

# Material Balance

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# Content

- Material-balance (MB) concept
- Drive Mechanisms
- MB for gas reservoirs
- MB for oil reservoirs

Refs: Applied Petroleum-Reservoir Engineering, Craft & Hawkins  
Fundamentals of Reservoir Engineering, Dake  
Lecture notes of Wim Swinkels  
Lecture notes of Willem Schulte

# Material-Balance Concept

- Since reservoir volume is constant, the sum of volume changes (including production and injection) of the oil, free gas, and water must equal zero
- In other words, expansion should be equal to voidage:
  - the net voidage (production minus injection minus influx) must be made up by expansion of the in-place materials
  - a volume balance which equates the cumulative observed production, expressed as an underground withdrawal, to the expansion of the fluids in the reservoir resulting from a finite pressure drop

# Material Balance

- Equations that link pressure to net withdrawals
- Constrained by conservation of mass
- Thus production balanced by
  - oil expansion
  - dissolved gas liberation
  - expansion of gas cap
  - expansion of connate water
  - water influx
  - compaction of pore volume
- Combined with dynamic processes provides basis for reservoir prediction

# Drive Mechanisms

- Fluid Expansion
  - Occurs as reservoir undergoes pressure depletion
- Solution Gas Drive
  - When reservoir pressure falls below bubble-point, gas is liberated from hydrocarbon liquid phase. Expansion of gas phase contributes to displacement of liquid phase.
- Water Drive
  - For reservoirs connected to natural aquifers, reservoir pressure declines, water starts to expand and flow into reservoir
- Gas-Cap Drive
  - Volume of free gas in upper part of structure expands into oil zone to displace oil downdip
- Compaction Drive
  - Pressure depletion generates an increase in effective pressure acting over rock. Depending on formation compressibility, this increase may induce a decrease in pore volume providing some energy
- MB applied to gain an understanding of reservoir-drive mechanisms under primary-recovery conditions

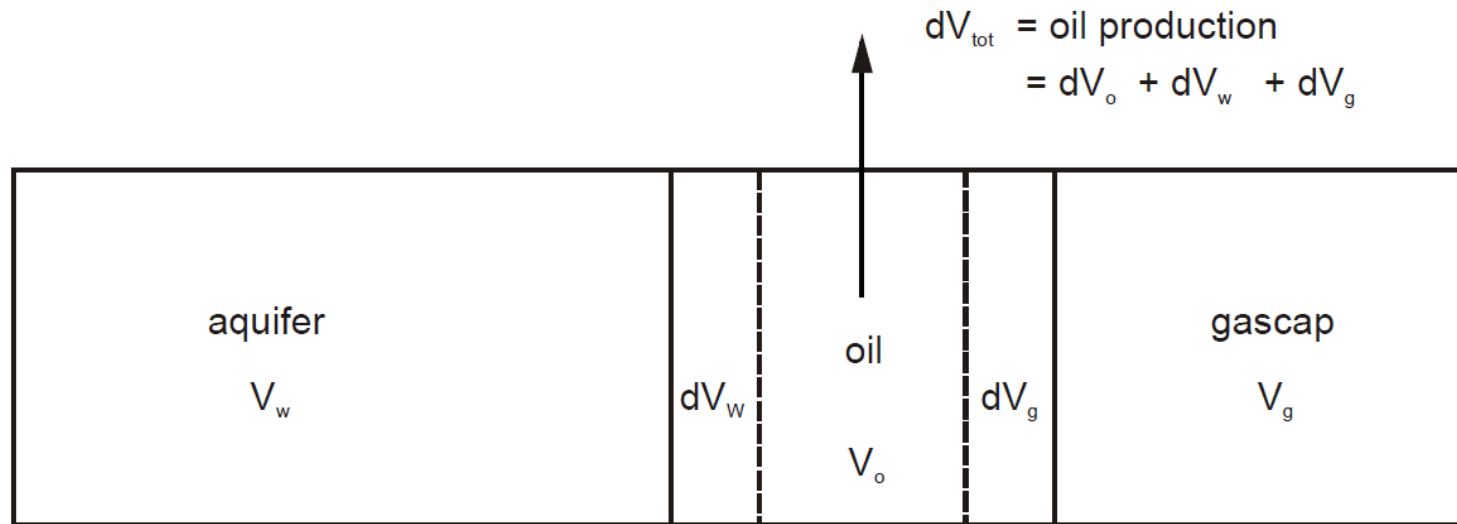
# Fluid and Rock Properties for Expansion

- Solution gas/oil ratio ( $R_s$ )
- Oil-formation-volume factor ( $B_o$ )
- Gas-formation-volume factor ( $B_g$ )
- Total-formation-volume factor ( $B_t$ )
- Formation compressibility ( $c_f$ )
- Water compressibility ( $c_w$ )

# Nomenclature-Definitions

- OIP/GIP: oil/free gas in place
- N/G: original OIP/GIP
- $N_p$ : cumulative oil production
- $G_p$ : cumulative gas production
- $W_p$ : cumulative water production
- $W_i$ : cumulative water influx/injection
- $G_i$ : cumulative gas injection
  - Note: All except for OIP/GIP are at standard conditions

# Primary Oil Recovery Resulting from Oil, Water, and Gas Expansion



$$dV_{tot} = \text{oil production} = dV_o + dV_w + dV_g$$

$$dV_{tot} = c_o V_o \Delta P + c_w V_w \Delta P + c_g V_g \Delta P$$

Typical values for compressibility factors at 2000 psia (138 bar):

$$c_o = 15 \times 10^{-6} \text{ 1/psi}, c_w = 3 \times 10^{-6} \text{ 1/psi}, c_g = 500 \times 10^{-6} \text{ 1/psi}$$

Contribution to oil production by oil and water expansion only significant if  $V_o$  and  $V_w$  are large. In contrast, because of its very high compressibility, relatively small volume of gas cap contributes significantly to oil production.



# Gas Reservoirs (Expansion Factor)

Calculates expansion factor by using  $z$

$$\text{Expansion factor: } E = \frac{V_{sc}}{V} = B_g$$

$$\text{Expansion factor: } E = \frac{V_{sc}}{V} = \frac{z_{sc} T_{sc} P}{z T P_{sc}} = a \frac{P}{z T}$$

for field units  $E = 35.37 P/zT$  (vol/vol)

