

CO Reduction

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# Enhanced Carbon Monoxide Electroreduction to $>1 \text{ A cm}^{-2} \text{ C}_{2+}$ Products Using Copper Catalysts Dispersed on MgAl Layered Double Hydroxide Nanosheet House-of-Cards Scaffolds

Sungun Kwon, Jie Zhang, Ramesha Ganganahalli, Sumit Verma, and Boon Siang Yeo\*

**Abstract:** Cu catalysts are most apt for reducing  $\text{CO}_{(2)}$  to multi-carbon products in aqueous electrolytes. To enhance the product yield, we can increase the overpotential and the catalyst mass loading. However, these approaches can cause inadequate mass transport of  $\text{CO}_{(2)}$  to the catalytic sites, which will then lead to  $\text{H}_2$  evolution dominating the product selectivity. Herein, we use a MgAl LDH nanosheet ‘house-of-cards’ scaffold to disperse CuO-derived Cu (OD-Cu). With this support-catalyst design, at  $-0.7 \text{ V}_{\text{RHE}}$ , CO could be reduced to  $\text{C}_{2+}$  products with a current density ( $j_{\text{C}_{2+}}$ ) of  $-1251 \text{ mA cm}^{-2}$ . This is  $14\times$  that of the  $j_{\text{C}_{2+}}$  shown by unsupported OD-Cu. The current densities of  $\text{C}_{2+}$  alcohols and  $\text{C}_2\text{H}_4$  were also high at  $-369$  and  $-816 \text{ mA cm}^{-2}$  respectively. We propose that the porosity of the LDH nanosheet scaffold enhances CO diffusion through the Cu sites. The CO reduction rate can thus be increased, while minimizing  $\text{H}_2$  evolution, even when high catalyst loadings and large overpotentials are used.

## Introduction

The electrocatalytic  $\text{CO}_2$  or CO reduction reaction ( $\text{CO}_2\text{RR}$  or CORR) in aqueous electrolytes, powered by renewable electricity, has drawn attention in recent years as a sustainable approach to produce green fuels and chemical

feedstocks.<sup>[1–3]</sup> In order to scale up this process for widespread deployment, it is necessary to enhance the yield (current densities) of products formed.<sup>[2,4]</sup> The most direct way to achieve this would be to increase the catalyst mass loading on the electrode. However, this practice can lead to an unwanted agglomeration of the catalyst particles.<sup>[4,5]</sup> As such, catalyst mass loadings are often kept to  $<2 \text{ mg cm}^{-2}$ .<sup>[2,4–6]</sup> To prevent agglomeration of catalyst particles, supports such as high surface area graphene or carbon nanotubes can be used.<sup>[7,8]</sup> Unfortunately, trace metal impurities, known to be present on these carbon materials, can alter the properties of the catalysts, or worse still, poison and catalytically deactivate them.<sup>[9–11]</sup> Another method to increase the reaction yield is to apply a larger overpotential. These commonly used approaches have a major drawback: As the reaction rate per geometric surface area of the electrode increases, the  $\text{CO}_2$  or CO feedstock may percolate insufficiently into the catalyst layer.<sup>[2,5,7]</sup> Consequently, the parasitic hydrogen evolution reaction (HER) will start to dominate the selectivity of products formed. For this reason, considerable efforts have been devoted to understanding changes in the structures and properties of catalyst films as a function of its composition, and the effect of these changes on the rate and selectivity of  $\text{CO}_2$  or CO reduction.

An alternative catalyst support is layered double hydroxides (LDH). The general formula of LDH is  $[\text{M}^{2+}_{(1-x)}\text{M}^{3+}_x(\text{OH})_2]\text{A}^{n-}_{(x/n)} \cdot m\text{H}_2\text{O}$ , where  $\text{M}^{2+}$  and  $\text{M}^{3+}$  are the divalent and trivalent metal ions respectively, and  $\text{A}^{n-}$  is the intercalating anion.<sup>[12,13]</sup> LDH nanoparticles can also be exfoliated to high surface area nanosheets.<sup>[14–16]</sup> A property of the LDH nanoparticles or nanosheets is that as the number of their surface atoms relative to bulk atoms increases, the surface-to-surface attraction between the particles is enhanced.<sup>[17]</sup> Continuous films made up of LDH nanoparticles/nanosheets can thus be formed, exhibiting structures that resemble ‘house-of-cards’.<sup>[17,18]</sup> We envisage that these structures can serve as scaffolds to disperse the catalysts (Figure 1a–b). The resulting porosity in the catalyst layer will thus allow better CO or  $\text{CO}_2$  gas penetration.

