

# FT II – Teste 2024.1 Resolução

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## Conteúdo

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# Questão 1

- Altura:  $h = 30 \text{ cm}$
- Altura líquido A:  $h_0 = 10 \text{ cm}$
- Diâmetro:  $d = 1 \text{ cm}$
- $y_{A,h} = 0$

Dados a  $25^\circ\text{C}$

- $D_{A,ar} = 2 \text{ E}^{-5} \text{ m}^2/\text{s}$
- $P = 1 \text{ atm} = 80 \text{ mmHg} = 10 \text{ E}^5 \text{ Pa}$
- $R = 8.314 \text{ 462 618 J mol}^{-1} \text{ K}^{-1}$
- $M_A = 30 \text{ g/mol}$
- $P_A^* = 80 \text{ mmHg}$
- $\rho_A = 0.9 \text{ E}^3 \text{ kg/m}^3$

Q1 a.

Expressão para evaporação completa em função do tempo

Resposta

Evaporação em geometria linear:

$$\begin{aligned} N_{A,z} &= Q_A = \\ &= -C_{A,ar} \frac{dV}{dt} = -C_{A,ar} \frac{d\pi (d/2)^2 z}{dt} = -C_{A,ar} \pi (d/2)^2 \frac{dz}{dt} \implies \\ \implies \int_0^t N_{A,z} dt &= N_{A,z} \int_0^t dt = N_{A,z} t = \\ &= \int_{h/3}^0 -C_{A,ar} \pi d^2 dz / 4 = -\frac{C_{A,ar} \pi d^2}{4} (-h/3) \implies \\ \implies N_{A,z} &= \frac{C_{A,ar} \pi d^2}{12} h/t \end{aligned}$$

Condições de fronteira para fluxo:

$$\begin{cases} z = h_0 & y_A = y_A^* \\ z = h & y_A = 0 \end{cases};$$

Fluxo molar:

$$\begin{aligned} N_A &= y_{A,z} N_A - C \mathcal{D}_{A,ar} \frac{dy_{A,z}}{dz} \implies \\ \implies \int N_A dz &= N_A (h - h_0) = \\ &= \int_{y_A^*}^0 -C \mathcal{D}_{A,ar} \frac{dy_{A,z}}{1 - y_{A,z}} = \\ &= C \mathcal{D}_{A,ar} \int_{y_A^*}^0 \frac{d(1 - y_{A,z})}{1 - y_{A,z}} = \\ &= C \mathcal{D}_{A,ar} \ln(1 - y_{A,z}^*) \implies \\ \implies N_A &= \frac{C \mathcal{D}_{A,ar}}{h - h_0} \ln(1 - y_{A,z}^*) \end{aligned}$$

Q1 b.

Calcule esse tempo

Q1 c.

Novo tempo para metade da altura e dobro do diâmetro, commente

## Questão 2

- $d = 1 \text{ cm}$
- $T = 1500 \text{ K}$
- $P = 1 \text{ atm}$
- Velocidade limit pela dif do  $\text{O}_2$
- $M = 1280 \text{ kg/m}^3$
- $\mathcal{D}_{\text{O}_2,ar} = 1 \text{ E}^{-4} \text{ m}^2/\text{s}$



Q2 a.

Expr: vel de consumo de  $\text{O}_2$  e cond fronteira

Resposta

$$\begin{aligned} N_{\text{O}_2,r} &= \\ &= y_{\text{O}_2,r} (N_{\text{C}} + N_{\text{O}_2} + N_{\text{CO}} + N_{\text{CO}_2}) - C \mathcal{D}_{\text{O}_2,ar} \frac{dy_{\text{O}_2,r}}{dr} = \\ &= y_{\text{O}_2,r} (N_{\text{O}_2}/3 + N_{\text{O}_2}/2 - N_{\text{O}_2}/2 - N_{\text{O}_2}) - C \mathcal{D}_{\text{O}_2,ar} \frac{dy_{\text{O}_2,r}}{dr} = \\ &= y_{\text{O}_2,r} N_{\text{O}_2} (-2/3) - C \mathcal{D}_{\text{O}_2,ar} \frac{dy_{\text{O}_2,r}}{dr} \implies \end{aligned}$$

Condições de fronteira

$$\begin{aligned} &\begin{cases} r = R & y_{\text{O}_2} = 0 \\ r = \infty & y_{\text{O}_2} = y_{\text{O}_2}^* \end{cases} \\ \implies \int_R^\infty N_{\text{O}_2} dr &= \int_R^\infty \frac{Q_{\text{O}_2}}{4\pi r^2} dr = \frac{Q_{\text{O}_2}}{4\pi} \int_R^\infty \frac{dr}{r^2} = \\ &= \frac{Q_{\text{O}_2}}{4\pi} (R^{-1} - 0) = \frac{Q_{\text{O}_2}}{4\pi R} = \\ &= -C \mathcal{D}_{\text{O}_2,ar} \frac{dy_{\text{O}_2,r}}{1 + y_{\text{O}_2,r} 2/3} = -\frac{C \mathcal{D}_{\text{O}_2,ar}}{2/3} \frac{d(1 + y_{\text{O}_2,r} 2/3)}{1 + y_{\text{O}_2,r} 2/3} = \\ &= -\frac{C \mathcal{D}_{\text{O}_2,ar}}{2/3} \ln(1 + y_{\text{O}_2,r}^* 2/3) \implies \\ \implies Q_{\text{O}_2} &= -\frac{4\pi R C \mathcal{D}_{\text{O}_2,ar}}{2/3} \ln(1 + y_{\text{O}_2,r}^* 2/3) = \\ &= -\frac{4\pi R P \mathcal{D}_{\text{O}_2,ar}}{RT 2/3} \ln(1 + y_{\text{O}_2,r}^* 2/3) \end{aligned}$$

Q2 b.

Vel de consumo de C