Standard conditions:

$$T_{sc} = 16^\circ\text{C or } 60^\circ\text{F}$$

$$P_{sc} = 101 \text{ kPa or } 14.7 \text{ psi}$$

$$\text{Gas initially in place (GIIP): } G = V\phi(1 - S_{wc})E_i$$

# Gas Reservoir (Depletion, No Water Influx)

- Hydrocarbon pore volume:  $HCPV = V\phi(1 - S_{wc}) = G/E_i$

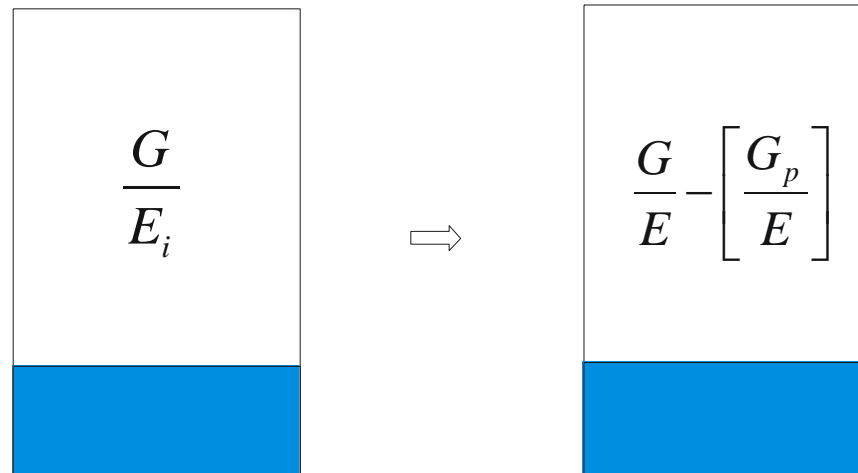
$$\text{Production (sc)} = \text{GIIP} - \text{Unproduced Gas (sc)}$$

$$G_p = G - (HCPV)E$$

$$G_p = G - \frac{G}{E_i} E$$

$$\frac{G_p}{G} = 1 - \frac{E}{E_i}$$

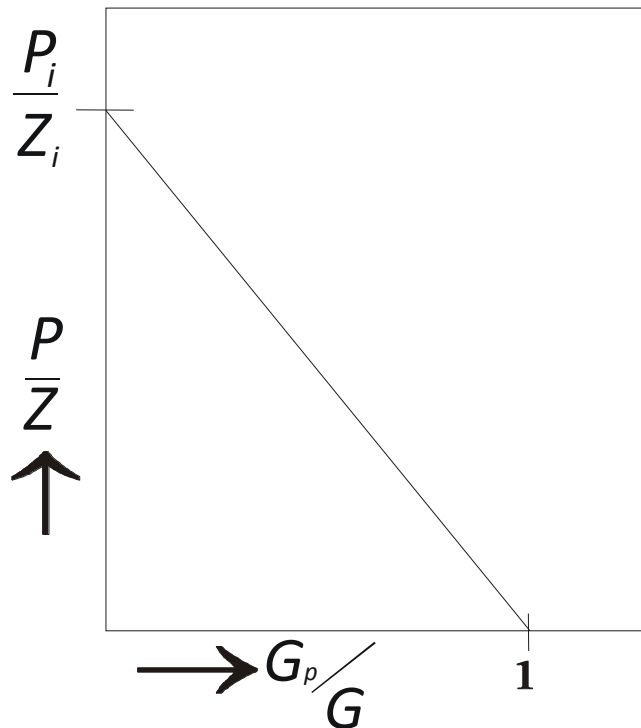
$$\frac{P}{z} = \frac{P_i}{z_i} \left( 1 - \frac{G_p}{G} \right)$$



# Gas Reservoirs

- Relation between production and pressure over time

$$\frac{P}{Z} = \frac{P_i}{Z_i} \left( 1 - \frac{G_p}{G} \right)$$



# Connate-Water Expansion and Grain-Pressure Increase

- Total change in hydrocarbon pore volume

$$d(\text{HCPV}) = -dV_w + dV_f$$

- Negative sign is because expansion of connate water leads to reduction in HCPV

$$d(\text{HCPV}) = -(c_w V_w + c_f V_f) \Delta P$$

$$V_f = PV = \frac{\text{HCPV}}{(1 - S_{wc})} = \frac{G}{E_i(1 - S_{wc})}$$

$$V_w = PV \times S_{wc} = \frac{GS_{wc}}{E_i(1 - S_{wc})}$$

$$\frac{G_p}{G} = 1 - \left( 1 - \frac{(c_w S_{wc} + c_f) \Delta P}{1 - S_{wc}} \right) \frac{E}{E_i}$$

# Gas Reservoirs

$$\frac{G_p}{G} = 1 - \left( 1 - \frac{(c_w S_{wc} + c_f) \Delta P}{1 - S_{wc}} \right) \frac{E}{E_i}$$

For typical reservoirs, reduction in hydrocarbon pore volume, due to connate water expansion and rock compaction, is negligible:

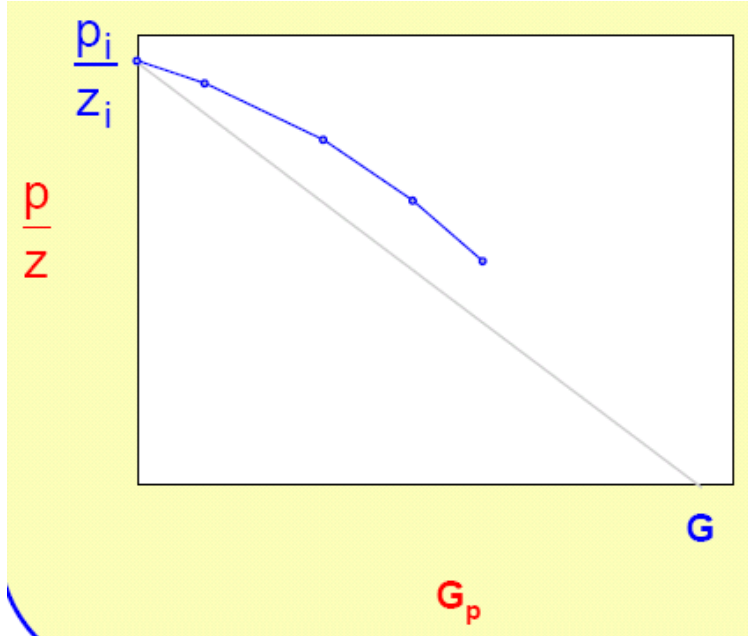
$c_w = 3 \times 10^{-6}$  1/psi,  $c_f = 10 \times 10^{-6}$  1/psi,  $S_{wc} = 0.2$ ,  $\Delta P = 1000$  psi, the term in parenthesis becomes:

$$1 - \frac{(3 \times 0.2 + 10)}{0.8} \times 10^{-6} \times 10^3 = 1 - 0.013$$

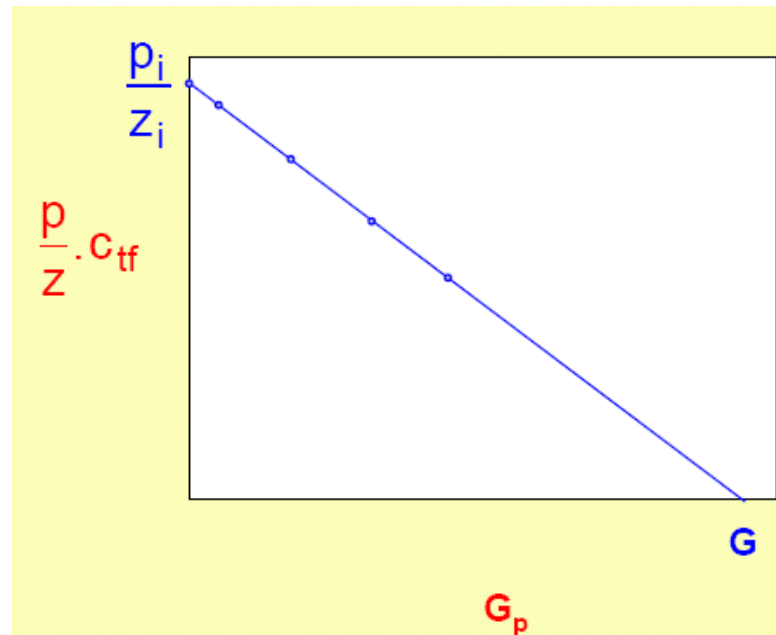
Not always, e.g., shallow unconsolidated reservoirs ( $c_f = 100 \times 10^{-6}$  1/psi)

