

# HWRS 505: Vadose Zone Hydrology

Lecture 4

8/31/2023

Today:

1. Wrap up the review of solute transport under saturated flow
2. Air-water system in capillary tubes

# Solute transport under saturated flow

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Fall 2023

## Review of Lecture 3

- ❖ Derivation of 3D transient groundwater flow.
- ❖ Solute transport under saturated flow.
  - Advection ( $v = q/\phi$ )
  - Molecular diffusion
  - Mechanical dispersion

“The dispersion coefficient is a lumped fitting parameter that adequately describes relatively large-scale observations.”

$$\begin{aligned} q_c &= \phi(vC - D\nabla C) \\ &= qC - \phi D \nabla C \end{aligned}$$

$$\int_0^L f(x) dx = 0 \quad [0, L] \text{ is arbitrary.}$$

Suppose for  $x^*$ ,  $f(x^*) \neq 0$



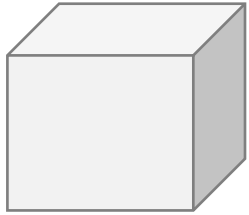
$$\int_{x^* - \Delta x/2}^{x^* + \Delta x/2} f(x) dx = 0$$

$$\lim_{\Delta x \rightarrow 0} \int_{x^* - \Delta x/2}^{x^* + \Delta x/2} f(x) dx = \Delta x \cdot f(x^*) \quad \Rightarrow$$

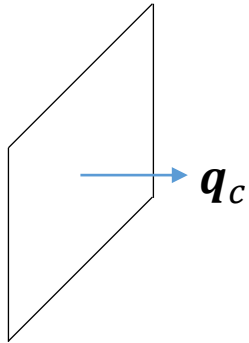
$\Rightarrow f(x^*) = 0$ , which  
contradicts  $f(x^*) \neq 0$

$\Rightarrow f(x) = 0$  every where.

# Solute transport under saturated flow

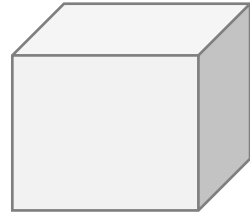


Saturated  
porous medium

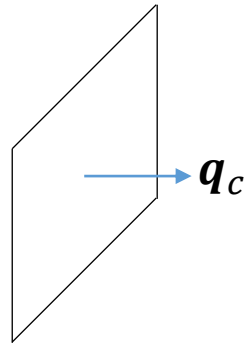


$$\begin{aligned} \mathbf{q}_c &= \phi(\mathbf{v}C - \mathbf{D}\nabla C) \\ &= \mathbf{q}C - \phi\mathbf{D}\nabla C \end{aligned}$$

$$\mathbf{D} = \alpha_T |\mathbf{v}| \mathbf{I} + (\alpha_L - \alpha_T) \frac{\mathbf{v}\mathbf{v}}{|\mathbf{v}|} + wD_0 \mathbf{I}$$

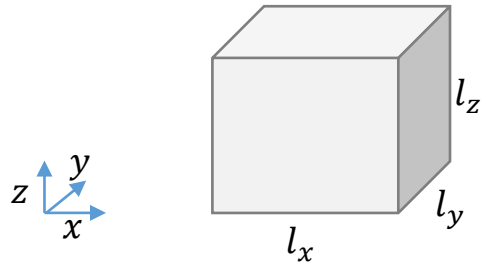


Fluid only  
(e.g., free water)



$$\mathbf{q}_c = \mathbf{v}C - D_0\nabla C$$

# Solute transport under saturated flow



$$C(x, y, z, t) = \frac{\text{mass of solute}}{\text{unit fluid volume}}$$

Mass conservation: Change of mass storage = mass in – mass out.

