

Nov. 27/18

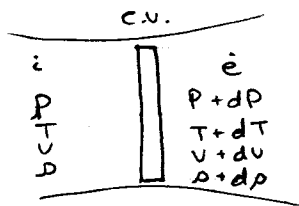
Example: Velocity of sound @ 300 K In Ks (so multiply by 1000)

$$C = \sqrt{\gamma R T} \rightarrow C = \sqrt{(1.4)(0.287)(300 \text{ K})(1000)}$$

(For air): $\gamma = 1.4$ $C = 547.2 \text{ m/s}$

Reversible, adiabatic, one-dimensional flow of an ideal gas through a nozzle

↳ minimum cross-sectional area is the "throat"



$$\cancel{z} + h_i + \cancel{V_i^2/2} + \cancel{gz_i} = \cancel{z} + h_e + \cancel{V_e^2/2} + \cancel{gz_e}$$

$$\cancel{h} + \cancel{V^2/2} = (h + dh) + \frac{(V + dV)^2}{2} = (h + dh) + \frac{1}{2}(V^2 + 2VdV + dV^2)$$

$$0 = dh + VdV$$

Energy eq'n: $dh + VdV = 0$ (I)

Property eq'n: $Tds = dh - dp/\rho$ (II)

Continuity eq'n: $\dot{m} = \rho VA$

$$d\dot{m} = 0 = (d\rho)VA + \rho A dV + \rho V dA$$

$$\Rightarrow \frac{d\rho}{\rho} + \frac{dA}{A} + \frac{dV}{V} = 0 \quad \text{(III)}$$

Combine (I) and (II) for isentropic process

$$dh = dp/\rho \Rightarrow \boxed{\frac{dp}{\rho} = -VdV} \quad \text{(IV)}$$

$$\boxed{dV = -\frac{1}{\rho V} dp} \quad \text{(IV)}$$

From (III): $\frac{dA}{A} = \left(-\frac{dp}{\rho} - \frac{dV}{V}\right)$

Substitute (IV) in (III) \Rightarrow

$$\boxed{\frac{dA}{A} = -\frac{dp}{\rho} \left(\frac{dp}{dp}\right) + \left(\frac{1}{\rho V^2}\right) dp}$$

$$\frac{dA}{A} = -\frac{dp}{\rho} \left(\frac{dp}{dp} - \frac{1}{V^2}\right) = \frac{dp}{\rho} \left(-\frac{1}{dp/dp} + \frac{1}{V^2}\right)$$

$$dp/dp = c^2 = \left(\frac{V}{m_a}\right)^2$$

$$\boxed{\frac{dA}{A} = \frac{dp}{\rho V^2} (1 - M_a^2)}$$

For a nozzle, $dp < 0$:

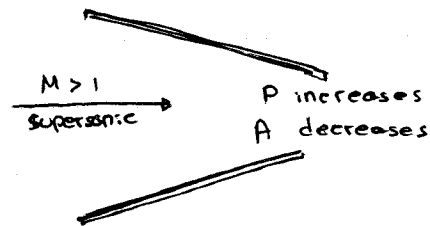
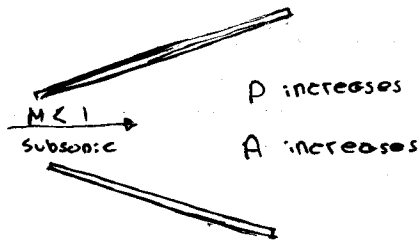
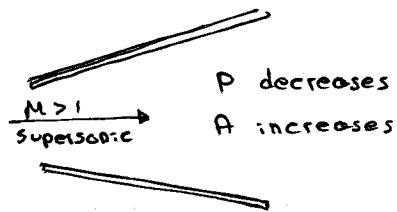
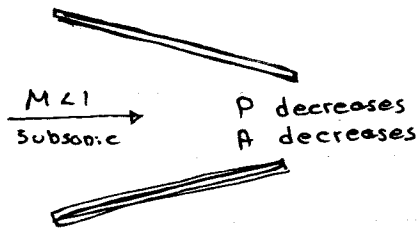
Subsonic nozzle: $M < 1$, $dA < 0$: nozzle converging

Supersonic nozzle: $M > 1$, $dA > 0$: nozzle diverging

For a diffuser, $dp > 0$:

