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# **1 Introduction**

## **1.1 Motivation**

The fundamental idea is to test models of condensation and evaporation of liquids in confinement. To this end, a well characterized confinement is necessary. The latter shall be realized using nanoporous alumina membranes. The production of these is rather advanced as they are commonly used for the production of nanowires. Moreover, the shape of the pores is ideally cylindrical which makes for a simple geometry. A nanoporous alumina membrane includes a large number of parallel pores. Therefore, any experiment conducted on one of these membranes yields a result that averages over all of these pores. This is why, ideally, monodisperse alumina membranes shall be produced.

As a liquid to condense inside the pores of these membranes, hexane is used. There are multiple reasons for that. First, other teams have used hexane for this type of experiments before. This means that reference isotherms exist that the results can be compared to. Moreover, hexane permits to experiment at ambient temperature which makes things much easier. The fact that this is only a preexperiment for later experiments using helium, the use of liquids like nitrogen seems to make experimenting more difficult while offering no advantages.

The models to be tested are primarily the KELVIN equation and the SAAM and COLE theory. There are multiple variations though, as for example there is a modified KELVIN equation taking into account the wetting film which the basic KELVIN equation does not. In addition to that, thermal activation and the temperature relative to the critical temperature of the used fluid are relevant. The latter is one reason why finally, the experiment is planned to be conducted using helium. Finally, there are other more sophisticated models that need to be tested. Due to the small variations that are expected, again, the probing of the latter requires helium. Last but not least, in order to also study cavitation in alumina membranes, inc bottle like cavities with constricted openings must be produced. As for both, the helium experiments and for the inc bottle openings, pores of sub ten nanometer diameter must be synthesized in a controlled way, the production process needs to be improved. This becomes the main goal of the conducted experiments described in this article.

## **1.2 Troubles**

Early on, the conducted experiments prove the membranes to be not as ideal as was hoped for. The idea of the perfect cylindrical pores of the same diameter is replaced by the conclusion that the pores' diameter is not only distributed over the membranes but also varies within a single pore. This variation manifests in the way of a funnelling aspect that makes for a conical shape, rather than a cylindrical, and also as corrugations. As explained above, the confinement needs to be well characterized to be able to test the models of condensation and evaporation. In contrast to that, the geometrical shape of the pores does not allow for this kind of precise characterization. Using electron beam microscopy, the opening diameters of the pores can be checked on top and bottom side. Furthermore, a cross section view yields some information about the straightness and possible defects along the length of the pores. As the pores' length ranges in the order of micrometers though, while the diameters' magnitude is nanometers, this still gives little information about the overall pore shape. Moreover, the microscopy images can not be precisely evaluated due to the unknown porosity of the membranes and again the lack of information on the shape. In the course of the experiments

a way is developed to at least delimit a range for the porosity and so allow for a more sophisticated analysis of the electron beam microscopy images under the assumption of a certain pore geometry.

The bottom line is that neither the exact geometry and distribution of pore shapes and sizes is known, nor are the condensation and evaporation models clear. Thus, the first step must be to understand and refine the production process of the membranes and to hereby make for the best possible characterization of the confinement.

### **1.3 Approach**

To understand the membranes' characteristics and to use this knowledge to improve the production process, rather large pore diameters of above fourty nanometer diameter, for which KELVIN equation is assumed to be sufficiently precise, are probed using multiple techniques. The core of the conducted experiments relies on thermodynamics using volumetric measurements. In addition, optical measurements and also visual documentation are used along with electron beam microscopy. All the aquired data is then interpreted and tested for coherence to finally draw conclusions on the membranes' characteristics. From the aquired results, questions rise about the effects of different production steps which are then taken a closer look at.

## 2 Theory

### **3 Experimental**

## 4 Analysis

### 4.1 Isotherm computation

In the following, evaluation of the recorded raw data is presented for volumetric (section 4.1.1) and for the optical measurements (section 4.1.2).

#### 4.1.1 Volumetric isotherm

To compute the isotherms from the recorded data the experiment needs to be conducted not only with a membrane inside of the cell, but also with an empty cell. From here on, the following indices shall be used:

- 1 → no membrane
- 2 → membrane.

Furthermore, the variables  $P_i$ ,  $\dot{P}_i$ ,  $V_i$ ,  $T_i$ ,  $n_i$  and  $\dot{n}_i$ ,  $i \in \{1, 2\}$ , refer to the values measured inside of the cell, in explanation the red marked part of the system in ???. The raw isotherms of the two experiments are shown in fig. 4.1. The plateaus of the yellow curve with membrane inside the cell of the plot versus time correspond to the dips of the time derivative of the pressure of the versus pressure plot. This can be explained by the hexane condensing inside the membrane's pores at a given pressure due to which the continuing matter flow into the cell does not yield an increase of pressure.

Regarding the system with an empty cell, it is clear that the ideal gas law can be used to compute the flow rate of hexane (compare ??). By solving for the amount of matter

$$n_1 = \frac{P_1 V_1}{R T_1},$$

taking into account that the temperature of the cell is regulated at  $T_1$  and the volume  $V_1$  is constant, the flow of matter becomes

$$\dot{n}_1 = \frac{V_1}{R T_1} \cdot \dot{P}_1.$$

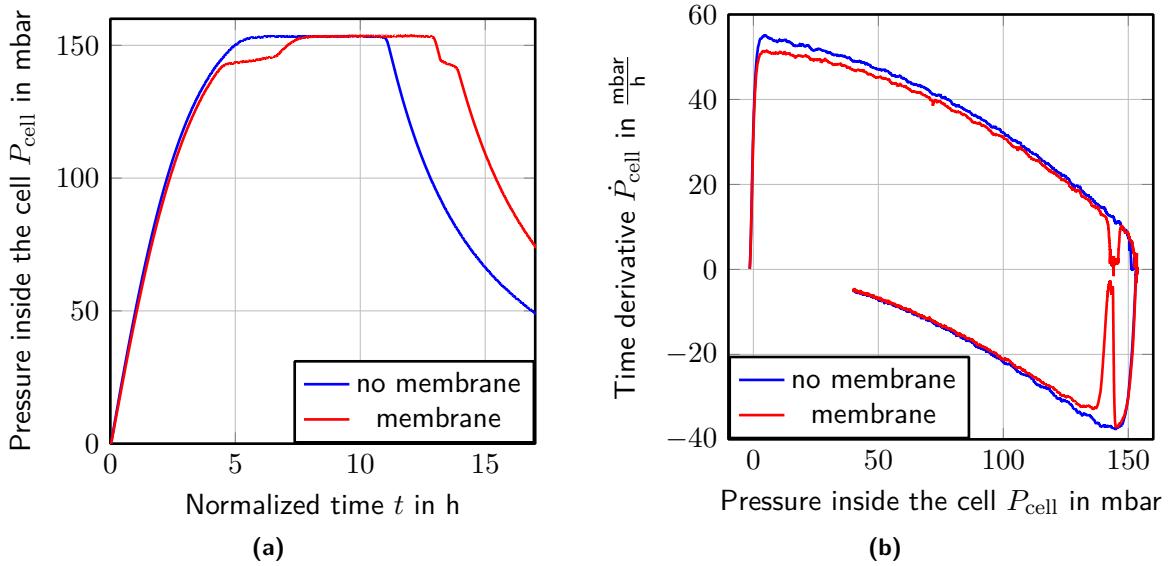
Furthermore, the flow of matter for the system with a membrane inside the cell can be interpreted as the sum of the flow into the membrane  $\dot{n}_2^{\text{mem}}$  and the flow into the system volume excluding the membrane  $\dot{n}_2^{\text{cell}}$ . This can be rewritten yielding

$$\dot{n}_2^{\text{mem}} = \dot{n}_2 - \dot{n}_2^{\text{cell}},$$

where  $\dot{n}_2^{\text{cell}}$  obeys ideal gas law. Using the fact that the flow through the PFEIFFER valve only depends on the pressure difference  $\Delta P_i = P_i^{\text{tank}} - P_i^{\text{cell}}$ , assuming that  $P_1^{\text{tank}} = P_2^{\text{tank}}$  leads to

$$\begin{aligned}\dot{n}_2^{\text{mem}}(P_2) &= \dot{n}_1(P_2) - \dot{n}_2^{\text{cell}}(P_2) \\ &= \frac{V_1}{R T_1} \cdot \dot{P}_1(P_2) - \frac{V_2}{R T_2} \cdot \dot{P}_2(P_2)\end{aligned}\tag{4.1}$$

Figure 4.2(a) shows the computation steps visually using the respective plots versus time.



**Figure 4.1** Raw volumetric isotherm data recorded with the experimental setup as explained in ?? for one cycle without a membrane inside the cell and one with a membrane inside the cell. (a) shows the pressure values over time making the condensation and evaporation plateaus of absorption and desorption of hexane within the membrane's pores visible. (b) is the pressure loop which is relevant for the computation of the isotherms. Again, the before mentioned plateaus are visible as dips in the time derivative of the pressure.

As the temperature of the system is regulated ( $T = T_1 = T_2 = \text{const.}$ ) and because  $V = V_1 \approx V_2$  since  $V_{\text{mem}} \ll V_1$ , equation eq. (4.1) yields

$$n_2^{\text{membrane}} = \frac{V}{RT} \int_0^{t_2} (\dot{P}_1(t'_1) - \dot{P}_2(t'_2)) dt'_2. \quad (4.2)$$

Important at this point is the dependency of  $\dot{P}_1(t_1)$  on  $t_1$  while the integration is over  $t_2$ .

As the experimental setup yields discrete values at given time intervals  $\Delta t$ , the data evaluation makes use of a sum rather than an integration.

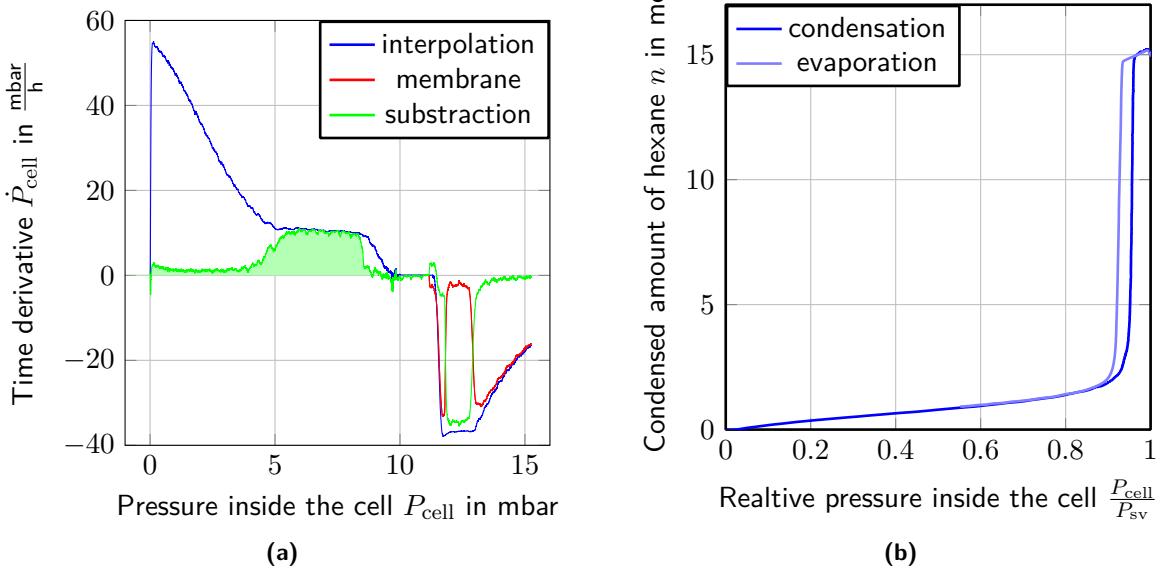
$$n = \frac{V}{RT} \sum (\dot{P}_1(P_1 = P_2) - \dot{P}_2(P_2)) \cdot \Delta t \quad (4.3)$$

yields the molar amount of hexane condensed inside the membrane. Figure fig. 4.2(b) shows the result of the integration eq. (4.3) for membrane 296d. It is an absorption and desorption isotherm for hexane inside the porous alumina membrane. The bulk condensation and evaporation is not visible, as it is also recorded with the reference isotherm without membrane inside the cell.