Rate of mass change: 
$$\frac{d}{dt} \int_0^{l_x} \int_0^{l_y} \int_0^{l_z} C(x, y, z, t) dx dy dz = \frac{d}{dt} \int_{\Omega} C(x, y, z, t) dV$$

Net fluxes: 
$$\begin{aligned} & \int_0^{l_y} \int_0^{l_z} q_{c,x} \big|_{x=0} dy dz - \int_0^{l_y} \int_0^{l_z} q_{c,x} \big|_{x=l_x} dy dz \\ & + \int_0^{l_x} \int_0^{l_z} q_{c,y} \big|_{y=0} dx dz - \int_0^{l_x} \int_0^{l_z} q_{c,y} \big|_{y=l_y} dx dz \\ & + \int_0^{l_x} \int_0^{l_y} q_{c,z} \big|_{z=0} dx dy - \int_0^{l_x} \int_0^{l_y} q_{c,z} \big|_{z=l_z} dx dy \end{aligned}$$

# Solute transport under saturated flow

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$$\Rightarrow - \int_{\partial \Omega} \underline{\underline{q}}_c \cdot \underline{\underline{n}} \, dS = - \int_{\Omega} \nabla \cdot \underline{\underline{q}}_c \, dV \quad \text{Divergence theorem}$$

$$\Rightarrow \frac{\partial}{\partial t} \int_{\Omega} \phi c \, dV = - \int_{\Omega} \nabla \cdot \underline{\underline{q}}_c \, dV$$

$\downarrow \Omega \neq \Omega(t)$

$$\Rightarrow \int_{\Omega} \frac{\partial}{\partial t} (\phi c) \, dV = - \int_{\Omega} \nabla \cdot \underline{\underline{q}}_c \, dV$$

$$\Rightarrow \int_{\Omega} \left( \frac{\partial}{\partial t} (\phi c) + \nabla \cdot \underline{\underline{q}}_c \right) dV = 0$$

$\downarrow \Omega$  is arbitrary

$$\left. \begin{aligned} \Rightarrow \frac{\partial}{\partial t} (\phi c) + \nabla \cdot \underline{\underline{q}}_c &= 0 \\ \underline{\underline{q}}_c &= \underline{\underline{q}}^c - \phi \underline{\underline{D}} \nabla c \end{aligned} \right\} \Rightarrow \boxed{\frac{\partial}{\partial t} (\phi c) + \nabla \cdot (\underline{\underline{q}}^c) - \nabla \cdot (\phi \underline{\underline{D}} \nabla c) = 0}$$

General 3D governing equation for  
solute transport in porous media.

# Air-water system in capillary tubes

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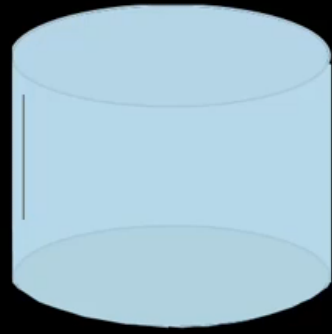
1. Why does the water try to hold together?
2. Why does the water not wet the surface?

# Air-water system in capillary tubes

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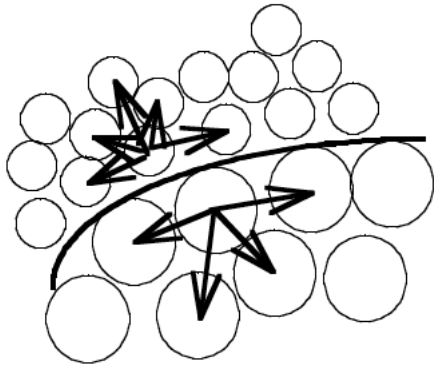
**SURFACE  
TENSION**



Link to the video: <https://youtu.be/zMzqiAuOSz0>

# Air-water system in capillary tubes

- Two and three phase systems: water, oil, air
- *Interfacial tension (cohesive forces between fluid molecules)*

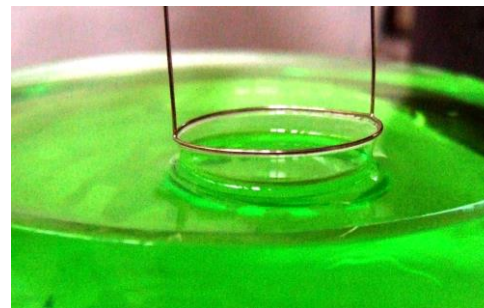


How to measure interfacial tension?

