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IIT(BHU) VARANASI
STUDENTS' NOTES

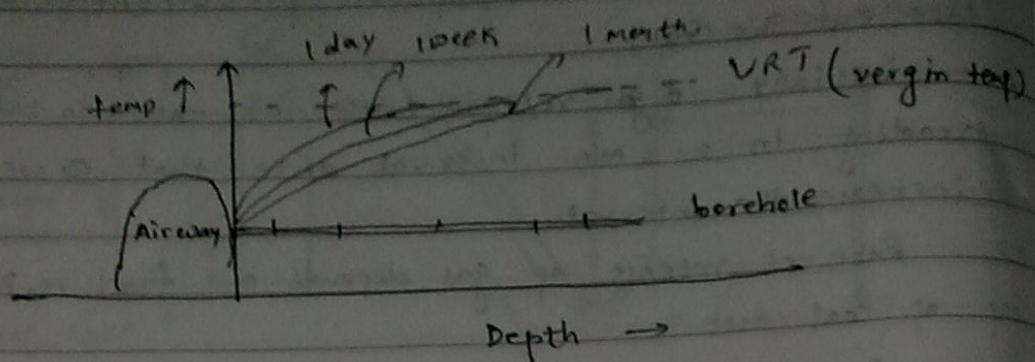
UNDERGROUND MINE ENVIRONMENT
FIFTH SEMESTER
TOPIC-MINE FAN

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20/9/2011

SASTRY.

Rock to Air heat transfer, →

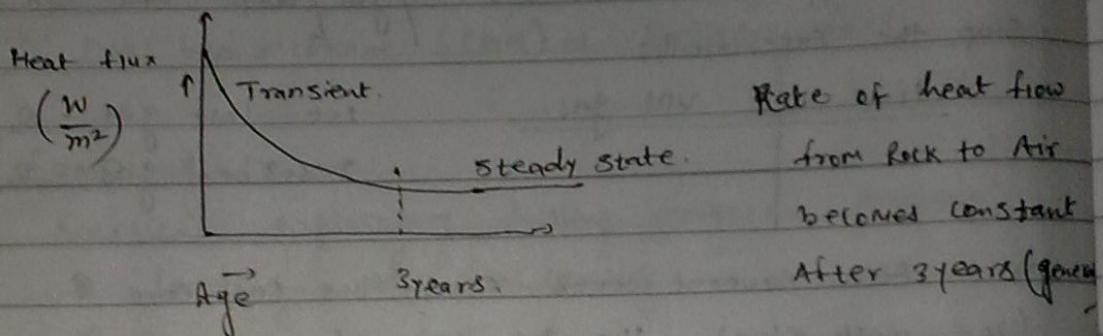


if wet
2 Surface

if Bur
heat tra

- # Methods
- ① Empiric
- ② Analyt

Empirical



Rate of heat flow

from Rock to Air

becomes constant

After 3 years (given)

convective hea

$$Q_c \propto (T_d - h_c)$$

$$h_c =$$

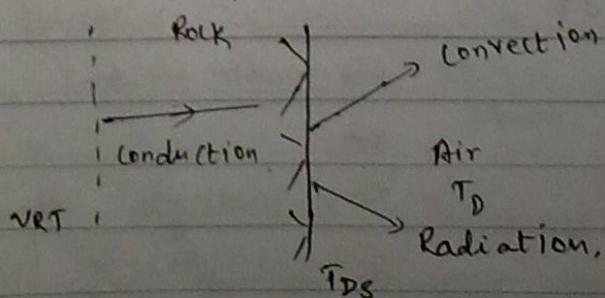
factors determining rock to air heat transfer-

- 1.) Surrounding rock properties: VRT; Density, specific heat, conductivity; geothermal gradient.
- 2.) Roadway properties → Dimensions; Age.
- 3.) Ventilation air properties : m ; psychrometric properties
- 4.) Rock to air interface properties: Wetness of the surface.

Radia

hr

Add



Rock surface is dry than 2 types of heat transfer

- ① convection
- ② radiation, or combined form
Sensible heat

If wet surface than evaporation take place.
 & Surface temp. is known as T_{ws} .

VRT (vapour temp.)

hole

→ If surface is rough than there is better heat transfer in comparison to smooth surface.

- # Methods of determining rock to air heat transfer-
- ① Empirical Methods.
- ② Analytical Methods.

Empirical methods → Assignment (Q. 4)

$$\begin{array}{c} \text{convective heat flux.} \\ \text{Rock, } T_{ws} \\ \text{Air, } T_D \\ \hline h_c \propto (T_{ws} - T_D) \\ = h_c (T_{ws} - T_D) \end{array}$$

— (1)

e of heat flow

from rock to Air

convection constant

after 3 years (general)

(Heat flux)

+ transfer-

Density, specific

g.e.

metric properties
of the surface.

h_c = Convective heat transfer coefficient

$\frac{\text{Watt}}{\text{m}^2 \cdot ^\circ\text{C}}$

$$h_c = \frac{\text{Watt}}{\text{m}^2}$$

Radiant heat flux.

$$h_r = h_r (T_{ws} - T_D) \quad — (2)$$

h_r = Radiant Heat Transfer coefficient.

Add (1) & (2)

$$\text{Sensible heat Transfer} = h_s (T_{ws} - T_D)$$

$$h_s = h_r + h_c$$

s: sensible heat

heat transfer
combined form

Rock

T_D

T_{ws}

Convective heat flux.

$$\begin{aligned} Q_c &\propto (T_{ws} - T_D) \\ &= h_c (T_{ws} - T_D) \end{aligned}$$

Radiant heat flux.

$$Q_r = h_r (T_{ws} - T_D)$$

Evaporative heat flux.

$$Q_e \propto (e_{ws} - e)$$

e_{ws} → Saturation vapor pressure at T_{ws}

e → Partial vapor pressure of atmosphere

$$Q_e = \frac{B \cdot L \cdot (e_{ws} - e)}{B}$$

B = Moisture Transfer Coeff. $\left(\frac{\text{kg}}{\text{m}^2 \cdot \text{s}} \right)$

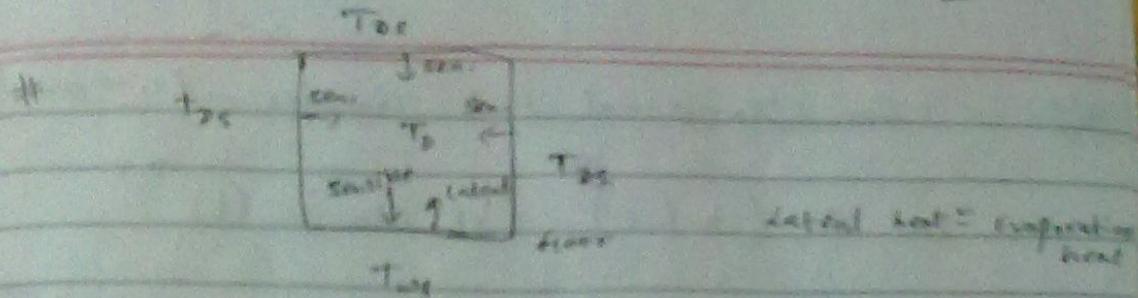
h = Latent heat of vaporization,

B = Barometric pressure.

$$B = 0.0007 \cdot h_c \quad (\text{Empirical})$$

$$\frac{\text{kg}}{\text{m}^3 \cdot \text{Pa}}$$

$$\frac{w}{\text{m}^2 \cdot ^\circ\text{C}}$$



12/12

Latent heat = Evaporation heat

Empirical Methods to estimate Rock to air heat transfer

Ramstden Equation:

$$Q_r = 5.57 (T_w + 25) (VRT - T_b) \left(\frac{p}{n} \right)^{0.37} \left(\frac{n}{3} \right)^{-0.02} \left(\frac{k}{5.5} \right)^{-0.53}$$

Q_r = Heat Transfer in kW per m length
(flow)

at Toe
of atmosphere.

f_w = fraction of roadway roadway perimeter that is wet.

p = Perimeter, m

n = Age, years

K = Rock, Thermal conductivity $\frac{W}{m \cdot K}$

$VRT \rightarrow T_w \rightarrow T_b$

$47 \rightarrow 35.5 \rightarrow 35$

tion.

Whiller Equations →

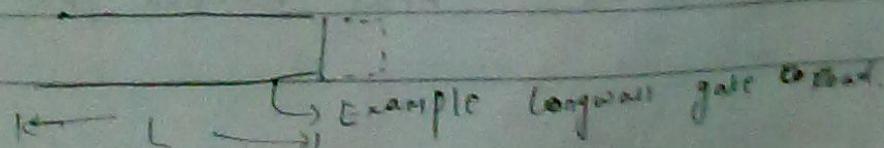
i) For Advancing Heading.

$$Q_j = 0.006 \frac{J}{KW} K (L + DFA) (VRT - T_b)$$

\downarrow
Rock thermal conductivity,

L = heading length m.

DFA = Daily advance face Advance



2.) One Dimensional Heat Transfer \rightarrow Ex. of Stop

$$B = A \cdot (k \cdot f \cdot c)^{0.5} (V_R T - T_B)^{0.5} (t)^{0.5}$$

A \rightarrow Surface Area.

B \rightarrow watt.

K \rightarrow RTC (Rock Thermal Conductivity)

$$\frac{W}{m \cdot ^\circ C}$$

f \rightarrow Rock Density kg/m^3

Rock \rightarrow Rock Specific heat $\frac{J}{kg \cdot ^\circ C}$

t \rightarrow Age in seconds.

3.) Tunnel heat flow

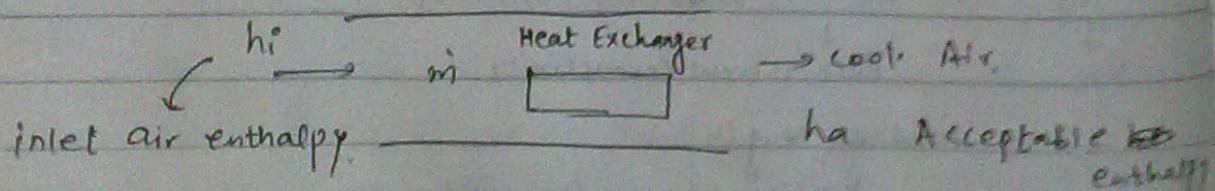
$$B = 3.35 \cdot L \cdot k^{0.554} (V_R T - T_B)$$

B \rightarrow watt.

L \rightarrow Tunnel length 'm'

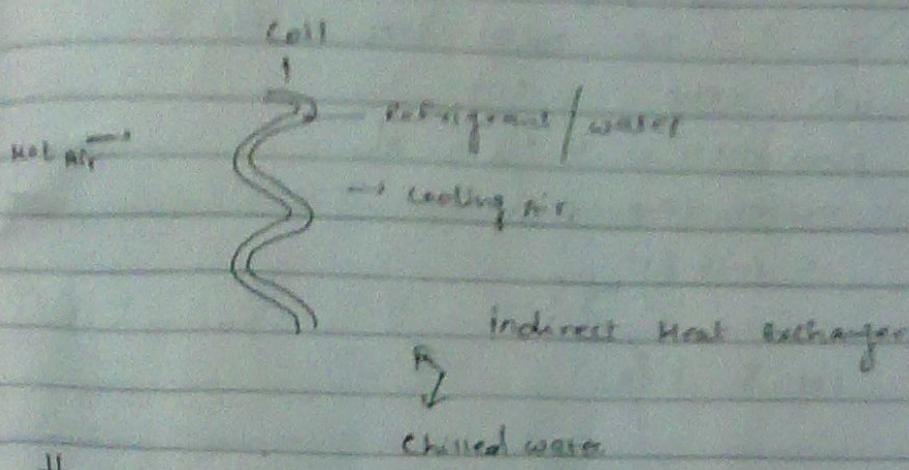
k \rightarrow RTC $\frac{W}{m \cdot ^\circ C}$

Air Cooling \rightarrow



$$m (h_i - h_a) = \text{Heat Removal (kw)}$$

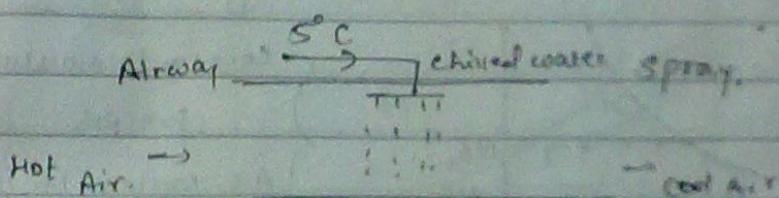
As a heat exchanger typically chilled water is used (S).



#

Hot Air → → cooled Air.

or



$$\underline{\text{e.g.}} \quad m = 20 \text{ kg/s}$$

$$h_i = 110 \frac{\text{kJ}}{\text{kg}} / \text{kg}$$

$$h_o = 90$$

$$\text{Water inlet temp.} = 5^\circ\text{C}$$

$$\text{Water flow rate} = 10 \text{ kg/s.}$$

$$\text{Water outlet temp.} = ?$$

$$\text{Ans. Heat lost by Air} = m (h_i - h_o) = 400 \text{ kW}$$

$$\text{Heat gained by water} = m_w (T_w - T_{w_i}) \text{ CP}_w$$

water Specific heat
= 4.18 kJ/kg°C

Q.2

$$m = 20 \text{ kg/s}$$

$$h_f = 110 \text{ kJ/kg} \cdot \text{K}$$

$h_o = ? \rightarrow$ outlet temp. of Air?

Water inlet temp. = 5°C

Water flow rate = $10 \text{ l/s} = m_w$

Water outlet temp. = 15°C .

$$c_{pw} = 4.18 \text{ kJ/kg} \cdot \text{K}$$

$$P = 101.3 \text{ kPa}$$

A.

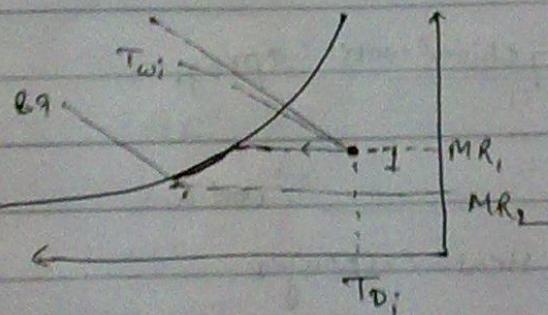
$$\text{Heat Exchange} = 10 \times 10 \times 4.18$$

$$= 418 \text{ kW}$$

$$= 20 (110 - h_o)$$

$$\Rightarrow h_o \approx 89 \text{ kJ/kg}$$

h_i

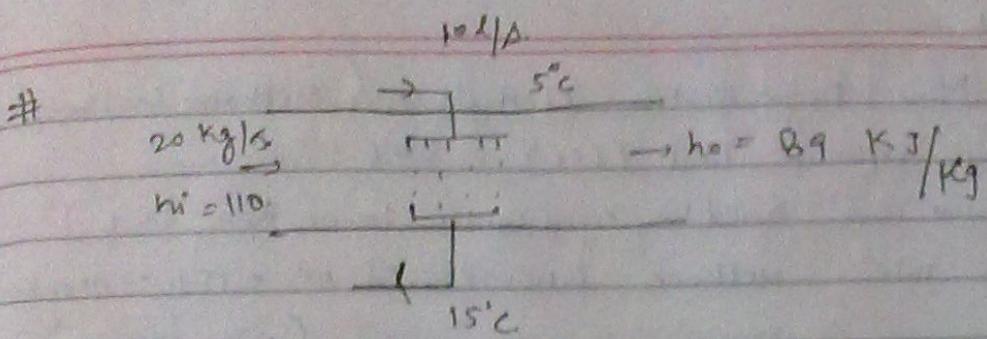


constant moisture process
As water is in pipes.

