

高精度状态方程

包括两相区，PVT，亥姆霍兹型

参数来源于经验，优点是极端条件也比较准确，不足是无法计算混合物 PVT

也可以用于实验数据较不广泛和较不准确的物质（参数用哪个？？？）

$$\frac{a(T, \rho)}{RT} = \frac{a^{\text{id}}(T, \rho) + a^{\text{R}}(T, \rho)}{RT} = \alpha^{\text{id}}(\tau, \delta) + \alpha^{\text{R}}(\tau, \delta) \quad (2.108)$$

$$\tau = T_c/T, \quad \delta = \rho/\rho_c = \frac{m/V}{m/V_c} = V_c/V$$

$$\begin{aligned} a^{\text{id}}(T, v) &= u^{\text{id}}(T) - Ts^{\text{id}}(T, v) \\ &= \int_{T_0}^T c_v^{\text{id}} dT - T \int_{T_0}^T c_v^{\text{id}} \frac{dT}{T} - RT \ln \frac{v}{v_0} + a(T_0, v_0) \end{aligned} \quad (2.109)$$

or

$$a^{\text{id}}(T, \rho) = \int_{T_0}^T c_v^{\text{id}} dT - T \int_{T_0}^T c_v^{\text{id}} \frac{dT}{T} + RT \ln \frac{\rho}{\rho_0} + a(T_0, \rho_0) \quad (2.110)$$

Table 2.3 Typical accuracy demands for technical equations of state [29].

	$\rho(P, T)$ [%]	$w^*(P, T)$ [%]	$c_p(P, T)$ [%]	$P^s(T)$ [%]	$\rho'(T)$ [%]	$\rho''(T)$ [%]
$P < 30$ MPa	0.2	1–2	1–2	0.2	0.2	0.2
$P > 30$ MPa	0.5	2	2	—	—	—

For nonpolar fluids [32, 33] (methane, ethane, propane, n-butane, n-pentane, n-hexane, n-heptane, n-octane, argon, oxygen, nitrogen, ethylene, isobutane, cyclohexane, sulfur hexafluoride, carbon monoxide, carbonyl sulfide, n-decane, hydrogen sulfide, isopentane, neopentane, isohexane, krypton, n-nonane, toluene, xenon, and R116 六氟乙烷):

$$\begin{aligned} \alpha^{\text{R}}(\tau, \delta) &= n_1 \delta \tau^{0.25} + n_2 \delta \tau^{1.125} + n_3 \delta \tau^{1.5} + n_4 \delta^2 \tau^{1.375} + n_5 \delta^3 \tau^{0.25} + n_6 \delta^7 \tau^{0.875} \\ &\quad + n_7 \delta^2 \tau^{0.625} e^{-\delta} + n_8 \delta^5 \tau^{1.75} e^{-\delta} + n_9 \delta \tau^{3.625} e^{-\delta^2} + n_{10} \delta^4 \tau^{3.625} e^{-\delta^2} \\ &\quad + n_{11} \delta^3 \tau^{14.5} e^{-\delta^3} + n_{12} \delta^4 \tau^{12} e^{-\delta^3} \end{aligned} \quad (2.112)$$

For polar fluids [33, 34] (R11, R12, R22, R32, R113, R123, R125, R134a, R143a, R152a, carbon dioxide, ammonia, acetone, nitrous oxide, sulfur dioxide [35], R141b, 1,1-二氯-1-氟乙烷, R142b, 1-氯-1,1-二氟乙烷, R218 八氟丙烷, and R245fa, 1,1,1,3,3-五氟丙烷):

$$\begin{aligned} \alpha^{\text{R}}(\tau, \delta) &= n_1 \delta \tau^{0.25} + n_2 \delta \tau^{1.25} + n_3 \delta \tau^{1.5} + n_4 \delta^3 \tau^{0.25} + n_5 \delta^7 \tau^{0.875} + n_6 \delta \tau^{2.375} e^{-\delta} \\ &\quad + n_7 \delta^2 \tau^2 e^{-\delta} + n_8 \delta^5 \tau^{2.125} e^{-\delta} + n_9 \delta \tau^{3.5} e^{-\delta^2} + n_{10} \delta \tau^{6.5} e^{-\delta^2} \\ &\quad + n_{11} \delta^4 \tau^{4.75} e^{-\delta^2} + n_{12} \delta^2 \tau^{12.5} e^{-\delta^3} \end{aligned} \quad (2.113)$$

$$P(T, \rho) = -(\partial a / \partial v)_T = \rho RT \left[1 + \delta \left(\frac{\partial \alpha^{\text{R}}}{\partial \delta} \right)_{\tau} \right] \quad (2.114)$$

