# FTIR and Reaction Kinetics Studies of the Hydrodehalogenation of $CF_2Br_2$ , $CH_2Br_2$ , and $CD_2Br_2$ over a $Pd/\gamma$ -Al<sub>2</sub>O<sub>3</sub> Catalyst

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A combination of FTIR and chemical reaction kinetics studies was employed to investigate the hydrodehalogenation of  $CF_2Br_2$ ,  $CH_2Br_2$ , and  $CD_2Br_2$  catalyzed by  $Pd/\gamma$ - $Al_2O_3$ . The products of the  $CF_2Br_2$ + $H_2$  reaction ( $CF_2H_2$ ,  $CF_3H$ ,  $C_1$ - $C_3$  hydrocarbons) are typical for a reaction mechanism with the participation of : $CF_2$  and : $CH_2$  carbenes as the reaction intermediates. It was not possible to detect : $CF_2$  carbenes by FTIR during the adsorption studies. It is proposed that the carbenes are unstable on the Pd surface in the absence of  $H_2$  and readily decompose to form carbonaceous deposits and adsorbed halogen atoms. Thus, room-temperature hydrogenation of the surface species formed during adsorption of  $CF_2Br_2$  on  $Pd/\gamma$ - $Al_2O_3$  at room temperature yields only  $CH_4$ ,  $CH_2$  and  $CH_3$  and  $CH_4$  carbonaceous formed from dissociation of  $CD_2Br_2$  and  $CH_2Br_2$  adsorbed on the Pd surface are stable at room temperature, as indicated by the formation of  $CD_2H_2$  upon hydrogenation of adsorbed species by  $CH_2$  and  $CH_3$ , respectively.

#### Introduction

Dehalogenation has developed into an important branch of environmental catalysis. Although the macroscopic performance of many catalytic systems has been documented, fundamental research is still needed to develop a molecular level description of the elementary reaction steps. Of particular importance are the factors that affect the activation and cleavage of the C–X bond and the hydrogenation of the surface alkyl fragments and halogen atoms. Both the cleavage of the first C–X bond<sup>1–3</sup> and the hydrogenation of surface chlorine<sup>4</sup> have been proposed to be the rate-determining step of the reaction.

Supported noble metals are used as catalysts for halocarbon conversion reactions.  $^{5-8}$  The rate of C–Cl bond cleavage and the rate of hydrogenation of surface chlorine are sufficiently fast for commercial applications and the deactivation can be controlled.  $^{6,9-14}$  Supported palladium catalysts are selective for the complete hydrodechlorination of CFCs to yield hydrofluorocarbons.  $^{6,9-14}$  Under steady-state reaction conditions, the CF<sub>2</sub>Cl<sub>2</sub> is converted into CF<sub>2</sub>H<sub>2</sub> over alumina-supported Pd with the selectivity higher than 60%.  $^{15}$  On the basis of the analysis of the product distribution of CF<sub>2</sub>Cl<sub>2</sub> hydrodechlorination, it was concluded that the reaction pathway includes the participation of difluorocarbenes.  $^{6,11,12,16}$ 

With CFCs containing two carbon atoms, several surface species have been identified spectroscopically. The adsorption of CF<sub>3</sub>CFCl<sub>2</sub> on the surface of a Pd/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> catalyst at room temperature results in the formation of adsorbed CF<sub>3</sub>CF= carbene and CF<sub>3</sub>C≡ trifluoroethylidyne species that were identified by their IR spectra. <sup>17</sup> These surface species are hydrogenated to CF<sub>3</sub>CFH<sub>2</sub> and CF<sub>3</sub>CH<sub>3</sub>, the products of the CF<sub>3</sub>-CFCl<sub>2</sub>+H<sub>2</sub> reaction, upon exposure to H<sub>2</sub> at room temperature. However, there is no direct spectroscopic evidence that :CF<sub>2</sub>

carbenes form as intermediates during the hydrodechlorination of  $CF_2Cl_2$ . In the presence of hydrogen, supported Pd catalyzes the conversion of  $CF_2Cl_2$  into methane and a mixture of saturated and unsaturated hydrocarbons  $C_1$ – $C_4$ . This indicates that C–F bond dissociation also takes place on the Pd surface and suggests that, similar to the Fischer–Tropsch reaction,  $^{18-20}$  the : $CH_2$  carbenes may be a reaction intermediate for the reaction of hydrocarbon formation from  $CF_2Cl_2$  and  $CH_2X_2$ .  $^{12}$ 

Thus, it was our objective to probe by spectroscopy and kinetics the surface species that are formed from C<sub>1</sub> halocarbon conversion reactions catalyzed by supported noble metals. The spectroscopic investigations were linked to kinetics investigations through the use of the same catalyst,  $Pd/\gamma$ -Al<sub>2</sub>O<sub>3</sub>, and the catalyst pretreatment conditions. The bromofluorocarbon molecule (CF<sub>2</sub>Br<sub>2</sub>) was used instead of CF<sub>2</sub>Cl<sub>2</sub>, as the C-Br bonds are weaker than the C-Cl bonds and would facilitate the formation of the :CF<sub>2</sub> carbenes during adsorption. When interpreting the results from this investigation, it was assumed that the mechanisms of CF<sub>2</sub>Br<sub>2</sub> debromination and CF<sub>2</sub>Cl<sub>2</sub> dechlorination catalyzed by Pd are the same and the effect of the coadsorbed surface halide on the bonding and reactions of the surface species is small.<sup>21</sup> Another aspect of the research centered on the dissociation of CH<sub>2</sub>Br<sub>2</sub> and CD<sub>2</sub>Br<sub>2</sub> on the surface of alumina-supported Pd to form adsorbed :CH2 and :CD<sub>2</sub> carbene species, and the reactivity of these species toward coadsorbed H atoms was also investigated.

