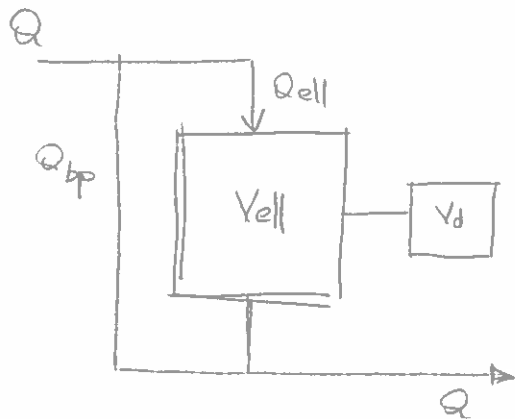


# PRACTICAL SESSION 5

## EXERCISE 2

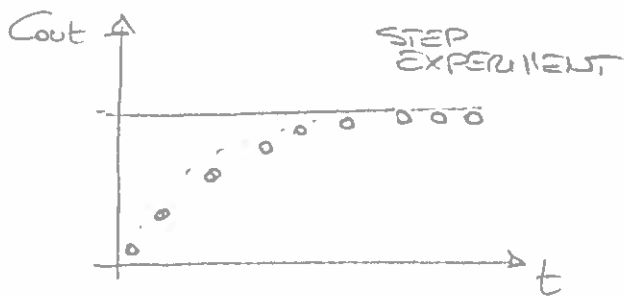


compartment model

2 parameters

$\alpha, \beta$

$$\begin{cases} Q_{bp} = \alpha Q & \alpha \in [0; 1] \\ V_{dead} = \beta V & \beta \in [0; 1] \end{cases}$$



$$\frac{C_{out}}{C_0} = 1 - (1 - \alpha) e^{-\frac{1 - \alpha}{1 - \beta} \frac{t}{\tau}}$$

$C_0$  is not given, but it can be inferred from the experimental data as the asymptotic value of the curve

linearization of the curve

$$\frac{C_{out}}{C_0} - 1 = - (1 - \alpha) e^{-\frac{1 - \alpha}{1 - \beta} \frac{t}{\tau}}$$

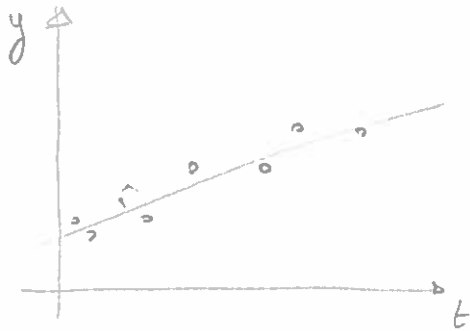
$$\frac{C_{out} - C_0}{C_0} = - (1 - \alpha) e^{-\frac{1 - \alpha}{1 - \beta} \frac{t}{\tau}}$$

$$\frac{C_0}{C_{out} - C_0} = - \left[ (1 - \alpha) e^{-\frac{1 - \alpha}{1 - \beta} \frac{t}{\tau}} \right]^{-1}$$

$$\frac{C_0}{C_0 - C_{out}} = \frac{e^{\frac{1 - \alpha}{1 - \beta} \frac{t}{\tau}}}{1 - \alpha}$$

$$\ln \frac{C_0}{C_0 - C_{out}} = \ln \frac{1}{1 - \alpha} + \frac{1 - \alpha}{1 - \beta} \frac{t}{\tau} \quad \text{linear model} \rightarrow \text{linear regression analysis}$$

$$\underbrace{\ln \frac{C_0}{C_0 - C_{out}}}_y = \underbrace{\ln \frac{1}{1-\alpha}}_q + \underbrace{\frac{1-\alpha}{1-\beta} \frac{t}{\tau}}_{mt}$$



$$\begin{cases} q = \ln \frac{1}{1-\alpha} \\ m = \frac{1-\alpha}{(1-\beta)\tau} \end{cases}$$

from the  
regression  
analysis

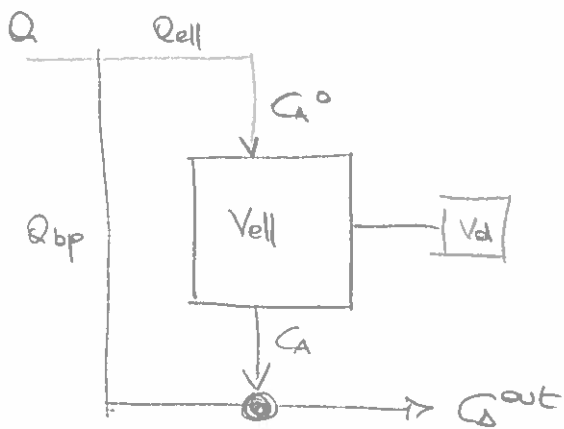
$$\underline{Y} = \left[ \ln \frac{C_0}{C_0 - C_{out}} \right]_i = \left[ \ln \frac{1}{1 - F_{exp}} \right]_i$$

