

HWRS 505: Vadose Zone Hydrology

Lecture 4

9/5/2024

Today:

1. Wrap up the review of solute transport under saturated flow
2. Air-water system in capillary tubes

Solute transport under saturated flow

HWRS 505
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Fall 2024

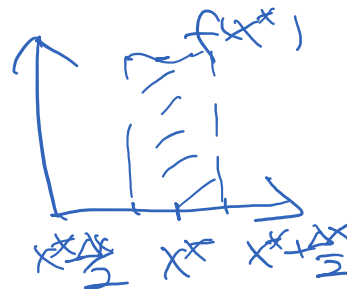
Review of Lecture 3

- ❖ Derivation of 3D transient groundwater flow.
- ❖ Solute transport under saturated flow.
 - Advection ($\mathbf{v} = \mathbf{q}/\phi$)
 - Molecular diffusion
 - Mechanical dispersion

"The dispersion coefficient is a lumped fitting parameter that adequately describes relatively large-scale observations."



$$\begin{aligned} \mathbf{q}_c &= \phi(\mathbf{v}C - \mathbf{D}\nabla C) \\ &= \mathbf{q}C - \phi\mathbf{D}\nabla C \end{aligned}$$



$$\begin{aligned} &\left\{ \int_V \left[\frac{\partial}{\partial t}(\rho\phi) + \nabla \cdot \mathbf{q} \right] dV = 0 \right. \\ &\quad \swarrow \text{arbitrary} \\ &\Rightarrow \frac{\partial}{\partial t}(\rho\phi) + \nabla \cdot \mathbf{q} = 0 \end{aligned}$$

$$\int_0^L f(x) dx = 0 \quad [0, L] \text{ arbitrary}$$

Suppose $\underline{f(x^*) \neq 0}$

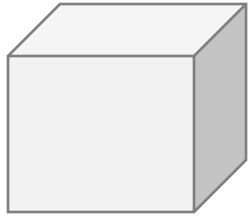
$$\lim_{\Delta x \rightarrow 0} \int_{x^* - \Delta x/2}^{x^* + \Delta x/2} f(x) dx = f(x^*) \Delta x = 0$$

$\underline{f(x^*) = 0}$

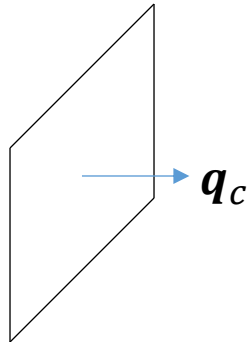
$\Rightarrow f(x^*) = 0$ contradicts $\underline{f(x^*) \neq 0}$

$\Rightarrow f(x) = 0$ everywhere

Solute transport under saturated flow

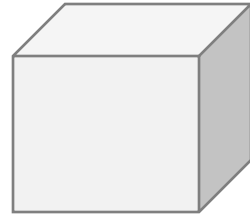


Saturated
porous medium

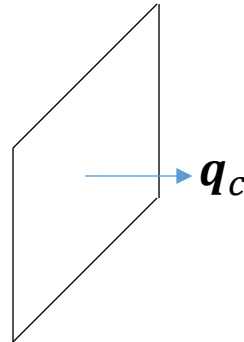


$$\begin{aligned} \mathbf{q}_c &= \phi(\mathbf{v}C - \mathbf{D}\nabla C) \\ &= \mathbf{q}C - \phi\mathbf{D}\nabla C \end{aligned}$$

$$\mathbf{D} = \alpha_T |\mathbf{v}| + (\alpha_L - \alpha_T) \frac{\mathbf{v}\mathbf{v}}{|\mathbf{v}|} + \omega D_0 \mathbf{I}$$

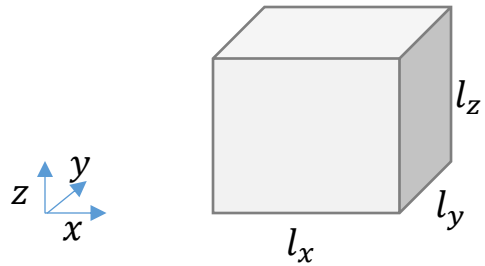


Fluid only
(e.g., free water)



$$\mathbf{q}_c = \mathbf{v}C - D_0\nabla C$$

Solute transport under saturated flow



$$C(x, y, z, t) = \frac{\text{mass of solute}}{\text{unit fluid volume}}$$

Mass conservation: Change of mass storage = mass in – mass out.