What stings the eye is that the sharp rise of the condensation branch does not start at the liquid fraction  $LF = 0$ . The same goes for the evaporation branch. It only drops to a liquid fraction value  $LF > 0$  and then decreases superimposed with the condensation branch. While it would be reasonable to renormalize the graph so only the mentioned sharp rise and drop are relevant for the isotherm as this part is where the pores fill or empty at spinodal or equilibrium pressure (??), it is not done here. The reason for this is that the initial rise of the isotherms is assumed to be due to the build up of a film on the membranes surfaces. This is part of the theory of condensation and evaporation in confinement even though the film is ignored in the basic KELVIN equation (??). ???MAKE A COMPUTATION AS TO HOW MANY MOLES OF LIQUID ARE EXPECTED FOR THE FILMS ON ONE SINGLE MEMBRANE???

Moreover, the plots

$$i \quad \text{over} \quad j, \quad i \in \{n, LF, FF\}, \quad j \in \{P_{\text{cell}}, P_{\text{rel}}, D_{\text{kelvin}}\} \quad (4.4)$$



**Figure 4.2** (a) shows the raw data of the isotherm with membrane and interpolation of the reference isotherm without membrane. Also, the subtraction of the latter (compare integrand of eq. (4.1)) is plotted where the area to be integrated for the absorption and desorption isotherm is shaded light green. The integration according to eq. (4.3) results in the isotherm displayed in (b).

are of interest, where

$$P_{\text{rel}} = \frac{P_{\text{cell}}}{P_{\text{sv}}^{\text{exp}}}, \quad (4.5)$$

with the saturated vapor pressure  $P_{\text{sv}}$ .

$$LF = \frac{n}{n_{\max}} \quad (4.6)$$

is the liquid fraction of hexane condensed inside the pores of the membrane using the total maximum amount of condensed hexane  $n_{\max}$  and last,

$$FF = \frac{V_{\text{hex}}^{\text{cond}}}{V_{\text{mem}}} \quad (4.7)$$

with the volume of condensed hexane  $V_{\text{hex}}^{\text{cond}}$  and the membrane's volume  $V_{\text{mem}}$ , is the filled fraction of the membrane. Its maximum corresponds to the porosity of the membrane. For the computation please refer to ??.

For the computation of the introduced physical sizes, the saturated vapor pressure  $P_{\text{sv}}$  must be determined.

#### 4.1.1.1 Porosity

Equation eq. (4.3) gives the molar amount of hexane  $n_{\text{hex}}$  condensed inside the membrane's pores. Furthermore, for the given pressures 0 mbar to 160 mbar hexane in its liquid form can be regarded as incompressible and therefore the hexane's volume be computed via

$$V_{\text{hex}} = n_{\text{hex}} \cdot V_{\text{mol,hex}}.$$

. The thickness  $l_{\text{pore}}$  of the membrane is easily determinable via MEB views since its magnitude is micrometers. Finally, the area  $A_{\text{mem}}$  of the measured samples is derived from a photo taken using binoculars.

Using these information the porosity  $\phi$  of a given membrane is given by

$$\phi = 1 - \frac{V_{\text{hex}}}{V_{\text{mem}}}, \quad (4.8)$$

with the membrane's volume

$$V_{\text{mem}} = A_{\text{mem}} \cdot l_{\text{pore}}.$$

#### 4.1.1.2 Determination of the saturated vapor pressure

As the bulk condensation plateau shows a slight drift (compare figure fig. 4.1), using the maximum measured pressure  $P_{\text{cell}}$  does not yield the saturated vapor pressure  $P_{\text{sv}}$  but a higher value. In addition, depending on the contamination of the system by air or degassing grease, the measured value for  $P_{\text{sv}}$  shifts due to the partial pressures. To probe the reproducibility of an isotherm loop including the grade of contamination, the node[anchor=south]maximum measured pressure for different membranes is compared. As the system is opened to replace the membrane in between the isotherms, each cycle is independent. For the change of membrane process please read ???. The result of the experiment is that  $P_{\text{sv}}^{\text{exp}}$  fluctuates by

$$\delta P_{\text{sv}}^{\text{exp}} = \pm 0,5 \text{ mbar}. \quad (4.9)$$

As the relevant plateau of condensation and evaporation inside the pores of the membrane occur at about

$$P_{\text{plateaus}} = 140 \text{ mbar}, \quad (4.10)$$

$\delta P_{\text{sv}}^{\text{exp}}$  translates to an error of about

$$\delta P_{\text{rel}} \leq \pm 0,005. \quad (4.11)$$

#### 4.1.1.3 Diameter error using Kelvin equation

GAUSSIAN error propagation to check the precision of the experiment.

### 4.1.2 Optical measurements

As mentioned in ??, the light transmission setup is independent from the volumetric measurements and also the evaluations do not depend on each other. The light transmission is rather a tool to check on the theory of evaporation and condensation within the membrane using a different approach.

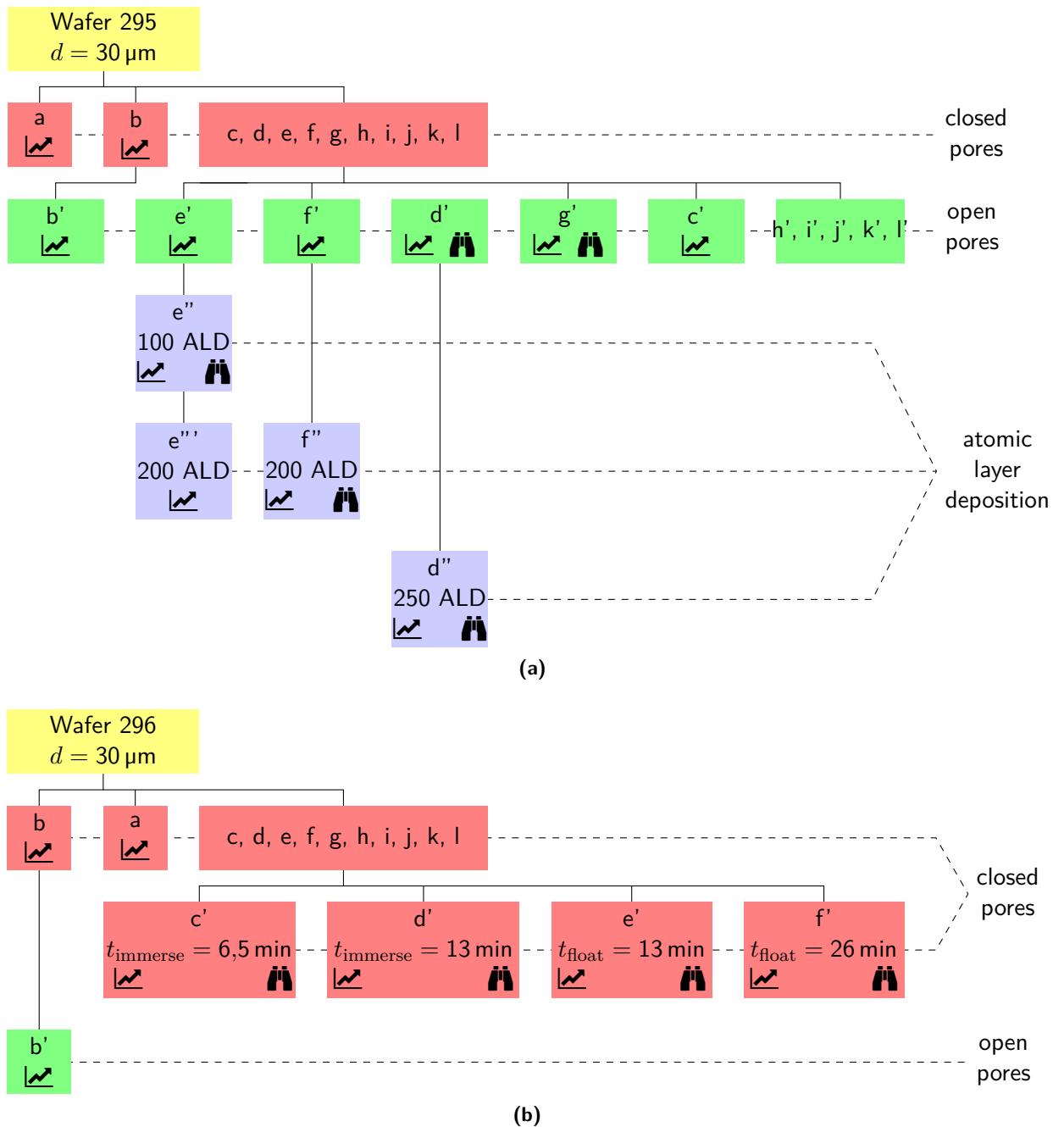
To compute the transmission coefficient of a membrane, it is measured in dry state using the same transmission setup as during the volumetric experiment yielding  $T_{\text{mem}}^{\text{dry}}$ . Then, the first measured intensity value  $I_0$  of a given isotherm is assigned to the dry coefficient as at this point no hexane is condensed inside of the membranes pores yet. From there on, each intensity measurement is translated to a transmission coefficient according to

$$T(t) = T_{\text{mem}}^{\text{dry}} \cdot \frac{I_0}{I(t)}. \quad (4.12)$$

The aquired physical size can be interpreted as explained in the following ??.

As a forword shall be mentioned that the observed transmission drops' magnitude cannot be explained by simple media transmissions as explained in ???. Even counting multiple transitions for a diagonal transmission of a membrane, the regular transmission is not a sufficient explanation as the filled state of a membrane should by that theory be less transmitting than the empty state whereas the opposite is observed. To explain the phenomena, RAYLEIGH scattering and index matching, which are explained in ?? and ?? respectively, must be taken into account.

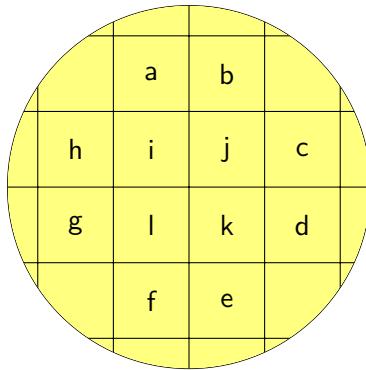
## 4.2 Conducted measurements



**Figure 4.3** Wafer 295 and 296 processing scheme. While a  $\text{graph}_{\text{isotherm}}$  signifies a recorded isotherm, the  $\text{binoculars}$  means MEB pictures have been taken. Red marks pores closed on one end, green pores open on both ends. The processed wafers are immersed in phosphoric acid for  $t_{\text{immerse}}$  or floated on for  $t_{\text{float}}$ .

