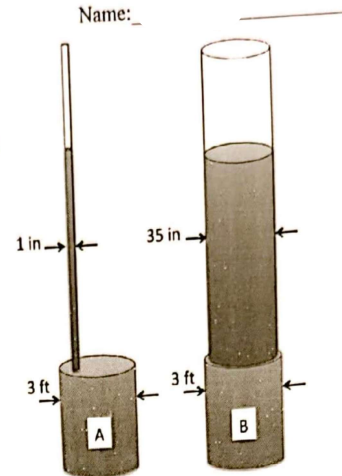


1. Multiple choice questions: [5 points each]

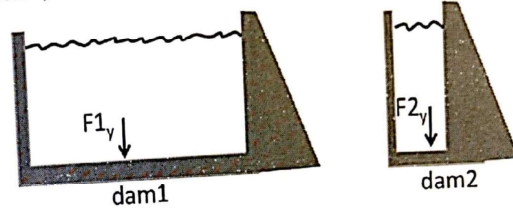
C i) Identical drum A and B are being tested for strength by continuously filling w/ water to the same height.

- a) Drum A should burst first
b) Drum B should burst first
c) Drum A and B should burst at same time
d) If additional info is needed, what is it



A ii) Consider the figure of two dams below, what is the correct statement

- a) $F_{1y} > F_{2y}$
b) $F_{1y} < F_{2y}$
c) $F_{1y} = F_{2y}$
d) Cannot be determined



B iii) $u = 4xy^3$; $v = -4x^3y$.
The set of equations above represents a:

- a) two-dimensional incompressible flow
b) two-dimensional compressible flow
c) uncertain

C iv) A 0.3 m by 0.5 m rectangular air duct carries a flow of $0.45 \text{ m}^3/\text{s}$ at a density of 2 kg/m^3 . The velocity in the duct is

- a) 1.5 m/s
b) 0.9 m/s
c) 3 m/s
d) Infinite m/s

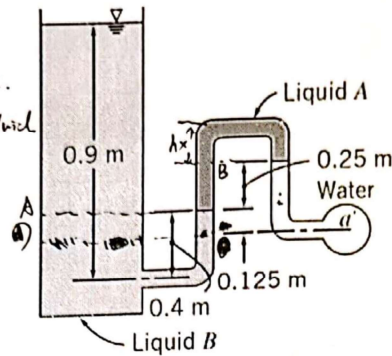
25

2. Determine the gage pressure in kPa at point *a*, if liquid A has SG = 1.20 and liquid B has SG = 0.75. The liquid surrounding point *a* is water, and the tank on the left is open to the atmosphere. $\rho_{\text{water}} = 1,000 \text{ kg/m}^3$. [25pts]

assumption: Steady state.

Incompressible fluid

$$g = 9.8 \text{ m/s}^2$$



At ~~the~~ A:

$$P_A = P_{\text{atm}} + \rho_A g h_A$$

$$P_A = P_B$$

$$P_B = P_{\text{atm}} + \rho_A g (h_A + 0.25) + \rho_B g (0.125)$$

$$\text{for point B: } P_B + \rho_A g \cdot 0.25 = P_A$$

$$P_B = P_A - \rho_A g \cdot 0.25$$

At a:

$$P_a = P_B + \rho_{\text{water}} g (0.25 + 0.125)$$

$$P_a = P_B + \rho_{\text{water}} g (0.375)$$

$$\Rightarrow P_a = P_{\text{atm}} - \rho_A g \cdot 0.25 + \rho_{\text{water}} g \cdot (0.375), \quad \rho_A = 1.2 \rho_{\text{water}}$$

$$P_a = P_{\text{atm}} - \rho_A g \cdot 0.25 + \rho_{\text{water}} g \cdot (0.375)$$

$$\rho_B = 0.75 \rho_{\text{water}}$$

$$h_A = (0.9 - 0.4) = 0.5 \text{ m}$$

$$\Rightarrow P_a = (0.75 \cdot 9.8 \cdot 0.5 \text{ m} - 1.2 \cdot 9.8 \cdot 0.25 \text{ m} + 9.8 \cdot 0.375 \text{ m}) \rho_{\text{water}}$$

$$= 4410 \text{ Pa}$$

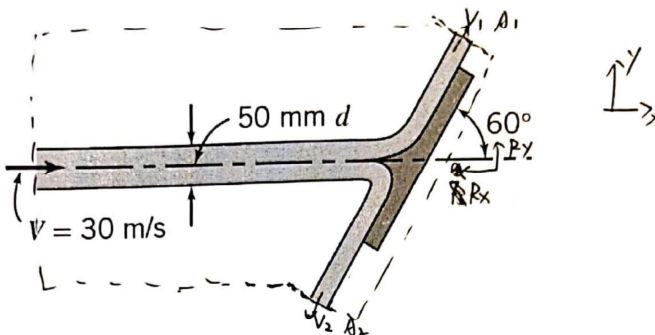
$$= 4.41 \text{ kPa}$$

3. This water jet of 50 mm diameter moving at 30 m/s is divided in half by a "splitter" on the stationary flat plate. Calculate the magnitude and direction of the force on the plate. Assume that flow is in a horizontal plane. $\rho_{\text{water}} = 999 \text{ kg/m}^3$. [25pts]

assumption:

Steady state.