$$\underline{X} = \begin{bmatrix} 1 & t_i \\ 1 & t_i \\ \vdots & \vdots \end{bmatrix} \quad a = \begin{bmatrix} q \\ m \end{bmatrix}$$

$$\underline{A} \underline{a} = \underline{b} \quad \begin{cases} \underline{A} = \underline{X}' \underline{X} \\ \underline{b} = \underline{X}' \underline{Y} \end{cases} \Rightarrow \text{linear regression analysis } q, m$$

$$\begin{cases} \alpha = 1 - \frac{1}{\exp(q)} \\ \beta = 1 - \frac{1-\alpha}{m\tau} \end{cases} \quad \text{complete characterization of the 2 parameter model}$$

$$\tau_{cell} = \frac{V_{ell}}{Q_{ell}} = \frac{(1-\beta)V}{(1-\alpha)Q} = \frac{1-\beta}{1-\alpha} \tau$$



concentrations  
at the exit of  
the ideal CSTR

CSTR ( $\tau_{ell}$ )

$$\tau = k C_A^2$$

$$\frac{C_A^0 - C_A}{\tau_{ell}} + R_A = 0$$

$$\frac{C_A^0 - C_A}{\tau_{ell}} - k C_A^2 = 0$$

$$C_A^0 - C_A - k \tau_{ell} C_A^2 = 0$$

$$k \tau_{ell} C_A^2 + C_A - C_A^0 = 0$$

$$C_A = \frac{-1 + \sqrt{1 + 4k \tau_{ell} C_A^0}}{2k \tau_{ell}}$$

outlet concentrations

$$Q C_A^{out} = Q_{ell} C_A + Q_{bp} C_A^0$$

$$C_A^{out} = (1-\alpha) C_A + \alpha C_A^0$$

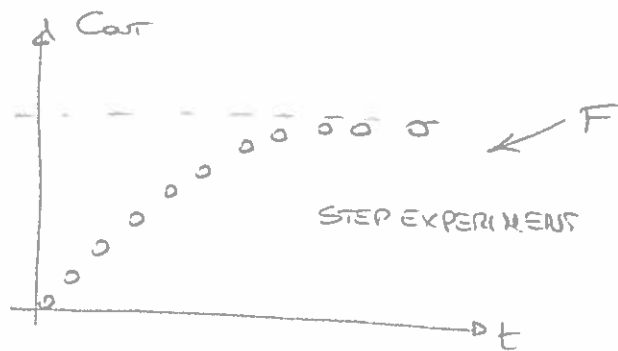
$$C_A^{out} = (1-\alpha) \frac{-1 + \sqrt{1 + 4k \tau_{ell} C_A^0}}{2k \tau_{ell}} + \alpha C_A^0$$

Comparison with ideal CSTR behavior

$$C_A^{CSTR} = \frac{-1 + \sqrt{1 + 4k \tau C_A^0}}{2k \tau}$$

the only difference with respect to  $C_A$  from the effective CSTR above is the residence time  $\tau$  vs  $\tau_{ell}$

## EXERCISE 3



Sequential model

from the CDF  $F$  we have to infer the RTD  $E$

We can proceed in two different ways:

1) numerical differentiation of  $F$  to have  $E$   
(uncertainties can arise)

→ 2) fitting of  $F$  with a proper non linear function and then analytical differentiation

If we look qualitatively at the shape of  $F$  we can imagine that the reactor has a mixed flow like behavior, so we can try to see if we can use the following fitting function with 2 parameters  $C_2$  and  $C_3$

$$F(t) = 1 - C_2 \exp\left(-\frac{t}{C_3}\right)$$

in case of perfect CSTR  $C_2 = 1$   
 $C_3 = \tau$

even if a linear representation is possible, we can also proceed using non linear representation tools

linear representation

$$1 - F = C_2 \exp\left(-\frac{t}{C_3}\right)$$

$$\underbrace{\ln(1-F)}_y = \underbrace{\ln C_2}_q - \underbrace{\frac{1}{C_3} t}_{mt}$$