General: From one wafer we can test different things as we have 12 membranes. Wafer produced as a whole so membranes should be equivalent. ADD THE CIRCLE HERE!!!

Membranes of four different wafers produced according to ?? have been measured. The wafers specifications are noted in table 4.1. As multiple membranes in the same state of the same wafer yielded different results, the position of the single membranes on the wafer were taken note for newly produced wafers. Therefore, for the wafers 295 and 296, the membranes' names correspond to the positions shown in fig. 4.4. Furthermore, all conducted measurements on the membranes in different states are noted on fig. 4.3.



**Figure 4.4** For multiple measured membranes of the same wafer that were expected to show the same characteristics, the conducted measurements noted differences. To find possible patterns in these variations, for the newly produced wafers 295 and 296, the above shown enumeration of membranes is valid.

**Table 4.1** Wafer specifications. The wafers thickness  $l_{\text{pore}}$ , floating time  $t_{\text{float}}$  of the *barrier layer* dissolution process and pore diameter dispersion  $\Delta d_{\text{pore}}^{\text{MEB}}$  measured by electron beam microscopy are noted. The latter two parameters apply to the open pore membranes of the respective wafer.

Wafer	$l_{\text{pore}}$ [μm]	$t_{\text{float}}$ [min]	$\Delta d_{\text{pore}}^{\text{MEB}}$ [nm]
292	60	0	
294	60	0	
295	60	35	
296	30	40	7

### 4.3 Inhomogeneities on one wafer

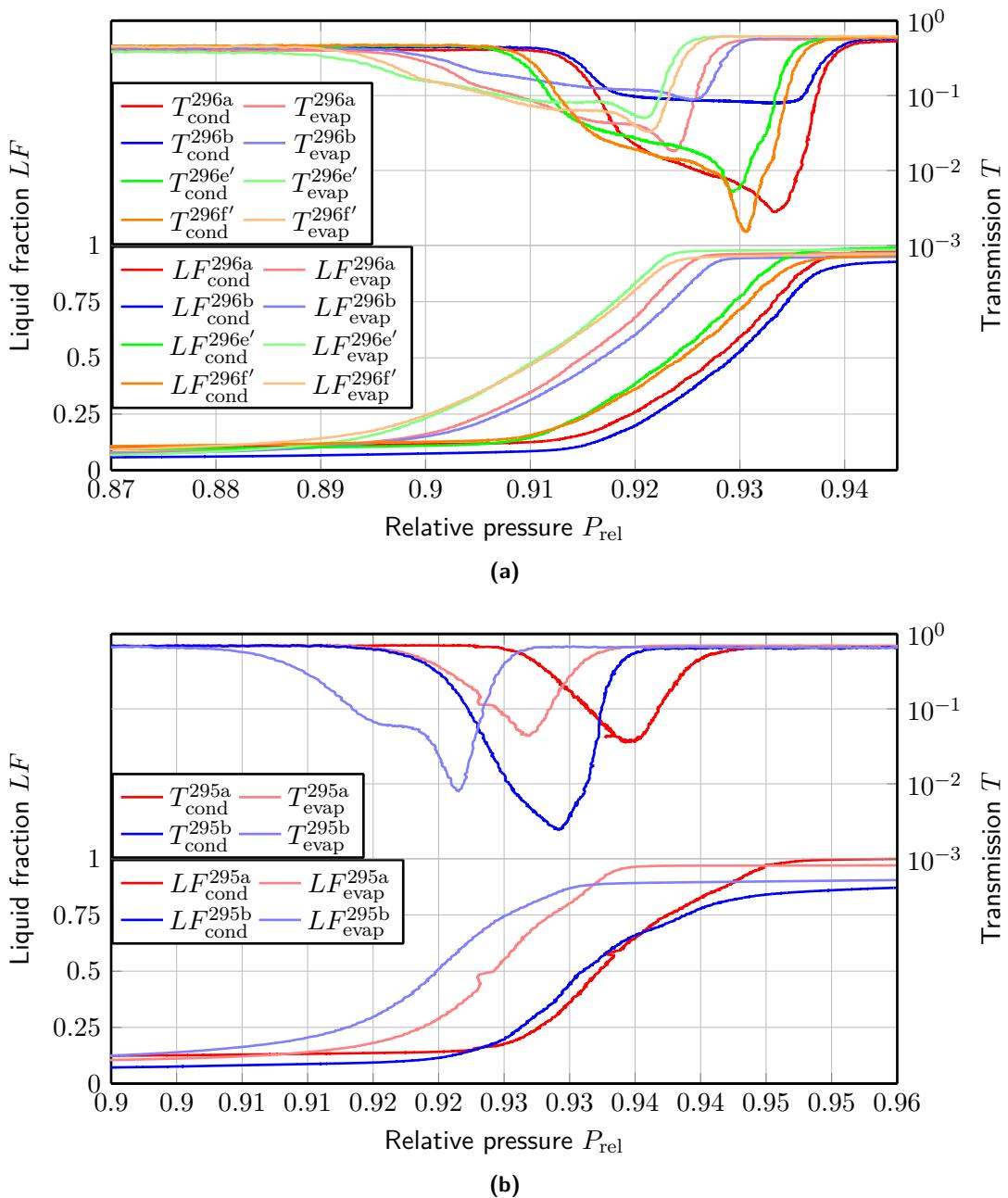
To start with, the wafers shall be tested for inhomogeneities. Therefore, isotherms of one wafer's membranes which are in the same technical state, meaning they have undergone exactly the same treatments, are compared. This is done for both, closed pore membranes and open pore membranes. Because opening the membranes' pores involves one more production step, here, closed pore membranes are regarded first.

Figure 4.5 shows a comparison of closed pore membranes for wafer 295 and 296. Even though the membranes 296e' and 296f' had already been treated using phosphoric acid at the time of the measurements, the pores are still assumed to be closed as will be explained in section 4.4.

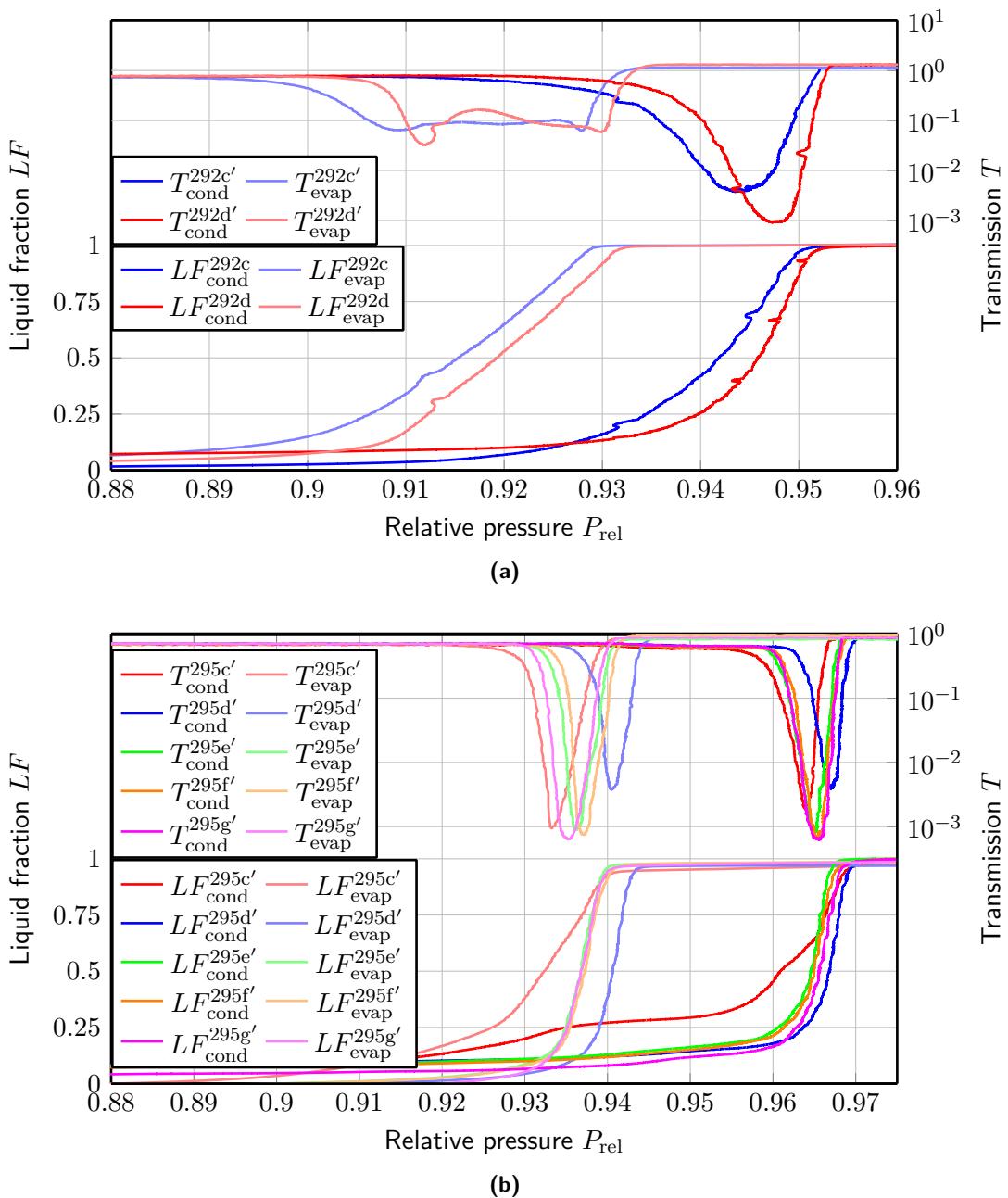
While for both wafers, with one exception being membrane 295c, the overall shape of the different membranes' volumetric isotherms matches, they are distributed along a short distance of the  $P_{\text{rel}}$ -axis. As long as the shapes and also the size of the hysteresis match, this can be explained by a differing pore size distribution for the different membranes. NEED DIAMETER CONVERSION FOR THIS??? Membrane 295c shall not be analysed at this point as it will be dealt with in detail in section 4.8. Moreover, also the transmission measurements yield optical signals of similar shapes. Unclear at this point is the variation in magnitude that can be extreme for some membranes as the example of 296f' compared to 296b shows.

### 4.4 Comparison of closed and open pores

Show comparison of 294, 295 and 296. Speak about the context to theory. Testing the efficiency of opening procedure. Theory test relies on the fact that pores are well open. ADD ONE THAT DID



**Figure 4.5** Comparison of closed pore membranes of one wafer. (a) compares membranes of wafer 296 while fig. 4.5(b) deals with 295.



**Figure 4.6** Comparison of open pore membranes of one wafer. (a) compares membranes of wafer 292 while fig. 4.6(b) deals with 295.

## NOT WORK

Hysteresis for closed: corrugations  
Hysteresis difference: Coherent with theory

This section shall serve to determine a systematic change of the isotherm by the *barrier layer* dissolution process which opens the pores on the bottom side. Moreover, the coherence with theory shall be regarded. Figure 4.7 shows the comparisons of closed pore and open pore membranes of the wafers 295 and 296. For both, closed and open pore measurements, the same membranes are used before and after the *barrier layer* dissolution to leave no doubt as to the inhomogeneities of the wafers.

Firstly, in reference to the model explained in ??, the occurrence of a hysteresis for the volumetric isotherm of a closed pore membrane must be explained. The answer to that question has already been given by (???cite bruschi???: It occurs due to intra pore corrugations. The modulation of the diameter along the pore's length corresponds to a varying equilibrium pressure. This makes for a non vertical isotherm.