## **Experimental Section**

A 5% Pd/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> catalyst was prepared by impregnation of powered  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> (Vista-B, 300 m²/g, average pore diameter, 55 Å) with an aqueous solution of Pd(NH<sub>4</sub>)Cl<sub>2</sub>·H<sub>2</sub>O (Alfa, 99.9% purity). The material was dried in air at ambient temperature for 10 h and then at 373 K for 20 h. The catalyst sample was treated with flowing O<sub>2</sub> (60 mL min<sup>-1</sup>) while heated from ambient temperature to 773 K at the rate of 4 K min<sup>-1</sup> and held at 773 K for 1 h. Then, it was cooled to ambient temperature in flowing O<sub>2</sub> and purged with He (60 mL min<sup>-1</sup>) for 15 min. The He flow was switched to H<sub>2</sub> (90 mL min<sup>-1</sup>).

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The catalyst was heated to 573 K at the rate of 4 K min $^{-1}$ , held at 573 K for 1 h followed by purging with He (60 mL min $^{-1}$ ) at the same temperature for 15 min, and cooled to room temperature. Subsequently, the fraction of Pd atoms exposed was determined by  $O_2$ – $H_2$  titration. $^{22}$  Approximately 44% of the Pd atoms were exposed, which corresponds to an average particle size of 2.0 nm. $^{23}$ 

The infrared spectra were recorded with a Research Series II FTIR spectrometer (Mattson, Inc) equipped with a liquid  $N_2$  cooled MCT detector. The IR cell was similar to that described elsewhere.<sup>24</sup> The cell volume was 200 cm³ and the light path length was 15 cm. The cell was equipped with glass stopcocks connected to gas inlet/outlet ports. The spectra of adsorbed  $CF_2Br_2$ ,  $CH_2Br_2$ ,  $CD_2Br_2$ , and CO were measured with a resolution of 4 cm $^{-1}$  and 400 scans were accumulated per spectrum. The spectra of gaseous products of the  $CF_2Br_2$ ,  $CH_2Br_2$ , and  $CD_2Br_2$  reaction with  $H_2$  were measured with a resolution of 2 cm $^{-1}$  and 128 scans were accumulated per spectrum.

The self-supporting catalyst wafers (10–30 mg/cm² thick) were prepared from the powdered catalyst by pressing at 830 atm for 3 min. After a wafer was placed in the in situ IR cell, it was pretreated by heating from room temperature to 773 K at 4 K min<sup>-1</sup> in a 10% O<sub>2</sub>/He mixture (UHP, Liquid Carbonic) flowing at 60 mL min<sup>-1</sup>. It was held at 773 K for 1 h before cooling to room temperature in the flowing 10% O<sub>2</sub>/He mixture. The cell was evacuated for 0.5 h to a pressure of 10<sup>-5</sup> Torr to remove all traces of O<sub>2</sub>. Then, the sample was heated in flowing H<sub>2</sub> (UHP, Penn Oxygen) (80 mL min<sup>-1</sup>) or D<sub>2</sub> (Cambrige Isotope Laboratories, 99.6%) (80 mL min<sup>-1</sup>) to 573 K at 5 K min<sup>-1</sup> and held at this temperature for 1 h before evacuating at 573 K to a pressure of 10<sup>-5</sup> Torr.

The adsorption of the probe molecules was performed after the H<sub>2</sub> treatment. From 5 to 10 Torr of CF<sub>2</sub>Br<sub>2</sub> (Aldrich, 97%), CH<sub>2</sub>Br<sub>2</sub> (Aldrich, 99%), CD<sub>2</sub>Br<sub>2</sub> (Aldrich, 99.6 at. % D), or CO (Air Product, 99.995%) was admitted to the evacuated cell at room temperature for 0.5-3 h, during which spectra were collected, before evacuation for 20 min. The hydrogenation kinetics of the surface species that formed during exposure of the catalyst wafer to CF<sub>2</sub>Br<sub>2</sub>, CH<sub>2</sub>Br<sub>2</sub>, or CD<sub>2</sub>Br<sub>2</sub> were measured using a reduced fresh<sup>25</sup> catalyst wafer. The wafer was exposed to 10 Torr of the corresponding halocarbon at 473 K for 1 h. Then, the wafer was rereduced at 573 K for 1 h, cooled to room temperature, and exposed to 5 Torr of the halocarbon for 0.5 h before evacuation for 20 min. Then, 10 Torr H<sub>2</sub> was admitted to the cell at room temperature, and the vibrational spectra of the gas-phase products were monitored by FTIR as a function of time.

The kinetics of the CF<sub>2</sub>Br<sub>2</sub>+H<sub>2</sub>, CH<sub>2</sub>Br<sub>2</sub>+H<sub>2</sub>, and CD<sub>2</sub>Br<sub>2</sub>+H<sub>2</sub> reactions were investigated using the wafers that had previously been used in the experiments to hydrogenate surface species from halocarbon adsorption at room temperature. After the hydrogenation experiment, the catalyst wafer was rereduced at 573 K for 1 h and evacuated at the reduction temperature to a pressure of  $10^{-5}$  Torr. Then, the wafer was cooled to the reaction temperature of 473 K, and 8 Torr of halocarbon and 40 Torr of H<sub>2</sub> were admitted into the cell. The concentrations of gaseous products from the reaction of CF<sub>2</sub>Br<sub>2</sub>, CH<sub>2</sub>Br<sub>2</sub>, and CD<sub>2</sub>Br<sub>2</sub> with H<sub>2</sub> were measured in terms of intensities of the signature vibrations for the gaseous compounds:<sup>26–28</sup> 1140 cm<sup>-1</sup> (CF<sub>2</sub>Br<sub>2</sub>),  $1208 \text{ cm}^{-1} \text{ (CF}_3\text{Br)}, 1090 \text{ cm}^{-1} \text{ (CF}_2\text{H}_2), 1152 \text{ cm}^{-1} \text{ (CF}_3\text{H)},$  $1190 \text{ cm}^{-1} \text{ (CH}_2\text{Br}_2), 1234 \text{ cm}^{-1} \text{ (CD}_2\text{H}_2), 2259 \text{ cm}^{-1} \text{ (CD}_4),$  $3017 \text{ cm}^{-1} \text{ (CH}_4), 2970 \text{ cm}^{-1} \text{ (C}_x \text{H}_{2x+2}). \text{ A band at } 1030 \text{ cm}^{-1},$ which is characteristic of SiF<sub>4</sub>,<sup>28</sup> was detected in the experiments

with  $CF_2Br_2$ . The  $SiF_4$  forms from the interaction of HF(DF), a product of the  $CF_2Br_2+H_2(D_2)$  reaction, with quartz walls of the IR cell.

