

**Homework Number 6**  
**Ae 121b, Winter Term 2017**  
**Due: Wednesday, March 8, 2017**

**General Instructions:**

1. Homework solutions should be neat and logically presented. Show all steps of your work so that we can follow what you are doing. This helps particularly in assigning partial credit if you do not get the correct final answer.
2. For problems which involve a control volume analysis, include a sketch of the flow/system, and indicate clearly your choice of control surface as necessary.
3. If a problem calls for a qualitative plot of something you may hand-sketch it, otherwise it should be a quantitatively correct, computer-generated plot.
4. Always state and justify any assumptions you make. For instance, if you use a 1D equation, indicate why it should apply in this case.
5. If you use any results or equations that were derived or presented in class, you do not need to derive them. However, if you use results or equations from other references you must show how they are derived and justify their use (i.e. describe the assumptions that go into the derivation and show that those assumptions are valid for the problem).
6. If the problem requires writing a program, please submit a hardcopy of your code.
7. You may not use Ae121 materials from previous years.

**Homework Problems:**

**Problem 1: Combustion Chamber Model**

Assume you have a combustion chamber for a LOX-methane rocket with a cross-sectional area of  $0.157 \text{ m}^2$ , a length of  $0.75 \text{ m}$ , and an total fuel injector cross-sectional area of  $0.0157 \text{ m}^2$ . The overall equivalence ratio is  $1.139$  (slightly fuel-rich). Assume that the oxidizer is injected as a gas and the fuel partly as a gas (with an initial equivalence ratio of  $0.45$ ) and partly as a liquid with an injection velocity of  $10 \text{ m/s}$  (use this also as the initial droplet velocity). The inlet gas temperature is  $600\text{K}$  and the combustion chamber pressure is  $3.4474 \text{ MPa}$ .

a) For initial (injected) droplet diameters of  $30, 50, 80, 100, \text{ and } 200 \text{ }\mu\text{m}$  calculate the droplet diameter, gas temperature, equivalence ratio, gas and droplet velocities, and liquid and vapor flow rates as a function of position along the axis of the combustion chamber. Plot these parameters and identify the droplet size that gives the best balance between good combustion efficiency and heat load on the injector.

This problem involves solving the equations developed in class along the axis of the combustion chamber. There are several algebraic relations that are required, two derivatives for which there are algebraic equations ( $dm_l/dx$  and  $d\phi/dx$ ), and a system of three ode's that can be solved with a routine such as ode45 in Matlab. The ode's are written in terms of the derivatives  $dD^2/dx$ ,  $dv_d/dx$ , and  $dT_g/dx$ . The following pseudocode will give you a start on constructing the solution. Use GRI30 as the gas model. It may also be useful to create functions for the gas enthalpy  $h_g$  and viscosity  $\mu$  that return these properties as a function of  $T_g, P, \phi$ .

b) (will not be graded, but submit plots). Vary the droplet injection velocity in the code for a few of the droplet diameters to see what effect this has on the distance required to evaporate the droplets.

---

**Algorithm 1** Combustion Chamber Model

---

```
1: procedure MAIN
2:   Define globals
3:   Define constants and conditions at inlet
4:   Compute flow rates at inlet
5:   Equilibrate gas with inlet stoichiometry to get inlet  $T_g$ 
6:   Call ode45 or equivalent to solve system of 3 ode's
7:   Plot results
8: end procedure

1: procedure FUNCTION FOR RHS OF ODE'S TO USE WITH ODE45
2:   if Droplet diameter > 0 then
3:     Compute flow rates
4:     Get gas properties from Cantera
5:     Calculate  $v_g$ ,  $Re$ , and  $C_D$ 
6:     Calculate evaporation constant  $K$  (implement as a separate function)
7:     Calculate  $dm_l/dx$  and  $d\phi/dx$  (algebraic relations)
8:     Set RHS's for ODE's  $dD^2/dx$ ,  $dv_d/dx$ , and  $dT_g/dx$  (requires functions for  $dh_g/d\phi$  and  $d\phi/dT_g$ )
9:   else
10:    Set RHS's to zero
11:   end if
12: end procedure

1: procedure FUNCTION FOR EVAPORATION CONSTANT  $K(T_g, P, \phi)$ 
2:   Define constants for methane
3:   Calculate  $T_b$  from Clausius-Clapeyron equation
4:   Calculate average temperature  $\bar{T}$  (use a reasonable guess for  $T_f$ )
5:   Set the state of the fuel and oxidizer at  $\bar{T}$  and  $P$ 
6:   Calculate  $k_g$  and  $C_p$ 
7:   Calculate  $B_o q$ 
8:   Calculate  $K$ 
9: end procedure

1: procedure FUNCTION FOR  $dh_g/d\phi(T_g, P, \phi)$ 
2:   Define a  $\phi_1$  and  $\phi_2$  that are slightly above and below  $\phi$ 
3:   Set gas to these compositions in Cantera and equilibrate (use TP)
4:   Calculate gas enthalpies at these two conditions
5:   Calculate estimate of  $dh_g/d\phi$  from slope over this interval
6: end procedure

1: procedure FUNCTION FOR  $dh_g/dT(T_g, P, \phi)$ 
2:   Define a  $T_{g1}$  and  $T_{g2}$  that are slightly above and below  $T_g$ 
3:   Equilibrate in Cantera using the current composition at these two values of  $T_g$ 
4:   Calculate gas enthalpies at these two conditions
5:   Calculate estimate of  $dh_g/dT$  from slope over this interval
6: end procedure
```

---