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Chapter 29. Psychrometrics

Practice Problems

1.

A room contains air at 80°F (27°C) dry-bulb and 67°F (19°C) wet-bulb. The total pressure is 1 atm. Assuming a specific heat capacity for steam of 0.4 Btu/lbm/F, the specific heat of the room's atmosphere is

(A)

0.234 Btu/lbm-°F (0.979 kJ/kg·K)

(B)

0.237 Btu/lbm-°F (0.991 kJ/kg·K)

(C)

0.239 Btu/lbm-°F (0.999 kJ/kg·K)

(D)

 $0.242 \text{ Btu/lbm-}^{\circ}\text{F} (1.012 \text{ kJ/kg} \cdot \text{K})$

<u>2</u>.

 $1000~\rm ft^3/min~(0.5~m^3/s)$ of air at $50^{\circ}F~(10^{\circ}C)$ dry-bulb and 95% relative humidity are mixed with $1500~\rm ft^3/min~(0.75~m^3/s)$ of air at $76^{\circ}F~(24^{\circ}C)$ dry-bulb and 45% relative humidity. The specific humidity of the mixture is most nearly

(A)

0.008 lbm/lbm (0.008 kg/kg)

(B)

0.009 lbm/lbm (0.009 kg/kg)

(C)

0.010 lbm/lbm (0.010 kg/kg)

(D)

0.011 lbm/lbm (0.011 kg/kg)

<u>3</u>.

95°F (35°C) dry-bulb, 75°F (24°C) wet-bulb air passes through a cooling tower and leaves at 85°F (29°C) dry-bulb and 90% relative humidity. The change in moisture content per cubic foot (meter) of air is most nearly

(A)

 $1.8 \times 10^{-4} \text{ lbm/ft}^3 (2.7 \times 10^{-3} \text{ kg/m}^3)$

(B)

```
3.3 \times 10^{-4} \text{ lbm/ft}^3 (4.5 \times 10^{-3} \text{ kg/m}^3) (C)

6.7 \times 10^{-4} \text{ lbm/ft}^3 (9.9 \times 10^{-3} \text{ kg/m}^3) (D)

9.2 \times 10^{-4} \text{ lbm/ft}^3 (14 \times 10^{-3} \text{ kg/m}^3) 4.
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An air washer receives 1800 ft³/min (0.85 m³/s) of air at 70°F (21°C) and 40% relative humidity and discharges the air at 75% relative humidity. A recirculating water spray with a constant temperature of 50°F (10°C) is used. What mass of makeup water is required per minute?

```
(A)
0.127 lbm/min (0.00141 kg/s)
(B)
0.267 lbm/min (0.00296 kg/s)
(C)
0.374 lbm/min (0.00415 kg/s)
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0.961 lbm/min (0.01067 kg/s)

5.

(D)

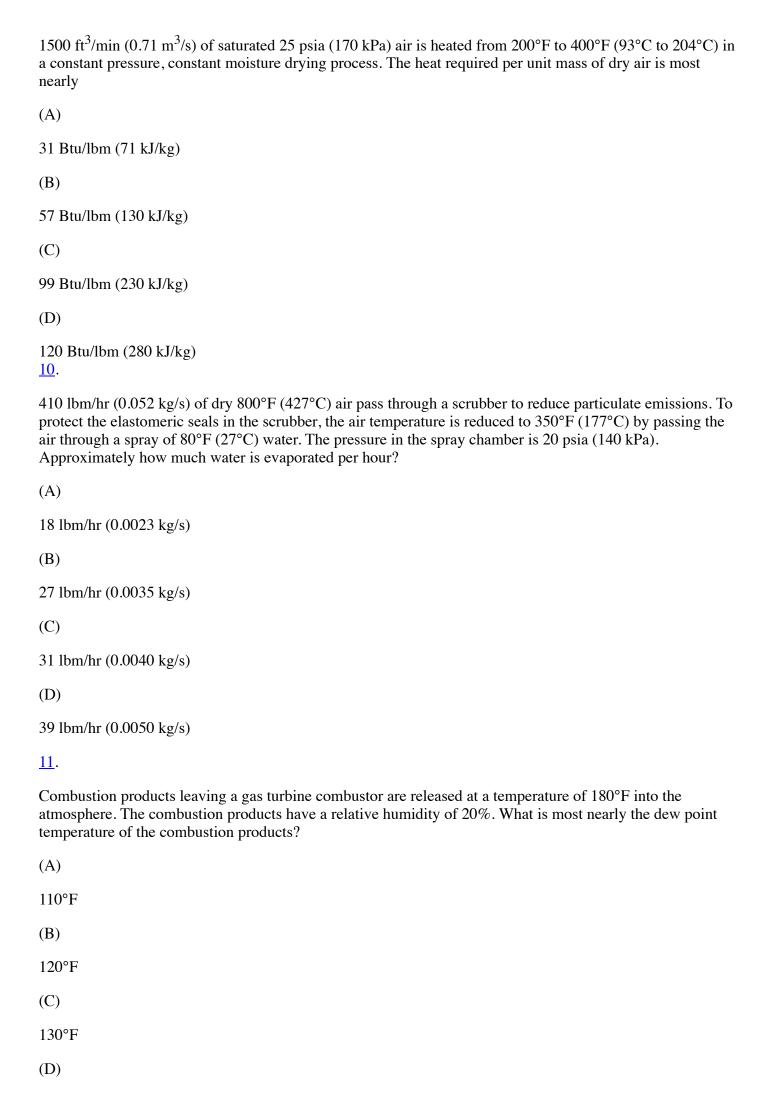
An air washer receives 1800 ft³/min (0.85 m³/s) of air. Air is received at 70°F (21°C) and 40% relative humidity and discharges at 75% relative humidity. The air washer recirculates a spray of saturated steam at atmospheric pressure. The mass of makeup water required is most nearly

```
(A)
0.801 lbm/min (0.0056 kg/s)
(B)
1.437 lbm/min (0.01005 kg/s)
(C)
1.907 lbm/min (0.01333 kg/s)
(D)
3.541 lbm/min (0.02476 kg/s)
6.
```

During performances, a theater experiences a sensible heat load of 500,000 Btu/hr (150 kW) and a moisture load of 175 lbm/hr (80 kg/h). Air enters the theater at 65°F (18°C) and 55% relative humidity and is removed when it reaches 75°F (24°C) or 60% relative humidity, whichever comes first. What is the relative humidity of the air leaving the theater?

(A)

```
38%
(B)
44%
(C)
58%
(D)
62%
7.
500 ft<sup>3</sup>/min (0.25 m<sup>3</sup>/s) of air at 80°F (27°C) dry-bulb and 70% relative humidity are removed from a room.
150 ft<sup>3</sup>/min (0.075 m<sup>3</sup>/s) pass through an air conditioner and leave saturated at 50°F (10°C). The remaining
350 ft<sup>3</sup>/min (0.175 m<sup>3</sup>/s) bypass the air conditioner and mix with the conditioned air at 1 atm. The heat load
(in tons) of the air conditioner is most nearly
(A)
0.90 ton
(B)
1.3 ton
(C)
2.4 tons
(D)
2.9 tons
<u>8</u>.
A dehumidifier takes 5000~{\rm ft^3/min} (2.36 m³/s) of air at 95^{\circ}{\rm F} (35°C) dry-bulb and 70\% relative humidity and
discharges it at 60°F (16°C) dry-bulb and 95% relative humidity. The dehumidifier uses a wet R-12
refrigeration cycle operating between 100°F (saturated) (38°C) and 50°F (10°C). Find the quantity of heat
removed from the air.
(A)
8345 Btu/min (143.0 kW)
(B)
8551 Btu/min (146.5 kW)
(C)
10,508 Btu/min (180.0 kW)
(D)
10,714 Btu/min (183.6 kW)
<u>9</u>.
```



Solutions

1.