The differential flow kinetics of the CF<sub>2</sub>Br<sub>2</sub>+H<sub>2</sub> reaction was conducted at atmospheric pressure in a stainless steel flow reaction system consisting of a down-flow quartz microreactor (10 mm i.d.) equipped with a quartz frit to support the catalyst. An electric furnace heated the reactor zone containing the catalyst. The catalyst bed temperature was measured and controlled with an accuracy of  $\pm 1$  K (Omega model CN2011). The gaseous reactants and pretreatment gases (He, H<sub>2</sub>, Praxair, 99.999%) were metered using mass flow controllers (Brooks, model 5850E) and mixed prior to entering the reactor. The CF<sub>2</sub>Br<sub>2</sub> was metered into the system by flowing He through a saturator containing the liquid. A constant concentration in the stream was ensured by holding the saturator at a fixed temperature of 273 K using a recirculating cooling system. The reaction temperature was 473  $\pm$  1 K, and the catalyst was maintained at that temperature using an electric furnace and a temperature controller (Omega model CN2011).

Prior to reaction, the catalyst was treated with a mixture of  $H_2$  (20 mL min<sup>-1</sup>) and He (30 mL min<sup>-1</sup>) as it was heated from room temperature to 573 K at the rate of 5 K min<sup>-1</sup> and then held at 573 K for 2 h. The catalyst was cooled in flowing He (30 mL min<sup>-1</sup>) to the reaction temperature, and the reactant mixture was introduced. The total flow rate of the reaction mixture was 56 mL min<sup>-1</sup> and consisted of 41 300 ppm CF<sub>2</sub>Br<sub>2</sub>, 206 400 ppm  $H_2$ , and the balance He. The catalyst weight was  $\sim 0.03$  g. The selectivities ( $S_i$ ) toward detectable carbon-containing products were calculated as follows:

$$S_i = \frac{n_i C_i}{\sum_i n_i C_i} \tag{1}$$

where  $n_i$  and  $C_i$  are the number of carbon atoms in a molecule and the mole concentration of the product i in the effluent gas, respectively. The formation of HF and HBr was detected by GC-MS but not quantified.

#### Results

The prolonged contact of the reduced fresh 5%  $Pd/\gamma$ - $Al_2O_3$  catalyst with  $CF_2Br_2$  or  $CH_2Br_2$  resulted in the formation of small quantities of gaseous  $CF_3Br$  and  $CH_4$ , respectively (not shown). When the catalyst was exposed to  $CH_2Br_2$ ,  $CH_4$  evolved independent of whether  $H_2$  or  $D_2$  was used for the catalyst reduction (not shown). The FTIR spectra measured at room temperature did not contain any bands associated with C-F or C-H bond vibrations of chemisorbed species formed on the catalyst surface after contact with either  $CF_2Br_2$  or  $CH_2Br_2$  at room temperature.

When the reduced fresh catalyst was exposed to 10 Torr of CF<sub>2</sub>Br<sub>2</sub> for 1.5 h and then evacuated at room temperature, the IR bands at 1230, 1460, 1650, 1865, 2105, and 2155 cm<sup>-1</sup> appeared (Figure 1a). The bands at 1230 and 1650 cm<sup>-1</sup> correspond to the asymmetric C–O bond stretching vibration and the C=O bond vibration of a bidentate carbonate I (Figure 2), respectively. The band at 1460 cm<sup>-1</sup> has been attributed to asymmetric C–O bond stretching vibration of carbonate ion CO<sub>3</sub><sup>2-</sup> (Structure III in Figure 2). The symmetric C–O bond vibration of the carbonate ion is IR inactive.<sup>29</sup> The 1865, 2105, and 2155 cm<sup>-1</sup> bands are ascribed to CO molecules adsorbed on palladium. The bands at 1860 and 2105 cm<sup>-1</sup> correspond to

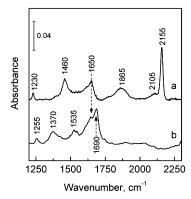


Figure 1. FTIR spectra of the reduced 5%  $Pd/\gamma$ - $Al_2O_3$  wafer after the exposure to 10 Torr of CF<sub>2</sub>Br<sub>2</sub> (a) or CH<sub>2</sub>Br<sub>2</sub> (b) for 1.5 h at room temperature followed by evacuation for 1 h.

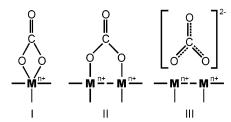


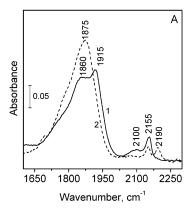
Figure 2. The structures of surface bidentate carbonates.

CO adsorbed on metallic Pd in bridging and linear forms, respectively, while the 2155 cm<sup>-1</sup> band is characteristic of complexes of CO with Pd<sup>2+</sup> cations.<sup>30</sup>

Several FTIR bands appeared in the 1200-2300 cm<sup>-1</sup> range when the reduced fresh catalyst was exposed to CH<sub>2</sub>Br<sub>2</sub> (Figure 1b). The bands at 1255 and 1690 cm<sup>-1</sup> correspond to the asymmetric C-O bond stretching vibration and the C=O bond vibration in the carbonate I (Figure 2).31,32 The two bands at 1370 and 1535 cm<sup>-1</sup> are attributed to vibrations of the carbonate II (Figure 2).31,32 The bands characteristic of CO adsorbed on Pd are absent in the spectrum of the catalyst exposed to CH<sub>2</sub>Br<sub>2</sub>.

