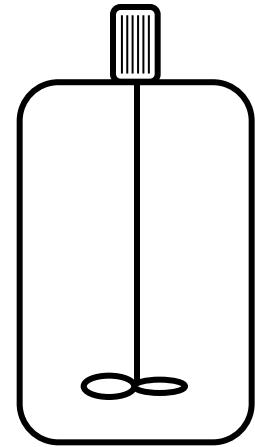
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## Lei cinética

Reacção de ordem n, Volume constante:

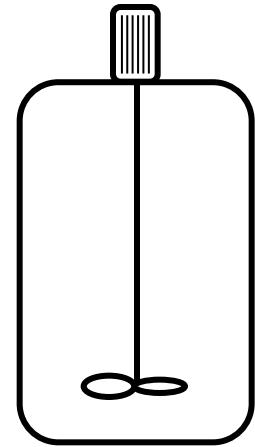


# Dimensionamento de reactores isotérmicos

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Lei cinética



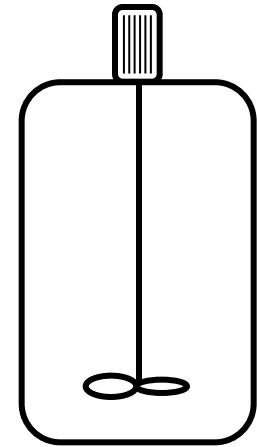
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# Dimensionamento de reactores isotérmicos

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## Lei cinética



Reacção de ordem n, Volume constante:

$$-r_A = k C_A^\alpha C_B^\beta$$

# Dimensionamento de reactores isotérmicos

## Reactor Batch

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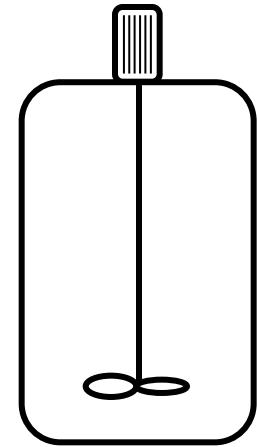
Lei cinética



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$$\therefore dt = \frac{N_{A0}}{V} \cdot \frac{dX}{k C_A^\alpha C_B^\beta}$$

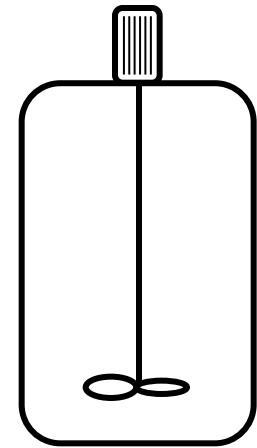


# Dimensionamento de reactores isotérmicos

## Reactor Batch

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## Lei cinética



Reacção de ordem n, Volume constante:

$$-r_A = k C_A^\alpha C_B^\beta$$

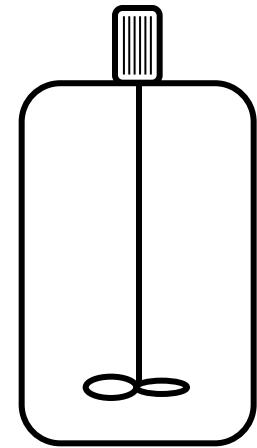
$$\therefore dt = \frac{N_{A0}}{V} \cdot \frac{dX}{k C_A^\alpha C_B^\beta} = \frac{N_{A0}}{V} \cdot \frac{dX}{k \left( \frac{N_A}{V} \square^\alpha \cdot \left( \frac{N_B}{V} \square^\beta \right) \right)}$$

# Dimensionamento de reactores isotérmicos

## Reactor Batch

Balanço molar     $r_A V = \frac{dN_A}{dt}$      $N_A = N_{A0} (1 - X)$

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## Lei cinética



Reacção de ordem n, Volume constante:

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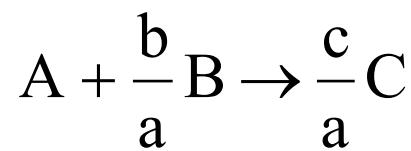
$$\therefore dt = \frac{N_{A0}}{V} \cdot \underbrace{\frac{dX}{k C_A^\alpha C_B^\beta}}_{-r_A} = \frac{N_{A0}}{V} \cdot \frac{dX}{k \left( \frac{N_A}{V} \square^\alpha \cdot \left( \frac{N_B}{V} \square^\beta \right) \right)}$$

$$dt = \frac{N_{A0}}{V} \cdot \frac{dX}{k\left(\frac{N_A}{V}\right)^\alpha \cdot \left(\frac{N_B}{V}\right)^\beta}$$



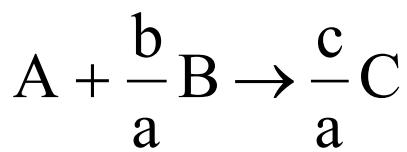
$$dt = \frac{N_{A0}}{V} \cdot \frac{dX}{k \left( \frac{N_A}{V} \square^{\alpha} \cdot \left( \frac{N_B}{V} \square^{\beta} \right. \right.}$$

$$aA + bB \rightarrow cC$$



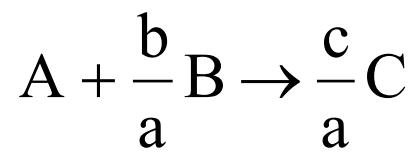
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$$aA + bB \rightarrow cC$$



$$\frac{d t}{d t} = \frac{N_{A0}}{V} \cdot \frac{d X}{k \left( \frac{N_A}{V} \square^{\alpha} \cdot \left( \frac{N_B}{V} \square^{\beta} \right. \right.}$$

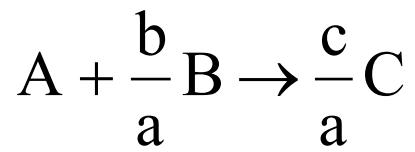
$$N_A=N_{A0}\cdot\left(1-X\right)$$



$$N_A = N_{A0} \cdot (1 - X)$$

$$N_B = N_{B0} \left( \theta_B - \frac{b}{a} X \right)$$

$$\frac{dN_A}{dt} = \frac{N_{A0}}{V} \cdot \frac{dX}{k \left( \frac{N_A}{V} \square^{\alpha} \cdot \left( \frac{N_B}{V} \square^{\beta} \right) \right)}$$

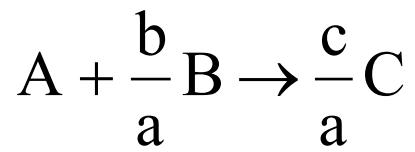


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$$dt = \frac{N_{A0}}{V} \cdot \frac{dX}{k \left( \frac{N_A}{V} \square^{\alpha} \cdot \left( \frac{N_B}{V} \square^{\beta} \right) \right)}$$

$$\therefore dt = \frac{N_{A0}}{V} \cdot \frac{dX}{k \left( \frac{N_{A0} \cdot (1 - X)}{V} \right)^{\alpha} \cdot \left( \frac{N_{A0} \cdot \left( \theta_B - \frac{b}{a} \cdot X \right)}{V} \right)^{\beta}}$$



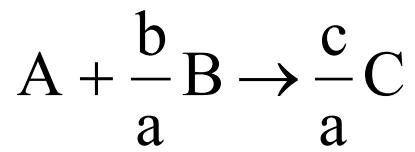
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$$\therefore dt = \left( \frac{N_{A0}}{V} \right)^{(1-n)} \cdot \frac{dX}{k (1 - X)^{\alpha} \cdot \left( \theta_B - \frac{b}{a} X \right)^{\beta}}$$



