

## Alkine Sour Water Corrosion Calculation for Asset ID k

## Asset Name/ID

k

#### **H2S** concentration in system

It is suggested to determine NH4HS value with ionic process models. However, approximate values may be calculated from API 581 Table 2.B.7.1

1.40 wt%

#### NH3 concentration in system

It is suggested to determine  $\,$  NH4HS  $\,$  value with ionic process models. However, approximate values may be calculated from API 581 Table 2.B.7.1

4.00 wt%

#### NH3 concentration in system

Determine the concentration of the H2SO4 present in this equipment/piping. If analytical results are not readily available, it should be estimated by a knowledgeable process engineer  $2.10~\rm wt\%$ 

## **Stream Velocity**

The vapor phase velocity should be used in a two-phase system. The liquid phase velocity should be used in a liquid full system.

5.00 m/s

## %mol H2S in the system

1.40 %

## System pressure

Fill the Total system pressure psia 120.00 psia

#### **H2S** partial pressure

Fill the Total system pressure KPa 26.00 psia

## Baseline CR mm/yr

0.11 mm/yr

#### Baseline CR mpy

4.33 mpy

## Adjusted CR mm/yr

0.17 mm/yr



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# Adjusted CR mpy 6.82 mpy

## **Corrosion Damage Morphology** General thinnig

## Remaining Life and Next Inspection Date Calculation

## **Corrosion Rate (overwritten)**

Corrosion Rate Overwritten by the user No

## **Material Thickness Units**

Units of the thickness in

## **T** Actual

Current thickness of the material 0.9

## T Required

 $\begin{array}{l} \mbox{Minimum required thickness for safe operation} \\ \mbox{0.85} \end{array}$ 

#### **Selected Date**

Start date of the remaining life Tue Apr 01 2025

## Remaining Life years/Retirement date

7.33 / Sat Jul 31 2032