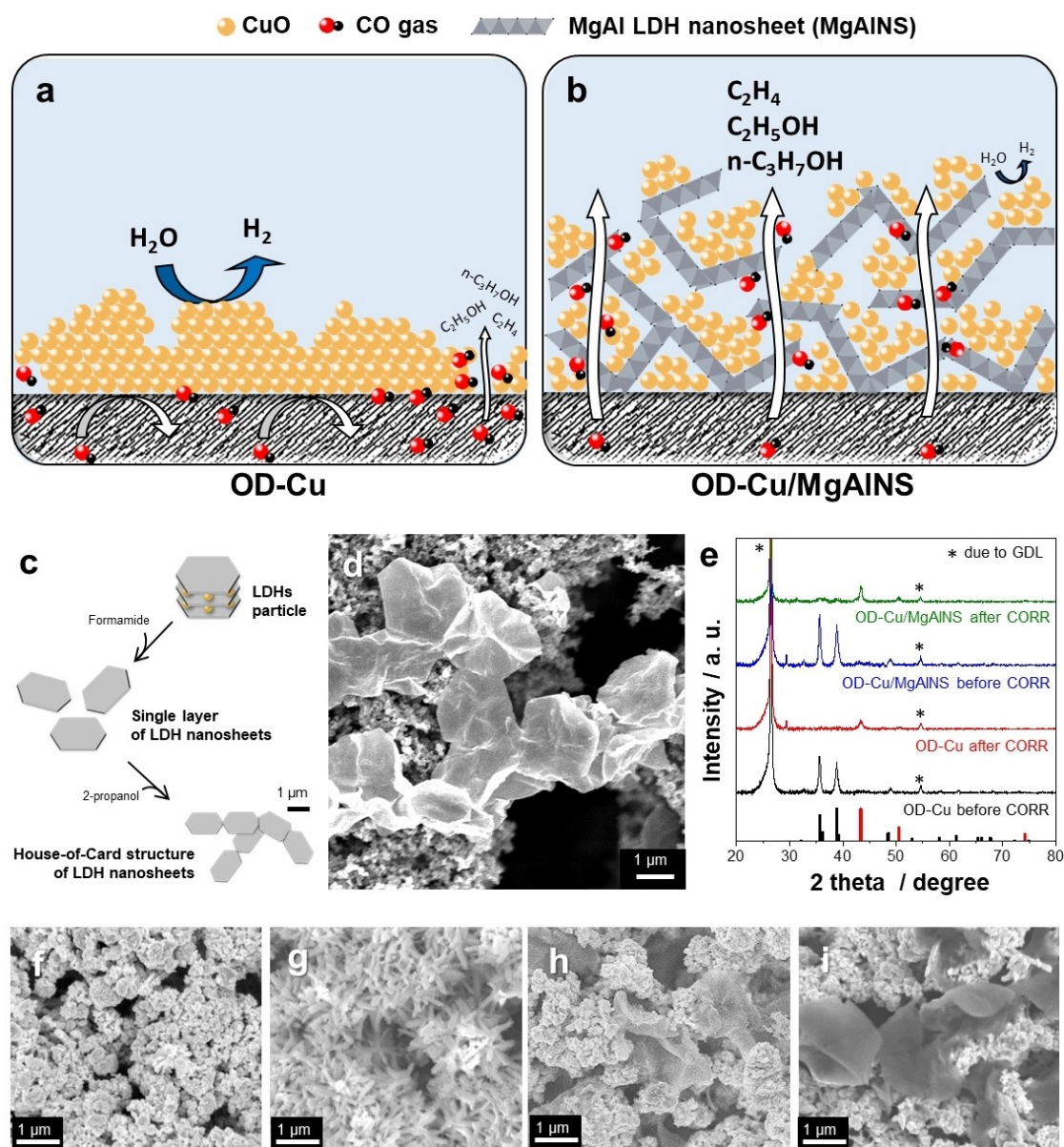
On the basis of the above discussion, we demonstrate herein the use of a house-of-cards scaffold made of MgAl LDH nanosheets to support CuO-derived Cu (OD-Cu) catalysts for CORR. The MgAl LDH nanosheet house-of-cards structure was effective in dispersing the OD-Cu nanoparticles during CORR. Together, they also reduced CO to  $\text{C}_{2+}$  products with high activity and selectivity. Using this system,  $\text{C}_{2+}$  products could be formed at  $-0.7 \text{ V}$  vs.

[\*] Dr. S. Kwon, Dr. J. Zhang, Prof. Dr. B. S. Yeo  
Department of Chemistry, Faculty of Science, National University of Singapore  
3 Science Drive 3, 117543 Singapore (Singapore)  
E-mail: chmyeos@nus.edu.sg

Dr. R. Ganganahalli  
Shell India Markets Private LTD Plot No. 7,  
Bengaluru Hardware Park, Mahadeva, Kodigehalli, 562149 Bangalore North (India)

Dr. S. Verma  
Shell International Exploration & Production Inc.  
3333 Highway 6 South, 77082 Houston, TX (USA)

