

# CH\_5

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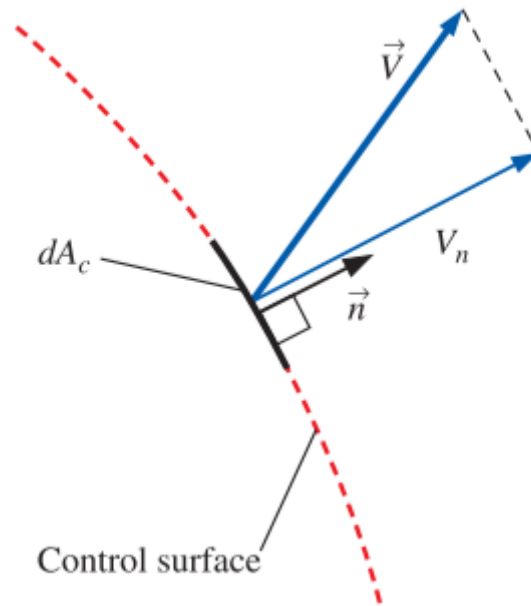
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## 5.1 Conversion of Mass

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### Mass and Volume Flow Rates

**mass flow rate**

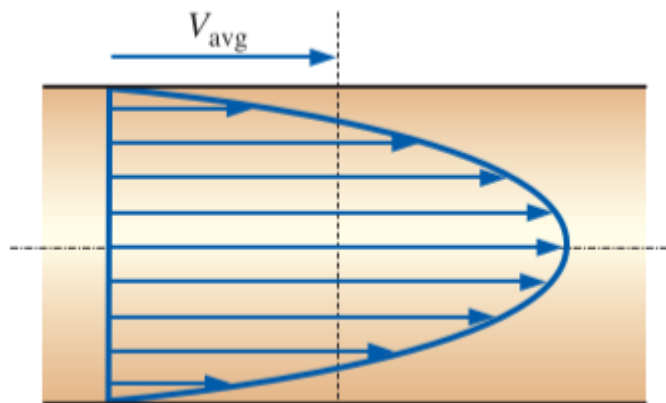


$$\delta \dot{m} = \rho V_n dA_c$$

$$\dot{m} = \int_{A_c} \delta \dot{m} = \int_{A_c} \rho V_n dA_c$$

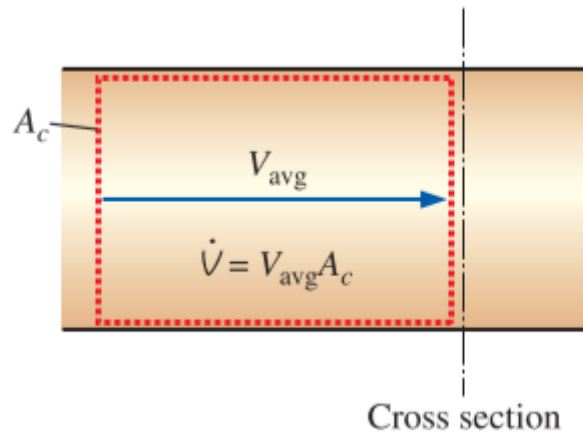
$$\dot{m} = \rho V_{avg} A_c$$

**average velocity**



$$V_{avg} = \frac{1}{A_c} \int_{A_c} V_n dA_c$$

**volume flow rate**



$$\dot{V} = \int_{A_c} V_n dA_c = V_{avg} A_c = V A_c$$

$$\dot{m} = \rho \dot{V} = \frac{\dot{V}}{\nu}$$

## Conversion of Mass Principle

mass balance

$$m_{in} - m_{out} = \Delta m_{CV}$$

$$\dot{m}_{in} - \dot{m}_{out} = \frac{dm_{CV}}{dt}$$

general conversion of mass

$$\frac{d}{dt} \int_{CV} \rho dV + \int_{CS} \rho (\vec{V} \cdot \vec{n}) dA = 0$$

$$\frac{d}{dt} \int_{CV} \rho dV = \sum_{in} \dot{m} - \sum_{out} \dot{m} \quad \frac{dm_{CV}}{dt} = \sum_{in} \dot{m} - \sum_{out} \dot{m}$$

## Mass Balance for Steady-Flow Processes

$$\sum_{in} \dot{m} = \sum_{out} \dot{m}$$

$$\rho_1 V_1 A_1 = \rho_2 V_2 A_2$$

## Special Case: Incompressible Flow

$$\sum_{in} \dot{V}_1 = \sum_{out} \dot{V}_2$$

$$V_1 A_1 = V_2 A_2$$

## 5.2 Flow Work and the Energy of a Flowing Fluid

$$w_{flow} = Pv$$

## Total Energy of a Flowing Fluid

the energy for the unit mass

$$e = u + ke + pe = u + \frac{V^2}{2} + gz$$

for the flowing fluid

$$\theta = Pv + e = (Pv + u) + ke + pe = h + \frac{V^2}{2} + gz$$

## Energy Transport by Mass

- Amount of energy transport:  $E_{mass} = m\theta = m(h + \frac{V^2}{2} + gz)$
- Rate of Energy transport:  $\dot{E}_{mass} = \dot{m}\theta = \dot{m}(h + \frac{V^2}{2} + gz)$

$$E_{in, mass} = \int_{m_i} \theta_i \delta m_i = \int_{m_i} (h_i + \frac{V_i^2}{2} + gz_i) \delta m_i$$

