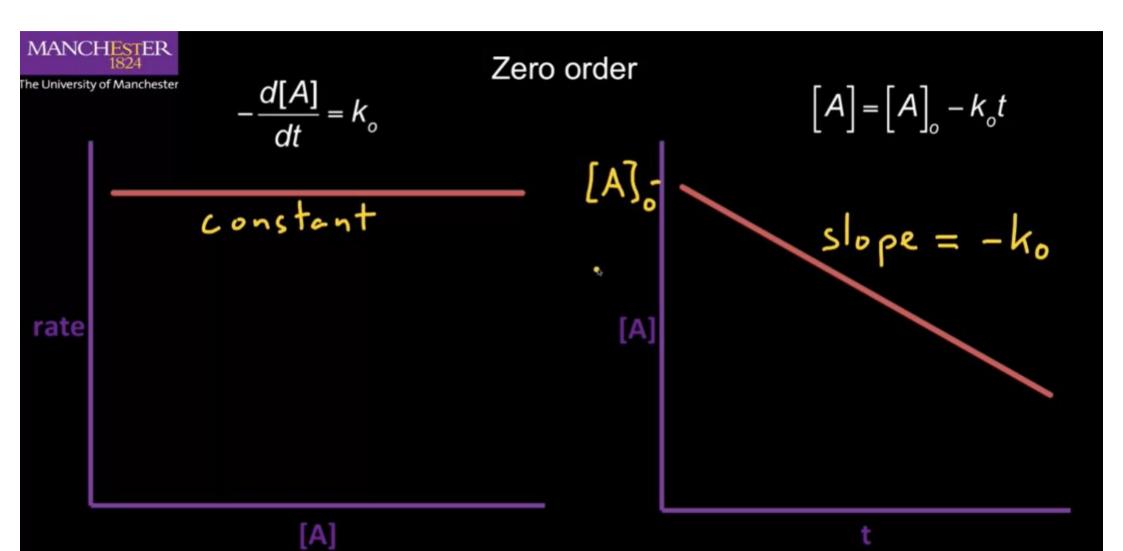
must integrate
$$-\frac{d[A]}{dt} = k_0$$

$$J[A] = -k_0 dt$$

$$\int_{[A]}^{[A]} J[A] = -k_0 \int_{[A]}^{[A]} J[A] = -k_0 \int_{[A]}^{[A]}$$

Zero order integrated rate expression



Zero order reactions are not common

i) gases on metals

$$2 \text{ NH}_{3}(g) \xrightarrow{\text{W}} \text{N}_{2}(g) + 3 \text{ H}_{2}(g)$$