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**Figure 1.** (a-b) Schematic illustration of catalysts loaded on gas diffusion layers during CORR: (a) OD-Cu only and (b) OD-Cu mixed with MgAl LDH nanosheets (MgAlNS). (c) Schematic representation of the formation of MgAl LDH nanosheet house-of-cards structures. (d) SEM image of MgAl LDH nanosheets, showing the house-of-cards structures. (e) XRD patterns of OD-Cu and OD-Cu/MgAlNS before and after they were used for CORR. Standard XRD patterns of CuO (black bars; Crystallography Open Database (COD) card number 1011194) and Cu (red bars; COD card number 4105681) are shown at the bottom of the figure. SEM images of OD-Cu (f) before and (g) after it was used as catalyst for CORR, and OD-Cu/MgAlNS (h) before and (i) after it was used as catalyst for CORR. The mass loadings of CuO and MgAlNS were respectively 2.91 and 0.29 mg cm<sup>-2</sup>. We believed that in the absence of a support, the CuO particles were more agglomerated and thus reduced to aggregates of Cu<sup>0</sup> rods (Figure 1g) during CORR. In contrast, the MgAlNS dispersed the CuO particles well, which thus reduced the change in its morphology during CORR (Figure 1i).

reversible hydrogen electrode (RHE) with an average  $FE_{C_2+}$  of 71 % and current density ( $j_{C_2+}$ ) of  $-1251 \text{ mA cm}^{-2}$ . We show that the unique house-of-cards structure made by the LDH nanosheets disperses the Cu catalyst such that the  $FE$  of  $C_2+$  products can be maintained even with a high catalyst mass loading and at large overpotentials.

## Results and Discussion

### Characterization of OD-Cu/MgAlNS

The synthesis of the MgAl LDH and its exfoliation to nanosheets are presented in Figure 1c, Sections S1.1 and S2.<sup>[15]</sup> X-ray diffraction (XRD) and scanning electron microscopy (SEM) revealed that the MgAl LDH are crystalline and hexagonally shaped with lengths 1–2  $\mu\text{m}$  (Figures S1 and

S2a). The exfoliated MgAl LDH nanosheets (MgAlNS) were first pre-assembled into a house-of-cards structure in solution (Figures 1d, S2b–S2d and S3).<sup>[17]</sup> They were then physically mixed with commercially-purchased CuO nanoparticles (<50 nm, Sigma–Aldrich) in a mass ratio of 1:10, and used as CORR catalyst.

CuO ( $2.91 \text{ mg cm}^{-2}$ ) and CuO/MgAlNS catalysts ( $2.91 \text{ mg cm}^{-2}$  CuO and  $0.29 \text{ mg cm}^{-2}$  MgAlNS) were respectively deposited onto carbon gas diffusion layers (GDL), and used as working electrodes in a flow cell electrolyzer. A Ag/AgCl reference electrode and a Ni foam counter electrode was used. Aqueous 1 M KOH served as electrolyte. A representative potential of  $-0.7 \text{ V}$  vs. RHE (all potentials reported hereafter are referenced to the RHE) was applied for 1 hr. The CuO nanoparticles were reduced to aggregates of  $\sim 500 \text{ nm}$  long  $\text{Cu}^0$  rods (which we now termed as OD-Cu) after they were used as catalysts for CORR (Figure 1e–g). SEM imaging of the CuO/MgAlNS composite shows the MgAlNS dispersing the CuO nanoparticles (Figure 1h). After the composite was used as catalyst for CORR, the MgAlNS house-of-cards remained intact. More importantly, the dispersion of the now OD-Cu particles amongst the MgAlNS was preserved (Figures 1h–i and S6–7). We further found, using a tape test method, that the OD-Cu/MgAlNS film (after being used for CORR) was mechanically attached onto the GDL  $\sim 20$  percentage points better, as compared to the unsupported OD-Cu (Section S3).<sup>[19]</sup>

### Effects of House-of-Cards Scaffold on OD-Cu for CO Reduction

The effect of having a MgAlNS house-of-cards scaffold to support the OD-Cu during CORR is first studied using linear sweep voltammetry in 1 M KOH electrolyte (Figure S10). OD-Cu/MgAlNS showed a lower onset potential and higher total current density, compared to that of the unsupported OD-Cu. MgAlNS itself is electrochemically-inactive.

We next investigate the effects of various catalyst mass loadings on CORR at a representative potential of  $-0.7 \text{ V}$  (Figure 2a–b, Tables S1 and S2; the potentials stated for all electrolyses have been iR-drop compensated). Mass loadings of CuO from  $0.36$  to  $5.82 \text{ mg cm}^{-2}$  were used. The major CORR products detected include ethylene, ethanol, 1-propanol and acetate (Figure S11).  $\text{H}_2$  gas was formed from the hydrogen evolution reaction. Using an electrode loaded with  $0.36 \text{ mg cm}^{-2}$  of CuO, CO could be reduced to  $\text{C}_{2+}$  products with a FE of 70 %. When the CuO mass loading was increased to  $0.73$  and  $1.46 \text{ mg cm}^{-2}$ , the  $\text{FE}_{\text{C}_{2+}}$  further increased to 72 and 73 %, respectively. However, at higher CuO mass loadings of  $2.91$  and  $5.82 \text{ mg cm}^{-2}$ , HER dominated, and the  $\text{FE}_{\text{C}_{2+}}$  decreased to 20 and 19 %, respectively. The  $j_{\text{C}_{2+}}$  also increased by only  $2.4\times$  from  $-37$  to  $-90 \text{ mA cm}^{-2}$ , as CuO mass loading increased. We attribute the decline in  $\text{FE}_{\text{C}_{2+}}$  when higher mass loading was used to the catalyst particles aggregating, which lessens porosity within the catalyst layer and reduces the population of available active sites.<sup>[2,4,5]</sup>