Next, the difference between the isotherms for closed and open pores is regarded. Clearly, the size of the hysteresis increases. This tendency is coherent with theory as the latter predicts a hysteresis for open pores but as mentioned above, none for closed pores. Moreover, the evaporation branch of the open pore isotherm is shifted towards higher pressures as compared to the closed pore isotherm. That implies an increase of the pore diameter upon dissolving the *barrier layer*.

To prove that all the closed pore membranes of wafer 296, of which some have been treated using phosphoric acid, are indeed closed pore membranes, they are added to the graph of the membranes 296b and 296b' as shown in fig. 4.8. The comparison of the different membranes yields a significant difference of the hysteresis' size of 296b op and all other membranes, which show a much smaller hysteresis. As the size of the hysteresis for the rest of the membranes is approximately uniform and the variation of the condensation and evaporation pressures are only slightly shifted, this implies that indeed, all membranes except 296b op contain pores open only on one end. Which cannot be observed though, that is whether the pores already have microscopic openings on the barrier layer side. If that were the case, hexane would condense there at spinodal pressures lower than the equilibrium pressure of the small ends. Hereby, the pores would be left in a closed shape. This case would not be visible on the volumetric measurements as the condensed amount of hexane necessary to close the pores were so small. If the openings were so large already as for the spinodal pressure to be larger than the equilibrium pressure of the small end, in explanation

$$P_{\text{sp}}(d_{\text{pore}}) \leq P_{\text{eq}}(d_{\text{pore}}), \quad (4.13)$$

where  $d_{\text{pore}}$  is the small end's pore diameter, that case would be visible on the isotherm because whole pores would fill at higher pressures. Therefore, the latter case can be excluded.

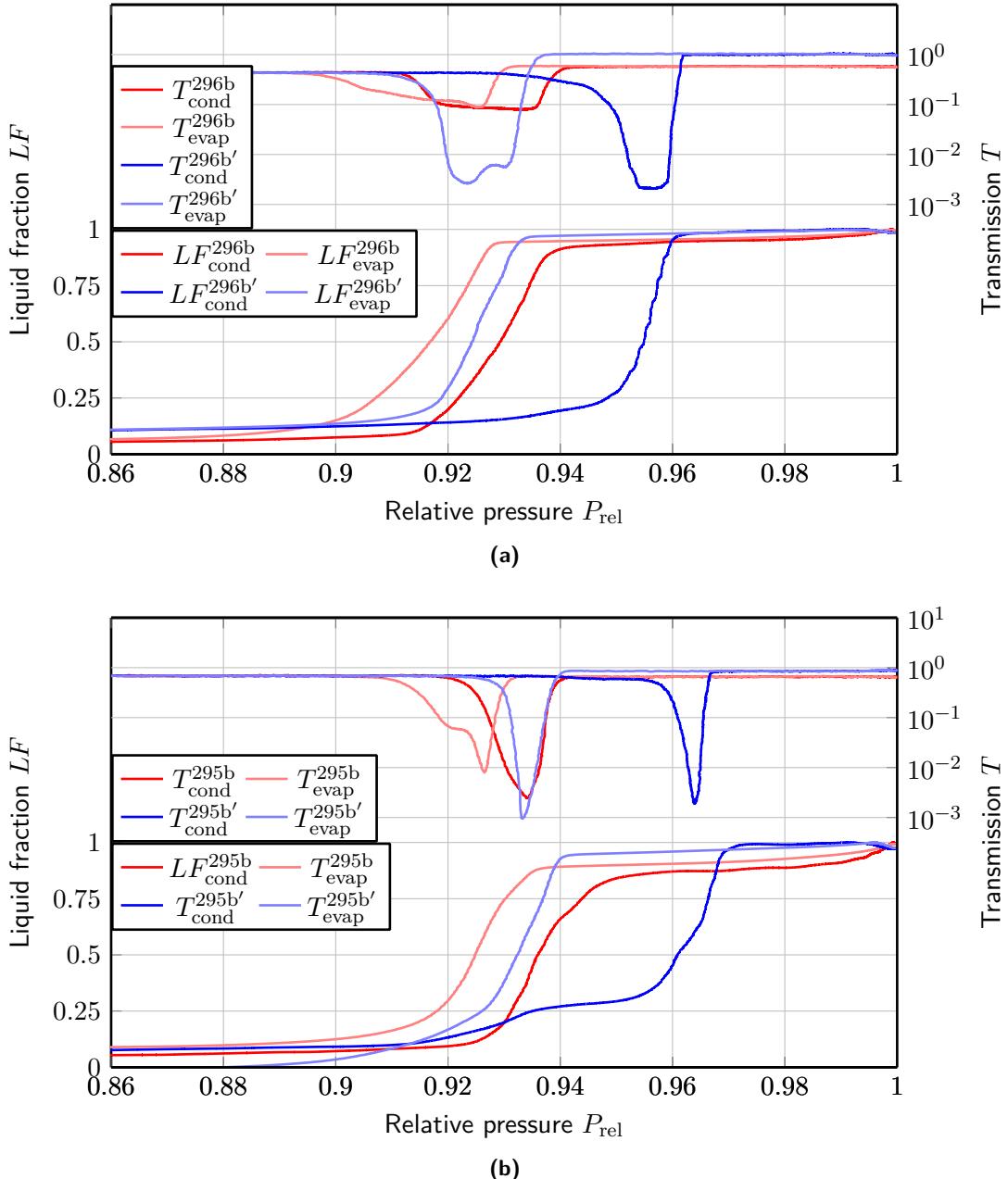
### 4.4.1 Bad open pores

Talks about 294 and leads to

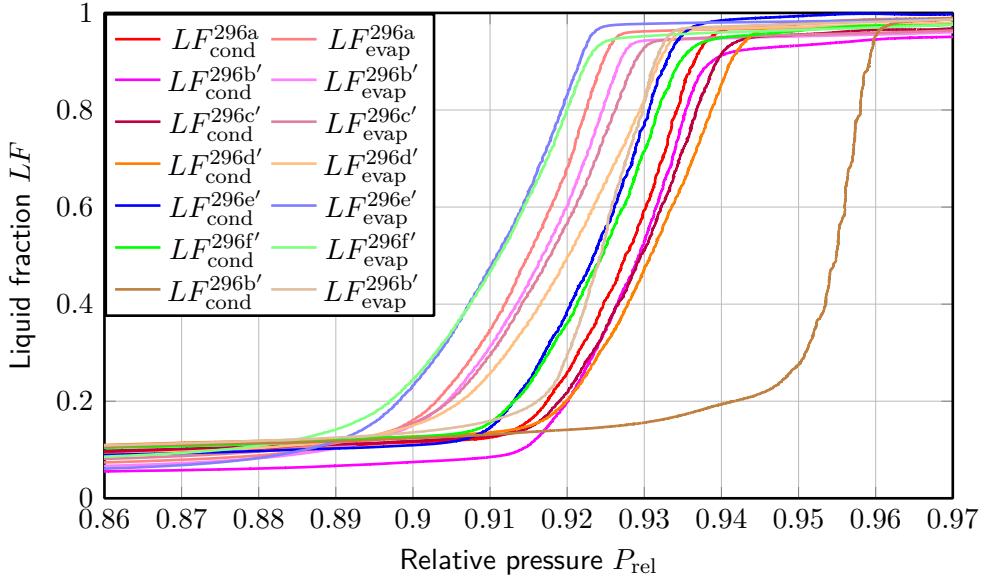
### 4.4.2 Inverse funnelling

What stings the eye of the attentive reader is that the evaporation branch also becomes more sharp for the open pores.

An explanation of the latter two phenomena can be taken from the production step of the *barrier layer* dissolution. As displayed in fig. 4.9(a), the wafer at some point becomes milky. Comparing these milky aspects to images taken during the condensation process of an isotherm as displayed in ??? leads to the conclusion, that at this point some of the pores start filling or are already filled with phosphoric acid. This phenomena lasting for a couple of minutes is followed by fifteen more



**Figure 4.7** Comparison of the isotherms of membranes with closed pores to those with open pores. (a) shows membranes of wafer 296, while (b) displays those of wafer 295. The increase of size of the hysteresis is clearly observable.



**Figure 4.8** Full comparison of the closed pore membranes of wafer 296 with the open pore membrane 296b'.  
For interpretation please refer to section 4.4.

minutes of floating until the wafer is completely covered by acid that flowed through the now open pores (compare fig. 4.9(b)). That means during at least

$$t_{\text{filled}} = 15 \text{ min} \quad (4.14)$$

the pores are filled by phosphoric acid. That at the end of the process, the wafer is covered by a clearly visible layer of acid, means that there must be some flux of acid through the pores. On the other hand, taking into account the sharpening evaporation branch of the volumetric isotherms implies either a sharpening pore size distribution or a decrease of the funnelling or corrugation aspect of the pores.

By linking the occurring milky aspects to the filling of only some of the pores, meaning not all pores fill at the same time but over a span of

$$t_{\text{milky}} = 3 \text{ min}, \quad (4.15)$$

implies that the pore size distribution should rather be increased than decreased. Excluding this point only leaves corrugations and funnelling as explanations for the sharpening isotherms. As there is no reason to believe that an etching process could flatten a corrugated surface though, the straightening of the pores is more likely. Moreover, this inverse funnelling could be explained by the acid saturating along the axis of the pores. The theory of inverse funnelling is probed by experiments that will be analysed in section 4.4.2.

#### 4.4.2.1 Immersion experiment

Derive and explain etch rate gradient and influence on the pores' shape.

Understanding the inverse funnelling becomes one of the main goals of the experiments with wafer 296 as it might be used to correct the shapes of the pores of a given membrane. Therefore, immersion experiments where two closed pore membranes are immersed in phosphoric acid for

$$\begin{aligned} t_{\text{im}}^{296c'} &= 6.5 \text{ min}, \\ t_{\text{im}}^{296d'} &= 13 \text{ min}, \end{aligned} \quad (4.16)$$

and then the shapes of the volumetric isotherms compared to each other and addition with an untreated closed pore membrane. Focus lies on the shape of the isotherms. Small shifts in diameters



**Figure 4.9** Images taken of wafer 295 during the *barrier layer* dissolution process. (a) shows milky aspects that appear after approximately twenty minutes while (b) has been taken just before removing the wafer from the acid. At this point the whole surface of the wafer is covered by phosphoric acid that passed through the pores.

