

# Fluid Dynamics

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13th February 2026

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# 1 Kinematics

## 1.1 Streamlines and pathlines

There are two natural ways to think of flow.

- (i) A stationary observer watching flow go past. This is the Eulerian perspective. This is the approach used through this course. We define a velocity field (continuum field)  $\mathbf{u}(\mathbf{x}, t)$ .
- (ii) A moving observing, travelling along with the flow. This is the Lagrangian perspective.

**Definition.** (Streamlines) These are curves that are everywhere parallel to the flow at a given instant.

*Remark.* The streamline that goes through  $\mathbf{x}_0$  at time  $t_0$  is given parametrically as  $\mathbf{x} = \mathbf{x}(s, \mathbf{x}_0, t_0)$  and

$$\frac{d\mathbf{x}}{ds} = \mathbf{u}(\mathbf{x}, t_0)$$

(with  $\mathbf{x} = \mathbf{x}_0$  at  $s = 0$ ).

The set of streamlines shows the direction of flow a *given* instant a time (all fluid particle at one given time). Take the example  $\mathbf{u} = (1, t)$ . So at  $t = 0$  we have  $\mathbf{u} = (1, 0)$  so the streamlines are horizontal lines. At  $t = 1$  we have  $\mathbf{u} = (1, 1)$ , so the streamlines are diagonal.

**Definition.** (Pathlines) A *pathline* is the trajectory of a fluid particle (a very small bit of fluid). The pathline  $\mathbf{x} = \mathbf{x}(t, \mathbf{x}_0)$  of a fluid which is at  $\mathbf{x}_0$  at  $t = 0$  is such that

$$\frac{d\mathbf{x}}{dt} = \mathbf{u}(\mathbf{x}, t)$$

with  $\mathbf{x}(0, \mathbf{x}_0) = \mathbf{x}_0$ .

Again if we take  $\mathbf{u} = (1, t)$  we get

$$\begin{cases} \frac{dx}{dt} = 1 \\ \frac{dy}{dt} = t \end{cases} \rightarrow \begin{cases} x = x_0 + t \\ y = y_0 + \frac{t^2}{2} \end{cases}$$

which describes the path  $y - y_0 = \frac{1}{2}(x - x_0)^2$ .

*Remark.* Pathlines are often called "Lagrangian trajectories". The applications are very useful to characterise transport (infectious diseases and pollution simulations).

If the flow is *steady* (so  $\mathbf{u}$  does not depend on time). Then pathlines and streamlines are the same.

## 1.2 The material derivative

We will characterise the rate of change of "stuff" moving with a fluid. Consider a quantity  $F(\mathbf{x}, t)$  in a fluid flow (intuition is  $F$  is temperature). We want to measure how the temperature changes as we move through the field  $F$  along the flow. Let compute the rate of change of (in time) seen

by a moving observer. We will call this  $\frac{DF}{Dt}$ . Take a small time interval  $\delta t$ . Then

$$\begin{aligned}\delta F &= F(\mathbf{x} + \delta \mathbf{x}, t + \delta t) - F(\mathbf{x}, t) \\ &= \delta t \frac{\partial F}{\partial t} + (\delta \mathbf{x} \cdot \nabla) F + (\text{higher order terms}).\end{aligned}$$

We have that  $\delta \mathbf{x} = \mathbf{u} \delta t$ , so

$$\frac{\delta F}{\delta t} = \frac{DF}{Dt} = \frac{\partial F}{\partial t} + (\mathbf{u} \cdot \nabla) F.$$

We have the derivative and the convected derivative. This should be thought of as moving along gradients of a field.

### 1.3 Conservation of mass

Consider the flow through a straight rigid pipe with constant cross section. Suppose we have a  $\mathbf{u}_{\text{in}}$  and a  $\mathbf{u}_{\text{out}}$ . Can we have  $\mathbf{u}_{\text{in}} \neq \mathbf{u}_{\text{out}}$ ? For a gas, yes we can since they can be compressed. For a fluid, we cannot, since they are incompressible.