# Compaction Drive

- Impact of compaction on P/Z plot

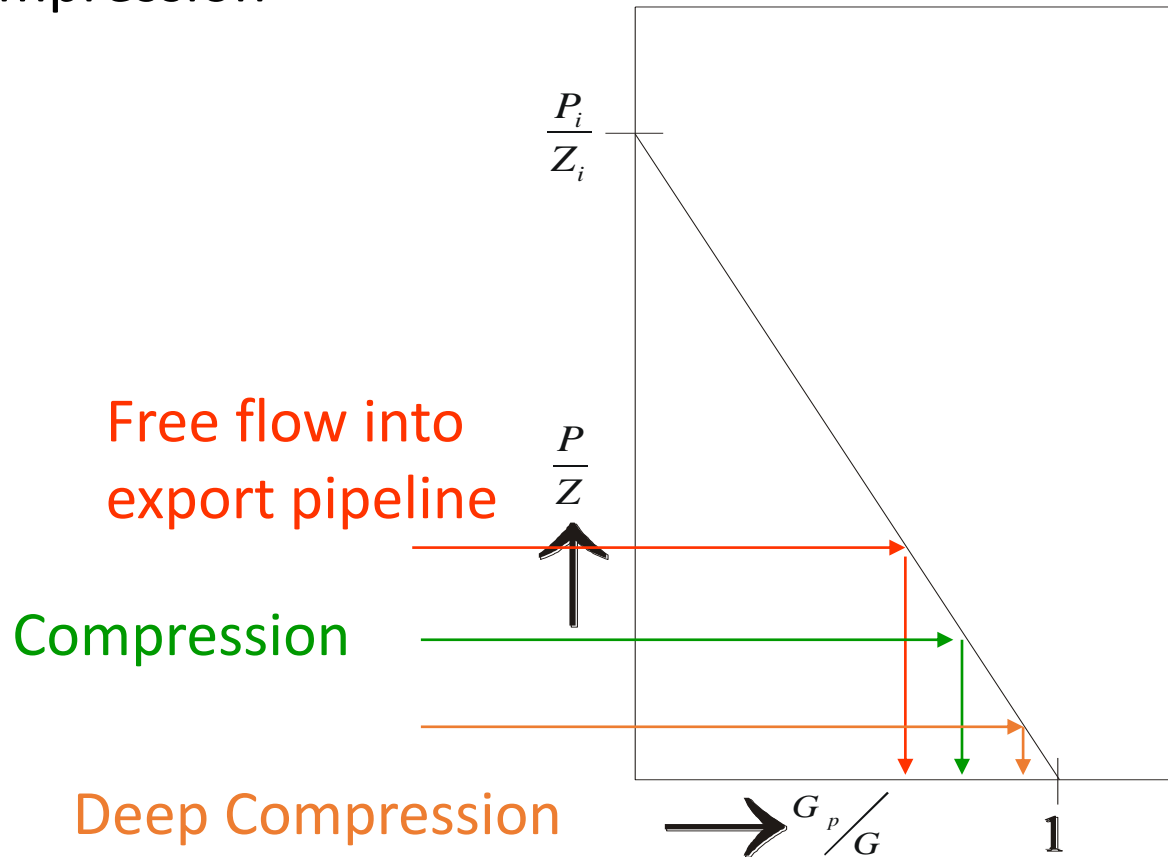


By including bracket term ( $c_{tf}$ ) in P/Z



# Groningen Gas Field

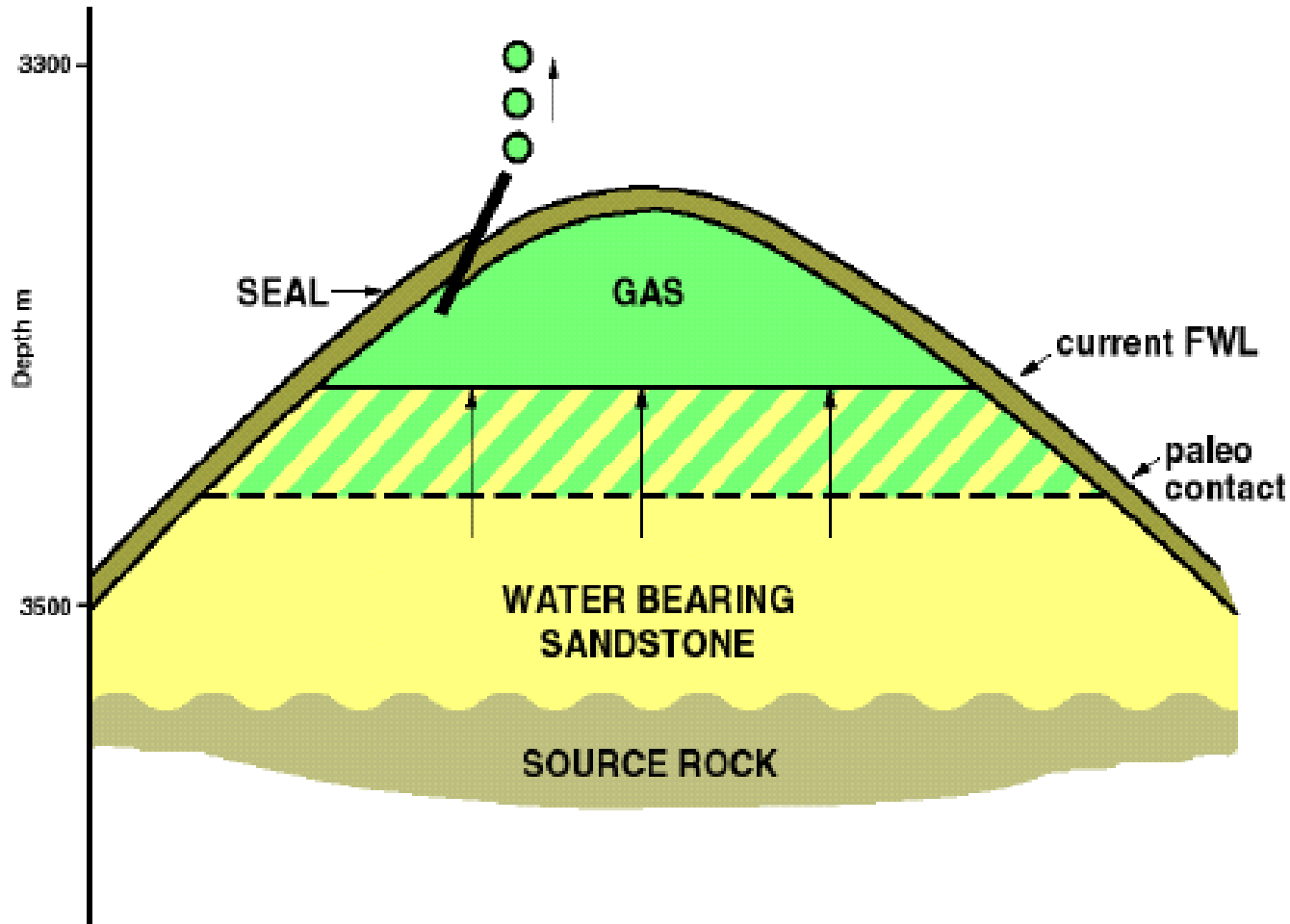
Improving recovery by lowering the abandonment pressure using compression