$$\begin{cases} y = 1 - F \\ m = -\frac{1}{C_3} \\ q = \ln C_2 \end{cases}$$

Residence time distribution function

$$E = \frac{dF}{dt}$$

$$E = \frac{C_2}{C_3} \exp\left(-\frac{t}{C_3}\right)$$

Segregated model

$$C_A^{out} = \int_0^{\infty} C_A^{batch}(t) E(t) dt$$

we need to find the expression of evolution in a batch reactor

$$\begin{cases} \frac{dC_A^{batch}}{dt} = -k C_A^{batch 2} \\ C_A^{batch}(t=0) = C_{A0} \end{cases}$$

$$C_A^{batch -2} dC_A^{batch} = -k dt$$

$$C_A^{batch}(t) = \frac{C_{A0}}{1 + k t C_{A0}}$$

$$C_A^{out} = \int_0^{\infty} \underbrace{\frac{C_{A0}}{1 + k t C_{A0}} \cdot \frac{C_2}{C_3} \exp\left(-\frac{t}{C_3}\right) dt}_{\text{numerical integration}}$$

Comparison with  
PFR and CSTR

$$C_{CSTR}^{out} = \frac{-1 + \sqrt{1 + 4k\tau C_{A0}}}{2k\tau}$$

$$C_{PFR}^{out} = \frac{C_{A0}}{1 + k\tau C_{A0}}$$

## EXERCISE 4

We can find the RTD exactly following the same steps in the previous exercise

$$\left. \begin{array}{l} \text{Maximum Mixedness Model} \\ \\ \end{array} \right\} \begin{array}{l} \frac{dC_A}{d\lambda} = \frac{F}{1-F} (C_A - C_A^0) - R_A \\ \\ C_A(\lambda \rightarrow \infty) = C_A^0 \end{array}$$

$\lambda \rightarrow \infty$  can be replaced with the maximum value of  $\lambda$  we can expect in our system

## EXERCISE 4



It is important to be sure that the area below the curve  $E$  is equal to 1 i.e. that the  $E$  curve is normalized

$$M_0 = \int_0^{\infty} E(t) dt = 1$$

mean residence time

$$t_m = \int_0^{\infty} t E(t) dt \quad (\text{this is also } \mu_1)$$

calculation of variance

$$M_2 = \int_0^{\infty} t^2 E(t) dt$$

$$\sigma^2 = M_2 - t_m^2$$

$$\sigma_{\theta}^2 = \frac{\sigma^2}{t_m^2}$$

DISPERSION MODEL

$$\sigma_{\theta}^2 = \frac{2}{Pe} \left[ 1 - \frac{1}{Pe} (1 - e^{-Pe}) \right]$$

if  $Pe \gg 1$

$$\sigma_{\theta}^2 = \frac{2}{Pe} \Rightarrow Pe = \frac{2}{\sigma_{\theta}^2}$$

iterative procedure

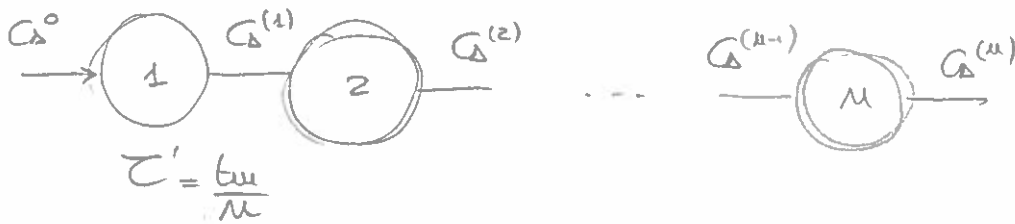
$$Pe^{(k+1)} = \frac{2}{\sigma_{\theta}^2} \left[ 1 - \frac{1}{Pe^{(k)}} (1 - e^{-Pe^{(k)}}) \right]$$

Effective dispersion  
coefficient

$$P_{dl} = \frac{L V}{P_e}$$

TANKS IN SERIES MODEL

$$M = \frac{1}{\sigma_0^2}$$



$$C_A^{(k)} = \frac{-1 + \sqrt{1 + 4k\tau' C_A^{(k-1)}}}{2k\tau'} \quad k = 1 \dots M$$



