				EMERSON				Press	ure Reli	ief Val	ve Sizin	g & Sele	ction Report	
	<u> </u>		edgardovid	ente.chiari@emers	on.com	0				7-jul	2021			
E	MEŘ	SON	J.	Spain										
			-	+34 911 111 320										
				ente,chiari@emers	on.com									
			mber: 094-0	92		No	Prp	d. Chk.	Appr.	D	ate		Revisio	n
	Client:	INTECSA												
	Location:	CARTAGE	NA					End-Use	er Ref. N	lo.:				
	Project:	REPSOL C	243					Proje	ct Ref. N	No.: 69	7751580	5		
1			Valve				41 42					NG DATA		
2	Tag No. 660-TSV -F17-30			'-30							ection VII	/III Sizing Std. API 520		
3					BRAZO 660-K-F17/105			Sizing Basis Blo			Block	ked Discharge	1	
4			660-A-C31-A-	•					Fluid State at Inlet Liquid					
5		Line No.	C43-1"P-0092	4-B4	Quantity							essure Relief		
6					1	1	46	Fluid Prop	perties					
7			GENE				47			uid Na			BIO	JET
8				Direct Spring-Op			48			Gravit				725
9	Saf		Safety Relief	Balanced			49			√iscosi			1.10000	
10		Nozzle			Closed	1	50			ynolds			1205	33. <i>4</i> 9
11			CONNEC				51		Reyno	olds No	. (max)		2891	125.5
12	Inlet	3/4"	Thrd.	MNPT	Stan	dard	52							
13	Outlet	1"	Thrd.	FNPT	ASME I	B1.20.1	53							
14				ONSTRUCTION			54							
15		Body Cylin		CS SA216	-		55							
16		Body Bas		316 S			56 57							
17														
18							58							
19						59 60	Sizing Co					Unit	-	
20								Effective K, Liquid				65		
21	Spindle			416 SST				Kw		Kc		1.0	1	
22		Guide			316 SST				Kv		Kv (m	ax)	0.998	1.0
23		Spring		17-7 PH	SST		63						- 0	
24							-	Required	Capacit	•			Unit	m³/hr
25		Cap Typ		Screwed &		d	65			Total			4.	92
26		R0175/ISO	15156:2015	No			66	_						
27 28 29	Accessories						_	Pressures					Unit	kg/cm² g
28	sso						68	I IV	1AWP		Opera	-	17	2.5
29	cce						69		Set	D	CDT	Р	17	17.00
30 31	∢	015	NO / OF! FOR	IONI CUITANA CON			70		Ove	er Pres	sure	D. St. 11	1.7	10%
	\/ab		NG / SELECT	ION SUMMARY			71 72		D I		Const	Built-U		0.057
32		Valve Model No.			961101MFB-P				Back essure				perimposed 0 perimposed 0	
33 34	Area	Calculate	d Selecte	Crosby® 29.639	70.	068	73 74	-	COOUIC		vanal	ole Super Total		0.057
35	(mm²)	Data Se				900	75		1.	nlet Lo	20	Total	0	0.037
36	(111111-)	Unit	Require			92	76				arometri	c)		kg/cm² a
37	Flow	Offic	Maximu			802	-	Temperati		enc (D	arometri	0)	Unit	°C
38	1 1000		IVIAAIITIU		11.0	002	78	remperau	ures	N	lormal S	vetem	Onit	U
39	Reaction	on Force O	l pen Discharge	14	M		79	On	erating	1,	Reliev		35	35
39 40			pen Discharge		/A		80	_	sign Min		Design	-	33	93
ŦŪ			A acc. ISO 129		<i>,</i> , ,		00		Jigir iviii		Doolgii	A		33
	2. Frosio C	ertificate.	400. 100 120							ဂ္ဂ		79.38	_	
'n	3. Special									ion		В		' _
ote	4. Thermal 5. ASME S		monitoring indired	ciude.						ens	E L	49.21	· <	/
ž				//agnetic/24VDC wi	res/24V	/Ex ia II	C T6	Ga		Ĭ	l ⊢	C	*	
	7. Full Noz			3						Valve Dimensions	2	07.98		\ <u>\</u> \\^
	8. Opening									/alv		Veight	¥ /	↓
	9. Certifica	te ATEX (20	014 / 34 EU)								[5 V	v eigi it	k-	

4.54

EMERSON							Pressure Relief Valve Calculation Report							
			edgardovi	icente.chi	ari@emerson.co	m 0				7-jul2021		•		
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_	MER	50	NI	Sp	ain									
	MER	.50	ъ.		111 320									
			edgardovi	icente,chi	ari@emerson.co	m								
		Quote	Number: 094-0			No	Prpd	. Chk.	Appr.	Date		Revision		
	Client:	INTECS												
	Location:	CARTA	GENA					End-Use	er Ref. N	lo.:				
