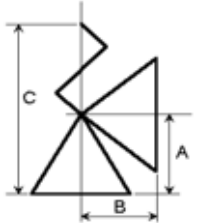


 <p>EMERSON edgardovicente.chiari@emerson.com Madrid, Spain +34 911 111 320 edgardovicente.chiari@emerson.com</p>				<b>Pressure Relief Valve Sizing &amp; Selection Report</b>					
				1	EVC			20-abr.-2022	New process data
				0	EVC			27-jul.-2021	
Quote Number: 093-093				No	Prpd.	Chk.	Appr.	Date	Revision
Client: <b>TECHNIP ENERGIES</b> Location: <b>CARTAGENA, SPAIN</b> Project: <b>C43 "New Bios 2G Hydrotreatment Unit"</b>									
End-User Ref. No.: <b>201754C001</b> Project Ref. No.: <b>U-608 Hydrogen Unit</b>									
1	<b>Valve ID</b>				41	<b>SIZING DATA</b>			
2	Tag No.	608-PSV-1038			42	Design Code	ASME VIII/XIII - UV Sizing Std. API 520		
3	Service	C-231 fuel gas K.O. Drum			43	Sizing Basis	Fire Case		
4	PID No.	P-C43-A-110990 H45			44	Fluid State at Inlet	Gas / Vapor		
5	Line No.	1-1/2"-FG-4512-B4-P	Quantity		45	Relieving Case	Pressure Relief		
6			1		46	<b>Fluid Properties</b>			
7	<b>GENERAL</b>				47	Fluid Name	HYDROCARBON		
8	Valve Type	Balanced Bellows, Direct Spring-Op			48	Molecular Weight, M	45.52		
9	Safety / Relief	Safety	Balanced	Yes	49	Compressibility, Z	0.912		
10	Nozzle	Full	Bonnet	Vented	50	Ratio of Sp. Heats, k (Cp / Cv)	1.108		
11	<b>CONNECTIONS</b>				51	Gas Constant, C	248.7		
12	Inlet	1"	Flngd.	300# RF Standard	52				
13	Outlet	2"	Flngd.	150# RF ASME B16.5	53				
14	<b>MATERIALS OF CONSTRUCTION</b>				54				
15	Body / Base	CS SA216-WCB/WCC			55				
16	Bonnet / Cylinder	CS SA216-WCB/WCC			56				
17	Nozzle	316 SST			57				
18	Disc	316 SST			58				
19	Seat	Metal			59	<b>Sizing Coefficients</b>			
20	Spindle	416 SST			60	Effective K, Gas	0.975		
21	Guide	SS A297 Gr. HE			61	Kb	Kc	0.968	1
22	Spring	Chrome Steel - Corr. Rest.			62				
23	Gaskets	316 SST			63				
24	Bellows	Inconel® 625			64	<b>Required Capacity</b>			
25	Cap Type	Screwed w/ Test Rod			65	Total	455		
26	NACE MR0175/ISO 15156:2015	No			66				
27	Accessories	Bug Screen			67	<b>Pressures</b>			
28					68	MAWP	Operating	5.8	3.7
29					69	Set	CDTP	5.8	5.800
30					70	Over Pressure	1.218 21%		
31	<b>SIZING / SELECTION SUMMARY</b>				71	Back Pressure	Built-Up	2.3	
32	Valve Model No.	1D2JBS-E35K-P			72		Constant Superimposed	0	
33	Brand	Crosby®			73		Variable Superimposed	0	
34	Area	Calculated	Selected	0.642 0.710	74		Total	2.3	
35	(cm²)	Data Set	Orifice	API D	75	Inlet Loss	0 0%		
36	Flow	Unit	Required	kg/hr 455	76	Atmospheric (Barometric)	1.033 kg/cm² a		
37			Maximum	503.131	77	<b>Temperatures</b>			
38					78	Normal System			
39	Reaction Force, Open Discharge		37 N		79	Operating	Relieving	38	67.9
40	Noise Level (db), Open Discharge		114.1 at 1.0000-m		80	Design Min	Design Max		150
Tag Notes	1. Standard C4M acc. ISO 12944				Valve Dimensions	mm	A		
	2. Opening Adjustment:5%.						104.90		
	3. NAC E 0103 certificate required (disc & bellow ).						B		
							114.30		
							C		
							514.35		
				kg	Weight				
						16.33			