Define  $\rho(\mathbf{x}, t)$  as the mass density with  $[\rho] = \frac{M}{L^3}$ . We want a relation between  $\rho$  and  $\mathbf{u}$ . Consider a fixed volume  $V$  and compute the rate of change of its mass,  $M$ .

$$M = \int_V \rho dV$$

Assume that mass can only change due to the flow of mass across the boundary surface  $\partial V$ . Take a small surface element  $\delta A$  with normal  $\mathbf{n}$ . The volume out of  $V$  during  $\delta t$  is  $(\mathbf{u} \cdot \mathbf{n}) \delta A \delta t$ . Hence the mass out is  $\rho(\mathbf{u} \cdot \mathbf{n}) \delta A \delta t$ , so we get that

$$\frac{dM}{dt} = - \int_{\partial V} \rho(\mathbf{u} \cdot \mathbf{n}) dA.$$

The divergence theorem will allow us to rewrite this as

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = 0.$$

We know from IA Vector Calculus that  $\nabla \cdot (\rho \mathbf{u}) = \rho \nabla \cdot \mathbf{u} + \mathbf{u} \cdot \nabla \rho$ , so we can write that

$$\frac{D\rho}{Dt} = -\rho \nabla \cdot \mathbf{u}.$$

**Definition.** (Incompressible) A fluid flow is *incompressible* if  $\frac{D\rho}{Dt} = 0$ .

This is then equivalent to  $\nabla \cdot \mathbf{u} = 0$  which is the equivalent condition we'll use for the course.

For this course we will assume that  $\rho$  is constant. This means as a consequence that  $\nabla \cdot \mathbf{u} = 0$ .

### 1.4 Kinematic boundary condition

Consider the material boundary, with unit norm  $\mathbf{n}$ , of a body of fluid has a given velocity  $\mathbf{U}(\mathbf{x}, t)$ . At a point  $\mathbf{x}$  on the boundary, the fluid velocity relative to the surface is  $\mathbf{u} - \mathbf{U}$ . Applying mass conservation on the interface over a small surface element  $\delta A$  in time  $\delta t$ . So

$$\rho(\mathbf{u} - \mathbf{U}) \cdot \mathbf{n} \delta A \delta t = 0.$$

Hence we require  $\mathbf{u} \cdot \mathbf{n} = \mathbf{U} \cdot \mathbf{n}$  at the interface. This is the kinematic boundary condition.

*Remark.*  $\mathbf{n}$  occurs on both sides, hence we don't need  $\mathbf{n}$  to be a unit vector.

We have some consequences of this condition.

- (i) If the boundary is fixed,  $\mathbf{U} = 0$  implies that  $\mathbf{u} \cdot \mathbf{n} = 0$ . This is called the no penetration condition.
- (ii) Consider an air/water interface (free surface). Suppose the surface is defined by  $z = \xi(x, y, t)$ . Then can think of the free space as  $F(x, y, z, t) = 0$  where  $F(x, y, z, t) = z - \xi(x, y, t)$ . So  $\mathbf{n}$  is perp to  $\nabla F = (-\xi_x, -\xi_y, 1)$ . Then if  $\mathbf{u} = (u, v, w)$  so  $\mathbf{U} = (0, 0, \xi_t)$ . Then the kinematic boundary condition becomes  $-u\xi_x - v\xi_y + w = \xi_t$ , so  $w = \xi_t + u\xi_x + v\xi_y = \frac{DF}{Dt}$ . This is equivalent to  $\frac{DF}{Dt} = 0$ .

## 1.5 Streamfunction for 2D incompressible flow

We know that  $\nabla \cdot \mathbf{u} = 0$  which is equivalent to there existing a vector potential  $\mathbf{A}$  such that  $\mathbf{u} = \nabla \times \mathbf{A}$ . In 2D if  $\mathbf{u} = (u, v, 0)$  then  $\mathbf{A} = (0, 0, \psi(x, y))$ . So

$$u = \frac{\partial \psi}{\partial y}, \quad v = -\frac{\partial \psi}{\partial x}.$$

We call  $\psi$  a *streamfunction*. Looking at dimensions we have that  $[\psi] = \text{L}^2 \text{T}^{-1}$ . Now we'll see an example.

Let  $\mathbf{u} = (y, x)$  (which we can see is incompressible) so

$$\frac{\partial \psi}{\partial y} = u = y$$

, hence  $\psi = \frac{1}{2}y^2 + f(x)$ . We also have that  $-\frac{\partial \psi}{\partial x} = -f'(x) = x$ , so  $\psi = \frac{1}{2}(y^2 - x^2) + C$ .