# Water Influx

## WATER REPLACING GAS IN PARTS OF RESERVOIR

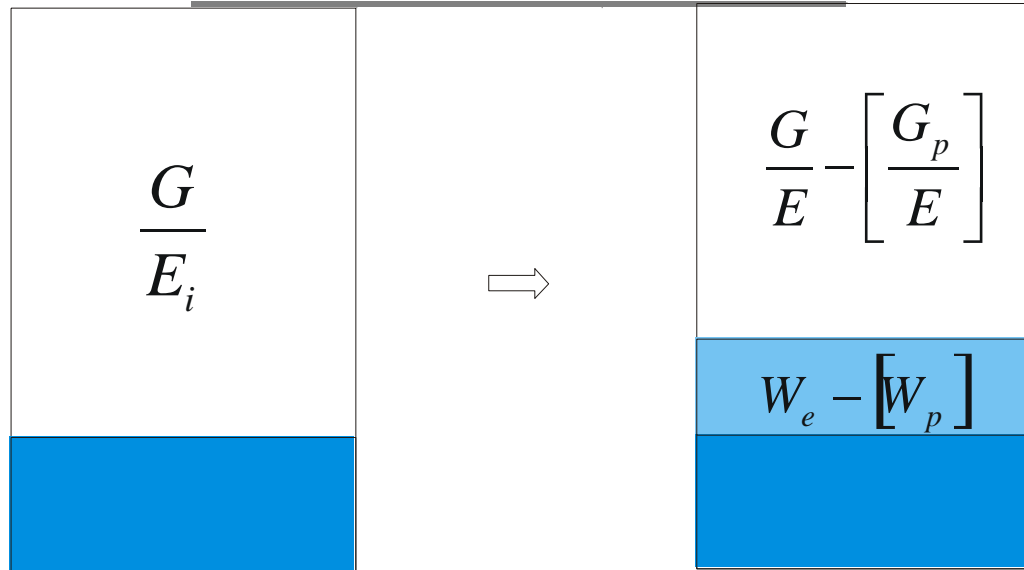
(Water imbibing in reservoir → imbibition)





# Gas Reservoir with Water Influx

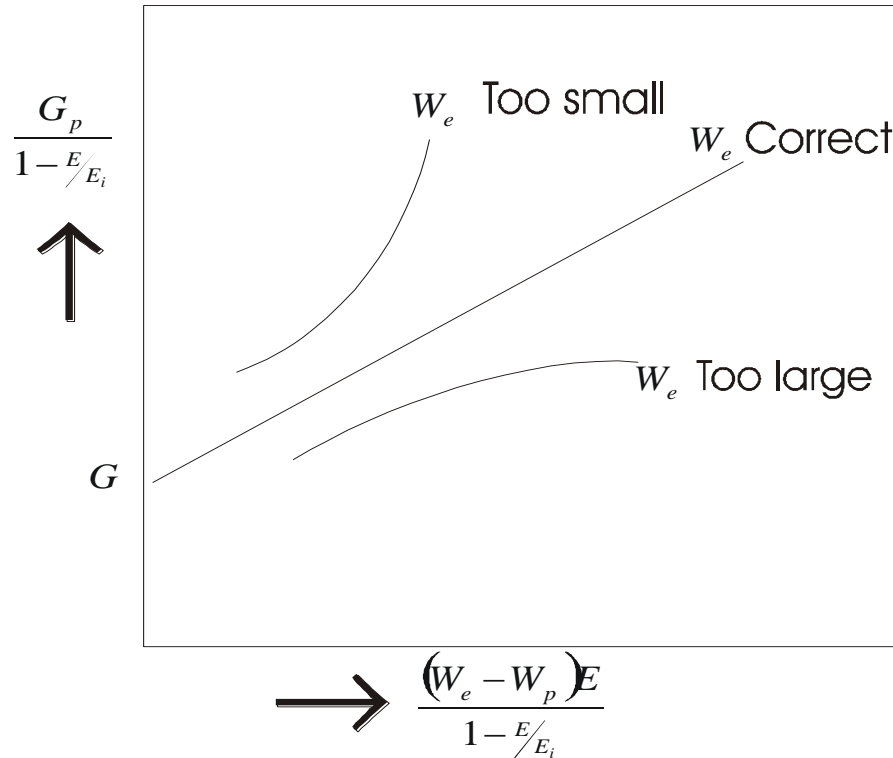
	Standard Conditions	Reservoir Conditions
Gas	$G_p$	$\frac{G_p}{E}$
Oil	—	—
Water	$W_p$	$W_p$