Appendix B

Coefficients for High-Precision Equations of State

Table B.1 Coefficients for nonpolar fluids (Eq. (2.113)).

	Methane	Ethane	Propane	<i>n</i> -Butane	<i>n</i> -Pentane
Coefficients	1	2	3	4	5
n_1	0.89269676	0.97628068	1.0403973	1.0626277	1.0968643
n_2	-2.5438282	-2.6905251	-2.8318404	-2.8620952	-2.9988888
n_3	0.64980978	0.73498222	0.8439381	0.88738233	0.99516887
n_4	0.020793471	-0.035366206	-0.076559592	-0.12570581	-0.16170709
n_5	0.070189104	0.084692031	0.094697373	0.10286309	0.1133446
n_6	0.00023700378	0.00024154594	0.00024796475	0.00025358041	0.00026760595
n_7	0.16653334	0.23964954	0.2774376	0.323252	0.40979882
n_8	-0.043855669	-0.042780093	-0.043846001	-0.037950761	-0.040876423
n_9	-0.1572678	-0.22308832	-0.26991065	-0.32534802	-0.38169482
n_{10}	-0.035311675	-0.051799954	-0.069313413	-0.079050969	-0.10931957
n_{11}	-0.029570024	-0.027178426	-0.029632146	-0.020636721	-0.032073223
n_{12}	0.014019842	0.011246305	0.014040127	0.0057053809	0.016877016

	<i>n</i> -Hexane	<i>n</i> -Heptane	<i>n</i> -Octane	Argon	Oxygen
Coefficients	6	7	8	9	10
n_1	1.0553238	1.0543748	1.0722545	0.85095715	0.88878286
n_2	-2.6120616	-2.6500682	-2.4632951	-2.4003223	-2.4879433
n_3	0.76613883	0.81730048	0.65386674	0.54127841	0.59750191
n_4	-0.29770321	-0.30451391	-0.36324974	0.016919771	0.0096501817
n_5	0.11879908	0.12253869	0.1271327	0.068825965	0.071970429
n_6	0.00027922861	0.00027266473	0.00030713573	0.00021428033	0.00022337443
n_7	0.4634759	0.49865826	0.52656857	0.17429895	0.18558686
n_8	0.011433197	-0.00071432815	0.019362863	-0.033654496	-0.038129368
n_9	-0.48256969	-0.54236896	-0.58939427	-0.135268	-0.15352245
n_{10}	-0.093750559	-0.13801822	-0.14069964	-0.016387351	-0.026726815
n_{11}	-0.0067273247	-0.0061595287	-0.0078966331	-0.024987667	-0.025675299
n_{12}	-0.0051141584	0.0004860251	0.0033036598	0.0088769205	0.0095714302

(Continued)

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Table B.1 (Continued)

	Nitrogen	Ethylene	Isobutane	Cyclohexane	SF ₆
Coefficients	11	12	13	14	15
n_1	0.92296567	0.9096223	1.0429332	1.0232354	1.2279403
n_2	-2.5575012	-2.4641015	-2.8184273	-2.9204964	-3.3035623
n_3	0.64482463	0.56175311	0.86176232	1.073663	1.2094019
n_4	0.01083102	-0.019688013	-0.10613619	-0.19573985	-0.12316
n_5	0.073924167	0.078831145	0.098615749	0.12228111	0.11044657
n_6	0.00023532962	0.00021478776	0.00023948209	0.00028943321	0.00032952153
n_7	0.18024854	0.23151337	0.30330005	0.27231767	0.27017629
n_8	-0.045660299	-0.037804454	-0.041598156	-0.04483332	-0.062910351
n_9	-0.1552106	-0.20122739	-0.29991937	-0.38253334	-0.3182889
n_{10}	-0.03811149	-0.044960157	-0.080369343	-0.089835333	-0.099557419
n_{11}	-0.031962422	-0.02834296	-0.029761373	-0.024874965	-0.036909694
n_{12}	0.015513532	0.012652824	0.01305963	0.010836132	0.019136427