We have some properties about the streamfunction,

- (i) Streamlines are given by  $\psi = \text{constant}$ .
- (ii)  $|\mathbf{u}| = |\nabla \psi|$ , so the flow is faster if the streamlines are closer together.
- (iii) If we take two points  $\mathbf{x}_0, \mathbf{x}_1$ , then then the volume flux crossing the line between  $\mathbf{x}_0$  and  $\mathbf{x}_1$  is

$$\int_{\mathbf{x}_0}^{\mathbf{x}_1} \mathbf{u} \cdot \mathbf{n} d\ell = \psi(\mathbf{x}_1) - \psi(\mathbf{x}_0).$$

- (iv)  $\psi$  is constant at rigid boundaries.

We can do the same in polar coordinates. So  $\mathbf{u} = (u_r(r, \theta), u_\theta(r, \theta), 0)$ . We have that

$$\mathbf{u} = \nabla \times \mathbf{A} = \left( \frac{1}{r} \frac{\partial \psi}{\partial \theta}, -\frac{\partial \psi}{\partial r}, 0 \right),$$

so we can check that  $\nabla \cdot \mathbf{u} = \frac{1}{r} \frac{\partial}{\partial r}(ru_r) + \frac{1}{r} \frac{\partial}{\partial \theta} = 0$

## 2 Dynamics of inviscid flow

### 2.1 Surface and volume forces

There are two types of forces exerted on a fluid.

- (i) Forces proportional to the volume (gravity);
- (ii) Forces proportional to the surface area (pressure, viscous stresses).

We'll first look at the first type, called volume forces. We'll denote  $F(\mathbf{x}, t)\delta V$  as the force acting on a small volume element  $\partial V$ . Let's take gravity as an example, so  $\mathbf{F} = \rho\mathbf{g}$ . Often we have that  $\mathbf{F}$  is conservative, so  $\mathbf{F} = -\nabla\chi$  for some function  $\chi$  (we know gravity is  $\chi = \rho gz$ ).

Now for surface forces. Consider a small element of area of  $\mathbf{n}\delta A$ . Denote the surface force exerted by the positive side on the negative side by  $\boldsymbol{\tau}(\mathbf{x}, t, \mathbf{n})\delta A$ . We say that  $\boldsymbol{\tau}$  is "stress" acting on a surface element. Note that  $\boldsymbol{\tau}$  depends on orientation. By Newton's third law, we have that  $\boldsymbol{\tau}(\mathbf{x}, t, -\mathbf{n}) = -\boldsymbol{\tau}(\mathbf{x}, t, \mathbf{n})$ .

There are many phenomena where friction inside a fluid (viscous stress) is negligible. For example a 10cm box of water, it takes hours for viscosity to bring the fluid to rest once disturbed.

**Definition.** (Inviscid) A fluid is said to be *inviscid* if we can neglect viscosity.

For inviscid flow,  $\boldsymbol{\tau}$  has no tangential component and its magnitude is independent of orientation. So  $\boldsymbol{\tau}(\mathbf{x}, t, \mathbf{n}) = -p(\mathbf{x}, t)\mathbf{n}$ , where  $p$  is the pressure. Note we have the minus sign because the positive side pushes with pressure  $p$  towards the negative side when  $p > 0$ .

### 2.2 The Euler Momentum equation

The idea here is that we do a similar calculation for mass conservation, but now for momentum instead. Consider an arbitrary fixed volume,  $V$  with boundary  $\partial V$ . Hence the momentum inside  $V$  is

$$\int_V \rho \mathbf{u} \, dV.$$

The momentum inside  $V$  can change due to

- (i) Flux of momentum across  $\partial V$ ;
- (ii) Force acting on  $V$  or  $\partial V$ .

The volume out of  $\delta A$  in  $\delta t$  is  $(\mathbf{u} \cdot \mathbf{n})\delta A \, \delta t$ . So the momentum out of  $\delta A$  in time  $\delta t$  is  $\rho \mathbf{u}(\mathbf{u} \cdot \mathbf{n})\delta A \, \delta t$ . Hence we get the following.