Several adsorption complexes of adsorbed CO formed with the catalyst that had been rereduced after preexposure to CH<sub>2</sub>Br<sub>2</sub> and CF<sub>2</sub>Br<sub>2</sub> and then exposed to CO. The spectra for both samples contained the bands at 1860, 1915, and 2155 cm<sup>-1</sup> (Figure 3, Spectra 1). The 1860 and 1915 cm<sup>-1</sup> bands have been assigned to CO molecules adsorbed on metallic Pd in tripleand double-coordinated modes.<sup>33</sup> The band at 2155 cm<sup>-1</sup> corresponds to a complex of CO with Pd<sup>2+</sup> cations.<sup>30</sup> There is, however, a little difference between Spectrum 1 shown in Figure 3A and 3B. The bands of multi-coordinated modes of CO adsorbed on Pd are less intense and more clearly resolved for the catalyst preexposed to CH<sub>2</sub>Br<sub>2</sub> (Figure 3A). The better resolution of the triple- and double-coordinated CO bands for this sample seems to be a result of a larger fraction of doublecoordinated complexes (band at 1915 cm<sup>-1</sup>) than for the sample preexposed to CF<sub>2</sub>Br<sub>2</sub> (Figure 3B).

When CF<sub>2</sub>Br<sub>2</sub> or CH<sub>2</sub>Br<sub>2</sub> was adsorbed on the catalysts with preadsorbed CO, the band at 1915 cm<sup>-1</sup> either disappeared or red-shifted, leaving only a single symmetric band with a maximum at 1875 cm<sup>-1</sup> in the region of CO adsorbed on metallic Pd (Figure 3, spectra 2A and 2B). The integral intensity of the spectrum of CO adsorbed on metallic Pd in multicoordinated modes noticeably decreased after the CF2Br2 adsorption (Figure 3B). However, it increased after CH<sub>2</sub>Br<sub>2</sub> adsorption (Figure 3A). The adsorption of halocarbons on the sample with preadsorbed CO also resulted in the disappearance of the IR band for the CO adsorbed on Pd<sup>0</sup> in the linear mode



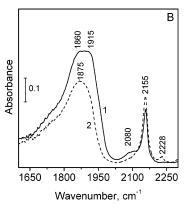


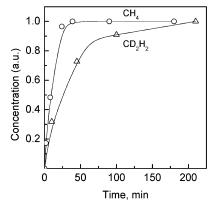
Figure 3. FTIR spectra of CO adsorbed on a reduced 5% Pd/γ-Al<sub>2</sub>O<sub>3</sub> sample preexposed to 10 Torr of CH<sub>2</sub>Br<sub>2</sub> (A) and CF<sub>2</sub>Br<sub>2</sub> (B) at ambient temperature for 3 h followed by repeated reduction with 100 Torr H<sub>2</sub> under static conditions; 1, spectra of CO resulting from the exposure of the catalyst wafer to 10 Torr CO for 20 min at room temperature followed by evacuation for 0.5 h; 2, spectra 1 after exposure of the catalyst wafer to 5 Torr of  $CF_2Br_2$  (A) or  $CH_2Br_2$  (B) and subsequent equilibration between surface and gas phase.

 $(2080-2100 \text{ cm}^{-1})$  and the appearance of bands at 2190 cm<sup>-1</sup> (Figure 3A) and 2228 cm<sup>-1</sup> (Figure 3B) which are characteristic of CO adsorbed on coordinatively unsaturated Al3+ cations in octahedral and tetrahedral coordinations, respectively. 34,35

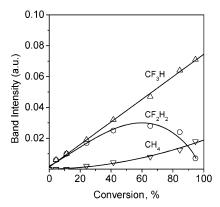
After heating the catalyst in CF<sub>2</sub>Br<sub>2</sub> or CH<sub>2</sub>Br<sub>2</sub> at 473 K and then reducing in H<sub>2</sub> at 573 K, the reactivity of the catalyst surface decreased. This is evident by the lack of IR bands in the region of carbonate species vibrations (1200-1700 cm<sup>-1</sup>) after subsequent adsorption of CF<sub>2</sub>Br<sub>2</sub> or CH<sub>2</sub>Br<sub>2</sub> at ambient temperature. The bands characteristic of gas-phase CF<sub>3</sub>Br and CH<sub>4</sub> formed from adsorption of CF<sub>2</sub>Br<sub>2</sub> or CH<sub>2</sub>Br<sub>2</sub> were also absent. However, when the same catalyst wafer was exposed to H<sub>2</sub> (10 Torr) at room temperature after prolonged evacuation at room temperature, methane evolved into gas phase. Substituting D<sub>2</sub> for H<sub>2</sub> resulted in the formation of CD<sub>4</sub> and CH<sub>2</sub>D<sub>2</sub>. Gas-phase CH<sub>2</sub>D<sub>2</sub> also formed when CD<sub>2</sub>Br<sub>2</sub>, instead of CH<sub>2</sub>Br<sub>2</sub>, was adsorbed and then the catalyst was exposed to H2 at room temperature.

The kinetics of CH<sub>4</sub> and CH<sub>2</sub>D<sub>2</sub> formation in the IR cell during the reaction of H2 with a catalyst wafer that was preexposed to CF<sub>2</sub>Br<sub>2</sub> or CD<sub>2</sub>Br<sub>2</sub> are shown in Figure 4. The rate of CH<sub>4</sub> formation from the catalyst preexposed to CF<sub>2</sub>Br<sub>2</sub> was much larger than that of CH<sub>2</sub>D<sub>2</sub> formation after preexposing to CD<sub>2</sub>Br<sub>2</sub>. However, the maximum concentration of CH<sub>2</sub>D<sub>2</sub> was about an order of magnitude higher than that of CH<sub>4</sub> (not shown).