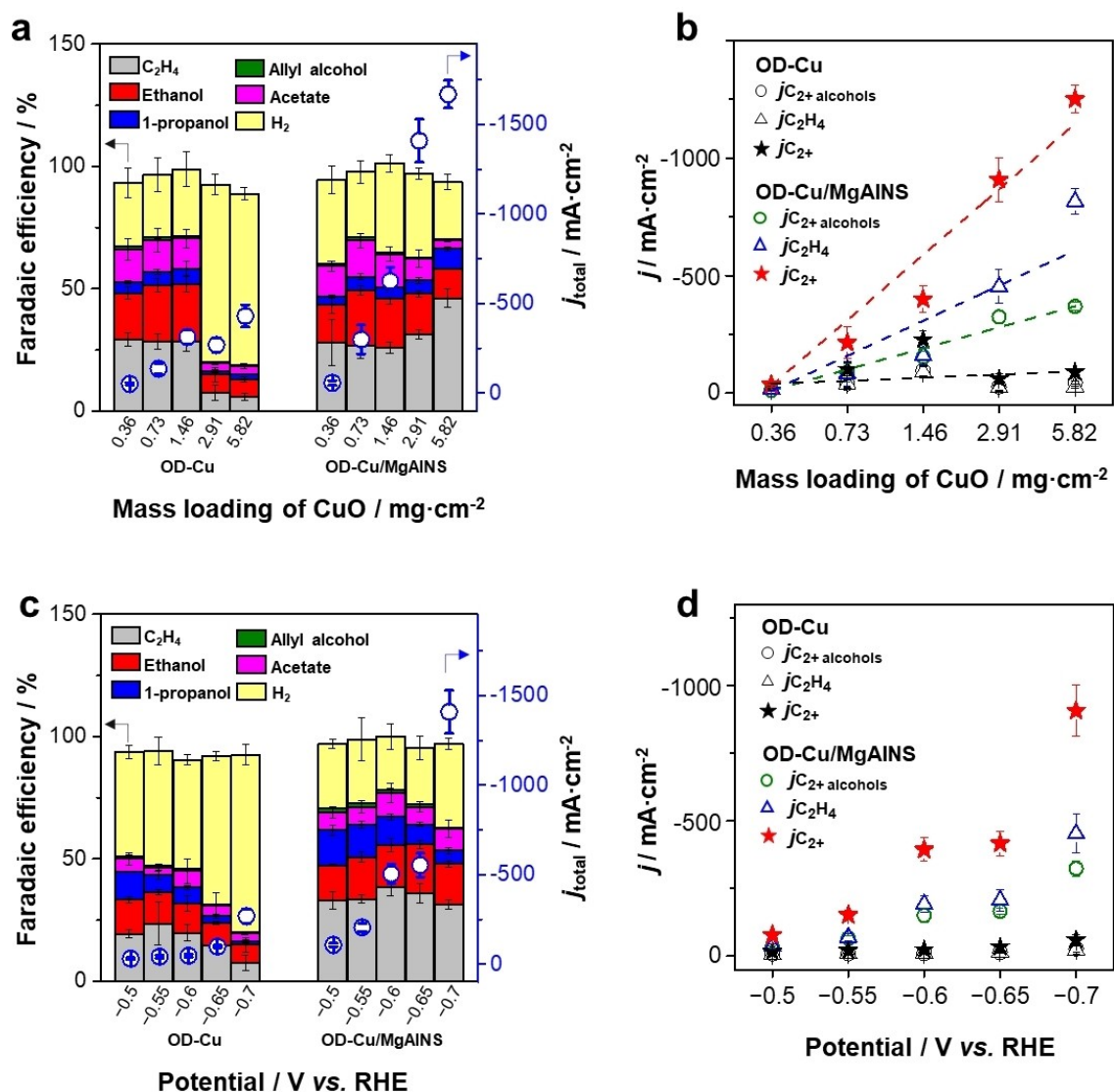
When CuO particles physically mixed with MgAlNS (in a 1:10 mass ratio) were used as CORR catalysts, the FEs of  $\text{C}_{2+}$  products could be maintained at 62–72 %, even with the highest CuO mass loading of  $5.82 \text{ mg cm}^{-2}$  (Figure 2a; Table S2). More interestingly, we note that the  $j_{\text{C}_{2+}}$  increased dramatically as the CuO/MgAlNS mass loadings increased (Figure 2b). Using  $5.82 \text{ mg cm}^{-2}$  of CuO mixed with  $0.58 \text{ mg cm}^{-2}$  MgAlNS, the average  $j_{\text{C}_{2+}}$  obtained during CORR was  $-1251 \text{ mA cm}^{-2}$ , which was 14-fold higher than that of using only CuO ( $-90 \text{ mA cm}^{-2}$ ). The partial current densities of ethylene and the  $\text{C}_{2+}$  alcohols were also remarkably high at  $-816$  and  $-369 \text{ mA cm}^{-2}$  respectively (compared with  $j_{\text{ethylene}} = -27 \text{ mA cm}^{-2}$  and  $j_{\text{C}_{2+} \text{ alcohols}} = -46 \text{ mA cm}^{-2}$  exhibited by unsupported OD-Cu; Table S1). These results illustrate that the MgAlNS promote the formation of  $\text{C}_{2+}$  products even at high CuO mass loadings over  $2 \text{ mg cm}^{-2}$ . We highlight here that the MgAlNS themselves have negligible CORR catalytic activity, catalysing mainly  $\text{H}_2$  evolution; the  $j_{\text{total}}$  exhibited by MgAlNS was only  $-0.3 \text{ mA cm}^{-2}$  (Table S3).