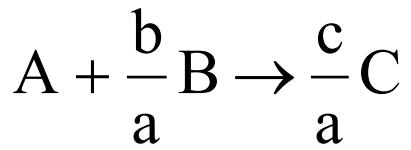
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$$N_A = N_{A0} \cdot (1 - X)$$

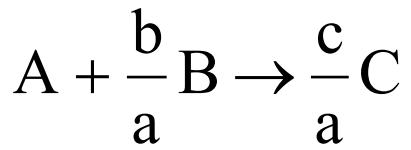
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$$dt = \frac{N_{A0}}{V} \cdot \frac{dX}{k \left( \frac{N_A}{V} \square^{\alpha} \cdot \left( \frac{N_B}{V} \square^{\beta} \right) \right)}$$

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$$t = \frac{1}{k} \left( \frac{N_{A0}}{V} \right)^{(1-n)X} \int_0^{\infty} \frac{dX}{(1 - X)^{\alpha} \cdot \left( \theta_B - \frac{b}{a} \cdot X \right)^{\beta}}$$



$$N_A = N_{A0} \cdot (1 - X)$$

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$$dt = \frac{N_{A0}}{V} \cdot \frac{dX}{k \left( \frac{N_A}{V} \square^{\alpha} \cdot \left( \frac{N_B}{V} \square^{\beta} \right) \right)}$$

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Exemplo

$$t = \frac{1}{k} \left( \frac{N_{A0}}{V} \right)^{(1-n)X} \int_0^{\infty} \frac{dX}{(1 - X)^{\alpha} \cdot \left( \theta_B - \frac{b}{a} \cdot X \right)^{\beta}}$$

# Dimensionamento de reactores isotérmicos

## Reactor Batch

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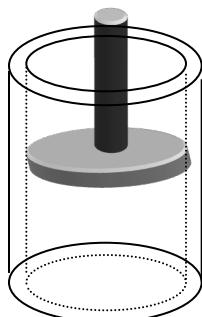
$\therefore r_A V = -N_{A0} \frac{dX}{dt}$        $\therefore dt = \frac{N_{A0}}{V} \cdot \frac{dX}{-r_A}$

Lei cinética



Reacção de ordem n, Volume variável:

$$-r_A = k C_A^\alpha C_B^\beta$$



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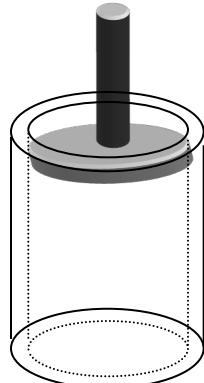
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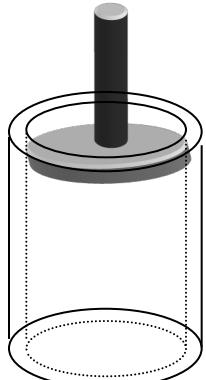
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Lei cinética



Reacção de ordem n, Volume variável:

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$$\therefore dt = \frac{N_{A0}}{V} \cdot \frac{dX}{\underbrace{k C_A^\alpha C_B^\beta}_{-r_A}} = \frac{N_{A0}}{V} \cdot \frac{dX}{k \left( \frac{N_A}{V} \right)^\alpha \cdot \left( \frac{N_B}{V} \right)^\beta}$$

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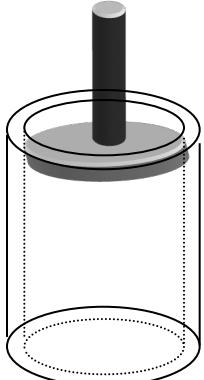
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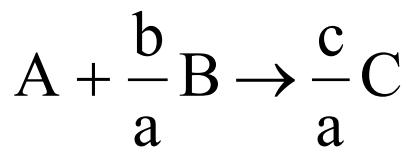


$$\therefore dt = \frac{dX}{k \frac{N_{A0}^{(n-1)} (1-X)^\alpha \left(\theta_B - \frac{b}{a} \cdot X\right)^\beta}{V^{(n-1)}}}$$

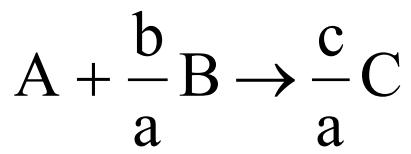
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$$\therefore \; \; dt \; = \frac{dX}{k\frac{N_{A0}^{(n-1)}(1-X)^\alpha\left(\theta_B-\frac{b}{a}\cdot X\right)^\beta}{V^{(n-1)}}}$$

$$V=V_0\left(1+\varepsilon\,X\right)\cdot\frac{T}{T_0}\cdot\frac{P_0}{P}$$

$$\therefore \; \; dt \; = \frac{dX}{k\frac{N_{A0}^{(n-1)}(1-X)^\alpha\left(\theta_B-\frac{b}{a}\cdot X\right)^\beta}{V^{(n-1)}}}$$

$$V=V_0\left(1+\varepsilon\,X\right)\cdot\frac{T}{T_0}\cdot\frac{P_0}{P}\\ \varepsilon=y_{A0}\,\delta$$

$$\therefore \;\; dt \; = \frac{dX}{k\frac{N_{A0}^{(\textcolor{violet}{n}-1)}(1-X)^\alpha\left(\theta_B-\frac{\textcolor{red}{b}}{a}\cdot X\right)^\beta}{V^{(\textcolor{blue}{n}-1)}}}$$

$$V=V_0\left(1+\varepsilon\,X\right)\cdot\frac{T}{T_0}\cdot\frac{P_0}{P}\\[1ex] \varepsilon=y_{A0}\,\delta$$

$$\delta=-1+\frac{b}{a}+\frac{c}{a}$$

$$T=T_\theta$$

$$V=V_0\left(1+\varepsilon\,X\right)\cdot\frac{T}{T_0}\cdot\frac{P_0}{P}$$

$$\varepsilon = y_{A0} \; \delta$$

$$\delta=-1+\frac{b}{a}+\frac{c}{a}$$

$$\therefore \;\; dt \;=\! \frac{dX}{k\,\dfrac{N_{A0}^{(\mathfrak{n}-1)}(1-X)^\alpha\!\left(\theta_B-\dfrac{\textcolor{red}{b}}{a}\!\cdot X\right)^\beta}{V^{(\mathfrak{n}-1)}}}$$

