

EX_5

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EX 5.1

(a)

(b)

EX 5.2

EX 5.3

(a)

(b)

(c)

EX 5.4

(a)

(b)

EX 5.5

EX 5.6

EX 5.7

EX 5.1

A garden hose attached with a nozzle is used to fill a 10-gal bucket. The inner diameter of the hose is 2 cm, and it reduces to 0.8 cm at the nozzle exit. If it takes 50 s to fill the bucket with water.

Determine (a) the volume and mass flow rates of water through the hose, and (b) the average velocity of water at the nozzle exit.

(a)

$$\begin{aligned}\dot{V} &= \frac{V}{\Delta t} = \frac{10 \text{ gal}}{50 \text{ s}} \cdot \frac{3.7854 \text{ L}}{1 \text{ gal}} \\ &= 0.757 \text{ L/s} \\ \dot{m} &= \rho \dot{V} \\ &= 1 \text{ kg/L} \times 0.757 \text{ L/s} = 0.757 \text{ kg}\end{aligned}$$

(b)

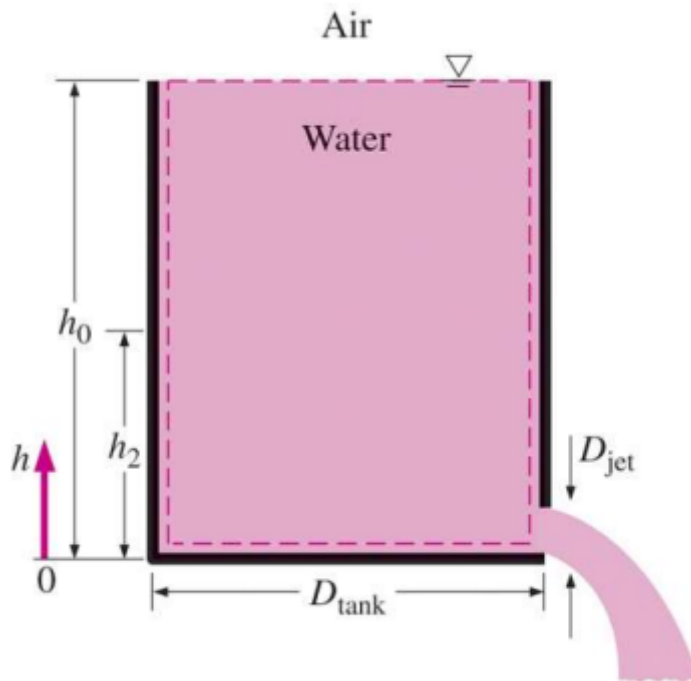
$$\begin{aligned}\dot{V} &= vS \\ v &= \frac{\dot{V}}{S} = \frac{7.57 \times 10^{-5} \text{ m}^3/\text{s}}{\frac{1}{4}\pi(8 \times 10^{-2})^2 \text{ m}^2} = 15.06 \text{ m/s}\end{aligned}$$

EX 5.2

A 4-ft-high, 3-ft-diameter cylindrical water tank whose top is open to the atmosphere is initially filled with water. Now the discharge plug near the bottom of the tank is pulled out, and a water jet whose diameter is 0.5 in stream out. The average velocity of the jet is given by $V = \sqrt{2gh}$ where h is the height of water in the tank measured from the center of the hole (a variable) and g

is the gravitational acceleration.

Determine how long it will drop to 2 *ft* from the bottom.



$$\dot{m}_{in} - \dot{m}_{out} = \frac{dm_{cv}}{dt}$$

$$-\dot{m}_{out} = \frac{dm_{cv}}{dt}$$

$$\rho A_{jet} \sqrt{2gh} = \frac{d(\rho A_{tank} h)}{dt}$$

$$dt = \frac{1}{\sqrt{2g}} \cdot \frac{A_{tank}}{A_{jet}} \cdot \frac{dh}{\sqrt{h}}$$

$$t = \frac{1}{\sqrt{2g}} \cdot \frac{D_{tank}^2}{D_{jet}^2} \int_{h_1}^{h_2} \frac{dh}{\sqrt{h}}$$