We then compare the CORR activities exhibited by OD-Cu and OD-Cu/MgAlNS at potentials from  $-0.5$  to  $-0.7 \text{ V}$  (CuO loading:  $2.91 \text{ mg cm}^{-2}$  and MgAlNS loading:  $0.29 \text{ mg cm}^{-2}$ ; Figure 2c–d, Tables S4–S5). It is again striking that by using a simple composite of MgAlNS physically mixed with CuO particles, CO could be sustainably reduced to  $\text{C}_{2+}$  products with FEs between 63–79 %. Over the same potential range, the  $j_{\text{C}_{2+}}$  also increased  $\sim 12\times$  from  $-79$  to  $-908 \text{ mA cm}^{-2}$ . In contrast, the  $\text{FE}_{\text{C}_{2+}}$  exhibited by the unsupported OD-Cu decreased from 52 to 20 %, as the applied potential becomes more negative from  $-0.5$  to  $-0.7 \text{ V}$ . Their  $j_{\text{C}_{2+}}$  were also low at between  $-17$  to  $-61 \text{ mA cm}^{-2}$ .

Carbon-based supports such as graphite and carbon nanotubes have been used to disperse catalyst particles and thereby increase their active catalytic areas.<sup>[20,21]</sup> However, these supports can alter, sometimes detrimentally, the intrinsic selectivities of the catalysts towards  $\text{CO}_2$ RR or CORR.<sup>[22]</sup> For example, multi-walled carbon nanotubes (MWCNT) loaded with Cu–Ni have been shown to promote hydrogen evolution, instead of  $\text{CO}_2$  reduction.<sup>[22]</sup> Here in this study, we note that the relative selectivities of the various COR products formed did not change considerably whether OD-Cu or OD-Cu/MgAlNS catalysts were used. For example, during CORR at  $-0.7 \text{ V}$ , the  $\text{FE}_{\text{ethanol}}/\text{FE}_{\text{ethylene}}$  exhibited by OD-Cu and OD-Cu/MgAlNS were close at  $\sim 0.8$  (Tables S1 and S2; loadings of CuO and MgAlNS were respectively  $0.73$  and  $0.073 \text{ mg cm}^{-2}$ ). This observation indicates that the MgAlNS scaffolds do not affect the intrinsic catalytic activity of the OD-Cu.

The CORR activity and selectivity of our commercially-purchased CuO was further compared with that of highly CORR-active CuO nanoparticles synthesized using the procedure published by Jiao and co-workers (Figure S12 and Table S6).<sup>[4]</sup> At  $-0.7 \text{ V}$ , the Cu catalyst synthesized using Jiao's method (which we shall termed as Cu<sub>J</sub>) exhibited a  $j_{\text{C}_{2+}}$  of  $-415 \text{ mA cm}^{-2}$  and a  $\text{FE}_{\text{C}_{2+}}$  of 65 %, which are significantly higher than that of the OD-Cu ( $j_{\text{C}_{2+}} = -61 \text{ mA cm}^{-2}$ ;  $\text{FE}_{\text{C}_{2+}} = 20 \%$ ). The enhanced performance





**Figure 2.** (a) Faradaic efficiencies and (b) partial current densities of major products formed during CORR at  $-0.7$  V using various loadings of OD-Cu and OD-Cu/MgAlNS. The mass ratio of MgAlNS and CuO loaded on the GDL was always kept at 1:10. (c) Faradaic efficiencies and (d) partial current densities of major CORR products formed using OD-Cu and OD-Cu/MgAlNS at different applied potentials. The mass loadings of CuO and MgAlNS were respectively 2.91 and 0.29  $\text{mg}\cdot\text{cm}^{-2}$ . Minor products with FEs less than 1% are not shown in (a) and (c). Measurements were performed in a flow cell electrolyzer with 1 M KOH electrolyte.

