

Supp. Info. for “Process-based modelling of microbial community dynamics in the human colon”

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July 1, 2022

1 Mathematical Model

1.1 Simple Model

In this section we present a very simple model with one microbial group and one colon compartment that we then use to derive bounds on parameters (e.g. absorption of SCFA and water) and to look at the bulk properties of the system, e.g. the relationship between transit time and SCFA concentration.

This simple model consists of, bacteria (X), substrate (S), SCFA mass (Z) and water (W) all with units of mass. We set f_s as the fraction of the waste products of X that are SCFA, and Y is the amount of microbial growth for 1 g of S and a_Z and a_W are the absorption rates of Z and W . The rates of change are given by

$$\frac{dX(t)}{dt} = G(t)X(t) - X(t)V \quad (1)$$

$$\frac{dS(t)}{dt} = \dot{S}_{in} - \frac{G(t)X(t)}{Y} - S(t)V \quad (2)$$

$$\frac{dZ(t)}{dt} = f_s \left(\frac{1}{Y} - 1 \right) G(t)X(t) - (V + a_Z)Z(t) \quad (3)$$

$$\frac{dW(t)}{dt} = \dot{W}_{in} - (V + a_W)W(t) \quad (4)$$

where microbial growth, G , is given by

$$G(t) = G^m \frac{S(t)}{S(t) + K} \quad (5)$$

where K is the half-saturation constant and G^m is the maximum growth rate of X on S . Transit time is incorporated via the washout rate, V such that $V = 1/T_t$.

Steady state analysis (i.e. when the system is not changing with time) of the one group model can be used to give us some bounds or checks on the bulk properties of the system. The steady state solution (at time, t_s), assuming $X > 0$, is given by

$$X(t_s) = (\dot{S}_{in}/V - S(t_s))Y \quad (6)$$

$$S(t_s) = \frac{VK}{G^{\max} - V} \quad (7)$$

$$Z(t_s) \approx VX(t_s) \frac{1 - Y}{Y(a_Z + V)} \quad (8)$$

$$W(t_s) = \frac{\dot{W}_{in}}{a_W + V} \quad (9)$$

where \dot{X}_{in} is the inflow rate of X .

1.2 Microbial yield and substrate inflow

Assuming the microbes consume all available substrate, then the steady state mass of microbes can be approximated by

$$X(t_s) \approx \frac{\dot{S}_{in}Y}{V} \quad (10)$$

where \dot{S}_{in} is the dietary inflow of all substrates (i.e. dietary P, C and mucin); V is the wash out rate from the system and Y , the microbial yield. Assuming the output of microbes (given by $X_{t_s}V$) is 14-28 g d⁻¹ (Stephen and Cummings, 1980) (with midpoint of 21) and the substrate inflow is about 65 g d⁻¹; Eq. 10 suggests that Y is 21/65 i.e. about 0.3 which matches very well with the yield values for our functional groups which have yield values around 0.28 or 0.33 (see other Supp. Info. file).

1.3 Specific water absorption, a_W

Extending Eq. 9 to N compartments with downstream flow from 1 to N , and assuming the specific absorption rate is the same in all, then at steady state the water in each compartment is given by,

$$W_1 = \frac{\dot{W}_{in}}{a_W + V_1}, \quad (11)$$

$$W_2 = \frac{W_1 V_1}{a_W + V_2}, \dots \quad (12)$$

$$\dots, W_N = \frac{W_{N-1} V_{N-1}}{a_W + V_N} \quad (13)$$

Successively substituting for the unknowns gives

$$W_N = \frac{\dot{W}_{in} V_1 V_2 \dots V_{N-1}}{(a_W + V_1)(a_W + V_2) \dots (a_W + V_N)} \quad (14)$$

If 90% of water is absorbed over the transit time then in the last compartment, N , $W_N V_N = 0.1 \dot{W}_{in}$. Substituting this into Eq. 14 gives

$$\prod_{k=1}^N (a_W + V_k) = 10 \prod_{j=1}^N V_j. \quad (15)$$

This can be solved numerically where V_j is computed by dividing the colon into N compartments which each take fraction, f_j^T , of the total transit time to pass