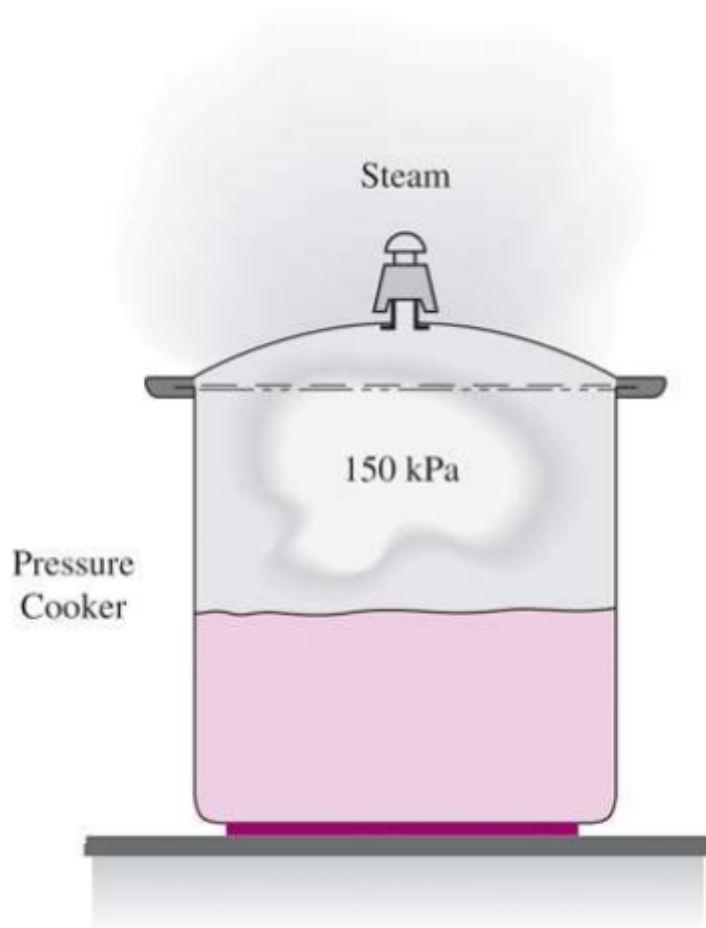
$$= \sqrt{\frac{2}{g}} \cdot \frac{D_{tank}^2}{D_{jet}^2} (\sqrt{h_1} - \sqrt{h_2})$$

$$= 756.8s$$

EX 5.3

Steam is leaving a 4 *L* pressure cooker whose operating pressure is 150 *kPa*. It is observed that the amount of liquid in the cooker has decreased by 0.6 *L* in 40 *min* after the steady operating conditions are established, and the cross-sectional area of the exit opening conditions are established, and the cross-sectional area of the exit opening is 8 *mm*².

Determine (a) the mass flow rate of the steam and exit velocity, (b) the total and flow energies of the steam per unit mass, and (c) the rate by steam



(a)

$$\Delta m = \frac{0.6L}{v_f} = \frac{0.0006m^3}{0.001053kg/m^3} = 0.57kg$$

$$\dot{m} = \frac{\Delta m}{\Delta t} = \frac{0.57kg}{40min} = 2.375 \times 10^{-4}kg/s$$

$$v = \frac{\dot{m}}{\rho_{air}A} = \frac{\dot{m}v_g}{A} = \frac{2.375 \times 10^{-4}kg/s \times 1.1594}{8 \times 10^{-6}} = 34.42m/s$$

(b)

