
 <p>EMERSON edgardovicente.chiari@emerson.com</p> <p>Spain +34 911 111 320 edgardovicente.chiari@emerson.com</p>				Pressure Relief Valve Calculation Report								
				0				7-jul.-2021				
Quote Number: 094-092				No	Prpd.	Chk.	Appr.	Date	Revision			
Client: INTECSA					End-User Ref. No.:							
Location: CARTAGENA					Project Ref. No.: 697751586							
Project: REPSOL C43												
1	VALVE ID				11	CALCULATION NOTES						
2	Tag No.	660-TSV -F17-30			12	1. Standard paint C4 M acc. ISO 12944. 2. Frosio Certificate. 3. Special nameplate. 4. Thermal relief valves monitoring include. 5. ASME STAMP required. 6. Go Switch: 7J-1356F-JSP. Type: Magnetic/24VDC wires/24V/Ex ia IIC T6 Ga 7. Full Nozzle and removable. 8. Opening Adjustment ±5% 9. Certificate ATEX (2014 / 34 EU)						
3	Valve Model No.	961101MFB-P		Qty. 1	13							
4	SIZING DATA				14							
5	Design Code	ASME Section VIII	Sizing Std.	API 520	15							
6	Fluid State at Inlet	Liquid			16							
7	CALCULATION SUMMARY											
8	Flow	Required	4.92 m³/hr		18					Area	Required	29.639 mm²
9		Maximum	11.802 m³/hr		19						Selected	70.968 mm²
10	Reaction Force, Open Discharge		14 N		20							
Variable Type		Variable Name		Symbol	Input Value / Units		Equation Value / Units					
Fluid Properties		Specific Gravity		SG	0.725		0.725					
		Viscosity		μ	1.10000 cP		1.10000 cP					
Process Cond.		Required Volumetric Flow		VL,req	4.92 m³/hr		21.662 GPM (US)					
		Set Pressure		Pset	17 kg/cm² g		241.797 psig					
		Over Pressure		Pover	1.7 kg/cm² g		24.18 psig					
		Inlet Line Loss		Ploss	0 kg/cm² g		0 psig					
		Back Pressure		Pback	0.057 kg/cm² g		0.811 psig					
		Rupture Disc CCF		Kc	1		1					
Valve Data		Discharge Coefficient (API)		K,API	0.65		0.65					
		Orifice Area		A	70.968 mm²		0.110 in²					
		Back Press. Correction Factor		Kw	1.0		1.0					
		Viscosity Correction (Rqd Flow)		Kv	0.998		0.998					
		Viscosity Correction (Max Flow)		Kv,max	1.0		1.0					
		Outlet Diameter		Do	26.64 mm		1.05 in					
Calculate Inlet Relieving and Outlet Pressures												
Pa = Pset + Pover - Ploss				Pa	265.977 psig							
Pb = Pback				Pb	0.811 psig							
Calculate Capacity of Selected Valve $VL = 38 * A * K,API * Kw * Kc * Kv,max * [(Pa - Pb) / SG]^{0.5}$				VL	11.802 m³/hr		51.961 GPM (US)					
Calculate Reynolds Number $R = 2800 * VL,req * SG / (\mu * A^{0.5})$ $R,max = 2800 * VL * SG / (\mu * A^{0.5})$				R	120533.49							
				R,max	289125.5							
Calculate Required Orifice Area $Areq = (A * VL,req * Kv,max) / (VL * Kv)$				Areq	29.639 mm²		0.046 in²					
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10	Reaction Force, Open Discharge		14 N		20				
Calculate Reaction Force for Open Discharge									
$A_o = (\pi * D_o^2) / 4$									
$F_r = [2.002 * P_a * (A * K_{API} * K_{v,max})^2] / A_o$									
				Fr	14 N				3.1 lbf

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