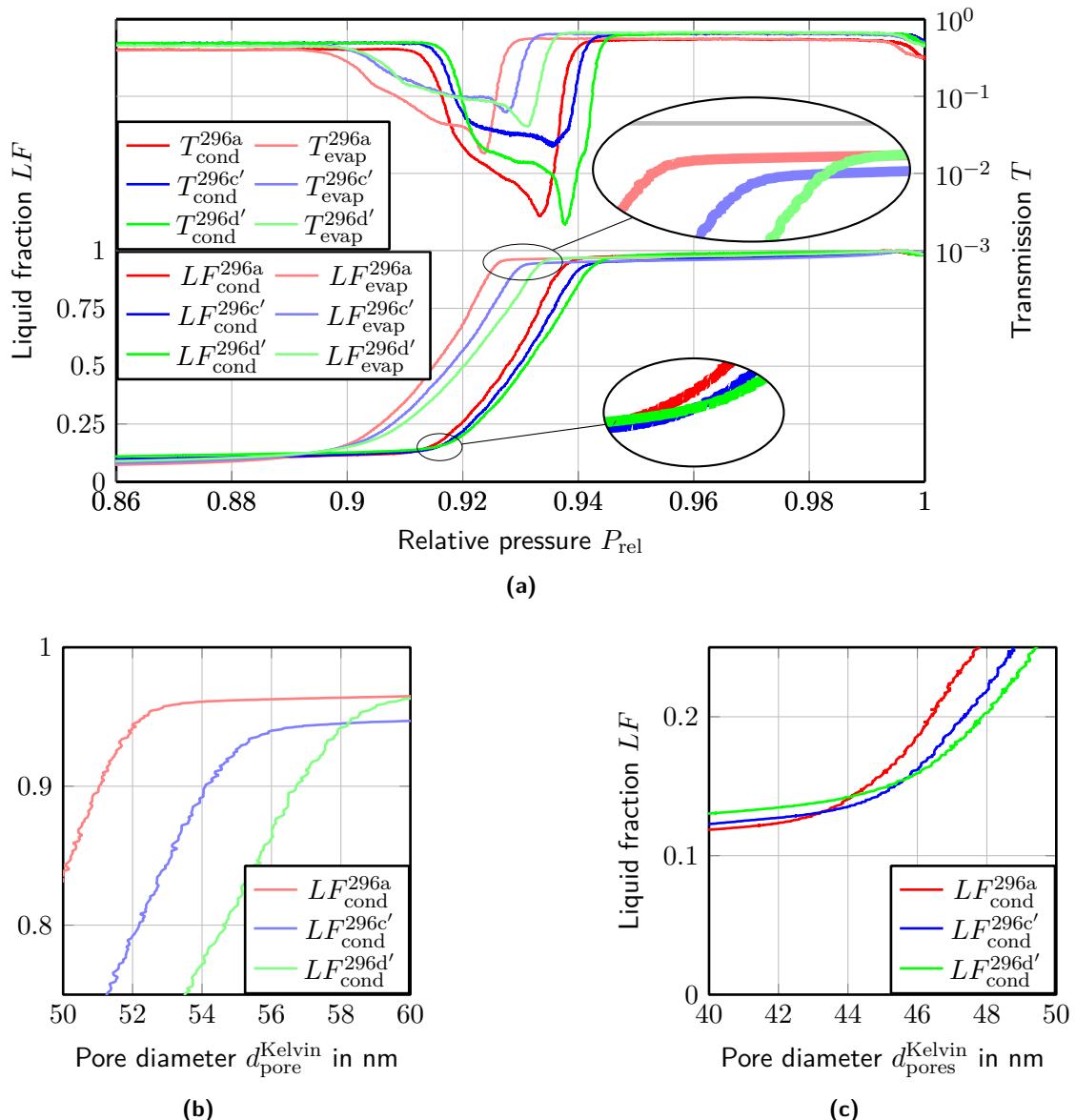
**Table 4.2** Diameter reduction per minute of immersion derived from the isotherms of the membranes 296a, 296c, 296d.

$t_{\text{im}}[\text{min}]$	$\Delta d_{h=60 \mu\text{m}}[\text{nm}]$	$\Delta d_{h=0 \mu\text{m}}[\text{nm}]$
0	0	0
6,5	3	0
13	6	0

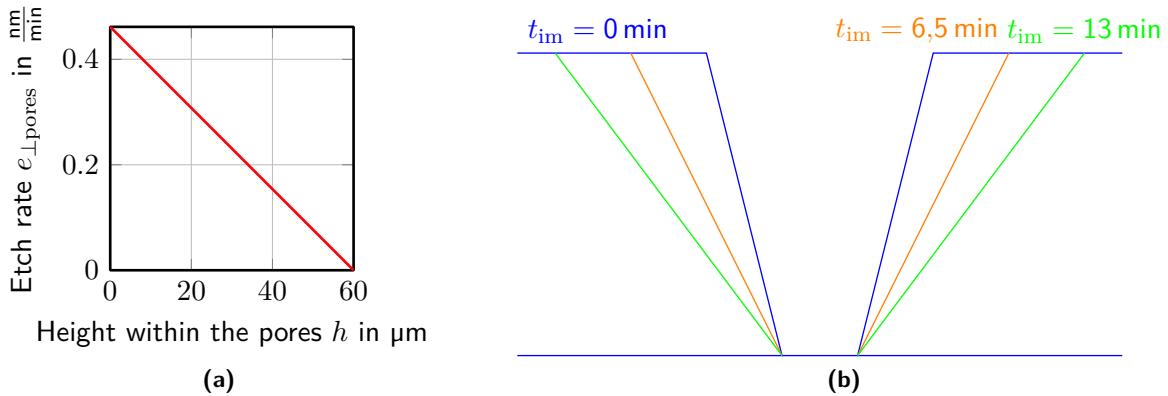
are of no interest as the inhomogeneity of the pore size distributions of a wafer has been proven already in section 4.3.

Figure 4.10(a) compares the volumetric and also the transmission measurements of the immersed membranes 296c and 296d, again adding the untreated membrane 296a. As explained in ??, condensation and evaporation in a closed funnelled pore occur at equilibrium pressure. Pores that are open on the large end start filling from the bottom and evaporating from the top so, regarding the isotherms in fig. 4.10(a), the lower end of the isotherm rising represents the small bottom end of the pores. This lower end of all three isotherms seems to be superimposed while the top end, representing the large open end of the pores, moves to larger diameters for longer immersion times. As the effect seems to occur linearly over the whole length of the pores, the acid seems to be saturating within the pores losing etching power. By ??, the process can be visually interpreted as a pore straightening as shown in fig. 4.11(b). Moreover, the increase of the funnelling aspect seems to be linear at least within the first 13 minutes of the immersion as doubling the immersion time yields double the diameter shift on the volumetric isotherm (compare ??). For instance, table 4.2 shows the diameter increase of the pores due to the immersion of the membranes in phosphoric acid. Using this data along with the assumption of a linear etch rate gradient along the length of the pore, the respective etch rate can be plotted as shown in fig. 4.11(a). Here, the parameter  $h$  is used as the height within a vertical pore, where  $h = 60 \mu\text{m}$  refers to the open top end of a  $60 \mu\text{m}$  long pore that is closed on the bottom side. The effect, that reduces the funnelling aspect of the pores when floating the membranes on phosphoric acid as to dissolve the *barrier layer* shall be referred to as *inverse funnelling* from now on.

As for the transmission measurements, the shifts of the beginning of the condensation dip and also the end of the evaporation dips correspond to the interpretation explained above. Ob the other



**Figure 4.10** Membrane 296c' has been immersed in phosphoric acid for  $t_{296c'} = 13$  min, 296d' for  $t_{296d'} = 26$  min. (a) shows the isotherms of the immersion experiment conducted using wafer 296. The shift to larger pressures of the beginning of the evaporation branch and the unmoving beginning of the condensation branch are clearly visible. (b) and (c) are higher resolution plots of the relevant areas of the evaporation and respectively condensation branch of the isotherm on a pore diameter scale. For interpretations please refer to ???. ???EXPLAIN WHY EVAP START AND COND START ARE THE SPOTS TO LOOK AT ???



**Figure 4.11** Immersion of a closed pore membrane resulting in an increase of the funnelling aspect of the pores as shown in (b) due to the saturation of the acid within the pores. The visualized theory is backed by the isotherms in fig. 4.10(a) which lead to the etch rate dependency plotted in (a) on the height within a pore. For further explanations please refer to ??.

hand, the magnitude difference of the three isotherms' dips cannot be explained, neither interpreted at this point.

#### 4.4.2.2 Inverse funnelling upon barrier layer dissolution

Explain that the pores appear to be straightened bc of floating. Refer to the theory, that there are two sorts of alumina (pure and acid polluted).

With the conclusions reached in section 4.4.2.1, it is clear now that indeed, the *barrier layer* dissolution process reduces the funnelling of the pores. One more thing still does not fit into the great picture, though, which is that the kink of the volumetric isotherm of membrane 295b (compare ??) disappears upon pore opening. So far, the etch rate has been proven to show a gradient along the length of the pore, but a linear one which cannot account for this type of change in shape.

Therefore, a different explanation must exist to account for this change. cite the nice book here and explain the two sorts of alumina which are etched at different rates. Check if that can be true with the thickness of that thing

### 4.4.3 Etch rate difference

#### 4.4.3.1 Pore opening widening pores much less than expected

The thickness of the *barrier layer* of wafer 292 has been determined to be

$$d_{\text{barrier-layer}} = 30 \text{ nm} \quad (4.17)$$

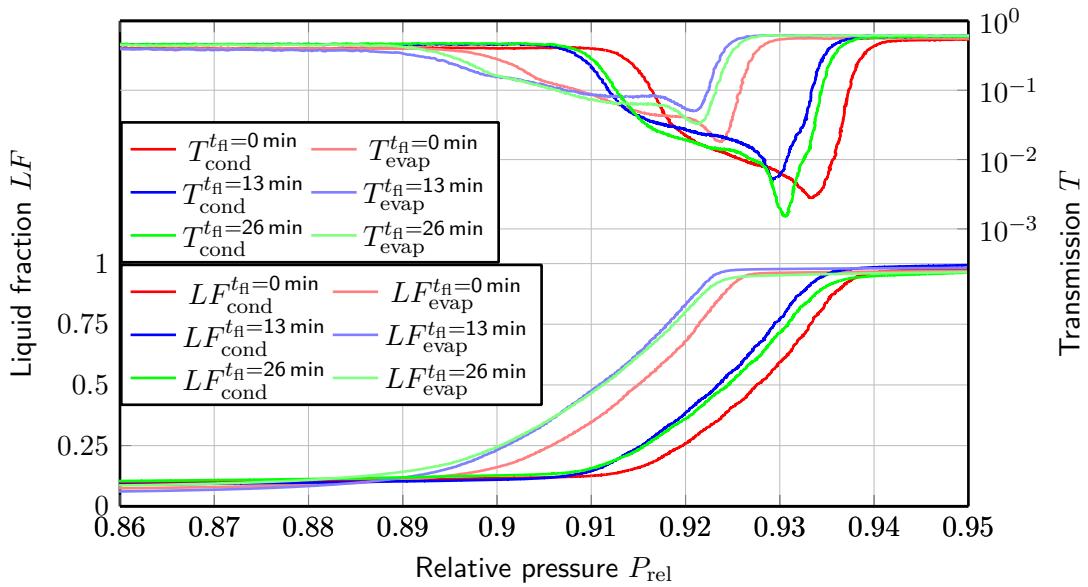
by electron beam microscopy. After having been floated for

$$t_{\text{float}}^{292} = 20 \text{ min}, \quad (4.18)$$

milky aspects as shown in fig. 4.9(a) appeared. As the latter are assumed to imply that the *barrier layer* is etched off the wafer, this makes for an etch rate of

$$e = 1,5 \frac{\text{nm}}{\text{min}}. \quad (4.19)$$

This result is drastically different from the etch rate computed in section 4.4.2.1 and thus raises questions regarding the etch rate of phosphoric acid on alumina.



**Figure 4.12** Comparison of the isotherms measured for the membranes 296a, 296e' and 296f'. While the pore diameters are marginally smaller for the membranes 296e' and 296f' than they are for 296a, the overall picture is equivalent. It makes for closed pores (or constricted open pores as explained in section 4.4) with the same funnelling aspect.