Project: REPSOL C43						Project Ref. No.: 697751586								
1 VALVE ID						11 CALCULATION NOTES						IOTES		
								1. Standard paint C4 M acc. ISO 12944.						
2	Tag No		No. 660-TSV -F17	7-30				2 2. Frosio Certificate.						
							3.	3. Special nameplate.						
3	Valve	Model I	No. 961101MFB-I	Р	Qty.	Qty. 1				lves monitoring	g include	Э.		
								ASME S			oo: Maar	netic/24VDC wires/24V/Ex	v in	
4			SIZING				C T6 Ga	JII. 7J-1	3301-33F. Typ	e. Mayı	Telle/24 v DC WITES/24 v/L)	(la		
_									zle and	removable.				
5	Desigr	n Code	ASME Secti	tion VIII	Sizing Std.	API 520				ment ±5%				
							9.	Certifica	te ATE	((2014 / 34 EU	J)			
6	Fluid Sta	te at Inle	et	Liquid			16							
_			CALCULATIO	ALCUMAN	ADV									
7				N SUIVIIVI			10			Poquirod		20 620 mm²		
8 9	Flow		Required		4.92 m³/hı		18 19	Area		Required		29.639 mm² 70.968 mm²		
	Daneti			11.802 m³/hı				Selected		70.966 111112				
Reaction Force, Open Discharge			е	14 N	mah a l	20	Innut	Value /	Unito		Faustien Value / Unite			
/ariable Type Variable Name Fluid Properties Specific Gravity					Symbol SG		Input Value / Units 0.725				Equation Value / Units 0.725			
iui	a Fropertie	5	Specific Gravity						123			0.775		
			\/iooooity						000 oB					
)ro	coss Cond		Viscosity	otrio Flow		J		1.100	000 cP	hr		1.10000 cP		
ro	cess Cond.		Required Volume	etric Flow	VL	req		1.100	.92 m³/			1.10000 cP 21.662 GPM (US)		
ro	icess Cond.		Required Volume Set Pressure	etric Flow	VL P:	req set		1.100 4	.92 m³/ 17 kg/	cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig		
Pro	cess Cond.		Required Volume Set Pressure Over Pressure	etric Flow	VL Ps Pc	req set ver		1.100 4	.92 m ³ / 17 kg/ 1.7 kg/	cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig		
Pro	cess Cond.		Required Volume Set Pressure Over Pressure Inlet Line Loss	etric Flow	VL P: Pc Ple	req set ver		1.100 4	.92 m ³ / 17 kg/ 1.7 kg/ 0 kg/	cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig		
Pro	icess Cond.		Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure		VL P: Pc Ple Pb	req set ver oss ack		1.100 4	17 kg/ 17 kg/ 1.7 kg/ 0 kg/ 057 kg/	cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig		
			Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC	:F	VL Ps Pc Pli Pb	req set ver oss ack		1.100	.92 m ³ / 17 kg/ 1.7 kg/ 0 kg/ 057 kg/	cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1		
	ve Data		Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure	:F	VL Ps Pc Pli Pb	req set ver oss ack		1.100	17 kg/ 17 kg/ 1.7 kg/ 0 kg/ 057 kg/	cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig		
		-	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffice	:F	VL P: Pc Pli Pb k	req set ver oss ack (c		0.0	1.92 m ³ / 17 kg/ 1.7 kg/ 0 kg/ 057 kg/ 1	cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65		
		-	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffic	F cient (AP	VL P: Pc Plc Plc Pb k	req req set ver oss ack cc API		0.0 70.9	92 m³/ 17 kg/ 1.7 kg/ 0 kg/ 057 kg/ 1 0.65	cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65		
		-	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffic Orifice Area Back Press. Corr	F cient (AP	VL P: Pc Plc Pb k I) K,	req set ver oss ack (c API		0.0	.92 m³/ 17 kg/ 1.7 kg/ 0 kg/ 057 kg/ 1 0.65	cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65		
