http://www.phy.anl.gov/div/esh/Cryogenic/Appendix%202/appendix%202a.htm

## **Physics Division**

## Cryogenic Safety Manual

or



## Introduction

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## **APPENDIX 2a: CONVECTIVE HEAT TRANSFER**

The convective heat transfer coefficient, h<sub>c</sub>, is given by (from <u>Heat Transmission</u>, W. H. McAdams, McGraw-Hill, NY (1942) pp 242-245):

$$\frac{h_c L}{k_f} = \frac{1}{2} \left[ \left( \frac{L^3 \rho_f^2 g \Delta T}{\mu_f^2 T_f} \right) \left( \frac{C_y \mu_f}{k_f} \right) \right]^{0.25}$$

$$h_c = \frac{1}{2} \left[ \frac{k_f^3 \rho_f^2 g C_p}{\mu_f T_f} \right]^{0.25} \left( \frac{\Delta T}{L} \right)^{0.25}$$
 Watt/cm<sup>2</sup> K

where k = thermal conductivity,  $\rho$  = density,  $C_p$  = specific heat,  $\mu$  = viscosity, g = gravitational acceleration. Note that CGS units are used.

The subscript f means the quantities are to be evaluated at the "gas film" temperature, the arithmetic means of the temperature at the surface of the solid, and the temperature of the bulk of the gas.

The quantity L is the characteristic dimension of the system: e.g. diameter of a cylinder, spacing of parallel plates, or the edge length of a plane square. Equation (1) is valid so long as

$$\chi = \left[ \frac{L^3 \ \rho_f^2 \ g \triangle T c_y}{\mu_f T_f k_f} \right] > 10^3$$

The actual heat flow Q is given by:

$$Q = h_c \Delta T \text{ Watts/cm}^2$$

We evaluate expression (1) for several gases and conditions (using CGS units):

I. Nitrogen at 293 K and 1 ATM

 $k_f = 2.5 \times 10^{-4} \text{ w/cm K}, \rho f = 1.16 \times 10^{-3}, C_p = 1.04 \text{ J/gm K}, \text{ and } \mu f = 17.4 \times 10^{-6} \text{ poise,}$  so that

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$$h_c = \frac{1}{2} \left[ \frac{(2.51 \times 10^{-4})^3 (1.16 \cdot 10^3)^2 \times 980 \times 1.04}{174 \times 10^{-6} \times 193} \right]^{1/4} \left( \frac{\Delta T}{L} \right)^{1/4}$$

= 
$$4.04 \times 10^{-4} \left(\frac{\Delta T}{L}\right) \text{Watt/cm}^2 \text{ K}$$

II. Nitrogen from 77 K to 293 K ( $T_f = 185 \text{ K}, \Delta T = 216 \text{ K}$ )

$$k_f = 1.8x10^{-4} \text{ W/cm K}, \rho_f = 1.84x10^{-3}, \mu_f = 121x10^{-6} \text{ and}$$

$$h_c = \frac{1}{2} \left[ \frac{(1.8 \cdot 10^{-4})^3 (1.84 \cdot 10^{-3})^2 x 980 x 1.04}{121 x 10^{-6} x 185} \right]^{1/4} \left( \frac{\Delta T}{L} \right)^{1/2}$$

$$= 4.89 \times 10^{-4} \left(\frac{\Delta T}{L}\right)^{1/4} \text{ Watt/cm}^2 \text{ K}$$

III. Helium from 15 K to 293 K ( $T_f = 154$ ,  $\Delta T = 278$ )

 $k_f = 9.9 \times 10^{-4} \text{ W/cm K}, \rho_f = 3.17 \times 10^{-4}, C_p = 5.5 \text{ J/gm K}, \mu_f = 131 \times 10^{-6} \text{ poise, so that}$ 

$$h_e = \frac{1}{2} \left[ \frac{(9.9 \times 10^{-4})^3 (3.17 \times 10^{-4})^2 \times 980 \times 5.5}{131 \times 10^{-6} \times 154} \right]^{1/4} \left( \frac{\Delta T}{L} \right)^{1/4}$$

= 1.13 x10<sup>-3</sup> 
$$\left(\frac{\Delta T}{L}\right)^{1/4}$$
 Watt/cm<sup>2</sup> K

IV. Helium from 15 K to 77 K ( $T_f = 46 \text{ K}$ ,  $\Delta T = 26 \text{ K}$ )

$$k_f = 4.52 \times 10^{-4} \text{ W/cm K}, \rho_f = 1.06 \times 10^{-3}, \ \mu_f = 60 \times 10^{-6} \text{ poise, thus}$$

$$h_c = \frac{1}{2} \left[ \frac{(4.52 \cdot 10^{-4})^3 (1.06 \cdot 10^{-3})^2 x 980 x 5.5}{60 \cdot 10^{-6} \cdot 46} \right]^{1/4} \left( \frac{\Delta T}{L} \right)^{1/4}$$

= 1.89x10<sup>-3</sup> 
$$\left(\frac{\Delta T}{L}\right)^{1/4}$$
 Watt/cm<sup>2</sup> K

V. Helium from 77 K to 293 K ( $T_f = 185, \Delta T = 216$ )

 $k_f = 1.11 \times 10^{-3} \text{ W/cm K}, \rho f = 2.64 \times 10^{-4}, C_p = 5.5 \text{ J/gm K}, \mu f = 148 \times 10^{-6} \text{ poise}$ 

$$h_{\mathbf{c}} = \frac{1}{2} \left[ \frac{(1.11 \times 10^{-3})^{3} (2.64 \cdot 10^{-4})^{2} \times 980 \times 5.5}{148 \times 10^{-6} \times 185} \right]^{1/4} \left( \frac{\Delta T}{L} \right)^{1/4}$$

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= 
$$1.04 \times 10^{-3} \left(\frac{\Delta T}{L}\right)^{1/4} \text{ Watt/cm}^2 \text{ K}$$

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