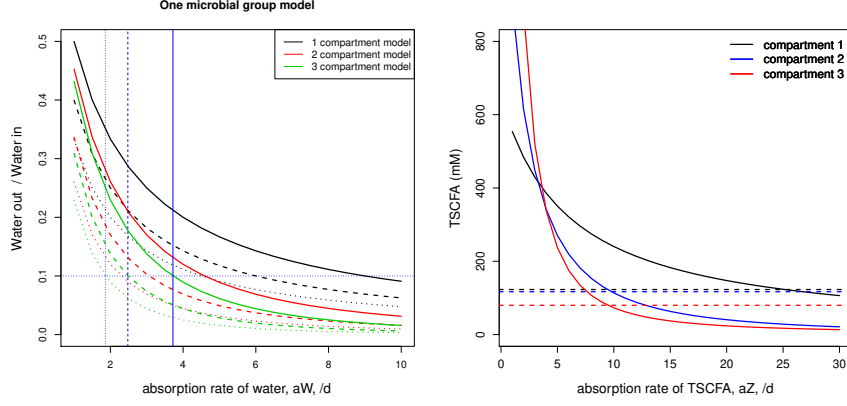


Figure S1: a) Achieving 90% water absorption for different transit times (1, 1.5 and 2 days represented by solid, dashed and dotted line respectively) and different number of compartments (1, 2, and 3 by colour, as shown in legend). The dotted horizontal line shows the required value for 90% incoming water absorption in the colon and the vertical blue lines show the a_W value which gives the correct total absorption for the 3 different transit times (which are as before, 1, 1.5 and 2 days represented by solid, dashed and dotted line respectively). b) Investigating SCFA absorption. TSCFA (mM) for different a_Z for transit time of 1.25 days, for the one group, three compartment model. a_Z is from 1,2,...30 /d with values constant throughout the colon. The dashed horizontal lines show the expected TSCFA in each compartment. The simulation is for 5 days and the results are the mean over the last day. Constant inflow and outflow (no meals or bowel movements) with a_W changing with transit time according to Eq. 16.

through. Using fractional times based on compartment volume (Fig. 1 in main manuscript) and assuming that a_W is the same in each compartment we find that for a one compartment model, $a_W = \frac{9}{T_t}$; for a two compartment model, $a_W = \frac{4.59}{T_t}$; and for a three compartment model, $a_W = \frac{3.72}{T_t}$ (see Fig. S1). This can be expressed exactly by

$$a_W = \frac{16.95 - 9.72N + 1.77N^2}{T_t} \quad (16)$$

where N is the number of compartments in the model. Note that this does not mean that specific water absorption changes with transit time, rather that to fulfill the 90% absorption criteria we can set a_W based on N and T_t . Once a typical transit time is chosen, the value of a_W can be fixed. As a rough estimation, $a_W \approx 3$ /d for a 3 compartment model with a transit time between one to one and a half days (Fig. S1). Given this will not be significantly affected by the microbial model (microbial uptake/production of water is small) this result will apply to all of the models in this work.

53 1.4 Specific SCFA absorption, a_Z

54 Using our one group microbial group model but adapted for 3 compartments,
 55 and our estimation for a_W based on transit time and the number of compart-
 56 ments (Eq. 16), we run the model for a transit times of 1.25 d with continuous
 57 inflow and outflow, over a range of a_Z from 1-30 d⁻¹. We compute TSCFA from
 58 our model by converting Z from g to mM using

$$Z_{mM} = 10^6 \frac{Z_g}{W_g m_Z} \quad (17)$$

59 where m_Z is computed by assuming TSCFA is in the ratio 3:1:1 (Ac:Bu:Pr)
 60 to give a weighted mean molar mass of TSCFA, m_Z of 68.4 g mol⁻¹. Fig. S1,
 61 shows the TSCFA in each model compartment versus a_Z . The horizontal dashed
 62 lines show the TSCFA value matching the model criteria, indicating the best
 63 estimates were a_Z equal to 25.2, 4.2 and 9.2 d⁻¹ in the proximal, transverse
 64 and distal colon respectively. However, this was determined using a_Z constant
 65 through the colon so if a_Z varies between compartments this will change the
 66 results. In the interests of a robust model (i.e. the fewer parameter values, the
 67 better) we made the decision to use one value for a_Z . Given the experimental
 68 value of 9.6 d⁻¹ compares well with our best estimate for the distal colon (9.2
 69 d⁻¹) we decided to set $a_Z = 9.6$ d⁻¹ throughout. It should be noted however
 70 that decreasing a_Z along the colon has been implemented in other models e.g.
 71 Labarthe et al. (2019).