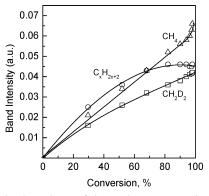
In the presence of hydrogen, CF<sub>2</sub>Br<sub>2</sub> was converted at 473 K over a rereduced Pd/γ-Al<sub>2</sub>O<sub>3</sub> catalyst into CF<sub>3</sub>H, CF<sub>2</sub>H<sub>2</sub>, CH<sub>4</sub>, HBr, and HF,36 which were identified using IR spectra reported



**Figure 4.** Kinetics of the  $CH_4$  and  $CD_2H_2$  formation at room temperature, respectively, from chemisorbed  $CF_2Br_2$  and  $CD_2Br_2$ . The  $H_2$  pressure in the IR cell was 10 Torr.



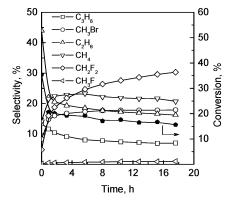
**Figure 5.** The dependence of the product concentration on  $CF_2Br_2$  conversion in the presence of hydrogen at 473 K. The initial concentrations of  $CF_2Br_2$  and  $H_2$  were 8 and 40 Torr, respectively.



**Figure 6.** The dependence of the product concentration on  $CD_2Br_2$  conversion in the presence of hydrogen at 473 K. The initial concentrations of  $CD_2Br_2$  and  $H_2$  were 8 and 40 Torr, respectively.

in the literature. $^{26-28}$  Figure 5 shows the relation between  $CF_2Br_2$  conversion and the band intensities characteristic of  $CF_3H$  (1152 cm $^{-1}$ ),  $CF_2H_2$  (1090 cm $^{-1}$ ), and  $CH_4$  (3017 cm $^{-1}$ ). In the conversion range of 0–95%, there was a linear increase in  $CF_3H$  concentration with increasing  $CF_2Br_2$  conversion. The concentration of  $CF_2H_2$  reached a maximum value when the  $CF_2Br_2$  conversion was 60%. At higher conversions, the  $CF_2H_2$  concentration decreased and the concentration of  $CH_4$  and  $CH_4$  and  $CH_4$  increased (not shown).

The reaction of  $CD_2Br_2$  and  $H_2$  at 473 K yielded  $CD_2H_2$ ,  $CH_4$ , heavier hydrocarbons, and HBr (Figure 6). When the  $CD_2Br_2$  conversion was less than 90%, there was almost a linear relationship between the  $CD_2Br_2$  conversion and the band intensities of  $CD_2H_2$  and  $CH_4$ . The concentration of  $C_{2+}$ 



**Figure 7.** Time on stream performance of the  $Pd/\gamma$ - $Al_2O_3$  in the  $CF_2Br_2+H_2$  reaction at 473 K in a continuous flow reactor at 473 K.

hydrocarbons increased until the  $CD_2Br_2$  conversion reached 80% and remained essentially constant thereafter.

The selectivity of the  $CF_2Br_2+H_2$  reaction catalyzed by the  $Pd/\gamma$ - $Al_2O_3$  varied with time on stream (TOS), as measured in a continuous flow reactor. Initially, the catalyst was selective toward  $C_2$ - $C_3$  hydrocarbons ( $\sim$ 60%) and was unselective toward  $CF_2H_2$  ( $\sim$ 5%) (Figure 7). With increasing TOS, the selectivity toward  $C_2H_6$  and  $C_3H_8$  decreased, whereas the selectivity toward  $CF_2H_2$  and  $CH_4$  increased. After approximately 3 h on stream,  $CF_2H_2$  and  $CH_4$  were the major products. The selectivity toward  $CH_3$ Br was relatively high ( $\sim$ 18%), and there was no  $CF_3H$  formed during the  $CF_2Br_2+H_2$  reaction.

### **Discussion**

Adsorption Studies: Interaction of CF<sub>2</sub>Br<sub>2</sub> and CH<sub>2</sub>Br<sub>2</sub> (CD<sub>2</sub>Br<sub>2</sub>) with the Surface of Pd/γ-Al<sub>2</sub>O<sub>3</sub> at Room Temperature. The adsorption of CF<sub>2</sub>Br<sub>2</sub> at room temperature on a reduced fresh catalyst leads to the formation of bidentate carbonates (bands at 1230 and 1650 cm<sup>-1</sup>) and carbonate-ions CO<sub>3</sub><sup>2-</sup> (band at 1460 cm<sup>-1</sup>) on the alumina surface. There is also CO adsorbed on metallic Pd (bands at 1860 and 2105 cm<sup>-1</sup>) and on Pd<sup>2+</sup> cations (band at 2155 cm<sup>-1</sup>) (Figure 1, spectrum a). The formation of the carbonate species and CO is the result of the direct reaction of the halocarbon with the support. The γ-Al<sub>2</sub>O<sub>3</sub> surface is thus halogenated. The fact that this occurs at room temperature is consistent with other investigations with C<sub>1</sub> and C<sub>2</sub> halocarbons. For example, the bands of adsorbed carbonates and those that may belong to CO adsorbed on the coordinatively unsaturated Al3+ cations were detected after exposure of metal-free γ-Al<sub>2</sub>O<sub>3</sub> to CF<sub>2</sub>Cl<sub>2</sub> at temperature as low as 120 K.<sup>37</sup> However, neither CO nor CO<sub>2</sub> forms during the reaction of CF<sub>3</sub>CFCl<sub>2</sub> with metal-free γ-Al<sub>2</sub>O<sub>3</sub> at temperatures below 593 K, but the formation of adsorbed trifluoroacetate species with concomitant halogenation of the alumina surface was observed at temperature as low as 298 K.<sup>24</sup>