$$\frac{G}{E_i} = \frac{G - G_p}{E} + W_e - W_p$$

# Gas Reservoir with Water Influx

- Linear plot 
$$\frac{G_p}{1 - E/E_i} = G + \frac{(W_e - W_p)E}{1 - E/E_i}$$

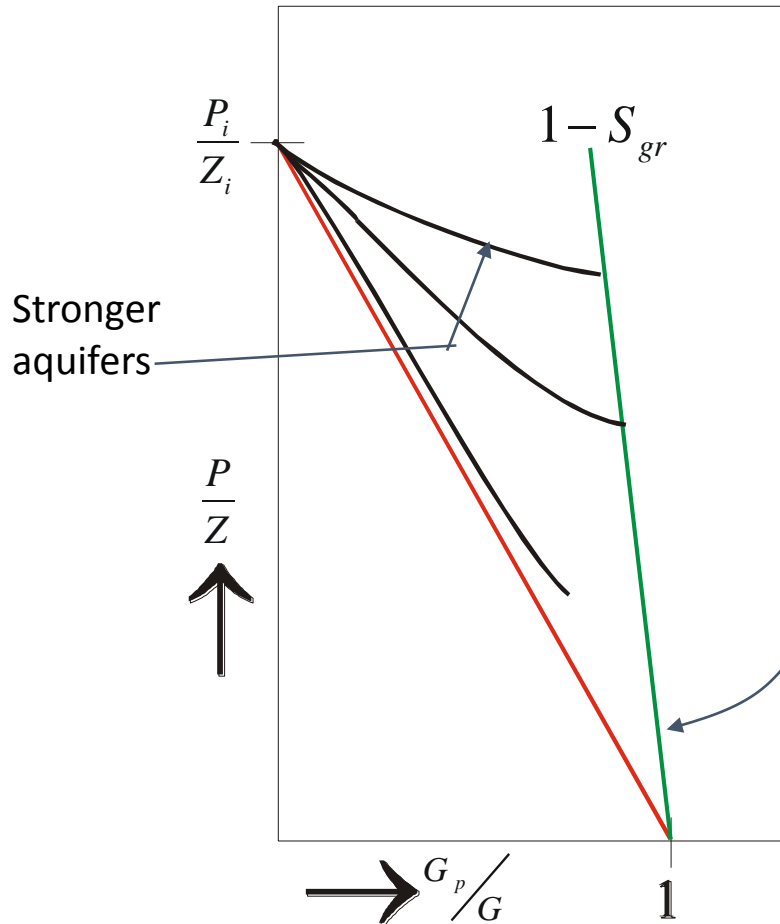


Note that you may have inaccuracy in  $G$  and  $W_e$   
 Note: linearity is independent of uncertainty in  $G$

# Gas Reservoir with Water Influx

- Rewrite MBE:

$$\frac{P}{Z} = \frac{\frac{P_i}{Z_i} \left( 1 - \frac{G_p}{G} \right)}{\left( 1 - \frac{E_i}{G} (W_e - W_p) \right)}$$



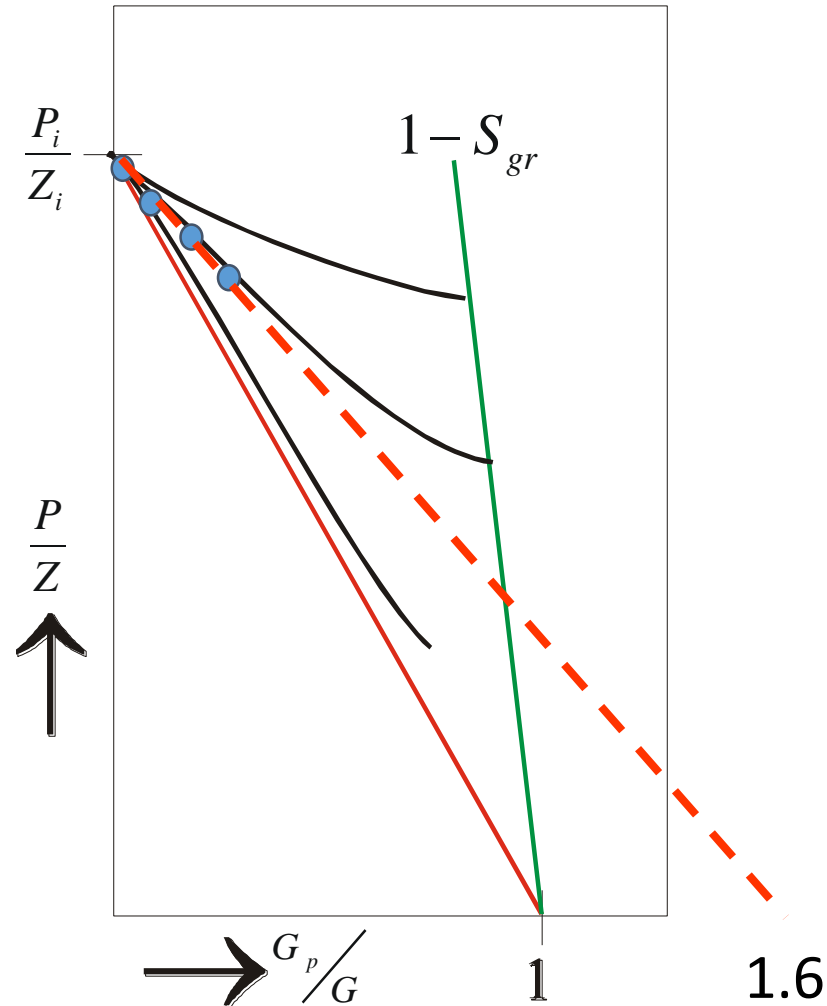
The aquifer influx does not allow a large pressure drop

ultimate possible under an effective waterdrive

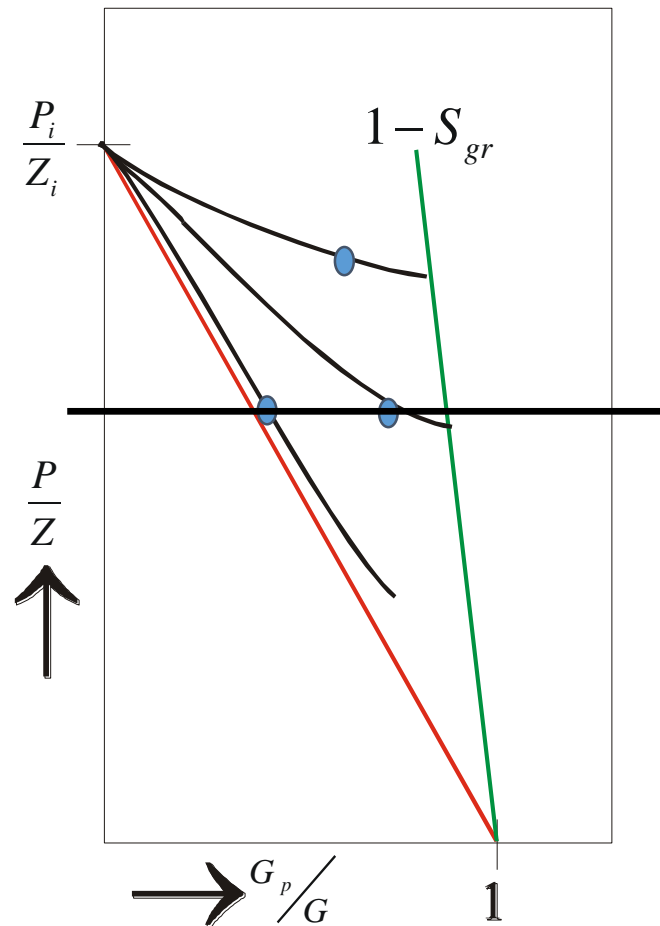
$S_{gr}$  is fixed, but the associated trapped / immobile gas is also a linear function of  $P/Z$