Customary U.S. Solution

Locate the intersection of 80°F dry-bulb and 67°F wet-bulb on the psychrometric chart (see appendixMERM38A (also *NCEES Handbook* figure "Psychrometric Chart (U.S. Customary Units)"). Read the value of humidity and enthalpy.

$$\omega = 0.0112$$
 lbm moisture/lbm dry air $(0.011 \ {
m lbm/lbm})$ $h = 31.5 \ {
m Btu/lbm}$ dry air

 c_p is gravimetrically weighted. c_p for air is 0.240 Btu/lbm-°F, and c_p for steam is approximately 0.40 Btu/lbm-°F.

$$egin{aligned} G_{
m air} &= rac{1}{1+0.0112} = 0.989 \ G_{
m steam} &= rac{0.0112}{1+0.0112} = 0.011 \ c_{p,
m mixture} &= G_{
m air} \, c_{p,
m air} + G_{
m steam} \, c_{p,
m steam} \ &= (0.989) \left(0.240 \, rac{
m Btu}{
m lbm-\,^\circ F}
ight) \ &+ (0.011) \left(0.40 \, rac{
m Btu}{
m lbm-\,^\circ F}
ight) \ &= 0.242 \,
m Btu/lbm-\,^\circ F \end{aligned}$$

The answer is (D).

SI Solution

Locate the intersection of 27°C dry-bulb and 19°C wet-bulb on the psychrometric chart (see appendixMERM38B (also *NCEES Handbook* figure "Psychrometric Chart (SI Units)"). Read the value of humidity and enthalpy.

$$\omega = \frac{10.5 \; \frac{\mathrm{g}}{\mathrm{kg} \; \mathrm{dry \; air}}}{1000 \; \frac{\mathrm{g}}{\mathrm{kg}}} = 0.0105 \; \mathrm{kg/kg \; dry \; air}$$

$$(0.011 \; \mathrm{kg/kg})$$

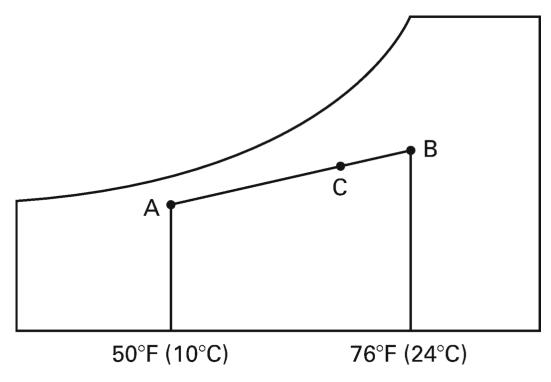
$$h = 53.9 \; \mathrm{kJ/kg \; dry \; air}$$

 c_p is gravimetrically weighted. c_p for air is 1.0048 kJ/kg·K, and c_p for steam is approximately 1.675 kJ/kg·K.

$$egin{aligned} G_{
m air} &= rac{1}{1+0.0105} = 0.990 \ G_{
m steam} &= rac{0.0105}{1+0.0105} = 0.010 \ c_{p,
m mixture} &= G_{
m air} c_{p,
m air} + G_{
m air} c_{p,
m steam} \ &= (0.990) \left(1.0048 \, rac{
m kJ}{
m kg\cdot K}
ight) \ &+ (0.010) \left(1.675 \, rac{
m kJ}{
m kg\cdot K}
ight) \ &= 1.0115 \,
m kJ/
m kg\cdot K \quad (1.012 \,
m kJ/
m kg\cdot K) \end{aligned}$$

The answer is (D).

Use the illustration shown for both the customary U.S. and SI solutions.



Customary U.S. Solution

Locate the two points on the psychrometric chart in appendixMERM38A (also *NCEES Handbook* figure "Psychrometric Chart (U.S. Customary Units)") and draw a line between them.

Reading from the chart (specific volumes),

$$v_{
m A}=13.0~{
m ft}^3/{
m lbm}$$
 $v_{
m B}=13.7~{
m ft}^3/{
m lbm}$

The density at each point is

$$ho_{
m A} = rac{1}{v_{
m A}} = rac{1}{13.0 \, rac{{
m ft}^3}{{
m lbm}}} = 0.0769 \, {
m lbm/ft}^3 \
ho_{
m B} = rac{1}{v_{
m B}} = rac{1}{13.7 \, rac{{
m ft}^3}{{
m lbm}}} = 0.0730 \, {
m lbm/ft}^3$$

As in NCEES Handbook: Conservation of Mass, the mass flow at each point is

$$\begin{split} \dot{m}_{\rm A} &= \rho_{\rm A} \dot{V}_{\rm A} = \left(0.0769 \; \frac{\rm lbm}{\rm ft^3}\right) \left(1000 \; \frac{\rm ft^3}{\rm min}\right) \\ &= 76.9 \; \rm lbm/min \\ \dot{m}_{\rm B} &= \rho_{\rm B} \dot{V}_{\rm B} = \left(0.0730 \; \frac{\rm lbm}{\rm ft^3}\right) \left(1500 \; \frac{\rm ft^3}{\rm min}\right) \\ &= 109.5 \; \rm lbm/min \end{split}$$

The gravimetric fraction of flow A is

$$rac{76.9 rac{ ext{lbm}}{ ext{min}}}{76.9 rac{ ext{lbm}}{ ext{min}} + 109.5 rac{ ext{lbm}}{ ext{min}}} = 0.413$$

Since the scales are all linear,

$$egin{aligned} 0.413 &= rac{T_{
m B} - T_{
m C}}{T_{
m B} - T_{
m A}} \ T_{
m C} &= T_{
m B} - (0.413) \, (T_{
m B} - T_{
m A}) \ &= 76\,{
m ^\circ F} - (0.413) \, (76\,{
m ^\circ F} - 50\,{
m ^\circ F}) \ &= 65.3\,{
m ^\circ F} \end{aligned}$$

$$\omega = rac{0.0082 ext{ lbm moisture/lbm dry air}}{(0.008 ext{ lbm/lbm})}$$

The answer is (A).

SI Solution

Locate the two points on the psychrometric chart in appendixMERM38B (also *NCEES Handbook* figure "Psychrometric Chart (SI Units)"), and draw a line between them.