**Theorem.** (Euler momentum integral equation)

$$\frac{d}{dt} \int_V \rho \mathbf{u} \, dV = - \int_{\partial V} \rho \mathbf{u}(\mathbf{u} \cdot \mathbf{n}) \, dA + \underbrace{\int_V \mathbf{f} \, dV}_{\text{volume force}} + \underbrace{\int_{\partial V} -p \mathbf{n} \, dA}_{\text{surface force}}.$$

In components,

$$\int_V \frac{\partial}{\partial t}(\rho u_i) dV = - \int_{\partial V} \rho u_i u_j n_j dA + \int_{\partial V} -p n_i dA + \int_V f_i dV.$$

Sometimes books call  $\rho u_i u_j$  the momentum flux tensor. We can apply the divergence theorem to the first two integrals which gives that those two integrals become

$$\int_V \left[ -\frac{\partial}{\partial x_j}(\rho u_i u_j) - \frac{\partial p}{\partial x_i} \right] dV.$$

Given that this true for any fixed volume  $V$ , the integrand must be zero, hence we have that

$$\frac{\partial}{\partial t}(\rho u_i) + \frac{\partial}{\partial x_j}(\rho u_i u_j) = -\frac{\partial p}{\partial x_i} + f_i.$$

This becomes

$$u_i \left[ \frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x_j}(\rho u_j) \right] + \rho \left[ \frac{\partial u_i}{\partial t} + u_j \frac{\partial}{\partial x_j} u_i \right] = -\frac{\partial p}{\partial x_i} + f_i.$$

So using mass conservation on the first part we get some simplification, so going back to vector form we have the Euler momentum equation,

$$\rho \frac{D\mathbf{u}}{Dt} = -\nabla p + \mathbf{f}.$$

This is the equation of motion for inviscid fluid flow.

Fluid particles accelerate under differences in pressure and volume (body) forces (inviscid flows only).

*Remark.* Note that at the surface, the stress exerted by the fluid at the surface is  $p\mathbf{n}$ .

Let's see an application of the momentum equation. Consider a  $90^\circ$  bent pipe with a flow  $U$ . What is the force exerted by flow on the pipe for a steady flow without gravity? We will use the Euler momentum integral equation. Since the flow is steady, the LHS term is zero and since there is no gravity, the volume force term is zero. Hence we have that

$$\int_{\text{walls}} + \int_{\text{end}} [\rho \mathbf{u}(\mathbf{u} \cdot \mathbf{n}) p \mathbf{n}] dA = 0$$

and because of our kinematic boundary condition,  $\mathbf{u} \cdot \mathbf{n} = 0$ , so our integral across the walls becomes

$$\int_{\text{walls}} p \mathbf{n} dA = \mathbf{F} = \text{Force exerted by fluid flow on the pipe.}$$

Across the ends,

$$\int_{\text{in} + \text{out}} [\rho \mathbf{u}(\mathbf{u} \cdot \mathbf{n}) + p] dA = \rho(-U)(-U\mathbf{n}_1)A_1 + p_1\mathbf{n}_1 + \rho U(U\mathbf{n}_2)A_2 + p_2\mathbf{n}_2A_2.$$

We have that  $p = p_1 = p_2$  and  $A_1 = A_2 = A$  so the integral becomes

$$= A[(p + \rho U^2)(\mathbf{n}_1 + \mathbf{n}_2)],$$

hence

$$\mathbf{F} = -A(p + \rho U^2)(\mathbf{n}_1 + \mathbf{n}_2).$$

## 2.3 Bernoulli equation for steady flow with potential forces

There are *two* Bernoulli equations in the course. We'll look at the first one for steady flow here.

Recall from the Euler equation that

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + (\mathbf{u} \cdot \nabla) \mathbf{u} \right) = -\nabla p + \mathbf{F}.$$

We will assume that

- (i) We have steady flow so  $\frac{\partial}{\partial t} = 0$ .
- (ii)  $\rho$  is constant (as always in IB Fluid Dynamics).
- (iii)  $\mathbf{F} = -\nabla \chi$  (conservative force).