# Gas Reservoir with Water Influx

- Errors if aquifer not accounted for



# Gas Reservoir with Water Influx



At given final pressure Some water influx is Beneficial

# Oil Reservoirs

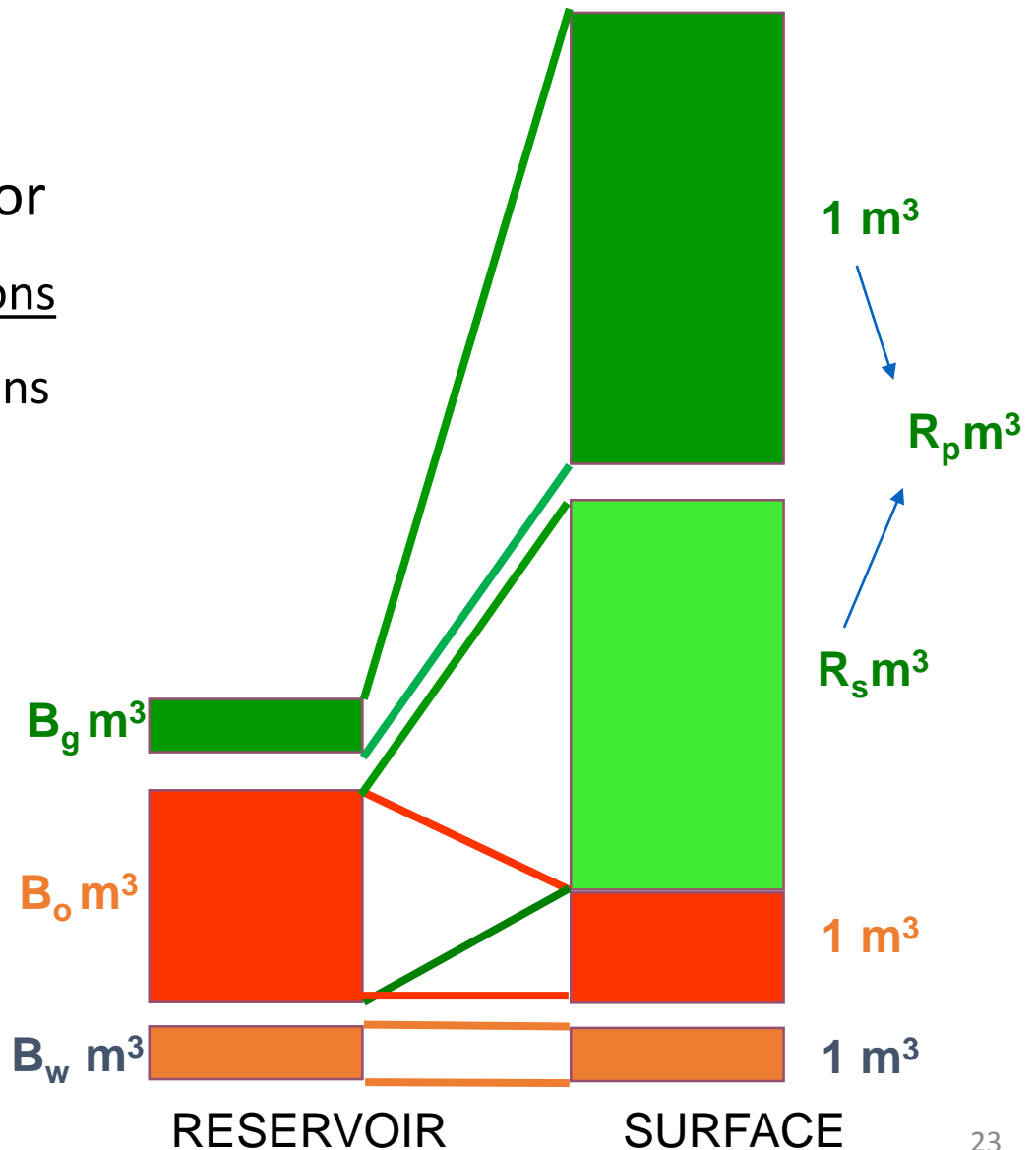
- Oil MBE is more complex than gas MBE as there are more phases involved
  - Oil
  - Dissolved gas
  - Free gas
  - Water
- Volume balance can be evaluated as

Underground withdrawal = expansion of oil + originally dissolved gas  
+ expansion of gas-cap gas  
+ reduction in HCPV due to connate-water expansion and decrease in pore volume

# Reservoir and Surface Volumes

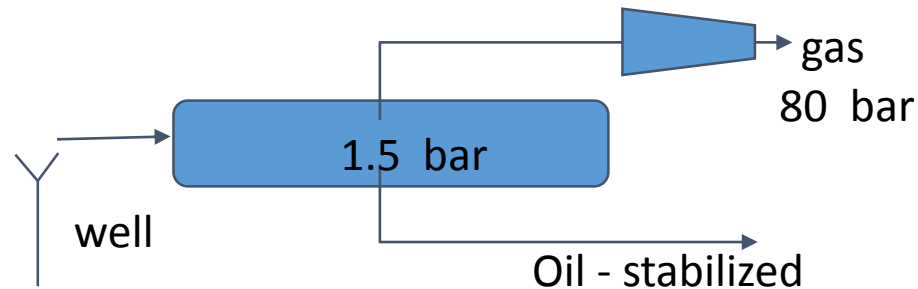
$B$  = Formation Volume Factor  
= volume at reservoir conditions  
volume at standard conditions

$R$  = Gas : Oil Ratio  
= volume of gas at standard conditions  
volume of oil at standard conditions