Subsonic diffuser: $M < 1$, $dA > 0$: diffuser diverging

Supersonic diffuser: $M > 1$, $dA < 0$: diffuser converging



$$h + \frac{V^2}{2} = h_0$$

Ideal gas $\Rightarrow C_p T + \frac{V^2}{2} = C_p T_0$

$$V^2 = 2C_p(T_0 - T)$$

$$C_p - C_v = R \quad \rightarrow \quad C_p = \frac{RK}{K-1} \quad (*)$$

$$C_p/C_v = K \quad \rightarrow \quad C_v = \frac{R}{K-1} \quad (**)$$

Substitute $(*)$ in $(IV) \Rightarrow V^2 = 2 \frac{KRT}{K-1} \left(\frac{T_0}{T} - 1 \right)$

$$V^2 = 2 \frac{C^2}{K-1} \left(\frac{T_0}{T} - 1 \right) \Rightarrow \frac{V^2}{C^2} = \frac{2}{K-1} \left(\frac{T_0}{T} - 1 \right)$$

$$M^2 = \frac{2}{K-1} \left(\frac{T_0}{T} - 1 \right) \Rightarrow \boxed{\frac{T_0}{T} = 1 + \frac{K-1}{2} M^2} \quad (A)$$

$$\left(\frac{T_0}{T} \right)^{K/(K-1)} = \frac{P_0}{P}$$

$$\boxed{\frac{P_0}{P} = \left[1 + \frac{K-1}{2} M^2 \right]^{K/(K-1)}} \quad (B)$$

(TABLE A.12)

$$\left(\frac{T_0}{T} \right)^{1/(K-1)} = \frac{P_0}{P}$$

$$\boxed{\frac{P_0}{P} = \left[1 + \frac{K-1}{2} M^2 \right]^{1/(K-1)}} \quad (C)$$

Throat condition (*) ($M = 1$)

$$T^*/T_0 = 2/(k+1)$$

$$\rho^*/\rho_0 = \left(\frac{2}{k+1}\right)^{1/(k-1)}$$

$$P^*/P_0 = \left(\frac{2}{k+1}\right)^{k/(k-1)}$$

T^*, P^*, ρ^* are critical properties

$$\dot{m} = \rho V A \rightarrow \dot{m}/A = \rho V = \frac{P}{RT} V \frac{\sqrt{kT_0}}{\sqrt{kT_0}} = \frac{\rho V}{\sqrt{kRT}} \sqrt{\frac{k}{R}} \sqrt{\frac{T_0}{T}} \sqrt{\frac{T}{T_0}}$$

$$\dot{m}/A = \frac{PM}{\sqrt{T_0}} \sqrt{\frac{k}{R}} \sqrt{1 + \frac{k-1}{2} M^2}$$

Use eqn (B) \Rightarrow

(bigger) $\left\{ \begin{aligned} \dot{m}/A &= P_0/\sqrt{T_0} \sqrt{\frac{k}{R}} \left(\frac{M}{(1 + \frac{k-1}{2} M^2)^{\frac{k+1}{2(k-1)}}} \right) \\ \frac{\dot{m}}{A} &= \frac{P_0}{\sqrt{T_0}} \left(\sqrt{\frac{k}{R}} \right) \left(\frac{M}{(1 + \frac{k-1}{2} M^2)^{\frac{k+1}{2(k-1)}}} \right) \end{aligned} \right.$

At the throat $\Rightarrow M = 1$

$$\frac{\dot{m}}{A^*} = \frac{P_0}{\sqrt{T_0}} \left(\sqrt{\frac{k}{R}} \right) \frac{1}{\left(\frac{k+1}{2} \right)^{\frac{k+1}{2(k-1)}}}$$

$$A/A^* = \frac{1}{M} \left[\left(\frac{2}{k+1} \right) \left(1 + \frac{k-1}{2} M^2 \right) \right]^{\frac{k+1}{2(k-1)}}$$

(1)

Nov. 29/18

Optional tutorial Tuesday @ Same class time, next week.

Example: "Convergent nozzle has an exit area..."

$$K = 1.4$$

Using table A.12

$$T^*/T_0 = 0.8333 \Rightarrow T^* = 300 \text{ K}$$

$$\text{When } M_1 = 1 \Rightarrow V = C = \sqrt{KRT}$$

$$= \sqrt{(1.4)(0.287)(1000)(300)} = 347.2$$

$$P^*/P_0 = \left(\frac{2}{K+1}\right)^{K/(K-1)}$$

$$P^* = 0.528$$

$$P^* = 528$$

→ ideal gas law

$$P^* = \rho^* R T^*$$

$$\rho^* = P^* / R T^*$$

$$\rho^* = \frac{528}{(0.287)(300)} = 6.1324$$

$$\dot{m} = \dot{m}^* = \rho A V = (6.1324)(500 \times 10^{-6})(347.2) = 1.0646 \text{ kg/s}$$

$$\text{If: } P_E = 800 \text{ kPa: } P_E/P_0 = 0.8$$

From Table A.12

$$M_E = 0.573$$

$$T_E/T_0 = 0.9381$$

$$T_E = 337.2 \text{ K}$$

$$C_E = \sqrt{KRT} = \sqrt{(1.4)(0.287)(1000)(337.2)} = 368.4 \text{ m/s}$$

$$M_E = V_E/C_E \Rightarrow V_E = M_E \cdot C_E$$

$$\Rightarrow V_E = (0.573)(368.4) = 211.1 \text{ m/s}$$

$$\rho_E = \frac{P_E}{R T_E} = \frac{800}{(0.287)(337.2)} = 8.2542 \text{ kg/m}^3$$

$$\dot{m} = (\rho V A)_E = (8.2542)(211.1)(500 \times 10^{-6}) = 0.8712 \text{ kg/s}$$