So the Euler equation gives that

$$\rho(\mathbf{u} \cdot \nabla) \mathbf{u} = -\nabla(p + \chi).$$

Now we have the identity

$$(\mathbf{u} \cdot \nabla) \mathbf{u} = \nabla \left( \frac{1}{2} u^2 \right) - \mathbf{u} \times (\nabla \times \mathbf{u}),$$

which gives that

$$\rho \left[ \nabla \left( \frac{1}{2} u^2 \right) - \mathbf{u} \times (\nabla \times \mathbf{u}) \right] = -\nabla(p + \chi).$$

Now since  $\rho$  is constant we can move it inside the  $\nabla$ . We'll now define  $\boldsymbol{\omega} = \nabla \times \mathbf{u}$ , the *vorticity* of the fluid, giving,

$$\nabla \left[ \frac{1}{2} \rho u^2 + p + \chi \right] = \rho \mathbf{u} \times \boldsymbol{\omega}.$$

We like to dot this with  $\mathbf{u}$  to get the Steady Bernoulli equation,

$$\mathbf{u} \cdot \nabla \left[ \frac{1}{2} \rho u^2 + p + \chi \right] = 0.$$

So this value  $H = \frac{1}{2} \rho u^2 + p + \chi$  is constant on streamlines for steady flow. The physical consequence of this is that when  $u$  increases,  $p$  decreases (ignoring gravity). Let's now see a simple application.

### 2.3.1 Tank of fluid with small drain

Take a tank full of fluid with a small hole at the bottom. The water height has height  $h$  and the fluid exists the tank with speed  $u$ . We assume that the size of the hole is small enough so the flow is steady. At the top of the tank, the pressure is atmospherical pressure and at the exit it is the same. Taking a streamline from the top on the tank to the exist we'll use the steady flow Bernoulli equation. We have gravity so  $\chi = -\rho gh$ . At the top we have  $H_1$  and at the bottom we have  $H_2$ , from Bernoulli,  $H_1 = H_2$ ,

$$\frac{1}{2} \rho u^2 = \rho gh,$$

so

$$u = \sqrt{2gh}.$$

*Remark.* We take the hole very small, so  $u = 0$  (approximately) at the top of the tank.



### 2.3.2 Venturi meter

This is a device to measure flow rates with no moving parts. We ignore gravity and assume the flow is steady and uniform across any cross section (gentle variations in the cross section  $A$ ). The device is a pipe which is pinched in the middle to a much smaller cross section area. Before the pinch we have  $A_1, u_1, p_1$  and in the pinched area we have  $A_2, u_2, p_2$ . By conservation of mass,  $A_1 u_1 = A_2 u_2$ . Now we attach two linked tubes of fluid which have a difference in height of fluid  $h$  one at the first point, and the other at the second point. From the Steady Bernoulli equation,  $\frac{1}{2}\rho u_1^2 + p_1 = \frac{1}{2}\rho u_2^2 + p_2$ . So using our mass conservation,

$$p_1 - p_2 = \frac{1}{2}\rho u_1^2 \left( \frac{A_1^2}{A_2^2} - 1 \right).$$

If we measure  $h$  using hydrostatic balance,

$$\rho g h = \frac{1}{2}\rho u_1^2 \left( \frac{A_1^2}{A_2^2} - 1 \right)$$

hence

$$A_1 u_1 = \sqrt{2gh} \frac{A_1 A_2}{\sqrt{A_1^2 - A_2^2}}.$$

Now for the final example, let's see a water jet on a 2D oblique plane. Let the angle under the jet and the angled plane be  $\beta$ . We will ignore gravity. We let the incoming fluid flow rate be  $U$  and the flow going up be  $a_2$  and the flow going down be  $a_1$ . We also want to know what the force exerted on the plane.

