

熱力学 4回目

[1] (1) オットーサイクル

(2) $2 \rightarrow 3$: 定容変化 $\therefore dV = 0$

$$dq = du + pdv \quad \therefore \quad dq = du = mC_v dT$$

$$\text{吸熱: } Q_{23} = U_3 - U_2 = mC_v(T_3 - T_2)$$

 $4 \rightarrow 1$: 定容変化 $\therefore dV = 0$

$$dq = du + pdv \quad \therefore \quad dq = du = mC_v dT$$

$$\text{放熱: } Q_{41} = -mC_v(T_1 - T_4) = mC_v(T_4 - T_1)$$

 $1 \rightarrow 2$: 断熱変化 $\therefore dq = 0$

$$T_1 V_1^{K-1} = T_2 V_2^{K-1}$$

$$\therefore T_2 = \varepsilon^{K-1} T_1$$

 $2 \rightarrow 3$: $dV = 0$

$$T_2/p_2 = T_3/p_3 \rightarrow T_3 = \frac{p_3}{p_2} T_2 = \frac{p_3}{p_2} \varepsilon^{K-1} T_1$$

 $3 \rightarrow 4$: $dq = 0$

$$T_3 V_3^{K-1} = T_4 V_4^{K-1}$$

$$T_4 = \left(\frac{V_3}{V_4}\right)^{K-1} T_3 = \left(\frac{V_2}{V_1}\right)^{K-1} \frac{p_3}{p_2} \varepsilon^{K-1} T_1 = \left(\frac{1}{\varepsilon}\right)^{K-1} \frac{p_3}{p_2} \varepsilon^{K-1} T_1 = \frac{p_3}{p_2} T_1$$

$$\eta = \frac{W}{Q} = \frac{Q_{23} - Q_{41}}{Q_{23}} = 1 - \frac{Q_{41}}{Q_{23}} = 1 - \frac{mC_v(T_4 - T_1)}{mC_v(T_3 - T_2)} = 1 - \frac{T_4 - T_1}{T_3 - T_2}$$

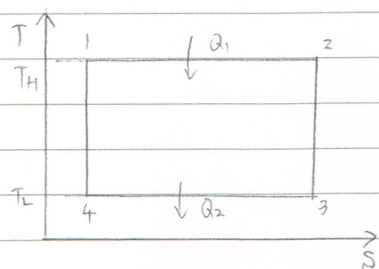
$$= 1 - \frac{\frac{p_3}{p_2} T_1 - T_1}{\frac{p_3}{p_2} \varepsilon^{K-1} T_1 - \varepsilon^{K-1} T_1} = 1 - \frac{\frac{p_3}{p_2} - 1}{\varepsilon^{K-1} \left(\frac{p_3}{p_2} - 1\right)} = \boxed{1 - \frac{1}{\varepsilon^{K-1}}}$$

(3) 圧縮比を大きくする

、比熱比を大きくする

、ポンプ損失を少なくする

[2] (1)

左図より, $ds = T ds$ を用いると,

$$Q_1 = T_H (S_2 - S_1)$$

$$Q_2 = T_L (S_3 - S_4)$$

$$S_1 = S_4, S_2 = S_3 \text{ より,}$$

$$Q_2 = T_L (S_2 - S_1)$$

$$\therefore \eta = \frac{W}{Q} = \frac{Q_1 - Q_2}{Q_1} = 1 - \frac{Q_2}{Q_1} = \boxed{1 - \frac{T_L}{T_H}}$$

(2) 最高温度から T_L のときの熱効率を,

$$\eta' = 1 - \frac{T_L}{T_1} \quad \text{--- ①}$$

$$Q = K(T_H - T_1) \text{ より, } T_1 = T_H - Q/K$$

①に代入

$$\therefore \eta' = 1 - \frac{T_L}{T_H - \frac{Q}{K}} = \boxed{1 - \frac{KT_L}{KT_H - Q}}$$

$$Q_a = \eta' Q = \boxed{\left(1 - \frac{KT_L}{KT_H - Q}\right) Q}$$

(3) 不可逆変化によりエントロピーが最大となると、有効エネルギーが0, 無効エネルギーが Q となるので,

$$Q_a = \left(1 - \frac{KT_L}{KT_H - Q}\right) Q = 0$$

$$1 - \frac{KT_L}{KT_H - Q} = 0 \rightarrow KT_H - Q = KT_L \rightarrow \therefore Q = \boxed{K(T_H - T_L)}$$

[3] (1) 沸点 = $T_R = 151.84(^{\circ}\text{C})$

$$(2) Q = h'' - h' = 2107.4 \text{ (kJ/kg)}$$

$$(3) h = h' + x(h'' - h') = 640.115 + 0.4 \cdot 2107.4 = 1483.075 \approx \boxed{1483.1 \text{ (kJ/kg)}}$$

$$(4) T_R = 179.88(^{\circ}\text{C}) < 200(^{\circ}\text{C}) \text{ より, 過熱蒸気}$$

$$(5) Q = 3052.1 - 419.7 = \boxed{2632.4 \text{ (kJ/kg)}}$$