

Introdução à Engenharia Química e Bioquímica

Aula 11
MIEQB
ano lectivo de 2020/2021

Sumário da aula

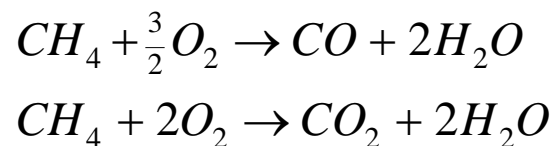
Balanços materiais a processos com reacção

- Estequiometria de uma reacção
- Reagente limitante e reagente em excesso; percentagem de excesso
- Conversão de uma reacção
- Rendimento e selectividade de uma reacção

4.4

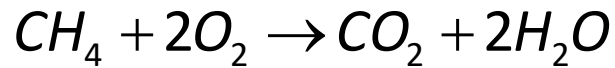
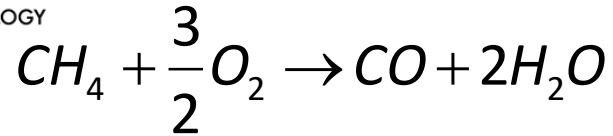
Queima-se metano com ar atmosférico num reactor de combustão contínuo, resultando à saída do reactor uma mistura gasosa de monóxido de carbono, dióxido de carbono e água.

As reacções que se desenrolam são:



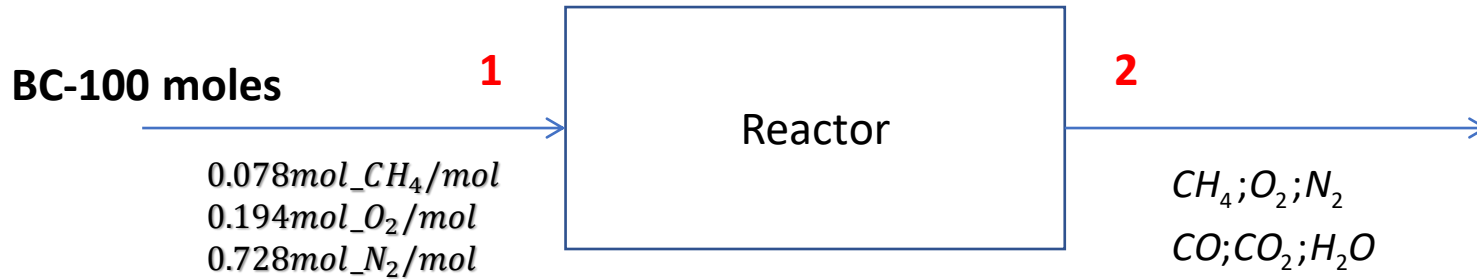
A alimentação ao reactor contém 7.8% molar CH_4 , 19.4% molar O_2 e 72.8% molar de N_2 . A conversão de metano é de 90% e a mistura gasosa que sai do reactor contém 8 moles de CO_2 por mole de CO . Calcule a composição molar da corrente de saída.

4.4



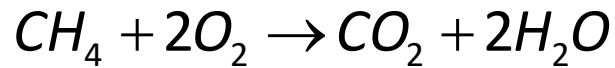
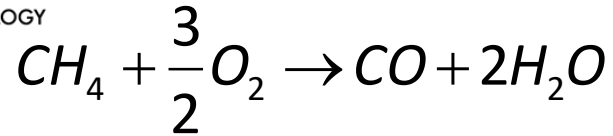
% conversão de metano = 90%