After  $CF_2Br_2$  adsorption, no absorption bands characteristic of chemisorbed species containing C-F bonds were detected. As well, the contact of the catalyst with hydrogen after the preadsorbed  $CF_2Br_2$  was removed by prolonged evacuation at room temperature leads to the  $CH_4$  formation. The strength<sup>38</sup> of the C-Br bond is so much less than the C-F bond (68 and 110 kcal mol<sup>-1</sup>, respectively<sup>39</sup>) that one would expect that the  $CF_2Br_2$  molecule would readily dissociate to form : $CF_2$ . The absence of  $CF_2H_2$  in hydrogenation products indicates that the : $CF_2$  carbene is not among chemisorbed species formed from adsorbed  $CF_2Br_2$ . It is possible that the strong interaction of F atoms with the Pd provides a strong driving force for the : $CF_2$  to undergo subsequent decomposition reactions. Thus, most likely the adsorbed  $CF_2Br_2$  decomposes to form carbon on the

Pd surface that is then hydrogenated at room temperature to form CH<sub>4</sub>. The significant decrease in the integral intensity of the band in the range of 1865–1915 cm<sup>-1</sup> may indicate oxidation of metallic Pd because of CF<sub>2</sub>Br<sub>2</sub> decomposition with the formation of coordinatively unsaturated PdF2 surface moieties. Similar chemistry was reported for CCl<sub>2</sub>F<sub>2</sub> on Fe(110).<sup>40</sup>

The evolution of gas-phase CF<sub>3</sub>Br after adsorption of CF<sub>2</sub>Br<sub>2</sub> shows that Br exchanges with F in the CF<sub>2</sub>Br<sub>2</sub> molecule. The source of fluorine is likely partially fluorinated alumina formed during the decomposition of CF<sub>2</sub>Br<sub>2</sub> into carbonates, CO, and carbon. As no oxygen was added to the system, it is clear that oxygen must come from the support to form carbonates and

The carbonates also form on the surface of the reduced fresh catalyst after adsorption of CH<sub>2</sub>Br<sub>2</sub> (Figure 1, spectrum b). However, there is no CO adsorbed on Pd (Figure 1, spectrum b). This reflexes different chemistry of the CF<sub>2</sub>Br<sub>2</sub> and CH<sub>2</sub>Br<sub>2</sub> interaction with the catalyst surface. The CH<sub>4</sub> observed during the adsorption of CH<sub>2</sub>Br<sub>2</sub> forms via the disproportionation of CH<sub>2</sub>. This chemistry occurs on the Pd surface and results in the deposition of carbonaceous species. The possibility that the CH<sub>4</sub> may form from CH<sub>2</sub> species and adsorbed H atoms leftover from the catalyst reduction step was ruled out by the experiment in which the catalyst was reduced with D2. No deuterated methanes formed in that case.

Further insight into the interaction of molecular CH<sub>2</sub>Br<sub>2</sub> with metallic palladium comes from the spectrum of CO adsorbed on Pd in bridging form (Figure 3A). The fact that the adsorption of CH<sub>2</sub>Br<sub>2</sub> on the sample with preadsorbed CO results in the shift of 1915 cm<sup>-1</sup> band to 1875 cm<sup>-1</sup> suggests that the electronic donor-accepting properties of Pd are modified. This modification is not accompanied by a decrease in the integral intensity of the spectrum of CO adsorbed on palladium. It may mean that CH<sub>2</sub>Br<sub>2</sub> does not oxidize the metallic Pd, and the electronic donor-accepting properties of Pd are modified through its interaction with strong Lewis acid sites emerging on the support surface after exposure to CH<sub>2</sub>Br<sub>2</sub>, as indicated by the band at 2190 cm<sup>-1</sup> (Figure 3A).

The CF<sub>2</sub>Br<sub>2</sub> interacts with supported metallic Pd as well. This interaction manifests itself by the change in the FTIR spectrum of CO adsorbed on Pd in bridging form after adsorption of CF<sub>2</sub>Br<sub>2</sub> on the catalyst (Figure 3B). The significant decrease in the integral intensity of the absorption bands in the range of 1865-1915 cm<sup>-1</sup> suggests a partial oxidation of metallic Pd by F atoms originated from the decomposition of CF<sub>2</sub>Br<sub>2</sub>.

When the alumina surface is halogenated to the extent that there are little to no oxygen atoms on the surface, the adsorbed halocarbon molecules will no longer decompose. With such surfaces, only halogen exchange reactions are possible, and the rate of these reactions is significant only at temperatures greater than 573 K.41-45 Hence, it is likely that after adsorption of CF<sub>2</sub>Br<sub>2</sub> on the sample pretreated with CF<sub>2</sub>Br<sub>2</sub> at 473 K followed by reduction with H2, active carbon is deposited on the Pd surface. This active carbon is hydrogenated by H2 or D2 into CH<sub>4</sub> or CD<sub>4</sub>. When CH<sub>2</sub>Br<sub>2</sub> is adsorbed on the sample pretreated with CH<sub>2</sub>Br<sub>2</sub> at 473 K followed by reduction with H<sub>2</sub>, the chemisorbed species are mainly: CH<sub>2</sub> carbenes, which are stable at room temperature. In the presence of H<sub>2</sub> or D<sub>2</sub>, the carbenes are hydrogenated into CH<sub>4</sub> or CD<sub>2</sub>H<sub>2</sub>, respectively. While it is tempting to conclude that the :CH2 carbenes do not dissociate at room temperature on the Pd surface even in the absence of coadsorbed H atoms, caution must be exercised because the energy of the C-H bond in the :CH<sub>2</sub> carbenes is lower that that of the C-F bonds in the :CF<sub>2</sub> carbenes (101 and 125 kcal  $\text{mol}^{-1}$ , respectively<sup>39,46</sup>). It is quite possible, however, that the lower stability of the :CF2 species is the result of the strong driving force for the C-F bond dissociation because of the high energy of F atom adsorption on Pd.<sup>47</sup> The conclusion on different nature of chemisorbed species formed from CF<sub>2</sub>Br<sub>2</sub> or CH<sub>2</sub>Br<sub>2</sub> is also supported by the vastly different rate of their hydrogenation (Figure 4) and by the evolution of CD<sub>2</sub>H<sub>2</sub> during hydrogenation by H<sub>2</sub> of chemisorbed species originated from the adsorbed CD<sub>2</sub>Br<sub>2</sub>.