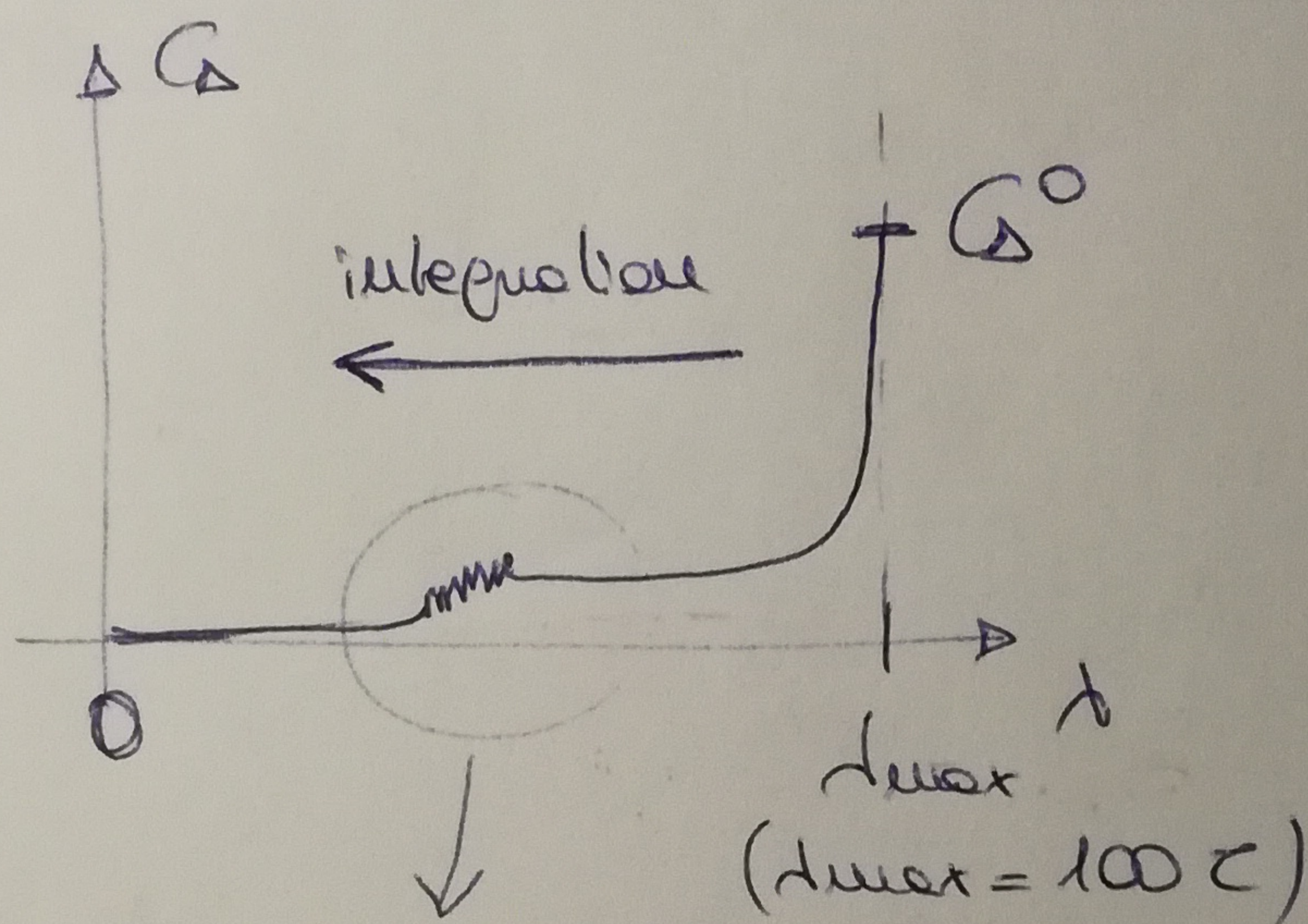
$$\frac{dC_A}{dt} = \frac{E}{1-F} (C_A - C_A^{in}) - R_A$$

$$C_A(t = t_{max}) = C_A^0$$

Problem:

$$\left\{ \begin{array}{l} \lim_{t \rightarrow 0} E = 0 \\ \lim_{t \rightarrow 0} (1-F) = 0 \end{array} \right. \rightarrow \text{if } t \rightarrow 0 \quad \frac{E}{1-F} \approx \frac{0}{0} ??$$

Example:



numerical problems

here  $\frac{E}{1-F} \approx \frac{0}{0}$  from this point the solution is wrong

Solution: just use the analytical expression of  $\frac{E}{1-F}$

$$E = \frac{C_2}{C_3} \exp(-t/C_3)$$

$$1-F = 1 - (1 - C_2 \exp(-t/C_3)) = C_2 \exp(-t/C_3)$$

$$\frac{E}{1-F} = \frac{\frac{C_2}{C_3} \exp(-t/C_3)}{C_2 \exp(-t/C_3)} = \frac{1}{C_3} \quad !$$

no numerical issues,  $\frac{E}{1-F}$  is always numerically ok!