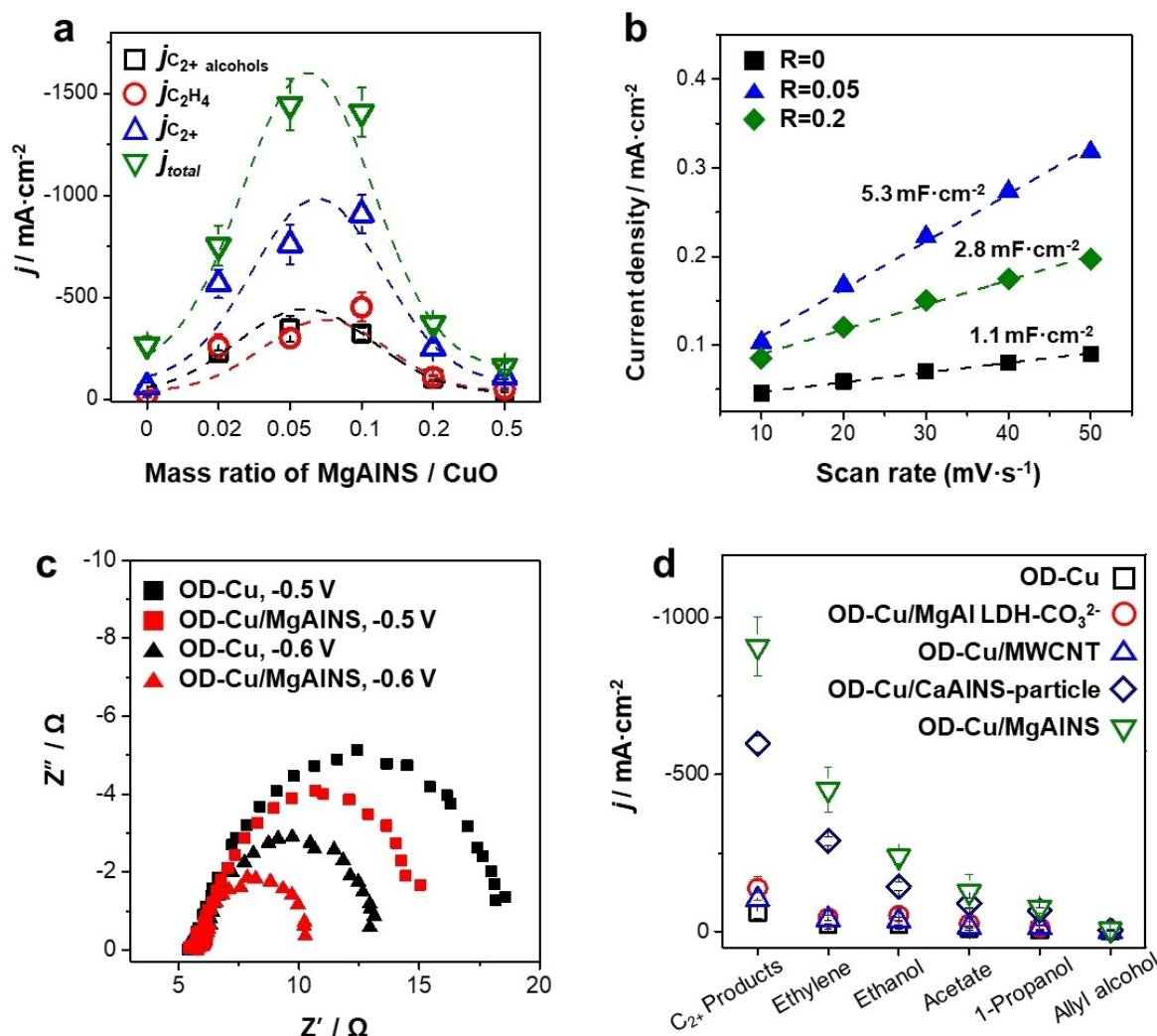
of  $\text{Cu}_j$  has been attributed to its porous structure that facilitated rapid gas transport across the electrode-electrolyte interface. Interestingly, after mixing with MgAlNS, the performance disparity between these two catalysts became considerably bridged. Specifically, the  $FE_{\text{C}_2+}$  of OD-Cu/MgAlNS and  $\text{Cu}_j/\text{MgAlNS}$  are now similar at 63–72%, and their  $j_{\text{C}_2+}$  range at  $-908$  to  $-1195$   $\text{mA}\cdot\text{cm}^{-2}$ .  $\text{Cu}_j$  mixed with MgAlNS also appeared less aggregated as compared to the pure  $\text{Cu}_j$  (Figure S13a–d). This finding suggests that the careful dispersion of the electrocatalyst particles on the cathode is a more critical factor in determining its CORR activity and selectivity, rather than the original catalyst particle morphologies.<sup>[23]</sup>