72 2 Effect of Transit Time

73 Experimental evidence (e.g. (Lewis and Heaton, 1997)) shows that TSCFA
 74 (mM) decreases as transit time increases. We can explain why this is, mathe-
 75 matically, using a very simple one group model with monod growth, which we
 76 can solve analytically at steady state. To compute TSCFA in mM we need to
 77 use the fraction of P that is SCFA and then divide by the mean molar mass
 78 (m_m) and multiply by 1000 to find mmol. We then need to divide by W in litres,
 79 thus,

$$\text{TSCFA} = 10^6 \frac{P f_s}{W m_m} \quad (18)$$

80 Substituting for P and W , ignoring scaling constants and assuming remaining
 81 substrate at steady state is negligible, shows that TSCFA is linearly related to
 82 the expression

$$\frac{\dot{S}_{in}}{\dot{W}_{in}} \frac{a_W + V}{a_P + V} \quad (19)$$

83 To see the effect of simply changing the transit time through the colon on TSCFA
 84 we assume \dot{S}_{in} and \dot{W}_{in} are fixed and replace V by $1/Tt$ to get

$$\text{TSCFA} \propto \frac{a_W T_t + 1}{a_P T_t + 1} \quad (20)$$

85 Since we have $a_W = 3$ and $a_P = 9.6$, the denominator will increase much faster
 86 than the numerator as T_t increases thus, theoretically, TSCFA will decrease as
 87 transit time increases as SCFA are absorbed faster than water. Using realistic

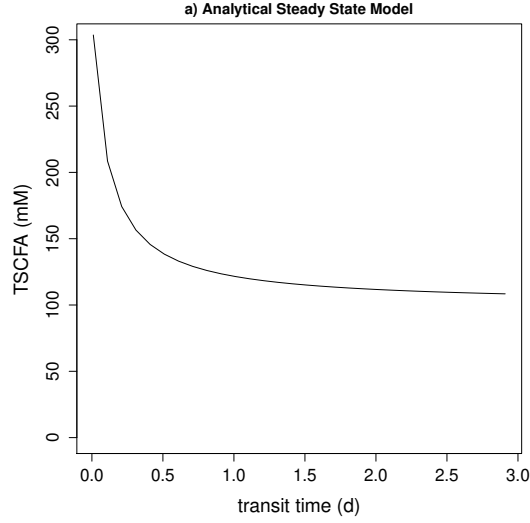


Figure S2: TSCFA as a function of transit time obtained from the solution of Eqs. 2-4. We convert from product mass, P , to moles using the average molar mass (weighted according to A:B:P = 3:1:1) of 68.5 g/mol and compute f_s as an average of the microPop microbial group stoichiometries to be approximately 0.5. We set inflowing substrate at 65 g/d (dietary substrate plus mucin) and inflowing water at 1100 g/d, with parameter values $Y=0.3$, $G^{\max}=20$ /d and $K=0.001$. [transitTimeModel.R]

parameter values in the above model (Eq. 2-4) allows us to plot TSCFA against transit time – see Fig S2 which compares very well with the experimental data shown in Fig. 1 by Lewis and Heaton (1997).

3 Microbial group parameter values

The parameters describing the different microbial groups are the same as the intrinsic functional groups given in the microPop R package (version 1.6), with one exception. We increased the maximum growth rate of Lactate Producers on RS from 6 d⁻¹ to 7 d⁻¹ and their pH tolerance were coordinates changed to tolerate lower pH (first two pH coordinates now 4.5 and 5.25, rather than 4.95 and 5.7) to ensure a better chance of their survival in the model. This section shows the data frames used for each microbial group in microPopGut. The following list explains the different entries in these data frames.