First we apply Bernoulli on the surface streamline. So since  $p$  is atmospherical everywhere hence  $u = U$  everywhere. By mass conservation,  $aU = a_1 U + a_2 U$ , hence

$$a = a_1 + a_2.$$

Now for more information, we apply the integral form of the Euler momentum equation. We'll take the volume  $V$  to be the entire volume of fluid.

$$\frac{d}{dt} \int_V \rho \mathbf{u} dt = \int_{\partial V} -\rho \mathbf{u} (\mathbf{u} \cdot \mathbf{n}) dA + \int_{\partial V} -p \mathbf{n} dA.$$

We've assumed the flow is steady, so the LHS is zero.  $p$  is atmospherical pressure everywhere except from the surface. On the surface streamlines due to the kinematic boundary condition,  $\mathbf{u} \cdot \mathbf{u} = 0$ . Components the Euler momentum equation on the surface gives

$$\rho a U^2 \cos \beta = \rho a_2 U^2 - \rho a_1 U^2$$

hence

$$a_2 = a_1 + a \cos \beta$$

so solving gives that

$$a_1 = \frac{a}{2}(1 - \cos \beta) \quad a_2 = \frac{a}{2}(1 + \cos \beta).$$

Now instead if we calculate the component perpendicular to the surface,

$$F = \int p \mathbf{n} dA = \rho a U^2 \sin \beta.$$

## 2.4 Hydrostatic pressure and Archimedes

What if we set  $\mathbf{u} = 0$  in the Euler equation? Then  $0 = -\nabla p + \mathbf{f}$ . However there is a non-trivial distribution of pressure in the fluid. For example if we take gravity, so  $\mathbf{f} = \rho\mathbf{g}$ , hence

$$0 = -\nabla p + \rho\mathbf{g} = -\nabla(p + \chi).$$

So  $p + \chi$  is constant, so  $p = p_0 - \rho gz$ . If we take  $z = 0$  to the top of the water, then we have  $p_0$  as atmospheric pressure. This is called hydrostatic pressure. We can use this to mathematically derive Archimedes principle.

We want to calculate the total pressure force on a body exerted due to a fluid with no flow. Let  $\mathbf{n}$  be a normal to the body surface  $\partial V$ .  $\mathbf{F}$  is the force exerted by the hydrostatic pressure field on the body. Hence

$$\begin{aligned}\mathbf{F} &= \int_{\partial V} -p\mathbf{n}dS \\ &= \int_{\partial V} -(p_0 - \rho gz)\mathbf{n}dS \\ &= - \int_V \nabla(p_0 - \rho gz)dV \\ &= \int_V \rho g\hat{z}dV \\ &= \rho gV\hat{z}.\end{aligned}$$

Where we've extended the fluid pressure field into the body.  $\rho gV$  is the weight of the displaced fluid which is the buoyancy force.

*Remark.* Suppose we have the Euler equation

$$\rho \frac{D\mathbf{u}}{Dt} = -\nabla p + \rho\mathbf{g}.$$

We will write  $p = p_{\text{static}} + p'$ , where  $p'$  is called the dynamic pressure, so our Euler equation becomes

$$\rho \frac{D\mathbf{u}}{Dt} = -\nabla p'$$

hence  $p'$  denotes the pressure in fluid to motion only.

## 2.5 Vorticity

Recall we defined  $\boldsymbol{\omega} = \nabla \times \mathbf{u}$  as the *vorticity* of the flow. Let's see some examples of vorticity.

- Let  $\mathbf{u} = \boldsymbol{\Omega} \times$  (solid body rotation). Then using IA Vector Calculus identities, we have that  $\boldsymbol{\omega} = 2\boldsymbol{\Omega}$ .
- Let  $\mathbf{u}$  be the *shear flow*  $\mathbf{u} = (0, \gamma x, 0)$ , so  $\boldsymbol{\omega} = (0, 0, \gamma)$ .
- Let  $\mathbf{u} = \frac{k}{2\pi r}\mathbf{e}_\phi$  in cylindrical coordinates, representing a line singular vortex. Then  $\boldsymbol{\omega} = 0$  everywhere except at  $r = 0$ , where

$$\oint_r \mathbf{u} \cdot d\boldsymbol{\rho} = k = \iint \boldsymbol{\omega} \cdot \mathbf{n}dS$$

by Stokes' theorem, giving that  $\boldsymbol{\omega} = (0, 0, k\delta(r))$

### 2.5.1 Interpretation of $\boldsymbol{\omega}$

Here we will show  $\boldsymbol{\omega}$  is equivalent to twice the local rotation rate of fluid particles.