	Carbon monoxide	Carbonyl sulfide	<i>n</i> -Decane	Hydrogen sulfide	Isopentane
Coefficients	16	17	18	19	20
n_1	0.90554	0.94374	1.0461	0.87641	1.0963
n_2	-2.4515	-2.5348	-2.4807	-2.0367	-3.0402
n_3	0.53149	0.59058	0.74372	0.21634	1.0317
n_4	0.024173	-0.021488	-0.52579	-0.050199	-0.1541
n_5	0.072156	0.082083	0.15315	0.066994	0.11535
n_6	0.00018818	0.00024689	0.00032865	0.00019076	0.00029809
n_7	0.19405	0.21226	0.84178	0.20227	0.39571
n_8	-0.043268	-0.041251	0.055424	-0.0045348	-0.045881
n_9	-0.12778	-0.22333	-0.73555	-0.2223	-0.35804
n_{10}	-0.027896	-0.050828	-0.18507	-0.034714	-0.10107
n_{11}	-0.034154	-0.028333	-0.020775	-0.014885	-0.035484
n_{12}	0.016329	0.016983	0.012335	0.0074154	0.018156

Table B.1 (Continued)

	Neopentane	Isohexane	Krypton	<i>n</i> -Nonane	Toluene
Coefficients	21	22	23	24	25
n_1	1.1136	1.1027	0.83561	1.1151	0.96464
n_2	-3.1792	-2.9699	-2.3725	-2.702	-2.7855
n_3	1.1411	1.0295	0.54567	0.83416	0.86712
n_4	-0.10467	-0.21238	0.014361	-0.38828	-0.1886
n_5	0.11754	0.11897	0.066502	0.1376	0.11804
n_6	0.00034058	0.00027738	0.0001931	0.00028185	0.00025181
n_7	0.29553	0.40103	0.16818	0.62037	0.57196
n_8	-0.074765	-0.034238	-0.033133	0.015847	-0.029287
n_9	-0.31474	-0.43584	-0.15008	-0.61726	-0.43351
n_{10}	-0.099401	-0.11693	-0.022897	-0.15043	-0.1254
n_{11}	-0.039569	-0.019262	-0.021454	-0.012982	-0.028207
n_{12}	0.023177	0.0080783	0.0069397	0.0044325	0.014076

	Xenon	R116
Coefficients	26	27
n_1	0.83115	1.1632
n_2	-2.3553	-2.8123
n_3	0.53904	0.77202
n_4	0.014382	-0.14331
n_5	0.066309	0.10227
n_6	0.00019649	0.00024629
n_7	0.14996	0.30893
n_8	-0.035319	-0.028499
n_9	-0.15929	-0.30343
n_{10}	-0.027521	-0.068793
n_{11}	-0.023305	-0.027218
n_{12}	0.0086941	0.010665

Table B.2 Coefficients for polar fluids (Eq. (2.114)).

