Chapter 2

Finite Element Equations for Heat Transfer

Abstract Solution of heat transfer problems is considered. Finite element equations are obtained using the Galerkin method. The conductivity matrix for a triangular finite element is calculated.

2.1 Problem Statement

Let us consider an isotropic body with temperature-dependent heat transfer. A basic equation of heat transfer has the following form [15]:

$$-\left(\frac{\partial q_x}{\partial x} + \frac{\partial q_y}{\partial y} + \frac{\partial q_z}{\partial z}\right) + Q = \rho c \frac{\partial T}{\partial t}.$$
 (2.1)

Here, q_x , q_y and q_z are components of heat flow through the unit area; Q = Q(x,y,z,t) is the inner heat-generation rate per unit volume; ρ is material density; c is heat capacity; T is temperature and t is time. According to Fourier's law the components of heat flow can be expressed as follows:

$$q_{x} = -k \frac{\partial T}{\partial x},$$

$$q_{y} = -k \frac{\partial T}{\partial y},$$

$$q_{z} = -k \frac{\partial T}{\partial z},$$
(2.2)

where *k* is the thermal-conductivity coefficient of the media. Substitution of Fourier's relations gives the following basic heat transfer equation:

$$\frac{\partial}{\partial x} \left(k \frac{\partial T}{\partial x} \right) + \frac{\partial}{\partial y} \left(k \frac{\partial T}{\partial y} \right) + \frac{\partial}{\partial z} \left(k \frac{\partial T}{\partial z} \right) + Q = \rho c \frac{\partial T}{\partial t}. \tag{2.3}$$

It is assumed that the *boundary conditions* can be of the following types:

1. Specified temperature

$$T_{\rm s} = T_1(x,y,z,t)$$
 on S_1 .

2. Specified heat flow

$$q_x n_x + q_y n_y + q_z n_z = -q_s$$
 on S_2 .

3. Convection boundary conditions

$$q_x n_x + q_y n_y + q_z n_z = h(T_s - T_e)$$
 on S_3 ,

4. Radiation

$$q_x n_x + q_y n_y + q_z n_z = \sigma \varepsilon T_s^4 - \alpha q_r \text{ on } S_4$$

where h is the convection coefficient; T_s is an unknown surface temperature; T_e is a convective exchange temperature; σ is the Stefan–Boltzmann constant; ε is the surface emission coefficient; α is the surface absorption coefficient, and q_r is the incident radiant heat flow per unit surface area. For transient problems it is necessary to specify an initial temperature field for a body at the time t = 0:

$$T(x, y, z, 0) = T_0(x, y, z).$$
 (2.4)

2.2 Finite Element Discretization of Heat Transfer Equations

A domain V is divided into finite elements connected at nodes. We shall write all the relations for a finite element. Global equations for the domain can be assembled from finite element equations using connectivity information.

Shape functions N_i are used for interpolation of temperature inside a finite element:

$$T = [N]\{T\},$$

 $[N] = [N_1 \ N_2 \ ...],$
 $\{T\} = \{T_1 \ T_2 \ ...\}.$ (2.5)

Differentiation of the temperature-interpolation equation gives the following interpolation relation for temperature gradients:

Here, $\{T\}$ is a vector of temperatures at nodes, [N] is a matrix of shape functions, and [B] is a matrix for temperature-gradient interpolation.

Using the Galerkin method, we can rewrite the basic heat transfer equation in the following form:

$$\int_{V} \left(\frac{\partial q_x}{\partial x} + \frac{\partial q_y}{\partial y} + \frac{\partial q_z}{\partial z} - Q + \rho c \frac{\partial T}{\partial t} \right) N_i dV = 0.$$
 (2.7)