Reading from the chart (specific volumes),

$$v_{
m A} = 0.813~{
m m}^3/{
m kg}~{
m dry}~{
m air}$$
 $v_{
m B} = 0.856~{
m m}^3/{
m kg}~{
m dry}~{
m air}$

The density at each point is

$$ho_{
m A} = rac{1}{v_{
m A}} = rac{1}{0.813 \, rac{{
m m}^3}{{
m kg}}} = 1.23 \, {
m kg/m}^3 \
ho_{
m B} = rac{1}{v_{
m B}} = rac{1}{0.856 \, rac{{
m m}^3}{{
m kg}}} = 1.17 \, {
m kg/m}^3 \
ho_{
m B} = rac{1}{v_{
m B}} = rac{1}{0.856 \, rac{{
m m}^3}{{
m kg}}} = 1.17 \, {
m kg/m}^3 \
ho_{
m B} = rac{1}{0.856 \, rac{{
m m}^3}{{
m kg}}} = 1.17 \, {
m kg/m}^3 \
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m B} = rac{1}{0.856 \, rac{{
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m kg}}} = 1.17 \, {
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m kg/m}^3} \
ho_{
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ho_{
m B} = 1.17 \, {
ho$$

As in NCEES Handbook: Conservation of Mass, the mass flow at each point is

$$egin{aligned} \dot{m}_{
m A} &=
ho_{
m A} \dot{V}_{
m A} = \left(1.23 \; rac{
m kg}{
m m^3}
ight) \left(0.5 \; rac{
m m^3}{
m s}
ight) = 0.615 \;
m kg/s \ \\ \dot{m}_{
m B} &=
ho_{
m B} \dot{V}_{
m B} = \left(1.17 \; rac{
m kg}{
m m^3}
ight) \left(0.75 \; rac{
m m^3}{
m s}
ight) = 0.878 \;
m kg/s \end{aligned}$$

The gravimetric fraction of flow A is

$$\frac{0.615 \frac{\text{kg}}{\text{s}}}{0.615 \frac{\text{kg}}{\text{s}} + 0.878 \frac{\text{kg}}{\text{s}}} = 0.412$$

Since the scales are linear,

$$egin{aligned} 0.412 &= rac{T_{
m B} - T_{
m C}}{T_{
m B} - T_{
m A}} \ T_{
m C} &= T_{
m B} - (0.412) \, (T_{
m B} - T_{
m A}) \ &= 24\,{
m ^{\circ} C} - (0.412) \, (24\,{
m ^{\circ} C} - 10\,{
m ^{\circ} C}) \ &= 18.2\,{
m ^{\circ} C} \ \omega &= rac{8.0}{rac{
m g}{
m kg \, dry \, air}} \ 1000 \, rac{
m g}{
m kg} \ &= rac{0.008 \,
m kg \, moisture/kg \, dry \, air}{(0.008 \,
m kg/kg)} \end{aligned}$$

The answer is (A). 3.

Customary U.S. Solution

Refer to the psychrometric chart (see appendixMERM38A and *NCEES Handbook* figure "Psychrometric Chart (U.S. Customary Units)").

At point 1, properties of air at $T_{\rm db} = 95$ °F and $T_{\rm wb} = 75$ °F are

 $\omega_1 = 0.0141 \; \mathrm{lbm} \; \mathrm{moisture/lbm} \; \mathrm{air}$

 $h_1=38.4~\mathrm{Btu/lbm~air}$

 $v_1=14.3~{
m ft}^3/{
m lbm~air}$

At point 2, properties of air at $T_{\rm db}$ = 85°F and 90% relative humidity are

 $\omega_2\,=0.0237$ lbm moisture/lbm air

 $h_2 = 46.6 \; \mathrm{Btu/lbm} \; \mathrm{air}$

The enthalpy change is

$$egin{aligned} rac{h_2-h_1}{v_1} &= rac{46.6}{ ext{lbm air}} rac{ ext{Btu}}{ ext{lbm air}} - 38.4 rac{ ext{Btu}}{ ext{lbm air}} \ &= 14.3 rac{ ext{ft}^3}{ ext{lbm air}} \ &= 0.573 ext{ Btu/ft}^3 ext{ air} \end{aligned}$$

The moisture added is

$$\frac{\omega_2-\omega_1}{\upsilon_1} = \frac{0.0237 \, \frac{\mathrm{lbm \; moisture}}{\mathrm{lbm \; air}}}{-0.0141 \, \frac{\mathrm{lbm \; moisture}}{\mathrm{lbm \; air}}}$$

$$= \frac{14.3 \, \frac{\mathrm{ft}^3}{\mathrm{lbm \; air}}}{(6.7 \times 10^{-4} \, \mathrm{lbm/ft}^3 \, \mathrm{air})}$$

The answer is (C).

SI Solution

Refer to the psychrometric chart (see appendixMERM38B and *NCEES Handbook* figure "Psychrometric Chart (SI Units)").

At point 1, properties of air at $T_{\rm db} = 35^{\circ}{\rm C}$ and $T_{\rm wb} = 24^{\circ}{\rm C}$ are

 $\omega_1 = 14.3 \ \mathrm{g/kg \ air}$

 $h_1=71.8~{\rm kJ/kg~air}$

 $v_1=0.8893~\mathrm{m}^3/\mathrm{kg}$ air

At point 2, properties of air at $T_{\rm db}$ = 29°C and 90% relative humidity are

$$\omega_2\,=23.1~{
m g/kg}$$
 air

$$h_2 = 88 \; \mathrm{kJ/kg \; air}$$

The enthalpy change is

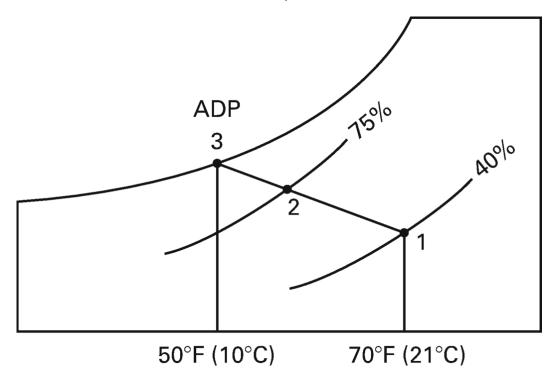
$$\frac{h_2 - h_1}{v_1} = \frac{88 \frac{\text{kJ}}{\text{kg air}} - 71.8 \frac{\text{kJ}}{\text{kg air}}}{0.8893 \frac{\text{m}^3}{\text{kg air}}}$$
$$= 18.2 \text{kJ/m}^3 \text{ air}$$

The moisture added is

$$egin{aligned} rac{\omega_2 - \omega_1}{v_1} &= rac{23.1 \, rac{
m g}{
m kg \, air} - 14.3 \, rac{
m g}{
m kg \, air}}{\left(0.8893 \, rac{
m m^3}{
m kg \, air}
ight) \left(1000 \, rac{
m g}{
m kg}
ight)} \ &= 9.9 imes 10^{-3} \,
m kg/m^3 \end{aligned}$$

The answer is (C). $\underline{4}$.

Use the illustration shown for both the customary U.S. and SI solutions.



Customary U.S. Solution

Refer to the psychrometric chart (see appendixMERM38A and *NCEES Handbook* figure "Psychrometric Chart (U.S. Customary Units)").

At point 1, properties of air at $T_{\rm db} = 70^{\circ} \rm F$ and $\phi = 40\%$ are

 $h_1=23.6~\mathrm{Btu/lbm~air}$

 $\omega_1\,=0.00625$ lbm moisture/lbm air

 $v_1=13.48~{
m ft}^3/{
m lbm~air}$

The mass flow rate of incoming air is

$$\dot{m}_{a,1} = rac{\dot{V}_1}{v_1} = rac{1800 \; rac{ ext{ft}^3}{ ext{min}}}{13.48 \; rac{ ext{ft}^3}{ ext{lbm air}}} = 133.53 \; ext{lbm air/min}$$

Locate point 1 on the psychrometric chart.

Notice that the temperature of the recirculating water is constant but not equal to the air's entering wet-bulb temperature. Therefore, this is not an adiabatic process.

Locate point 3 as 50°F saturated condition (water being sprayed) on the psychrometric chart.