- ‘Rtype’ refers to the substrate type on the pathway:
 - ‘X’: not involved in pathway
 - ‘S’: substitutable substrate (this can be interchanged with other substitutable substrates)
 - ‘Se’: essential substrate (the microbes can not grow without this)
 - ‘Sb’: boosting substrate (if this is present the microbe can grow faster)

- 107 – ‘Sw’: water
- 108 – ‘P’: metabolic product
- 109 • ‘halfsat’ is the half saturation constant for monod growth
- 110 • ‘yield’ is the microbial mass produced from one gram of substrate
- 111 • ‘maxGrowthRate’ is the specific maximum growth rate of the microbes
- 112 • ‘stoichiom’ refers to the number of moles of each molecules involved in
- 113 growth
- 114 • ‘keyResource’ is the substrate whose uptake rate is used to compute the
- 115 uptake of the other substrates on the pathway according to the stoichiom-
- 116 etry
- 117 • ‘numPathways’ defines how many metabolic pathways the microbial group
- 118 has. When there is more than one pathway, numbered parameter names
- 119 for the subsequent pathways are used.
- 120 For more details please refer to Kettle et al. (2015) and Kettle et al. (2018) or
- 121 use the help function within the microPopGut package.

Table 1: Bacteroides

| | units | Protein | NSP | RS | Acetate | Propionate | Succinate | H2 | CO2 | other |
|-----------------|-------|---------|-------|-------|---------|------------|-----------|----|-----|-------|
| Rtype | none | X | S | S | P | P | P | P | P | X |
| halfSat | g/l | | 0.001 | 0.001 | | | | | | |
| yield | g/g | | 0.286 | 0.333 | | | | | | |
| maxGrowthRate | /d | | 12 | 24 | | | | | | |
| stoichiom | mol | | 2 | 2 | 2 | 1 | 1 | 2 | 1 | |
| keyResource | none | | | | | | | | | |
| numPathways | none | 2 | | | | | | | | |
| Rtype.2 | none | S | X | X | P | P | P | P | P | P |
| halfSat.2 | g/l | 0.001 | | | | | | | | |
| yield.2 | g/g | 0.2 | | | | | | | | |
| maxGrowthRate.2 | /d | 24 | | | | | | | | |
| stoichiom.2 | mol | 6 | | | 2 | 1 | 1 | 2 | 1 | 7 |
| keyResource.2 | none | | | | | | | | | |
| pHcorners | pH | 5.6 | 6.35 | 7.85 | 8.6 | | | | | |

Table 2: NoButyStarchDeg

| | units | NSP | RS | Acetate | H2 | CO2 | H2O |
|---------------|-------|-------|-------|---------|------|-----|-----|
| Rtype | none | S | S | P | P | P | Sw |
| halfSat | g/l | 0.001 | 0.001 | | | | |
| yield | g/g | 0.286 | 0.333 | | | | |
| maxGrowthRate | /d | 3.6 | 14.4 | | | | |
| stoichiom | mol | 1 | 1 | 2 | 4 | 2 | 2 |
| keyResource | none | | | | | | |
| numPathways | none | 1 | | | | | |
| pHcorners | pH | 5.35 | 6.1 | 7.6 | 8.35 | | |

Table 3: NoButyFibreDeg

| | units | NSP | RS | Acetate | Succinate | H2 |
|---------------|-------|-------|-------|---------|-----------|----|
| Rtype | none | S | S | P | P | P |
| halfSat | g/l | 0.001 | 0.001 | | | |
| yield | g/g | 0.286 | 0.333 | | | |
| maxGrowthRate | /d | 16.8 | 3.6 | | | |
| stoichiom | mol | 1 | 1 | 1 | 1 | 1 |
| keyResource | none | | | | | |
| numPathways | none | 1 | | | | |
| pHcorners | pH | 5 | 5.75 | 7.25 | 8 | |

Table 4: LactateProducers

| | units | NSP | RS | Sugars | Acetate | Lactate | Formate | Ethanol | H2O |
|---------------|-------|-------|-------|--------|---------|---------|---------|---------|-----|
| Rtype | none | S | S | S | P | P | P | P | Sw |
| halfSat | g/l | 0.001 | 0.001 | 0.001 | | | | | |
| yield | g/g | 0.286 | 0.333 | 0.333 | | | | | |
| maxGrowthRate | /d | 7.2 | 7 | 24 | | | | | |
| stoichiom | mol | 6 | 6 | 6 | 10 | 4 | 2 | 1 | 1 |
| keyResource | none | | | | | | | | |
| numPathways | none | 1 | | | | | | | |
| pHcorners | pH | 4.5 | 5.25 | 7.2 | 7.95 | | | | |