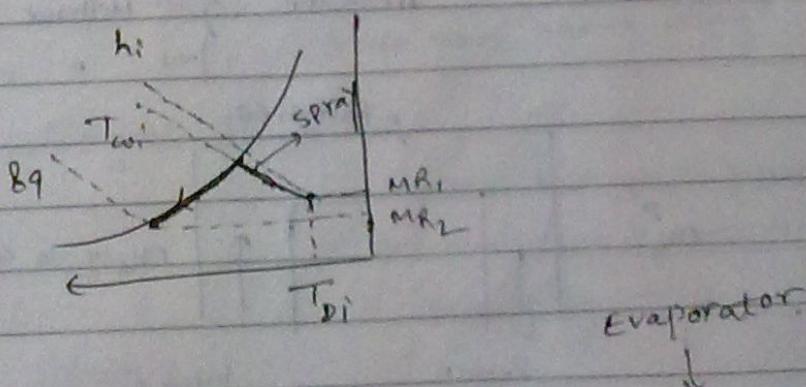
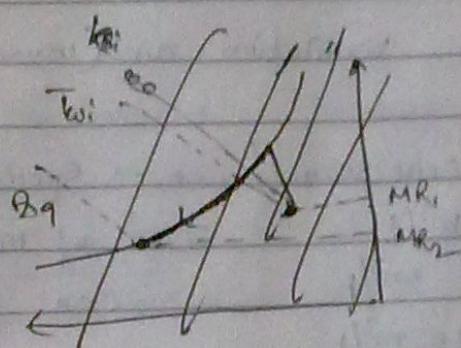
$T_{oi}/T_{wi} \rightarrow$ from $\rightarrow T_{Df}/T_{wo} ?$

$$\min (MR_1 - MR_2)$$

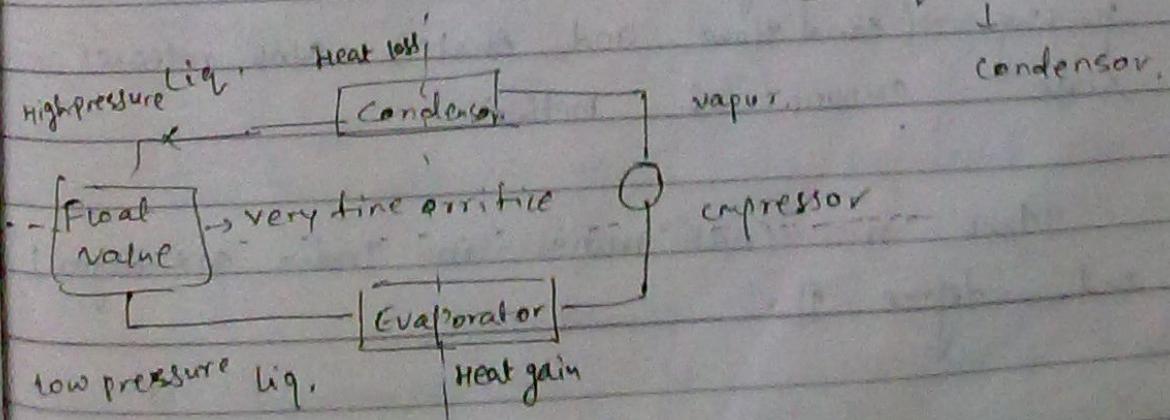
water condensed



Although h_o is same but process is diff.



Vapour Compression Refrigeration System { Removes heat from one location & physically transfers ~~heat~~ to another location.



10/10/2011

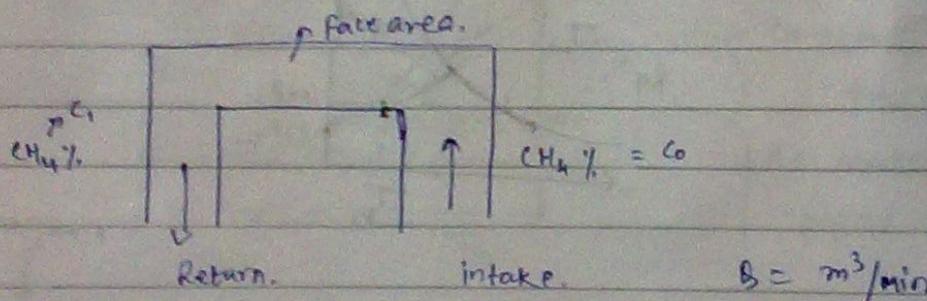
Pristy

- # Mine Degasification Method → (Methane Drainage) → Surface
 lower explosive limit (LEL) = 5.4%.
 (Methane conc. should be significantly lower than LEL)
 → Indian rule - Methane conc. should be 0.75%. → Anywhere
 (Mine Return)
 Wherever Methane emission conc. 1.25% . → face area.
- Dilution with Ventilation air (usually works for deg I & II)

→ Gasiness of coal seam / mine → Specific ~~methane~~ emission
 Degree I → $< 1 \text{ m}^3/\text{t}$ $\Rightarrow \frac{\text{m}^3 \text{ of methane emitted}}{\text{coal production t/day}}$
 Degree II → $1-10 \text{ m}^3/\text{t}$
 Degree III → $> 10 \text{ m}^3/\text{t}$

1) Vertical
 well spacing

Measure $\{ \Rightarrow \text{Methane conc. in return air}$
 $\Rightarrow \text{ " " " intake air}$



→ Specific methane emission can be higher than the gas content of coal seam as parting (sandstone and shale) also releases some amount of methane.

→ Most of Coal mines in India are degree I and degree II.

→ Coal bed drainage

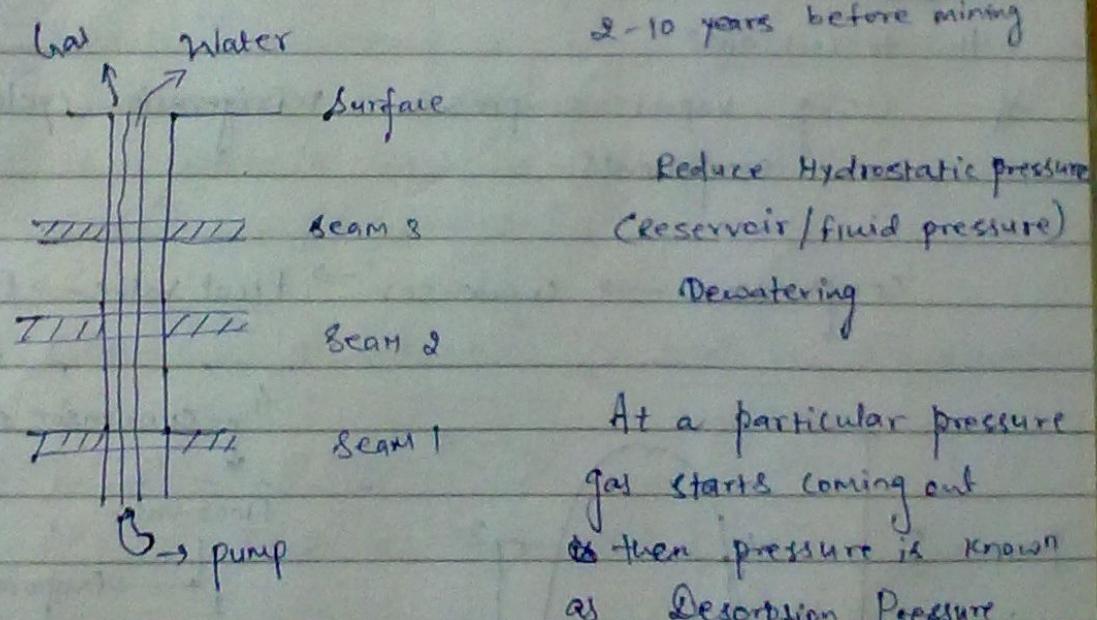
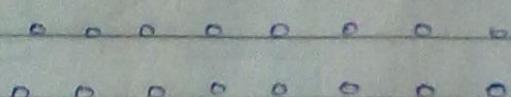
→ If pressure increase
 Methane

→ Surface Technique → vertical borehole with or without hydraulic fracturing
 → Underground Technique. → GOAF well

- (a) Inseam Horizontal Borehole.
- (b) Cross Measure Borehole.
- (c) Superjacent Gallery (Hirschbach Method)
- (d) Packed Cavity Method

1) Vertical Borehole - Premining method

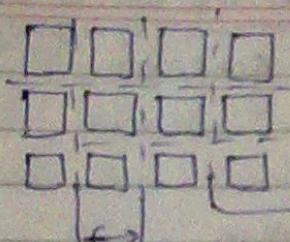
well spacing



→ Coal permeability plays an important role in drainage of methane by this method.

Permeability $> 5 \text{ millidarcy}$

→ If permeability is b/w 1 to 5 md then to increase permeability we perform ~~Hydraulic fracturing~~ Hydraulic stimulation



Cleat Spacing

cleat (provide pathway to flow water)

→ to Condense water, heat exch

→ Evaporator

hot water

Preppant

→ we can increase permeability 100 times, 1000 times.

11/10/2011

Sastry

How to cool air?

Using vapour compression refrigeration cycle.

4 - components -

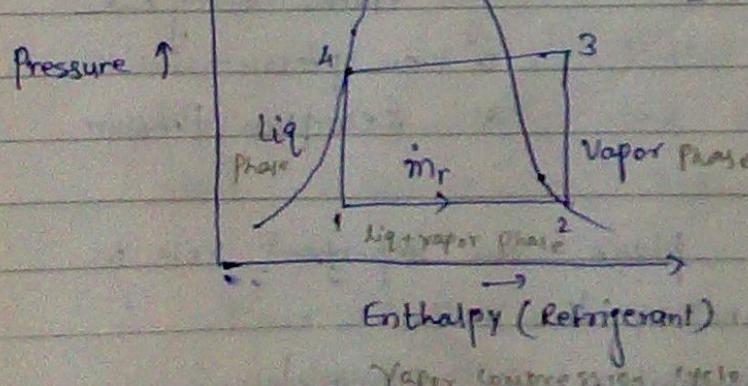
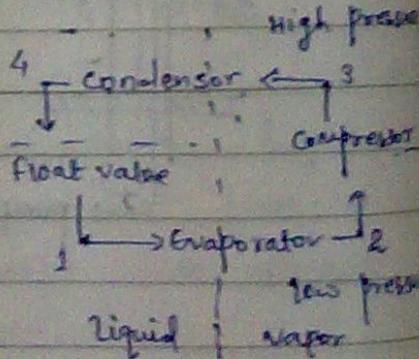
Theoretic

COP: Cool

COP is

COP

compressor → condenser → float valve → evaporator



→ Refrigerant is normally in vapor state at room temp. & pressure.

Plant

Evapo

wat

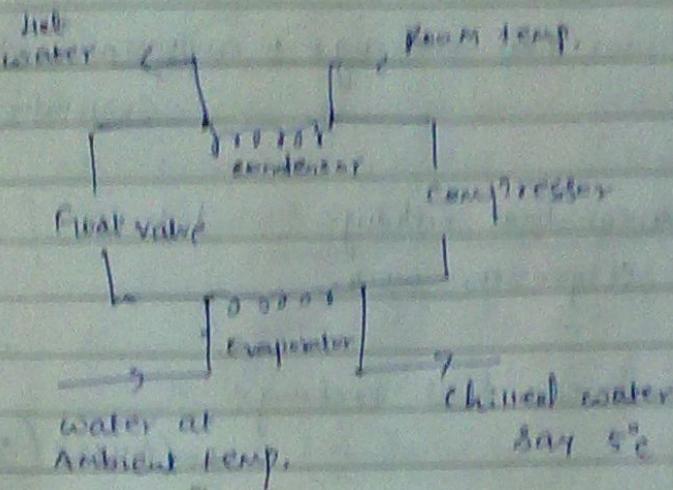
les w

pathway to flow
ex)

- Cooling load as a refrigeration load \rightarrow $Q = \dot{m} \cdot h_{fg}$ (Latent heat)
- Condenser outlet flow rate \rightarrow $Q = \dot{m} \cdot h_{fg}$
- > In condenser under its circulating line to chiller water, heat exchange takes place in condenser.
 - > Evaporator is also an heat exchanger.

No. of coils
Length (cm, m)

100 times, 1000



Theoretical efficiency = Carnot cycle efficiency

COP: Coefficient of performance

COP is constant for a particular refrigerator

COP ↑ Performance ↑

$$\text{COP} = \frac{\dot{m}_r (h_2 - h_1)}{\dot{m}_r (h_3 - h_2)}$$

Heat ex. at evaporator
compressor output work

$$\text{COP} \approx 1.6 \text{ to } 1.8 \text{ (Generally)}$$

valve → Evaporator
high pressure
condenser ← 3
Compressor
low
→ evaporator ← 2
high pressure
vapor

Ex1 Condenser cooler flow rate = 30 kg/s

$$T_{out} = 25^\circ\text{C} \quad T_{in} = 34^\circ\text{C}$$

$$\text{Plant COP} = 4.0$$

Evaporation water flow rate = 15 kg/s

$$\text{water inlet temp.} = 25^\circ\text{C}$$

what is the expected chilled water temp?

Let's assume heat exchange efficiency = 100%.

Ay

$$h_2 - h_4 = h_3 - h_2 + h_2 - h_1$$

(neglecting work)

$h_4 \approx h_1$

Condenser heat exchange \cong compressor work +
Evaporator heat ex.

$$\Rightarrow \frac{\text{Condenser heat exchange}}{\text{compressor work}} = 1 + \text{COP}$$

water at
cycle

$$\left\{ \begin{array}{l} m_R(h_3 - h_1) \\ \text{Assume} \end{array} \right\} = \text{Condenser heat exchange} =$$

$$30(4.183)(34 - 25) \text{ kJ}$$

$$\frac{\text{kg/s}}{\text{KJ/kg°C}} \quad \frac{1}{°C}$$

$$\Rightarrow \text{Compressor work} = \sqrt{225.882} = 1129.41$$

$$\text{Evaporator heat ex.} = \sqrt{ }$$

$$\text{final temp. of chilled water} = \sqrt{ }$$

water
at
cycle

$$\Rightarrow 1129.41 = \frac{225.882}{\text{Exch. heat ex.}} + \text{Evaporator heat ex.}$$