Draw a line from point 1 to point 3. The intersection of this line with 75% relative humidity defines point 2 as

$$h_2=21.4~{
m Btu/lbm~air}$$
 $\omega_2=0.0072~{
m lbm~moisture/lbm~air}$ $T_{
m db,2}=56\,{
m ^\circ F}$ $T_{
m wb,2}=51.8\,{
m ^\circ F}$

The moisture (water) added is

$$egin{aligned} \dot{m}_w &= \dot{m}_{a,1} \left(\omega_2 - \omega_1
ight) \ &= \left(133.53 \, rac{ ext{lbm air}}{ ext{min}}
ight) \ & imes \left(0.0072 \, rac{ ext{lbm moisture}}{ ext{lbm air}}
ight. \ &= 0.127 \, ext{lbm/min} \end{aligned}$$

The answer is (A).

SI Solution

Refer to the psychrometric chart (see appendixMERM38B and *NCEES Handbook* figure "Psychrometric Chart (SI Units)").

At point 1, properties of air at $T_{db} = 21^{\circ}\text{C}$ and $\phi = 40\%$ are

$$h_1=36.75~\mathrm{kJ/kg}$$
 air $\omega_1=6.2~\mathrm{g}$ moisture/kg air $v_1=0.842~\mathrm{m}^3/\mathrm{kg}$ air

The mass flow rate of incoming air is

$$\dot{m}_{a,1} = rac{\dot{V}_1}{v_1} = rac{0.85 rac{ ext{m}^3}{ ext{s}}}{0.842 rac{ ext{m}^3}{ ext{kg air}}} = 1.010 ext{ kg air/s}$$

Locate point 1 on the psychrometric chart.

Notice that the temperature of the recirculating water is constant but not equal to the air's entering wet-bulb temperature. Therefore, this is not an adiabatic process.

Locate point 3 as 10°C saturated condition (water being sprayed) on the psychrometric chart.

Draw a line from point 1 to point 3. The intersection of this line with 75% relative humidity defines point 2 as

$$h_2=34.1~ ext{kJ/kg}$$
 air $\omega_2=7.6~ ext{g}$ moisture/kg air $T_{ ext{db},2}=14.7\,^{\circ} ext{C}$ $T_{ ext{wb},2}=12.0\,^{\circ} ext{C}$

The water added is

$$egin{aligned} \dot{m}_w &= \dot{m}_{a,1} \left(\omega_2 - \omega_1
ight) \ &= rac{\left(1.010 \, rac{ ext{kg air}}{ ext{s}}
ight) \left(7.6 \, rac{ ext{g moisture}}{ ext{kg air}}
ight)}{-6.2 \, rac{ ext{g moisture}}{ ext{kg air}}
ight)} \ &= rac{1000 \, rac{ ext{g}}{ ext{kg}}}{= 0.00141 \, ext{kg/s}} \end{aligned}$$

The answer is (A). 5.

Customary U.S. Solution

(See the SI solution for a trial-and-error solution procedure.)

From appendixMERM38A (also NCEES Handbook figure "Psychrometric Chart (U.S. Customary Units)"),

 $\omega_1 = 0.00623 \ \mathrm{lbm} \ \mathrm{moisture/lbm} \ \mathrm{air}$

 $h_1=23.6~\mathrm{Btu/lbm~air}$

 $\dot{m}_{a,1}=133.53~\mathrm{lbm~air/min}$

From the steam table in appendixMERM35E (also *NCEES Handbook* table "Saturated Steam (U.S. Units)—Temperature Table"), for 1 atm steam, $h_{\text{steam}} = 1150.3 \text{ Btu/lbm}$.

From the conservation of energy equation,

$$\dot{m}_{a,1}h_1 + \dot{m}_{
m steam}h_{
m steam} = \dot{m}_{a,1}h_2$$

$$egin{aligned} \left(133.53 \ rac{ ext{lbm air}}{ ext{min}}
ight) \left(23.6 \ rac{ ext{Btu}}{ ext{lbm air}}
ight) \ + \dot{m}_{ ext{steam}} \left(1150.3 \ rac{ ext{Btu}}{ ext{lbm}}
ight) = \left(133.53 \ rac{ ext{lbm air}}{ ext{min}}
ight) h_2 \quad ext{[Eq. 1]} \end{aligned}$$

Solve for $\dot{m}_{\rm steam}$.

$$\dot{m}_{\text{steam}} = 0.1161h_2 - 2.740$$
 [Eq. 3]

From a conservation of mass for the water,

$$\dot{m}_{a,1}\omega_1+\dot{m}_{
m steam}=\dot{m}_{a,2}\omega_2$$

$$egin{aligned} \left(133.53 \ rac{ ext{lbm air}}{ ext{min}}
ight) \left(0.00623 \ rac{ ext{lbm moisture}}{ ext{lbm air}}
ight) \ + \dot{m}_{ ext{steam}} = \left(133.53 \ rac{ ext{lbm air}}{ ext{min}}
ight) \omega_2 \quad ext{[Eq. 2]} \end{aligned}$$

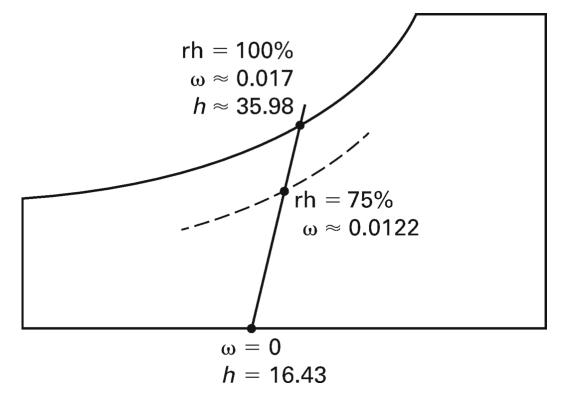
Solve for $\dot{m}_{\rm steam}$.

$$\dot{m}_{\rm steam} = 133.53\omega_2 - 0.8319$$
 [Eq. 4]

Equate Eq. 3 and Eq. 4.

$$0.1161h_2 - 2.740 = 133.53\omega_2 - 0.8319 \ h_2 = 1150.1\omega_2 + 16.43$$

Plot this line on the psychrometric chart, and determine properties where it crosses the 75% relative humidity line.



At 75% relative humidity, from the psychrometric chart,

 $\omega_2\,=0.0122$ lbm moisture/lbm air

 $h_2 = 30.5 \, \mathrm{Btu/lbm}$

 $T_{
m db} = 72\,{}^{\circ}{
m F}$

 $T_{
m wb} = 66\,{}^{\circ}{
m F}$

The mass flow rate is

$$\dot{m}_{
m steam} = (0.1161) \left(30.5 \ rac{
m Btu}{
m lbm}
ight) - 2.740 = \ 0.801 \
m lbm/min$$

The answer is (A).

SI Solution

(See the customary U.S. solution for a graphical method.)

As in NCEES Handbook figure "Psychrometric Chart (SI Units),"

 $\omega_1 = 6.2 \text{ g moisture/kg air}$

 $h_1=36.75~\mathrm{kJ/kg~air}$

 $\dot{m}_{a,1} = 1.010~\mathrm{kg~air/s}$

From the steam table in appendixMERM35F (also *NCEES Handbook* table "Saturated Steam (SI Units)—Temperature Table"), for 1 atm steam, $h_{\text{steam}} = 2675.4 \text{ kJ/kg}$.