Finally, at  $-0.7$  V, the OD-Cu/MgAlNS catalyst could sustainably reduce, over 5 hr, CO to  $\text{C}_2+$  products with an

average  $FE_{\text{C}_2+}$  of 74% and  $j_{\text{C}_2+}$  of  $-1070$   $\text{mA}\cdot\text{cm}^{-2}$  (Figure S14). All in all, we demonstrate that OD-Cu supported on MgAlNS house-of-cards structures enabled larger CORR current densities and stable FEs to be obtained at high mass loadings and at more negative potentials.

#### Effect of MgAlNS on the CORR Performance of OD-Cu

The influence of the MgAlNS on the CORR performance of the OD-Cu was investigated. We first vary the amount of MgAlNS in the composite, while fixing the quantity of CuO to 2.91  $\text{mg}\cdot\text{cm}^{-2}$  (Figure 3a and Table S7). Six mixtures were prepared. The partial current density of the  $\text{C}_2+$  products formed during CORR at  $-0.7$  V increased dramatically



**Figure 3.** (a) Total current densities and partial current densities of  $C_{2+}$  products at  $-0.7$  V vs. RHE formed during CORR using OD-Cu (CuO loading  $2.91 \text{ mg cm}^{-2}$ ) mixed with different amounts of MgAlNS. The mass ratio or  $R$  is defined as the mass of MgAlNS loaded divided by that of CuO ( $2.91 \text{ mg cm}^{-2}$ ). (b) Double layer capacitance measurements of OD-Cu (CuO loading  $2.91 \text{ mg cm}^{-2}$ ) mixed with different amounts of MgAlNS. The double-layer capacitances of samples with  $R=0$ ,  $0.05$  and  $0.2$  are shown in the figure. The measurements are made in  $N_2$ -saturated  $1 \text{ M KOH}$  electrolyte. (c) Nyquist plots of OD-Cu and OD-Cu/MgAlNS at  $-0.5$  and  $-0.6$  V vs. RHE in  $CO$ -saturated  $1 \text{ M KOH}$  electrolyte, respectively. The frequency range was from  $10^5 \text{ Hz}$  to  $1 \text{ Hz}$ . (d) Partial current densities of  $C_{2+}$  products formed during CORR at  $-0.7$  V vs. RHE using OD-Cu, and OD-Cu mixed with MgAl LDH- $CO_3^{2-}$ , MWCNT, CaAlNS-particle and MgAlNS. The mass ratios of the CuO and supports are kept at  $10:1$ . CuO loading  $2.91 \text{ mg cm}^{-2}$ .

when a small amount of LDH nanosheet was added: from  $-61 \text{ mA cm}^{-2}$  when  $\frac{\text{Mass loading of MgAlNS}}{\text{Mass loading of CuO}} = R = \frac{0}{2.91} = 0$  to  $-568 \text{ mA cm}^{-2}$  when  $R=0.02$ . An optimized  $j_{C_{2+}}$  value of  $-908 \text{ mA cm}^{-2}$  could be achieved when the ratio of mass loadings of the MgAlNS to that of CuO was  $0.1$ . Unexpectedly, upon further increasing the MgAlNS loading ( $R=0.2$  and  $0.5$ ), the current density of  $j_{C_{2+}}$  decreased. We attribute this change to the aggregation of the LDH nanosheets into the LDH carbonate particles, as shown by XRD analysis (a peak at  $11.7^\circ$ ; Figure S15).<sup>[14,18,24]</sup> Consequently, the OD-Cu catalysts would be less dispersed/more agglomerated. Following this line of reasoning, we would then expect the electrochemically-active surface areas (ECSAs) of the six catalyst composites to vary in a ‘volcano’-like trend as the amount of LDH nanosheets added increases. We thus

measured their double layer capacitances (which are proportional to their ECSAs) after they were used for CORR. A positive correlation between the current densities of  $C_{2+}$  products and double layer capacitances of the catalyst composites was indeed observed (Figures 3b and S16).

Electrochemical impedance spectroscopy (EIS) of the OD-Cu and OD-Cu/MgAlNS in  $CO$ -purged  $1 \text{ M KOH}$  electrolyte further showed that the charge transfer resistances ( $R_{ct}$ ) of OD-Cu and OD-Cu/MgAlNS were similar at respectively  $13.7$  and  $9.7 \Omega$  at  $-0.5 \text{ V}$  ( $7.7$  and  $4.6 \Omega$  at  $-0.6 \text{ V}$ ) (Figure 3c). This confirms that the CORR charge transfer kinetics of the OD-Cu do not change considerably with the addition of the MgAlNS. These lines of evidences strongly suggest that the key role of the MgAlNS was to

optimally disperse the OD-Cu, thereby better exposing its catalytically-active sites to the CO feedstock.