Using the result eq. (4.19) for further calculations yields a theoretical pore diameter increase of

$$\Delta d_{\text{pore}} = 22.5 \text{ nm} \quad (4.20)$$

during the fifteen minutes etching of filled pores when disregarding the acid saturation within the pores. Nevertheless, even regarding the saturation, the bottom end of the pores that is exposed to the bulk acid reservoir should be widened dramatically which is not observed on either electron beam microscopy images nor the volumetric measurements. Further analysis on the difference of the etch rate parallel to the pore axis  $e_{\parallel}$  and perpendicular to the axis  $e_{\text{perp}}$  follows in section 4.4.3.

As a way to not increase the distribution of pore diameters on a given wafer, the idea of floating the wafer on acid for a time just short enough to not open any pores, followed by its full immersion in acid has been developed. As to not increase the pores diameter by too much regardless of the acids saturation, the immediate immersion of the whole wafer without prefloating discarded. Again, the acid's etch rate on the *barrier layer* is a prerequisite and shall be deduced in section 4.4.3.

#### 4.4.3.2 Floating experiment

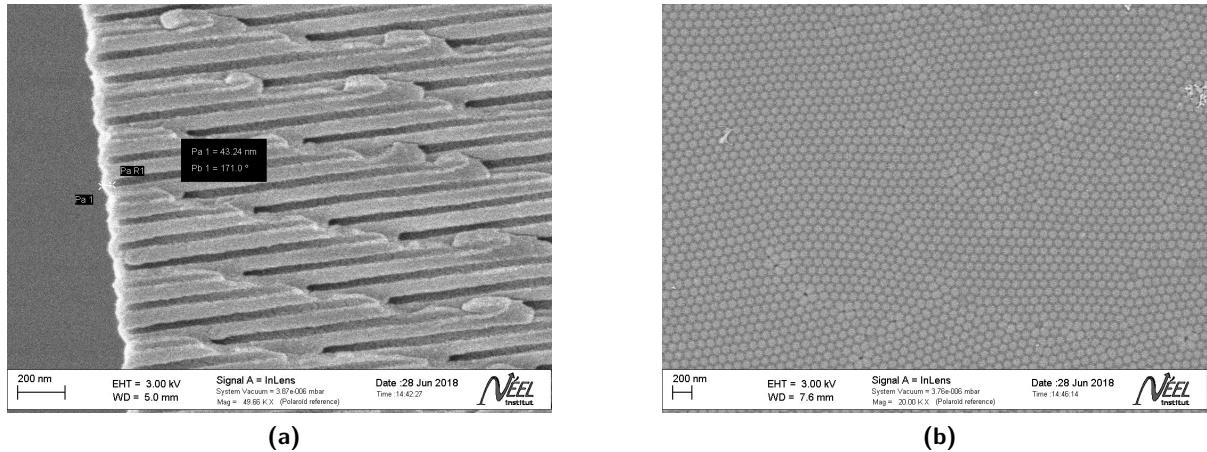
Explain that the shapes of the isotherms are correct, but that no real conclusion could be made due to the bad MEB views.

In order to calibrate the etch rate on the *barrier layer* of a give wafer and to try to reduce its thickness in order to immerse the wafer after for the final pore opening, two membranes are floated on phosphoric acid for

$$\begin{aligned} t_{\text{fl}}^{296e} &= 13 \text{ min}, \\ t_{\text{fl}}^{296f} &= 26 \text{ min}. \end{aligned} \quad (4.21)$$

After, measurements are conducted and the results compared to membrane 296a, which is an untreated membrane in closed pore state, for a reference (fig. 4.12). While a slight shift in diameter between the floated membranes and the untreated one is visible, this is assumed not to be due to the treatments but rather due to the inhomogeneity of a given wafer. Moreover, the shapes of the isotherm do not show any significant slopewise deviation. Still, as explained before, the membranes

could include pores badly open on the *barrier layer* side. Anyways, to probe the thickness of the *barrier layer*, electron beam microscopy is used and along with the cross section, the two sides of the membranes are imaged. Due to the drift that could not be resolve, the attempt to measure the thickness of the *barrier layer* did not work out well as can be seen on fig. 4.13(a). On the other hand, the views of the aluminum side of 295e' (fig. 4.13(b)) confirm that the pores of the membrane remain closed on the bottom side.



**Figure 4.13** Electron beam microscopy images of membrane 296e' that has been floated on acid for  $t_{\text{fl}} = 13 \text{ min}$ . (a) shows the cross section view with the attempt to measure the thickness of the membrane's *barrier layer*, while (b) is the aluminum side on which the membrane has been floated on.

#### 4.4.4 Do thinner membranes improve things?

Compare 295 and 296. Talk about the sharpness of both, the volumetric and the optical isotherm. Also speak about the rather broad isotherm for closed pores of 295 which is not understood. Use diameter translation by Kelvin law!!

Wafer 295 is only

$$l_{\text{pore}}^{295} = 30 \mu\text{m} \quad (4.22)$$

thick. Hereby, the effect of the funnelling observed upon the previously measured membranes of a thickness of

$$l_{\text{pore}}^{292,293,294,296} = 60 \mu\text{m} \quad (4.23)$$

is expected to be reduced. Assuming that the funneling aspect is linear implies a reduction of the effect by half which should lead to a sharper evaporation branch.

?? shows the comparison of the membranes 295a and 296b on a KELVIN diameter axis. Both membranes' pores are closed by the *barrier layer* on the bottom side. In contrast to expectations, the evaporation branches show a similar spread

$$\begin{aligned} \Delta d_{\text{evap}}^{295a} &= 15 \text{ nm} \\ \Delta d_{\text{evap}}^{296b} &= 17 \text{ nm}. \end{aligned} \quad (4.24)$$

To determine the latter, the volumetric isotherms' rise and also the transmission drops have been regarded. At this point, assuming some uncertainty also due to the slightly different values derivable from optics and volumetrics, the funneling aspect seems unchanged by moving to thinner membranes. But, looking at the condensation branches of the volumetric isotherms could bring clarity. While the condensation branch of membrane 296b shows approximately the same slope and shape as its evaporation branch, for membrane 295a this is not true. The latter membrane's condensation branch

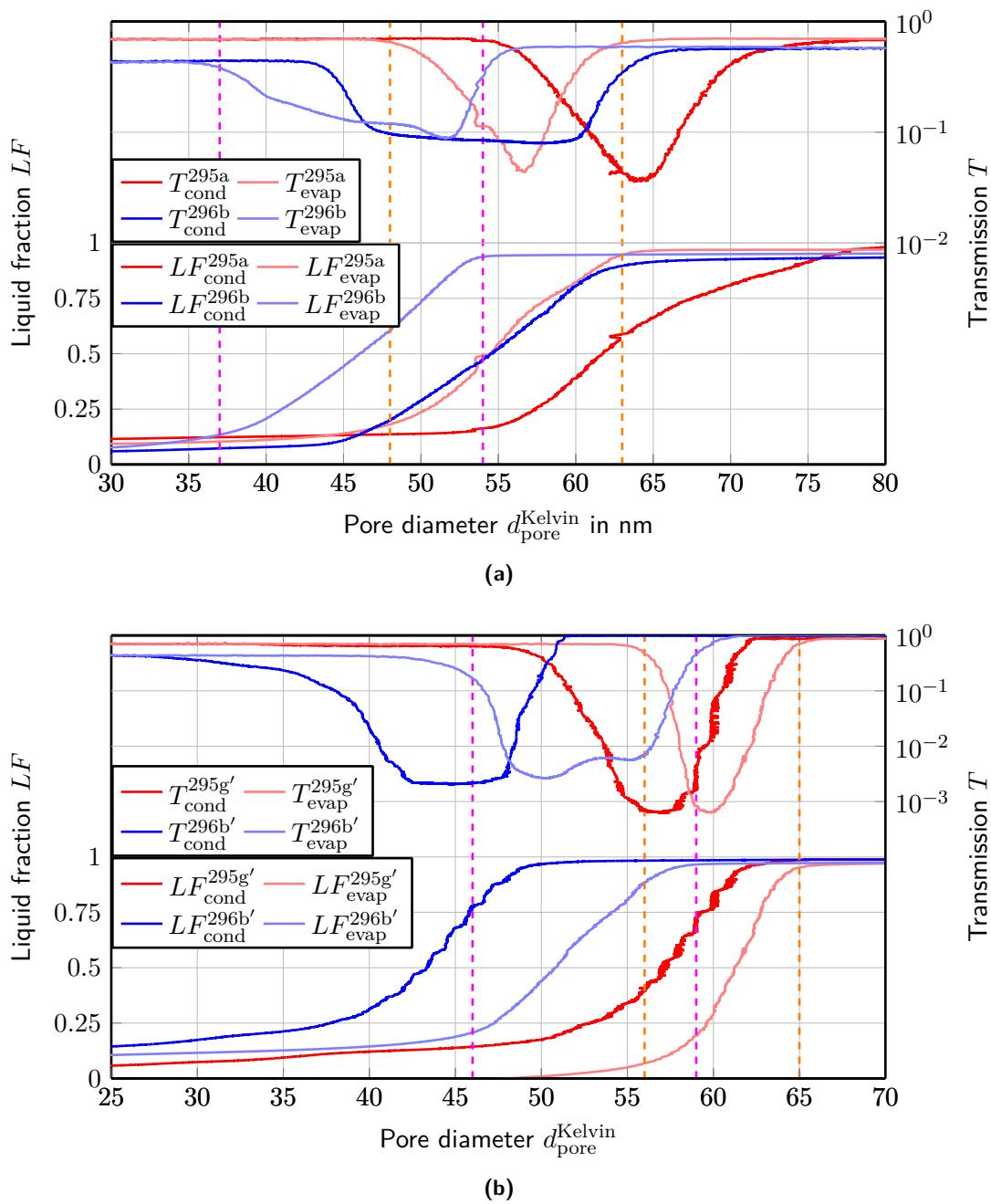


Figure 4.14

spreads out over about 25 nm so it is much broader than its evaporation branch. This can only be explained by severe corrugations within the pores as straight funnelling should not cause any differences in shape between the condensation and evaporation branches according to ???. The transmission signals match in magnitude for both membranes while it is much sharper for the thinner one. As a first guess, this could be interpreted as a sign more less flawed or even less corrugated pores, though that would contradict the before made analysis. In conclusion, from the closed pore isotherms no conclusion can be drawn as to how the funnelling aspect is affected by reducing the membrane thickness.