For the silica-supported Pd, the :CH<sub>2</sub> carbenes formed by dissociative adsorption of CH<sub>2</sub>Cl<sub>2</sub> are stable only in a narrow temperature range (233–243 K).<sup>48</sup> At temperatures higher than 250 K, the carbenes on Pd/SiO<sub>2</sub> decomposed and CH<sub>4</sub>, C<sub>2</sub>H<sub>4</sub>, HCl, and H<sub>2</sub>O form. With Pd/γ-Al<sub>2</sub>O<sub>3</sub>, the :CH<sub>2</sub> species are stable even at room temperature and consumed only upon exposure to H<sub>2</sub> to form CH<sub>4</sub>. Such difference in the stability of the :CH<sub>2</sub> carbenes on the surface of Pd supported on SiO<sub>2</sub> and Al<sub>2</sub>O<sub>3</sub> may be caused by different interactions of small Pd particles with different oxide supports.

The reactivity of the surface carbon species formed from CF<sub>2</sub>Br<sub>2</sub> and carbene species formed from CD<sub>2</sub>H<sub>2</sub> with respect to H<sub>2</sub> is quite different (Figure 4). Gas-phase studies have shown that carbon atoms are not less reactive toward H2 than :CH2 carbenes.<sup>49</sup> By clustering the carbon atoms on the metal surface, the degree of coordinative unsaturation of the atoms is decreased and there is a concomitant loss in reactivity. However, it is reasonable to suggest that a small fraction of the C atoms, likely those located at the corners of the clusters, are still highly coordinatively unsaturated and, hence, highly reactive toward hydrogen. The fact that the amount of CH<sub>4</sub> formed by hydrogenation of the surface species formed from the CF<sub>2</sub>Br<sub>2</sub> adsorption is 1 order of magnitude less than the amount of CD<sub>2</sub>H<sub>2</sub> formed by hydrogenation of the surface species formed from the CD<sub>2</sub>Br<sub>2</sub> adsorption suggests that only a small fraction of the C atoms formed from CF<sub>2</sub>Br<sub>2</sub> are sufficiently reactive to be hydrogenated at room temperature.

Reaction Studies: Conversion of CF<sub>2</sub>Br<sub>2</sub> over Pd/γ-Al<sub>2</sub>O<sub>3</sub> in the Presence of H<sub>2</sub> at 473 K. On the basis of the results of the chemical kinetics experiments, it is reasonable to suggest that two different reaction pathways account for the formation of CF<sub>2</sub>H<sub>2</sub> and CF<sub>3</sub>H from CF<sub>2</sub>Br<sub>2</sub> reaction with H<sub>2</sub> at 473 K (Figure 5). At low conversions, the concentration of both CF<sub>2</sub>H<sub>2</sub> and CF<sub>3</sub>H increases linearly with increasing CF<sub>2</sub>Br<sub>2</sub> conversion and the ratio of the CF<sub>2</sub>H<sub>2</sub> and CF<sub>3</sub>H concentrations in the limit of zero conversion is a finite quantity. This indicates that both CF<sub>2</sub>H<sub>2</sub> and CF<sub>3</sub>H are primary reaction products.

The CF<sub>2</sub>H<sub>2</sub> is likely formed from :CF<sub>2</sub> carbene species. The absence of CH<sub>4</sub> among the reaction products at low CF<sub>2</sub>Br<sub>2</sub> conversions suggests that the rate of the surface reaction of :CF<sub>2</sub> carbene hydrogenation to form CF<sub>2</sub>H<sub>2</sub> significantly exceeds that of :CF<sub>2</sub> species dissociation to form surface carbon and eventually CH<sub>4</sub>. The fact that the concentration of CF<sub>2</sub>H<sub>2</sub> increases with increasing CF<sub>2</sub>Br<sub>2</sub> conversion only up to 60% and decreases thereafter is consistent with the idea that CH<sub>4</sub> is a secondary product of the CF<sub>2</sub>Br<sub>2</sub> conversion. The hypothesis that CF<sub>2</sub>H<sub>2</sub> converts into CH<sub>4</sub> at higher conversion was tested in additional experiments on CF<sub>2</sub>H<sub>2</sub> conversion in the presence of H<sub>2</sub> at 473 K. Under these conditions, CF<sub>2</sub>H<sub>2</sub> selectively converts into CH<sub>4</sub>, and HF is detected as SiF<sub>4</sub> because of HF reaction with the quartz walls of the IR cell. In a previous kinetics investigation of the CF<sub>2</sub>Cl<sub>2</sub>+H<sub>2</sub> reaction, it was also concluded that CH<sub>4</sub> is a secondary product of CF<sub>2</sub>Cl<sub>2</sub> hydrodechlorination.<sup>12</sup>