From equationMERM38033, the conservation of energy equation,

$$egin{align*} \dot{m}_{a,1}h_1 + \dot{m}_{
m steam}h_{
m steam} &= \dot{m}_{a,1}h_2 \ igg(1.010~rac{
m kg~air}{
m s}igg) \left(36.75~rac{
m kJ}{
m kg~air}
ight) \ &+ \dot{m}_{
m steam} \left(2675.4~rac{
m kJ}{
m kg}
ight) = \left(1.010~rac{
m kg~air}{
m s}
ight)h_2 \quad ext{[Eq. 1]} \end{aligned}$$

From equationMERM38034, a conservation of mass for the water,

$$egin{align*} \dot{m}_{a,1} \omega_1 + \dot{m}_{ ext{steam}} &= \dot{m}_{a,2} \omega_2 \ & rac{\left(1.010 \; rac{ ext{kg air}}{ ext{s}}
ight) \left(6.2 \; rac{ ext{g moisture}}{ ext{kg air}}
ight)}{\left(1000 \; rac{ ext{kg}}{ ext{g}}
ight)} \ & + \dot{m}_{ ext{steam}} &= \left(1.010 \; rac{ ext{kg air}}{ ext{s}}
ight) \omega_2 \quad ext{[Eq. 2]} \end{aligned}$$

Since no single relationship exists between ω_2 , $\dot{m}_{\rm steam}$, and h_2 , a trial-and-error solution can be used. Once $\dot{m}_{\rm steam}$ is selected, ω_2 and h_2 can be found from Eq. 1 and Eq. 2 as

$$h_2 = 36.75 + 2648.9 \dot{m}_{
m steam} \ \omega_2 = 0.0062 + 0.99 \dot{m}_{
m steam}$$

Once h_2 and ω_2 are known, the relative humidity can be determined from the psychrometric chart. Continue the process until a relative humidity of 75% is achieved.

$$\begin{array}{cccc} \dot{m}_{\rm steam} & \omega_2 & h_2 & \phi_2 \\ \left(\frac{\rm kg}{\rm s}\right) & \left(\frac{\rm kg\ moisture}{\rm kg\ air}\right) & \left(\frac{\rm kJ}{\rm kg\ air}\right) & (\%) \\ 0.005 & 0.0112 & 49.99 & 69.5 \\ 0.0055 & 0.0116 & 51.32 & 74.5 \\ 0.0056 & 0.0117 & 51.58 & 75.0 \end{array}$$

$$egin{aligned} \dot{m}_{
m steam} &= 0.0056 \
m kg/s \ & \omega_2 = \left(0.0117 \ rac{
m kg \ moisture}{
m kg \ air}
ight) \left(1000 \ rac{
m g}{
m kg}
ight) \ &= 11.7 \
m g \ moisture/kg \ air \ & T_{
m db} = 21.3 \
m C \ & T_{
m wb} = 18.2 \
m C \end{aligned}$$

The answer is (A). $\underline{6}$.

Customary U.S. Solution

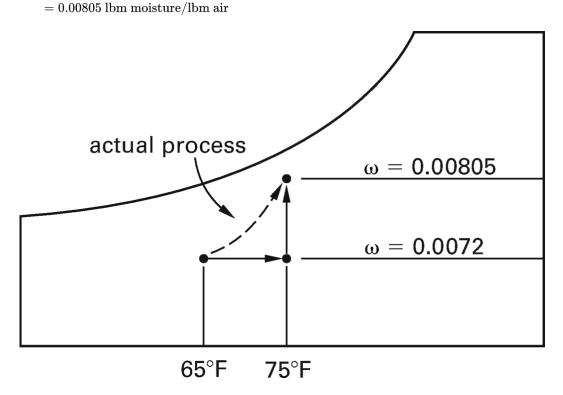
From the psychrometric chart (see appendixMERM38A and *NCEES Handbook* figure "Psychrometric Chart (U.S. Customary Units)"), for incoming air at 65°F and 55% relative humidity, $\omega_1 = 0.0072$ lbm moisture/lbm air.

With sensible heating as a limiting factor, calculate the mass flow rate of air entering the theater from equationMERM38025 (ventilation rate).

$$egin{aligned} \dot{q} &= \dot{m}_a \left(c_{p, ext{air}} + \omega c_{p, ext{moisture}}
ight) \left(T_2 - T_1
ight) \ 500,\!000 \, rac{ ext{Btu}}{ ext{hr}} &= \dot{m}_a \ & \left(0.240 \, rac{ ext{Btu}}{ ext{lbm-°F}}
ight. \ & \left(0.0072 \, rac{ ext{lbm moisture}}{ ext{lbm air}}
ight. \ & \left(0.444 \, rac{ ext{Btu}}{ ext{lbm-°F}}
ight) \ & ext{} imes \left(75\, {
m ^{\circ}F} - 65\, {
m ^{\circ}F}
ight) \ & \dot{m}_a = 2.056 imes 10^5 \, ext{lbm air/hr} \end{aligned}$$

Assume that this air absorbs all the moisture. Then, the final humidity ratio is given by

$$egin{align} \dot{m}_w &= \dot{m}_a \left(\omega_2 - \omega_1
ight) \ \omega_2 &= \left(rac{\dot{m}_w}{\dot{m}_a}
ight) + \omega_1 \ &= rac{175}{rac{ ext{lbm moisture}}{ ext{hr}}} {2.056 imes 10^5} rac{ ext{lbm air}}{ ext{hr}} + 0.0072 rac{ ext{lbm moisture}}{ ext{lbm air}} \ \end{aligned}$$



The final conditions are

$$T_{
m db} = 75\,{
m ^\circ F} \quad {
m [given]} \ \omega_2 \ = 0.00805 \ {
m lbm \ moisture/lbm \ air}$$

From the psychrometric chart (see appendixMERM38A and *NCEES Handbook* figure "Psychrometric Chart (U.S. Customary Units)"), the relative humidity is 44%. This is below 60%.

The answer is (B).

SI Solution

From the psychrometric chart (see appendixMERM38B and *NCEES Handbook* figure "Psychrometric Chart (SI Units)"), for incoming air at 18°C and 55% relative humidity, $\omega_1 = 7.1$ g moisture/kg air.

With sensible heating as a limiting factor, calculate the mass flow rate of air entering the theater from equationMERM38025 (ventilation rate).

$$\dot{q}=\dot{m}_a\left(c_{p,\mathrm{air}}+\omega c_{p,\mathrm{moisture}}
ight)\left(T_2-T_1
ight) \ \left(150\,\mathrm{kW}
ight) \ imes \left(1.005\,rac{\mathrm{kJ}}{\mathrm{kg}\cdot{}^\circ\mathrm{C}}
ight)\left(1000\,rac{\mathrm{J}}{\mathrm{kJ}}
ight) \ +\left(1.805\,rac{\mathrm{kJ}}{\mathrm{kg}\cdot{}^\circ\mathrm{C}}
ight)\left(1000\,rac{\mathrm{J}}{\mathrm{kJ}}
ight) \ imes \left(\frac{7.1\,rac{\mathrm{g\ moisture}}{\mathrm{kg\ air}}}{1000\,rac{\mathrm{g}}{\mathrm{kg}}}
ight) \ imes (24\,{}^\circ\mathrm{C}-18\,{}^\circ\mathrm{C}) \ \dot{m}_a=24.56\,\mathrm{kg/s}$$

Assume that this air absorbs all the moisture. Then, the final humidity ratio is given by

$$egin{align} \dot{m}_w &= \dot{m}_a \left(\omega_2 - \omega_1
ight) \ \omega_2 &= rac{\dot{m}_w}{\dot{m}_a} + \omega_1 \ &= rac{80 \; rac{\mathrm{kg}}{\mathrm{h}}}{\left(24.56 \; rac{\mathrm{kg}}{\mathrm{s}}
ight) \left(3600 \; rac{\mathrm{s}}{\mathrm{h}}
ight)} + rac{7.0 \; rac{\mathrm{g \; moisture}}{\mathrm{kg \; air}}}{1000 \; rac{\mathrm{g}}{\mathrm{kg}}} \ &= 0.00790 \; \mathrm{kg \; moisture/kg \; air} \ \end{split}$$