$$\Rightarrow 867.85 + \text{Evaporator heat ex.}$$

Cool Air → fan
ID Fan

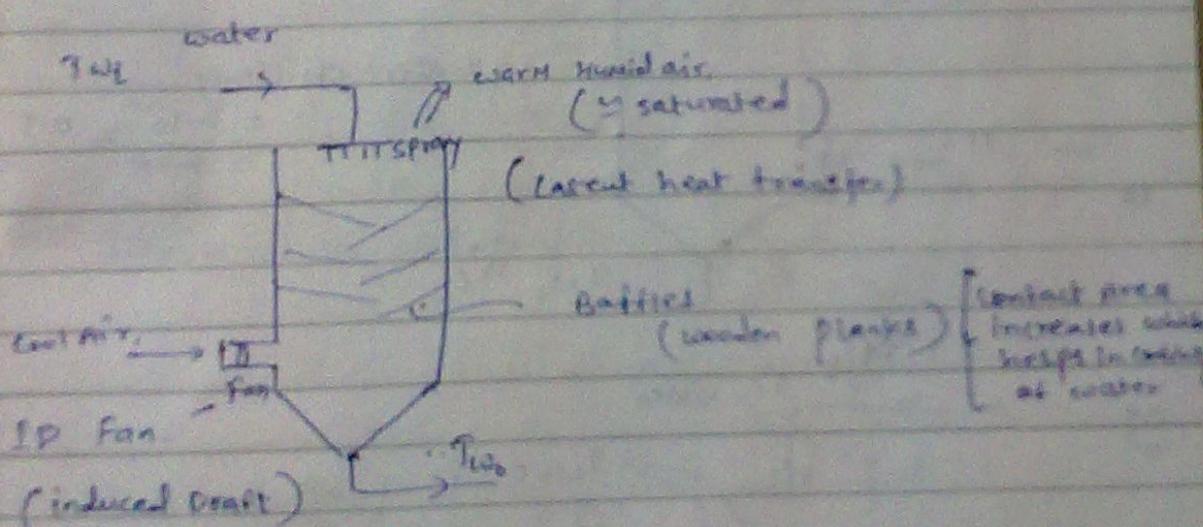
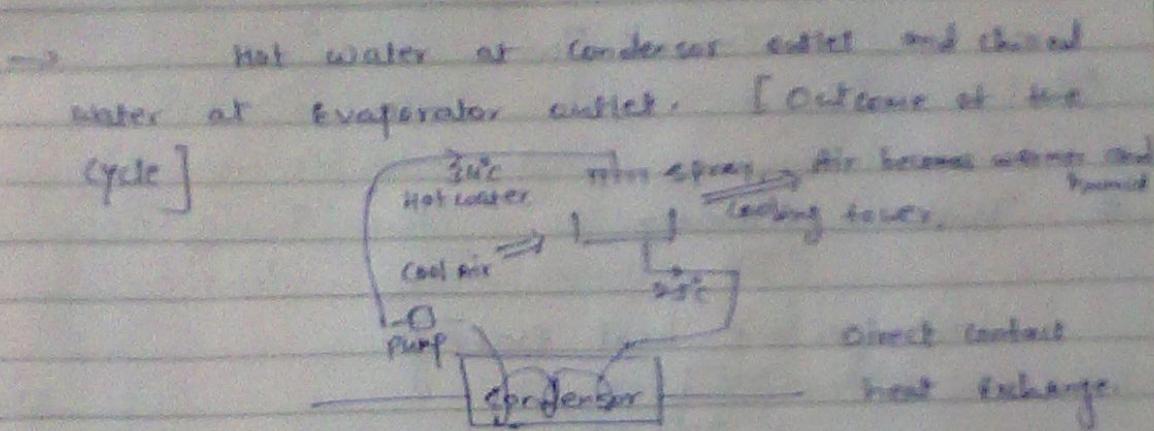
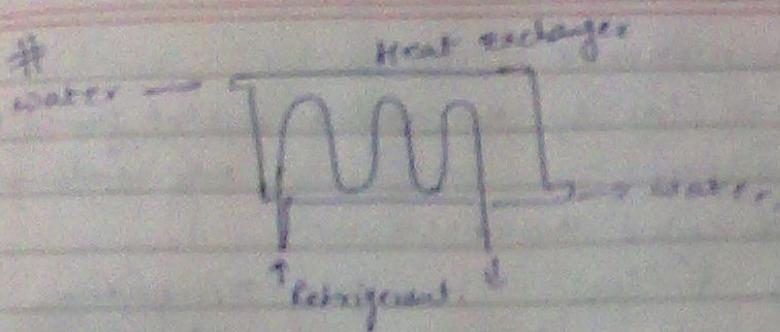
$$\text{Evaporator heat ex.} = \frac{415.764}{\text{Exch. heat ex.}} = 903.58$$

$$\Rightarrow 15 \times 4.183(T_f - 25) = 415.764$$

$$T_f = \frac{10.6^{\circ}\text{C}}{ }$$

Water #
Water.

Air
 m_a



Section II Direct heat Exchange -

Water
 m_w , T_{wi} , T_{wo}

Air

m_a (dry air) is $T_{wi} - T_{wo}$

Sign heat is $= f(T_{ab})$

Enthalpy is $= f(T_{ab}, T_{db})$

but Enthalpy \approx Sign heat (Approx.)

1st Law of Thermodynamics =

Heat lost by one medium = Heat gained by other medium.

2nd Law of Thermodynamics =

In a water cooled system

$$T_{wo} \neq T_{obi}$$

in an air cooled system.

$$T_{wo} \neq T_{oi}$$

{ Thermodynamic
Limits }

→ factor of n
, size
depends on } com
f

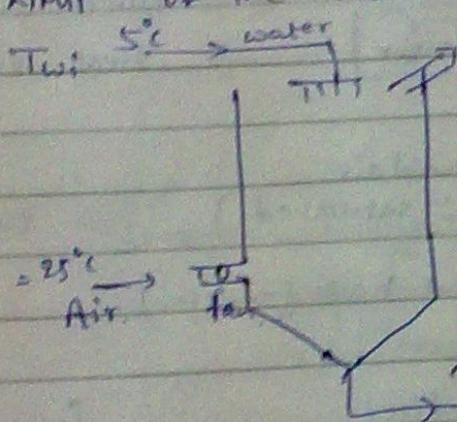
Empirically
Thermal Co

factor of
(Property o

P.D.

Water Efficiency = $\frac{T_{wi} - T_{wo}}{T_{wi} - T_{obi}}$

Limit of the heat exchange.

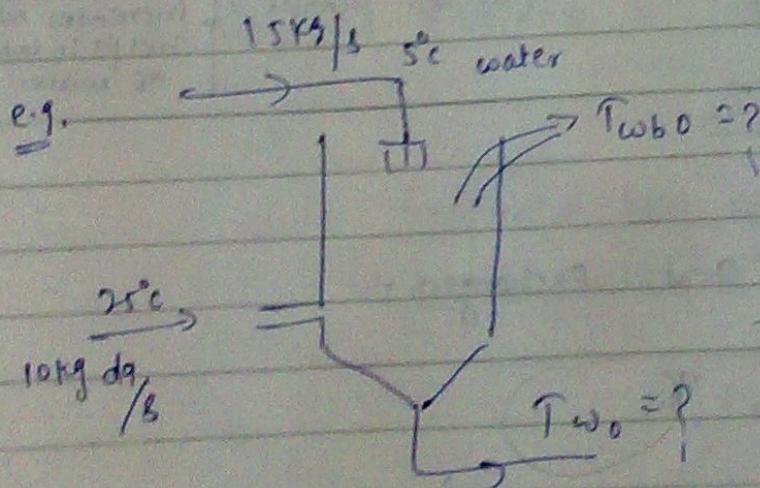


water efficiency

$$= \frac{-10}{-20} = 0.5$$

R =

Determined



Equivalent specific
heat of
(Air + wa

Water ↑

Heat gained by other medium.

Thermodynamic Limits

→ Factor of Merit of a Direct Contact heat exchanger.

Depends on } Size of water droplets
Contact area
flow rate, etc.

Empirically Explained in terms of water efficiency and Thermal Capacity Ratio.

factor of Merit = f (water η : Thermal Capacity ratio)
(Property of Heat Exchanger)

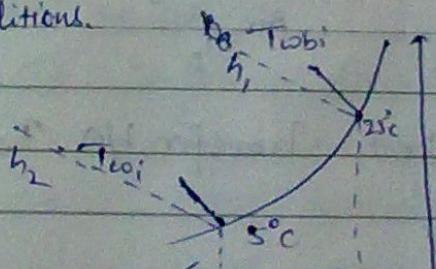
R = Thermal capacity ratio

$$R = \frac{\text{Heat Exchange ability of water per } ^\circ\text{C}}{\text{Heat Exchange ability of air per } ^\circ\text{C}}$$

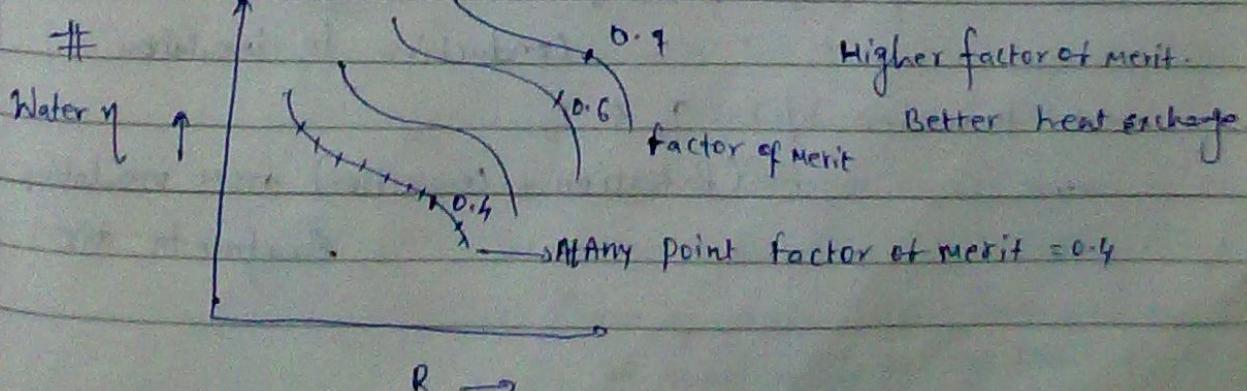
$$= \frac{-10}{-20} = 0.5$$

$$R = \frac{\dot{m}_w (h_{183})}{\dot{m}_a (C_p)}$$

Determined by inlet conditions.

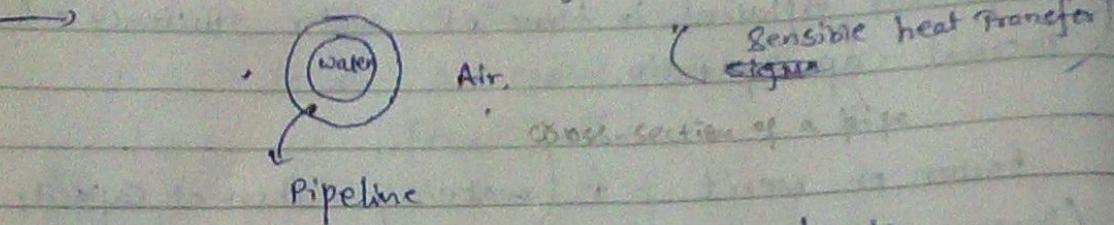


$$\text{Equivalent specific heat of air + water vapor mix.} = \frac{h_1 - h_2}{25 - 5} = C_p$$

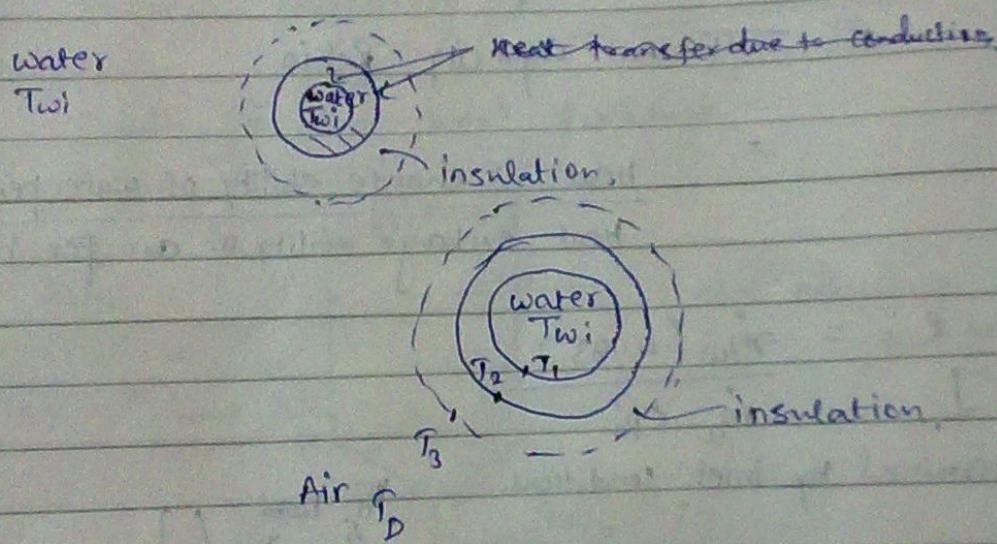


→ If for a tower factor of merit is known and it is calculated from inlet conditions, then we can estimate water η .

Indirect Heat exchange (coil)



To prevent heat transfer insulate the pipeline



Heat Transfer b/w T_{wi} & T_1

= Convection b/w water and Metal Surface.

Heat transfer b/w T_1 & T_2

= conduction in metal

Heat transfer b/w T_2 & T_3

= conduction in insulation

Heat transfer b/w T_3 & T_d

= (Radiation + Convection) from insulation

Surface to air

On air

Newton's law of motion

$V_{A,r}$ = Radial component of the absolute velocity with respect to air
 $V_{A,t}$ = Tangential component of the absolute velocity
 The radius of the impeller inlet is r_i
 outlet is r_o

$Q = \text{Quantity of air passing } m^3/s$

$\rho = \text{Density of air}$

mass = $\rho Q = \text{kg/s}$

Change of momentum from inlet to outlet

$$= \rho Q (V_{A,t} - V_A)$$

change of moment of momentum from inlet to outlet

$$= \rho Q (\omega r_o - \omega r_i)$$

$$\left\{ \begin{array}{l} T = \rho Q (V_{A,t} - V_A) \\ \therefore F = \end{array} \right.$$

Power = $T \times \omega$ [$\omega = \text{Angular vel.}$]

$$\text{Total power} = \rho Q \omega (V_{A,t} - V_A)$$

$$\Rightarrow \text{Head H} = \frac{\text{Power}}{\rho g} = \frac{\omega (V_{A,t} - V_A)}{g}$$

$$= \frac{(V_{A,t} - V_A)}{g}$$

for a special case of meridional entry (where there is no rotation initially), it will be the pressurization of air

$$V_1 + V_{R_1} + V_{U_1} = 0$$

$$H = \frac{V_{U_2} U_2}{g} \quad V_{U_2} = U_2 - V_{R_2} \cot \beta_2$$

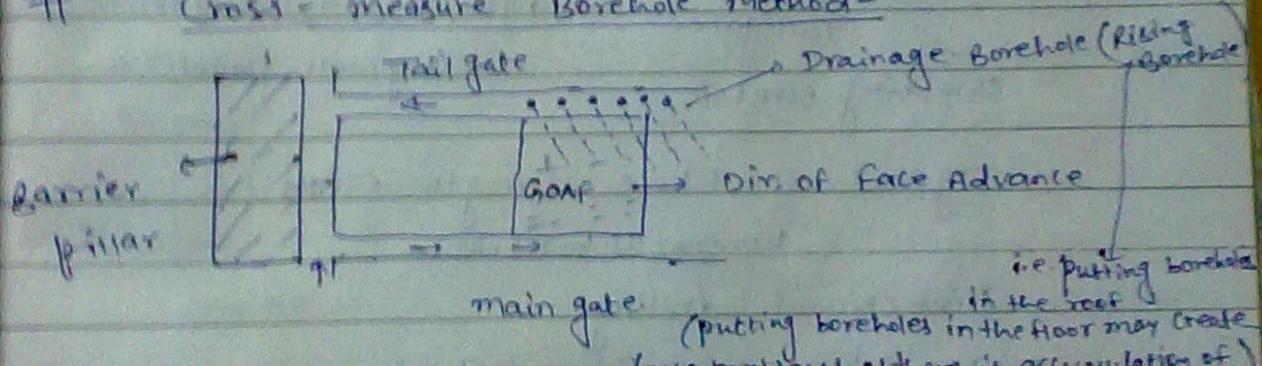
$$H \text{ or } U_2 (U_2 - V_{R_2} \cot \beta_2) \quad (\text{Theoretical Head})$$

MSD factor
as Euler's head

→ for a backward bladed centrifugal fan β_2 is always less than 90° . And it is eq. to 90° for radial bladed & greater than 90° for a forward bladed fan.

Priority:

II Cross-measure Borehole method-



- Drilling of borehole is being done before the formation of GOAF.
- Angle of Drilling $30^\circ - 50^\circ$
- Generally we prefer drilling of borehole in tail gate side. But if seam is very gassy then we can also drill boreholes in main gate side.
- Small Dia boreholes - $65 - 120\text{mm}$.
- Spacing between 2 boreholes → $10 - 30\text{m}$. Sometimes it may be upto $100 - 150\text{m}$
- Length of borehole → $25 - 40\text{m}$.
- Angle $30^\circ, 60^\circ$

- This method is followed in European mines.
- for the deep mines we prefer U/G method.

- Examples of how

Horizontal boreholes in advance of working-

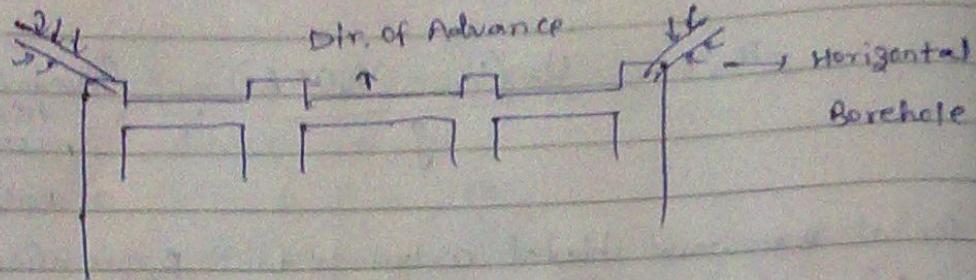


fig: for a Room & Pillar working.