### Effects of other supports

To show the efficacy of the MgAlNS house-of-cards scaffold in enhancing the CORR activity of OD-Cu, we compare the current densities of  $C_{2+}$  products formed using catalyst composites consisting of 2.91 mg cm<sup>-2</sup> CuO mixed with 0.29 mg cm<sup>-2</sup> MgAl LDH-CO<sub>3</sub><sup>2-</sup> particles, MWCNT or CaAl LDH nanosheets/particles (CaAlNS-particle) (Figures 3d, S17 and S18; Section S1.1). CO reduction was performed at -0.7 V in 1 M KOH electrolyte.

The  $j_{C_{2+}}$  exhibited by OD-Cu/MgAl LDH-CO<sub>3</sub><sup>2-</sup> and OD-Cu/MWCNTs were at -138 and -103 mA cm<sup>-2</sup>, which were  $\sim 2\times$  higher than that of pure OD-Cu (-61 mA cm<sup>-2</sup>), but  $\sim 7-9\times$  lower than that of OD-Cu/MgAlNS (-908 mA cm<sup>-2</sup>). We further note that the  $FE_{H_2}$  of OD-Cu/MgAl LDH-CO<sub>3</sub><sup>2-</sup> was 38 %, which was lower than that (73 %) of OD-Cu (Table S8). These results implied that the LDH particle support do aid the mass transport of CO gas within the OD-Cu catalysts layer. However, they do not disperse the OD-Cu as well as the MgAlNS ( $FE_{H_2}=34\%$ ), which thus account for their higher H<sub>2</sub> selectivity and lower  $j_{C_{2+}}$ . With the use of MWCNT, HER dominated with a  $FE$  of 72 % (Table S8).

The average  $j_{C_{2+}}$  exhibited by OD-Cu/CaAlNS-particle was at -598 mA cm<sup>-2</sup>, which was  $\sim 4-10\times$  higher than that of OD-Cu, OD-Cu/MgAl LDH-CO<sub>3</sub><sup>2-</sup> and OD-Cu/MWCNT, but  $\sim 1.5\times$  lower than that of OD-Cu/MgAlNS. We attribute this to the CaAl LDH-NO<sub>3</sub><sup>-</sup> particles not being entirely exfoliated into nanosheets. Thus, less house-of-cards structures could be formed (Figures S18a-b and S19). Consequently, while this support does disperse OD-Cu, it did not do so as efficaciously as the MgAlNS.

In a broader context, by using OD-Cu/MgAlNS composite, we have shown that CO could be reduced to  $C_{2+}$  products with a  $j_{C_{2+}}$  that is  $14\times$  higher than that of using unsupported OD-Cu (Figure 2a-b). The partial current density of  $C_{2+}$  alcohols could reach -369 mA cm<sup>-2</sup>. These figures-of-merit compare favourably against those exhibited by Cu catalysts mixed with other supports (Figure 3d), and also those of Cu nanorods supported on nitrogen-doped carbon quantum dots ( $j_{C_{2+}}$  alcohols of -147.8 mA cm<sup>-2</sup> during CO<sub>2</sub>RR at -0.9 V vs. RHE).<sup>[25]</sup> It is noteworthy that unlike many other supports, the MgAlNS scaffold is electrochemically inert and does not appear to alter the intrinsic catalytic activity of the OD-Cu. Its primary role is, instead, to promote CO gas flow through the OD-Cu catalyst layer. We thus believe that it can be applied as a general support for catalysts used in other (electro)catalytic reactions.

### Conclusion

We have shown that MgAlNS house-of-cards scaffolds can serve as suitable supports for OD-Cu catalysts for CORR. Their use allow the rate of CO percolation through the

catalyst layer to be enhanced, even when high mass loadings of catalysts and large overpotentials are applied. Consequently, CO reduction can be improved significantly, while H<sub>2</sub> evolution is minimized. Using this support-catalyst configuration, CO could be reduced to  $C_{2+}$  products with an average  $j_{C_{2+}}$  of -1251 mA cm<sup>-2</sup> at -0.7 V in 1 M KOH electrolyte. This  $j_{C_{2+}}$  figure-of-merit is  $14\times$  higher compared to that exhibited by OD-Cu alone. The MgAlNS also aided in the mechanical stability of the catalyst layer on the GDL. Overall, we believe that the development of facilely-prepared Cu catalysts mixed with a MgAlNS house-of-cards support is a significant step towards the realization of industrial-scale CO reduction to multi-carbon products.

### Experimental Section

Detailed experimental procedures can be found in Sections S1 and S3 of the Supporting Information.

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### Conflict of Interest

The authors declare no conflict of interest.

### Data Availability Statement

The data that support the findings of this study are available from the corresponding author upon reasonable request.

**Keywords:** CO Electroreduction • Copper • Electrocatalysts • Layered Double Hydroxide Nanosheet

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