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$$\therefore dt = \frac{dX}{k \frac{N_{A0}^{(n-1)} (1-X)^\alpha \left( \theta_B - \frac{b}{a} \cdot X \right)^\beta}{V^{(n-1)}}}$$

$$T = T_0$$

$$V = V_0 (1 + \varepsilon X) \cdot \frac{P_0}{P}$$

$$\varepsilon = y_{A0} \delta$$

## Reactor isobárico:

$$\delta = -1 + \frac{b}{a} + \frac{c}{a}$$

$$\therefore dt = \frac{dX}{k \frac{N_{A0}^{(n-1)} (1-X)^\alpha \left( \theta_B - \frac{b}{a} \cdot X \right)^\beta}{V^{(n-1)}}}$$

$$T = T_0$$

$$V = V_0 (1 + \varepsilon X) \cdot \frac{P_0}{P}$$

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**Reactor isobárico:**  $P = P_0$

$$\delta = -1 + \frac{b}{a} + \frac{c}{a}$$

$$dX$$

$$\therefore dt = \frac{dX}{k \frac{N_{A0}^{(n-1)} (1-X)^\alpha \left( \theta_B - \frac{b}{a} \cdot X \right)^\beta}{V^{(n-1)}}}$$

$$T = T_0$$

$$V = V_0 (1 + \varepsilon X) \cdot \frac{P_0}{P}$$

$$\varepsilon = y_{A0} \delta$$

**Reactor isobárico:**

$$P = P_0$$

$$\Rightarrow$$

$$V = V_0 (1 + \varepsilon X)$$

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**Reactor isobárico:**  $P = P_0 \quad \Rightarrow \quad V = V_0 (1 + \varepsilon X)$

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**Reactor isobárico:**  $P = P_0 \quad \Rightarrow \quad V = V_0 (1 + \varepsilon X)$

$$\therefore dt = \frac{dX}{k \frac{N_{A0}^{(n-1)} (1-X)^\alpha \left( \theta_B - \frac{b}{a} \cdot X \right)^\beta}{V_0^{(n-1)} (1 + \varepsilon X)^{(n-1)}}}$$

$$\therefore dt = \frac{1}{k} \cdot \frac{(1 + \varepsilon X)^{(n-1)}}{C_{A0}^{(n-1)} (1-X)^\alpha \left( \theta_B - \frac{b}{a} \cdot X \right)^\beta} dX$$

$$\therefore dt = \frac{dX}{k \frac{N_{A0}^{(n-1)} (1-X)^\alpha \left( \theta_B - \frac{b}{a} \cdot X \right)^\beta}{V^{(n-1)}}}$$

$$T = T_0 \\ V = V_0 (1 + \varepsilon X) \cdot \frac{P_0}{P} \\ \varepsilon = y_{A0} \delta$$

$$\text{Reactor isobárico: } P = P_0 \quad \Rightarrow \quad V = V_0 (1 + \varepsilon X) \quad \delta = -1 + \frac{b}{a} + \frac{c}{a}$$

$$\therefore dt = \frac{dX}{k \frac{N_{A0}^{(n-1)} (1-X)^\alpha \left( \theta_B - \frac{b}{a} \cdot X \right)^\beta}{V_0^{(n-1)} (1 + \varepsilon X)^{(n-1)}}}$$

$$t = \frac{1}{k C_{A0}^{(n-1)}} \cdot \int_0^X \frac{(1 + \varepsilon X)^{(n-1)}}{(1-X)^\alpha \left( \theta_B - \frac{b}{a} \cdot X \right)^\beta} dX$$

$$\therefore dt = \frac{1}{k} \cdot \frac{(1 + \varepsilon X)^{(n-1)}}{C_{A0}^{(n-1)} (1-X)^\alpha \left( \theta_B - \frac{b}{a} \cdot X \right)^\beta} dX$$

$$\therefore \; \; dt \; = \frac{dX}{k\frac{N_{A0}^{(n-1)}(1-X)^\alpha\left(\theta_B-\frac{b}{a}\cdot X\right)^\beta}{V^{(n-1)}}}$$

$$V=V_0\left(1+\varepsilon\,X\right)\cdot\frac{P_0}{P}\\[1mm] \varepsilon=y_{A0}\;\delta$$

$$\therefore dt = \frac{dX}{k \frac{N_{A0}^{(n-1)} (1-X)^\alpha \left( \theta_B - \frac{b}{a} \cdot X \right)^\beta}{V^{(n-1)}}}$$

$$V = V_0 (1 + \varepsilon X) \cdot \frac{P_0}{P}$$

$$\varepsilon = y_{A0} \delta$$

**Reactor não isobárico:**

$$\therefore dt = \frac{dX}{k \frac{N_{A0}^{(n-1)} (1-X)^\alpha \left( \theta_B - \frac{b}{a} \cdot X \right)^\beta}{V^{(n-1)}}}$$

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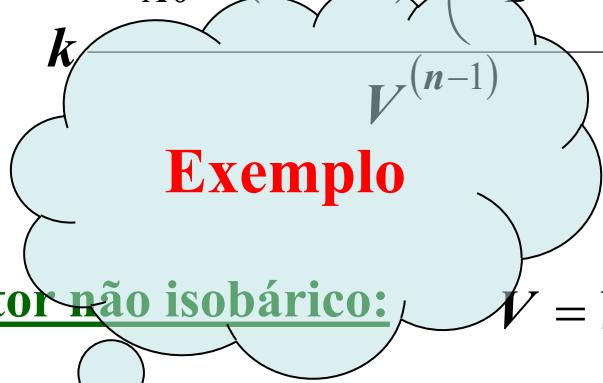
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**Reactor não isobárico:**  $V = V_0 (1 + \varepsilon X) \cdot \frac{P_0}{P}$

$$\frac{P}{P_0} = f(V)$$

$$\therefore dt = \frac{dX}{k N_{A0}^{(n-1)} (1-X)^\alpha \left( \theta_B - \frac{b}{a} \cdot X \right)^\beta}$$



Reactor não isobárico:

$$\frac{P}{P_0} = \gamma V$$

$$V = V_0 (1 + \varepsilon X) \cdot \frac{P_0}{P}$$

$$\varepsilon = y_{A0} \delta$$

$$\frac{P}{P_0} = f(V)$$

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$$\therefore V = \left[ \frac{V_0 \cdot (1 + \varepsilon X)}{\gamma} \right]^{1/2}$$

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$$\therefore dt = \frac{dX}{k \frac{N_{A0}^{(n-1)} (1-X)^\alpha \left( \theta_B - \frac{\mathbf{b}}{\mathbf{a}} \cdot \mathbf{X} \right)^\beta}{V^{(n-1)}}}$$

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$$\therefore dt = \frac{dX}{k \frac{N_{A0}^{(n-1)} (1-X)^\alpha \left( \theta_B - \frac{\mathbf{b}}{\mathbf{a}} \cdot \mathbf{X} \right)^\beta}{V^{(n-1)}}}$$

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$$\therefore V = \left[ \frac{V_0 \cdot (1 + \varepsilon X)}{\gamma} \right]^{\frac{1}{2}}$$

$$\therefore dt = \frac{V_0^{\frac{(n-1)}{2}}}{N_{A0}^{(n-1)} \cdot k \cdot \gamma^{\frac{(n-1)}{2}}} \cdot \frac{(1 + \varepsilon X)^{\frac{(n-1)}{2}}}{(1 - X)^\alpha \left( \theta_B - \frac{\mathbf{b}}{\mathbf{a}} \cdot \mathbf{X} \right)^\beta} dX$$

$$\therefore dt = \frac{dX}{k \frac{N_{A0}^{(n-1)} (1-X)^\alpha \left( \theta_B - \frac{\mathbf{b}}{\mathbf{a}} \cdot \mathbf{X} \right)^\beta}{V^{(n-1)}}}$$

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$$\therefore V = \left[ \frac{V_0 \cdot (1 + \varepsilon X)}{\gamma} \right]^{1/2}$$

$$t = \frac{V_0^{(n-1)/2}}{N_{A0}^{(n-1)} \cdot k \cdot \gamma^{(n-1)/2}} \cdot \int_0^X \frac{(1 + \varepsilon X)^{(n-1)/2}}{(1 - X)^\alpha \left( \theta_B - \frac{\mathbf{b}}{\mathbf{a}} \cdot \mathbf{X} \right)^\beta} dX$$