$$\theta = h + ke + pe$$

$$= h + v^2/2 = 2936.1 + 0.592 \approx 2936.7kJ$$

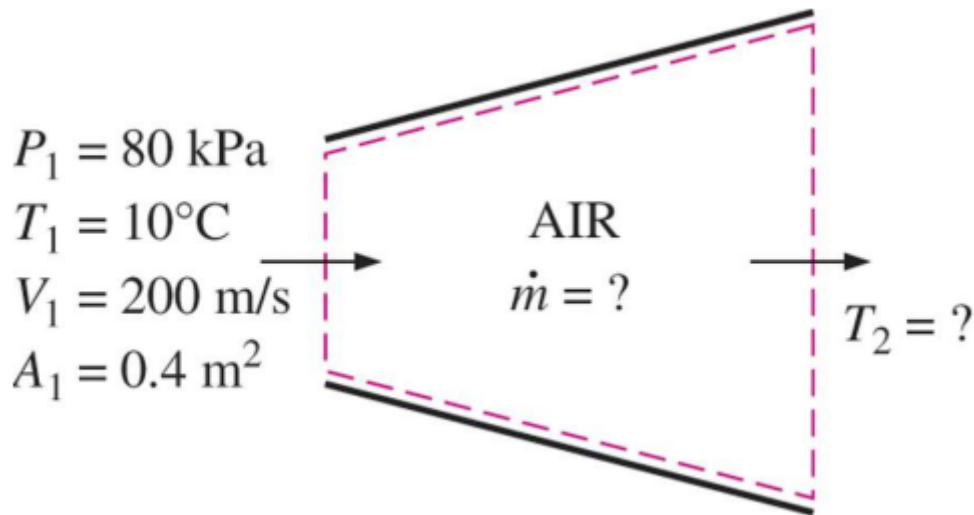
(c)

$$\dot{E}_{mass} = \dot{m}\theta = 0.697kW$$

EX 5.4

Air at $10^\circ C$ and $80 kPa$ enters the diffuser of a jet engine steadily with a velocity of $200 m/s$. The inlet area of the diffuser is $0.4 m^2$. The air leaves the diffuser with a velocity that is very small compared with the inlet velocity.

Determine (a) the mass flow rate of the air and (b) the temperature of the air leaving the diffuser.



(a)

$$P_1 V = m R T_1$$

$$v_1 = \frac{V}{m} = \frac{R T_1}{P_1} = \frac{0.2870 \text{ kJ/kg} \cdot \text{K} \times 283.15 \text{ K}}{80 \text{ kPa}}$$

$$= 1.016 \text{ m}^3/\text{kg}$$

$$\dot{m} = \frac{A_1 V_1}{v_1} = \frac{0.4 \text{ m}^2 \times 200 \text{ m/s}}{1.016 \text{ m}^3/\text{kg}} = 78.74 \text{ kg/s}$$

(b)

according to the model of the nozzle, the internal energy remain the same during the process.

Therefore, $h_1 + ke_1 = h_2 + ke_2$

$$h_1 = 283.14 \text{ kJ/kg}$$

$$ke_1 = V_1^2/2 = 20 \text{ kJ/kg}$$

$$ke_2 \cong 0 \text{ kJ/kg}$$

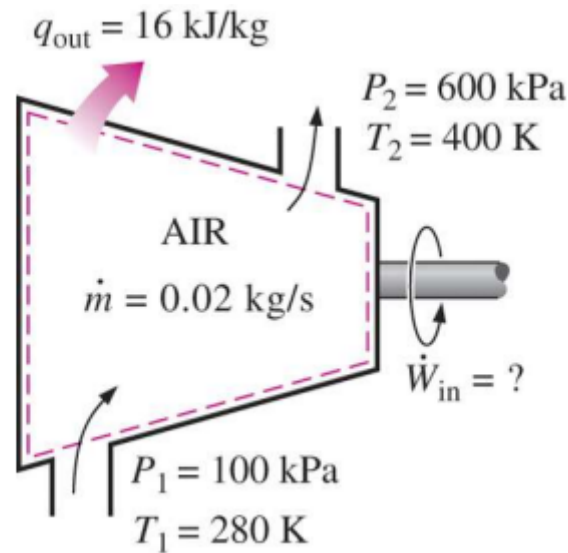
$$h_2 = 303.14 \text{ kJ/kg}$$

where the temperature of the enthalpy equals to 302.9 K

EX 5.5

Air at 100 kPa and 280 K is compressed steadily to 600 kPa and 400 K . The mass flow rate of the air is 0.02 kg/s , and a heat loss of 16 kJ/kg occurs during the process. Assuming the changes in kinetic and potential energies are negligible.

Determine the necessary power input to the compressor.

