



# Electrocatalysis

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# Selective and Efficient Reduction of Carbon Dioxide to Carbon Monoxide on Oxide-Derived Nanostructured Silver Electrocatalysts

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Abstract: In this work, the selective electrocatalytic reduction of carbon dioxide to carbon monoxide on oxide-derived silver electrocatalysts is presented. By a simple synthesis technique, the overall high faradaic efficiency for CO production on the oxide-derived Ag was shifted by more than 400 mV towards a lower overpotential compared to that of untreated Ag. Notably, the Ag resulting from Ag oxide is capable of electrochemically reducing CO2 to CO with approximately 80% catalytic selectivity at a moderate overpotential of 0.49 V, which is much higher than that (ca. 4%) of untreated Ag under identical conditions. Electrokinetic studies show that the improved catalytic activity is ascribed to the enhanced stabilization of COOH intermediate. Furthermore, highly nanostructured Ag is likely able to create a high local pH near the catalyst surface, which may also facilitate the catalytic activity for the reduction of  $CO_2$  with suppressed  $H_2$  evolution.

he electrochemical conversion of CO<sub>2</sub> into carbon-based fuels is an attractive strategy for utilizing CO2 captured at large emission sources.<sup>[1-5]</sup> In order to close the anthropogenic carbon cycle, the electrocatalytic reduction of CO2 to fuels should be powered by a renewable electricity source. [6] For achieving this goal, the essential step is to develop a cheap, stable, and efficient catalyst with high selectivity for a desired product. Over the past few decades, several catalyst materials with the capability of reducing CO2 electrochemically in CO2 saturated-aqueous solutions have been identified. [3,7-18] It has been demonstrated that polycrystalline Au is capable of reducing CO<sub>2</sub> to CO with a high faradaic efficiency (FE) of about 87% at -0.74 vs. reversible hydrogen electrode (RHE).<sup>[5]</sup> While Au is currently the most efficient electrocatalytic surface for CO<sub>2</sub> reduction to CO, the low abundance and high cost of Au may prevent its large-scale applications. To find a cost-effective and stable catalyst with high selectivity and efficiency remains a challenge for achieving practical utilization of  ${\rm CO_2}$  reduction to CO.

Metallic Ag has attracted considerable attention due to its significantly lower cost compared to Au and high selectivity for the conversion of CO<sub>2</sub> to CO.<sup>[7,11]</sup> However, the high overpotential (>0.9 V) on Ag catalysts is required for driving the electrocatalytic reduction of CO2 efficiently and selectively with suppressed H<sub>2</sub>O reduction.<sup>[5]</sup> The large overpotential required for the reduction of CO<sub>2</sub> is attributed to the hindrance for the initial electron transfer to a CO2 molecule. [2,19-21] Lu et al. [19] reported that a nanoporous Ag catalyst with a fast initial electron transfer prepared by the de-alloying of an Ag-Al prescursor is capable of reducing CO2 electrochemically to CO efficiently and selectively at reduced overpotential. Recently, Kanan et al.[21,22] discovered that oxide-derived Cu and Au nanoparticle films exhibit a dramatically improved selectivity for the reduction of CO<sub>2</sub> to CO at low overpotential and high resistance to catalytic deactivation compared to polycrystalline metals.

This study is the first exploration of the catalytic activity of the electrochemical reduction of CO<sub>2</sub> on oxide-derived nanostructured Ag catalysts (OD-Ag). Here we demonstrate that a nanostructured Ag electrode resulting from silver oxide is capable of electrochemically reducing CO<sub>2</sub> to CO with high selectivity at much lower overpotential compared to that of the polycrystalline Ag, and the increased catalytic activity is linked to the improved stabilization of the COOH intermediate.

The thermal oxidation of Ag foils is prohibited because the decomposition of silver oxide becomes significant at temperatures above 200°C.[23] Here, we used a simple and scalable electrochemical method for oxidizing Ag electrodes. Potential anodization in alkaline solutions was an effective and simple method for the formation of Ag oxide on Ag electrodes.<sup>[24-28]</sup> Here, an electrode made of a polycrystalline Ag foil was immersed in 0.2 m NaOH solutions in a twocompartment cell with a Pt counter electrode and an Ag/AgCl reference electrode (cyclic voltammetry of Ag in 0.2 M NaOH is shown in Figure S1 in the Supporting Information). The two-compartment cell was separated by a Nafion-115 proton exchange membrane to avoid Pt deposition on Ag electrodes during the electrochemical synthesis. A symmetric 50 Hz square-wave pulsed potential was applied on Ag electrodes to synthesize Ag oxide layers. We found that the fabricated Ag oxide layers exhibit a porous structure, as shown in Figure S2. The resulting Ag oxide electrodes were directly used in the electrochemical reduction of CO<sub>2</sub>, and were electrochemically reduced to metallic Ag in the early stage of electrolysis.

