

# PID controllers and modified PID controllers

Dr. Ing. Rodrigo Gonzalez

`rodrazalez@fing.uncu.edu.ar`

Control y Sistemas, Facultad de Ingeniería, Universidad Nacional de Cuyo

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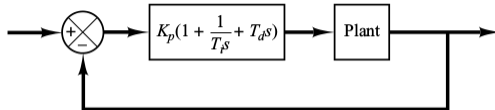
- 1 Ziegler–Nichols Rules for Tuning PID Controllers
- 2 Design of PID Controllers with Computational Optimization Approach
- 3 Modifications of PID Control Schemes
- 4 Two-Degrees-of-Freedom Control Systems
- 5 Zero-Placement Approach to Improve Response Characteristics

# Ziegler–Nichols Rules for Tuning PID Controllers

## PID Control of Plants

- If the plant mathematical model cannot be easily obtained, then an analytical or computational approach to the design of a PID controller is not possible.
- Then we must resort to experimental approaches to the tuning of PID controllers.
- Ziegler and Nichols suggested rules for tuning PID controllers (values  $K_p$ ,  $T_i$ , and  $T_d$ ) based on:
  - Experimental step responses (Method 1) or
  - Based on the value of  $K_p$  that results in marginal stability when only proportional control action is used (Method 2).

**Figure 8–1**  
PID control  
of a plant.



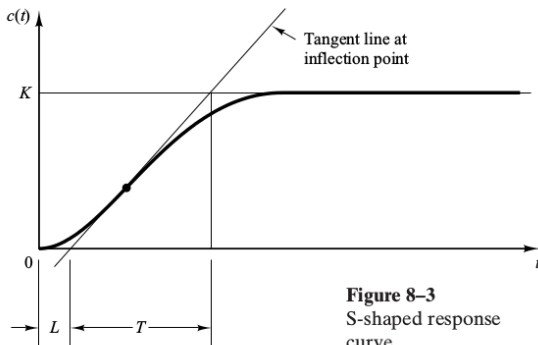
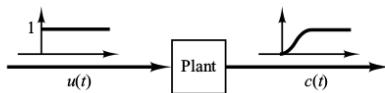
# Ziegler–Nichols Rules for Tuning PID Controllers

## First Method

- We obtain experimentally the response of the plant to a unit-step input.
- This method applies if the response to a step input exhibits an S-shaped curve.

**Figure 8–2**

Unit-step response of a plant.



**Figure 8–3**  
S-shaped response curve.

# Ziegler–Nichols Rules for Tuning PID Controllers

## First Method

**Table 8–1** Ziegler–Nichols Tuning Rule Based on Step Response of Plant (First Method)

Type of Controller	$K_p$	$T_i$	$T_d$
P	$\frac{T}{L}$	$\infty$	0
PI	$0.9 \frac{T}{L}$	$\frac{L}{0.3}$	0
PID	$1.2 \frac{T}{L}$	$2L$	$0.5L$

function  $C(s)/U(s)$  may then be approximated by a first-order system with a transport lag as follows:

$$\frac{C(s)}{U(s)} = \frac{Ke^{-Ls}}{Ts + 1}$$

Ziegler and Nichols suggested to set the values of  $K_p$ ,  $T_i$ , and  $T_d$  according to the formula shown in Table 8–1.

Notice that the PID controller tuned by the first method of Ziegler–Nichols rules gives

$$\begin{aligned} G_c(s) &= K_p \left( 1 + \frac{1}{T_i s} + T_d s \right) \\ &= 1.2 \frac{T}{L} \left( 1 + \frac{1}{2Ls} + 0.5Ls \right) \\ &= 0.6T \frac{\left( s + \frac{1}{L} \right)^2}{s} \end{aligned}$$

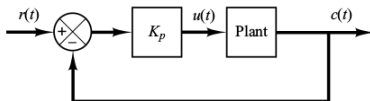
Thus, the PID controller has a pole at the origin and double zeros at  $s = -1/L$ .

# Ziegler–Nichols Rules for Tuning PID Controllers

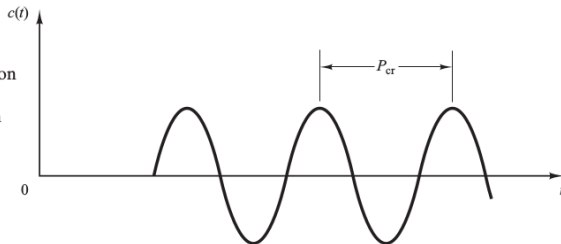
## Second Method

- We first set  $T_i = \infty$ , and  $T_d = 0$
- Increase  $K_p$  from 0 to a critical value  $K_{cr}$  at which the output first exhibits sustained oscillations.
- Thus, the critical gain  $K_{cr}$  and the corresponding period  $P_{cr}$  are experimentally determined.