## 5.3 Energy Analysis of Steady-Flow Systems

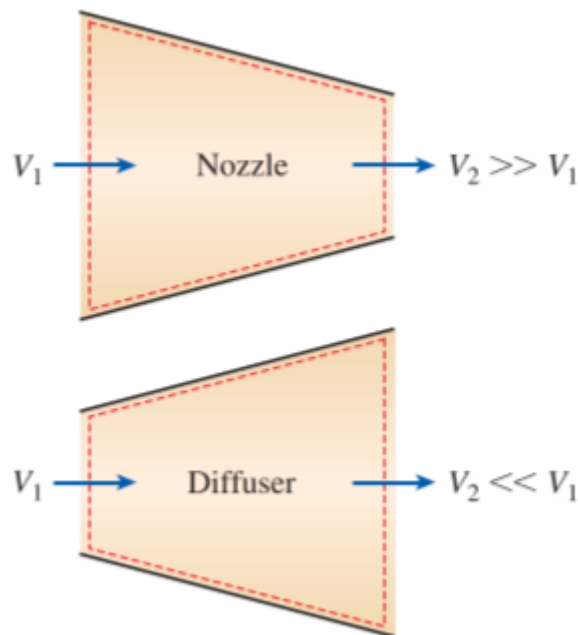
$$\dot{E}_{in} = \dot{E}_{out}$$

$$\dot{Q} - \dot{W} = \dot{m}[h_2 - h_1 + \frac{V_2^2 - V_1^2}{2} + g(z_2 - z_1)]$$

- $\dot{Q}$ : rate of heat transfer between the control volume and its surroundings
- $\dot{W}$ : power
- $\Delta h$ :  $h_2 - h_1$ , the enthalpy change of a fluid
- $\Delta ke$ :  $(V_2^2 - V_1^2)/2$ , the kinetic energy change
- $\Delta pe$ :  $g(z_2 - z_1)$ , the potential energy change

## 5.4 Some Steady-Flow Engineering Devices

### 1 Nozzles and Diffusers



- $\dot{Q} \approx 0$
- $\dot{W} = 0$
- $\Delta pe \approx 0$
- $\Delta ke \neq 0$

## Nozzle

a device that **increases the velocity of a fluid** at the expense of the pressure

## Diffuser

a device that **increases the pressure of a fluid** by slowing it down

## 2 Turbines and Compressors



- $\dot{Q} \approx 0$
- $\dot{W} \neq 0$
- $\Delta p_e \approx 0$
- $\Delta k_e \approx 0$

## Fan

increases the pressure of a gas slightly and is mainly used to mobilize a gas

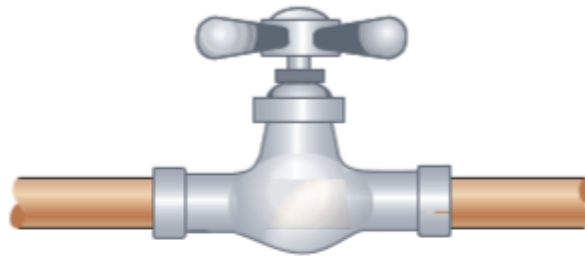
## Compressor

is capable of compressing the gas to very high pressures

## Pumps

work very much like compressors except that they handle liquids instead of gases

## 3 Throttling Valves



(a) An adjustable valve



(b) A porous plug



(c) A capillary tube

any kind of slow-restricting devices devices that cause a significant pressure drop in the fluid without involving any work

- $\dot{Q} \approx 0$
- $\dot{W} = 0$
- $\Delta pe \approx 0$
- $\Delta ke \approx 0$

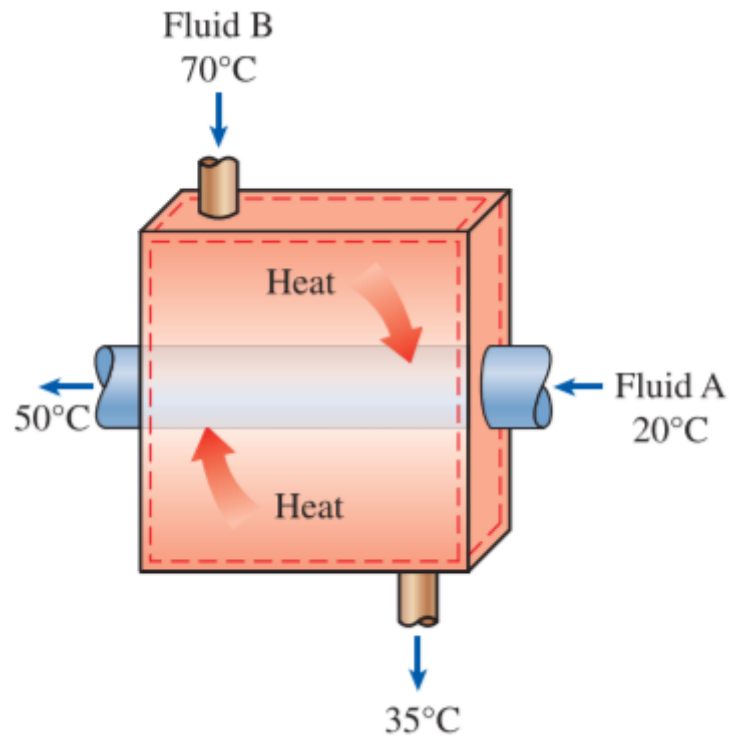
## 4a Mixing Chambers

the section where the mixing process takes place is commonly referred to as a mixing chamber

- $\dot{Q} \approx 0$
- $\dot{W} = 0$
- $\Delta pe \approx 0$
- $\Delta ke \approx 0$

## 4b Heat Exchanges

heat exchanges are device where two moving fluid streams exchange heat without mixing



- $\dot{Q}$  varies
- $\dot{W} = 0$
- $\Delta pe \approx 0$
- $\Delta ke \approx 0$

## 5 Pipe and Duct Flow

