OSF - Equipment Size reduction

Felipe B. Pinto 61387 – MIEQB

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1 Crushing rolls

Compress particles between two rolls

$$\coseta/2=rac{r_1+b/2}{r_1+r_2}.$$

 r_1 : Roll radius

 r_2 : Feed particle size

b: Distance between rolls

 $\beta = 31^{\circ}$: Parametrizado em 31°

2 Jaw Crushers

Crush the particles between two jaw like contraptions

• Two jaws one fixed one mobile

- Nin angle a. 30
- Nip angle $\sim 30^\circ$
- Coarse reduction

3 Energy for size reduction

Very low efficiency $0.1 \rightarrow 2.0$ but effetive size reduction

- · In producing elastic deformation of the particles before fracture occurs
- In causing elastic distortion of the equipment.
- In friction between particles, and between particles and the machine.
- In noise, heat and vibration in the plant, and In friction losses in the plant itself.

Empirical Law of Energy for size reduction

$$rac{\mathrm{d} E}{\mathrm{d} L} = -C\,L^p$$

- E Energy spent for size reduction [kJ/kg]
- L size of solids calculated as the mean diameter based on voume (d_V/m) Alternativelly Bond's diameter (d_{bond}/m) can be used, its estimated as the mesh size trough which 80% of the material passes in a sieving characterization experiment.
- C empirical constant related to the solid properties and equipment properties
- p empirical constant related to the size of solids
 - $\cdot = -1.0$ Coarse reduction
 - $\cdot = -1.5$ Intermediate reduction
 - $\cdot = -2.0$ Fine reduction

Specifying p for each reduction and integrating we derive the following three laws

Rittinger's law (Fine reduction, p = -2.0)

$$E=C\; \Delta L^{-1}=K_R\, f_c\; \Delta L^{-1}$$
 $C=K_R\, f_c egin{cases} K_R: & ext{Depende do triturador} \ f_c: & ext{Depende das particulas} \end{cases}$

Note: Greater efficiency, $E \propto d^{-1}$

Bond's Law (Intermediate reduction, p = -1.5)

$$E = 2\,C\,\,\Delta L^{-1/2} = E_i\,\sqrt{100/L_1}\,\Big(1-q^{-1/2}\Big) \ egin{cases} C = E_i\,\sqrt{100} \ q = L_0/L_1 \end{cases}$$

Notes: Intermediate Efficiency, $E \propto L_0^{-1}$

Kick's Law (Coarse reduction, p = -1.0)

$$E=C \; \Delta \ln L = K_K \, f_c \; \Delta \ln L$$
 $C=K_K \, f_c \, egin{cases} K_K: \; ext{ Depende do triturador} \ f_c: \; ext{ Depende das particulas} \end{cases}$

Notes: Less energy efficiency, $E \propto L_0/L_1$