ii) some solution reactions

$$CH_3COCH_3(aq) + I_2(aq) \rightarrow CH_3COCH_2I(aq) + H^+(aq) + I^-(aq)$$

iii) enzyme reactions

•

$$\frac{d[A]}{dt} = -k_{_1}[A]$$

$$\int_{A}^{A} \left[A \right] = -k, dt$$

$$\int_{A}^{A} \left[A \right] = -k, \int_{A}^{A} dt$$

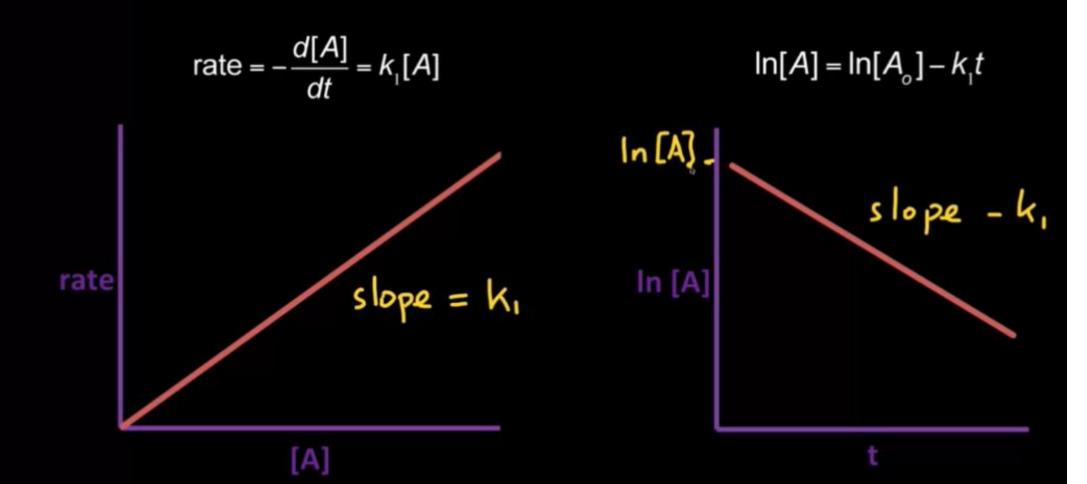
$$ln[A] - ln[A] = -k,t$$

or $ln[A] = -k,t$
 $[A] = [A] = [A] = e^{-k,t}$

First order integrated rate expression



First order



Examples of first order reactions

i) Radioactive decay

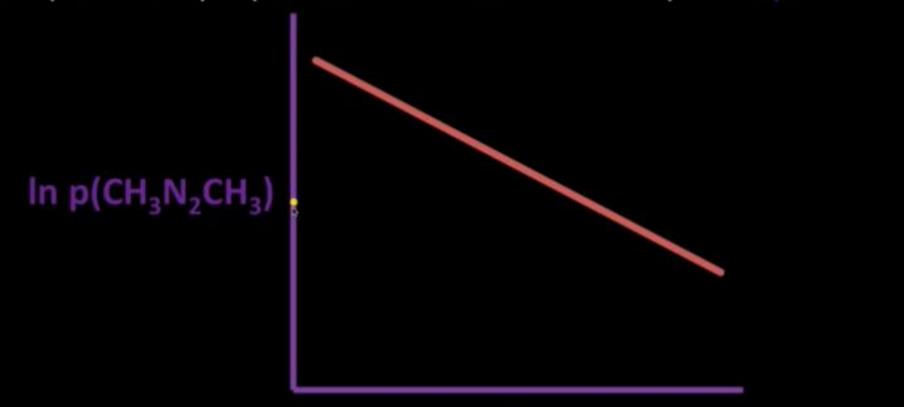
$$^{226}_{88}$$
Ra $\rightarrow ^{222}_{86}$ Rn $+ ^{4}_{2}$ He

$$\frac{d^{226}Ra}{dt} = -k[^{226}_{88}Ra]$$

ii) Gas phase reactions

$$CH_3N_2CH_3(g) \rightarrow CH_3CH_3(g) + N_2(g)$$

As pressure proportional to concentration plot In p versus t





Half-life

Half-life is time $\tau_{1/2}$ for concentration of [A] to drop from [A]_o to [A]_o/2