Consider a material line  $\delta\boldsymbol{\ell}$ . How does  $\boldsymbol{\ell}$  change from  $t$  to  $t + \delta t$ .

$$\mathbf{x} + \delta\boldsymbol{\ell} \rightarrow \mathbf{x} + \delta\boldsymbol{\ell} + \mathbf{u}(\mathbf{x} + \delta\boldsymbol{\ell}, t)\delta t$$

and

$$\mathbf{x} \rightarrow \mathbf{x} + \mathbf{u}(\mathbf{x}, t)\delta t.$$

Hence our difference  $\delta\boldsymbol{\ell}$  goes to

$$\begin{aligned}\delta\boldsymbol{\ell} &\rightarrow \mathbf{x} + \delta\boldsymbol{\ell} + \mathbf{u}(\mathbf{x}, \delta\boldsymbol{\ell}, t)\delta t - [\mathbf{x} + \mathbf{u}(\mathbf{x}, t)\delta t] \\ &= \delta\boldsymbol{\ell} + (\delta\boldsymbol{\ell} \cdot \nabla)\mathbf{u}\delta t.\end{aligned}$$

Hence

$$\frac{D}{Dt}\delta\boldsymbol{\ell} = (\delta\boldsymbol{\ell} \cdot \nabla)\mathbf{u}.$$

Hence the tensor  $\frac{\partial u_i}{\partial x_j}$  determines changes in material lines (local rate of deformation). Write

$$\begin{aligned}\frac{\partial u_i}{\partial x_j} &= \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) + \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} - \frac{\partial u_j}{\partial x_i} \right) \\ &= e_{ij} + \frac{1}{2} \varepsilon_{ijk} \omega_k,\end{aligned}$$

where  $\boldsymbol{\omega} = \nabla \times \mathbf{u}$  by the standard decomposition of the antisymmetric tensor as a vector. The contribution of the second term to  $\frac{D}{Dt}\delta\boldsymbol{\ell}_i$  is

$$\begin{aligned}\frac{1}{2} \varepsilon_{jik} \omega_k \delta\ell_j &= \frac{1}{2} \varepsilon_{ikj} \omega_k \delta\ell_j \\ &= \frac{1}{2} (\boldsymbol{\omega} \times \delta\boldsymbol{\ell})_i.\end{aligned}$$

This is the rigid body rotation with angular velocity  $\boldsymbol{\Omega} = \frac{1}{2}\boldsymbol{\omega}$ . So  $\frac{1}{2}\boldsymbol{\omega}(\mathbf{x}, t)$  represents the average rotation rate of fluid particles. This is *not* the same as having flow with circular streamline.

### 2.5.2 Vorticity equation

Let's start with the Euler momentum equation,

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + (\mathbf{u} \cdot \nabla)\mathbf{u} \right) = -\nabla p + \mathbf{f}.$$

Assume that  $\rho$  is constant and  $\mathbf{f} = -\nabla\chi$ . We know that  $\mathbf{u} \cdot \nabla)\mathbf{u} = \nabla(\frac{1}{2}u^2) - \mathbf{u} \times \boldsymbol{\omega}$ , so taking the curl of the Euler equation we get that

$$\frac{\partial \boldsymbol{\omega}}{\partial t} - \nabla \times [\mathbf{u} \times \boldsymbol{\omega}] = 0.$$

Evaluating the  $i$ th component of this equation,

$$\begin{aligned}[\nabla \times (\mathbf{u} \times \boldsymbol{\omega})]_i &= \varepsilon_{ijk} \frac{\partial}{\partial x_j} [\varepsilon_{kmn} u_m \omega_n] \\ &= (\delta_{im} \delta_{jn} - \delta_{in} \delta_{jm}) \left( \frac{\partial u_m}{\partial x_j} \omega_n + u_m \frac{\partial \omega_n}{\partial x_j} \right) \\ &= \omega_j \frac{\partial u_i}{\partial x_j} - \omega_i \frac{\partial u_j}{\partial x_j} + u_i \frac{\partial \omega_j}{\partial x_j} - u_j \frac{\partial \omega_i}{\partial x_j}.\end{aligned}$$

Mass is conserved and the divergence of the curl is zero, so the second and third terms are zero, hence this is equal to

$$(\boldsymbol{\omega} \cdot \nabla) u_i - (\mathbf{u} \cdot \nabla) \omega_i.$$

So the vorticity equation is

$$\frac{\partial \boldsymbol{\omega}}{\partial t} + (\mathbf{u} \cdot \nabla) \boldsymbol{\omega} = (\boldsymbol{\omega} \cdot \nabla) \mathbf{u}.$$

This is equivalent to

$$\frac{D}{Dt} \boldsymbol{\omega} = (\boldsymbol{\omega} \cdot \nabla) \mathbf{u}.$$

The material derivative recall is the rate of change of the field while moving with the flow.