		-	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffic Orifice Area Back Press. Corr Viscosity Correct	F cient (AP rection Fa tion (Rqd	VL Ps Pc Pli Pb k I) K, sector K Flow)	req set ver oss ack (c API		0.0 0.0 70.9	.92 m³/ 17 kg/ 1.7 kg/ 0 kg/ 057 kg/ 1 .65	cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65 0.110 in ² 1.0 0.998		
		-	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffic Orifice Area Back Press. Corr Viscosity Correct Viscosity Correct	F cient (AP rection Fa tion (Rqd	VL Ps Pc Pli Pb k I) K, actor K Flow) Flow) Kv,	J.,req set ver oss ack (c API		0.0 0.0 70.9	92 m³/ 17 kg/ 1.7 kg/ 0 kg/ 057 kg/ 1 0.65	cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65 0.110 in ² 1.0 0.998 1.0		
/al¹	ve Data	-	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffic Orifice Area Back Press. Corr Viscosity Correct Viscosity Correct Outlet Diameter	F cient (AP rection Fa tion (Rqd tion (Max	VL Ps Pc Plo Plo k I) K, ictor K Flow) Kv,	req set ver oss ack (c API		0.0 0.0 70.9	.92 m³/ 17 kg/ 1.7 kg/ 0 kg/ 057 kg/ 1 .65	cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65 0.110 in ² 1.0 0.998		
/al	ve Data	t Reliev	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffic Orifice Area Back Press. Corr Viscosity Correct Viscosity Correct Outlet Diameter ing and Outlet P	F cient (AP rection Fa tion (Rqd tion (Max	VL P: Pc Pli Pb k I) K, actor K Flow) K Flow) Kv,	req set ver oss ack ack ac API		0.0 0.0 70.9	92 m³/ 17 kg/ 1.7 kg/ 0 kg/ 057 kg/ 1 0.65	cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65 0.110 in² 1.0 0.998 1.0 1.05 in		
/al	ve Data Culate Inle	t Reliev + Pover	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffic Orifice Area Back Press. Corr Viscosity Correct Viscosity Correct Outlet Diameter ing and Outlet P	F cient (AP rection Fa tion (Rqd tion (Max	VL P: Pc Plo Plo Pb II) K, Ictor K Flow) Flow) Kv,	req feet ver foss fack fcc API A fw fv max foo		0.0 0.0 70.9	92 m³/ 17 kg/ 1.7 kg/ 0 kg/ 057 kg/ 1 0.65	cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65 0.110 in² 1.0 0.998 1.0 1.05 in		
/al	ve Data	t Reliev + Pover	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffic Orifice Area Back Press. Corr Viscosity Correct Viscosity Correct Outlet Diameter ing and Outlet P	F cient (AP rection Fa tion (Rqd tion (Max	VL P: Pc Plo Plo Pb II) K, Ictor K Flow) Flow) Kv,	req set ver oss ack ack ac API		0.0 0.0 70.9	92 m³/ 17 kg/ 1.7 kg/ 0 kg/ 057 kg/ 1 0.65	cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65 0.110 in² 1.0 0.998 1.0 1.05 in		
∕al¹	ve Data Culate Inle Pa = Pset Pb = Pback	t Reliev + Pover k	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffic Orifice Area Back Press. Corr Viscosity Correct Viscosity Correct Outlet Diameter ing and Outlet P - Ploss	cient (AP rection Fa tion (Rqd tion (Max Pressures	VL P: Pc Plo	req req set ver oss ack c API A w v v max oo		1.100 4 0.0 70.9 0.9	998 1.0 964 mm	cm² g cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65 0.110 in² 1.0 0.998 1.0 1.05 in 265.977 psig 0.811 psig		