Figure 1 a,b show scanning electron microscope (SEM) images of electrodes resulting from Ag oxide after the

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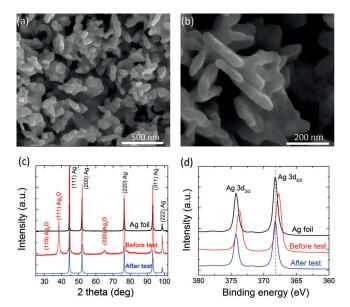


Figure 1. a,b) SEM images of oxide-derived Ag. c) XRD patterns and d) XPS spectrum of the polycrystalline Ag electrode (black line) and Ag oxide electrode before (red line) and after (blue line)  $CO_2$  reduction electrolysis, respectively.

electrocatalytic reduction of  $\mathrm{CO}_2$  in  $\mathrm{CO}_2$ -saturated electrolytes. The SEM images indicate that a porous-like nanostructured Ag surface was formed as a result of the reduction of Ag oxide after electrolysis. The X-ray diffraction (XRD) pattern in Figure 1 c confirms the presence of  $\mathrm{Ag}_2\mathrm{O}$  on Ag foil synthesized by anodization in alkaline solutions. After  $\mathrm{CO}_2$  reduction electrolysis, XRD pattern shows only Ag peaks with no more indication of any remaining Ag oxide. In addition, the Ag foil fabricated by anodization turned a black color (Figure S3), which is also indicative of the formation of Ag oxide, and the sample had no remaining black color after  $\mathrm{CO}_2$  reduction electrolysis.

To further confirm the composition of the samples before and after electrolysis, X-ray photoelectron spectroscopy (XPS) measurements were performed. The Ag  $3d_{5/2}$  peak at 368.2 eV was observed for polycrystalline Ag in Figure 1 d. For the synthesized Ag oxide, the Ag  $3d_{5/2}$  peak shifted to the binding energy of 367.7 eV, which corresponds to the Ag<sub>2</sub>O formation according to the Ag  $3d_{5/2}$  peak analysis for Ag and

Ag oxide in previous work.  $^{[29]}$  After electrolysis, the Ag  $^{3}$ d $_{5/2}$  peak shifted back to  $^{3}$ 68.2 eV, implying the surface was metallic Ag without any Ag oxide.  $^{[29]}$  The Ag  $^{3}$ d XPS spectrum analysis is consistent with the results of the XRD patterns, indicating the electroreduction of  $^{4}$ d $^{2}$ O to metallic Ag was complete within the detection limit of these characterization techniques.

The electrocatalytic reduction of CO<sub>2</sub> on OD-Ag and polycrystalline Ag were performed in CO<sub>2</sub>-saturated 0.1M KHCO<sub>3</sub> (99.95%) electrolyte (pH 6.83) at ambient temperature and pressure. In the initial period of electrolysis, OD-Ag electrodes were directly formed in situ by the electroreduction of the Ag oxide film formed on the Ag electrode. CO<sub>2</sub> reduction electrolysis experiments were performed in an electrochemical cell consisting of working and counter electrode compartments, separated by a Nafion-115 proton exchange membrane to prevent the oxidation of CO<sub>2</sub> reduction products. The cathodic compartment was continuously purged with CO<sub>2</sub> at a constant flow rate and vented directly into the gas-sampling loop of a gas chromatograph (GC) for the periodic quantification of the gas-phase products. Liquid products formed in the CO2 reduction were detected by <sup>1</sup>H nuclear magnetic resonance (NMR) spectroscopy after completion of the electrolysis experiments.

The comparison of the CO<sub>2</sub> reduction activity of untreated polycrystalline Ag and OD-Ag is presented in Figure 2. The OD-Ag exhibited a high initial current density  $(j_{tot})$  (Figure S4), which stems from the reduction of the Ag oxide layer in the initial period of electrolysis. Subsequently, the OD-Ag exhibited a  $j_{\text{tot}}$  of 1.15 mA cm<sup>-2</sup> with CO faradaic efficiency of 89% at  $-0.8\,\mathrm{V}$  vs. RHE, as shown in Figure 2a. At a less negative potential of -0.7 V vs. RHE, a decreased FE of 82.4% for CO formation was observed (Figure 2b). Notably, the FE of 80% for CO production was achieved at -0.6 V vs. RHE (Figure 2c), corresponding to a modest overpotental  $(\eta_{CO})$  of 0.49 V relative to the CO<sub>2</sub>/CO equilibrium potential of -0.11 V vs. RHE. In contrast, the polycrystalline Ag electrodes experienced low  $j_{tot}$ , accompanying with very low FE for CO formation (22.4%, 12% and 4.1% at -0.8 V, -0.7 V and -0.6 V vs. RHE, respectively).