Rate of mass change:
$$\frac{d}{dt} \int_0^{l_x} \int_0^{l_y} \int_0^{l_z} \phi C(x, y, z, t) dx dy dz = \frac{d}{dt} \int_V \phi C(\vec{x}, t) dV$$

Net fluxes:
$$\begin{aligned} & \int_0^{l_x} \int_0^{l_z} q_{c,x} \big|_{x=0} dy dz - \int_0^{l_y} \int_0^{l_z} q_{c,x} \big|_{x=l_x} dy dz \\ & + \int_0^{l_x} \int_0^{l_z} q_{c,y} \big|_{y=0} dx dz - \int_0^{l_x} \int_0^{l_z} q_{c,y} \big|_{y=l_y} dx dz \\ & + \int_0^{l_x} \int_0^{l_y} q_{c,z} \big|_{z=0} dx dy - \int_0^{l_x} \int_0^{l_y} q_{c,z} \big|_{z=l_z} dx dy \end{aligned}$$

Solute transport under saturated flow

$$\Rightarrow - \int_{\partial \Omega} \mathbf{q}_c \cdot \mathbf{n} dS = - \int_{\Omega} \nabla \cdot \mathbf{q}_c dV \quad \text{divergence theorem}$$

$$\Rightarrow \frac{\partial}{\partial t} \int_{\Omega} \phi c dV = - \int_{\Omega} \nabla \cdot \mathbf{q}_c dV$$

↓ $n \neq n(t)$

$$\int_{\Omega} \frac{\partial}{\partial t} \phi c dV = - \int_{\Omega} \nabla \cdot \mathbf{q}_c dV$$

$$\int_{\Omega} \left(\frac{\partial}{\partial t} \phi c + \nabla \cdot \mathbf{q}_c \right) dV = 0$$

↓ Ω is arbitrary

$$\Rightarrow \left. \begin{aligned} \frac{\partial}{\partial t} \phi c + \nabla \cdot \mathbf{q}_c &= 0 \\ \mathbf{q}_c &= \mathbf{q} c - \phi D \nabla c \end{aligned} \right\}$$

$$\frac{\partial}{\partial t} (\phi c) + \nabla \cdot (c \mathbf{q}) - \nabla \cdot (\phi D \nabla c) = 0$$

General 3D governing equation for
solute transport in porous media

Air-water system in capillary tubes

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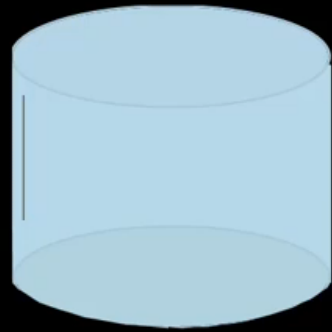


1. Why does the water try to hold together?
2. Why does the water not wet the surface?

Air-water system in capillary tubes

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**SURFACE
TENSION**



Link to the video: <https://youtu.be/zMzqiAuOSz0>

Air-water system in capillary tubes

- Two and three phase systems: water, oil, air
- *Interfacial tension (cohesive forces between fluid molecules)*

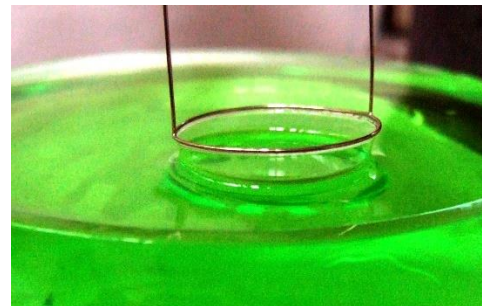


How to measure interfacial tension?