/al	ve Data culate Inle Pa = Pset - Pb = Pbace	t Reliev + Pover k	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffic Orifice Area Back Press. Corr Viscosity Correct Viscosity Correct Outlet Diameter ing and Outlet P - Ploss Selected Valve	rection Fation (Rqd tion (Max	VL Ps Pc Plo Plo Pb k I) K, ictor K Flow) K Flow) Kv, C F	req feet ver foss fack fcc API A fw fv max foo		1.100 4 0.0 70.9 0.9	92 m³/ 17 kg/ 1.7 kg/ 0 kg/ 057 kg/ 1 0.65	cm² g cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65 0.110 in² 1.0 0.998 1.0 1.05 in		
/al	ve Data culate Inle Pa = Pset - Pb = Pbace	t Reliev + Pover k	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffic Orifice Area Back Press. Corr Viscosity Correct Viscosity Correct Outlet Diameter ing and Outlet P - Ploss	rection Fation (Rqd tion (Max	VL Ps Pc Plo Plo Pb k I) K, ictor K Flow) K Flow) Kv, C F	req req set ver oss ack c API A w v v max oo		1.100 4 0.0 70.9 0.9	998 1.0 964 mm	cm² g cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65 0.110 in² 1.0 0.998 1.0 1.05 in 265.977 psig 0.811 psig		
/al	ve Data culate Inle Pa = Pset Pb = Pbace culate Cap	t Reliev + Pover k pacity of	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffic Orifice Area Back Press. Corr Viscosity Correct Viscosity Correct Outlet Diameter ing and Outlet P - Ploss Selected Valve I * Kw * Kc * Kv,n	rection Fation (Rqd tion (Max	VL Ps Pc Plo Pb k I) K, actor k Flow) k Flow) Kv, C Fl	req req set ver oss ack c API A w v v max oo		1.100 4 0.0 70.9 0.9	998 1.0 964 mm	cm² g cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65 0.110 in² 1.0 0.998 1.0 1.05 in 265.977 psig 0.811 psig		
/al	ve Data culate Inle Pa = Pset Pb = Pback culate Cap VL = 38 * A	t Reliev + Pover k pacity of \(\delta\) * K,AP	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffic Orifice Area Back Press. Corr Viscosity Correct Viscosity Correct Outlet Diameter ing and Outlet P - Ploss Selected Valve I * Kw * Kc * Kv,n	rection Fation (Rqd tion (Max Pressures	VL Ps Pc Plo Pb k I) K, actor k Flow) k Flow) Kv, C Fl	Jareq		1.100 4 0.0 70.9 0.9	998 1.0 964 mm	cm² g cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65 0.110 in² 1.0 0.998 1.0 1.05 in 265.977 psig 0.811 psig		
/al	ve Data Culate Inle Pa = Pset Pb = Pback Culate Cap VL = 38 * # Culate Rey R = 2800 *	t Reliev + Pover k pacity of A * K,AP	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffic Orifice Area Back Press. Corr Viscosity Correct Viscosity Correct Outlet Diameter ing and Outlet P - Ploss Selected Valve I * Kw * Kc * Kv,n	rection Fation (Rqd tion (Max Pressures max * [(Pa	VL Ps Pc Plo Plo Ri I) K, Inctor K Flow) K Flow) Kv, C Flow) Kv, C Flow) Soj^0.5	Jarreq Ja		1.100 4 0.0 70.9 0.9	998 1.0 964 mm	cm² g cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65 0.110 in² 1.0 0.998 1.0 1.05 in 265.977 psig 0.811 psig 51.961 GPM (US)		
/al	ve Data Culate Inle Pa = Pset Pb = Pback Culate Cap VL = 38 * # Culate Rey R = 2800 *	t Reliev + Pover k pacity of A * K,AP	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffic Orifice Area Back Press. Corr Viscosity Correct Viscosity Correct Outlet Diameter ing and Outlet P - Ploss Selected Valve I * Kw * Kc * Kv,n	rection Fation (Rqd tion (Max Pressures max * [(Pa	VL Ps Pc Plo Plo Ri I) K, Inctor K Flow) K Flow) Kv, C Flow) Kv, C Flow) Soj^0.5	Jareq		1.100 4 0.0 70.9 0.9	998 1.0 964 mm	cm² g cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65 0.110 in² 1.0 0.998 1.0 1.05 in 265.977 psig 0.811 psig		