Figure 4.14(b) then shows the isotherm comparison of the open pore membranes 295g' and 296b'. For these isotherms, the condensation does match the evaporation branch shapewise. The spread of the evaporation is

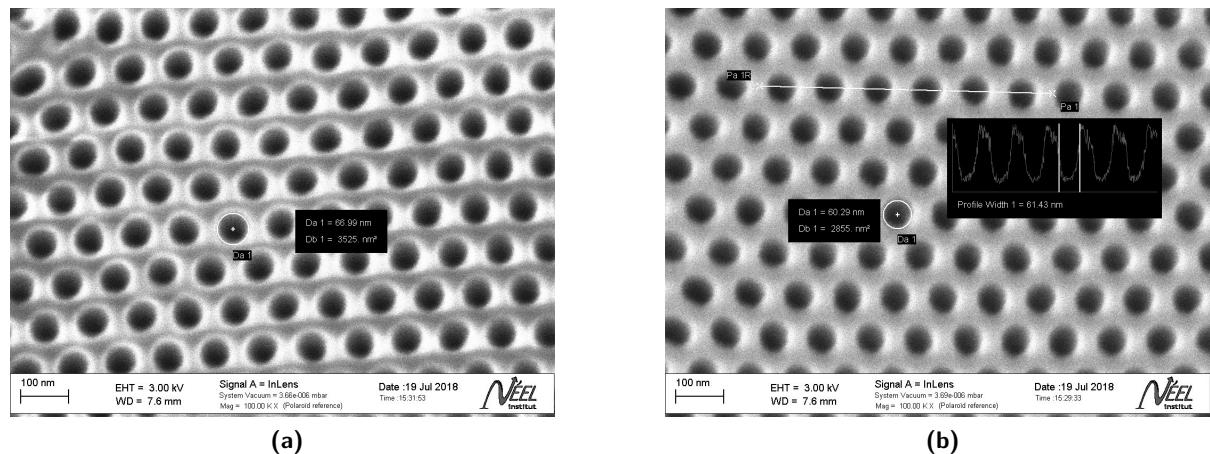
$$\begin{aligned}\Delta d_{\text{evap}}^{295g'} &= 9 \text{ nm} \\ \Delta d_{\text{evap}}^{296b'} &= 13 \text{ nm.}\end{aligned}\quad (4.25)$$

Again, the transmission drops for the thirty micrometer membrane 295g' are more sharp but within the same magnitude as those of 296b'. A difference in funnelling seems more probable from this measurement even though, the bottom line is that no precise conclusion can be drawn from the measurements at this point.

For more clarity, electron beam microscopy is used to check the difference of the diameters on solution and aluminum side. Figure 4.15 shows the images for the membranes 295g' and 296b' which state a diameter offset of about

$$\begin{aligned}\Delta d_{\text{sem}}^{295g'} &= 6 \text{ nm,} \\ \Delta d_{\text{sem}}^{296b'} &= 6 \text{ nm.}\end{aligned}\quad (4.26)$$

So the SEM images show the same tendency as the volumetric and optical measurements.



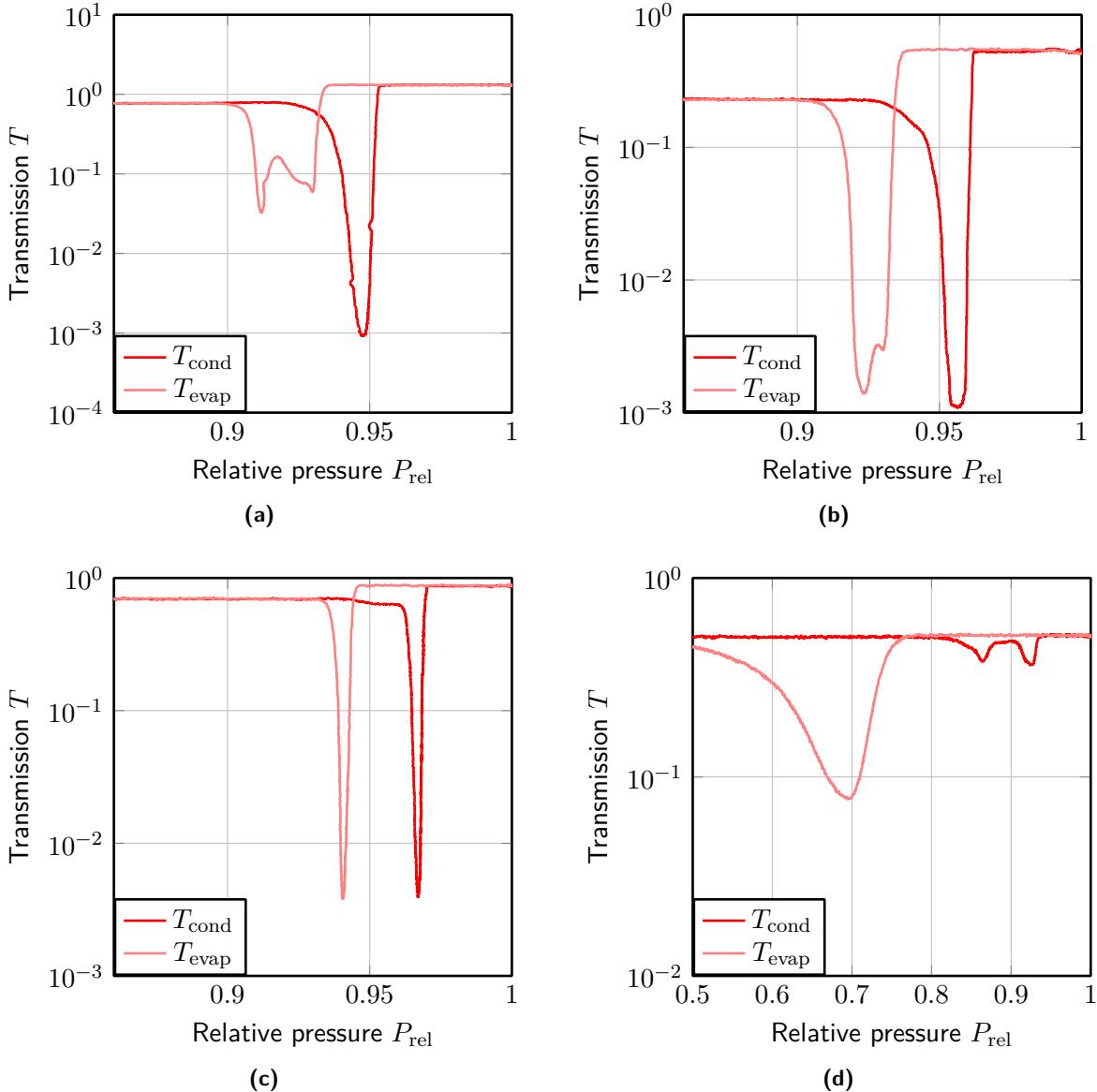
**Figure 4.15** Electron beam microscopy images of membrane 295g' with measurements of the pore diameters on the solution side (a) and aluminum side (b).

To conclude with, even though the effect is not as significant as expected, thinner membranes indeed do improve the pore quality.

#### 4.4.5 Transmission signal not well understood

To begin with it must be mentioned here, that all open pore membranes measured before the wafers 295 and 296 have shown the same transmission characteristics in regard of the significant magnitude difference of the condensation and evaporation isotherm branch which can be seen on ???. Therefore,

a theory to explain this phenomenon were developed. The prominent one at the beginning of the conducted experiments mentioned in this report shall be explained in the following.



**Figure 4.16**  $P_{\text{rel}}$  transmission isotherms of the membranes 292d (a), 296b (b), 295d (c), and 295f 200ALD (d). All membranes have open pores. Unlike the isotherm of membrane 292d, the transmission drops of condensation and evaporation are of the same magnitude. The magnitudes of condensation and evaporation dip are reversed in respect to membrane 292d for membrane 295f 200ALD.

Firstly, a completely filled membrane should always yield a higher transmission coefficient  $T$  than it would in its dry state according to the theory of index matching explained in ???. This fact serves as a tool to optically detect membranes that do not fill completely due to constrictions which by experience show a weaker transmission after the condensation process is complete than they did before. Furthermore, due to the disorder created by pore filling and emptying, the transmission drops during the processes. Phenomena occurring on the volumetric measurements can therefore be linked to the measured transmission coefficient.

Moreover, the phenomenon of the transmission dropping to lower values for the condensation than for evaporation branch of a given isotherm has been repeatedly observed on open pore membranes. An example is given by membrane 292d's isotherm which is displayed in fig. 4.16(a). At this point it must be mentioned that all open pore membranes measured before the wafers 295 and 296 have

shown this same transmission characteristics. As interpretation serves the degree of disorder caused inside the membrane by the respective process. As the membrane contains pores open on both ends, the condensation occurs at spinodal pressure  $P_{sp}(d_{pore})$ . Due to the distribution of pore sizes, funnelization, corrugation and constrictions, the pores fill at different pressures  $P_{sp}^1 \neq P_{sp}^2$ . At a given pressure

$$P_{sp}^1 < P < P_{sp}^2,$$

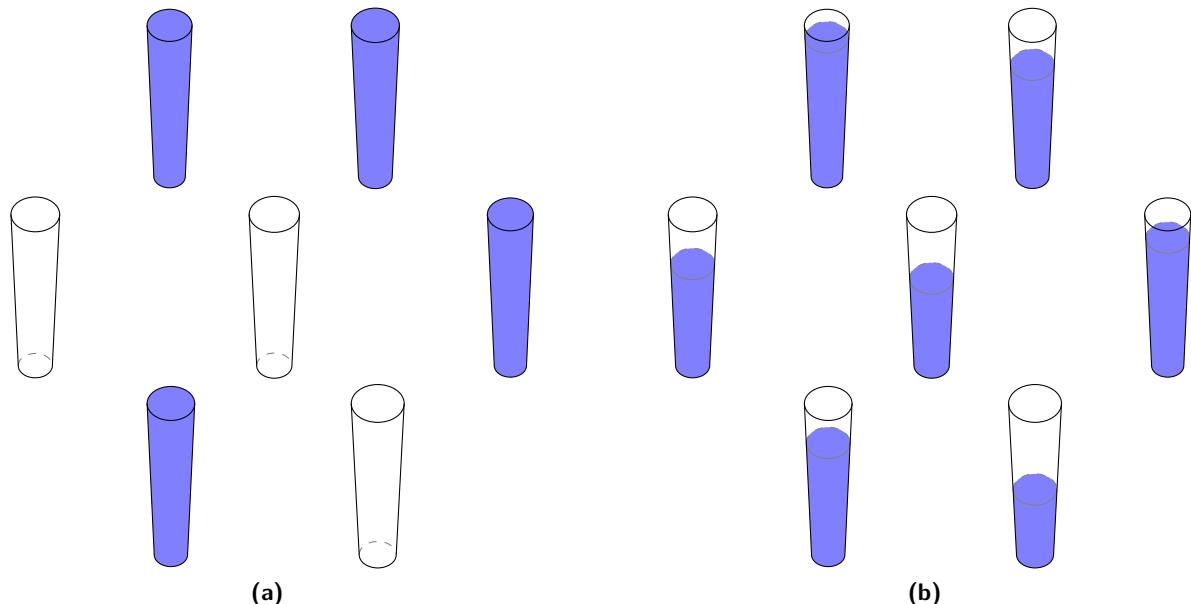
where  $P_{sp}^1$  shall correspond to the smallest pore diameter found on the membrane and  $P_{sp}^2$  the largest one, the state of the membrane regarding filled and empty pores is assumed to be comparable to figure fig. 4.17(a). The hexane evaporates at equilibrium pressure  $P_{eq}$ , though. That means that, assuming the same pore size distribution, funnelization, corrugation and constrictions, the pores empty continuously. The theoretical state of the membrane is visualized in fig. 4.17(b).

The difference is given by the most significant contrasts between neighboring pores during the condensation process, in explanation empty and filled pores, for spinodal condensation, while for evaporation at equilibrium pressure the pores only show different levels of liquid during most of the process. As a result, the absorption of hexane creates a higher grade of disorder than the desorption and therefore causes a more significant drop of the transmission coefficient (compare fig. 4.16(a)).

The splitting of the evaporation drop into two dips separated by a small local maximum cannot be explained by this theory, nor by any other means mentioned in this report. Moreover, the later analysed membranes of wafer 295 and 296 yield a more even dip distribution (compare fig. 4.16(c) and fig. 4.16(b)) and upon reducing the pore diameter of 295 using ALD, the membranes even show the inverse behaviour (fig. 4.16(d)).

