

Alkine Sour Water Corrosion Calculation for Asset ID ssss

Asset Name/ID

SSSS

H2S concentration in system

It is suggested to determine NH4HS value with ionic process models. However, approximate values may be calculated from API 581 Table 2.B.7.1

1.50 wt%

NH3 concentration in system

It is suggested to determine $\,$ NH4HS $\,$ value with ionic process models. However, approximate values may be calculated from API 581 Table 2.B.7.1

4.00 wt%

NH3 concentration in system

Determine the concentration of the H2SO4 present in this equipment/piping. If analytical results are not readily available, it should be estimated by a knowledgeable process engineer 2.25 wt%

Stream Velocity

The vapor phase velocity should be used in a two-phase system. The liquid phase velocity should be used in a liquid full system.

5.00 m/s

%mol H2S in the system

1.50 %

System pressure

Fill the Total system pressure psia 120.00 psia

H2S partial pressure

Fill the Total system pressure KPa 30.00 psia

Baseline CR mm/yr

0.12 mm/yr

Baseline CR mpy

4.59 mpy

Adjusted CR mm/yr

0.92 mm/yr



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Adjusted CR mpy

36.17 mpy

Corrosion Damage Morphology

General thinnig

Remaining Life and Next Inspection Date Calculation

Corrosion Rate (overwritten)

Corrosion Rate Overwritten by the user Yes

Material Thickness Units

Units of the thickness in

T Actual

Current thickness of the material 0.9

T Required

 $\begin{array}{l} \mbox{Minimum required thickness for safe operation} \\ \mbox{0.85} \end{array}$

Selected Date

Start date of the remaining life Tue Apr 01 2025

Remaining Life years/Retirement date

1.38 / Wed Aug 19 2026

Do you want to estimate the next inspection date?

Next inspection date Yes

Recommended next inspection date based on t actual date

Recommended next thickness measurement date (one-half remaining life or maximum interval per piping type of circuit class, whichever is less)

Thu Apr 01 2027



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Piping Asset Class Piping Asset Class Class 1