

# Derivations

## 1 Heat Transfer Equation

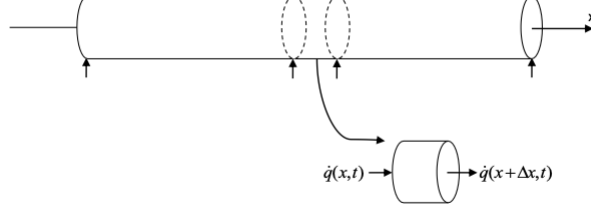


Figure 1: Diagram of a one-dimensional heat rod with its axis along the x-axis

Start with the conservation of energy expressed as:

$$\dot{Q}_{in}(x, t) = \dot{Q}_{out}(x + \Delta x, t) + \dot{Q}_{stored} \quad (1)$$

where

$$\dot{Q}_{in}(x, t) = \dot{q}_{in}(x, t)A \quad [W] \quad (2)$$

$$\dot{Q}_{out}(x, t) = \dot{q}_{out}(x, t)A \quad [W] \quad (3)$$

The rate of energy that is stored in a unit cross-section of the material can be defined as the product of the specific heat, mass, and change in temperature with respect to time.

$$Q = mc_p \Delta T \quad [J] \quad (4)$$

The mass of the material can be written as the product of the density and volume.

$$m = \rho V = \rho A \Delta x \quad [kg] \quad (5)$$

Plugging the mass equation into the rate of heat energy equation,  $\dot{Q}_{stored}$  can be expressed as:

$$\dot{Q}_{stored}(x, t) = \rho c_p A \Delta x \frac{\partial u(x, t)}{\partial t} \quad [W] \quad (6)$$

where  $u(x, t)$  is a unique solution to the heat equation.

From here, apply all the equations of the rate of heat energy to the conservation of energy, which yields:

$$\dot{q}_{in}(x, t) = \dot{q}_{out}(x + \Delta x, t) + \rho c_p \Delta x \frac{\partial u(x, t)}{\partial t} \quad [W] \quad (7)$$

Rearrange the above equation:

$$\frac{\dot{q}_{in}(x, t) - \dot{q}_{out}(x + \Delta x, t)}{\Delta x} = \rho c_p \Delta x \frac{\partial u(x, t)}{\partial t} \quad (8)$$

Simplify the left-hand term as the length of the element goes to zero:

$$\frac{\dot{q}_{in}(x, t) - \dot{q}_{out}(x + \Delta x, t)}{\Delta x} = \rho c_p \Delta x \frac{\partial u(x, t)}{\partial t} \quad (9)$$

$$\lim_{\Delta x \rightarrow 0} \frac{\dot{q}_{in}(x, t) - \dot{q}_{out}(x + \Delta x, t)}{\Delta x} = - \frac{\partial \dot{q}(x, t)}{\partial t} \quad (10)$$

Since only one dimension is considered, it turns out that the conservation of energy is simplified as below:

$$- \frac{\partial \dot{q}(x, t)}{\partial t} = \rho c_p \frac{\partial u(x, t)}{\partial t} \quad (11)$$

Additionally, Fourier's Law of Heat Conduction defines heat flux as the negative of the product of the thermal conductivity,  $k$ , and the change in

## 2 Steady State Solution

- An initial condition for the temperature distribution  $f(x)$

$$u(x, 0) = f(x) \quad \text{at} \quad 0 < x < L, \quad t = 0 \quad (16)$$

- A fixed temperature boundary condition at the beginning of the rod

$$u(0, t) = T_0 = A \quad \text{at} \quad x = 0 \quad (17)$$

- A steady state heat flow rate at the end of the rod

$$\frac{\partial u(L, t)}{\partial x} = H = \frac{\dot{Q}}{kA} = B \quad \text{at} \quad x = L \quad (18)$$

- A steady state solution

$$\frac{d^2 v(x)}{dx^2} = 0 \quad \text{when} \quad 0 \leq x \leq L \quad (19)$$

Considering these initial and boundary conditions, the steady-state solution can be described as:

$$v(x) = A + Bx \quad (20)$$

$$v(x) = T_0 + Hx \quad [^\circ C] \quad (21)$$

where

$$H = \frac{\dot{Q}}{kA} \quad [^\circ C/m] \quad (22)$$

\*In this lab, the system is treated as the steady-state as the time goes to infinity. Thus, the heat transfer equation is only a function of the location of the rod.

## 3 Transient Solution

The steady-state solution does not describe the entire equation of the temperature change. Therefore, the transient solution  $w(x, t)$  needs to be taken into account to describe the complete temperature change  $u(x, t)$ .

$$u(x, t) = w(x, t) + v(x) \quad (23)$$

To start with, initial and boundary conditions have to be set. For the initial condition, it can be said:

$$u(x, 0) = w(x, 0) + v(x) = f(x) \quad (24)$$

For the boundary conditions,

- As one of the assumptions, the temperature at the beginning of the rod is constant over time. Therefore,

$$u(0, t) = w(0, t) + v(0) = T_0 \quad (25)$$

- The derivative of  $w(L, t)$  must be zero

$$\frac{\partial u(L, t)}{\partial x} = \frac{\partial w(L, t)}{\partial x} + \frac{\partial v(L)}{\partial x} = H \quad (26)$$

Using the separation of variables and Fourier Series based on these initial and boundary conditions, the temperature at a given point in time and along the rod can be defined as follows:

$$u(x, t) = T_0 + Hx + \sum_{n=1}^{\infty} b_n \sin(\lambda_n x) e^{-\lambda_n^2 \alpha t} \quad [^{\circ}C] \quad (27)$$

where

$$\lambda_n = \frac{(2n-1)\pi}{2L} \quad \text{where } n = 1, 2, 3, \dots \quad (28)$$

$$b_n = -\frac{2H}{L} \int_0^L x \sin(\lambda_n x) dx \quad (29)$$