Drop weight method



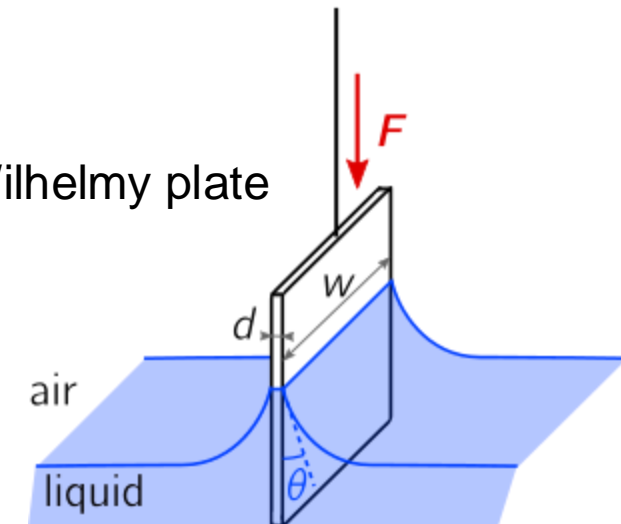
ring method



Typical values of surface tension:

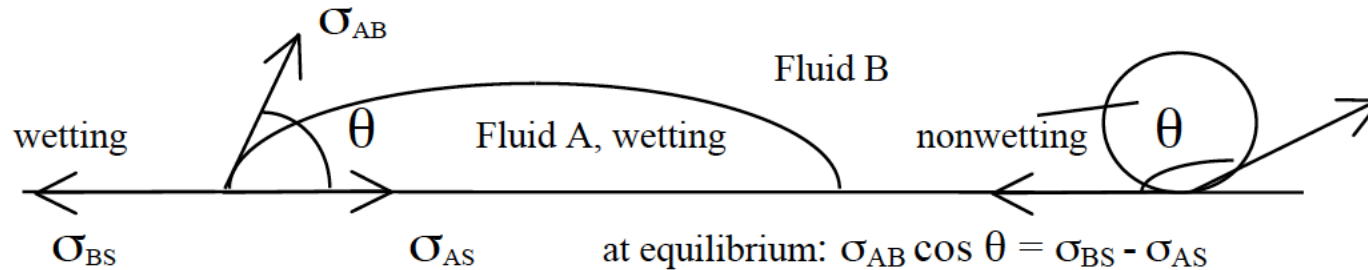
air-water	0.072 N/m
oil-water	0.20 N/m
oil-water w/ soap	0.0001 N/m

Wilhelmy plate



Air-water system in capillary tubes

- *Wettability (adhesive forces between the fluid and solid surface)*



$\theta < 90^\circ$: fluid A is wetting with respect to fluid B on the solid S

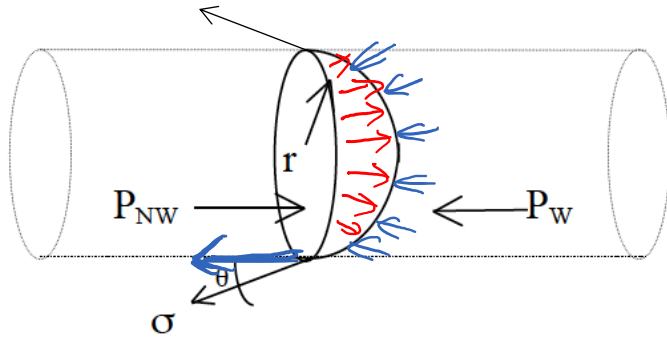
$\theta > 90^\circ$: fluid A is nonwetting with respect to fluid B on the solid S

Wettability is a function of the fluid properties, soil properties, and history of contact. For most soils, the relative wettabilities are: water > oil > air

Recommended video for the concepts of *viscosity, cohesive and adhesive forces, surface tension, and capillary action* https://www.youtube.com/watch?v=P_jQ1B9UwpU

Air-water system in capillary tubes

Capillary pressure (difference between the nonwetting and wetting phase pressures)



Force balance at equilibrium:

$$\pi r^2 P_{NW} - \pi r^2 P_W = 2\pi r \sigma \cos \theta$$

$$P_{NW} - P_W = \frac{2\sigma \cos \theta}{r}$$

$$P_c = \frac{2\sigma \cos \theta}{r}$$

Young-Laplace Equation

1. more general equation
for any m-n interface

$$P_c = \sigma \left(\frac{1}{r_1} + \frac{1}{r_2} \right)$$



For the capillary tube: $r_1 = r_2 = \frac{r}{\cos \theta}$

2. For a perfectly wetting fluid

$$\theta = 0, \quad P_c = \frac{2\sigma}{r}$$