

# Energy conversions

Power:

$$P_{gr} = \rho Q g H_{gr}$$

Francis Turbine

$$P_R = \rho Q (u_1 c_{u1} - u_2 c_{u2})$$



Kaplan Turbine

$$P_R = \rho Q (u_1 c_{u1} - u_2 c_{u2})$$

$$U = u_1 = u_2$$

$$P_R = \rho Q U (c_{u1} - c_{u2})$$

Euler Turbomachine EQ

$$Power_{req} = \dot{m} (U_2 V_{\theta 2} - U_1 V_{\theta 1})$$

$$h = \frac{1}{g} (U_2 V_{\theta 2} - U_1 V_{\theta 1})$$

$$Power_{req} > 0 \rightarrow \text{Compressor}$$

$$Power_{req} < 0 \rightarrow \text{Turbine}$$

Pelton turbine

Power:

$$\Delta W = U w_1 (1 - k \cos(\beta_2)) = U (c_1 - U) (1 - k \cos(\beta_2))$$

Runner Power:

$$P_R = \rho Q U (c_{u1} - c_{u2}) \quad - \text{Pelton}$$

$$P_R = \rho Q (u_1 c_{u1} - u_2 c_{u2}) \quad - \text{General}$$

Total available Power

$$P_n = \rho Q g H_n$$

Hydraulic efficiency

$$\eta_h = \frac{P_R}{P_n} = \frac{1}{g H_n} (u_1 c_{u1} - u_2 c_{u2})$$

Power of the Runner

$$P_R = \rho Q (u_1 c_{u1} - u_2 c_{u2})$$

Main Turbine equation

$$\eta_h H_n = \frac{1}{g} (u_1 c_{u1} - u_2 c_{u2})$$

Total sum off losses

$$h_L = \frac{1}{2} (\zeta_1 c_1^2 + \zeta_2 c_2^2 + \zeta_2 c_2^2 + (1 + \zeta_3) c_{13}^2 + E_1^2)$$

Total sum of energy transfer

$$H_n = (1 + \zeta_1) \frac{c_1^2}{2g} - \frac{c_2^2}{2g} + (1 + \zeta_2) \frac{V_2^2}{2g} - \frac{V_1^2}{2g} + \frac{u_1^2}{2g} + \frac{u_2^2}{2g} + (1 + \zeta_3) \frac{c_3^2}{2g} + \frac{E_1^2}{2g}$$

$$\underline{c} = \frac{c}{\sqrt{2gH_n}}$$

$$\underline{u} = \frac{u}{\sqrt{2gH_n}}$$

$$\underline{V} = \frac{V}{\sqrt{2gH_n}}$$

Reduced main turbine equation

$$\eta = 2(\underline{u}_1 \underline{c}_{u1} - \underline{u}_2 \underline{c}_{u2})$$

Others:

$$\underline{h} = \frac{h_p}{H_n}$$

$$\underline{Q} = \frac{Q}{\sqrt{2gH_n}}$$

$$\underline{\omega} = \frac{\omega}{\sqrt{2gH_n}}$$

Speed Number

$$\frac{\eta_q}{89} = \underline{\Omega} = \underline{\omega} \sqrt{\underline{Q}}$$

# Fluid Dynamics

## Design of Pelton wheel

Absolute velocity from nozzle

$$C_1 = \sqrt{2gH_n}$$

$$\underline{C}_1 = \frac{C_1}{\sqrt{2gH_n}} = 1$$

Circumferential speed

$$u_1 = \frac{C_{1u}}{2} = \frac{1}{2} \sqrt{2gH_n}$$

$$\underline{u}_1 = \frac{u_1}{\sqrt{2gH_n}} = 0,5$$

Euler's Turbine equation

$$\eta_h = 2(\underline{u}_1 \underline{C}_{1u} - \underline{u}_2 \underline{C}_{2u})$$

In a perfect world:  
with  $\underline{C}_{1u} = 1$   $\underline{C}_{2u} = 0$

$$\eta_h = 2(0,5 \cdot 1 - 0,5 \cdot 0) = 1$$

we set it to be:

$$\eta = 0,96$$

$$0,99 \leq \underline{C}_{1u} \leq 0,995$$

$$\underline{u}_1 = \frac{\eta}{2 \underline{C}_{1u}} = \frac{0,96}{2 \cdot 1} = 0,48$$