To better understand the catalytic activity for CO<sub>2</sub> reduction, the FE for the major products of CO<sub>2</sub> reduction was plotted at various potentials for the polycrystalline Ag and the OD-Ag (Figure 3). As noted in Figure 3a, the FE for

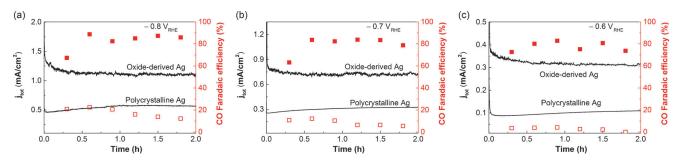


Figure 2. CO $_2$  reduction performance of untreated Ag and oxide-derived Ag. The total current density (left axis) and the CO faradaic efficiency (right axis) on untreated Ag and oxide-derived Ag (■ and □ represent CO faradaic efficiency on oxide-derived Ag and untreated Ag, respectively) at a) −0.8 V and b) −0.7 V, and c) −0.6 V versus RHE in CO $_2$ -saturated 0.1 M KHCO $_3$  electrolytes.

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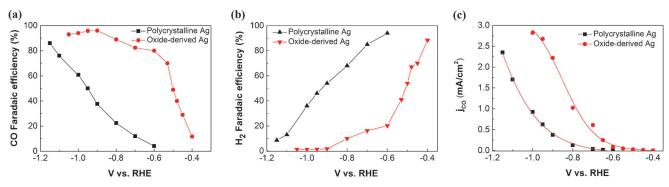


Figure 3. Comparison of the electrocatalytic activity of polycrystalline Ag and oxide-derived Ag. Faradaic efficiency for CO (a) and  $H_2$  (b) on polycrystalline Ag and oxide-derived Ag at various potentials in  $CO_2$ -saturated 0.1 M KHCO<sub>3</sub> (pH 6.8). c) Current density for CO at various potentials.

the electrochemical reduction of CO<sub>2</sub> to CO on both the polycrystalline Ag and the OD-Ag gradually increased with enhancing overpotentials. The increase of the FE for CO corresponds to a decrease in the related FE for H<sub>2</sub> production (Figure 3b). In addition, a small amount of formate was only detected at high overpotentials (Figure S5). Interestingly, Figure 3a shows that the overall FE for CO on the OD-Ag was shifted by  $> 400 \,\mathrm{mV}$  toward the positive potential compared to that of untreated Ag (at a FE range for CO of more than 30%). In addition, the current density for CO production as a function of potentials in Figure 3c implies the onset potential for  $CO_2$  reduction on OD-Ag was -0.4 V vs. RHE ( $\eta_{\rm CO} = 0.29 \text{ V}$ ), which is a positive shift by about 200 mV compared to that (-0.6 V vs. RHE) of polycrystalline Ag. More importantly, for driving the electrocatalytic reduction of  $CO_2$  to CO with a high FE of 80%, a potential of -0.6 V vs. RHE was required on OD-Ag, which is significantly reduced by 500 mV compared to that of untreated Ag (-1.1 V vs. RHE). These results indicate that OD-Ag acts as an efficient catalyst for the electrocatalytic reduction of CO2 to CO with significantly suppressed H<sub>2</sub> evolution at decreased overpo-

To gain insight into the electrokinetic mechanism of  $\mathrm{CO}_2$  reduction on both catalysts, Tafel analysis was performed. Here, Tafel plots of the OD-Ag and the polycrystalline Ag (overpotential versus log of the partial current density for CO production) are shown in Figure 4. Hori has proposed that a two-electron transfer is involved in the electrochemical reduction of  $\mathrm{CO}_2$  to  $\mathrm{CO}$  (Scheme 1). [11,30] In addition, most of the computational studies on reaction paths for  $\mathrm{CO}_2$  reduc-

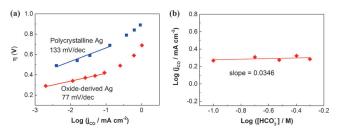
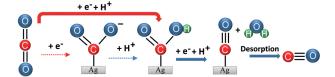


Figure 4. a) Tafel plots of the CO partial current density for polycrystalline Ag and oxide-derived Ag. b) Bicarbonate concentration at constant potential for oxide-derived Ag.