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				0	EVC			27-jul.-2021	
Quote Number: 093-093				No	Prpd.	Chk.	Appr.	Date	Revision
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End-User Ref. No.: <b>201754C001</b> Project Ref. No.: <b>U-608 Hydrogen Unit</b>									
1	<b>VALVE ID</b>				11	<b>CALCULATION NOTES</b>			
2	Tag No.	608-PSV-1038			12	1. Standard C4M acc. ISO 12944 2. Opening Adjustment:5%. 3. NAC E 0103 certificate required (disc & bellow ).			
3	Valve Model No.	1D2JBS-E35K-P		Qty. 1	13				
4	<b>SIZING DATA</b>				14				
5	Design Code	ASME VIII/XIII - UV		Sizing Std.	API 520	15			
6	Fluid State at Inlet	Gas / Vapor			16				
7	<b>CALCULATION SUMMARY</b>								
8	Flow	Required	455 kg/hr		18	Area	Required	0.642 cm²	
9		Maximum	503.131 kg/hr		19		Selected	0.710 cm²	
10	Reaction Force, Open Discharge		37 N		20	Noise Level (db), Open Discharge		114.1 at 1.0000 m	
<b>Variable Type</b>	<b>Variable Name</b>	<b>Symbol</b>		<b>Input Value</b>		<b>Equation Value</b>			
Fluid Properties	Molecular Weight	M		45.52		45.52			
	Ratio of Specific Heats	k		1.108		1.108			
	Compressibility	Z		0.912		0.912			
Process Cond.	Required Mass Flow	Wreq		455 kg/hr		455 kg/hr			
	Set Pressure	Pset		5.8 kg/cm² g		5.688 barg			
	Over Pressure	Pover		1.218 kg/cm² g		1.194 barg			
	Inlet Line Loss	Ploss		0 kg/cm² g		0 barg			
	Back Pressure	Pback		2.3 kg/cm² g		2.256 barg			
	Atmospheric Pressure	Patm		1.033 kg/cm² a		1.013 bara			
	Relieving Temperature	T		67.9 °C		341.050 °K			
	Distance from Valve (noise)	r		1.0000 m		1.0000 m			
	Rupture Disc CCF	Kc		1		1			
Valve Data	Discharge Coefficient (API)	K,API		0.975		0.975			
	Orifice Area	A		0.710 cm²		0.710 cm²			
	Back Press. Correction Factor	Kb		0.968		0.968			
	Outlet Diameter	Do		52.5 mm		5.25 cm			
<b>Calculate Inlet Relieving Pressure, Outlet Pressure, Absolute Pressure Ratio</b>									
P1 = Pset + Pover - Ploss + Patm		<b>P1</b>				7.896 bara			
P2 = Pback + Patm		<b>P2</b>				3.269 bara			
PR = P2 / P1		<b>PR</b>				0.414			
<b>Calculate Gas Constant</b>									
C = 394.8 * {k * [2 / (k + 1)]^[(k + 1) / (k - 1)]}^0.5		<b>C</b>				248.7			
<b>Calculate Mass Critical Flow</b>									
W = A * C * K,API * P1 * Kb * Kc * [M / (T * Z)]^0.5		<b>W</b>		503.131 kg/hr		503.131 kg/hr			
<b>Calculate Required Orifice Area</b>									
Areq = A * Wreq / W		<b>Areq</b>		0.642 cm²		0.642 cm²			

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9		Maximum	503.131 kg/hr		19		Selected	0.710 cm²	
10	Reaction Force, Open Discharge		37 N		20	Noise Level (db), Open Discharge		114.1 at 1.0000 m	
<b>Calculate Noise Level at 100-ft (30-m) L100</b>									
L100 = [87.75 * log( 1/PR ) + 14.09] + [10 * log(1.1552 * W * k * T / M)]									
<b>Calculate Noise Level at Distance, r Lp</b>									
Lp = L100 - 20 * log(r / 30)									
<b>Calculate Reaction Force for Open Discharge Fr</b>									
Fr = (A * C * K,API * P1 * Kc / 27.907) * {k / [(k + 1) * Z]}^0.5									

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