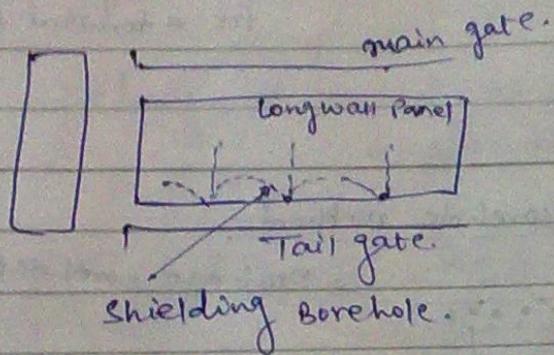
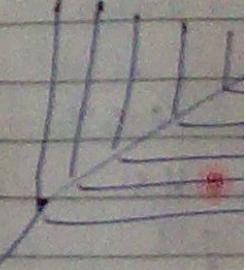
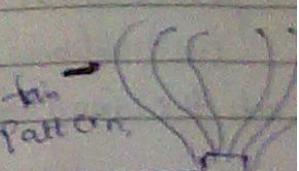


fig: Horizontal boreholes in longwall panels.



→ Horizontal methane expensive.

Typical short hole (Length < 300m)
Horizontal boreholes.

18/10/2011

Answer

→ Directional drilling.

→ Now Advancement in drilling. We can create a horizontal borehole upto a 1500m dist.

This type of boreholes are known as long horizontal borehole.

→ Also known as In seam borehole Technique.

→ Pocahontas no.3 coalbed of Pennsylvania USA.

→ Drainage efficiency $\approx 30\% - 60\%$.

→ Lead time \rightarrow 6 to 18 months.

After putting boreholes How much time it is getting for drainage of gas. is known as Lead time. Depends on face advancement rate.

Ex 1 The
fan ha
1200 mm
theoretical
rotating
Meridio

region mines.
U/G method.

of working -

→ Horizontal
Borehole

total boreholes in
11 panels.

on)

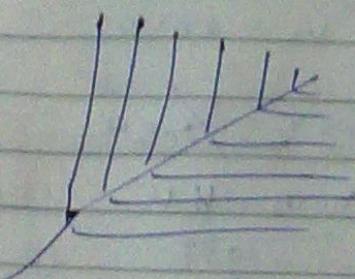
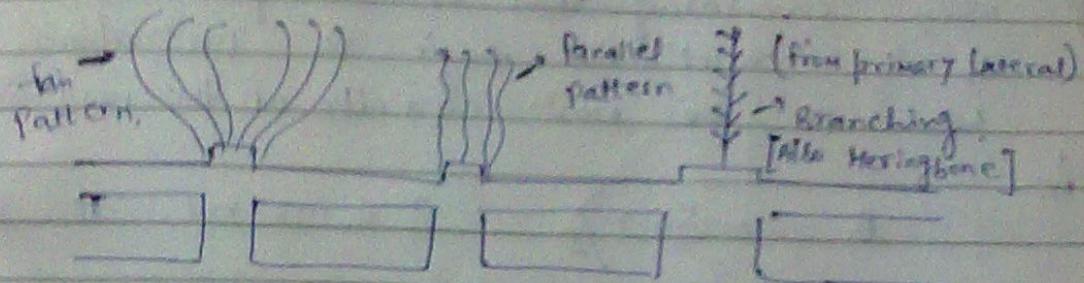
We can create
room dist.

as long

Technique.
penn by Manita

time it is
known as .
out rate.

- Examples of horizontal drilling -



pinnate drilling (Leaf shape)

→ Horizontal borehole is most effective as far as methane drainage is concerned. But it is more expensive.

18/10/2011

Samantha

$$H_e = \frac{U_2^2 - U_2 V_{R_2} \cos \beta_2}{g}$$

$$U_2 = \omega R_2 = 2\pi n R_2 \quad \text{r.p.s.}$$

At Max theoretical fan capacity

$$V_{R_2} = U_2 \tan \beta$$

$$U_2 = \frac{\omega}{2\pi R_2} b_2$$

~~U_2~~ b_2 = width of the fan

Ex.1 The impeller of a backward bladed centrifugal fan has a diameter of 2500 mm & a width of 1200 mm at the outlet. Calculate the maximum theoretical head the fan will develop when rotating at a speed of 280 r.p.m. Assume Meridional entry into the impeller. What will

At Maximum fan capacity $V_{R2} = \frac{U_2 \tan \beta}{g}$

be the theoretical head developed by the fan when circulating 50 m^3 of air per second.

If the outlet fan angle is 1.13 radian .

What is the max^m capacity of the fan (theoretical).

Ans.

$$Q_s = 50 \text{ m}^3/\text{s} \quad \beta = 1.13 \text{ rad.}$$

$$n = \frac{280}{\pi \times 60} \text{ r.p.s.} \Rightarrow U_2 = 2\pi \times 50$$

$$\text{diameter at outlet} = 25.00 \text{ mm} \\ \text{width} = 1200 \text{ mm} \Rightarrow V_{R2} = \frac{U_2}{2\pi r_2 w}$$

$$\Rightarrow \text{maximum theoretical head} = \frac{V_{R2} U_2 - V_{U_1} U_1}{g}$$

for meridional condition $V_{U_1} = 0 \text{ f. } V_{R1} = 0$

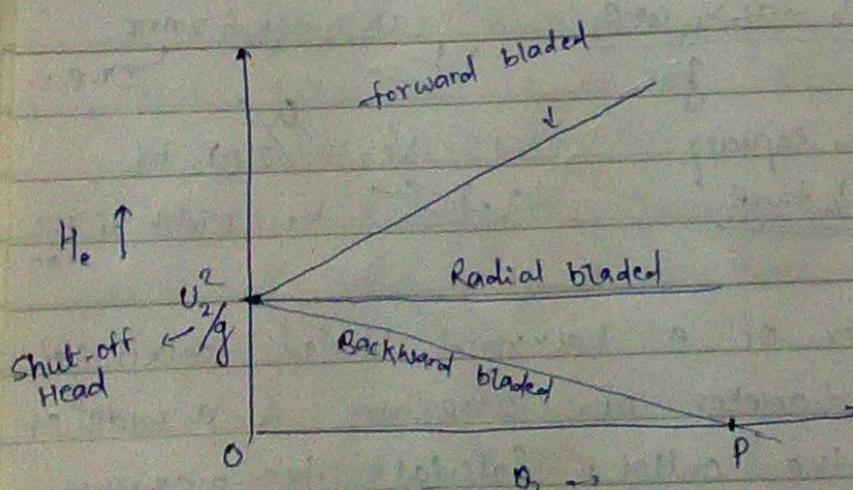
$$H = \frac{V_{R2} U_2 - V_{U_1} U_1}{g}$$

$$\Rightarrow ① \text{ Max. theoretical head} = \frac{U_2^2 - C_{f2} V_{R2}^2 \cot \beta}{g} = \left(2 \times \pi \times \frac{2.5}{2} \times \frac{280}{60} \right)^2 = 137.07 \text{ m}$$

$$② \text{ Theoretical head developed} = \frac{U_2^2 - V_{U_1} V_{R2} \cot \beta}{g}$$

$$③ \text{ fan capacity} = \frac{V_{R2}}{g} = \frac{U_2 \tan \beta}{g}$$

Head vs Quantity curve \rightarrow



OP - Max capacity
of a backward bladed fan.

ii) Mechani

Input Pow

\rightarrow At the 'O' quantity fan (backward bladed) produces max head.

$\beta_2 \leq 90^\circ$

$\beta_2 = 90^\circ$

$\beta_2 \geq 90^\circ$

Shut-off

is known

Various

There

i) Hyd

ii) M

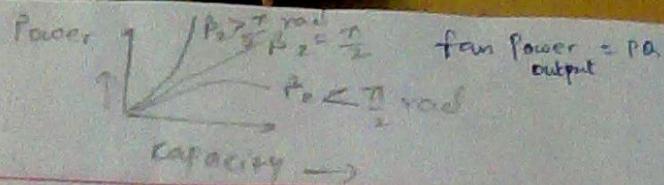
iii) bearing

iv) Lea

between
machine.

losses
impeller,
losses
attributed

Yield



y the fan.

Second.

radian.

e fan (Theoretical)

$\beta_2 \leq 90^\circ$ for backward bladed. $\Rightarrow \alpha$

$\beta_2 = 90^\circ$ for radial bladed

$\beta_2 \geq 90^\circ$ for forward bladed.

at '0' quantity $N_{Re} = 0$.

Shut-off Head → at '0' quantity head developed
is known as Shut-off head.

$H = 0$ at shut-off head

Various losses in fan →

There are 3 type of losses -

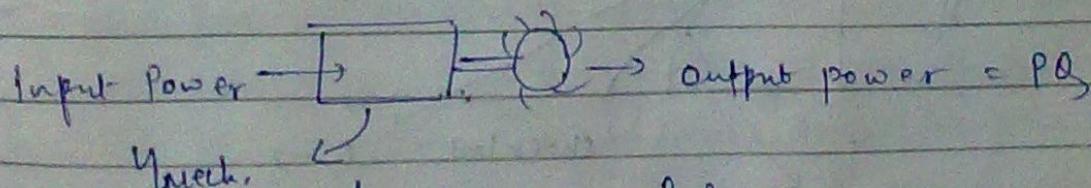
i) Hydraulic Losses

ii) Mechanical losses of power due to friction at bearings & disc friction.

iii) Leakage losses - leakage through clearances between the rotating and stationary points of a turbo machine. (Volumetric Efficiency)

Losses due to skin friction and diffusion in the impeller, and losses due to eddy and separation losses at the impeller inlet & outlet. This loss attributed to the head loss.

ii) Mechanical losses →



$$\text{Air power} = P_a \cdot \eta_a$$

$$\text{Actual power} = \frac{P_a}{\eta_{Mech}}$$

→ different fan quantity at output

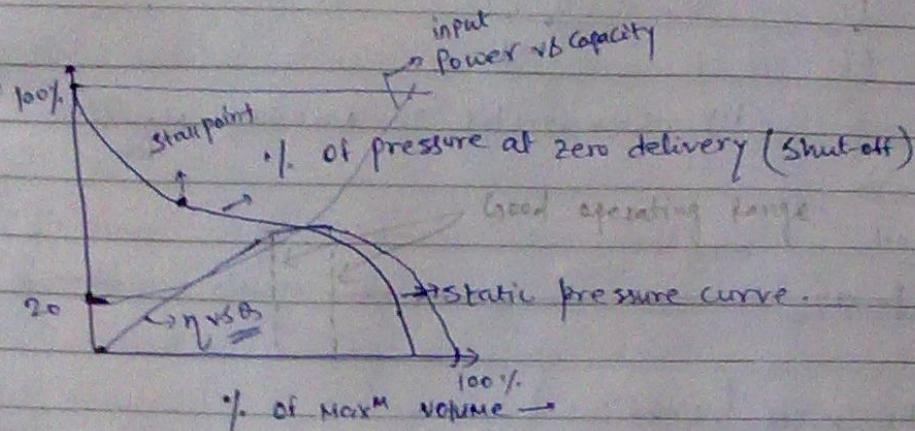
→ Velocity

Fan Characteristics →

- i) Head - Capacity characteristics
- ii) Power - capacity (B)
- iii) Efficiency - capacity

↓ characteristics

fig: extraction losses
friction loss



Max. efficiency $\approx 60-70\%$

fig: forward bladed characteristics

R_s - Shock loss quantity

$$(R_s - R_{s3})^2$$

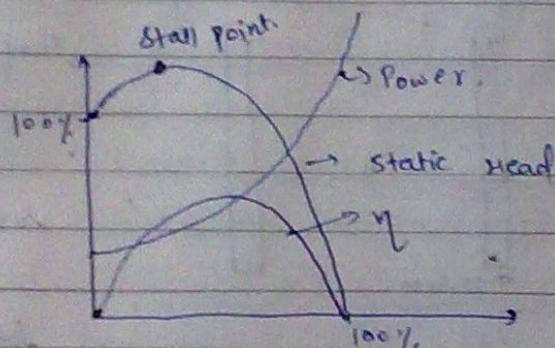


fig: radial bladed fan characteristics

"% of Max^m capacity."

Stall Point → fan generally operates below the stall point.

At stall point there is generation of max sound and lot of disturbances & ultimately lead to decrease in efficiency.

In all types fan, the operating point should be fixed to the right of the aerodynamics stall point 'P' which is point of reverse flexure, for at capacities less than this the performance of the fan becomes unstable and occurs fluctuation of air velocity characterized by throbbing and noise.

considering Hydrostatic losses

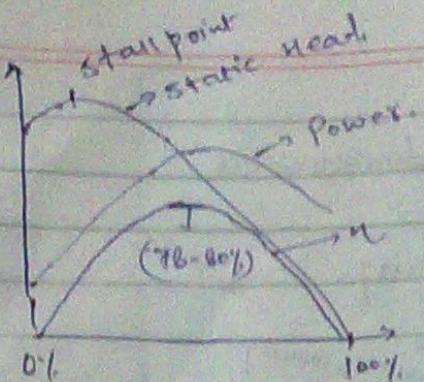
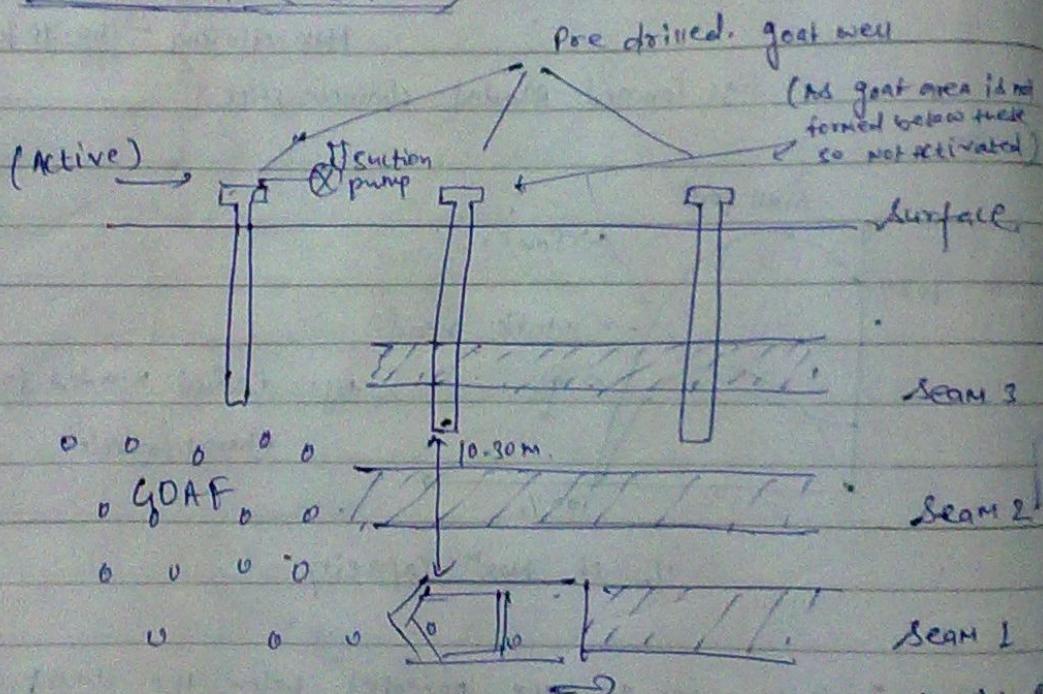


fig. characteristic of backward bladed fan

24/10/2011

Porousy

GDAF Well (vertical)



permeability increased (orders of magnitude 10^6)

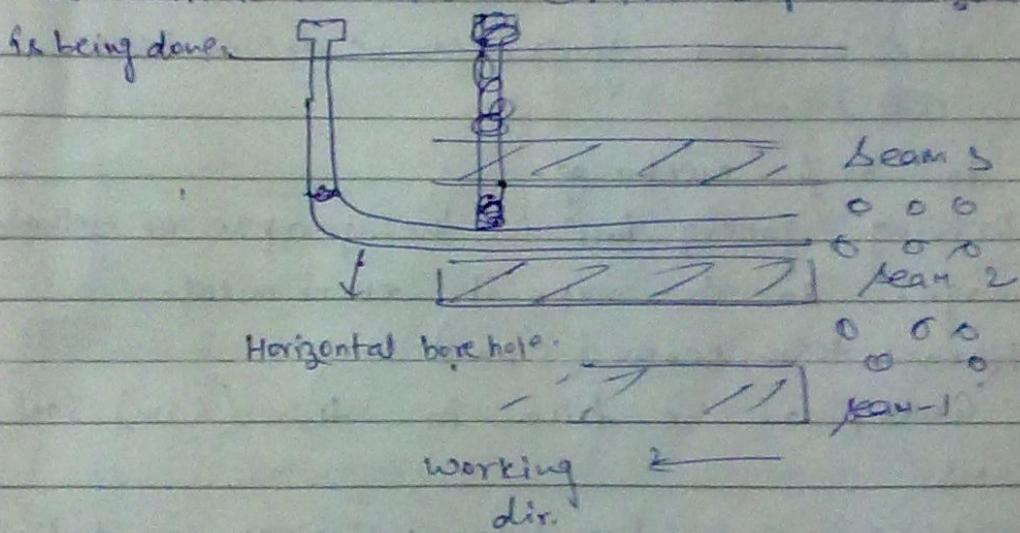
$\approx 10^2, 3, \dots$

- Life of the Bore hole is not so long. (Life $\approx 2-3$ years)
- Open hole completion (No casing is required as life span is short)
- Mostly used in mines of less to moderate depth.