In connection with the sharper isotherms, the first phenomenon could be explained by the pores being less flawed talking corrugations and funneling. The latter assumption is backed by the fact, that the transmission drops of 295d are of smaller magnitude than those of 296b. While both are open pore membranes, membrane 295d is only half as thick as 296b, meaning the pores are only half as long and therefore the influence of the funneling aspect is reduced respectively by half.

The second one remains unclear though.



**Figure 4.17** Disorder between neighboring pores during absorption (a) and desorption (b). Important is the larger degree of disorder upon the absorption process. Upon condensation pores fill immediately when the spinodal pressure  $P_{sp}(d_{min})$  is reached, where  $d_{min}$  is the radius of the opening at the small end. The evaporation is continuous at equilibrium pressure  $P_{eq}(d)$  and empties each pore simultaneously while the diameter  $d$  is large enough.

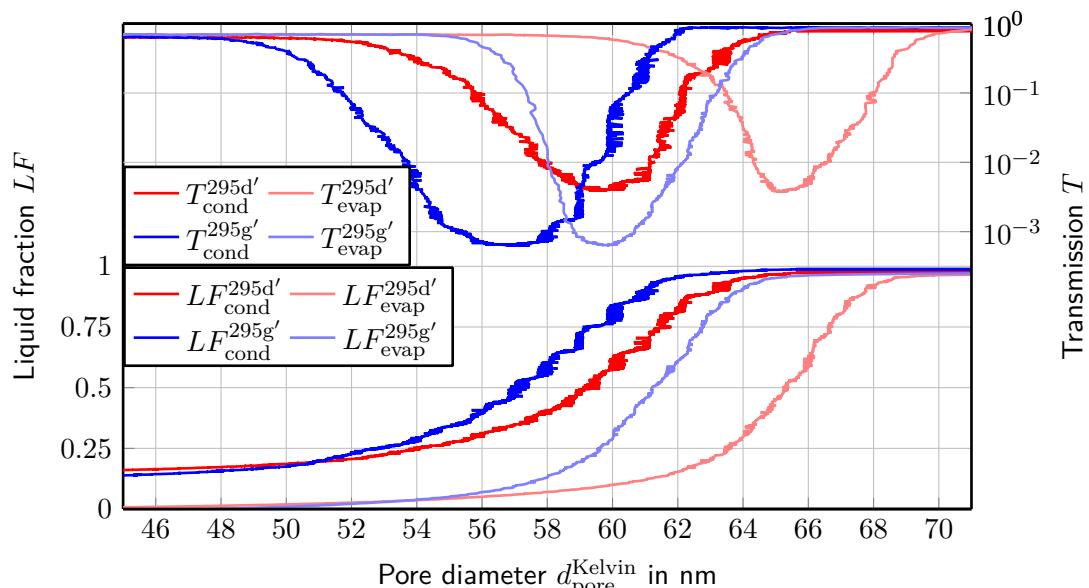
## 4.5 Pore quality linked to transmission drop and hysteresis

As of now the shapes of the isotherms are more familiar to the reader, at this point the isotherms of the open pore membranes of wafer 295 are analysed in more detail. For this please refer to the isotherms shown in fig. 4.6(b) of section 4.3. There are two isotherms that sting the eye as they do not blend in: The membranes 295d' and 295g'. Again, the analysis of membrane 295c' shall be postponed. Focusing on 295d' shows that its isotherm is not only shifted to larger pressures in comparison to the other membranes, but also is the hysteresis smaller. Moreover, the transmission drops are of a smaller magnitude for membrane 295d' than for all others. As the pressures translate to diameters

$$d_{\text{pore}} > 60 \text{ nm}, \quad (4.27)$$

KELVIN equation is assumed to be sufficiently correct. The isotherms of the membranes 295d' and 295g', which is from here on used as a representative of the rest of the open pores membranes of wafer 295, are plotted over a diameter axis in section 4.5. Interesting at this point is, that hysteresis is actually smaller for membrane 295g' on a KELVIN diameter scale. Also, the evaporation branch seems sharper which could account for less funnelled pores.

Very weird stuff here... HELP???



**Figure 4.18** Comparison of the isotherms of the membranes 295d' and 295g' on a KELVIN diameter axis. Important for the analysis in section 4.5 is.

## 4.6 Testing theory using electron beam microscopy

## 4.7 Pore size reduction using atomic layer deposition

Finally, as the open pore membranes of wafer 295 prove to be very good in the sense of producing very sharp isotherms and showing similar diameters, the goal of sub ten nanometer pore diameters is resumed. The pore diameters are reduced using atomic layer deposition (ALD). ?? shows the treatments and measurements of the inspected membranes of wafer 295.

### **4.7.1 Atomic layer deposition effectively reduces pore diameters**

The first important question is if ALD works to serve as a diameter reduction at all. Therefore, on membrane 295e' 100 cycles of ALD are conducted and the membrane then probed using the experimental setup and SEM. The measurement results are shown in fig. 4.19. While the result for the first 100 cycles of ALD matches expectations perfectly, the second 100 cycles give a very different impression, though, and its result's discussion shall be postponed in favor of the analysis of 295e' and 295e'' at this point.

Firstly, the shape of the volumetric isotherm does not change for membrane 295e'' in comparison to 295e'. It is only shifted towards lower pressures. Only the hysteresis increases by a little bit which can be explained by the logarithmic context of relative pressure to pore diameters though. Regarding the isotherms of 295e' and 295e'' on a KELVIN diameter axis as shown in fig. 4.19(b), the change of the hysteresis disappears and the evaporation branches show the same spread for both membranes. Furthermore, the diameter reduction by 100 cycles of ALD according to the isotherms is

$$\Delta d_{\text{pore}}^{295e' \rightarrow 295e''} = 20 \text{ nm} \quad (4.28)$$

which makes for

$$\Delta = 0,2 \text{ nm} \quad (4.29)$$

diameter reduction per ALD cycle. This value matches the expectations of

$$\Delta = 0,2 \text{ nm} \quad (4.30)$$

per cycle as explained in ???.

The transmission measurements also yield very sharp drops for the membranes 295e' and 295''. One phenomenon, which has not been observed before, is that the evaporation transmission drop of membrane 295e'' is deeper than its condensation transmission drop. This does not go together with the theory for the before observed inverse phenomenon as explained in ????. Up to this point, no explanation could be found for the observation.

### **4.7.2 Diameter reduction by atomic layer deposition is reproducible**

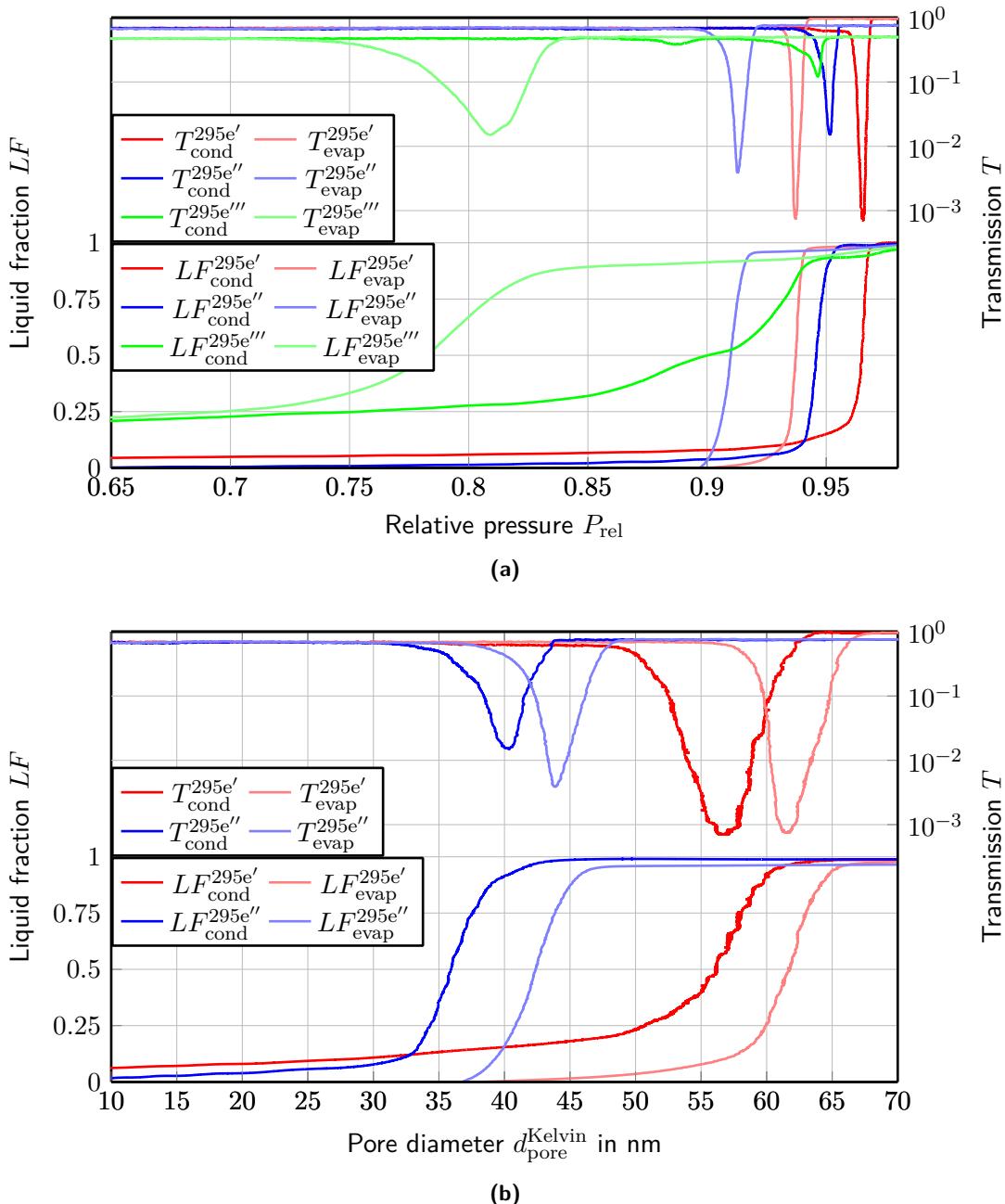
Next, membrane 295e'' and 295f'' must be compared to probe the reproducibility of the pore diameter reduction using atomic layer deposition. As on the one hand the membranes 295e' and 295f' yielded equivalent measurement results as can be seen in fig. 4.6(b) and on the other hand both, 295e'' and 295f'', have undergone 200 cycles of ALD in total, their measurements should produce very similar results.

### **4.7.3 Atomic layer deposition parameters need improvement**

Last, reducing the pores' diameters using a given number of cycles of ALD yields the same results for a deposition in one single run (200 cycles of ALD) and for one conducted in multiple stages (100 + 100 cycles of ALD).

## **4.8 Isotherms proves powerful to detect and characterize defects**

Bring up membrane 293 (constricted pore ends) and membrane 295c (closed pores). MAYBE PUT THIS IN THE CONCLUSIONS CHAPTER???



**Figure 4.19** Comparison of membrane 295e' in initial open pore state and after 100 and 200 cycles of ALD over relative pressure axis in (a). While the shape of the isotherm does not change for the first 100 cycles, the result after the second 100 cycles is drastic. (b) shows the comparison of initial state membrane 295e' and 100 cycles of ALD membrane 295e'' on a KELVIN diameter axis. For analysis please read section 4.7.

## Bibliography

[Cd15] Universität Konstanz: Corporate Design Manual. Universität Konstanz, (2015)