

(1)

Oct. 12/17

$$Q - W = m \left[(h_2 - h_1) + \left(\frac{V_2^2 - V_1^2}{2} \right) + g(z_2 - z_1) \right] \quad \text{Thermal}$$

$$q - w = h_2 - h_1 + \frac{V_2^2 - V_1^2}{2} + g(z_2 - z_1)$$

Throttling Values:

$$\left\{ \begin{array}{l} q \approx 0, \quad w \approx 0, \quad \Delta P_e \approx 0, \quad \Delta K_e \approx 0 \\ 0 = h_2 - h_1 + 0 + 0 \end{array} \right.$$

$$\therefore h_1 = h_2 \rightarrow \text{isenthalpic}$$

$$U_1 + P_1 V_1 = U_2 + P_2 V_2$$

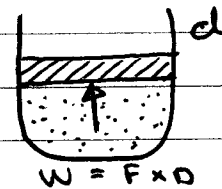
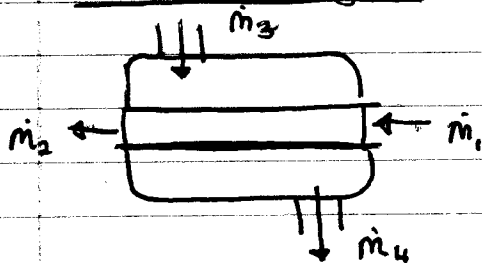
Mixing Chamber:

$$\left\{ \begin{array}{l} q \approx 0, \quad w \approx 0 \\ \Delta K_e \approx 0, \quad \Delta P_e \approx 0 \end{array} \right.$$

$$\therefore h_1 = h_2$$

$$\left\{ \begin{array}{l} \dot{m}_1 h_1 + \dot{m}_2 h_2 = \dot{m}_3 h_3 \\ \downarrow \text{cold} \quad \downarrow \text{hot} \quad \downarrow \text{warm} \end{array} \right.$$

$$h_1 + h_2 = h_3$$

Heat Exchangers

$$\dot{m}_1 = \dot{m}_2$$

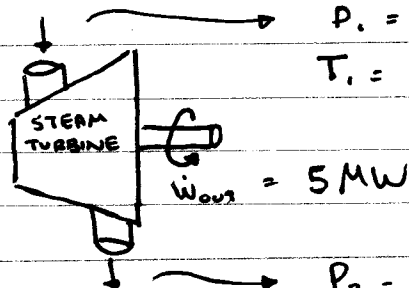
$$\dot{m}_3 = \dot{m}_4$$

$$\dot{E}_1 = \dot{E}_2$$

$$\dot{m}_1 + \dot{m}_3 = \dot{m}_2 + \dot{m}_4$$

$$\dot{m}_1 h_1 + \dot{m}_3 h_3 = \dot{m}_2 h_2 + \dot{m}_4 h_4$$

Example: 5-7 (from textbook)



$$P_1 = 2 \text{ MPa}$$

$$T_1 = 400^\circ \text{C}$$

$$V_1 = 50 \text{ m/s}$$

$$Z_1 = 10 \text{ m}$$

$$\dot{W}_{\text{out}} = 5 \text{ MW}$$

$$P_2 = 15 \text{ kPa}$$

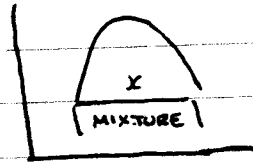
$$x_2 = 0.90$$

$$V_2 = 180 \text{ m/s}$$

$$Z_2 = 6 \text{ m}$$

Cont'd :