$$\frac{n_{CO_2-2}}{n_{CO-2}} = 8$$



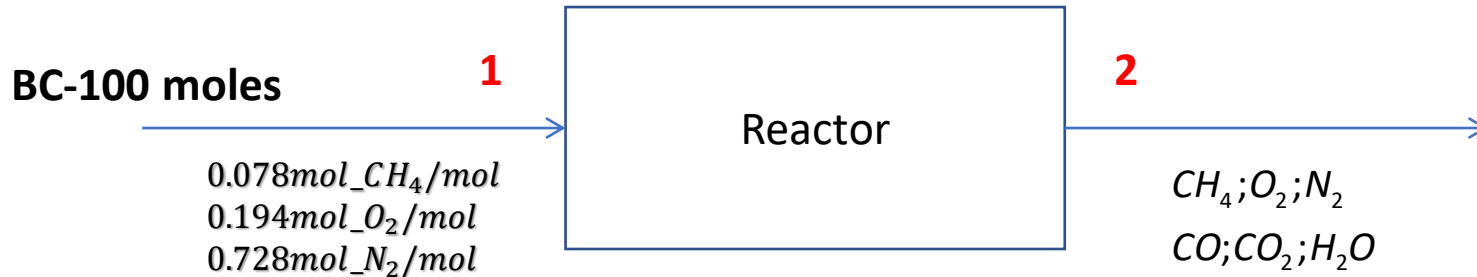
moles	1	2
CH4	7.8	
O2	19.4	
CO	0	
CO2	0	
H2O	0	
N2	72.8	
Total	100	

4.4



% conversão de metano = 90%

$$\frac{n_{CO_2-2}}{n_{CO_2}} = 8$$



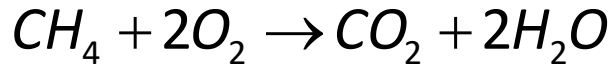
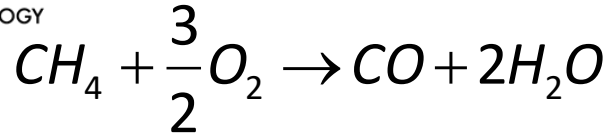
Sabe-se que conversão de metano é 90%,
logo 10% não reage e passa para corrente 2

$$n_{CH_4 2} = 0.1 \times n_{CH_4 1}$$

$$n_{CH_4 2} = 0.1 \times 0.078 \times 100 = 0.78 \text{ moles}$$

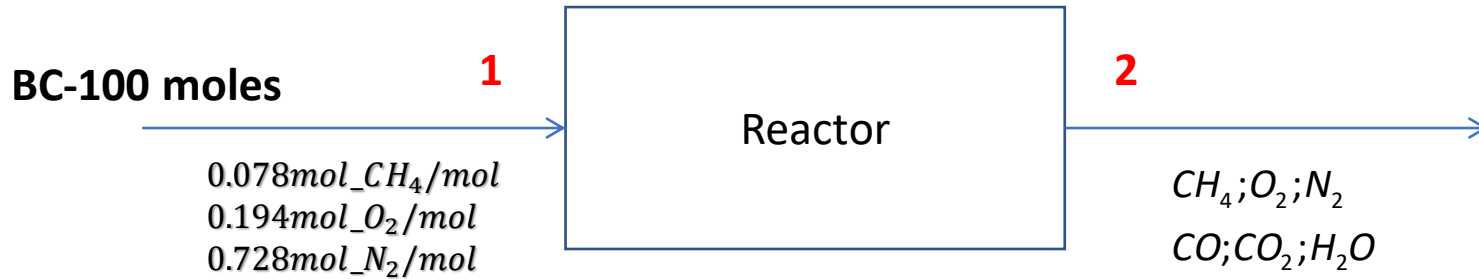
moles	1	2
CH4	7.8	0.78
O2	19.4	
CO	0	
CO2	0	
H2O	0	
N2	72.8	
Total	100	

4.4



% conversão de metano = 90%

$$\frac{n_{CO_2-2}}{n_{CO_2}} = 8$$



Sabe-se que conversão de metano é 90%,
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$$n_{CH_4 2} = 0.1 \times n_{CH_4 1}$$