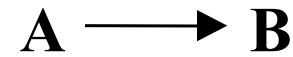
**Exemplo**

# **Dimensionamento de reactores isotérmicos**

## **Reactor Batch**

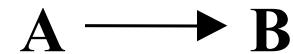
# Dimensionamento de reactores isotérmicos

Reactor Batch



# Dimensionamento de reactores isotérmicos

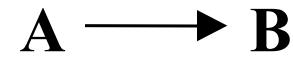
**Reactor Batch**



Velocidade de produção:

# Dimensionamento de reactores isotérmicos

Reactor Batch

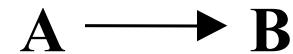


Velocidade de produção:

$$v_{prod} = \frac{N_B}{t_{oper}}$$

# Dimensionamento de reactores isotérmicos

Reactor Batch



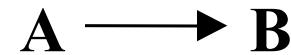
Velocidade de produção:

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Tempo de  
operação

# Dimensionamento de reactores isotérmicos

Reactor Batch



Velocidade de produção:

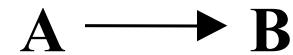
$$v_{prod} = \frac{N_B}{t_{oper}}$$

Tempo de  
operação

*t<sub>oper</sub>*

# Dimensionamento de reactores isotérmicos

Reactor Batch



Velocidade de produção:

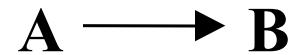
$$v_{prod} = \frac{N_B}{t_{oper}}$$

Tempo de  
operação

$$t_{oper} = t$$

# Dimensionamento de reactores isotérmicos

Reactor Batch



Velocidade de produção:

$$v_{prod} = \frac{N_B}{t_{oper}}$$

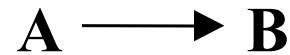
Tempo de reacção

$$t_{oper} = t$$

Tempo de operação

# Dimensionamento de reactores isotérmicos

Reactor Batch



Velocidade de produção:

$$v_{prod} = \frac{N_B}{t_{oper}}$$

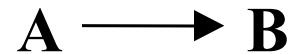
Tempo de reacção

$$t_{oper} = t + t_d$$

Tempo de operação

# Dimensionamento de reactores isotérmicos

Reactor Batch



Velocidade de produção:

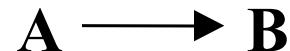
$$v_{prod} = \frac{N_B}{t_{oper}}$$



$$t_{oper} = t + t_d$$

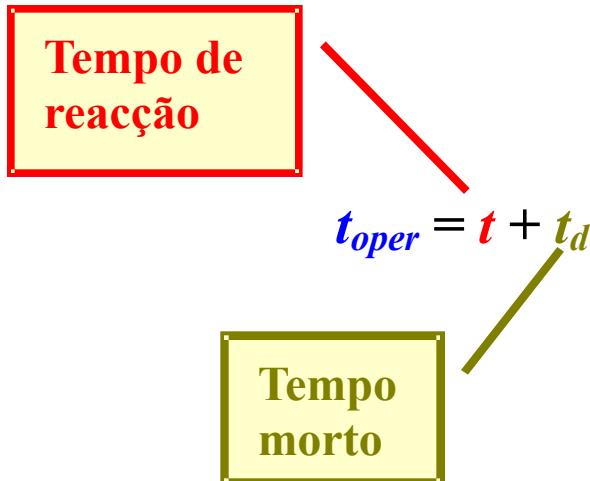
# Dimensionamento de reactores isotérmicos

## Reactor Batch



Velocidade de produção:

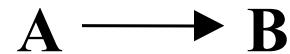
$$v_{prod} = \frac{N_B}{t_{oper}}$$



A conversão óptima e o tempo de operação óptimo correspondem à velocidade de produção máxima

# Dimensionamento de reactores isotérmicos

## Reactor Batch



Velocidade de produção:

$$v_{prod} = \frac{N_B}{t_{oper}}$$

Tempo de reacção

Tempo morto

$$t_{oper} = t + t_d$$

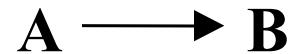
Tempo de operação

A conversão óptima e o tempo de operação óptimo correspondem à velocidade de produção máxima

Condição de máximo:

# Dimensionamento de reactores isotérmicos

## Reactor Batch



Velocidade de produção:

$$v_{prod} = \frac{N_B}{t_{oper}}$$

Tempo de operação

Tempo de reacção

$$t_{oper} = t + t_d$$

Tempo morto

A conversão óptima e o tempo de operação óptimo correspondem à velocidade de produção máxima

Condição de máximo:

$$\frac{dv_{prod}}{dt} = 0$$

$$\frac{dv_{prod}}{dt}=0$$

$$\frac{dv_{prod}}{dt} = 0 \quad \therefore \quad \frac{d}{dt} \left( \frac{N_{A0} X}{t_{oper}} \right) = 0$$

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$$\therefore \frac{d}{dt} \left( \frac{N_{A0} X}{t_{oper}} \right) = 0$$

$$\therefore \frac{\frac{dX}{dt}(t + t_d) - X}{t_{oper}^2} = 0$$

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$$\therefore \quad X = \frac{dX}{dt} t + \frac{dX}{dt} t_d$$