@ 2 MPa, $T_{\text{sat}} = 212^\circ\text{C}$



$$\left. \begin{array}{l} P_1 = 2 \text{ MPa} \\ T_1 = 400^\circ\text{C} \end{array} \right\} \text{Table A-6}$$

$$h_1 = 3248.4 \text{ kJ/kg}$$

$$\begin{aligned} h_2 &= h_f + x_2 h_{fg} \\ &= 225.94 + (0.9)(2372.3) \end{aligned}$$

$$\therefore h_2 = 2361. \sim \text{kJ/kg}$$

$$\begin{aligned} \Delta h &= h_2 - h_1 \\ &= 2361 - 3248.4 \\ &= -887.4 \text{ kJ/kg} \end{aligned}$$

$$\begin{aligned} \Delta h_e &= \frac{V_2^2}{2} - \frac{V_1^2}{2} \\ &= \frac{(180)^2 - 50^2}{2 \times 1000} \\ &= 14.95 \text{ kJ/kg} \end{aligned}$$

$$\begin{aligned} \Delta P_e &= g(z_2 - z_1) \\ &= \frac{(9.81)(6 - 10)}{1000} \\ &= -0.04 \text{ kJ/kg} \end{aligned}$$

$$\rightarrow \dot{Q}_{\text{in}} + \dot{W}_{\text{in}} + \dot{m}(h_1 + \frac{V_1^2}{2} + gz_1) = \dot{Q}_{\text{out}} + \dot{W}_{\text{out}} + \dot{m}(h_2 + \frac{V_2^2}{2} + gz_2)$$

$$\begin{aligned} W_{\text{out}} &= - \left[(h_2 - h_1) + \left(\frac{V_2^2 - V_1^2}{2} \right) + g(z_2 - z_1) \right] \\ \therefore W_{\text{out}} &= 872.48 \text{ kJ/kg} \end{aligned}$$

$$W_{\text{out}} = \dot{m} w_{\text{out}}$$

$$\therefore \dot{m} = \frac{W_{\text{out}}}{w_{\text{out}}} = \frac{5 \times 1000}{872.48 \text{ kJ/kg}}$$

$$\therefore \dot{m} = 5.73 \text{ kg/s}$$

Midterm Review

75 minutes

two sections

A - theory

1-15 Multiple choice, T/F, Short answers

B - Problem section

4-5 Problems

Practice

- ASSIGNMENT PROBS
- CLASS PROBLEMS
- PRACTICE PROBLEMS

HEAT TRANSFER

Chapter 1: Intro and Basic Concepts

Obj: 1) Understand basic mechanisms of heat transfer

2) Understand different laws of heat transfer

- i) conduction
- ii) convection
- iii) Radiation

laws: conduction: Fourier's Law

convection: Newton's Law of cool.

Radiation: Stefan-Boltzman law

Conduction:

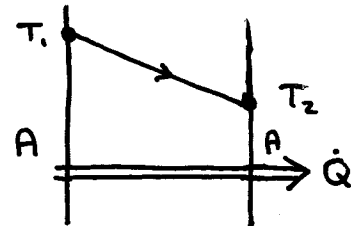


In solid, liquid, gas



↑ heat

Fourier's Law of Heat Conduction



① $Q \propto \text{Area}$

② $\dot{Q} \propto (T_2 - T_1)$

③ $\dot{Q} \propto (1/\Delta x)$

$\dot{Q} \propto \frac{A(T_1 - T_2)}{\Delta x}$
(in Watt)

$\Rightarrow \boxed{\dot{Q} = \frac{K A (T_1 - T_2)}{\Delta x}}$

Watt = $(K) \cdot \frac{m^2 \cdot K}{m}$

Thermal conductivity
 $K = W/m \cdot K$

$K_{H_2O} = 0.607 \text{ W/m} \cdot K$

$K_{IRON} = 80.2 \text{ W/m} \cdot K$

$0^\circ K \rightarrow 20000 \text{ W/m} \cdot K$

$\dot{Q}_{COND} = -KA \left(\frac{\Delta T}{\Delta x} \right)$

$(\Delta T = T_2 - T_1)$

$\dot{Q}_{COND} = -KA \left(\frac{dT}{dx} \right)$

Table 1-1

$K_{DIAMOND} = 2300 \text{ W/m} \cdot K (\approx) \text{ W/m} \cdot ^\circ C$

$K_{COPPER} = 401 \text{ W/m} \cdot K @ 20^\circ C$

$K_{WATER} = 0.601 \text{ W/m} \cdot K$

$K_{AIR} = 0.026 \text{ W/m} \cdot K$

$k \rightarrow$ high to low

- 1) Non-metal crystals
- 2) Pure metals
- 3) Metal alloys
- 4) Non-metallic solids
- 5) Liquids
- 6) Insulators
- 7) Gases