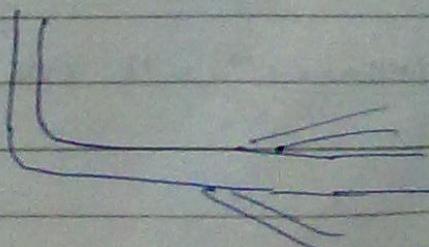
→ Boreholes are coal seam caved zone fracture 2
→ Quality of gas beyond 30%.
→ As life To make it bore hole
Instead of is sufficient in being done

- Boreholes are now not to be bring to working coal seam AS caved zone \rightarrow 3 times coal seam thickness fracture zone \rightarrow 50 times coal seam thickness.
- Quality of gas \rightarrow Initially quality is upto 70%. But beyond that it degrades & go below to 30%. that's why life span is very short.
- As life span is very short it is more costly. To make it profitable horizontal drilling is used and borehole changes to as shown in figure.

Instead of using multiple borehole only 1 borehole is sufficient & after certain depth horizontal drilling is being done.



- This technique is used very much in Australia (Bulli seam mine)
- To make drainage more efficient we can make multiple lateral.



blasted
fan

out well

(As goat area is not formed below these so not activated)

surface,

Seam 3

Seam 2

Seam 1

)

so long. (Life \rightarrow 15 required as

to moderate

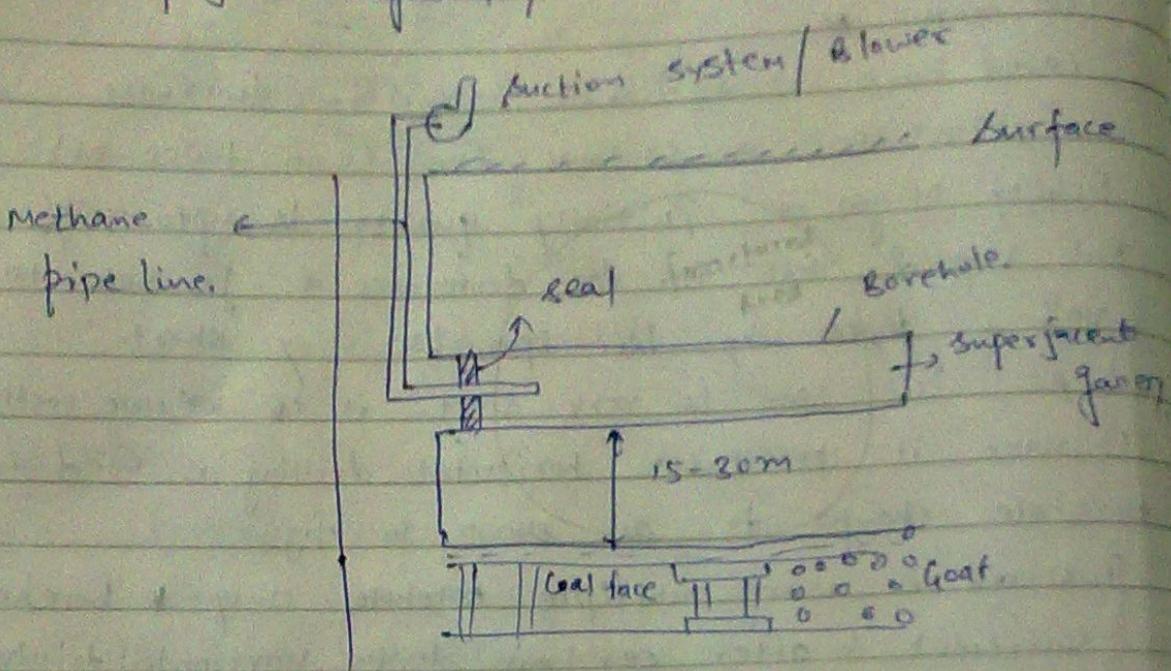
Discuss the technological and aspects of

Assignment

25/10/2011

Samantha

Superjacent gallery / Hirschbach Method →



→ In some of cases gallery can be driven below the coal seam.

→ 70-80% methane.

→ Driving gallery just for the purpose of methane drainage. So to make it economical.

→ When thin seam ($< 1\text{m}$)

(a) Gallery can be driven in thin ($< 1\text{m}$) coal seams.

(b) using 2-3 bore hole using Horizontal drilling.

(c) By using unused gallery or preexisting gallery.

Highly gassy mines of Europe (Germany, for example)

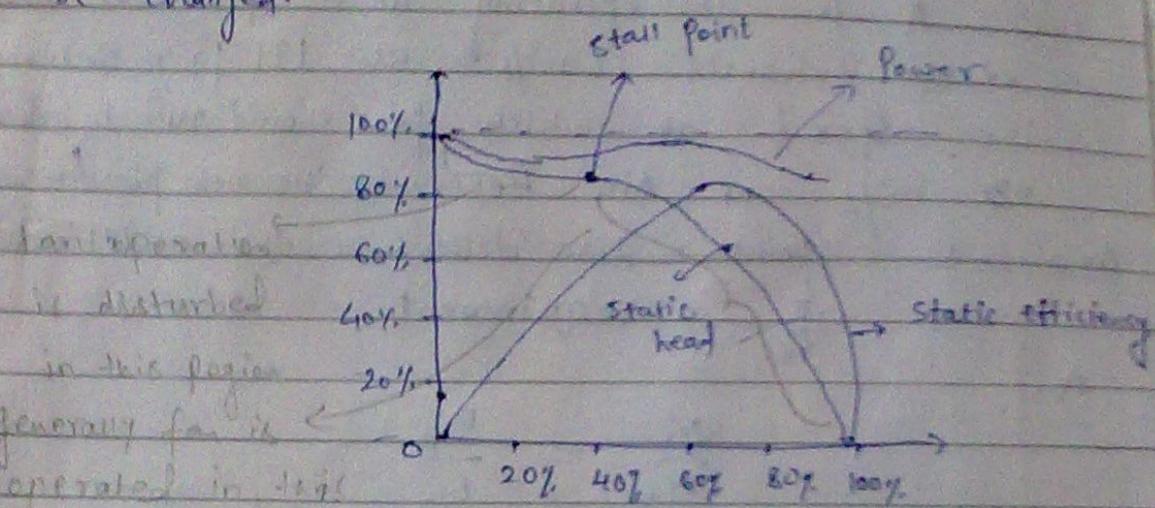
Use of methane → i) CNG ii) Power production

25/10/2022

Bhartiya

Axial flow Fan \rightarrow In India Axial flow fan is used generally. As it takes less space in installation as compare to centrifugal fan.

Also it is easier to change blade angle of axial fan so that and hence fan characteristics can be changed.



Fan Laws \rightarrow

- i) Fan Speed $\{ \Rightarrow$ fan characteristics can be changed, if we change anyone
- ii) fan diameter $\}$ ~~anyone~~ of these parameters.

a) When fan diameter is kept constant and fan speed changes, then

$$\begin{aligned} \text{(Capacity)} \quad \text{Quantity} &\propto \omega^1 \text{ (Angular velocity)} \\ \text{Head} &\propto \omega^2 \\ \text{Power} &\propto \omega^3 \end{aligned}$$

→ b) When Speed is constant (specific speed) then
 $H \propto D^2$ ($D = \text{diameter}$)
 $B \propto D^3$
 $P \propto D^5$

Ex1 A fan is operating at a speed of 1000 rev/min which exhausts $66 \text{ m}^3/\text{s}$ at 171 Pa . Determine the speed at which fan should run to exhaust $83 \text{ m}^3/\text{s}$ of Air. Determine the new pressure at this point. Also determine the additional power requirement.

Ans.

$$\frac{W_1}{W_2} = \frac{B_{21}}{B_{22}}$$

$$\Rightarrow \frac{1000}{W_2} = \frac{66}{83}$$

$$\Rightarrow W_2 = \frac{83000}{66} \text{ rev/s}$$

$$\Rightarrow P_2 = \frac{\left(\frac{83000}{66}\right)^2}{(1000)^2} \times 171$$

$$\therefore \text{Power} = \frac{\left(\frac{83000}{66}\right)^2}{(1000)^2} \times [171]$$

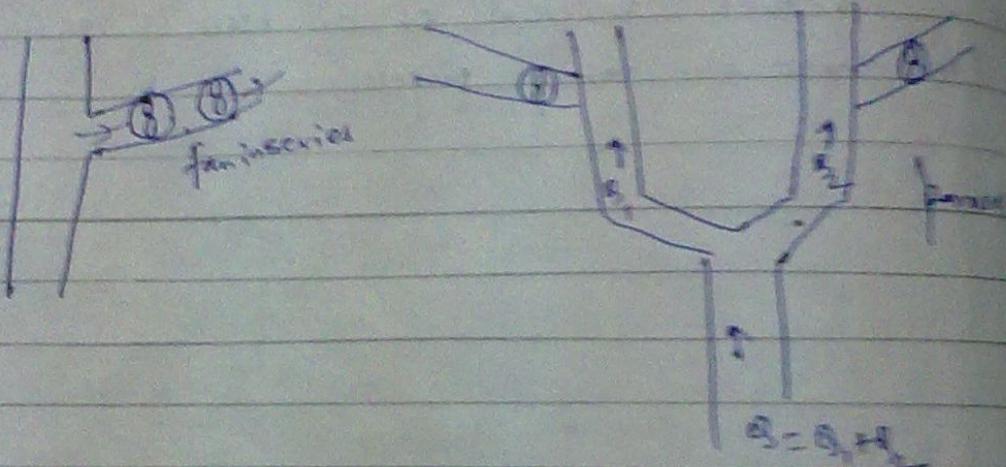
Multiple fans → if fans connected in series

a) ~~fan travel.~~ (when quantity is more)

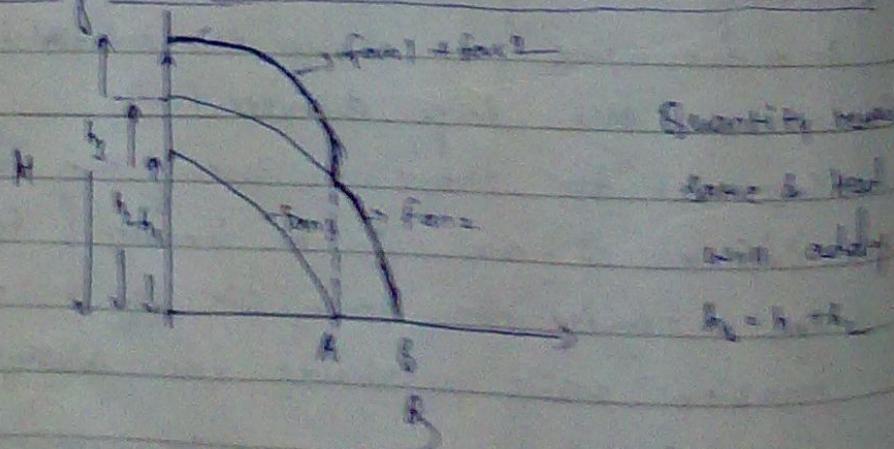
Combination of nine fans -

- (a) fan in series → Each fan in series handles amount of current and the req. pressure to overcome the resistance is shared by both of them [Quantity is same & pressure of different fans are added]

- (b) fan in parallel → Each fan will operate in same pressure but handles different amount of air current.



Operating characteristics curve (fan in series)

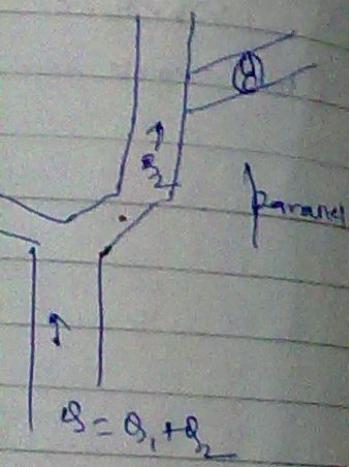


If quantity is the same then fan 1 & 2 increase resistance.

be put in series [because
et. (when quantity is
more)

an in series handled
eq. pressure to over lay
both of them.
[fans are added]

operate in same pressure
air current.



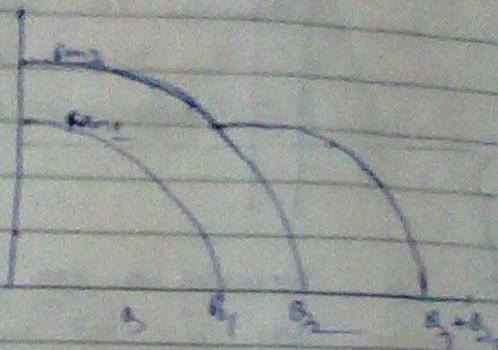
(fan in series) →

Quantity remain
same & Head
will add up

$$h_1 + h_2 + h_3$$

fan 1 & 2 will

fan in parallel

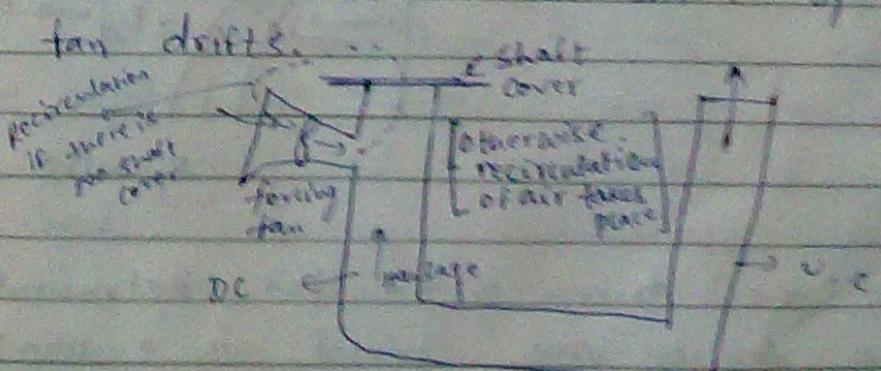


Add Quantity added up.