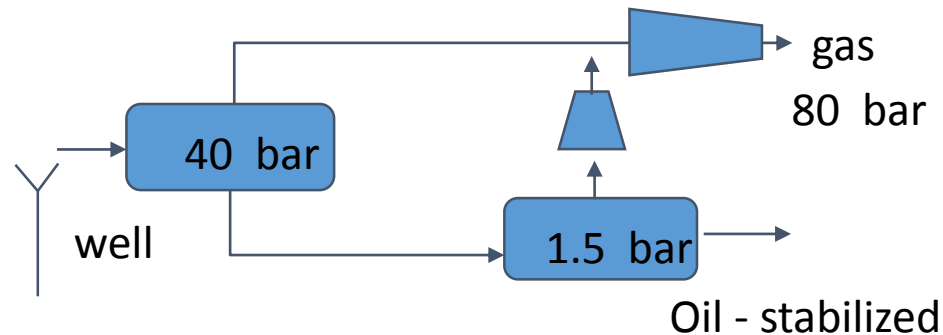


# $B_o$ and $B_g$ are dependent on surface facilities

## Option 1:



## Option 2:

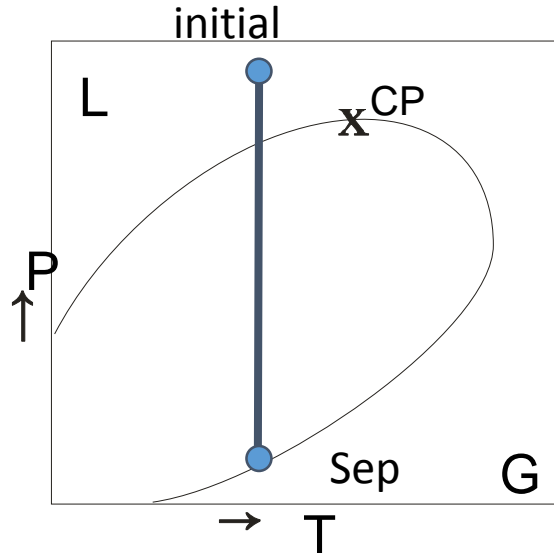


**Option 2 gives a lower  $B_o$  and more liquid reserves**



# Hydrocarbon Phase Behavior

## Explanation in phase diagram

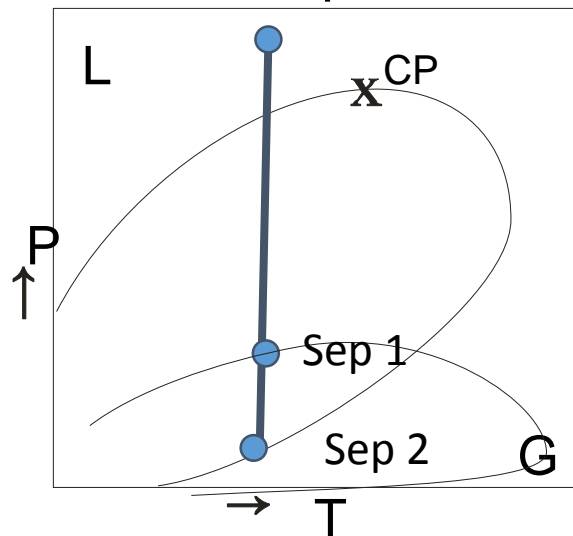


The extreme case:

Single step to atmospheric:  
All you have is gas – no liquids

Two steps:

At first step:  
take only the liquid to next separator  
This liquid has a different PVT diagram  
Result: liquids in the tank



Task of the facility engineer: optimize liquid yield  
while considering energy and facility cost

# Expansion of Fluids

Expansion of fluids as we go from initial pressure to a lower pressure

Expansion of oil and dissolved gas:

- Liquid expansion:

$$N(B_o - B_{oi})$$

- Expansion of gas-cap gas:

$$N(R_{si} - R_s)B_g$$

- Expansion of gas-cap gas:

- Total volume of gas cap gas is  $mNB_{oi}$  (rb), which is  $G = mNB_{oi}/B_{gi}$  at scf
- This amount of gas at lower pressure  $mNB_{oi} B_g/B_{gi}$  (rb)
- Therefore, expansion of gas-cap is

$$mNB_{oi} \left( \frac{B_g}{B_{gi}} - 1 \right)$$

# Change in HCPV

## (Connate-Water Expansion and Pore-Volume Reduction)

Total volume change:  $d(\text{HCPV}) = -dV_w + dV_f$  or

$$d(\text{HCPV}) = -(c_w V_w + c_f V_f) \Delta P \text{ where}$$

$V_f$  is total pore volume =  $\text{HCPV} / (1 - S_{wc})$  and

$V_w$  is connate water volume =  $V_f \times S_{wc}$

Total HCPV including gascap is  $(1+m)NB_{oi}$

then HCPV reduction can be expressed as

$$-d(\text{HCPV}) = (1 + m)NB_{oi} \left( \frac{c_w S_{wc} + c_f}{1 - S_{wc}} \right) \Delta P$$

# Underground Withdrawal

Observed surface production during pressure drop  $\Delta P$  is  $N_p$  stb of oil and  $N_p R_p$  scf of gas ( $N_p R_s$  comes from dissolved gas and remaining  $N(R_p - R_s)$  is from gas cap).

Total underground withdrawal at reservoir condition is

$$N_p (B_o + (R_p - R_s) B_g)$$

Equating this withdrawal with the sum of volume changes leads

$$\begin{aligned} & N_p (B_o + (R_p - R_s) B_g) \\ &= N B_{oi} \left[ \frac{(B_o - B_{oi}) + (R_{si} - R_s) B_g}{B_{oi}} + m \left( \frac{B_g}{B_{gi}} - 1 \right) \right] \end{aligned}$$

# MB Expressed as Linear Equation

Presented by (Havlena and Odeh)

Production:  $F = N_p (B_o + (R_p - R_s)B_g) + W_p B_w$

Expansion of oil and dissolved gas:  $E_o = (B_o - B_{oi}) + (R_{si} - R_s) B_g$

Expansion of gas-cap gas:  $E_g = B_{oi}(B_g/B_{gi} - 1)$

Expansion of connate water and reduction in pore volume:

$$E_{f,w} = (1 + m)B_{oi} \left( \frac{c_w S_{wc} + c_f}{1 - S_{wc}} \right) \Delta P$$