The concentration of CF<sub>3</sub>H increases proportionally with  $CF_2Br_2$  conversion from 0 to  $\sim 100\%$ . This indicates that  $CF_3H$ 

does not participate in secondary reactions. The high selectivity toward CF<sub>3</sub>H that results from the CF<sub>2</sub>Br<sub>2</sub> hydrodehalogenation reaction catalyzed by Pd/γ-Al<sub>2</sub>O<sub>3</sub> under static conditions (Figure 5) is difficult to understand. The CF<sub>3</sub>H was not among the reaction products when the CF<sub>2</sub>Br<sub>2</sub>+H<sub>2</sub> reaction was conducted in a continuous flow reactor (Figure 7). In fact, the CF<sub>3</sub>H may be a secondary product of the CF<sub>2</sub>Br<sub>2</sub> halogen disproportionation reaction catalyzed by the Lewis sites<sup>24,37,50-52</sup> located at the Pdalumina interface. The high Lewis acidity of the CF<sub>2</sub>Br<sub>2</sub> pretreated alumina is indicated by the IR band at 2228 cm<sup>-1</sup> of adsorbed CO (Figure 3B). It is possible that the CF<sub>3</sub>Br forms by disproportionation of CF<sub>2</sub>Br<sub>2</sub> on the Lewis acid site and then diffuses onto the metal sites where the hydrodebromination takes place and CF<sub>3</sub>H is formed. As the reactivity of the C<sub>1</sub> fluorohalocarbons increases with a decrease in the number of F atoms in the molecule, 12,53 the other disproportionation reaction product (CFBr<sub>3</sub>) should rapidly convert into surface or bulk carbonates on alumina or into CH<sub>4</sub> on the Pd. The absence of CF<sub>3</sub>H among the CF<sub>2</sub>Br<sub>2</sub>+H<sub>2</sub> reaction products in the continuous flow reactor (Figure 7) indicates that the alumina support does not have strong acid sites under the continuous flow reaction conditions. These sites may be blocked by the C<sub>2+</sub> hydrocarbon products of the CF<sub>2</sub>Br<sub>2</sub>+H<sub>2</sub> reaction. A strong inverse correlation between C2+ hydrocarbon and CF3H selectivities for the CF<sub>2</sub>Cl<sub>2</sub>+H<sub>2</sub> reaction catalyzed by supported Pt bimetallic catalysts was reported earlier.<sup>54</sup>

Reaction Studies: Conversion of CH<sub>2</sub>Br<sub>2</sub> and CD<sub>2</sub>Br<sub>2</sub> over Pd/γ-Al<sub>2</sub>O<sub>3</sub> in the Presence of H<sub>2</sub> at 473 K. In the presence of H<sub>2</sub> at 473 K, the CH<sub>2</sub>Br<sub>2</sub> reacts to form CH<sub>4</sub> and heavier hydrocarbons, most likely of the form of  $C_xH_{2x+2}$ . When  $CD_2Br_2$ reacts with H<sub>2</sub> under the same conditions, large amounts of CH<sub>4</sub> and  $C_{2+}$  hydrocarbons form in addition to  $CD_2H_2$  (Figure 6). These results are consistent with the idea that :CD<sub>2</sub> carbenes participate in the conversion of CD<sub>2</sub>Br<sub>2</sub>. The formation of CH<sub>4</sub> and higher hydrocarbons indicate that :CD<sub>2</sub> carbenes, which form from the dissociative adsorption of CD<sub>2</sub>Br<sub>2</sub> at 473 K, undergo H-D exchange followed by either hydrogenation to form CH<sub>4</sub> or oligomerization into C<sub>2+</sub> hydrocarbons analogous to Fischer-Tropsch synthesis chemistry catalyzed by ruthenium<sup>55</sup> and iron.<sup>56</sup>

## Conclusion

The reaction of CF<sub>2</sub>Br<sub>2</sub>, CH<sub>2</sub>Br<sub>2</sub>, and CD<sub>2</sub>Br<sub>2</sub> hydrodehalogenation catalyzed by a Pd/γ-Al<sub>2</sub>O<sub>3</sub> catalyst was investigated by a combination of FTIR and reaction kinetics studies. In a continuous flow reactor, CF<sub>2</sub>H<sub>2</sub>, CH<sub>4</sub>, and C<sub>2</sub>–C<sub>3</sub> hydrocarbons form from the reaction of CF<sub>2</sub>Br<sub>2</sub>+H<sub>2</sub> at 473 K, whereas CF<sub>3</sub>H forms in addition to CF<sub>2</sub>H<sub>2</sub> and hydrocarbons in the IR cell under static conditions. The difference in product composition was explained in terms of a different impact of the support to the CF<sub>2</sub>Br<sub>2</sub> conversion depending on the reaction conditions.

The adsorption of CF<sub>2</sub>Br<sub>2</sub> on the catalyst surface at room temperature results in the complete decomposition of the halocarbon molecules on Pd to form C and halogen atoms thereon. These moieties hydrogenate to CH<sub>4</sub>, HF, and HBr under exposure of the catalyst to H<sub>2</sub> at room temperature. The adsorption of CH<sub>2</sub>Br<sub>2</sub> and CD<sub>2</sub>Br<sub>2</sub> on a Pd/γ-Al<sub>2</sub>O<sub>3</sub> results in the dissociation of both C-Br bonds of the halocarbons on Pd to form surface Br and :CH<sub>2</sub> or :CD<sub>2</sub> species, identified by the products of their reaction with H<sub>2</sub> (HBr, CH<sub>4</sub>, or CD<sub>2</sub>H<sub>2</sub>) at room temperature.

It was concluded that unlike the :CH<sub>2</sub> carbenes, the :CF<sub>2</sub> species are unstable at room temperature on the Pd surface and tend to decompose in the absence of coadsorbed H atoms. Thus, the selectivity of the Pd toward CF<sub>2</sub>H<sub>2</sub> in the CF<sub>2</sub>Br<sub>2</sub>+H<sub>2</sub> reaction is determined by the relative rates of two parallel pathways for the intermediate :CF<sub>2</sub> species: dissociation to form surface carbon that is hydrogenated to CH<sub>4</sub> and reaction with coadsorbed H to form CF<sub>2</sub>H<sub>2</sub>.

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