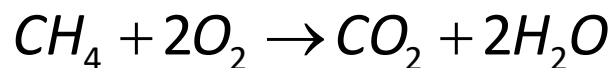
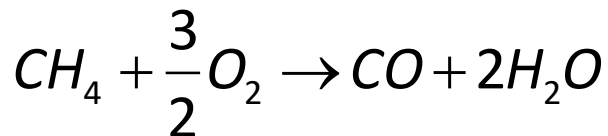
$$n_{CH_4 2} = 0.1 \times 0.078 \times 100 = 0.78 \text{ moles}$$

Fazendo um balanço à espécie não reactiva (inerte):

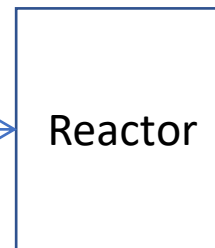
$$n_{N_2 1} = n_{N_2 2} = 72.8 \text{ mol}$$

moles	1	2
CH4	7.8	0.78
O2	19.4	
CO	0	
CO2	0	
H2O	0	
N2	72.8	72.8
Total	100	

4.4



BC-100 moles **1**
0.078mol_{CH₄}/mol
0.194mol_{O₂}/mol
0.728mol_{N₂}/mol



2

CH₄;O₂;N₂
CO;CO₂;H₂O

Fazendo agora um balanço ao CH₄ (carbono):

$$n_{CH_4 \text{ convertidas}} = n_{CH_4 \text{ 1}} - n_{CH_4 \text{ 2}} = 7.8 - 0.78 = 7.02 \text{ moles}$$

E também sabemos que:

$$n_{CH_4 \text{ convertidas}} = n_{CO_2 \text{ 1}} + n_{CO_2 \text{ 2}} = n_{CO_2 \text{ 1}} + 8 \times n_{CO_2 \text{ 1}} = 7.02 \text{ moles}$$

$$n_{CO_2 \text{ 2}} = 8n_{CO_2 \text{ 1}}$$

$$n_{CO_2 \text{ 1}} = 0.78 \text{ moles}$$

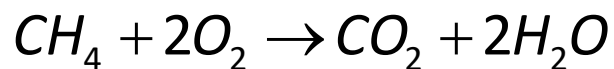
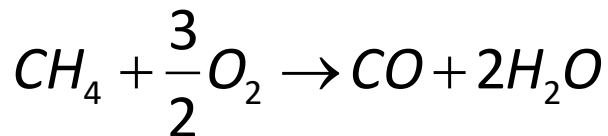
$$n_{CO_2 \text{ 2}} = 8 \times 0.78 = 6.24 \text{ moles}$$

Para a água:

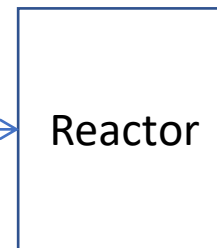
$$n_{H_2O \text{ 2}} = 2 \times n_{CO_2 \text{ 2}} + 2 \times n_{CO_2 \text{ 1}} = 14.04 \text{ moles}$$

moles	1	2
CH ₄	7.8	0.78
O ₂	19.4	
CO	0	0.78
CO ₂	0	6.24
H ₂ O	0	14.04
N ₂	72.8	72.8
Total	100	

4.4



BC-100 moles **1**
0.078mol_{CH₄}/mol
0.194mol_{O₂}/mol
0.728mol_{N₂}/mol



2

CH₄;O₂;N₂
CO;CO₂;H₂O

Para o oxigénio:

$$n_{O_2 \text{ convertidas}} = \frac{3}{2} \times n_{CO} + 2 \times n_{CO_2} = 13.65 \text{ moles}$$

$$n_{O_2} = n_{O_2 \text{ iniciais}} - n_{O_2 \text{ convertidas}} = 19.4 - 13.65 = 5.75 \text{ moles}$$

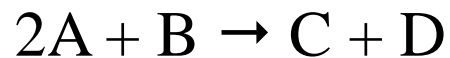
moles	1	2
CH4	7.8	0.78
O2	19.4	5.75
CO	0	0.78
CO2	0	6.24
H2O	0	14.04
N2	72.8	72.8
Total	100	100.4

Prob. 4.5

As seguintes reacções ocorrem num dado reactor:



Suponha que são alimentados 30 mole de A e 50 mole de B ao reactor. Quantas moles saem do reactor e qual a composição molar do efluente reaccional?