Using integrated rate expression $\ln \left[A\right] = -k_1 + \frac{1}{2}$

$$\ln \frac{1}{2} = -k_1 \frac{\gamma_2}{\gamma_2}$$

$$\frac{1}{2} = \frac{1}{2} \frac{2}{k_1}$$

$$\ln (\alpha - x_1) = k_1(t_2 - t_1)$$

$$(\alpha - x_2) = Interval formula$$

Second Order Reactions

$$\frac{1}{[A]} - \frac{1}{[A]_o} = k_2 t$$





Half-life for second order reactions

$$\frac{1}{[A]} - \frac{1}{[A]_o} = k_2 t$$

when
$$t = \tau_{1/2}$$

$$[A] = \frac{[A]_o}{2}$$

$$2 - 1 - [A]_o = k_2 \tau_2$$

$$C_1 = k_2 [A]_o$$

$$\tau_2 = k_2 [A]_o$$

2nd order reactions are the most common requiring two species to interact



1) INTEGRATION METHOD

Determine the concentration of reactants at a series of times t

This can either be the amount x or the amount remaining [A] = $[A]_{\circ} - x$

Then make a series of plots of the relevant functions

The best straight line will give you the order of reaction



2) ISOLATION METHOD

Useful when reaction contains more than one reactant

e.g.
$$A + B \rightarrow products$$

have a large excess of B

then concentration of B will hardly vary during the reaction

$$-\frac{d[A]}{dt} = k_2[A][B]$$

$$[B] \approx [B]_o$$
Then
$$-J[A] = k_2[B]_o[A]$$

$$= k_1[A]$$

$$= k_1[A]$$

k₁' is a pseudo 1st order rate constant

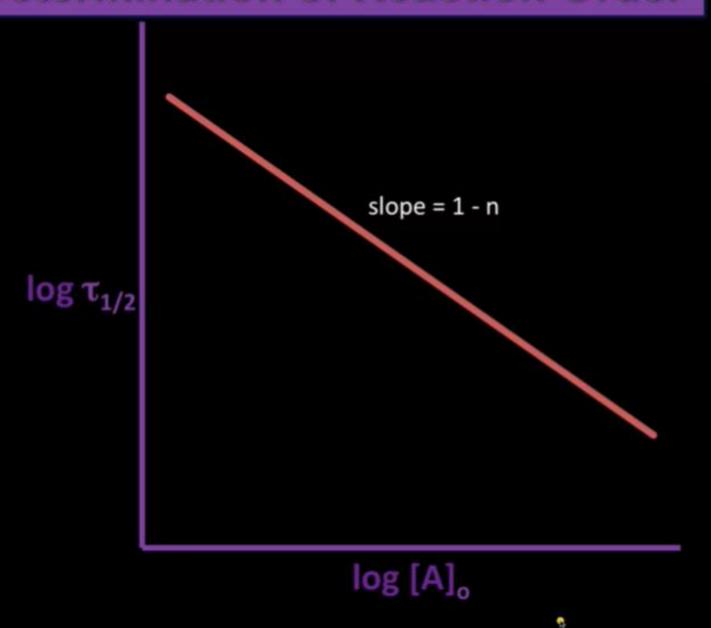
Then determine reaction order by integration



3) HALF-LIFE METHOD

For reaction of type

$$T_{2}$$
 $\propto [A]_{-n}^{-n}$ $n - order of reaction$ take logs



vary initial concentration [A], and measure time for half-reaction



4) INITIAL RATE (DIFFERENTIAL METHOD)

Consider

$$A + B \rightarrow products$$

rate =
$$k_2 [A]^a [B]^b$$

at
$$t = 0$$

$$(rate)_{initial} = k_2 [A]_o [B]_o$$

take logs

$$log(rate)_{initial} = log k_2 + a log [A]_o + b log [B]_o$$

$$log(rate)_{initial} = log k_2 + a log [A]_o + b log [B]_o$$

keep [B] constant, vary [A]



log [A]

Repeat for b keeping [A], constant



Experimental Determination of Rates

1) CHEMICAL DETERMINATION OF CONCENTRATIONS

e.g. titration. Useful when reactants or products contain a functional group (especially acids and bases)

2) PRESSURE CHANGES

Useful only when there is a pressure change

e.g.
$$2N_2O_5(g) \rightarrow 4NO_2(g) + O_2(g)$$

pressure increases upon reaction



Experimental Determination of Rates

3) SPECTROSCOPY

If NO pressure change BUT one component varies its spectral characteristics

e.g.
$$H_2(g) + Br_2(g) \rightarrow 2HBr(g)$$

Br2(g) absorbs visible light

4) POLARIMETRY

Measure optical rotation

e.g. hydrolysis of sucrose

Experimental Determination of Rates

5) ELECTROCHEMICAL METHODS

Useful when number or nature of ions in solution changes

e.g.
$$CH_3CO_2C_2H_5 + Na^+OH^- \rightarrow C_2H_5OH + CH_3CO_2^-Na^+$$

measure conductance of solution

6) DILATOMETRY

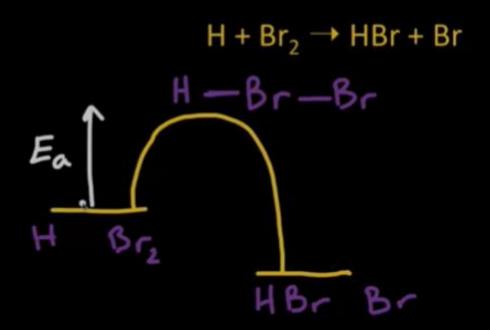
Measure small volume changes in a solution