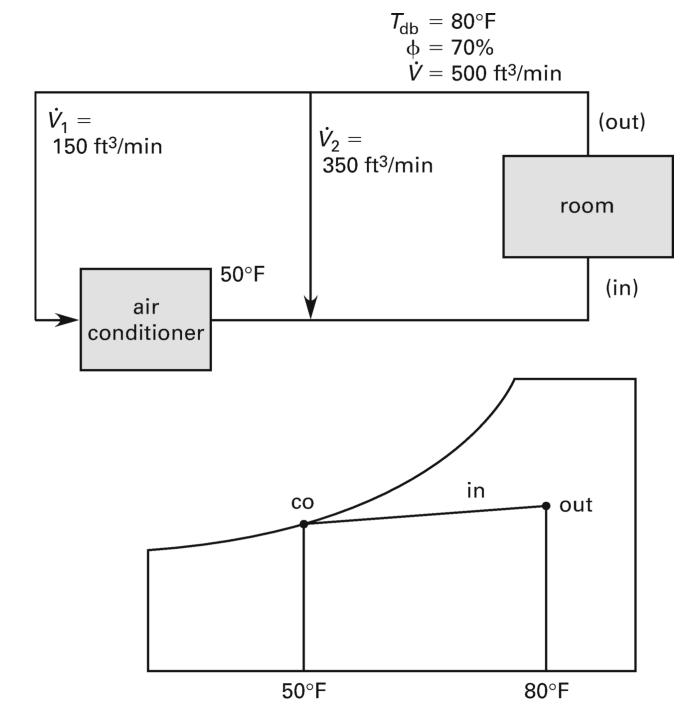
The final conditions are

$$\begin{split} T_{\rm db} &= 24\,^{\circ}{\rm C} \\ \omega_2 &= \left(0.00790~\frac{\rm kg~moisture}{\rm kg~air}\right) \, \left(1000~\frac{\rm g}{\rm kg}\right) \\ &= 7.9~{\rm g~moisture/kg~air} \end{split}$$

From the psychrometric chart (see *NCEES Handbook* figure "Psychrometric Chart (SI Units)"), the relative humidity is 44%. This is below 60%.

The answer is (B). $\underline{7}$.

Use the illustration shown for both customary U.S. and SI solutions.



Customary U.S. Solution

Locate point "out" ($T_{\rm db}$ = 80°F and ϕ = 70%) and point "co" (saturated at 50°F) on the psychrometric chart. At point "out" from appendixMERM38A (also *NCEES Handbook* figure "Psychrometric Chart (U.S. Customary Units)"),

$$v_{
m out} = 13.95~{
m ft}^3/{
m lbm~air} \ h_{
m out} = 36.2~{
m Btu/lbm~air}$$

At point "co," $h_{co} = 20.3 \text{ Btu/lbm air.}$

The air conditioner capacity is given by

$$egin{aligned} \dot{Q} &= \dot{m}_{
m air} \ (h_{t,2} - h_{t,1}) = \dot{m}_1 \ (h_{
m out} - h_{
m co}) \ &= \left(10.75 \ rac{
m lbm \ air}{
m min}
ight) \left(36.2 \ rac{
m Btu}{
m lbm \ air} - 20.3 \ rac{
m Btu}{
m lbm \ air}
ight) \ & imes \left(rac{1 \
m ton}{200 \ rac{
m Btu}{
m min}}
ight) \ &= 0.85 \
m ton \quad (0.90 \
m ton) \end{aligned}$$

The answer is (A).

SI Solution

Locate point "out" ($T_{\rm db} = 27$ °C, $\phi = 70\%$) and point "co" (saturated at 10°C) on the psychrometric chart. At point "out" from appendixMERM38B (also *NCEES Handbook* figure "Psychrometric Chart (SI Units)"),

$$v_{
m out} = 0.872~{
m m}^3/{
m kg~air}$$
 $h_{
m out} = 67.3~{
m kJ/kg~air}$

At point "co" from appendixMERM38B (also *NCEES Handbook* figure "Psychrometric Chart (SI Units)"), $h_{co} = 29.26 \text{ kJ/kg air.}$

As in NCEES Handbook: Conservation of Mass, at mass flow rate through the air conditioner,

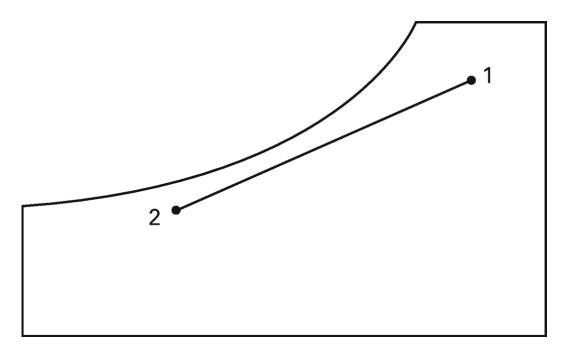
$$\dot{m}_1 = rac{\dot{V}_1}{v} = rac{0.075 rac{ ext{m}^3}{ ext{s}}}{0.872 rac{ ext{m}^3}{ ext{kg air}}} = 0.0860 ext{ kg air/s}$$

The air conditioner capacity is given by

$$egin{aligned} \dot{Q} &= \dot{m}_{
m air} \ (h_{t,2} - h_{t,1}) = \dot{m}_1 \ (h_{
m out} - h_{
m co}) \ &= \left(0.0860 \ rac{
m kg \ air}{
m s}
ight) \left(67.3 \ rac{
m kJ}{
m kg \ air} - 29.26 \ rac{
m kJ}{
m kg \ air}
ight) \ & imes \left(0.2843 \ rac{
m ton}{
m kW}
ight) \ &= 0.93 \
m ton \ \ \ (0.90 \
m ton) \end{aligned}$$

The answer is (A).

Use the illustration shown for both customary U.S. and SI solutions.



Customary U.S. Solution

At point 1, from the psychrometric chart (see appendixMERM38A and *NCEES Handbook* figure "Psychrometric Chart (U.S. Customary Units)") at $T_{\rm db} = 95^{\circ}$ F and $\phi = 70\%$,

 $h_1 = 50.7 \, \mathrm{Btu/lbm} \ \mathrm{air}$

 $v_1 = 14.56 \; {\rm ft}^3/{\rm lbm \; air}$

 $\omega_1\,=0.0253\;\mathrm{lbm\;water/lbm\;air}$

At point 2, from the psychrometric chart (see appendixMERM38A and *NCEES Handbook* figure "Psychrometric Chart (U.S. Customary Units)") at $T_{\rm db} = 60^{\circ}$ F and $\phi = 95\%$,

 $h_2 = 25.8 \, \mathrm{Btu/lbm}$ air

 $\omega_2\,=0.0105\,\mathrm{lbm}\;\mathrm{water/lbm}\;\mathrm{air}$

As in NCEES Handbook: Conservation of Mass, the air mass flow rate is

$$\dot{m}_a=rac{\dot{V}}{v_1}=rac{5000 \; rac{ ext{ft}^3}{ ext{min}}}{14.56 \; rac{ ext{ft}^3}{ ext{lbm air}}}=343.4 \; ext{lbm air/min}$$

From equationMERM38027, the quantity of heat removed is

$$egin{aligned} \dot{q} &= \dot{m}_a \left(h_1 - h_2
ight) \ &= \left(343.4 \, rac{ ext{lbm air}}{ ext{min}}
ight) \left(50.7 \, rac{ ext{Btu}}{ ext{lbm air}} - 25.8 \, rac{ ext{Btu}}{ ext{lbm air}}
ight) \ &= 8551 \, ext{Btu/min} \end{aligned}$$

The answer is (B).