	R11	R12	R22	R32
Coefficients	1	2	3	4
n_1	1.0656383	1.0557228	0.96268924	0.92876414
n_2	−3.2495206	−3.3312001	−2.5275103	−2.4673952
n_3	0.87823894	1.0197244	0.31308745	0.40129043
n_4	0.087611569	0.084155115	0.072432837	0.055101049
n_5	0.00029950049	0.00028520742	0.00021930233	0.00011559754
n_6	0.42896949	0.39625057	0.33294864	−0.25209758
n_7	0.70828452	0.63995721	0.63201229	0.42091879
n_8	−0.017391823	−0.021423411	−0.0032787841	0.0037071833
n_9	−0.37626522	−0.36249173	−0.33680834	−0.10308607
n_{10}	0.011605284	0.001934199	−0.022749022	−0.11592089
n_{11}	−0.089550567	−0.092993833	−0.087867308	−0.044350855
n_{12}	−0.030063991	−0.024876461	−0.021108145	−0.012788805
	R113	R123	R125	R134a
Coefficients	5	6	7	8
n_1	1.0519071	1.116973	1.1290996	1.0663189
n_2	−2.8724742	−3.074593	−2.8349269	−2.449597
n_3	0.41983153	0.51063873	0.29968733	0.044645718
n_4	0.087107788	0.094478812	0.087282204	0.075656884
n_5	0.00024105194	0.00029532752	0.00026347747	0.00020652089
n_6	0.70738262	0.66974438	0.61056963	0.42006912
n_7	0.93513411	0.96438575	0.90073581	0.76739111
n_8	−0.0096713512	−0.014865424	−0.0068788457	0.0017897427
n_9	−0.52595315	−0.49221959	−0.44211186	−0.36219746
n_{10}	0.022691984	−0.022831038	−0.035041493	−0.06780937
n_{11}	−0.14556325	−0.1407486	−0.1269863	−0.10616419
n_{12}	−0.02741995	−0.025117301	−0.025185874	−0.018185791

Table B.2 (Continued)

	R143a	R152a	Carbon dioxide	Ammonia
Coefficients	9	10	11	12
n_1	1.0306886	0.95702326	0.89875108	0.7302272
n_2	-2.9497307	-2.3707196	-2.1281985	-1.1879116
n_3	0.6943523	0.18748463	-0.06819032	-0.68319136
n_4	0.071552102	0.063800843	0.076355306	0.040028683
n_5	0.00019155982	0.00016625977	0.00022053253	0.000090801215
n_6	0.079764936	0.082208165	0.41541823	-0.056216175
n_7	0.56859424	0.57243518	0.71335657	0.44935601
n_8	-0.0090946566	0.0039476701	0.00030354234	0.029897121
n_9	-0.24199452	-0.23848654	-0.36643143	-0.18181684
n_{10}	-0.070610813	-0.080711618	-0.0014407781	-0.09841666
n_{11}	-0.075041709	-0.073103558	-0.089166707	-0.055083744
n_{12}	-0.016411241	-0.015538724	-0.023699887	-0.0088983219
	Acetone	N ₂ O	Sulfur dioxide	R141b
Coefficients	13	14	15	16
n_1	0.90041	0.88045	0.93061	1.1469
n_2	-2.1267	-2.4235	-1.9528	-3.6799
n_3	-0.083409	0.38237	-0.17467	1.3469
n_4	0.065683	0.068917	0.061524	0.083329
n_5	0.00016527	0.00020367	0.00017711	0.00025137
n_6	-0.039663	0.13122	0.21615	0.3272
n_7	0.72085	0.46032	0.51353	0.46946
n_8	0.0092318	-0.0036985	0.010419	-0.029829
n_9	-0.17217	-0.23263	-0.25286	-0.31621
n_{10}	-0.14961	-0.00042859	-0.05472	-0.026219
n_{11}	-0.076124	-0.04281	-0.059856	-0.078043
n_{12}	-0.018166	-0.023038	-0.016523	-0.020498

(Continued)

Table B.2 (Continued)

	R142b	R218	R245fa
Coefficients	17	18	19
n_1	1.0038	1.327	1.2904
n_2	-2.7662	-3.8433	-3.2154
n_3	0.42921	0.922	0.50693
n_4	0.081363	0.1136	0.093148
n_5	0.00024174	0.00036195	0.00027638
n_6	0.48246	1.1001	0.71458
n_7	0.75542	1.1896	0.87252
n_8	-0.00743	-0.025147	-0.015077
n_9	-0.4146	-0.65923	-0.40645
n_{10}	-0.016558	-0.027969	-0.11701
n_{11}	-0.10644	-0.1833	-0.13062
n_{12}	-0.021704	-0.02163	-0.022952

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