### 2.5.3 Vortex stretching

Let's compare the two equations

$$\frac{D}{Dt} \delta \ell = (\delta \ell \cdot \nabla) \mathbf{u} \quad \frac{D}{Dt} \boldsymbol{\omega} = (\boldsymbol{\omega} \cdot \nabla) \mathbf{u}.$$

We can see these are the same equation. So moving with the fluid,  $\boldsymbol{\omega}$  changes just like a material line element initially parallel to  $\boldsymbol{\omega}$ . In particular, if  $\delta \ell$  gets longer (stretching) then  $\boldsymbol{\omega}$  gets larger. This is conservation of angular momentum. When the fluid is stretched in the direction of  $\boldsymbol{\omega}$ , we get an increase in vorticity.

**Definition.** (Circulation) Given a closed curve  $\Gamma$ , the *circulation* around  $\Gamma$  is defined as

$$C(t) = \int_{\Gamma} \mathbf{u} \cdot d\boldsymbol{\ell}.$$

By Stokes' theorem we have that

$$C(t) = \iint_S \boldsymbol{\omega} \cdot \mathbf{S}$$

where  $S$  is an open surface with  $\partial S = \Gamma$ .

**Theorem.** *Non-examinable* (Kelvine circulation theorem) For an inviscid fluid with constant density and conservative body forces then if we take  $\Gamma$  to be a material line then

$$\frac{d}{dt} C = 0$$

*Remark.* If the flow is irrotational at  $t = 0$  then it is irrotational at all times.

## 3 Viscosity

The previous chapter only covered flows which were inviscid and we neglected any friction in fluid flow. We had that

(i)  $\boldsymbol{\tau} = -p\mathbf{n}$

(ii) In our momentum balance equation (Euler) we had  $\rho \frac{D\mathbf{u}}{Dt} \sim (\nabla p; \mathbf{F})$ .

Now we will include viscosity; we will find

- (i) New *tangential* stress between fluid layers or between fluid and the boundary.
- (ii) New term in the momentum balance equation.

Here in IB Fluid Dynamics we will only focus on 2D parallel viscous flows. So we will have that

$$\mathbf{u} = (u(y, t), 0, 0).$$

We instantly get that  $\nabla \cdot \mathbf{u} = 0$ .

### 3.1 Plane Couette flow

Consider a steady flow between two parallel plates, driven only by the motion of the top plate parallel to the bottom one with speed  $U$ . Experiments report that for the wide variety of fluids (Newtonian fluids) they find that

- (i) The fluid velocity at the top is  $U$  and at the bottom it is zero.
- (ii) The fluid flow velocity varies linearly between 0 and  $U$ , so  $u(y) = U \frac{y}{h}$ .
- (iii) The tangential force  $\tau$  required to move the top plane is linear in  $U$  and inversely proportional to  $h$ .

So we have that

$$\tau \propto \frac{U}{h}$$

**Definition.** (Dynamic viscosity) The *dynamic viscosity*,  $\mu$ , of a fluid is the proportionality constant from above, so

$$\tau = \mu \frac{U}{h}.$$

We usually write this as

$$\tau = \mu \frac{\partial u}{\partial n},$$

the viscous tangential stress exerted by the positive side to the negative side, where the normal is pointing from the interface to the positive side.

*Remark.* The viscosity is a material property of the fluid.

We call  $\frac{U}{h}$  the shear rate of the fluid.

### 3.2 2D parallel viscous flow

#### 3.2.1 Steady case with $\mathbf{F} = 0$

Consider an infinitesimal volume of fluid  $\delta x \delta y$ . Consider a flow  $u(y, t)$  moving left to right in the volume. On the left and right side we only have the pressure force and no tangential forces. On the top and bottom we have the tangential frictional forces equal to

$$\pm \mu \frac{\partial u}{\partial y}.$$