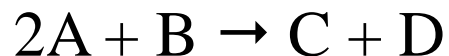
Prob. 4.5


$$2 \times 9.5 \quad 9.5 \quad 9.5 \quad 9.5$$

$$\% \text{ Convers\~{a}o}_B = 19\%$$

$$0.19 \times 50 \text{ mol } B = 9.5$$

moles	Entrada	Saída	
A	30		
B	50		
C	-		
D	-		
E	-		
Total	80		

Prob. 4.5


$$2 \times 9.5 \quad 9.5 \quad 9.5 \quad 9.5$$



$$8 \quad 8 \quad 8$$



$$6.5 \quad 6.5 \quad 6.5$$

$$\% \text{ Convers\~{a}o}_B = 19\%$$

$$0.19 \times 50 \text{ mol } B = 9.5$$

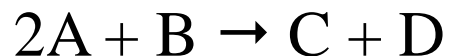
$$\% \text{ Convers\~{a}o}_B = 16\%$$

$$0.16 \times 50 \text{ mol } B = 8$$

$$\% \text{ Convers\~{a}o}_B = 13\%$$

$$0.13 \times 50 \text{ mol } B = 6.5$$

moles	Entrada	Saída	
A	30		
B	50		
C	-		
D	-		
E	-		
Total	80		

Prob. 4.5


$$2 \times 9.5 \quad 9.5 \quad 9.5 \quad 9.5$$



$$8 \quad 8 \quad 8$$



$$6.5 \quad 6.5 \quad 6.5$$

$$A: 30 - 2 \times 9.5 + 6.5 = 17.5$$

$$B: 50 - 9.5 - 8 - 6.5 = 26$$

$$C: 0 + 9.5 = 9.5$$

$$D: 0 + 9.5 - 8 = 1.5$$

$$E: 0 + 8 - 6.5 = 1.5$$

$$\% \text{ Convers\~{a}o}_B = 19\%$$

$$0.19 \times 50 \text{ mol } B = 9.5$$

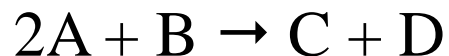
$$\% \text{ Convers\~{a}o}_B = 16\%$$

$$0.16 \times 50 \text{ mol } B = 8$$

$$\% \text{ Convers\~{a}o}_B = 13\%$$

$$0.13 \times 50 \text{ mol } B = 8$$

moles	Entrada	Saída	
A	30	17.5	
B	50	26	
C	-	9.5	
D	-	1.5	
E	-	1.5	
Total	80	56	

Prob. 4.5


$$2 \times 9.5 \quad 9.5 \quad 9.5 \quad 9.5$$



$$8 \quad 8 \quad 8$$



$$6.5 \quad 6.5 \quad 6.5$$

$$A: 30 - 2 \times 9.5 + 6.5 = 17.5$$

$$B: 50 - 9.5 - 8 - 6.5 = 26$$

$$C: 0 + 9.5 = 9.5$$

$$D: 0 + 9.5 - 8 = 1.5$$

$$E: 0 + 8 - 6.5 = 1.5$$

$$\% \text{ Convers\~{a}o}_B = 19\%$$

$$0.19 \times 50 \text{ mol } B = 9.5$$

$$\% \text{ Convers\~{a}o}_B = 16\%$$

$$0.16 \times 50 \text{ mol } B = 8$$

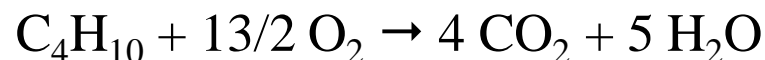
$$\% \text{ Convers\~{a}o}_B = 13\%$$

$$0.13 \times 50 \text{ mol } B = 6.5$$

moles	Entrada	Saída	
A	30	17.5	31.25%
B	50	26	46.4%
C	-	9.5	16.96%
D	-	1.5	2.68%
E	-	1.5	2.68%
Total	80	56	