Example: $A_E/A^* \Rightarrow M_E = 2.197$
 $P_E/P_0 = 0.0939$
 $T_E/T_0 = 0.5089$ } Interpolate

$$P_E = 0.0939 (1000) = 93.9 \text{ kPa}$$

$$T_E = 0.5089 (360) = 183.2 \text{ K}$$

$$C_E = \sqrt{\gamma R T_E} = \sqrt{(1.4)(0.287)(1000)(183.2)} = 271.3 \text{ m/s}$$

$$V_E = M_E C_E = 2.197 (271.3) = 596.1 \text{ m/s}$$

b) $A_E/A^* = 2 \Rightarrow M_E = 0.308$
 (subsonic) $P_E/P_0 = 0.936$
 $T_E/T_0 = 0.9812$ } Interpolate

$$P_E = (0.936)(1000) = 936 \text{ kPa}$$

$$T_E = (0.9812)(360) = 353.3 \text{ K}$$

$$C_E = \sqrt{\gamma R T_E} \Rightarrow \sqrt{(1.4)(0.287)(1000)(353.3)} = 376.8 \text{ m/s}$$

$$V_E = M_E C_E \Rightarrow (0.308)(376.8) = 116 \text{ m/s}$$

→ 15.15 (From 8th)

Example: "Steam leaves a nozzle with a pressure of 500 kPa, temp of 350 °C, Velocity of ..."

$$h_0 = h_1 + V^2/2$$

$$P_1 = 500 \text{ kPa}$$

$$T_1 = 350^\circ\text{C}$$

From steam table:

$$h_1 = 3167.7 \text{ kJ/kg}$$

$$h_0 = 3167.7 + \left(\frac{250^2}{2 \times 1000} \right) = 3198 \text{ kJ/kg}$$

$$S_0 = S_1 = 7.6329 \text{ kJ/kg} \cdot \text{K}$$

From steam table → $T_0 = 365^\circ\text{C}$

$$P_0 = 558 \text{ kPa}$$

Example: "Air leaves a compressor in a pipe with a stagnation..."

$$h_o = h_i + V^2/2$$

$$h_o - h_i = V^2/2 \Rightarrow C_p(T_o - T_i) = V^2/2$$

$$(1.004)(150 - T_i) = \frac{125^2}{2000} \Rightarrow 142.2^\circ\text{C}$$

$$T_i = 142.2^\circ\text{C}$$

$$P_i/P_o = (T_i/T_o)^{\kappa/\kappa-1} \Rightarrow P_i = P_o (T_i/T_o)^{\kappa/\kappa-1}$$

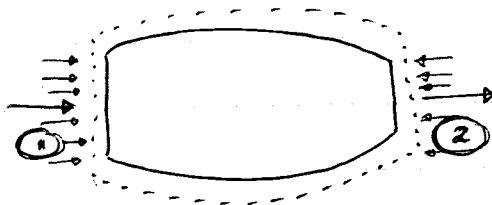
$$= (300) (415.4/432.2)^{1.4/0.4} = 281 \text{ kPa}$$

$$\dot{m} = \rho V A \rightarrow (P_i/RT_i) V_i A_i = \left[\frac{281}{(0.287)(415.4)} \right] (125)(0.02)$$

$$\dot{m} = 5.9 \text{ kg/s}$$

#27

Example: "A jet engine at takeoff has air at 20°C ..."



$$A_1 = (\pi/4) D_1^2 = 0.7854 \text{ m}^2$$

$$A_2 = 0.1257 \text{ m}^2$$

$$V_1 = \frac{RT_1}{P_1} = \frac{(0.287)(293.15)}{100} = 0.8409 \text{ m}^3/\text{kg}$$

$$V_2 = 3.444 \text{ m}^3/\text{kg}$$

$$\dot{m}_1 = \dot{m}_2 = 23.35 \text{ kg/s}$$

$$\dot{m}_1 = \rho_1 A_1 V_1 = \frac{A_1 V_1}{V_1} = \frac{(0.7854)(25)}{(0.8409)} = 23.35 \text{ kg/s}$$

$$\dot{m}_2 = \rho_2 A_2 V_2 \rightarrow V_2 = \frac{\dot{m}_2 V_2}{A_2} = \frac{(23.35)(3.444)}{(0.1257)}$$

$$V_2 = 641 \text{ m/s}$$

$$\sum F_x = (\dot{m}V)_{\text{out}} - (\dot{m}V)_{\text{in}}$$

$$-F - (P_1 - P_o)A_1 + (P_2 - P_o)A_2 = \dot{m}_2 V_2 - \dot{m}_1 V_1$$

$$-F = \dot{m}(V_2 - V_1) \rightarrow F = 14383 \text{ N}$$