Diameter of water stream

$$d_s = \sqrt{\frac{4Q}{z \pi C_{1u}}}$$

$z$  = Number of nozzles

$Q$  = flow rate

$$C_{1u} = \sqrt{2gH_n}$$

Runner diameter

$$D = 10 \cdot d_s \quad H_n \leq 500 \text{ m}$$

$$D = 15 \cdot d_s \quad H_n = 1300 \text{ m}$$

Ratio size bucket and nozzles

$$3,1 \leq \frac{B}{d_s} \leq 3,4$$

$$B = 3,1 d_s, \quad z = 1$$

$$B = 3,2 d_s, \quad z = 2$$

$$B = 3,3 d_s, \quad z = 3-5$$

$$B > 3,3 d_s, \quad z = 6$$

$D < 9,5 d_s$  must be avoided

$D > 15 d_s$  is very high head pelton

## Speed number

$$\underline{\Omega} = \underline{\omega} \sqrt{Qz}$$

$$\underline{Q} = \frac{\pi d_s^2}{4} \underline{c}_{in}$$

$$\underline{\omega} = \frac{\omega}{\sqrt{2gH_n}}$$

With  $\underline{c}_{in} = 1$ ,  $\underline{\omega}_1 = 0,5$ :

$$\underline{\Omega} = \frac{d_s}{D} \sqrt{\frac{\pi z}{4}}$$

$$0,09 \leq \underline{\Omega} \leq 0,22$$

## Dependency $C_v$

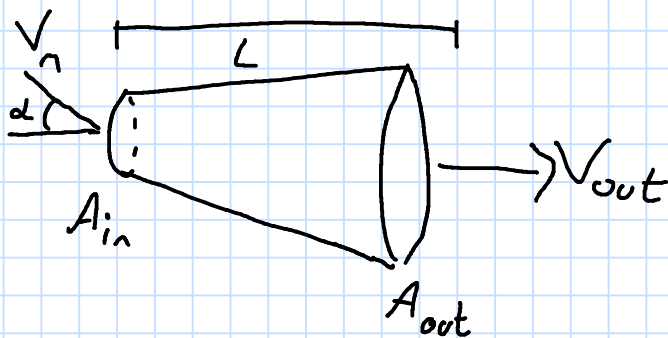
$$Q = \frac{\dot{m}}{\rho}$$

$$C_v = \frac{Q}{A \sqrt{2(\rho_{in} - \rho_{out})/\rho}}$$

$$C_v = \frac{\dot{m}}{A \rho \sqrt{2(\rho_{in} - \rho_{out})}}$$

## Basics

### Control Volume



### Extensive properties:

Depend on system size  
or amount of material

ex: mass, energy

### Intensive properties

Not

ex: density, temp,

### Change of $\phi$ of fluid dV

$$d\phi = \frac{\partial \phi}{\partial t} dt + \frac{\partial \phi}{\partial x_1} dx_1 + \frac{\partial \phi}{\partial x_2} dx_2 + \frac{\partial \phi}{\partial x_3} dx_3$$

$$dx_i = V_i dt$$

$$\frac{d\phi}{dt} = \frac{\partial \phi}{\partial t} + \frac{\partial \phi}{\partial x_1} V_1 + \frac{\partial \phi}{\partial x_2} V_2 + \frac{\partial \phi}{\partial x_3} V_3$$

$$= \frac{d\phi}{dt} + (\mathbf{V} \cdot \nabla) \phi$$

$$= \frac{\partial \phi}{\partial t} + \frac{\partial \phi}{\partial x_i} V_i$$

# Fluid Dynamics:

Density :

$$\frac{d\rho}{dt} = \frac{\partial \rho}{\partial t} \bigg|_p + \frac{\partial \rho}{\partial t} \bigg|_T \frac{dp}{dt}$$

$$\frac{dT}{dt} = \frac{\dot{E}_{tot}}{m c_v} - \frac{\sum \dot{m}}{m} (T - T_{ref})$$

$$\frac{dp}{dt} = \beta \left( \frac{\sum \dot{m}}{m} - \frac{1}{V} \frac{dV}{dt} - \frac{\alpha_T}{\beta} \frac{dT}{dt} \right)$$