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Equação de  
uma recta

$$\frac{dv_{prod}}{dt} = 0$$

$$\therefore \frac{d}{dt} \left( N_{A0} \frac{X}{t_{oper}} \right) = 0$$

$$\therefore \frac{\frac{dX}{dt}(t + t_d) - X}{t_{oper}^2} = 0$$

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Equação de  
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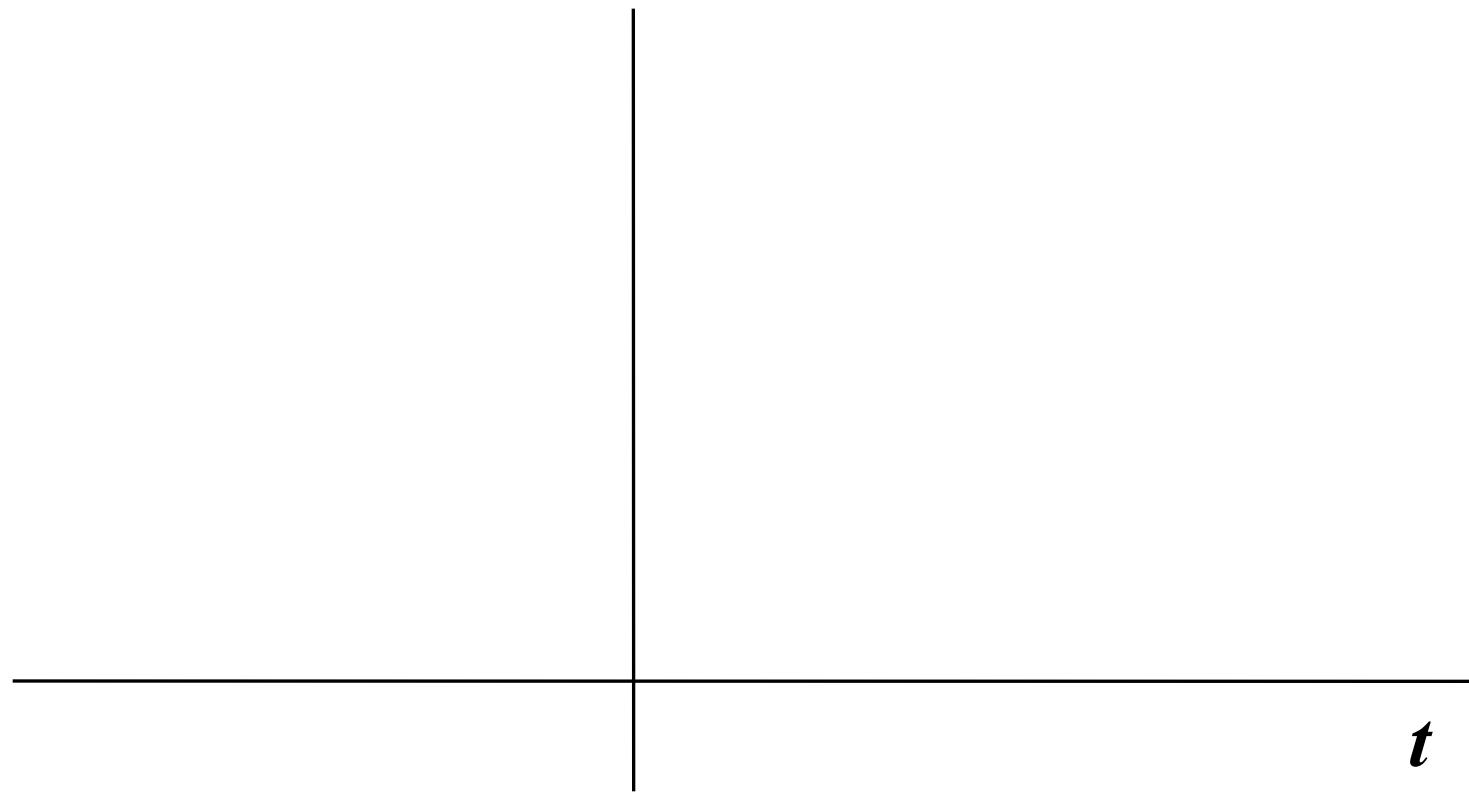
$$\frac{d}{dt} \left( \frac{N_{A0} X}{t_{oper}} \right) \quad \begin{array}{l} \text{Inclinação} \\ \text{Ordenada na origem} \end{array} \quad \therefore \quad \frac{\frac{dX}{dt}(t + t_d) - X}{t_{oper}^2} = 0$$