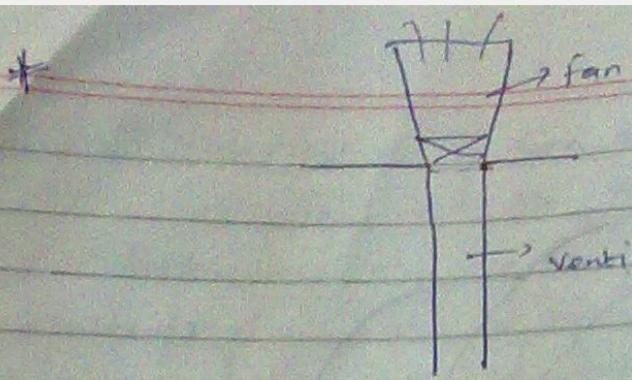
27/10/2011 Savantha

Installation of Mine fan

Main Mine fans are installed at the surface. They can be directly mounted over the shaft with their axis vertical. They can be horizontally on the ground connected to the shaft by a suitable bend. The later is essential in coal mines with the fan being located at least 5m away from the shaft in order to protect it from possible explosion. Where separate ventilation shaft can not be provided and fans have to be installed on operating shaft they are connected to the shaft by well designed



If shaft is only for ventilation purpose then we do not use fan drift. If shaft is for ventilation & transfer of men & mat. purpose then fan drift is used



This type of mounting of fan is being done only in metal mine not in coal mines. As coal mines are prone to explosion if there is an explosion then explosion pressure will rise and will damage the fan.

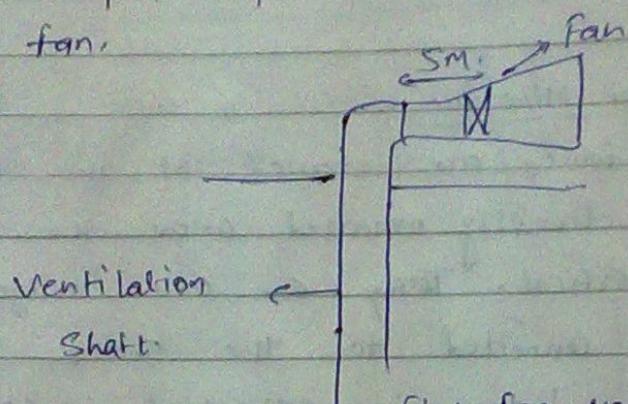
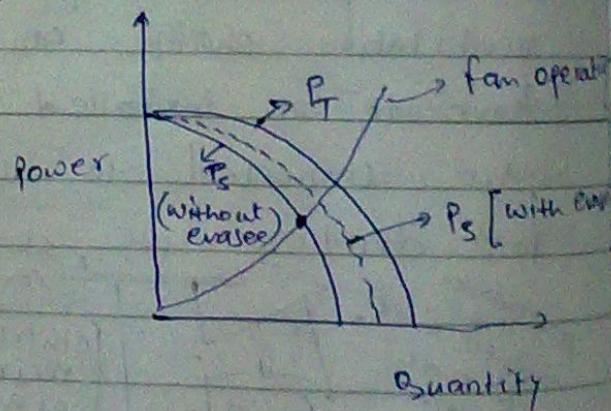


Fig: Fan mounting in ventilation shaft in coal mines.

Note: Use of Evasee



Normally the drive of the fan, instrument & control devices are housed in a rain proof dust proofed & fire proofed building provided locking arrangement, lightning arrestor.

shaft.

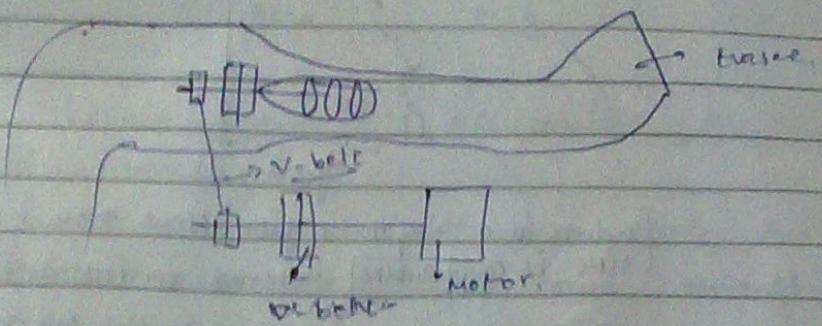
is being done only
in coal mines.
It is an explosion
risk and will damage
the equipment.

ounting in ventilation
in coal mines.

fan operating
Ps [with draft]
Quantity

instrument &
in a rain proof
protected building
& lightning

The top of the base is an exhaust fan
& the fan inlet in a forcing fan are
covered by a protective wire netting.



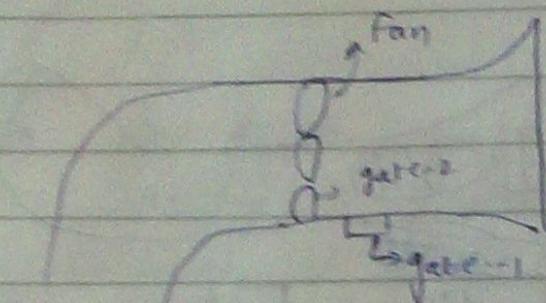
Surface vs Underground Installation ->

Main fans at collieries are req. by law than
it has to install fans at surface. So that they
are readily accessible in the event of flood,
fires or explosives. They are easier & cheaper to install
and maintain. Besides it may be difficult to
find a suitable U/g site for a main
fan. U/g fans can not be installed
until the workings are ready to
receive them. They are usually
of axial flow type owing to the restriction
of space and hence are of limited
head. Another disadvantage with U/g fan
is they usually require air locked on
Main level which becomes a constant source
of leakage and recirculation. On the other
hand U/g fans avoid leakage at surface

21/10/

air locks and shaft collars, leakage at surface air locks can amount to 10-20%.

Quantity circulated by fans.



[2 doors at a time if 1 gate opens another gate closed automatically]

Upf fans are commonly used in Metal Mines, where separate fans for diff. levels may be chosen for a more flexible control of ventilation. Also where all the openings are req. for active operation, it may be better practice to install fans upf, rather than that has air locks at the top of the shafts.

Leakage amount to 10-20%.

opens another gate
automatically.
Metal Mines.
H. levels may
More flexible
where all
active
ter practice to
than that have
the shafts.

Priority

Methane Layering \rightarrow expressed specific gravity of gas \rightarrow in terms of Air density

$$\text{Air density} = 1.2 \text{ m}^3/\text{kg}$$

$$\text{Sp. gravity} = 0.56$$

Methane tend to accumulate at the roof & forms layer.

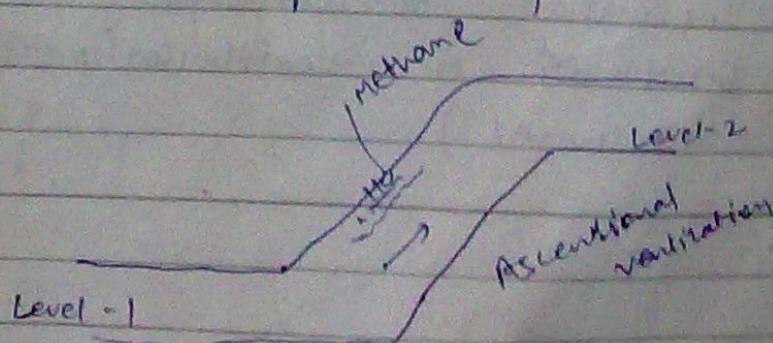
- Ascensional ventilation \rightarrow fresh air from lower level to upper level through a drift.
- Descensional ventilation \rightarrow fresh air from upper level to lower level.

Normally ~~metak~~ Methane emitted mixed with Air by diffusion.

- Any Accumulation of methane in the roof where conc. of methane is more than 5.4% is called methane layer, & Minimum length of the methane accumulation should be more or equal to the width of the roadway.



#



Less relative vel. \rightarrow less turbulent mixing.

for a long
time technique to
hazard.

$$\text{Methane layer } 'L' = \frac{V}{(4.37 \nu_w)^{1/2}}$$

L = Methane layer no.

It will suggest that whether there will be
formation of Methane layer or not.

ventilation

dir. [Methane
bulent mixing
layer ext

* For a Horizontal road way -

$$L \leq$$

Buoyancy dominates, Pronounced
methane layering.

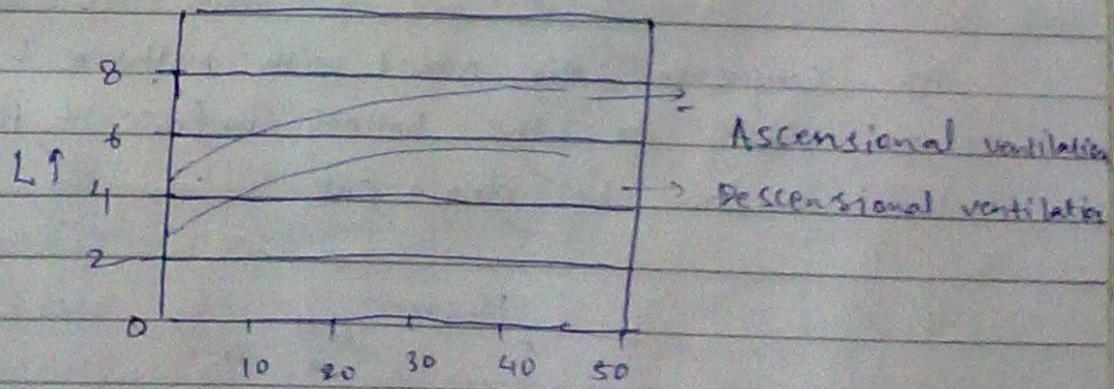
$$L > 2$$

No turbulent mixing

$$> 10$$

No layering / rapid mixing

* If Roadways are inclined -



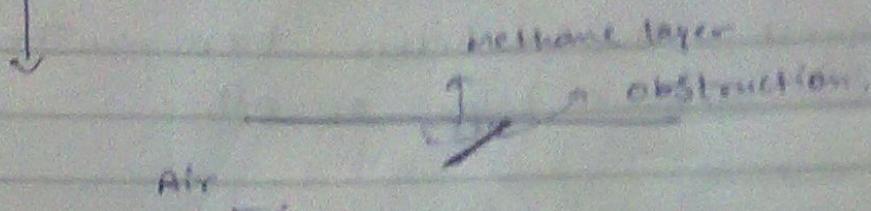
Roadway inclination, deg. →

→ Turbulent Mixing is starting around '2' for both ascendental
ventilation & there is no methane layering
beyond '6'.

→ .

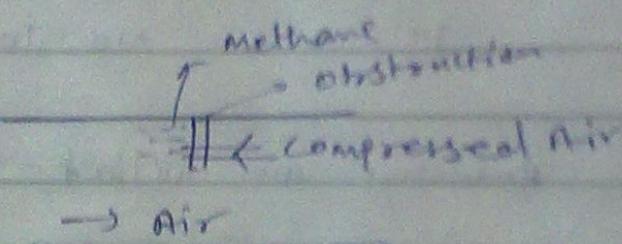
II Dispersal of methane layer

- ① Mixing lattice
- ② compressed air ejection



Due to obstruction eddy current generated turbulent mixing started. However resistance to air flow increased.

Compressed air →



② Compressed Air mixed with methane & comes down to the bottom surface & thus Methane can be drain out.

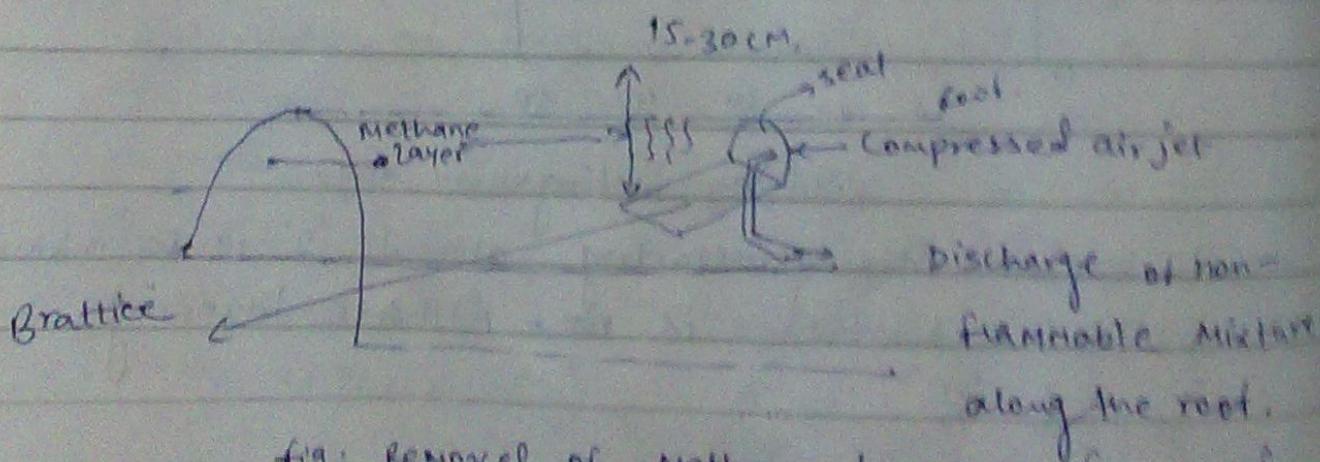


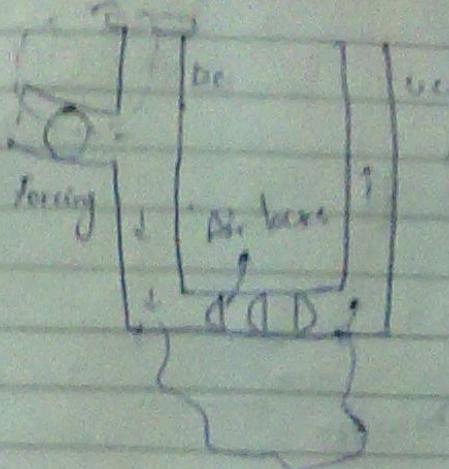
fig: Removal of Methane layer and from root by compressed Air ejection

Slips

Leakage

Air Circulation

H



current generated &
water resistance

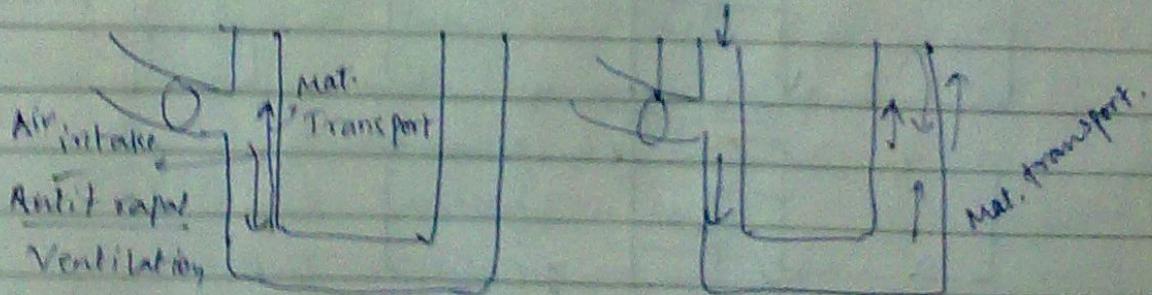
air

methane &
face & thus

ed air jet

range of non-
combustible mixture
ing the roof.
from roof

- Generally material is transported through ~~the~~ the + face. A lot of Air circulation / ~~the~~ leakage takes place.
- In IP we transport material through U.C. then we have to ~~be~~ open or close air locks again & again & the air ~~will~~ won't go to the face.
- Forcing types of fans are used in metal mines.
- Exhaust types of fans are used in coal mines.
- If forcing type of fans are used then face ~~at~~ at the face there will be accumulation of methane ~~for~~ instance

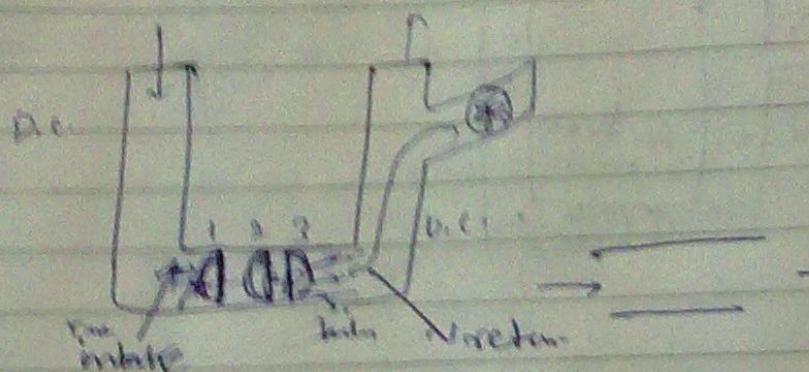


- In Antitrapal ventilation a lot of dust generated while in Mettrapal ventilation dust generated is less in comparison to Antitrapal.
- So generally Mettrapal is preferred.