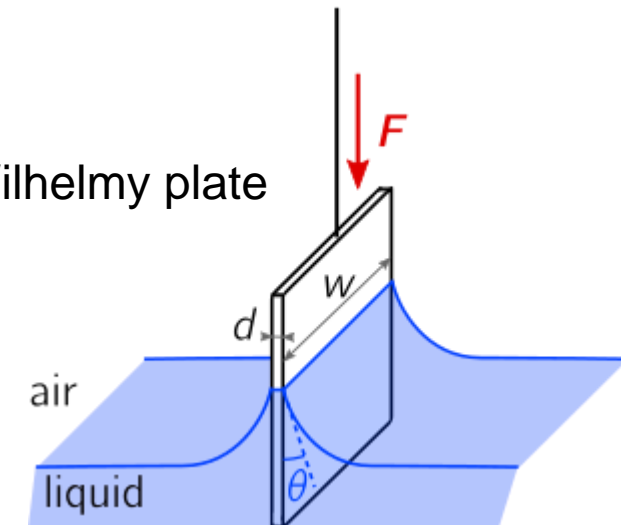
Drop weight  
method



ring method



Wilhelmy plate



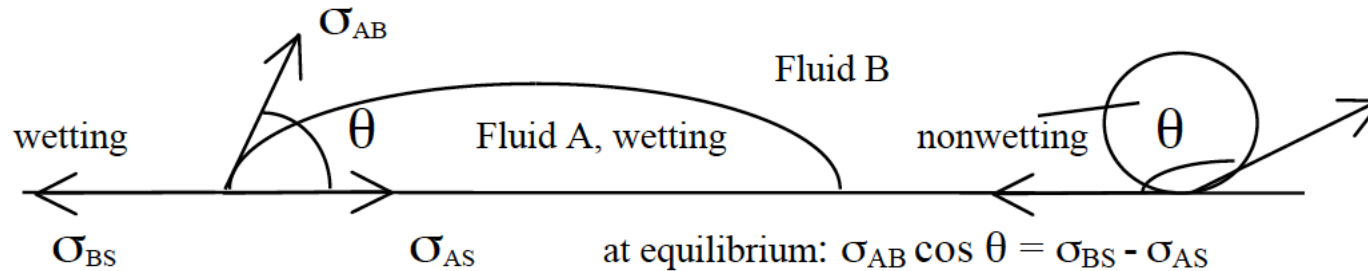
Typical values of surface tension:

air-water	0.072 N/m
oil-water	0.20 N/m
oil-water w/ soap	0.0001 N/m



# Air-water system in capillary tubes

- Wettability (adhesive forces between the fluid and solid surface)



$\theta < 90^\circ$ : fluid A is wetting with respect to fluid B on the solid S

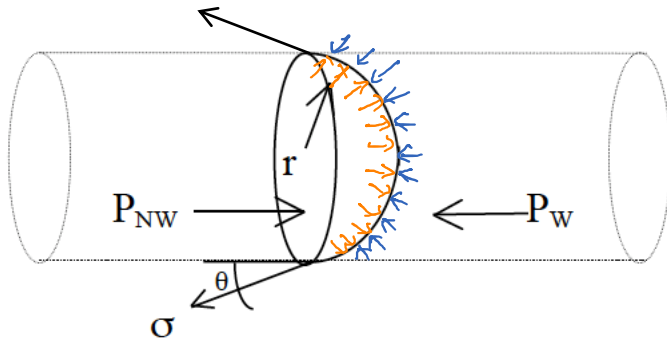
$\theta > 90^\circ$ : fluid A is nonwetting with respect to fluid B on the solid S

Wettability is a function of the fluid properties, soil properties, and history of contact. For most soils, the relative wettabilities are: water > oil > air

Recommended video for the concepts of *viscosity, cohesive and adhesive forces, surface tension, and capillary action* [https://www.youtube.com/watch?v=P\\_jQ1B9UwpU](https://www.youtube.com/watch?v=P_jQ1B9UwpU)

# Air-water system in capillary tubes

Capillary pressure (difference between the nonwetting and wetting phase pressures)



Force balance at equilibrium:

$$2\pi r \sigma \cos \theta = \pi r^2 P_{nw} - \pi r^2 P_w \Rightarrow P_{nw} - P_w = \frac{2\sigma \cos \theta}{r}$$

$$\Rightarrow \boxed{P_c = \frac{2\sigma \cos \theta}{r}} \quad \text{Young-Laplace Equation.}$$

1°. More general equation for any nw-w interface:  $P_c = \sigma \left( \frac{1}{r_1} + \frac{1}{r_2} \right)$

2°. For a perfectly wetting fluid,  $P_c = \frac{2\sigma}{r}$   
( $\theta = 0$ )

For the capillary tube:  
 $r_1 = r_2 = r / \cos \theta$