

ERQ I – Teste 1 Resolução

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Questão 1

The reversible reaction $A \rightleftharpoons B$ is carried out in a battery of two CSTR reactors arranged in series, it being known that the second reactor is double the volume of the first reactor. Reagent A is fed to the reactor battery in a concentration of 0.5 mol dm^{-3} at a volumetric flow rate of 20 L/min . The direct and reverse reactions are elementary and the values of the direct reaction kinetic constant and the equilibrium constant are 0.15 min^{-1} and 28, respectively.

Q1 a.

Derive the expression of the rate law.

Resposta

$$-r_A = k ([A] - [B]/k_e) = k ([A]_0 (1 - X) - [A]_0 X/k_e) = k [A]_0 (1 - X (1 + 1/k_e))$$

Q1 b.

For each of the reactors, derive the expressions that relate the volume of the reactor to the conversion.

Resposta

1 Reator:

$$\tau_1 = V_1/v;$$

$$\begin{aligned} 0 &= F_{A0} - F_A + r_{A1} V_1 = F_{A0} - F_{A0} (1 - X_1) + r_{A1} V_1 = \\ &= F_{A0} X_1 + r_{A1} V_1 \implies \\ \implies 0 &= F_{A0} X_1/v + r_{A1} V/v = C_{A0} X_1 + r_{A1} \tau_1 \implies \\ \implies \tau_1 &= \frac{C_{A0} X_1}{-r_{A1}} = \frac{C_{A0} X_1}{k C_{A0} (1 - X_1 (1 + 1/k_e))} = \\ &= \frac{1}{k (1/X_1 - 1 - 1/k_e)} \end{aligned}$$

2 Reator:

$$\tau_2 = V_2/v;$$

$$\begin{aligned} 0 &= F_{A1} - F_{A2} + r_{A2} V_2 = \\ &= F_{A0} (1 - X_1) - F_{A0} (1 - X_2) + r_{A2} V_2 = \\ &= F_{A0} (X_1 - X_2) + r_{A2} V_2 \implies \\ \implies 0 &= F_{A0} (X_1 - X_2)/v + r_{A2} V_2/v = \\ &= C_{A0} (X_1 - X_2) + r_{A2} \tau_2 \implies \\ \implies \tau_2 &= \frac{C_{A0} (X_1 - X_2)}{-r_{A2}} = \frac{C_{A0} (X_1 - X_2)}{k C_{A0} (1 - X_2 (1 + 1/k_e))} = \\ &= \frac{X_1 - X_2}{k (1 - X_2 (1 + 1/k_e))} \end{aligned}$$

Q1 c.

Determine the value of the equilibrium conversion.

Resposta

$$\begin{aligned} X_e &= \frac{[B]_e}{[A]_0} = 1 - \frac{[A]_e}{[A]_0}; \\ \frac{[B]_e}{[A]_e} &= \frac{[A]_0 X_e}{[A]_0 (1 - X_e)} = \frac{1}{1/X_e - 1} = k_e \implies \\ \implies X_e &= \frac{1}{1/k_e + 1} = \frac{1}{1/28 + 1} \cong 0.966 \end{aligned}$$

Q1 d.

Knowing that the conversion at the exit of the 2nd reactor corresponds to 99% of the equilibrium conversion, determine the conversion at the exit of the 1st reactor.

Resposta

$$\begin{aligned} \frac{1}{k (1/X_1 - 1 - 1/k_e)} &= \tau_1 = \\ &= \tau_2/2 = \frac{X_1 - X_2}{2 k (1 - X_2 (1 + 1/k_e))} \implies \\ \implies 0 &= \begin{pmatrix} X_1^2 (1 + 1/k_e) & + \\ -X_1 (1 + X_2 (1 + 5/k_e + 4)) & + \\ +X_2 & \end{pmatrix} = \\ &= \begin{pmatrix} X_1^2 (1 + 1/k_e) & + \\ -X_1 (1 + X_e 0.99 (1 + 5/k_e + 4)) & + \\ +X_e 0.99 & \end{pmatrix} \cong \\ &\cong \begin{pmatrix} X_1^2 (1 + 1/28) & + \\ -X_1 (1 + 0.966 * 0.99 (1 + 5/28 + 4)) & + \\ +0.966 * 0.99 & \end{pmatrix} \cong \\ &\cong \begin{pmatrix} X_1^2 1.036 & + \\ -X_1 2.010 & + \\ +0.956 & \end{pmatrix} \begin{cases} 1.106 \\ 0.834 \end{cases} \therefore X_1 \cong 0.834 \end{aligned}$$

Q1 e.

Determine the volumes of the reactors.