**Figure 8–4**  
Closed-loop system with a proportional controller.



**Figure 8–5**  
Sustained oscillation with period  $P_{cr}$ .  
( $P_{cr}$  is measured in sec.)



# Ziegler–Nichols Rules for Tuning PID Controllers

## Second Method

**Table 8–2** Ziegler–Nichols Tuning Rule Based on Critical Gain  $K_{cr}$  and Critical Period  $P_{cr}$  (Second Method)

Type of Controller	$K_p$	$T_i$	$T_d$
P	$0.5K_{cr}$	$\infty$	0
PI	$0.45K_{cr}$	$\frac{1}{1.2} P_{cr}$	0
PID	$0.6K_{cr}$	$0.5P_{cr}$	$0.125P_{cr}$

Notice that the PID controller tuned by the second method of Ziegler–Nichols rules gives

$$\begin{aligned} G_c(s) &= K_p \left( 1 + \frac{1}{T_i s} + T_d s \right) \\ &= 0.6K_{cr} \left( 1 + \frac{1}{0.5P_{cr}s} + 0.125P_{cr}s \right) \\ &= 0.075K_{cr}P_{cr} \frac{\left( s + \frac{4}{P_{cr}} \right)^2}{s} \end{aligned}$$

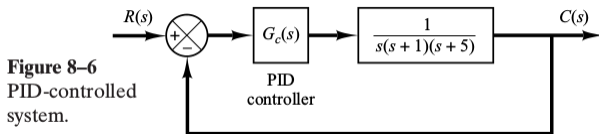
Thus, the PID controller has a pole at the origin and double zeros at  $s = -4/P_{cr}$ .



**EXAMPLE 8-1** Consider the control system shown in Figure 8-6 in which a PID controller is used to control the system. The PID controller has the transfer function

$$G_c(s) = K_p \left( 1 + \frac{1}{T_i s} + T_d s \right)$$

Although many analytical methods are available for the design of a PID controller for the present system, let us apply a Ziegler–Nichols tuning rule for the determination of the values of parameters  $K_p$ ,  $T_i$ , and  $T_d$ . Then obtain a unit-step response curve and check to see if the designed system exhibits approximately 25% maximum overshoot. If the maximum overshoot is excessive (40% or more), make a fine tuning and reduce the amount of the maximum overshoot to approximately 25% or less.



**EXAMPLE 8-2** Consider the PID-controlled system shown in Figure 8-19. The PID controller is given by

$$G_c(s) = K \frac{(s + a)^2}{s}$$

It is desired to find a combination of  $K$  and  $a$  such that the closed-loop system will have 10% (or less) maximum overshoot in the unit-step response. (We will not include any other condition in this problem. But other conditions can easily be included, such as that the settling time be less than a specified value. See, for example, Example 8-3.)

There may be more than one set of parameters that satisfy the specifications. In this example, we shall obtain all sets of parameters that satisfy the given specifications.

To solve this problem with MATLAB, we first specify the region to search for appropriate  $K$  and  $a$ . We then write a MATLAB program that, in the unit-step response, will find a combination of  $K$  and  $a$  which will satisfy the criterion that the maximum overshoot is 10% or less.

Note that the gain  $K$  should not be too large, so as to avoid the possibility that the system require an unnecessarily large power unit.

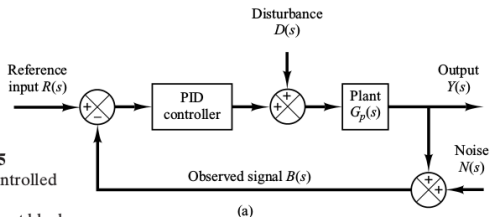
Assume that the region to search for  $K$  and  $a$  is

$$2 \leq K \leq 3 \quad \text{and} \quad 0.5 \leq a \leq 1.5$$

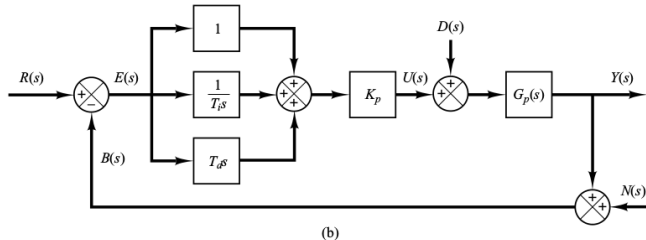
# Modifications of PID Control Schemes

## PI-D Control

- If  $u(t)$  change abruptly, the derivative term in the control action will involve an impulse function.
- Such a phenomenon is called *set-point kick*.