SI Solution

At point 1, from the psychrometric chart (see appendixMERM38B and *NCEES Handbook* figure "Psychrometric Chart (SI Units)") at $T_{\rm db} = 35$ °C and $\phi = 70\%$,

$$\begin{split} h_1 &= 99.9 \text{ kJ/kg air} \\ v_1 &= 0.91 \text{ m}^3/\text{kg air} \\ \omega_1 &= \frac{25.3 \frac{\text{g moisture}}{\text{kg air}}}{1000 \frac{\text{g}}{\text{kg}}} = 0.0253 \text{ kg moisture/kg air} \end{split}$$

At point 2, from the psychrometric chart (see appendixMERM38B and *NCEES Handbook* figure "Psychrometric Chart (SI Units)") at $T_{\rm db} = 16$ °C and $\phi = 95\%$,

$$h_2=43.4~{
m kJ/kg~air} \ \omega_2=rac{10.8~rac{{
m g~moisture}}{{
m kg~air}}}{1000~rac{{
m g}}{{
m kg}}}=0.0108~{
m kg~moisture/kg~air}$$

As in NCEES Handbook: Conservation of Mass, the air mass flow rate is

$$\dot{m}_a = rac{\dot{V}_1}{v_1} = rac{\dot{V}_1}{v_{
m out}} = rac{2.36 rac{
m m^3}{
m s}}{0.91 rac{
m m^3}{
m kg~air}} = 2.593 \, {
m kg~air/s}$$

From equationMERM38027, the quantity of heat removed is

$$egin{aligned} \dot{q} &= \dot{m}_a \left(h_1 - h_2
ight) \ &= \left(2.593 \, rac{\mathrm{kg \, air}}{\mathrm{s}}
ight) \left(99.9 \, rac{\mathrm{kJ}}{\mathrm{kg \, air}} - 43.4 \, rac{\mathrm{kJ}}{\mathrm{kg \, air}}
ight) \ &= 146.5 \, \mathrm{kW} \end{aligned}$$

The answer is (B). 9.

Customary U.S. Solution

The saturation pressure at 200°F from appendixMERM24A (also *NCEES Handbook* table "Saturated Steam (U.S. Units)—Temperature Table"), is $p_{\text{sat},1} = 11.538$ psia.

Since air is saturated (100% relative humidity), the water vapor pressure is equal to the saturation pressure.

$$p_{w,1} = p_{\text{sat},1} = 11.538 \text{ psia}$$

The partial pressure of the air is

$$p_{a,1} = p_1 - p_{w,1} = 25 \; \mathrm{psia} - 11.538 \; \mathrm{psia}$$
 = 13.462 psia

Use equationMERM38007 (also NCEES Handbook: Air-Water Systems) to determine the humidity ratio.

$$\omega = 0.622 \left(\frac{p_{w,1}}{p_{a.1}}\right) = (0.622) \left(\frac{11.538 \; \mathrm{psia}}{13.462 \; \mathrm{psia}}\right) = 0.533$$

Since it is a constant pressure, constant moisture drying process, mole fractions and partial pressures do not change.

$$p_{w,2} = p_{w,1} = 11.538 \text{ psia}$$

The saturation pressure at 400°F from appendixMERM24A (also *NCEES Handbook* table "Saturated Steam (U.S. Units)—Temperature Table") is $p_{\text{sat},2} = 247.3$ psia.

The relative humidity at state 2 is

$$\phi_2 = \frac{p_{w,2}}{p_{\mathrm{sat.2}}} = \frac{11.538 \; \mathrm{psia}}{247.3 \; \mathrm{psia}} = 0.0467$$

Although the volume may change, the mass does not. The specific humidity remains constant.

$$\omega_2 = \omega_1 = 0.533$$
 lbm water/lbm air

The heat required consists of two parts.

As in NCEES Handbook table "Conversion Table for Temperature Units," the absolute temperatures are

$$T_1 = 200\,\mathrm{^\circ F} + 460\,\mathrm{^\circ} = 660\,\mathrm{^\circ R}$$

 $T_2 = 400\,\mathrm{^\circ F} + 460\,\mathrm{^\circ} = 860\,\mathrm{^\circ R}$

As in *NCEES Handbook:* Temperature-Dependent Properties of Air (U.S. Customary Units), the heat capacity is 0.2424 Btu/lbm-°F. The heat absorbed by air is

$$egin{array}{ll} q_1 &= h_2 - h_1 = c_p \, (T_2 - T_1) \ &= \left(0.2424 \, rac{ ext{Btu}}{ ext{lbm-}^{\circ} ext{F}}
ight) (860\,^{\circ} ext{R} - 660\,^{\circ} ext{R}) \ &= 48.48 \, ext{Btu/lbm} \, ext{dry air} \end{array}$$

From the Mollier diagram (also *NCEES Handbook* figure "Temperature-Entropy (T-S) Diagram (U.S. Customary Units)"), for water, h_1 at 200°F and 11.529 psia is 1146 Btu/lbm (almost saturated).

Follow a constant 11.529 psia pressure curve up to 400°F.

$$h_2 = 1240~\mathrm{Btu/lbm}$$

The heat absorbed by the steam is

$$q_2 = \omega (h_2 - h_1)$$

$$= \left(0.532 \frac{\text{lbm water}}{\text{lbm air}}\right) \left(1240 \frac{\text{Btu}}{\text{lbm}} - 1146 \frac{\text{Btu}}{\text{lbm}}\right)$$

$$= 50.01 \text{ Btu/lbm air}$$

The total heat absorbed is

$$\begin{split} q_{\rm total} &= q_1 + q_2 = 48.48 \, \frac{\rm Btu}{\rm lbm \, air} + 50.01 \, \frac{\rm Btu}{\rm lbm \, air} \\ &= 98.49 \, \rm Btu/lbm \, air \quad (99 \, \rm Btu/lbm) \end{split}$$

The answer is (C).

SI Solution

From appendixMERM24N (also *NCEES Handbook* table "Saturated Steam (SI Units)—Temperature Table"), the saturation pressure at 93°C is

$$p_{{
m sat},1} = (0.7884~{
m bar}) \left(100~{
m rac{kPa}{bar}}
ight) = 78.84~{
m kPa}$$

Since air is saturated (100% relative humidity), water vapor pressure is equal to saturation pressure.

$$p_{w,1} = p_{\text{sat},1} = 78.84 \text{ kPa}$$

The partial pressure of air is

$$\begin{split} p_{a,1} &= p_1 - p_{w,1} = 170 \: \text{kPa} - 78.84 \: \text{kPa} \\ &= 91.16 \: \text{kPa} \end{split}$$

Use equationMERM38007 (also NCEES Handbook: Air-Water Systems) to determine the humidity ratio.

$$\omega = 0.622 \left(rac{p_{w,1}}{p_{a,1}}
ight) = (0.622) \left(rac{78.84 \ \mathrm{kPa}}{91.16 \ \mathrm{kPa}}
ight)$$
 = 0.538 kg water/kg air

Since it is a constant pressure, constant moisture drying process, mole fractions and partial pressure do not change.

$$p_{w,2} = p_{w,1} = 78.84 \text{ kPa}$$

The saturation pressure at 204°C from appendixMERM24N (also *NCEES Handbook* table "Saturated Steam (SI Units)") is

$$p_{\mathrm{sat,2}} = (16.90~\mathrm{bar}) \left(100~rac{\mathrm{kPa}}{\mathrm{bar}}
ight) = 1690~\mathrm{kPa}$$

The relative humidity at state 2 is

$$\phi_2 = \frac{p_{w,2}}{p_{\text{sat 2}}} = \frac{78.84 \text{ kPa}}{1690 \text{ kPa}} = 0.0467$$

Although the volume may change, the mass does not. The specific humidity remains constant.

$$\omega_2 = \omega_1 = 0.538 \; \mathrm{kg} \; \mathrm{water/kg} \; \mathrm{air}$$

The heat required consists of two parts.