Pure metallic alloy (k)

Copper - 401

Aluminum - 237

Bronze - 52 (P. 299)
(90% Cu + 10% Al)

Thermal Diffusivity: $\rightarrow \alpha = \frac{\text{Thermal Conductivity (k)}}{\text{Heat Storage}}$

$C_p \rightarrow$ sp. heat

$$(C_p)_{H_2O} = 4.18 \text{ kJ/kg}^\circ\text{C}$$

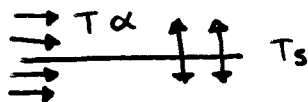
$$(C_p)_{\text{iron}} = 0.45 \text{ kJ/kg}^\circ\text{C}$$

$\rho C_p =$ per unit volume

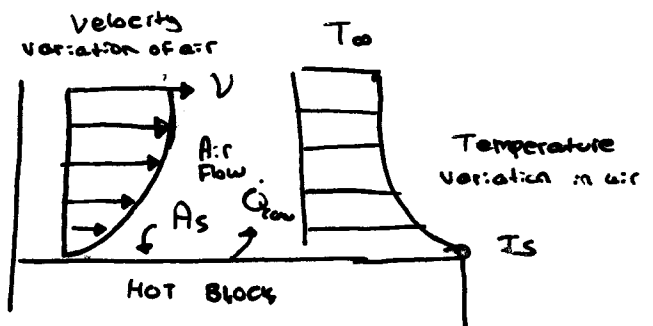
$$= \frac{k}{\rho C_p} \quad (\text{m}^2/\text{s})$$

$$= \text{W/m} \cdot \text{K} \times \frac{\text{m}^3}{\text{kg} \times \text{kJ} \times \text{kg} \cdot \text{K}}$$

Convection:



$$T_s > T_\infty$$



Newton's Law of Cooling

$$\dot{Q}_{\text{conv}} = h A_s (T_s - T_\infty)$$

convective coefficient

$$h = \text{W/m}^2 \cdot \text{K} \quad \text{W/m}^2 \cdot \text{K}$$

$$\dot{Q}_{\text{conv}} \propto A_s$$

$$\dot{Q}_{\text{conv}} \propto T_s - T_\infty$$

Free conv. of gases: 2-25

Free conv. of liquids: 10-1000

Forced conv. of gases: 25-250

Forced conv. of liquids: 50-20000

Boiling and Condensation: 2500-100000

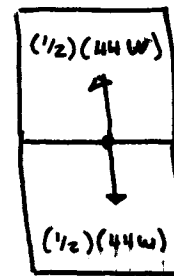
Example 1-6 (From textbook):

$$\begin{aligned} W_{e,12} = \dot{Q}_{total} &= VI \\ &= (110\text{V})(0.4\text{A}) \\ &= 44\text{W} \end{aligned}$$

$$\dot{Q} = \frac{kA(T_1 - T_2)}{L}$$

$$\therefore k = \frac{\dot{Q} \times L}{A(T_1 - T_2)} \Rightarrow \frac{(22)(0.03)}{(\pi 0.004)(15)}$$

$$\Rightarrow D = 5\text{cm} = 0.05\text{m}$$



$$\dot{Q} = 22\text{W}$$

$$\therefore k = 22.4\text{W/(m}\cdot\text{K)}$$

Example 1-8 (From textbook):

$$\begin{aligned} W_e &= \dot{Q} = VI \\ &= (60\text{V})(1.5\text{A}) \\ &= 90\text{W} \end{aligned}$$

$$\begin{aligned} A_s (\text{cylinder}) &= 2\pi rL \text{ or } \pi dL \\ \Rightarrow A_s &= \pi(0.003)(2) \end{aligned}$$

$$\dot{Q}_{conv} = hA_s(T_s - T_\infty)$$

$$h = \frac{\dot{Q}_{conv}}{A_s(T_s - T_\infty)} \Rightarrow \frac{(90)}{(A_s)(152 - 15)}$$

$$\therefore \downarrow \Rightarrow 34.9\text{W/m}^2\cdot^\circ\text{C}$$