e.g.
$$(CH_3)_2C=CH_2 + H_2O \rightarrow (CH_3)_3COH$$

Effect of temperature on reaction rate

Reaction cannot proceed directly to products but MUST pass through some transition state

This transition state might involve the lengthening of a bond or change in bond angles which requires energy



$$G = \frac{[A]}{[A] + [B]}G_{o} + \frac{[B]}{[A] + [B]}G_{o}$$

$$([A] + [B])G_{o} + [B]G_{o} + [B]G_{o}$$
but
$$[A] + [B] = [A]_{o}$$

$$+ [B] = [A]_{o} - [A]$$

$$[A]_{o} G_{o} = [A]_{o} - [A]$$

$$[A]_{o} G_{o} = [A]_{o} - [A]_{o}$$

$$[A]_{o} G_{o} = [A]_{o} - [A]_{o}$$



Effect of temperature on reaction rate

Reaction rates generally increase with temperature

Arrhenius Equation

consider

$$A \stackrel{K_f}{=} B$$

equilibrium constant

$$K = \frac{K_f}{K_b}$$

van't Hoff isochore relates K to T



Reactions moving towards equilibrium

Consider

$$A \stackrel{k_1}{\rightleftharpoons} B$$

Assume all reactions are 1st order

Back reaction:



rate =
$$-\frac{d[A]}{dt} = k_1[A] - k_{-1}[B]$$
 [B] = [A]₀ - [A]
 $-\frac{d[A]}{dt} = k_1[A] - k_{-1}([A], -[A])$
 $d[A] = -(k_1 + k_{-1})[A] + k_{-1}[A]$

This can be integrated to give:

$$[A] = [A], \{ \frac{1}{|K_1 + |K_2|} + \frac{1}{|K_1 + |K_2|} \}$$

If there is no back reaction

$$k_{-1} = 0$$

simple 1st order reaction that goes to completion

$$[A] = [A]_o \left\{ \frac{k_{-1} + k_1 \exp\left[-(k_1 + k_{-1})t\right]}{(k_1 + k_{-1})} \right\}$$

At t = ∞ system reaches equilibrium

$$[A]_{\infty} = \frac{k_{-1}}{k_{1} + k_{-1}} [A]_{o} \qquad [B]_{\infty} = \frac{k_{1}}{k_{1} + k_{-1}} [A]_{o}$$

$$K = [B]_{e} = [B]_{o} = \frac{k_{1}}{k_{1} + k_{-1}} [A]_{o}$$

A simple relationship between rate constants and equilibrium constant

Also holds for simple bimolecular reactions

$$A + B \stackrel{k_2}{\rightleftharpoons} C + D$$

$$K = \frac{[C]_{e}[D]_{e}}{[A]_{e}[B]_{e}} = \frac{[C]_{\infty}[D]_{\infty}}{[A]_{\infty}[B]_{\infty}} = \frac{k_{2}}{k_{-2}}$$



Consecutive reactions

Many reactions proceed through several consecutive steps

e.g.
$$A \xrightarrow{k_1} B \xrightarrow{k_1} C$$

B is a reaction intermediate

e.g.
$$\beta^ \beta^ \beta^-$$
 e.g. $239 \atop 92 U \longrightarrow 39 \atop 93 Np \longrightarrow 239 \atop 94 Pu$ $23.5 min$ $2.35 days$