$$\therefore X = \frac{dX}{dt} t + \frac{dX}{dt} t_d$$

Equação de  
uma recta

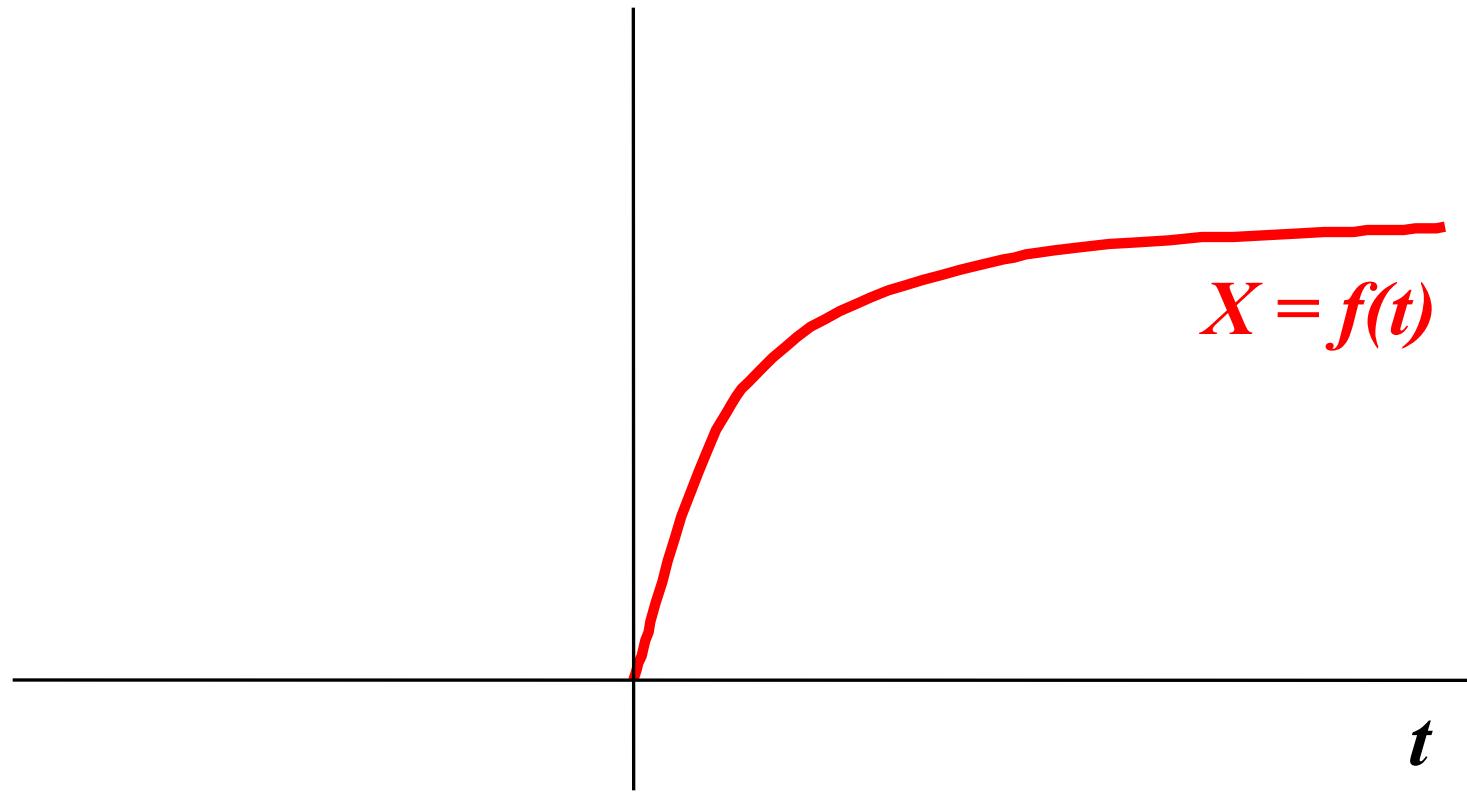
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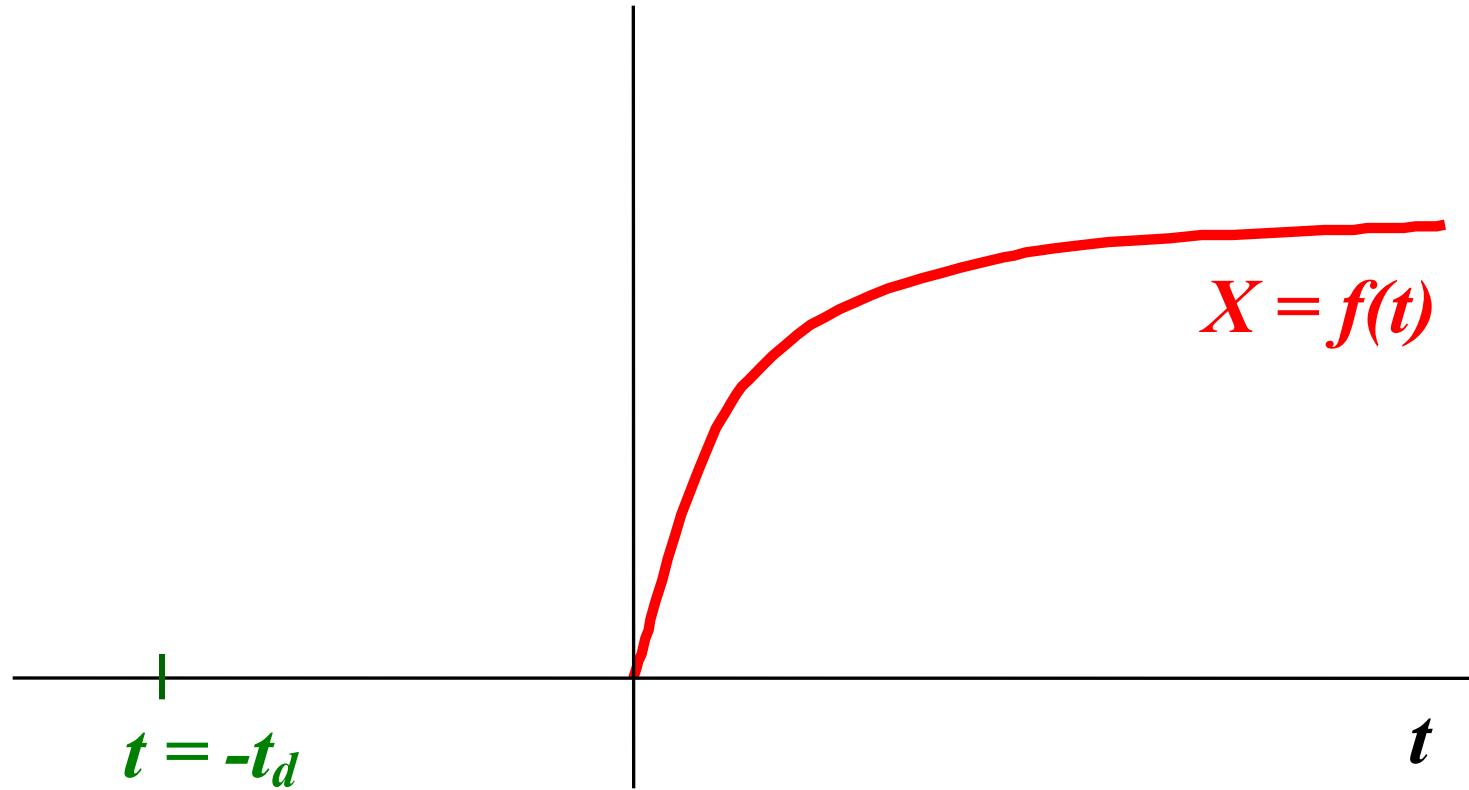