Applying the divergence theorem to the first three terms, we arrive at the relations:

$$\int_{V} \rho c \frac{\partial T}{\partial t} N_{i} dV - \int_{V} \left[\frac{\partial N_{i}}{\partial x} \frac{\partial N_{i}}{\partial y} \frac{\partial N_{i}}{\partial z} \right] \{q\} dV$$

$$= \int_{V} Q N_{i} dV - \int_{S} \{q\}^{T} \{n\} N_{i} dS,$$

$$\{q\}^{T} = \left[q_{x} \ q_{y} \ q_{z} \right],$$

$$\{n\}^{T} = \left[n_{x} \ n_{y} \ n_{z} \right],$$
(2.8)

where $\{n\}$ is an outer normal to the surface of the body. After insertion of boundary conditions into the above equation, the discretized equations are as follows:

$$\int_{V} \rho c \frac{\partial T}{\partial t} N_{i} dV - \int_{V} \left[\frac{\partial N_{i}}{\partial x} \frac{\partial N_{i}}{\partial y} \frac{\partial N_{i}}{\partial z} \right] \{q\} dV$$

$$= \int_{V} Q N_{i} dV - \int_{S_{1}} \{q\}^{T} \{n\} N_{i} dS$$

$$+ \int_{S_{2}} q_{s} N_{i} dS - \int_{S_{3}} h(T - T_{e}) N_{i} dS - \int_{S_{4}} (\sigma \varepsilon T^{4} - \alpha q_{r}) N_{i} dS.$$
(2.9)

It is worth noting that

$${q} = -k[B]{T}.$$
 (2.10)

The discretized finite element equations for heat transfer problems have the following form:

$$[C]\{\dot{T}\} + ([K_c] + [K_h] + [K_r])\{T\}$$

$$= \{R_T\} + \{R_Q\} + \{R_q\} + \{R_h\} + \{R_r\},$$
(2.11)

$$[C] = \int_{V} \rho c[N]^{T}[N]dV,$$

$$[K_{c}] = \int_{V} k[B]^{T}[B]dV,$$

$$[K_{h}] = \int_{S_{3}} h[N]^{T}[N]dS,$$

$$[K_{r}]\{T\} = \int_{S_{4}} \sigma \varepsilon T^{4}[N]^{T}dS,$$

$$\{R_{T}\} = -\int_{S_{1}} \{q\}^{T}\{n\}[N]^{T}dS,$$

$$\{R_{Q}\} = \int_{V} Q[N]^{T}dV,$$

$$\{R_{q}\} = \int_{S_{2}} q_{s}[N]^{T}dS,$$

$$\{R_{h}\} = \int_{S_{3}} hT_{e}[N]^{T}dS,$$

$$\{R_{r}\} = \int_{S_{4}} \alpha q_{r}[N]^{T}dS.$$

Here, $\{\dot{T}\}$ is a nodal vector of temperature derivatives with respect to time.

2.3 Different Type Problems

Equations for different types of problems can be deducted from the above general equation:

Stationary linear problem

$$([K_c] + [K_h])\{T\} = \{R_Q\} + \{R_q\} + \{R_h\}.$$
(2.13)

Stationary nonlinear problem

$$([K_c] + [K_h] + [K_r]) \{T\}$$

$$= \{R_O(T)\} + \{R_o(T)\} + \{R_h(T)\} + \{R_r(T)\}.$$
(2.14)

Transient linear problem

$$[C]{\dot{T}(t)} + ([K_c] + [K_h(t)]){T(t)}$$

$$= {R_O(t)} + {R_q(t)} + {R_h(t)}.$$
(2.15)

Transient nonlinear problem

$$[C(T)]\{\dot{T}\} + ([K_c(T)] + [K_h(T,t)] + [K_r(T)])\{T\}$$

$$= \{R_Q(T,t)\} + \{R_q(T,t)\} + \{R_h(T,t)\} + \{R_r(T,t)\}.$$
(2.16)

2.4 Triangular Element

Calculation of element conductivity matrix $[k_c]$ and heat flow vector $\{r_q\}$ is illustrated for a two-dimensional triangular element with three nodes. A simple triangular finite element is shown in Figure 2.1. The temperature distribution T(x,y) inside the triangular element is described by linear interpolation of its nodal values:

$$T(x,y) = N_1(x,y)T_1 + N_2(x,y)T_2 + N_3(x,y)T_3,$$

$$N_i(x,y) = \alpha_i + \beta_i x + \gamma_i y.$$
(2.17)