Table 5: ButyrateProducers1

| | units | NSP | RS | Sugars | Acetate | Butyrate | H2 | CO2 | H2O |
|---------------|-------|-------|-------|--------|---------|----------|----|-----|-----|
| Rtype | none | S | S | S | Sb | P | P | P | P |
| halfSat | g/l | 0.001 | 0.001 | 0.001 | 0.001 | | | | |
| yield | g/g | 0.286 | 0.333 | 0.333 | | | | | |
| maxGrowthRate | /d | 8.4 | 8.4 | 24 | | | | | |
| stoichiom | mol | 2 | 2 | 2 | 2 | 3 | 2 | 4 | 2 |
| keyResource | none | Hex | | | | | | | |
| numPathways | none | 1 | | | | | | | |
| nonBoostFrac | none | 0.75 | | | | | | | |
| pHcorners | pH | 4.95 | 5.7 | 7.2 | 7.95 | | | | |

Table 6: ButyrateProducers2

| | units | NSP | RS | Sugars | Acetate | Butyrate | Lactate | Formate | CO2 | H2O |
|---------------|-------|-------|-------|--------|---------|----------|---------|---------|-----|-----|
| Rtype | none | S | S | S | Sb | P | P | P | P | P |
| halfSat | g/l | 0.001 | 0.001 | 0.001 | 0.001 | | | | | |
| yield | g/g | 0.286 | 0.333 | 0.333 | | | | | | |
| maxGrowthRate | /d | 14.4 | 7.2 | 24 | | | | | | |
| stoichiom | mol | 6 | 6 | 6 | 4 | 7 | 2 | 6 | 4 | 4 |
| nonBoostFrac | none | 0.1 | | | | | | | | |
| keyResource | none | Hex | | | | | | | | |
| numPathways | none | 1 | | | | | | | | |
| pHcorners | pH | 4.85 | 5.6 | 7.1 | 7.85 | | | | | |

Table 7: PropionateProducers

| | units | NSP | RS | Sugars | Acetate | Propionate | CO2 | Lactate | H2O |
|-----------------|-------|---------|-------|--------|---------|------------|-----|---------|-----|
| Rtype | none | S | S | S | P | P | P | X | P |
| halfSat | g/l | 0.001 | 0.001 | 0.001 | | | | | |
| yield | g/g | 0.286 | 0.333 | 0.333 | | | | | |
| maxGrowthRate | /d | 7.2 | 7.2 | 24 | | | | | |
| stoichiom | moles | 3 | 3 | 3 | 2 | 4 | 2 | | 2 |
| keyResource | none | | | | | | | | |
| numPathways | none | 2 | | | | | | | |
| Rtype.2 | none | X | X | X | P | P | P | Se | P |
| halfSat.2 | g/l | | | | | | | 0.001 | |
| yield.2 | g/g | | | | | | | 0.111 | |
| maxGrowthRate.2 | /d | | | | | | | 4.8 | |
| stoichiom.2 | moles | | | | 1 | 2 | 1 | 3 | 1 |
| keyResource.2 | none | Lactate | | | | | | | |
| pHcorners | pH | 4.75 | 5.5 | 7 | 7.75 | | | | |

Table 8: ButyrateProducers3

| | units | NSP | RS | Sugars | Acetate | Butyrate | Formate | H2 | CO2 | Lactate | H2O |
|-----------------|-------|---------|-------|--------|---------|----------|---------|----|-----|---------|-----|
| Rtype | none | S | S | S | P | P | P | P | P | X | Sw |
| halfSat | g/l | 0.001 | 0.001 | 0.001 | | | | | | | |
| yield | g/g | 0.286 | 0.333 | 0.333 | | | | | | | |
| maxGrowthRate | /d | 7.2 | 7.2 | 24 | | | | | | | |
| stoichiom | mol | 10 | 10 | 10 | 2 | 9 | 12 | 10 | 8 | | 2 |
| keyResource | none | | | | | | | | | | |
| numPathways | none | 2 | | | | | | | | | |
| Rtype.2 | none | X | X | X | Se | P | X | P | P | Se | P |
| halfSat.2 | g/l | | | | 0.001 | | | | | 0.001 | |
| yield.2 | g/g | | | | | | | | | 0.111 | |
| maxGrowthRate.2 | /d | | | | | | | | | 4.8 | |
| stoichiom.2 | mol | | | | 2 | 3 | | 2 | 4 | 4 | 2 |
| keyResource.2 | none | Lactate | | | | | | | | | |
| pHcorners | pH | 4.85 | 5.6 | 7.1 | 7.85 | | | | | | |