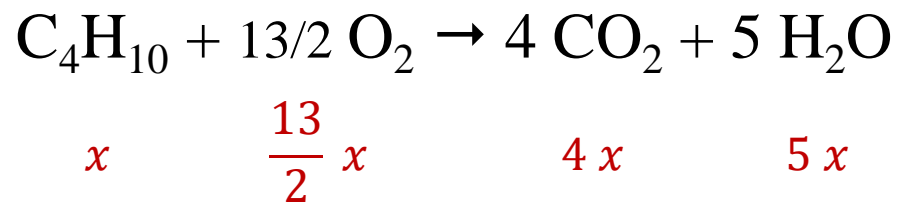
Prob. 4.6

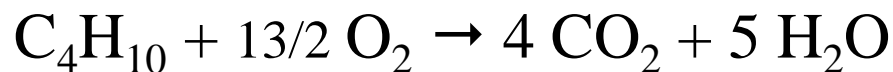
Butano é queimado com um excesso de ar (21% de O₂ e 79% de N₂) segundo a reacção:



Sabendo que a composição molar do gás de saída do reactor é, numa base seca, de 10.63% de CO₂, 5.12% mol de O₂ e 84.25% mol de N₂, calcule:

- a) A percentagem de conversão do butano
- b) A percentagem de excesso de ar
- c) A composição molar do gás de combustão (incluindo a água)

Prob. 4.6

Prob. 4.6


$$x \qquad \frac{13}{2} x \qquad 4 x \qquad 5 x$$

moles	1	2
C ₄ H ₁₀		-
O ₂		5.12
N ₂		84.25
CO ₂	-	10.63
H ₂ O	-	13.29

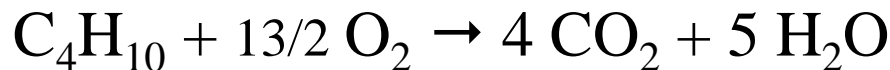
Base seca
BC 100 mol

N₂ é inerte!

$$n_{\text{CO}_2 \text{ produzidas}} = 10.63 \text{ moles} = 4x$$

$$4x = 10.63$$

$$x = 2.6575 = n_{\text{C}_4\text{H}_{10} \text{ convertido}}$$

Prob. 4.6


$$x \qquad \frac{13}{2} x \qquad 4 x \qquad 5 x$$

moles	1	2
C ₄ H ₁₀	2.6575	-
O ₂	22.394	5.12
N ₂	84.25	84.25
CO ₂	-	10.63
H ₂ O	-	13.29

Base seca
BC 100 mol

N₂ é inerte!

$$n_{\text{CO}_2 \text{ produzidas}} = 10.63 \text{ moles} = 4x$$

$$4x = 10.63$$

$$x = 2.6575 = n_{\text{C}_4\text{H}_{10} \text{ convertido}}$$

$$n_{\text{H}_2\text{O} \text{ produzidas}} = 5x = 5 \times 2.6575 = 13.29 \text{ moles}$$

$$n_{\text{O}_2 \text{ convertidas}} = \frac{13}{2} x = 17.274 \text{ moles}$$

$$n_{\text{O}_2 \text{ 1}} = n_{\text{O}_2 \text{ convertidas}} + n_{\text{O}_2 \text{ 2}} = 17.274 + 5.12 = 22.394 \text{ moles}$$

a) 100% de conversão de Butano
Não há butano à saída!