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$$A \xrightarrow{k_1} B \xrightarrow{k_1'} C$$

$$[A] = [A], e^{-k,t}$$

[B] and [C] much more difficult to solve

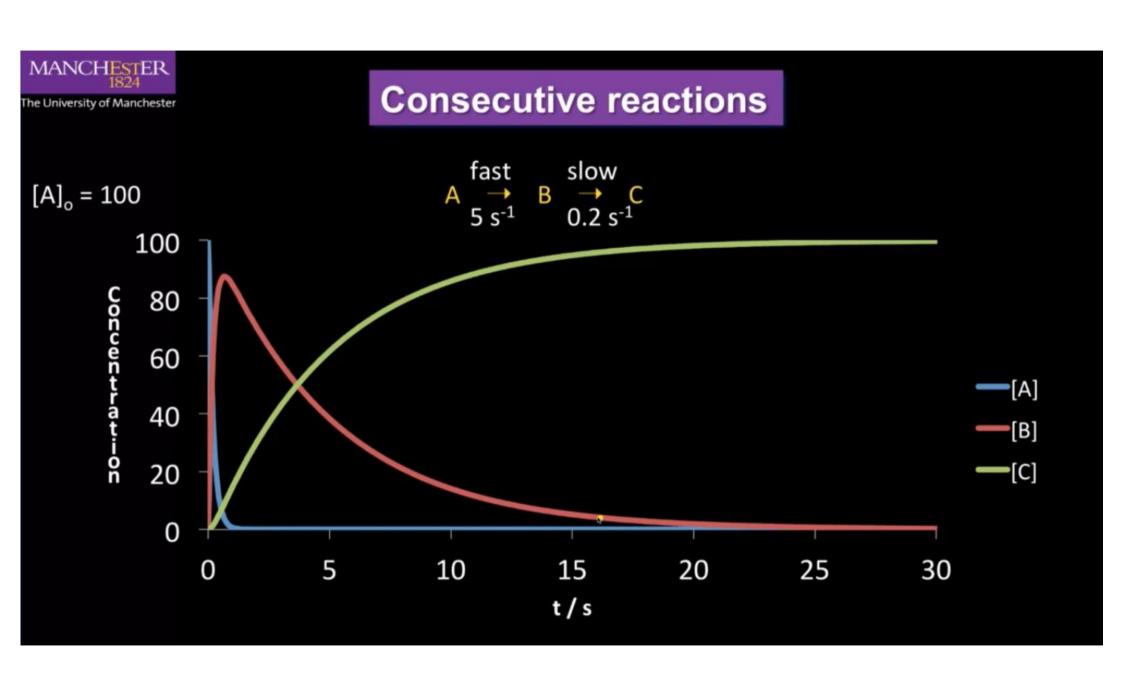
$$[B] = [A]_o \left\{ \frac{k_1}{k_1' - k_1} \right\} \left(e^{-k_1 t} - e^{-k_1' t} \right)$$

$$[C] = [A]_o \left\{ 1 + \left(\frac{1}{k_1 - k_1'} \right) \left(k_1' e^{-k_1 t} - k_1 e^{-k_1' t} \right) \right\}$$