/al	ve Data Culate Inle Pa = Pset Pb = Pbace VL = 38 * A Culate Rey R = 2800 * R,max = 28	t Reliev + Pover k nacity of A * K,AP nolds N VL,req 300 * VL	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffic Orifice Area Back Press. Corr Viscosity Correct Viscosity Correct Outlet Diameter ing and Outlet P - Ploss Selected Valve I * Kw * Kc * Kv,n	rection Fation (Rqd tion (Max Pressures max * [(Pa	VL Ps Pc Plo Plo Pb k I) K, fictor k Flow) k Flow) Kv, C F F R,r	Jarreq Ja		1.100 4 0.0 70.9 0.9	998 1.0 964 mm	cm² g cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65 0.110 in² 1.0 0.998 1.0 1.05 in 265.977 psig 0.811 psig 51.961 GPM (US)		
/al	ve Data culate Inle Pa = Pset Pb = Pback culate Cap VL = 38 * A culate Rey R = 2800 * R,max = 28	t Reliev + Pover k nacity of A * K,AP nolds N VL,req 300 * VL	Required Volume Set Pressure Over Pressure Inlet Line Loss Back Pressure Rupture Disc CC Discharge Coeffic Orifice Area Back Press. Corr Viscosity Correct Viscosity Correct Outlet Diameter ing and Outlet P - Ploss Selected Valve I * Kw * Kc * Kv,n	rection Fation (Rqd tion (Max Pressures max * [(Pa	VL Ps Pc Plo Plo Pb k I) K, fictor k Flow) k Flow) Kv, C F F R,r	Jareq		1.100 4 0.0 70.9 0.9	998 1.0 988 1.0 988 1.0 988 1.0 988 1.0 988 1.0 988 1.0	cm² g cm² g cm² g cm² g cm² g		1.10000 cP 21.662 GPM (US) 241.797 psig 24.18 psig 0 psig 0.811 psig 1 0.65 0.110 in² 1.0 0.998 1.0 1.05 in 265.977 psig 0.811 psig 51.961 GPM (US)		

Page: 2

Printed On: 24-feb.-2022

EMERSON						Pressure Relief Valve Calculation Report								
	edgardovicente.chiari@emerson.com					0				7-jul2021				
EMERSON. Spain														
+34 911 111 320														
edgardovicente,chiari@emerson.com														
Quote Number: 094-092						No	Prpc	d. Chk.	Appr.	Date		Revision		
	Client:	INTECSA												
	Location:	CARTAGE	ENA					End-Use	er Ref. N	No.:				
	Project:	REPSOL (C43				Project Ref. No.: 697751586							
1			VALVE ID				11		CALCULATION NOTES					
2	Tag No. 660-TSV -F17-30									C4 M acc. ISO 1	12944.			
							-	. Frosio C						
3	Valve Model No. 961101MFB-P				Qty. 1			Special nameplate. High results of the state of						
Ľ	valve iviodel No. 9611011virb-P Qty. 1							5. ASME STAMP required.						
4	SIZING DATA						4 6	6. Go Switch: 7J-1356F-JSP. Type: Magnetic/24VDC wires/24V/Ex i						
			1	1				IIC T6 Ga 7. Full Nozzle and removable.						
5	Design	Design Code ASME Section VIII Sizi			I. AF	PI 520		8. Opening Adjustment ±5%						
								9. Certificate ATEX (2014 / 34 EU)						
6	Fluid State at Inlet Liquid						16							
Z CALCULATION CHAMADY														
7 8	CALCULATION SUMMARY Required 4.92 m³/hr						18		Poguirod 20 630 mm			29.639 mm²		
9	Flow	Flow Required					19	Area	Required Selected			70.968 mm ²		
-	Maximum 11.802 m³/hr					20			70.900 111111-					
10 Reaction Force, Open Discharge 14 N							20	44.01				3.1 lbf		
Cal	Calculate Reaction Force for Open Discharge Fr Ao = $(\pi * Do^2) / 4$								14 N			3.1 IVI		
	`	,	: K ADI * Ku may\^21 /	٨٥										
	$\Gamma_1 = [2.002]$. ra (A	K,API * Kv,max)^2] /	AU										

Printed On: 24-feb2022	PRV2SIZE Software Version pr7_20210922.1	Page : 3

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