Using these terms, MB equation can be written as

$$F = N (E_o + mE_g + E_{f,w}) + W_e B_w$$

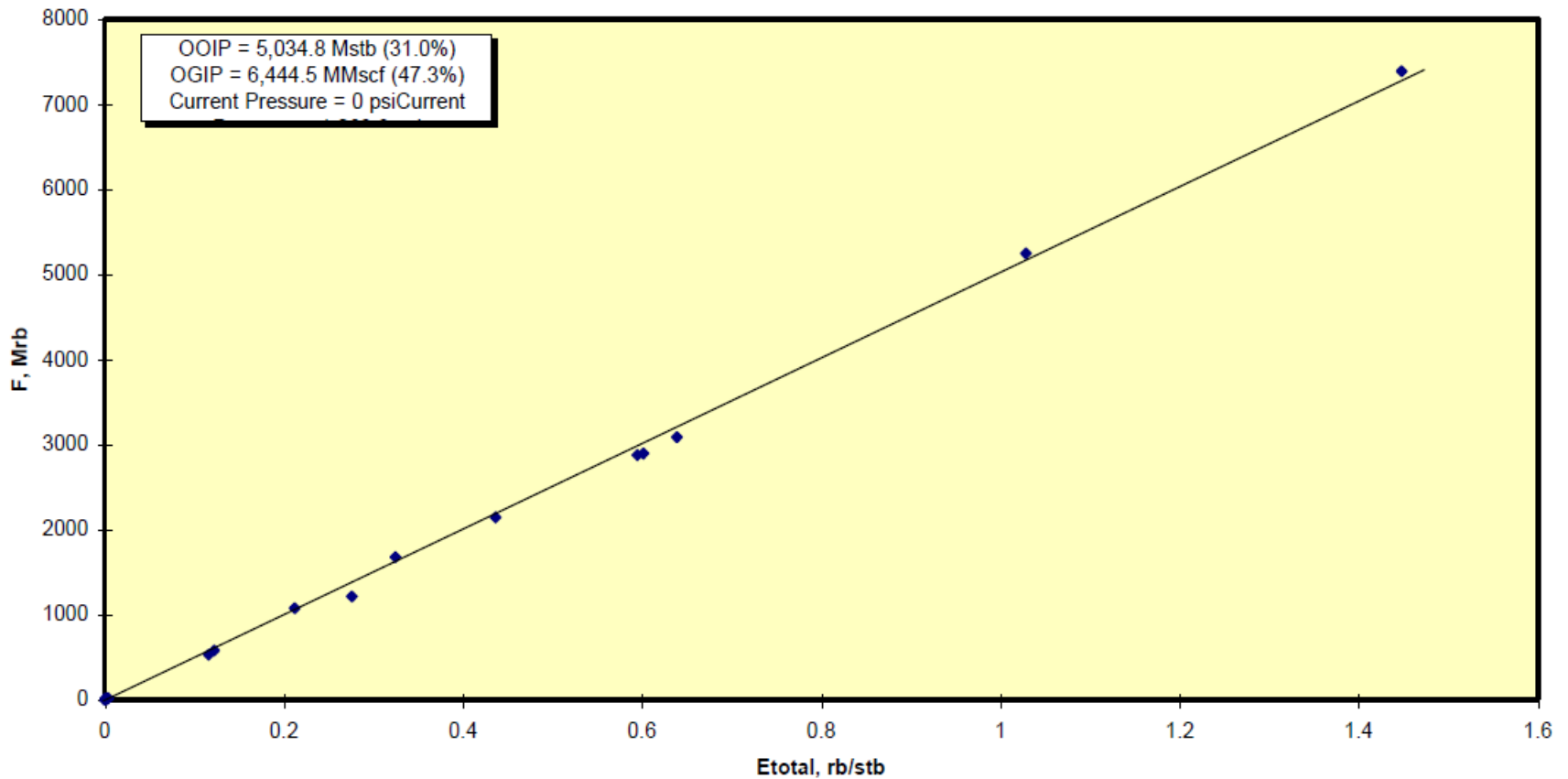
Consider it for different drive mechanisms (solution gas drive, gas-cap drive, water drive)

# Solution-Gas Drive

- Mechanisms: expansion of oil and release of its own gas
  - No gas cap:  $m = 0$
  - No water influx
- A. above bubble point:
  - $R_s = R_{si} = R_p$  therefore
  - $F = N (E_o + E_{f,w})$
- So plot  $F$  versus  $(E_o + E_{f,w})$  should be straight line with slope of  $N$  (STOIIP)
- B. below bubble point:
  - Free gas:  $R_s < R_{si}$
  - No initial gas cap
  - $F = N (E_o + E_{f,w})$
- So plot  $F$  versus  $(E_o + E_{f,w})$  should be straight line with slope of  $N$  (STOIIP)

# Plot of F vs. $E_{\text{total}}$

Should yield a straight line with a y intercept of zero and a slope of the original oil in place

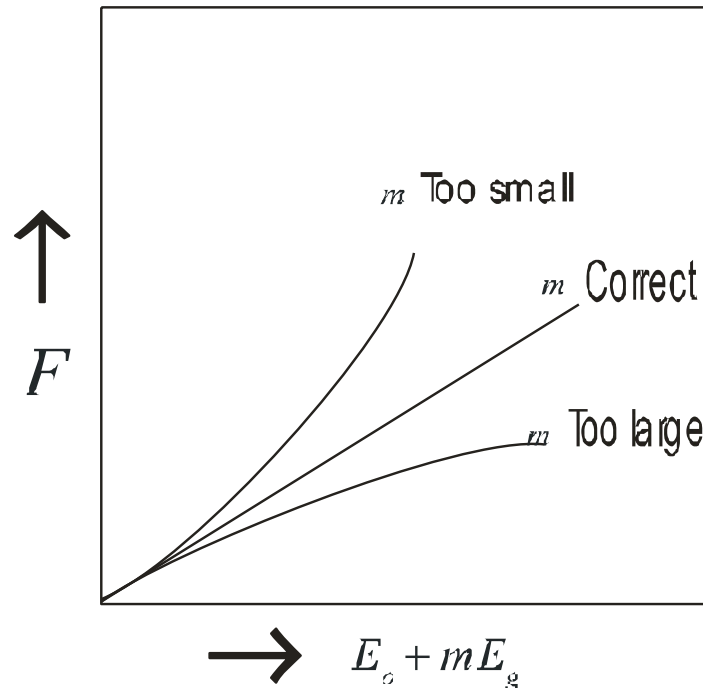


# Gas-Cap Drive

- Mechanisms: free gas
  - Pore compressibility negligible
  - No water influx

$$F = N (E_o + mE_g)$$

- So plot  $F$  versus  $(E_o + mE_g)$ , slope is  $N$ , select  $m$  such that a straight line results





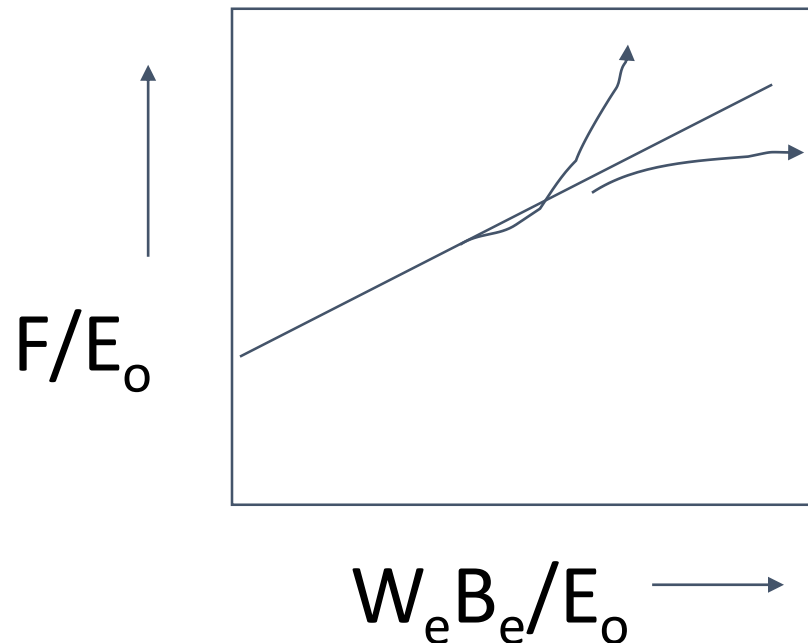
# Water Drive

- Mechanisms: water influx, aquifer or injector
  - Pore compressibility negligible

$$F = N (E_o) + W_e B_w$$

So, plot  $F/E_o$  versus  $W_e B_w/E_o$  should give a straight line

A good method to verify your aquifer model, which can be complex and a function of pressure and time



# Disadvantages MBE

- no flow dynamics
- assumes uniformity of
  - pressure
  - saturation
  - composition
- NO distribution of fluids therefore no real predictive power
- alternative
  - reservoir simulation (history matching)

**But ALWAYS do it as sanity check**