Table 9: Acetogens

| | units | NSP | RS | Sugars | Acetate | H2 | CO2 | Formate | H2O |
|-----------------|-------|-------|-------|--------|---------|-------|-------|---------|-----|
| Rtype | none | S | S | S | P | X | X | X | X |
| halfSat | g/l | 0.001 | 0.001 | 0.001 | | | | | |
| yield | g/g | 0.286 | 0.333 | 0.333 | | | | | |
| maxGrowthRate | /d | 7.2 | 7.2 | 24 | | | | | |
| stoichiom | moles | 1 | 1 | 1 | 3 | | | | |
| keyResource | none | | | | | | | | |
| numPathways | none | 3 | | | | | | | |
| Rtype.2 | none | X | X | X | P | Se | Se | X | P |
| halfSat.2 | g/l | | | | | 0.001 | 0.001 | | |
| yield.2 | g/g | | | | | | 0.03 | | |
| maxGrowthRate.2 | /d | | | | | | 2.4 | | |
| stoichiom.2 | moles | | | | 1 | 4 | 2 | | 2 |
| keyResource.2 | none | CO2 | | | | | | | |
| Rtype.3 | none | S | S | S | P | P | P | Se | X |
| halfSat.3 | g/l | 0.001 | 0.001 | 0.001 | | | | 0.001 | |
| yield.3 | g/g | 0.286 | 0.333 | 0.333 | | | | | |
| maxGrowthRate.3 | /d | 7.2 | 7.2 | 24 | | | | | |
| stoichiom.3 | moles | 1 | 1 | 1 | 3 | 2 | 2 | 2 | |
| keyResource.3 | none | Hex | | | | | | | |
| pHcorners | pH | 5.25 | 6 | 7.5 | 8.25 | | | | |

Table 10: Methanogens

| | units | H2 | CO2 | CH4 | H2O | Formate |
|-----------------|-------|---------|-------|-----|------|---------|
| Rtype | none | Se | Se | P | P | X |
| halfSat | g/l | 0.001 | 0.001 | | | |
| yield | g/g | | 0.03 | | | |
| maxGrowthRate | /d | | 2.4 | | | |
| stoichiom | mol | 4 | 1 | 1 | 2 | |
| keyResource | none | CO2 | | | | |
| numPathways | none | 2 | | | | |
| Rtype.2 | none | X | P | P | P | Se |
| halfSat.2 | g/l | | | | | 0.001 |
| yield.2 | g/g | | | | | 0.00724 |
| maxGrowthRate.2 | /d | | | | | 2.4 |
| stoichiom.2 | mol | | 3 | 1 | 2 | 4 |
| keyResource.2 | none | Formate | | | | |
| pHcorners | pH | 5.25 | 6 | 7.5 | 8.25 | |

122 References

- 123 H Kettle, G Holtrop, P Louis, and Harry J. Flint. micropop: Modelling micro-
124 bial populations and communities in r. *Methods in Ecology and Evolution*, 9
125 (2):399–409, 2018. doi: 10.1111/2041-210X.12873.
- 126 Helen Kettle, Petra Louis, G Holtrop, Sylvia H. Duncan, and Harry J. Flint.
127 Modelling the emergent dynamics and major metabolites of the human
128 colonic microbiota. *Environmental Microbiology*, 17(5):1615–1630, 2015. doi:
129 10.1111/1462-2920.12599.
- 130 Simon Labarthe, Bastien Polizzi, Thuy Phan, Thierry Goudon, Ma-
131 gali Ribot, and Beatrice Laroche. A mathematical model to in-
132 vestigate the key drivers of the biogeography of the colon micro-
133 biota. *Journal of Theoretical Biology*, 462:552 – 581, 2019. ISSN
134 0022-5193. doi: <https://doi.org/10.1016/j.jtbi.2018.12.009>. URL
135 <http://www.sciencedirect.com/science/article/pii/S002251931830599X>.
- 136 S.J. Lewis and K.W. Heaton. Increasing butyrate concentration in the distal
137 colon by accelerating intestinal transit. *Gut*, 41:245–251, 1997.
- 138 AM Stephen and JH Cummings. The microbial contribution to hu-
139 man fecal mass. *J. Medical Microbiology*, 13(1):45–56, 1980. doi:
140 <https://doi.org/10.1099/00222615-13-1-45>.