Air Crossing

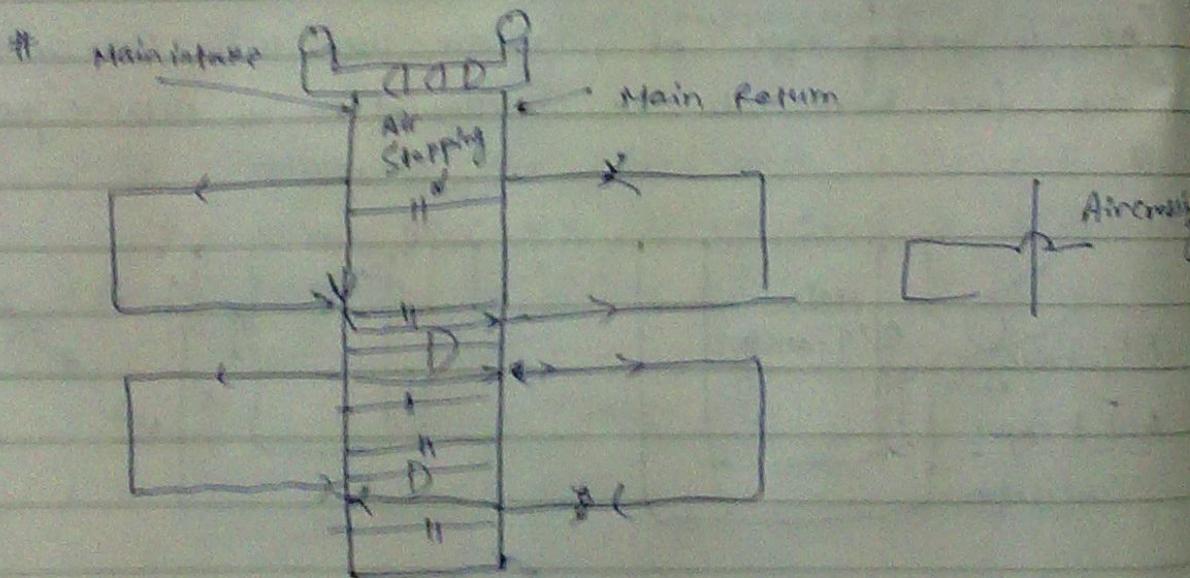
Booster fan:

Main \rightarrow DDD \rightarrow Return



\rightarrow 3 doors are provided. As if there is 1 door then due to high pressure diff at 2 sides of the doors it will be difficult to open the door.

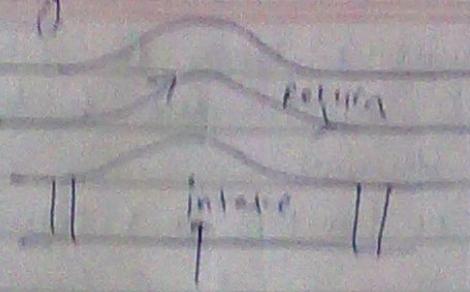
2nd door is provided only for air if there is air reversal takes place.



\rightarrow Main intake & Main return roadway are also known as trunk airway.
Air crossing

100% air flow

Air crossing



Regulator



Main controlling devices

- (A) Air locks
- (B) Air crossing
- (C) Slipping gates
- (D) Regulators



if O_2 is less than the amount which is needed

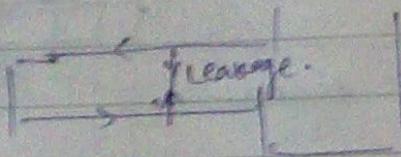
then there are some alternatives to increase O_2 :

- (A) By increasing power of the main fan
- (B) By putting regulator in path I. But by putting regulator there will be a lot of energy consumption.
- (C) Roaster fan. → Generation in coal mines is not recommended. [Due to gassing nature]
In metal mines also it is not recommended, nothing ventilation & there may be a possibility of explosion.

in roadway air

8/11/2011

- Also after installation of booster fan pressure drop across 'I' & 'O' also decreases. & hence quantity in path I decreased.
- After installation of booster start leakage also increases.



Critical pressure - pressure of the booster fan at which quantity flow in other split (ventilation dist.) become zero. That pressure of booster fan is known as critical pressure.

- Booster fan is generally installed in the return airway of the panel. [Because in entry airway it will hinder the transportation]
- Even ~~in~~ ^{selected} installation of booster fan in return airway booster fan is installed at neutral point in the airway. neutral point is chosen in such a way that there ^{should be} ~~be~~ least leakage

Ex-1 Two parallel split A & B have a pressure of 300 pa acting across them carrying a flow $15 \text{ m}^3/\text{s}$ in split 'B' & $10 \text{ m}^3/\text{s}$ in split 'A'. It is desired to reduce the quantity in split 'A' to $10 \text{ m}^3/\text{s}$ by

Ex. 2 A
 300 Pa
 $25 \text{ m}^3/\text{s}$
 consist
 $15 \text{ m}^3/\text{s}$
 +
 $15 \text{ m}^3/\text{s}$
 Calculate
 resistance
 is 0.2

$$R_A = R_B$$

$$\Rightarrow R_B =$$

$$R_T$$

$$P_B$$

$$Q_B$$

$$Q_A$$

$$Q_T$$

$$Q_B$$

$$Q_A$$

$$Q_T$$

$$Q_B$$

$$Q_A$$

$$Q_T$$

$$Q_B$$

$$Q_A$$

$$Q_T$$

Before installation of booster fan

$$S_{00} = R_T \times 25^2 + R_A \times 15^2 + R_B \times 10^2$$

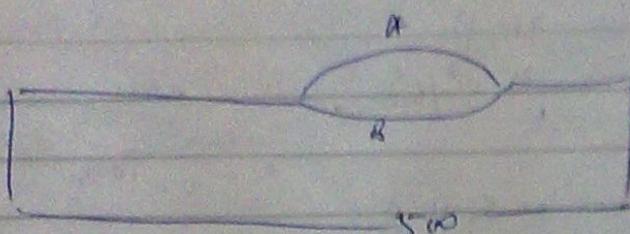
$$R_A = 1.67$$

$$R_B = 2 \times 7$$

After installation
of booster fan

After installation of booster fan.

[After installation of booster fan not only quantity in A increases but also total quantity flowing through system increases]



$$S_{00} = R_T B_T^2 + R_A (B_T - B_B)^2 + R_B B_B^2$$

$$= 0.2 B_T^2 + 1.67 (B_T - 15)^2 + 3.57 \times 15^2$$

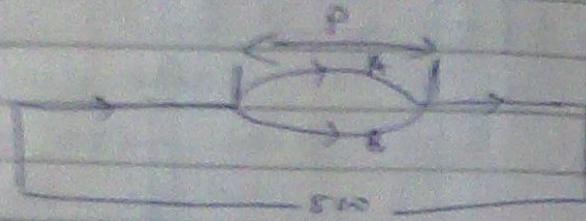
$$B_T = 29 \text{ m}^3/\text{s}$$

Now Considering flow in split B

$$S_{00} + P_B = R_B B_B^2 + R_T B_T^2$$
$$= 3.57 \times 15^2 + 0.2 \times 29^2$$

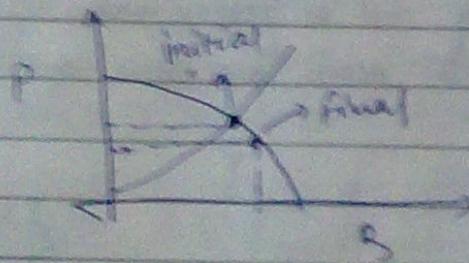
$$P_B = \underline{\underline{512 \text{ Pa}}}/\text{Area}$$

→ After installation of booster fan quantity across ducts + share decreased.

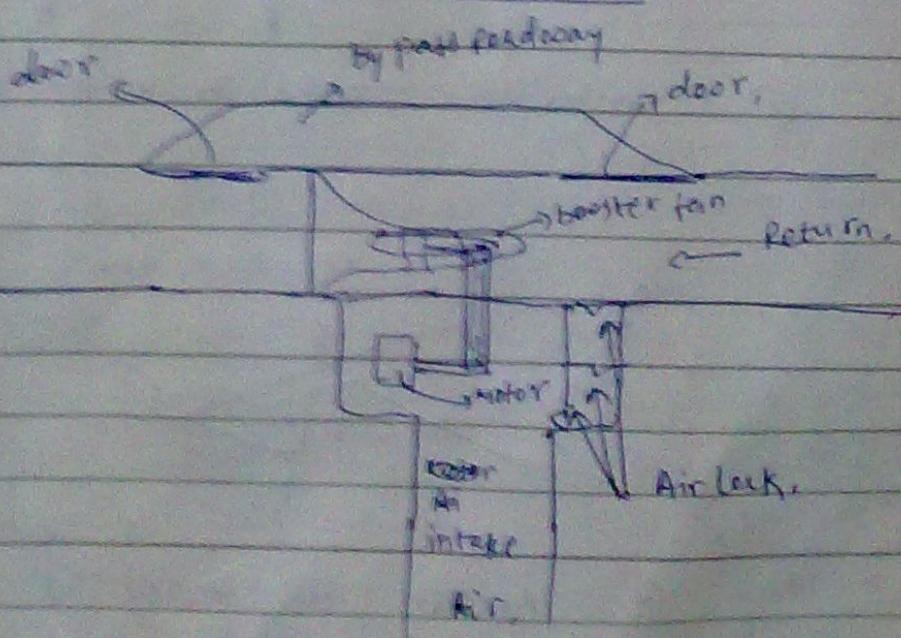


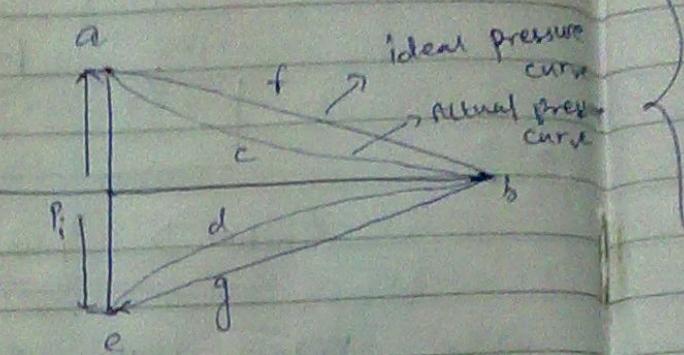
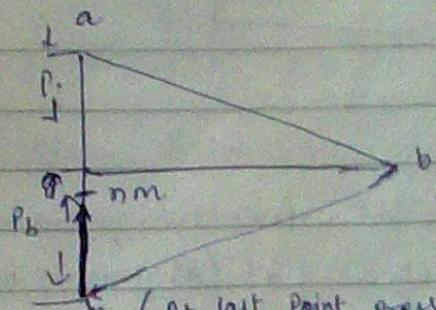
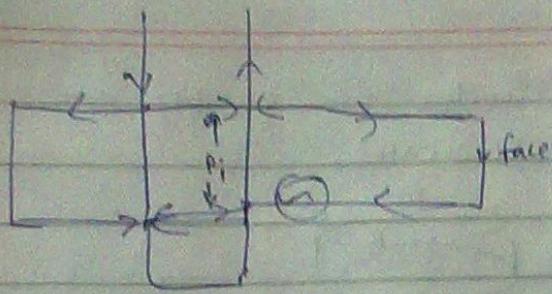
Initial \rightarrow Final

→ After installation of booster fan; main fan characteristics also changes (As quantity increased). In Solving above question we have assumed that fan operating characteristics is same.



Installation of Booster fan -



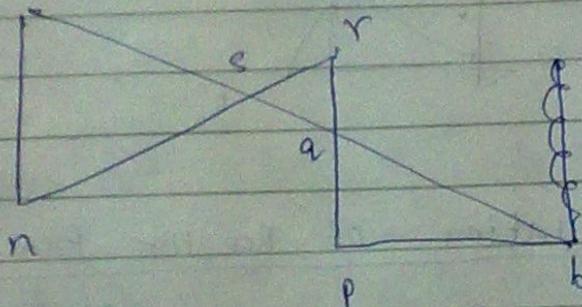


a) Before installing booster fan.

- (a) After installation of booster fan at outby end of return road

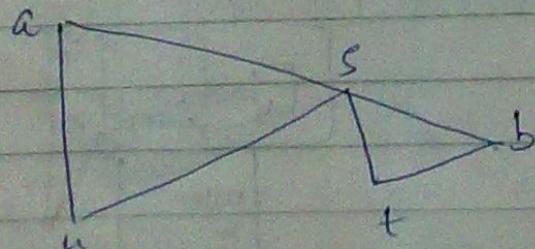
P_j = Pressure diff. Across the split due to main fan.

P_b = " " " " " " " Booster fan.



Case b

- (b) Booster fan located in return road near the face

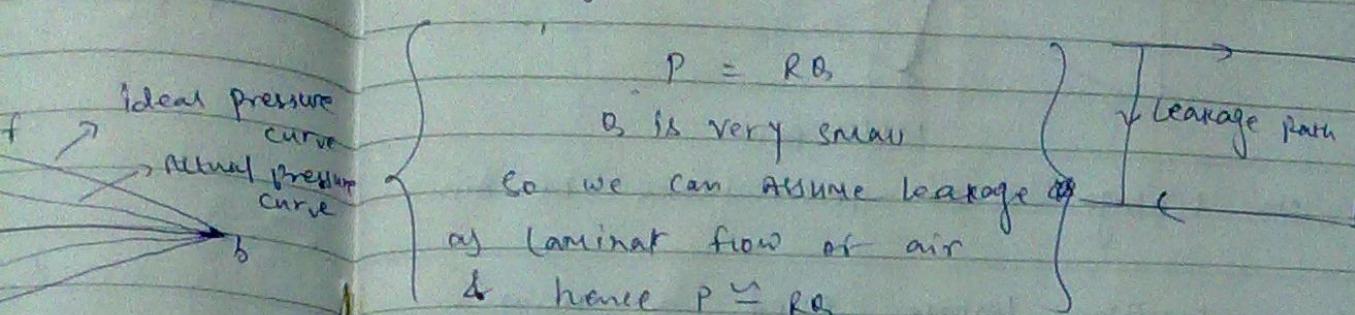


Case c

- (d) Booster fan located at neutral point

\rightarrow Leakage which

Leakage quantity $\propto \alpha, p$



$$B = RB$$

B is very small

so we can assume leakage \propto

as laminar flow of air

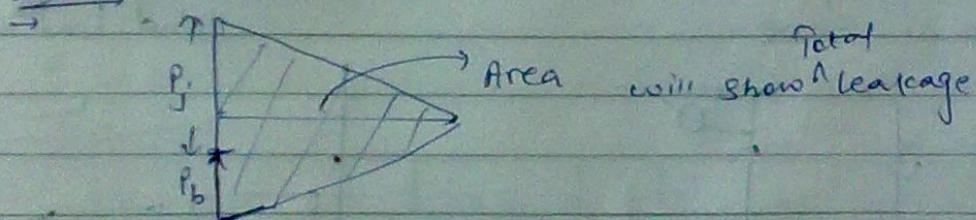
& hence $p \approx RB$

$$\Rightarrow B = P/R$$

$R \propto$ length $/L$ for leakage path.