$$b) \%Excesso = \left(\frac{N - N_s}{N_s} \right) \times 100$$

N- número de moles do reagente em excesso inicialmente presentes

N_s - número de moles do reagente em excesso estequiometricamente necessário para converter todo o reagente limitante.

$$\%Excesso \text{ O}_2 = \left(\frac{22.394 - 17.274}{17.274} \right) \times 100 = 29.7\%$$

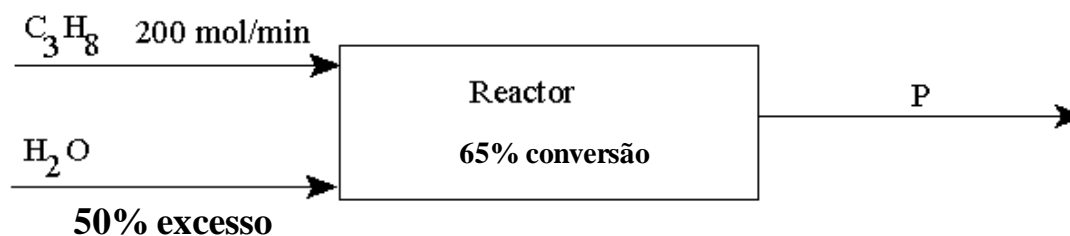
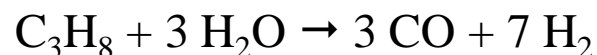
c) Composição molar do efluente

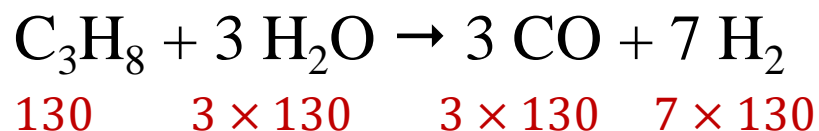
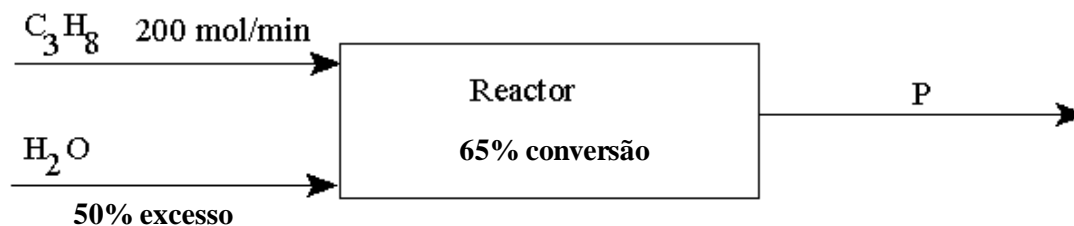
moles	1	2	% 2
C ₄ H ₁₀	2.6575	-	
O ₂	22.394	5.12	4.5
N ₂	84.25	84.25	74.4
CO ₂	-	10.63	9.4
H ₂ O	-	13.29	11.7
		113.29	

$$\%i = \frac{n_i}{n_{Total}} \times 100$$

Prob. 4.7

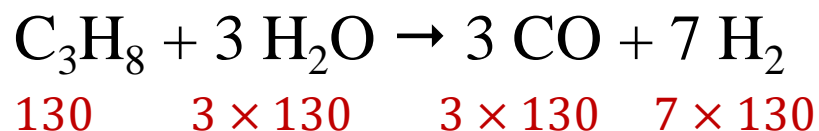
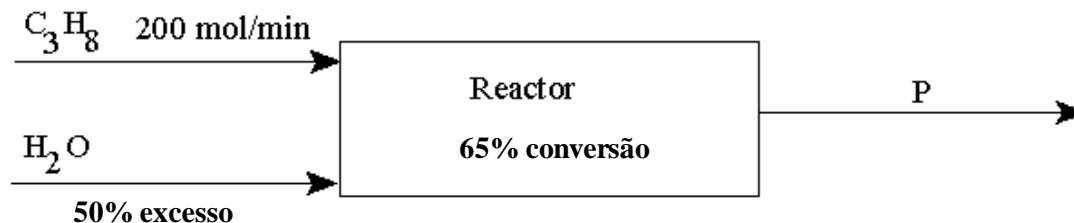
Dimensiona-se um reactor para converter 200 mol/min de propano em CO e H₂ com uma % de conversão de 65%, usando uma % de excesso de 50% de vapor de água. Determine as fracções molares do produto de saída do reactor.