$$\frac{d[A]}{dt} = -k_{_{|}}[A]$$

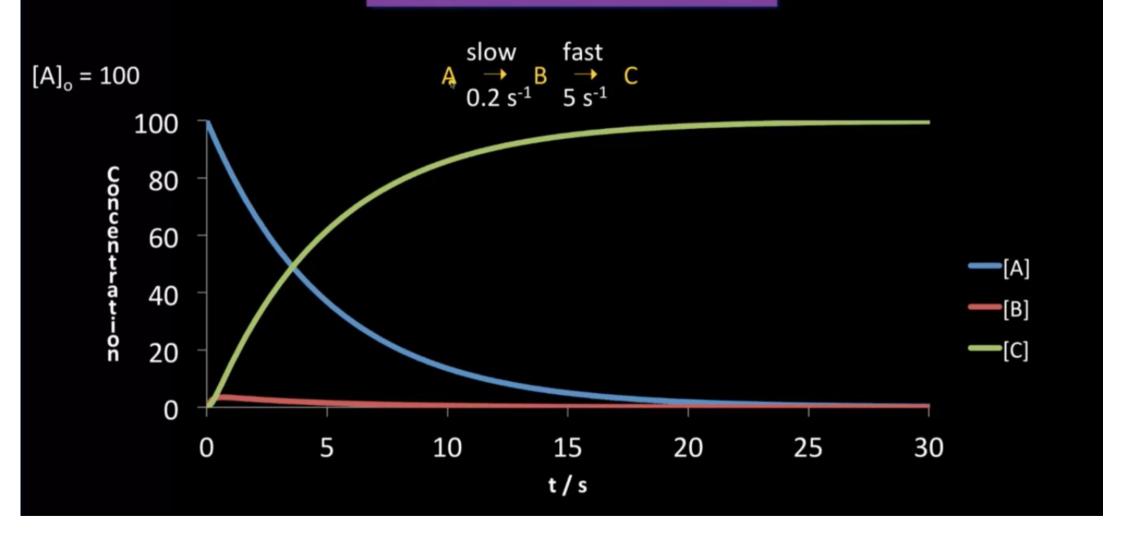
$$\frac{d[B]}{dt} = k_1[A] - k_1[B]$$

$$\frac{d[C]}{dt} = -k_1[B]$$

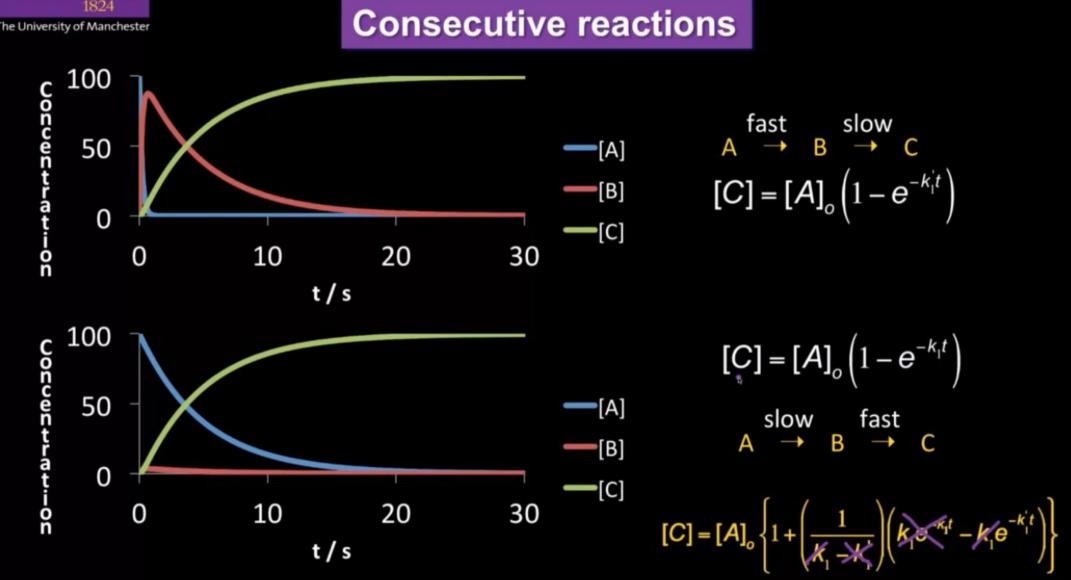




Consecutive reactions







Consecutive reactions

Only the slow step is important

RATE-DETERMINING STEP



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Steady-state approximation

$$\mathfrak{D}\frac{d[A]}{dt} = -k_{_{1}}[A]$$

$$2 \frac{d[B]}{dt} = k_1[A] - k_1[B] = 0$$

$$\Im \frac{d[C]}{dt} = k_1[B]$$

2) gives
$$[B] = \frac{k_1}{k_1!} [A] = \frac{k_1}{k_1!} [A]_e^{-k_1t}$$

$$d[c] = k_1[A] \cdot e^{-k_1t}$$

$$\int_{c}^{c} d[c] = k_1[A] \cdot e^{-k_1t} dt$$

$$[c] = k_1[A] \cdot (1 - e^{-k_1t}) \cdot k_1$$



Steady-state approximation

Example – First Order Reactions

$$A \rightarrow P$$

$$A + A \xrightarrow{k_2} A^* + A$$

$$A^* + A \rightarrow A + A$$

$$A^* \stackrel{k_1}{\longrightarrow} P$$

Steady-state approximation

rate of formation of products

$$\Delta + \Delta \xrightarrow{k_2} \Delta^* + \Delta$$

$$\frac{d[A^*]}{dt} = k_2[A]^2 - k_{-2}[A^*][A] - k_1[A^*] = 0$$

$$A^* + A \xrightarrow{K_{-2}} A + A$$

rearrange

$$A^* \stackrel{k_1}{\rightarrow} F$$

$$[A^*] = \frac{k_2 [A]^2}{k_1 + k_{-2} [A]}$$



$$\frac{d[P]}{dt} = \frac{k_1 k_2 [A]^2}{k_1 + k_{-2} [A]}$$



Steady-state approximation

$$\Delta + \Delta \xrightarrow{k_2} \Delta^* + \Delta$$

$$K_{-2}\gg K$$
, $d[P] = K_1K_2[A]$ I_{kinet}^{st} and K_{-2}

 $dt = k_1 + k_2[A]$

 $d[P] = k_1 k_2 [A]^2$

$$A^* + A \rightarrow A + A$$