Incompressible fluid.



Conservation of mass: $\frac{\partial}{\partial t} \int_{CV} \rho dV + \int_{CS} \rho \vec{V} \cdot \vec{n} dA = 0$, $A = \pi \left(\frac{0.05}{2} \right)^2 = 1.96 \times 10^{-3} \text{ m}^2$

$$\rightarrow -V \cdot A + V_1 A_1 + V_2 A_2 = 0$$

$$V_1 A_1 + V_2 A_2 = 0.059 \text{ m}^3/\text{s}$$

$$\rightarrow \text{divided in half, so } A_1 V_1 = A_2 V_2 = 0.029 \text{ m}^3/\text{s}$$

$$V_1 = V_2 = 15 \text{ m/s}$$

Momentum equation in x: $F_{sx} + F_{Bx} = \frac{\partial}{\partial t} \int_{CV} \rho \vec{V}_x dV + \int_{CS} \rho \vec{V}_x \cdot \vec{n} dA$

$$R_x = -U^2 \rho A + U_1 \rho V_1 A_1 - U_2 \rho V_2 A_2$$

$$U_1 = V_1 \cos 60^\circ, U_2 = V_2 \cos 60^\circ$$

$$\rightarrow -R_x = -30^2 \text{ m/s} \cdot 999 \text{ kg/m}^3 \cdot 1.96 \times 10^{-3} \text{ m}^2 + 15 \text{ m/s} \cos 60^\circ \cdot 999 \text{ kg/m}^3 \cdot 0.029 \text{ m}^3/\text{s}$$

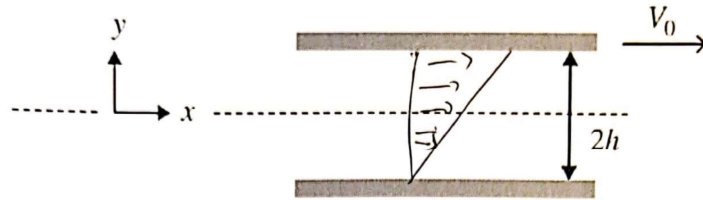
$$-15 \text{ m/s} \cos 60^\circ \cdot 999 \text{ kg/m}^3 \cdot 0.029 \text{ m}^3/\text{s}$$

$$R_x = 58.7412 \text{ N}$$

Momentum equation in y: $R_y = \rho V_1 A_1 \sin 60^\circ - \rho V_2 A_2 \sin 60^\circ$
 $= 0$

\Rightarrow Force on the plate is 58.7412 N in the $-x$ direction.

4. Consider a steady, laminar, fully developed incompressible flow between two infinite parallel plates separated by a distance $2h$ as shown. The top plate moves with a velocity V_0 . You can neglect the effect of gravity. Derive:



- a) an expression for the pressure gradient in the y-direction, [15 points]

$$x: \rho \left(\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} \right) = \rho g_x - \frac{\partial p}{\partial x} + \mu \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right)$$

$$y: \rho \left(\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} \right) = \rho g_y - \frac{\partial p}{\partial y} + \mu \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2} \right)$$

$$z: \rho \left(\frac{\partial w}{\partial t} + u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} \right) = \rho g_z - \frac{\partial p}{\partial z} + \mu \left(\frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2} \right)$$

for 2-D flow = ~~w = 0~~ $w = 0$, no z component, neglect the gravity: $g_x = g_y = g_z = 0$

for incompressible flow: $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$, for a steady state: $\frac{\partial}{\partial t} = 0$

for fully developed flow: $\frac{\partial u}{\partial x} = 0$

$$\rightarrow \frac{\partial v}{\partial y} = 0 \Rightarrow \rho \mu \frac{\partial v}{\partial x} = -\frac{\partial p}{\partial y} + \mu \frac{\partial^2 v}{\partial x^2} \quad \frac{\partial p}{\partial y} = \mu \frac{\partial^2 v}{\partial x^2} - \rho \mu \frac{\partial v}{\partial x}$$

- b) the velocity profile. [15 points] the velocity on the bottom plate is 0, so $v = 0$

$$\rightarrow \frac{\partial p}{\partial y} = 0$$

$$\text{in } x: \frac{\partial p}{\partial x} = \mu \frac{\partial^2 u}{\partial y^2}$$

with $\frac{\partial p}{\partial y} = 0$, p will not depend on y .

with two infinite parallel plates,