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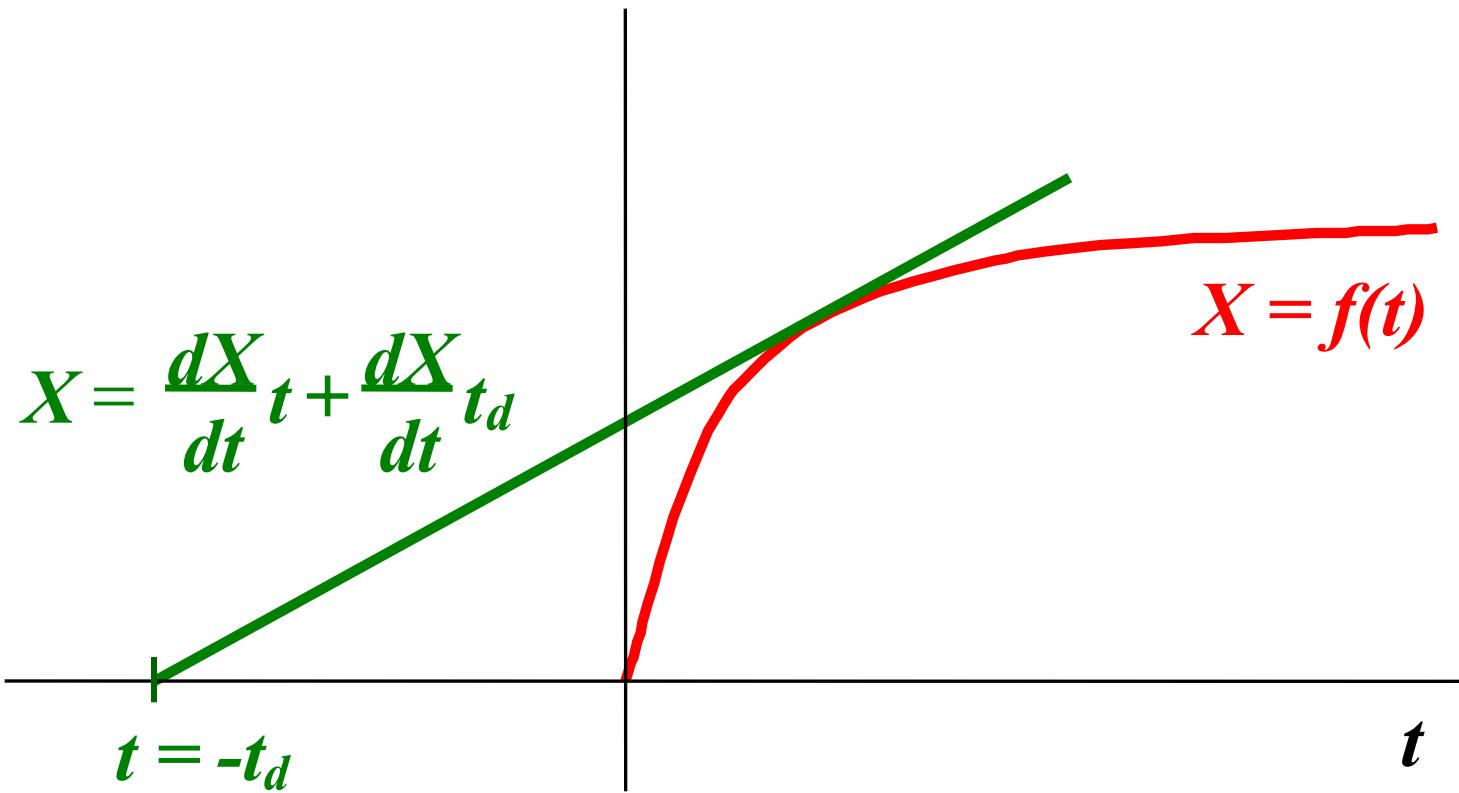
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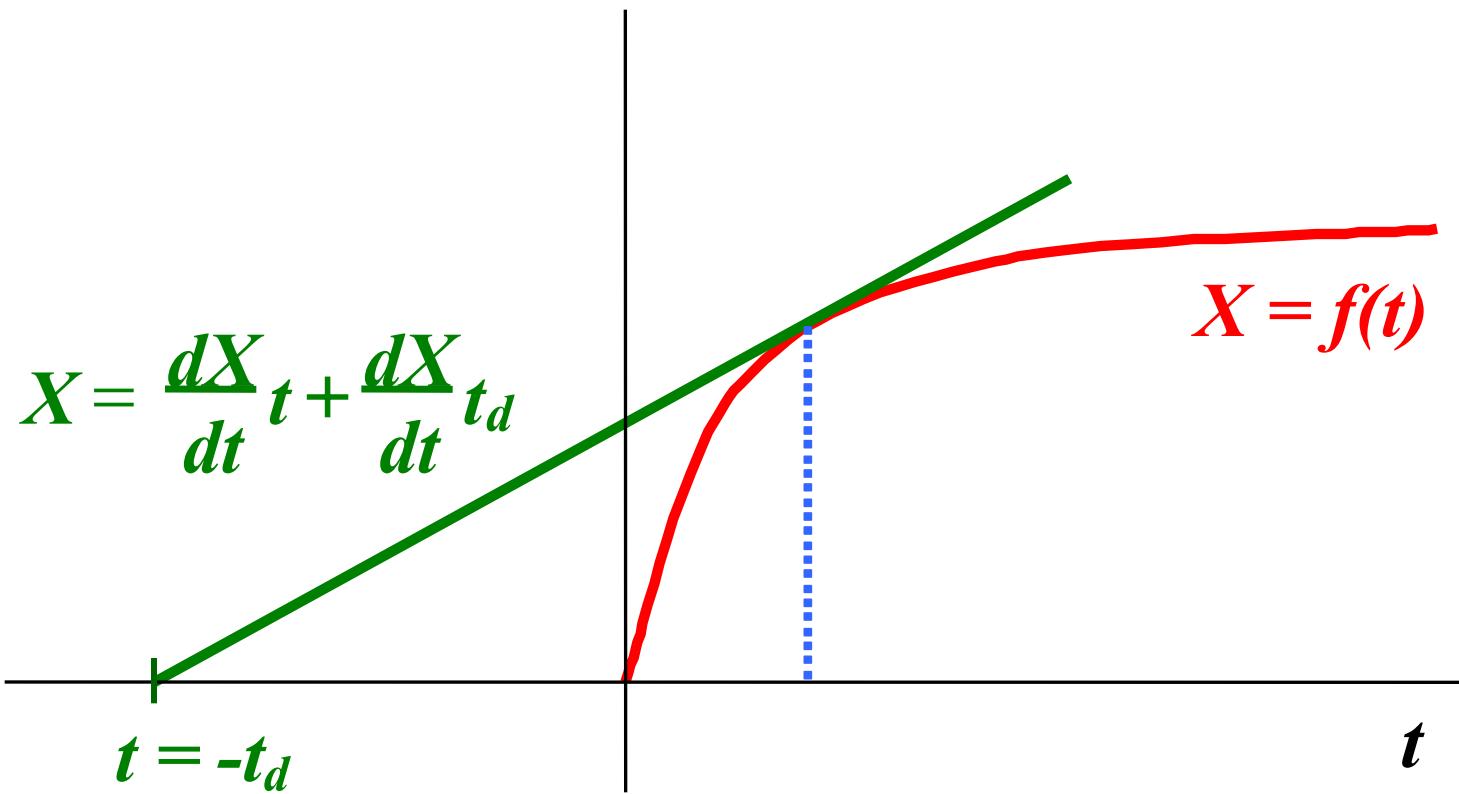
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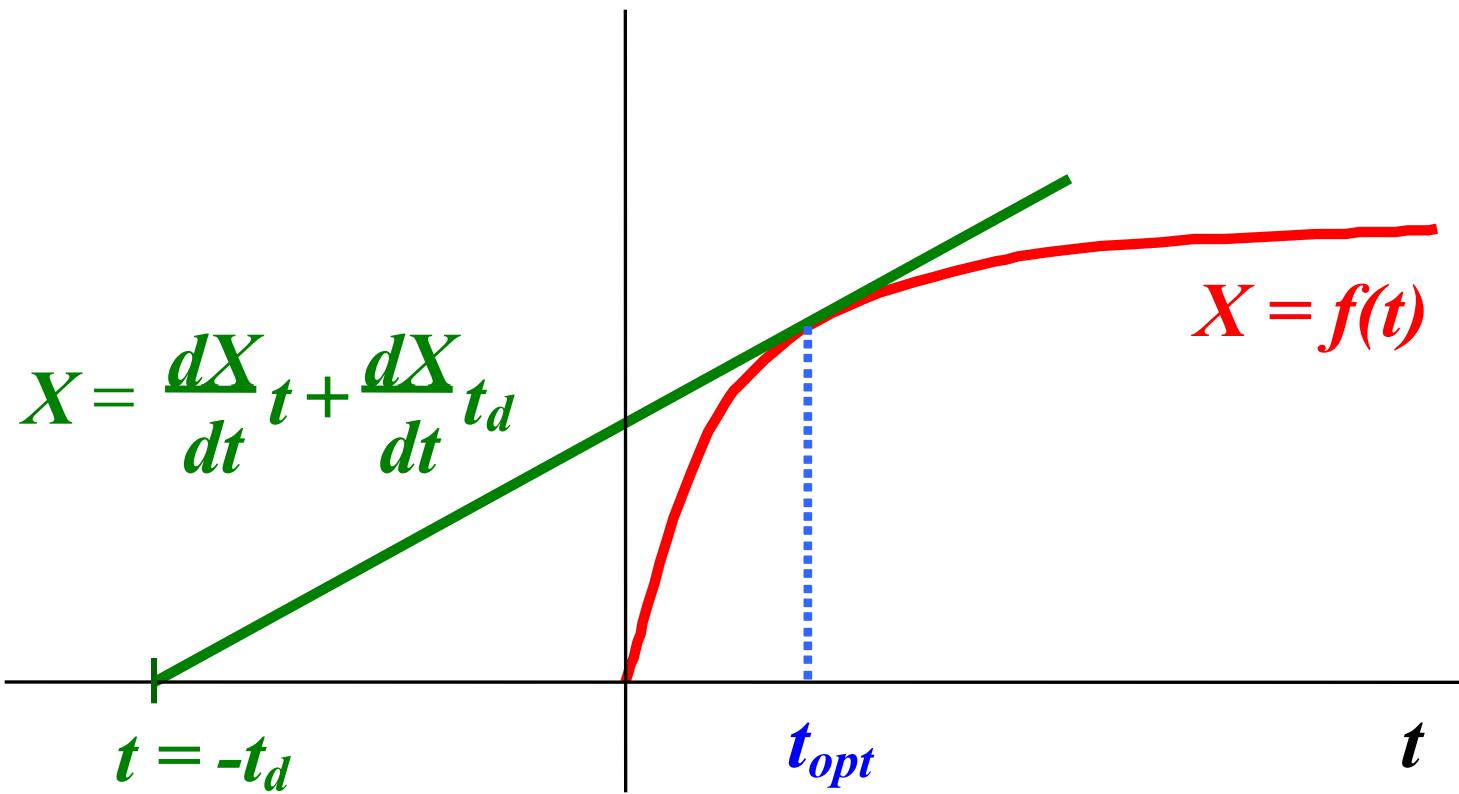