**Figure 8-25**  
(a) PID-controlled system;  
(b) equivalent block diagram.



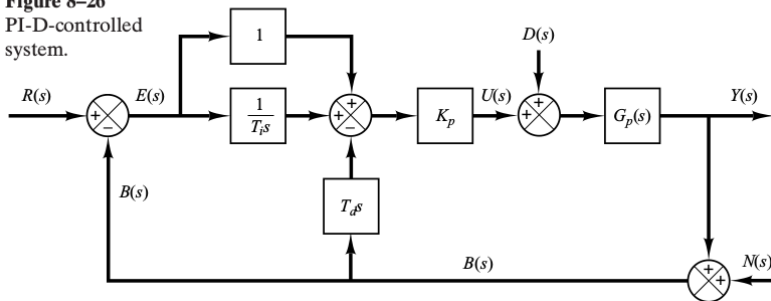
# Modifications of PID Control Schemes

## PI-D Control

$$U(s) = K_p \left( 1 + \frac{1}{T_i s} \right) R(s) - K_p \left( 1 + \frac{1}{T_i s} + T_d s \right) B(s)$$

**Figure 8–26**

PI-D-controlled system.



Notice that in the absence of the disturbances and noises, the closed-loop transfer function of the basic PID control system [shown in Figure 8–25(b)] and the PI-D control system (shown in Figure 8–26) are given, respectively, by

$$\frac{Y(s)}{R(s)} = \left(1 + \frac{1}{T_i s} + T_d s\right) \frac{K_p G_p(s)}{1 + \left(1 + \frac{1}{T_i s} + T_d s\right) K_p G_p(s)}$$

and

$$\frac{Y(s)}{R(s)} = \left(1 + \frac{1}{T_i s}\right) \frac{K_p G_p(s)}{1 + \left(1 + \frac{1}{T_i s} + T_d s\right) K_p G_p(s)}$$

It is important to point out that in the absence of the reference input and noises, the closed-loop transfer function between the disturbance  $D(s)$  and the output  $Y(s)$  in either case is the same and is given by

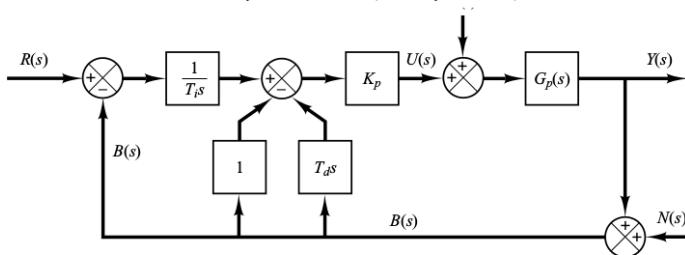
$$\frac{Y(s)}{D(s)} = \frac{G_p(s)}{1 + K_p G_p(s) \left(1 + \frac{1}{T_i s} + T_d s\right)}$$

# Modifications of PID Control Schemes

## I-PD Control

- The proportional action and derivative action are moved to the feedback path so that these actions affect the feedback signal only.

$$U(s) = K_p \frac{1}{T_i s} R(s) - K_p \left( 1 + \frac{1}{T_i s} + T_d s \right) B(s)$$

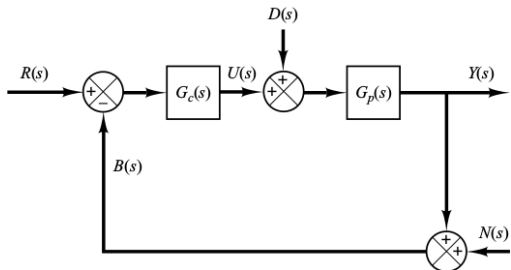


The closed-loop transfer function  $Y(s)/R(s)$  in the absence of the disturbance input and noise input is given by

$$\frac{Y(s)}{R(s)} = \left( \frac{1}{T_i s} \right) \frac{K_p G_p(s)}{1 + K_p G_p(s) \left( 1 + \frac{1}{T_i s} + T_d s \right)}$$