$$A^* \stackrel{k_1}{\rightarrow} F$$

At very low pressure
$$k_{-2}[A] \ll k_1$$

$$d[P] = k_2[A]^2$$

Lindemann mechanism

Example – isomerisation of cyclopropane

$$\triangle + \triangle \xrightarrow{k_2} \triangle^* + \triangle$$

$$\Delta^* + \Delta \xrightarrow{k_{-2}} \Delta + \Delta$$

$$\Delta^* \xrightarrow{k_1} CH=CH-CH_3$$

at high pressure

rate =
$$\frac{k_1 k_2 [\Delta]}{k_{-2}}$$

at low pressure



Chain reactions

e.g. gas phase reactions that proceed via free radicals (molecules with missing atoms)

e.g.
$$\cdot CH_3 + CH_3CH_3 \rightarrow CH_4 + \cdot CH_2CH_3$$



Four important steps

1) Initiation production of free-radicals

a) by collision
$$Cl_2 + Cl_2 \rightarrow 2Cl \cdot + Cl_2$$

b) Lindemann process (more complex molecules)

c) action of light
$$Cl_2 + h\nu \rightarrow 2Cl$$



Four important steps

2) Propagation

Attack of molecules by free-radicals with transfer of free radical

e.g.
$$Cl + H_2 \rightarrow HCl + H$$

3) Inhibition

٠

A free radical attacks a product slowing the reaction



Four important steps

4) Termination

a) dimerisation e.g.
$$\cdot CH_3 + \cdot CH_3 \rightarrow CH_3CH_3$$

b) reaction with walls of vessel

addition of radical scavenger such as NO



$$\frac{d[HBr]}{dt} = \frac{k'[H_2][Br_2]^{\frac{1}{2}}}{1 + k''([HBr]/[Br_2])}$$

Need a mechanism

Initiation:

$$R_a \rightarrow 2Br$$

 $H_2(g) + Br_2(g) \rightarrow 2HBr(g)$

Propagation:

$$Br \cdot + H_2 \xrightarrow{k_b} HBr + H \cdot$$
 $H \cdot + Br_2 \xrightarrow{k_c} HBr + Br \cdot$