The absolute temperatures are

$$T_1 = 93\degree \text{C} + 273\degree = 366 \text{K}$$

 $T_2 = 204\degree \text{C} + 273\degree = 477 \text{K}$

As in *NCEES Handbook:* Temperature-Dependent Properties of Air (SI Units), the heat capacity is 1.013 kJ/kg·K. The heat absorbed by air is

$$egin{array}{ll} q_1 &= h_2 - h_1 = c_p \left(T_2 - T_1
ight) \ &= \left(1.013 \, rac{ ext{kJ}}{ ext{kg·K}}
ight) \left(477 ext{K} - 366 ext{K}
ight) \ &= 112.44 \, ext{kJ/kg} \end{array}$$

For water, h_1 at 93°C and 78.79 kPa is 2670 kJ/kg (almost saturated).

Follow a constant 78.79 kPa pressure curve up to 204°C.

$$h_2 = 2890 \text{ kJ/kg}$$

The heat absorbed by steam is

$$egin{aligned} q_2 &= \omega \left(h_2 - h_1
ight) \ &= \left(0.537 \, rac{ ext{kg water}}{ ext{kg air}}
ight) \left(2890 \, rac{ ext{kJ}}{ ext{kg}} - 2670 \, rac{ ext{kJ}}{ ext{kg}}
ight) \ &= 118.14 \, ext{kJ/kg air} \end{aligned}$$

The total heat absorbed is

$$\begin{split} q_{\rm total} &= q_1 + q_2 = 112.44 \; \frac{\rm kJ}{\rm kg\; air} + 118.14 \; \frac{\rm kJ}{\rm kg\; air} \\ &= \; 230.58 \; \rm kJ/kg\; air \quad (230 \; \rm kJ/kg) \end{split}$$

The answer is (C).

10.

Customary U.S. Solution

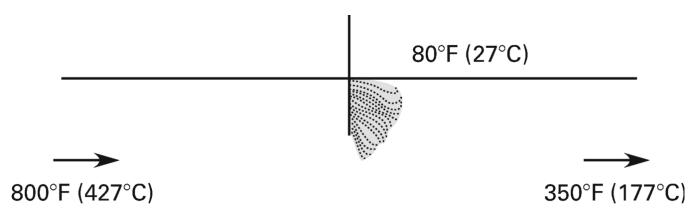
As in NCEES Handbook: Temperature, the absolute air temperatures are

$$T_1 = 800\,^{\circ}\mathrm{F} + 460\,^{\circ} = 1260\,^{\circ}\mathrm{R}$$

 $T_2 = 350\,^{\circ}\mathrm{F} + 460\,^{\circ} = 810\,^{\circ}\mathrm{R}$

From appendixMERM24A (also *NCEES Handbook* table "Physical Properties of Liquid Water (U.S. Units)"), the enthalpy of water at 80°F is $h_{w,1} = 48.07 \text{ Btu/lbm}$ (48 Btu/lbm).

From equationMERM38019(b) (also *NCEES Handbook:* Superheated Steam (U.S. Customary Units)), the enthalpy of steam at 350°F is 1216.4 Btu/lbm.



Air temperature is reduced from 800°F to 350°F, and this energy is used to change water at 80°F to steam at 350°F. From the energy balance equation,

$$egin{aligned} \dot{m}_w \left(h_{w,2} - h_{w,1}
ight) &= \dot{m}_a \left(h_1 - h_2
ight) \ \dot{m} &= rac{\dot{m}_a \left(h_1 - h_2
ight)}{h_{w,2} - h_{w,1}} = rac{\dot{m}_a c_p (T_1 - T_2)}{h_{w,2} - h_{w,1}} \ &= rac{\left(410 \; rac{ ext{lbm}}{ ext{hr}}
ight) \left(0.25 \; rac{ ext{Btu}}{ ext{lbm} \cdot ext{F}}
ight)}{2116.4 \; rac{ ext{Btu}}{ ext{lbm}} - 48.07 \; rac{ ext{Btu}}{ ext{lbm}}} \ &= \; 39.4 \; ext{lbm/hr} \; ext{water} \end{aligned}$$

The answer is (D).

SI Solution

As in NCEES Handbook: Temperature, the absolute temperatures are

$$T_1 = 427$$
°C + 273 ° = 700 K
 $T_2 = 177$ °C + 273 ° = 450 K

From appendixMERM24N (also *NCEES Handbook* table "Physical Properties of Liquid Water (SI Units)"), the enthalpy of water at 27°C is $h_{w,1} = 113.19 \text{ kJ/kg}$ (113 kJ/kg).

From equationMERM38019(a) (also *NCEES Handbook* table "Superheated Steam (SI Units)"), the enthalpy of steam at 177°C is

$$h_{w,2} = 2820.5 \text{ kJ/kg}$$

Air temperature is reduced from 427°C to 177°C, and this energy is used to change water at 27°C to steam at 177°C. From the energy balance equation,

$$\dot{m} = \frac{\dot{m}_a (h_1 - h_2)}{h_{w,2} - h_{w,1}} = \frac{\dot{m}_a c_p (T_1 - T_2)}{h_{w,2} - h_{w,1}}$$

$$= \frac{\left(0.052 \frac{\text{kg}}{\text{s}}\right) \left(1.04 \frac{\text{kJ}}{\text{kg·K}}\right) (700\text{K} - 450\text{K})}{2820.5 \frac{\text{kJ}}{\text{kg}} - 113.19 \frac{\text{kJ}}{\text{kg}}}$$

$$= 0.00502 \text{ kg/s} \quad (0.0050 \text{ kg/s})$$

The answer is (D).

<u>11</u>.

Interpolating from appendixMERM24B (also *NCEES Handbook* table "Saturated Steam (U.S. Units)— Temperature Table"), the saturation pressure, $p_{\rm sat}$, of 180°F water vapor is 7.515 psia. Use equationMERM38009 (also *NCEES Handbook*: Air-Water Systems) to find the partial pressure of the water vapor, p_w . The relative humidity, ϕ , is given as 20%.

$$egin{aligned} \phi &= rac{p_w}{p_{ ext{sat}}} \ p_w &= \phi p_{ ext{sat}} = (0.20) \left(7.515 \, rac{ ext{lbf}}{ ext{in}^2}
ight) \ &= 1.5 \, ext{lbf/in}^2 \end{aligned}$$

From appendixMERM24B (also *NCEES Handbook:* Temperature-Dependent Properties of Air (U.S. Customary Units)), the dew point temperature corresponding to 1.5 lbf/in² is 115.64°F (120°F).

The answer is (B).