# Two-Degrees-of-Freedom Control Systems

## One-degree-of-freedom Control System



For this system, three closed-loop transfer functions  $Y(s)/R(s) = G_{yr}$ ,  $Y(s)/D(s) = G_{yd}$ , and  $Y(s)/N(s) = G_{yn}$  may be derived. They are

$$G_{yr} = \frac{Y(s)}{R(s)} = \frac{G_c G_p}{1 + G_c G_p}$$

$$G_{yd} = \frac{Y(s)}{D(s)} = \frac{G_p}{1 + G_c G_p}$$

$$G_{yn} = \frac{Y(s)}{N(s)} = -\frac{G_c G_p}{1 + G_c G_p}$$

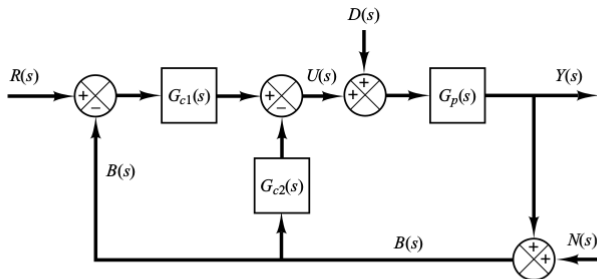
$$G_{yr} = \frac{G_p - G_{yd}}{G_p}$$

$$G_{yn} = \frac{G_{yd} - G_p}{G_p}$$

How many of these closed-loop transfer functions are independent?

# Two-Degrees-of-Freedom Control Systems

## Two-degree-of-freedom Control System



$$G_{yr} = \frac{Y(s)}{R(s)} = \frac{G_{c1}G_p}{1 + (G_{c1} + G_{c2})G_p}$$

$$G_{yd} = \frac{Y(s)}{D(s)} = \frac{G_p}{1 + (G_{c1} + G_{c2})G_p}$$

$$G_{yn} = \frac{Y(s)}{N(s)} = -\frac{(G_{c1} + G_{c2})G_p}{1 + (G_{c1} + G_{c2})G_p}$$

$$G_{yr} = G_{c1}G_{yd}$$

$$G_{yn} = \frac{G_{yd} - G_p}{G_p}$$

How many of these closed-loop transfer functions are independent?



# Two-Degrees-of-Freedom Control Systems

## Two-degree-of-freedom Control System (2)

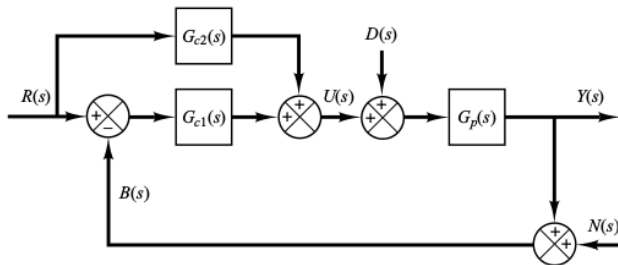
$$G_{yr} = \frac{Y(s)}{R(s)} = \frac{G_{c1}G_p}{1 + G_{c1}G_p} + \frac{G_{c2}G_p}{1 + G_{c1}G_p}$$

$$G_{yd} = \frac{Y(s)}{D(s)} = \frac{G_p}{1 + G_{c1}G_p}$$

$$G_{yn} = \frac{Y(s)}{N(s)} = -\frac{G_{c1}G_p}{1 + G_{c1}G_p}$$

$$G_{yr} = G_{c2}G_{yd} + \frac{G_p - G_{yd}}{G_p}$$

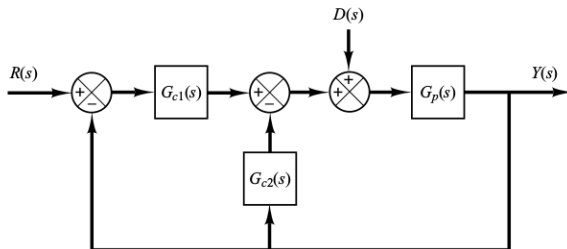
$$G_{yn} = \frac{G_{yd} - G_p}{G_p}$$



# Zero-Placement Approach to Improve Response Characteristics

Consider the two-degrees-of-freedom control system shown in Figure 8–31. Assume that the plant transfer function  $G_p(s)$  is a minimum-phase transfer function and is given by

$$G_p(s) = K \frac{A(s)}{B(s)}$$



- Ogata, Katsuhiko. Modern Control Engineering. Fifth Edition. Prentice Hall. 2009. Chapter 8.