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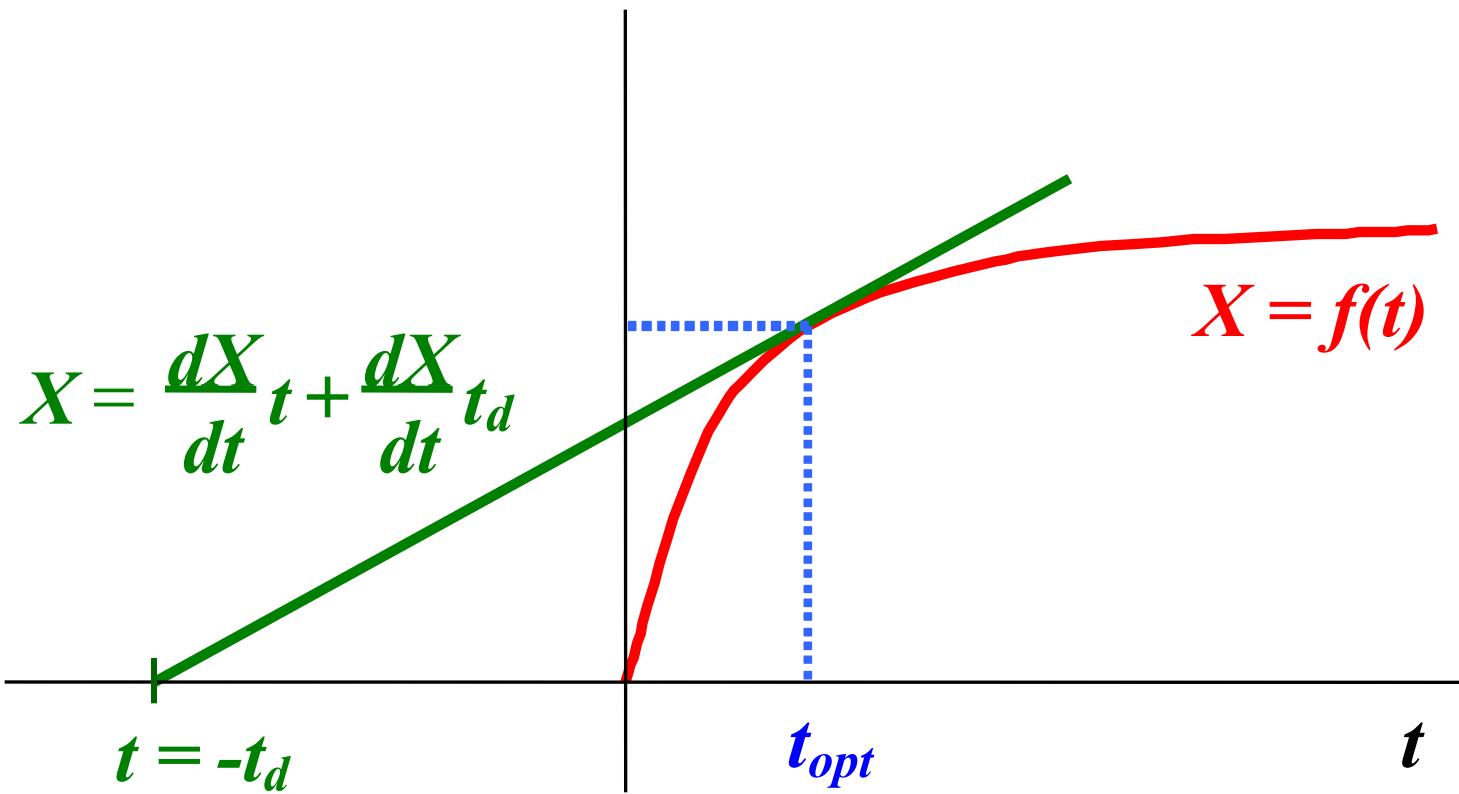
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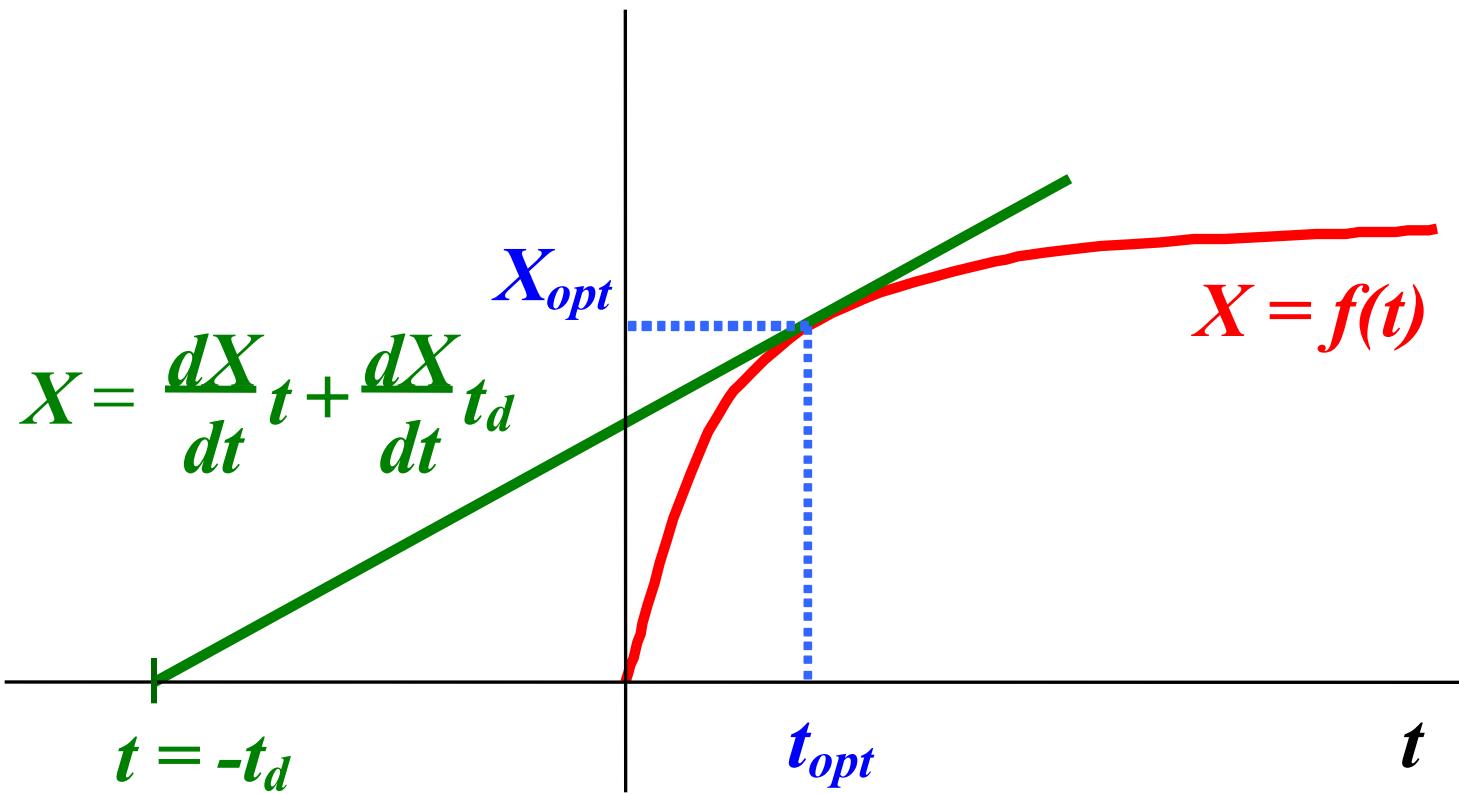
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