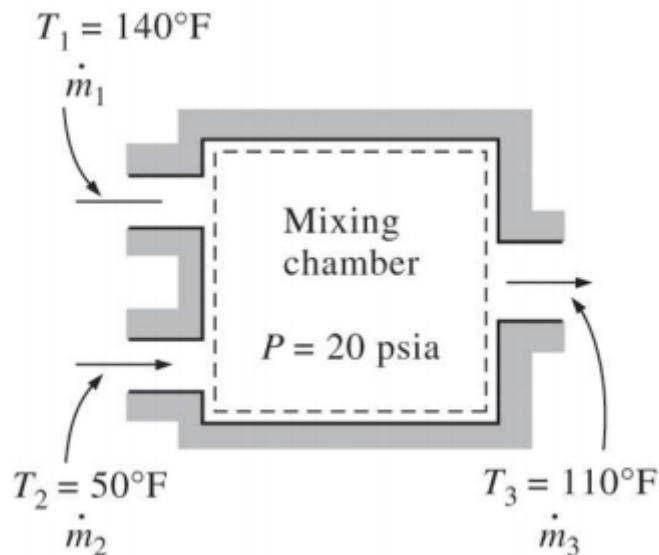


According to the model of the turbine, we could simply get the equation $h_1 + Q_{out} = h_2 + W$

$$\begin{aligned}
 \dot{W} &= \dot{m}q_{out} + \dot{m}(h_2 - h_1) \\
 &= 0.02 \times (16 + 400.98 - 280.13) \\
 &= 2.737 \text{ kW}
 \end{aligned}$$

EX 5.6

Consider an ordinary shower where hot water at 140°F is mixed with cold water at 50°F . If it is desired that a steady stream of warm water at 110°F be supplied, determine the ratio of the mass flow rates of the hot to cold water. Assume the heat losses from the mixing chamber to be negligible and the mixing to take place at a pressure of 20 psia



since there's no change in the internal energy and all temperatures are below the saturated temperature, we can get the conclusion that $\dot{m}_1 h_1 + \dot{m}_2 h_2 = \dot{m}_3 h_3$

$$\dot{m}_1 h_1 + \dot{m}_2 h_2 = (\dot{m}_1 + \dot{m}_2) h_3$$

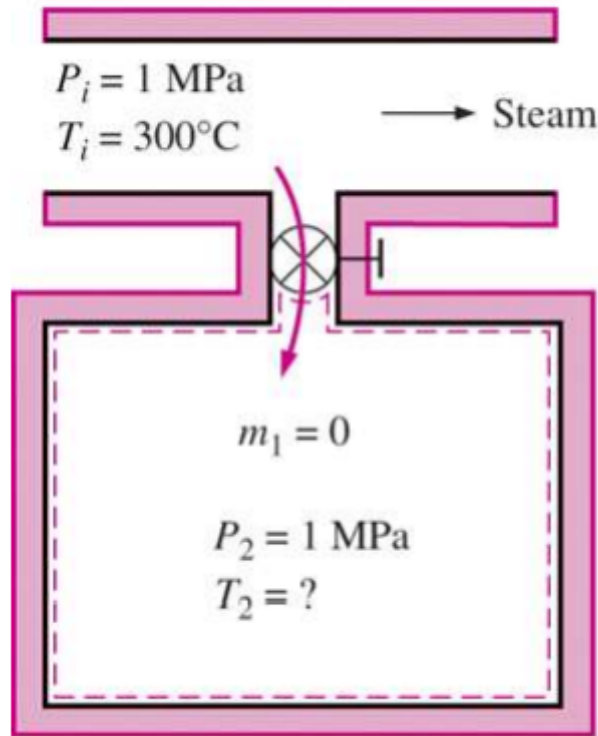
$$\frac{\dot{m}_1}{\dot{m}_2} h_1 + h_2 = \left(\frac{\dot{m}_1}{\dot{m}_2} + 1 \right) h_3$$

$$\frac{\dot{m}_1}{\dot{m}_2} = \frac{h_3 - h_2}{h_1 - h_3} = \frac{136.26 - 121.875}{143.47 - 136.26} = 2.00$$

EX 5.7

A rigid, insulated tank that is initially evacuated is connected through a valve to a supply line that carries steam at 1 MPa and 300°C . Now the valve is opened, and steam is allowed to flow slowly into the tank until the pressure reaches 1 MPa , at which point the valve is closed.

Determine the final temperature of the steam in the tank.



$$m_{in} + m_1 = m_2$$

$$m_{in}h_1 = m_2u_2$$

$$u_2 = h_2 = 3051.6 \text{ kJ/kg}$$

according to the table on Table A-6, get that the temperature equals to 456.07 K