Resposta

$$V_i = v \tau_i;$$

1 Reator

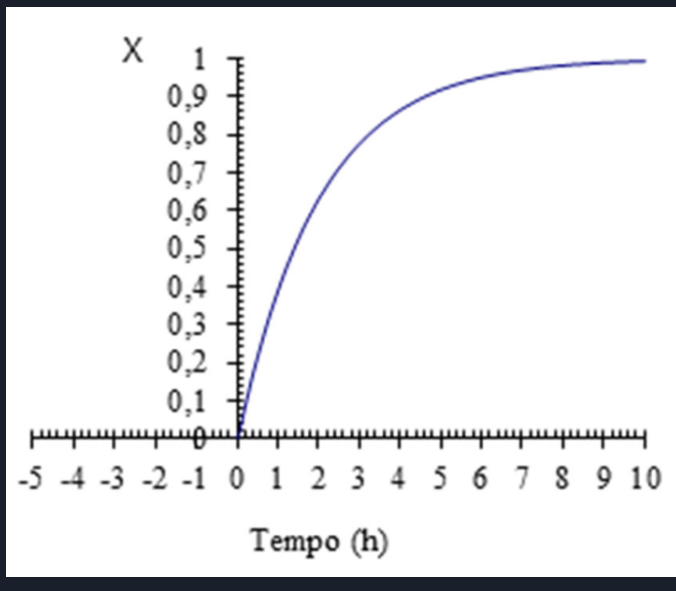
$$\begin{aligned} V_1 &= v \tau_1 = v \left(\frac{1}{k (1/X_1 - 1 - 1/k_e)} \right) \cong \\ &\cong \frac{20}{0.15 (1/0.834 - 1 - 1/28)} \cong 817.409 \end{aligned}$$

2 Reator

$$V_2 = v \tau_2 = v 2 \tau_1 = 2 V_1 \cong 2 817.409 \cong 1634.819$$

Questão 2

The figure shows the kinetic curve obtained in a batch reactor, corresponding to the elemental liquid phase reaction $2A \longrightarrow B$. The reaction is carried out in batch reactors of 5 m^3 , which are loaded with pure A.



Data:

- $t_d = 120 \text{ min}$.
- Molecular weight of A: 58 g/mol .
- Molecular weight of B: 116 g/mol .
- Density of A: 0.791 g/L .
- If you were not able to solve b) use $k = 0.074 \text{ dm}^3 \text{ mol}^{-1} \text{ h}^{-1}$.

Q2 a.

Write the expression of the rate law.

$$-r_A = k C_A^2 = k (C_{A0} (1 - X))^2 = k C_{A0}^2 (1 - X)^2$$

Q2 b.

Write the equation of the curve shown in the graphic.

Resposta

$$\begin{aligned} X = f(t) : -r_A V &= k C_{A0}^2 (1 - X)^2 V = \\ &= -\frac{dN_A}{dt} = -\frac{d(N_{A0}(1 - X))}{dt} = -N_{A0} \frac{d(1 - X)}{dt} = \\ &= -C_{A0} V \frac{d(1 - X)}{dt} \implies \\ \implies -\int_1^{1-X} \frac{d(1 - X)}{(1 - X)^2} &= \\ &= -(-1) \Delta(X^{-1}) \Big|_1^{1-X} = 1/(1 - X) - 1 = \frac{1}{1/X - 1} = \\ &= \int_0^t k C_{A0} dt = k C_{A0} \int_0^t dt = k C_{A0} t \implies \\ \implies X &= (1 + 1/k C_{A0} t)^{-1} \end{aligned}$$

Q2 c.

Evaluate the value of the kinetic constant. Use the graphic.

Resposta

$$\begin{aligned} k : X &= (1 + 1/k C_{A0} t)^{-1} \implies \\ \implies k &= ((1/X - 1) C_{A0} t)^{-1} = \\ &= ((1/X - 1) (N_{A0}/V) t)^{-1} = \\ &= ((1/X - 1) (m_{A0}/M_A V) t)^{-1} = \\ &= ((1/X - 1) (\rho_A V/M_A V) t)^{-1} = \\ &= ((1/X - 1) (\rho_A/M_A) t)^{-1} \cong \\ &\cong ((1/0.6 - 1) (791/58) 1.9)^{-1} \text{ L/mol h} \cong \\ &\cong 57.888 \text{ mL/mol h} \end{aligned}$$

Q2 d.

Calculate the optimal conversion and the optimal reaction time.

Resposta

Traça uma reta entre $(0, -t_d)$ e o gráfico, o ponto tangente é o ótimo:

$$X_{opt} \cong 0.68 \quad t_{opt} \cong 2.3 \text{ h}$$

Q2 e.

If the plant works 24 h day and 330 d/year , determine the number of reactors needed for an annual production of B of 1500 t . Use the conversion calculated in d) but if you were not able to, use any value at your choice.

Resposta



$$N_R = \lceil V_R / 5 \text{ m}^3 \rceil = \lceil 1.15 V / 5 \text{ m}^3 \rceil = \left\lceil \frac{1.15 (N_{A0}/C_{A0})}{5 \text{ m}^3} \right\rceil ;$$

$$\begin{aligned} N_{A0} X/2 &= N_B = \frac{1500 * 10^6}{M_B * N_{batch}} = \frac{1500 * 10^6}{116 * \frac{330 * 24}{t_{batch}}} = \\ &= \frac{1500 * 10^6}{\frac{116 * 330 * 24}{t_{opt} + t_d}} = \frac{1500 * 10^6}{\frac{116 * 330 * 24}{2.3 + 2}} \cong 7.021 \text{ E3 mol} \implies \end{aligned}$$

$$\implies N_{A0} \cong 2 * 7.021 \text{ E3} / 0.68 \cong 20.649 \implies$$

$$\begin{aligned} \implies N_R &\cong \left\lceil \frac{1.15 * 20.649}{(\rho_A/M_A)} \right\rceil = \left\lceil \frac{1.15 * 20.649}{5 * (0.791 * 10^3/58)} \right\rceil \cong \\ &\cong \lceil 0.348 \rceil = 1 \end{aligned}$$