[As length increases leakage path increases
& More parallel leakage \Rightarrow path generated
hence total resistance decreases]

case B $B \propto P_r L$

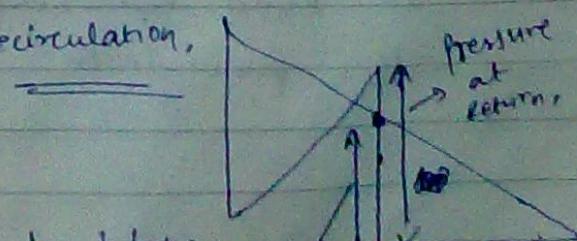
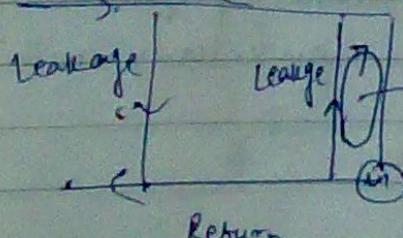


Case C

As near face pressure will be high

so there may be recirculation of Air,

intake



\Rightarrow Leakage from return to intake
which is dangerous.

neutral point

15/11/2011

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Ve

Page 9



Neutral Point

No leakage & no recirculation of air.

Line

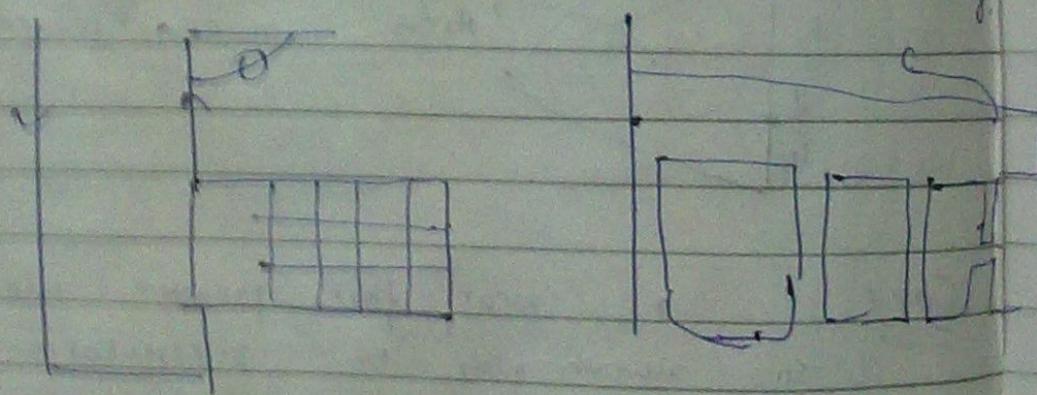
Maximum possible leakage saved by using a booster is half the total leakage when the booster position is at halfway in the return. Also the pressure of booster is same as that due to main fan.

For other booster pressure however the position of the neutral point as well as the amount of leakage saved will vary.

stoppin

II Auxiliary Ventilation :-

Blind heading

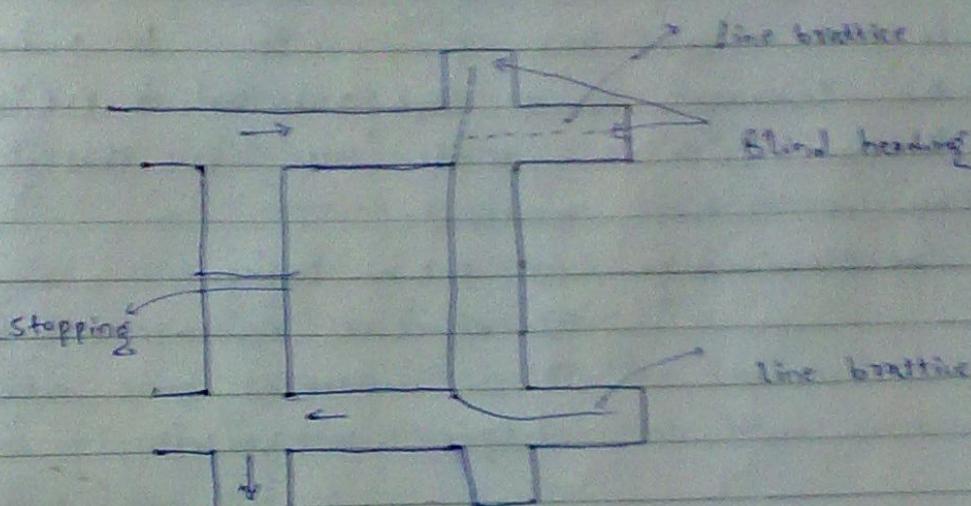


To create proper ventilation at Blind end heading auxiliary ventilation is provided.

15/11/2018

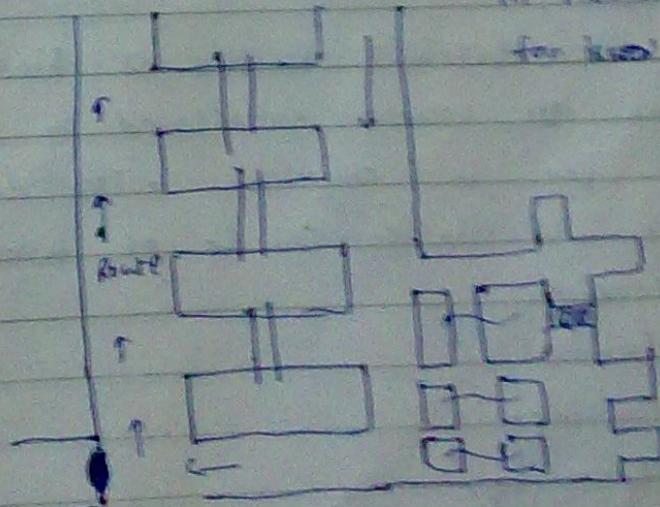
Bananta

Ventilation at a heading (Auxiliary ventilation)



Blind heading

Brattice is mainly used
in coal mines while
in metal mine Ausiliar
fan has used.



over ventilation
under ventilation,

Screen or curtain

of hessian cloth.

to heading.

This is just pasting

Cloth.

at 15m interval

air is not more than 20m.

Lattice cloth is that

so to reduce

brisied & PVC coated

& PVC coated hessian

package

resistance increases

and mine effective

be lost.

an auxiliary fan

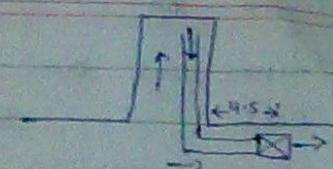
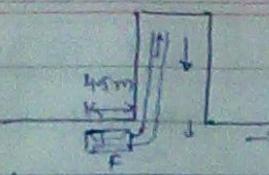
headings & drifts

by means of

its ducting.

following types-

→ Generally we place at 4.5 m from the heading gauge to prevent recirculation of air.



Forcing fan

Exhausting fan

[Preferably $\frac{1}{2}$ to $\frac{1}{3}$ of air should be circulated to the heading by the fan.]

→ Fans

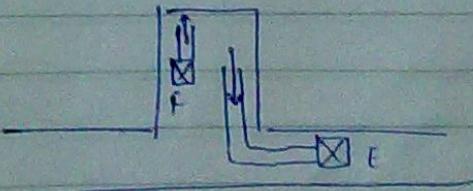
Advantages of forcing fans -

- ① It delivers ^{fresh} dry air at the face.
- ② In forcing system air travels to the face at higher velocity.
- ③ In forcing system, air directly impinges to the body. therefore it is more comfortable in heat and humid conditions.
- ④ In forcing systems the fan and motor is placed at face fresh intake air hence corrosion to the fan and Motor is less.

Advantages of Exhaust System -

- ① Clearance of dust, fumes, and gases are very effective in exhaust system.

Overlapping fans :

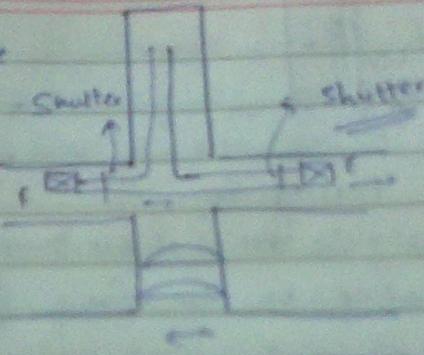


Reversible System

At a time only one fan for A/C.

If we have to use two fans then we

Put shutter before the exhaust fan and vice versa.



Flexible and rigid duct [Page no. 629] -
duct for auxiliary fans.

$$H = AQ^2 + BQ + C$$

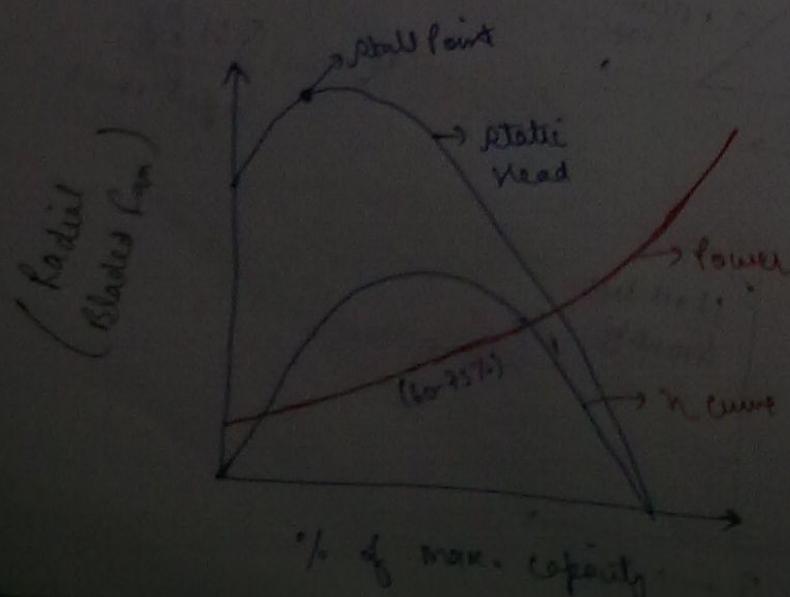
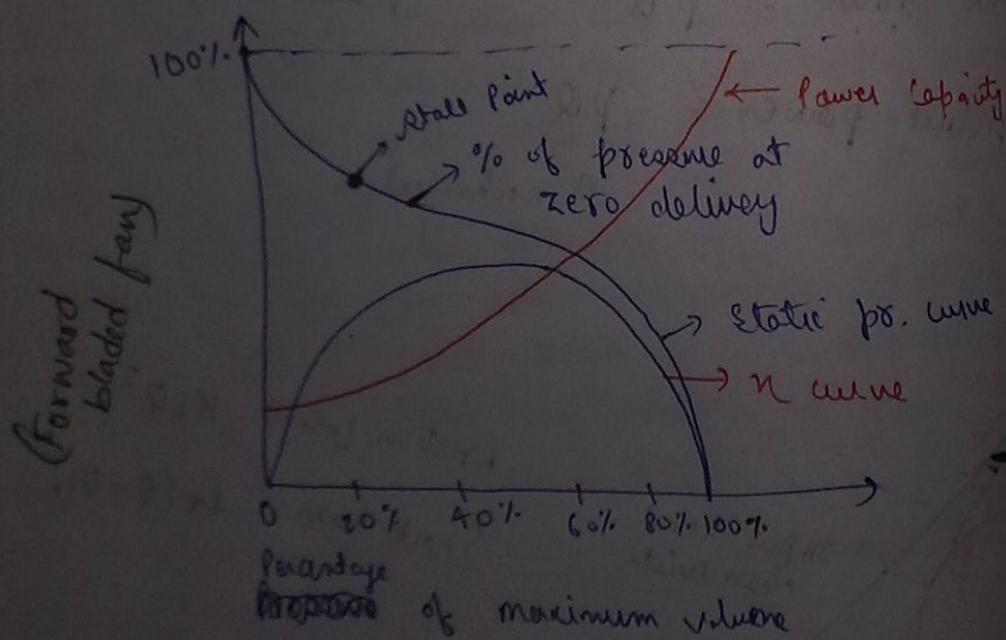
Fan Characteristics

① Head - Capacity Characteristic
(H) (Q)

② Power - Capacity
(P)

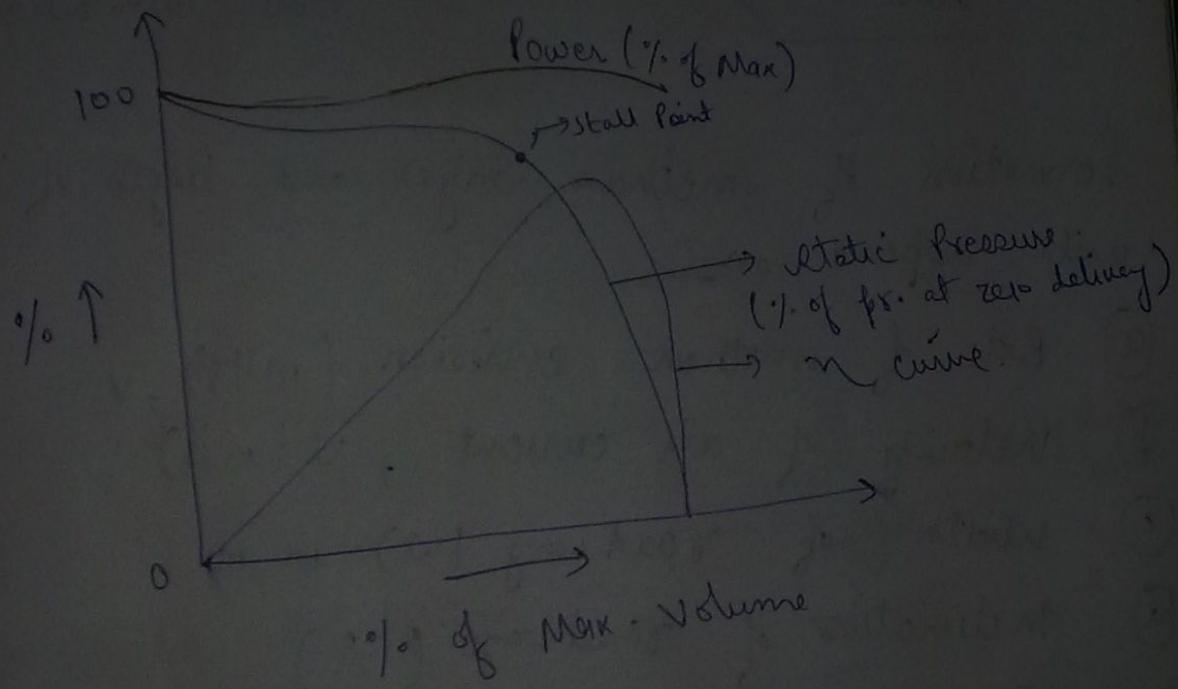
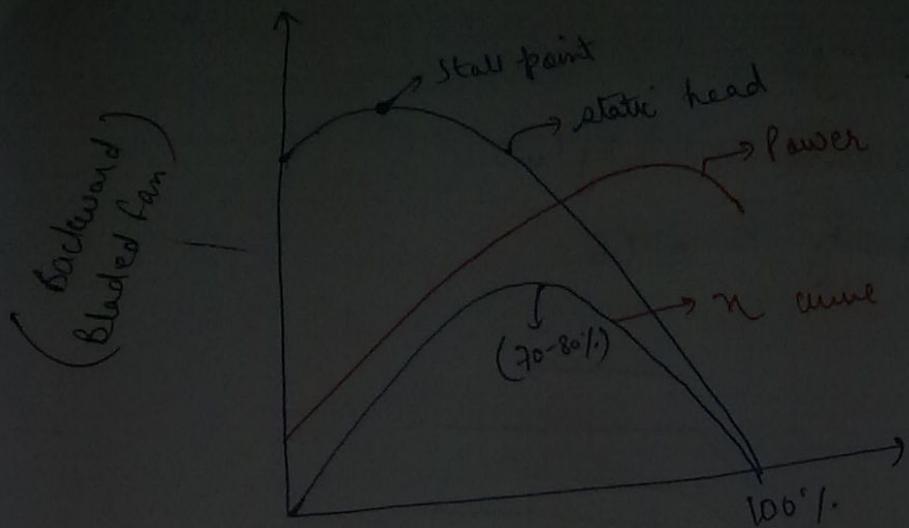
③ Efficiency (n) - Capacity (Q)

(backward bladed fan)
(Bladed Fan)



or fan needed
to be run after
stall point for
smooth functioning
and seal tight

- ① Selection of fan
- ② Combination



Characteristics of Axial flow fans

- ① Selection of Mine fan (9 points)
- ② Combination of fans