Prob. 4.7


Conversão=65%
 $0.65 \times 200 = 130 \text{ mol}$ que reagem

moles	In	Out	% Out
C ₃ H ₈	200		
H ₂ O			
CO			
H ₂			
Total			

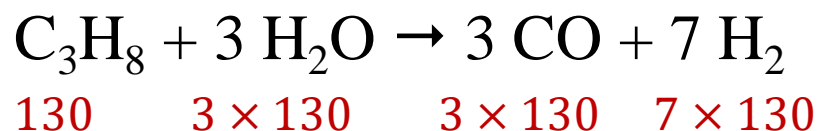
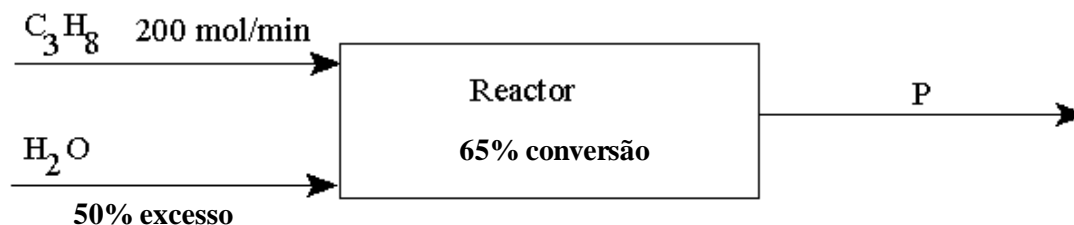
Prob. 4.7


$$\begin{aligned}
 \text{Convers\~ao} &= 65\% \\
 0.65 \times 200 &= 130 \text{ mol que reagem}
 \end{aligned}$$

$$\% \text{Excesso } \text{H}_2\text{O} = \left(\frac{n_{\text{H}_2\text{O inicial}} - 3 \times 200}{3 \times 200} \right) \times 100 = 50\%$$

$$n_{\text{H}_2\text{O inicial}} = 900 \text{ moles}$$

moles	In	Out	% Out
C ₃ H ₈	200		
H ₂ O	900		
CO	-		
H ₂	-		
Total	1100		

Prob. 4.7


$$\begin{aligned}
 \text{Convers\~ao} &= 65\% \\
 0.65 \times 200 &= 130 \text{ mol que reagem}
 \end{aligned}$$

$$\% \text{Excesso } \text{H}_2\text{O} = \left(\frac{n_{\text{H}_2\text{O inicial}} - 3 \times 200}{3 \times 200} \right) \times 100 = 50\%$$

$$n_{\text{H}_2\text{O inicial}} = 900 \text{ moles}$$

moles	In	Out	% Out
C ₃ H ₈	200	70	3.7
H ₂ O	900	510	27.1
CO	-	390	20.7
H ₂	-	910	48.4
Total	1100	1880	

$$n_{\text{C}_3\text{H}_8 \text{ out}} = 200 - 130 = 70 \text{ moles}$$

$$n_{\text{H}_2\text{O que reagem}} = 3 \times 130 = 390 \text{ moles}$$

$$n_{\text{H}_2\text{O out}} = 900 - 390 = 510 \text{ moles}$$

$$n_{\text{CO obtidos}} = 3 \times 130 = 390 \text{ moles}$$

$$\text{— } n_{\text{H}_2 \text{ obtidos}} = 7 \times 130 = 910 \text{ moles} \text{ —}$$