Inhibition:

$$H \cdot + HBr \xrightarrow{k_d} H_2 + Br \cdot$$

Termination:

$$k_e$$
Br· + Br· \rightarrow Br₂



$$H_2(g) + Br_2(g) \rightarrow 2HBr(g)$$

By experiment

$$\frac{d[HBr]}{dt} = \frac{k'[H_2][Br_2]^{\frac{1}{2}}}{1 + k''([HBr]/[Br_2])}$$



$$\frac{d[HBr]}{dt} = \frac{k'[H_2][Br_2]^{\frac{1}{2}}}{1 + k''([HBr]/[Br_2])}$$

$$k_{b}[Br \cdot][H_{2}] - k_{c}[H][Br_{2}] - k_{d}[H \cdot][HBr] = 0$$

$$H_2(g) + Br_2(g) \rightarrow 2HBr(g)$$

 $2k_{a}[Br_{2}] - k_{b}[Br \cdot][H_{2}] + k_{c}[H \cdot][Br_{2}] + k_{d}[H \cdot][HBr] - 2k_{e}[Br \cdot]^{2} = 0$

$$\frac{d[HBr]}{dt} = \frac{k'[H_2][Br_2]^{\frac{1}{2}}}{1 + k''([HBr]/[Br_2])}$$

$$H_2(g) + Br_2(g) \rightarrow 2HBr(g)$$

$$[Br\cdot] = \left\{\frac{k_a}{k_e}[Br_2]\right\}^{\frac{1}{2}}$$

Place in original equation

$$\frac{d[HBr]}{dt} = k_b[Br\cdot][H_2] + k_c[H\cdot][Br_2] - k_d[H\cdot][HBr]$$

$$\begin{aligned} \text{(4)} \quad [H \cdot] &= \frac{k_b \left(\frac{k_a}{k_e}\right)^{\frac{1}{2}} [H_2][Br_2]^{\frac{1}{2}}}{k_c [Br_2] + k_d [HBr]} \\ \text{(K)} &= 2 \text{ Kb} \left(\frac{K_a}{k_e}\right)^{\frac{1}{2}} = \frac{2k_b \left(\frac{k_a}{k_e}\right)^{\frac{1}{2}} [H_2][Br_2]^{\frac{1}{2}}}{dt} \\ \text{(HBr)} &= \frac{2k_b \left(\frac{k_a}{k_e}\right)^{\frac{1}{2}} [H_2][Br_2]^{\frac{1}{2}}}{1 + \frac{k_d}{k_c} ([HBr] / [Br_2])} \end{aligned}$$



Catalysis

Example of homogeneous catalysis

$$Br_2$$

2 $H_2O_2 \rightarrow 2 H_2O + O_2$ net reaction

$$Br_{2} + 2 H_{2}O \rightarrow HOBr + H_{3}O^{+} + Br^{-}$$

$$H_{3}O^{+} + HOOH \rightarrow HOOH_{2}^{+} + H_{2}O$$

$$HOOH_{2}^{+} + Br^{-} \rightarrow HOBr + H_{2}O$$

$$HOOH_{2}^{+} + Br^{-} \rightarrow HOBr + H_{2}O$$

$$HOBr + HOOH \xrightarrow{fast}_{k_{b}} H_{3}O^{+} + O_{2} + Br^{-}$$



Catalysis

Examples of heterogeneous catalysis

$$\frac{\text{W}}{2 \text{ NH}_3} \rightarrow \text{N}_2 + 3 \text{ H}_2$$

 $E_a = 162 \text{ kJ mol}^{-1}$ = 350 kJ mol $^{-1}$ without catalyst

Au
$$2 \text{ HI} \rightarrow \text{H}_2 + \text{I}_2$$

 $E_a = 105 \text{ kJ mol}^{-1}$ = 184 kJ mol $^{-1}$ without catalyst

Catalysis

If E_a reduced from 76 kJ mol⁻¹ to 57 kJ mol⁻¹

$$k = e^{\frac{-E_a}{RT}}$$

$$\frac{k_{\text{catalyst}}}{k_{\text{no catalyst}}} = \frac{e^{\frac{-57 \text{ kJ mol}^{-1}}{2.5 \text{ kJ mol}^{-1}}}}{e^{\frac{-76 \text{ kJ mol}^{-1}}{2.5 \text{ kJ mol}^{-1}}}} \approx 2000$$