**Scheme 1.** Proposed reaction paths for electrocatalytic reduction of  $CO_2$  to CO.

tion are based on the computational hydrogen electrode (CHE) model, in which it is assumed that a proton-coupled electron transfer (PCET) takes place at every reaction step.[31-35] Thus, a COOH is assumed to be formed by a PCET as the first CO<sub>2</sub> activation step in density functional theory (DFT) simulations.[31,33-35] However, in some experimental work, it is believed that the adsorbed CO2. intermediate is formed on the active sites of the metal surface through a one-electron transfer to a CO<sub>2</sub> molecule, and then the COOH intermediate is produced after accepting one proton.[19-22,36] Furthermore, it was reported that the first donation of a proton is from HCO<sub>3</sub><sup>-</sup>. [19,21,35] Subsequently, the COOH intermediate on the surface takes another electron and proton to form a CO and a H<sub>2</sub>O molecule. It has been demonstrated that the initial electron transfer for CO2 activation is the rate-determining step (RDS) for the overall process because the first electron transfer requires a much more negative potential compared to the following steps.[2,19-21]

A Tafel slope of 133 mV dec<sup>-1</sup> for polycrystalline Ag shown in Figure 4a corresponds to a transfer coefficient of 0.44 [Eq. (S2)]. This slope and the transfer coefficient are consistent with the fact that the rate-determining step is the initial electron transfer to CO<sub>2</sub>.<sup>[11,19]</sup> In contrast, OD-Ag exhibited a low Tafel slope of 77 mV dec<sup>-1</sup> at low overpotentials, which indicates a fast initial electron transfer to a CO<sub>2</sub> molecule according to previous studies.<sup>[7,19,21,22]</sup> Subsequently, we found a dramatic increases of the Tafel slope for OD-Ag at relatively high overpotentials, indicating the CO<sub>2</sub> electroreduction may reach a mass transport limitation on the porous-like nanostructured Ag.<sup>[35]</sup> Thus, while the mass transport in a nanostructured Ag catalyst is likely slower than in an untreated Ag (flat surface) at relatively high

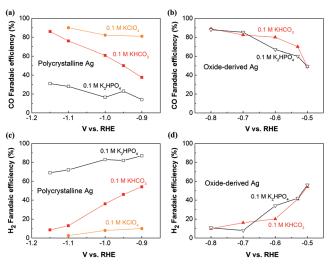




overpotentials, OD-Ag can offer better stabilization for the COOH intermediate than untreated Ag, thus decreasing the overpotential needed to drive CO<sub>2</sub> reduction to CO.

To further investigate the electrokinetics of  $\mathrm{CO_2}$  reduction on OD-Ag, electrolysis was performed at the  $\mathrm{HCO_3}^-$  concentrations from 0.5 to 0.1 M. A plot of  $\log(j_{\mathrm{CO}})$  vs.  $\log([\mathrm{HCO_3}^-])$  in Figure 4b shows a zero-order dependence of  $\mathrm{HCO_3}^-$  concentrations on  $\mathrm{CO_2}$  reduction activity, indicating that the donation of a proton from  $\mathrm{HCO_3}^-$  is not a rate-determining step for  $\mathrm{CO_2}$  reduction. [19]

It was reported that the surface of nanostructured Ag catalysts can provide the low-coordinated surface Ag sites, which plays a significant role for stabilizing the COOH intermediate through reducing the activation energy barrier of the initial electron transfer.<sup>[35]</sup> In addition, Kanan et al. proposed a grain boundary effect for OD-Cu<sup>[37]</sup> and OD-Au.<sup>[38]</sup> Here we propose a local pH effect to offer a new insight into the correlation of nanostructured Ag catalysts with the catalytic activity for CO<sub>2</sub> reduction. The pH rises locally at the electrode/electrolyte interface because of releasing OH<sup>-</sup> in the cathodic reactions (Equation S (4–5)).<sup>[39]</sup> Thus, the pH close to the electrode (local pH) is higher than the bulk pH. To understand the local pH effect, CO<sub>2</sub> reduction was performed on flat Ag and OD-Ag in 0.1 m K<sub>2</sub>HPO<sub>4</sub> and 0.1 m KHCO<sub>3</sub>, respectively. The FE for CO on flat Ag was



**Figure 5.** Faradaic efficiency for CO and  $H_2$  on polycrystalline Ag (a,c) and oxide-derived Ag (b,d) at various potentials in  $CO_2$ -saturated 0.1 M  $K_2HPO_4$  and  $CO_2$ -saturated 0.1 M KHCO $_3$ , respectively. CO2 reduction on flat Ag was also performed in  $CO_2$ -saturated 0.1 M KClO $_4$ .