Interpolation functions (usually called shape functions) $N_i(x,y)$ should satisfy the following conditions:

$$T(x_i, y_i) = T_i, \quad i = 1, 2, 3.$$
 (2.18)

Solution of the above equation system provides expressions for the shape functions:

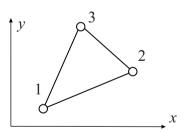


Fig. 2.1 Triangular finite element

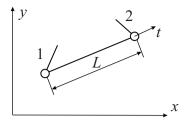


Fig. 2.2 Integration along an element side

$$N_{i} = \frac{1}{2\Delta} (a_{i} + b_{i}x + c_{i}y),$$

$$a_{i} = x_{i+1}y_{i+2} - x_{i+2}y_{i+1},$$

$$b_{i} = y_{i+1} - y_{i+2},$$

$$c_{i} = x_{i+2} - x_{i+1},$$

$$\Delta = \frac{1}{2} (x_{2}y_{3} + x_{3}y_{1} + x_{1}y_{2} - x_{2}y_{1} - x_{3}y_{2} - x_{1}y_{3}),$$

$$(2.19)$$

where Δ is the element area.

The conductivity matrix of the triangular element is determined by integration over element area A (assuming that the element has unit thickness),

$$[k_c] = \int_A k[B]^{\mathrm{T}}[B] dx dy. \tag{2.20}$$

The temperature differentiation matrix [B] has expression

$$[B] = \begin{bmatrix} \frac{\partial N_1}{\partial x} & \frac{\partial N_2}{\partial x} & \frac{\partial N_3}{\partial x} \\ \frac{\partial N_1}{\partial y} & \frac{\partial N_2}{\partial y} & \frac{\partial N_3}{\partial y} \end{bmatrix} = \frac{1}{2\Delta} \begin{bmatrix} b_1 & b_2 & b_3 \\ c_1 & c_2 & c_3 \end{bmatrix}.$$
(2.21)

Since the temperature differentiation matrix does not depend on coordinates, integration of the conductivity matrix is simple;

$$[k_c] = \frac{k}{4\Delta} \begin{bmatrix} b_1^2 + c_1^2 & b_1b_2 + c_1c_2 & b_1b_3 + c_1c_3 \\ b_1b_2 + c_1c_2 & b_2^2 + c_2^2 & b_2b_3 + c_2c_3 \\ b_1b_3 + c_1c_3 & b_2b_3 + c_2c_3 & b_3^2 + c_3^2 \end{bmatrix}.$$
(2.22)

The heat-flow vector $\{r_q\}$ is evaluated by integration over the element side, as shown in Figure 2.2

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$$\{r_q\} = -\int_L q_s[N]^{\mathsf{T}} dL = -\int_0^1 q_s[N_1 N_2]^{\mathsf{T}} L dt.$$
 (2.23)

Here, integration over an element side L is replaced by integration using variable t ranging from 0 to 1. Shape functions N_1 and N_2 on element side 1–2 can be expressed through t:

$$N_1 = 1 - t, \quad N_2 = t.$$
 (2.24)

After integration with substituting integration limits, the heat-flow vector equals

$$\{r_q\} = -q_s \frac{L}{2} \begin{bmatrix} 1\\1 \end{bmatrix}. \tag{2.25}$$

Element matrices and vectors are calculated for all elements in a mesh and assembled into the global equation system. After application of prescribed temperatures, solution of the global equation system produces temperatures at nodes.

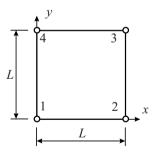
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2.1. Calculate matrix $[k_h]$ describing convection boundary conditions

$$[k_h] = \int_{L} h[N]^{\mathrm{T}}[N] dL$$

for a side of a triangular element (see Figure 2.2).

2.2. Obtain shape functions N_1 , N_2 , N_3 and N_4 for the square element shown below.



Assume that its size is L = 1 and that shape functions can be represented as $N_i = a_1(a_2 + x)(a_3 + y)$.

2.3. For the square element of the previous problem, estimate the heat-generation vector

$$\{r_Q\} = \int\limits_V Q[N]^{\mathrm{T}} dV.$$

Use the shape functions obtained in the previous problem.



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