significantly reduced (Figure 5 a) with dramatically enhanced FE for H<sub>2</sub> (Figure 5 c) in CO<sub>2</sub>-saturated 0.1 m K<sub>2</sub>HPO<sub>4</sub>, which is consistent with the work of Hori on flat Cu (FE for H<sub>2</sub> is 72.4% and 10.9% in 0.1 m K<sub>2</sub>HPO<sub>4</sub> and 0.1 m KHCO<sub>3</sub>, respectively).<sup>[11]</sup> This observation is due to the fact that the buffer action of CO<sub>2</sub>-saturated 0.1 m K<sub>2</sub>HPO<sub>4</sub> can easily neutralize OH<sup>-</sup> generated at the electrode surface, keeping local pH at relatively low value. The low pH value at the electrode/electrolyte interface favors H<sub>2</sub> evolution.<sup>[11]</sup> To further improve the local pH effect, CO<sub>2</sub> reduction was also

measured on flat Ag in 0.1m KClO<sub>4</sub>. KClO<sub>4</sub> does not have buffer ability, which results in a relatively high local pH at the electrode/electrolyte interface. We found that the FE for CO in CO<sub>2</sub>-saturated 0.1m KClO<sub>4</sub> was obviously higher than that of CO<sub>2</sub>-saturated 0.1m KHCO<sub>3</sub> (Figure 5a). These observations (the FE for CO on flat Ag: KClO<sub>4</sub>>KHCO<sub>3</sub>> K<sub>2</sub>HPO<sub>4</sub>) imply that the local pH may play an important role in the reduction of CO<sub>2</sub>.

In contrast, we found that FE for CO on OD-Ag was almost equal in the two different electrolytes (Figure 5b) at various potentials. This observation may be partly attributed to that the limitation of the diffusion process in nanoporous Ag catalysts (Figure 1 a,b) hinders the neutralization reaction for OH $^-$  generated near the catalyst surface, resulting in a high local pH in 0.1 m K<sub>2</sub>HPO<sub>4</sub>. In addition, H<sub>2</sub> evolution is not favorable at the high pH value. Thus, the high local pH created in nanoporous Ag may contribute to the suppressed H<sub>2</sub> evolution (Figure 5 d) with preferred CO<sub>2</sub> reduction (Figure 5 b).

In summary, nanostructured Ag catalysts prepared by electrochemically reducing Ag2O exhibited an enhanced catalytic activity for the reduction of CO2, and the high selectivity for CO was shifted by more than 400 mV to a lower overpotential than that of untreated polycrystalline Ag. At a moderate overpotential of 0.49 V, the oxide-derived nanostructured Ag was able to reduce CO<sub>2</sub> to CO with about 80 % faradaic efficiency, which is dramatically higher compared to that (ca. 4%) of untreated polycrystalline Ag at identical conditions. The dramatically improved catalytic activity and selectivity for CO<sub>2</sub> reduction to CO is likely correlated with the nanostructured surface, resulting in highly active sites for stabilizing COOH intermediate. In addition, a high local pH generated within the porous-like nanostructured Ag catalysts may also play a role in the improved CO<sub>2</sub> reduction along with suppressed H<sub>2</sub> evolution. This study shows that a selective and cost-effective oxide-derived Ag catalyst can efficiently and selectively reduce CO<sub>2</sub> to CO. While the catalytic activity of this oxide-derived Ag catalyst is not as high as the recent oxide-derived Au, its cost is significantly lower, and thus this catalyst and synthetic approach may provide a more practical platform for large-scale CO<sub>2</sub> electroreduction.

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**Keywords:** carbon dioxide · conversion of carbon dioxide · electrocatalysis · heterogeneous catalysis · surface chemistry

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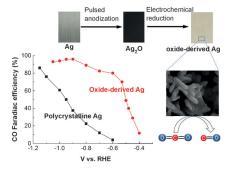
# **Communications**



#### Electrocatalysis

M. Ma, B. J. Trześniewski, J. Xie,
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Selective and Efficient Reduction of Carbon Dioxide to Carbon Monoxide on Oxide-Derived Nanostructured Silver Electrocatalysts



Nanostructured surfaces: An oxidederived silver electrocatalyst was synthesized for the conversion of carbon dioxide to carbon monoxide with a high Faraday efficiency at low overpotentials. The nanostructure of the catalyst lowered the overpotentials as compared to polycrystalline silver by creating a high local pH value near the surface of the catalyst.