

Assignment on pipe flows and losses in fittings

6.21 In Tinyland, houses are less than a foot high! The rainfall is laminar! The drainpipe in Fig. P6.21 is only 2 mm in diameter. (a) When the gutter is full, what is the rate of draining? (b) The gutter is designed for a sudden rainstorm of up to 5 mm per hour. For this condition, what is the maximum roof area that can be drained successfully? (c) What is Re_d ?

Solution: If the velocity at the gutter surface is neglected, the energy equation reduces to

$$\Delta z = \frac{V^2}{2g} + h_f, \quad \text{where } h_{f,\text{laminar}} = \frac{32\mu LV}{\rho g d^2}$$

For water, take $\rho = 998 \text{ kg/m}^3$ and $\mu = 0.001 \text{ kg/m}\cdot\text{s}$. (a) With Δz known, this is a quadratic equation for the pipe velocity V :

$$0.2 \text{ m} = \frac{V^2}{2(9.81 \text{ m/s}^2)} + \frac{32(0.001 \text{ kg/m}\cdot\text{s})(0.2 \text{ m})V}{(998 \text{ kg/m}^3)(9.81 \text{ m/s}^2)(0.002 \text{ m})^2},$$

$$\text{or: } 0.051V^2 + 0.1634V - 0.2 = 0, \quad \text{Solve for } V = 0.945 \frac{\text{m}}{\text{s}},$$

$$Q = \frac{\pi}{4}(0.002 \text{ m})^2 \left(0.945 \frac{\text{m}}{\text{s}} \right) = 2.97E-6 \frac{\text{m}^3}{\text{s}} = \mathbf{0.0107 \frac{\text{m}^3}{\text{h}}} \quad \text{Ans. (a)}$$

(b) The roof area needed for maximum rainfall is $0.0107 \text{ m}^3/\text{h} \div 0.005 \text{ m/h} = \mathbf{2.14 \text{ m}^2}$. *Ans. (b)*

(c) The Reynolds number of the gutter is $Re_d = (998)(0.945)(0.002)/(0.001) = \mathbf{1890}$ laminar. *Ans. (c)*

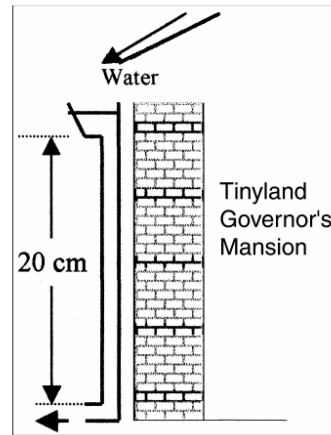


Fig. P6.21

6.28 For straightening and smoothing an airflow in a 50-cm-diameter duct, the duct is packed with a “honeycomb” of thin straws of length 30 cm and diameter 4 mm, as in Fig. P6.28. The inlet flow is air at 110 kPa and 20°C, moving at an average velocity of 6 m/s. Estimate the pressure drop across the honeycomb.

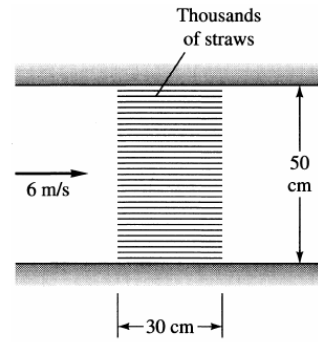


Fig. P6.28

Solution: For air at 20°C, take $\mu \approx 1.8\text{E-}5 \text{ kg/m}\cdot\text{s}$ and $\rho = 1.31 \text{ kg/m}^3$. There would be approximately 12000 straws, but each one would see the average velocity of 6 m/s. Thus

$$\Delta p_{\text{laminar}} = \frac{32\mu LV}{d^2} = \frac{32(1.8\text{E-}5)(0.3)(6.0)}{(0.004)^2} \approx \mathbf{65 \text{ Pa}} \quad \text{Ans.}$$

Check $\text{Re} = \rho V d / \mu = (1.31)(6.0)(0.004) / (1.8\text{E-}5) \approx 1750$ OK, laminar flow.

6.47 The gutter and smooth drainpipe in Fig. P6.47 remove rainwater from the roof of a building. The smooth drainpipe is 7 cm in diameter. (a) When the gutter is full, estimate the rate of draining. (b) The gutter is designed for a sudden rainstorm of up to 5 inches per hour. For this condition, what is the maximum roof area that can be drained successfully?

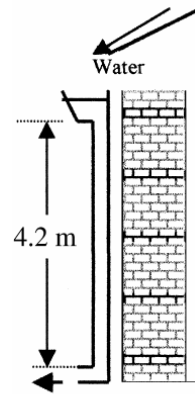


Fig. P6.47

Solution: If the velocity at the gutter surface is neglected, the energy equation reduces to

$$\Delta z = \frac{V^2}{2g} + h_f, \quad h_f = f \frac{L}{d} \frac{V^2}{2g}, \quad \text{solve } V^2 = \frac{2g\Delta z}{1 + fL/d} = \frac{2(9.81)(4.2)}{1 + f(4.2/0.07)}$$

For water, take $\rho = 998 \text{ kg/m}^3$ and $\mu = 0.001 \text{ kg/m}\cdot\text{s}$. Guess $f \approx 0.02$ to obtain the velocity estimate $V \approx 6 \text{ m/s}$ above. Then $\text{Re} \approx \rho V d / \mu \approx (998)(6)(0.07) / (0.001) \approx 428,000$ (turbulent). Then, for a smooth pipe, $f \approx 0.0135$, and V is changed slightly to 6.74 m/s. After convergence, we obtain

$$V = 6.77 \text{ m/s}, \quad Q = V(\pi/4)(0.07)^2 = \mathbf{0.026 \text{ m}^3/\text{s}} \quad \text{Ans. (a)}$$

A rainfall of 5 in/h = (5/12 ft/h)(0.3048 m/ft)/(3600 s/h) = 0.0000353 m/s. The required roof area is

$$A_{\text{roof}} = Q_{\text{drain}} / V_{\text{rain}} = (0.026 \text{ m}^3/\text{s}) / 0.0000353 \text{ m/s} \approx \mathbf{740 \text{ m}^2} \quad \text{Ans. (b)}$$

6.55 The reservoirs in Fig. P6.55 contain water at 20°C. If the pipe is smooth with $L = 4500$ m and $d = 4$ cm, what will the flow rate in m^3/h be for $\Delta z = 100$ m?

Solution: For water at 20°C, take $\rho = 998 \text{ kg/m}^3$ and $\mu = 0.001 \text{ kg/m}\cdot\text{s}$. The energy equation from surface 1 to surface 2 gives

$$p_1 = p_2 \quad \text{and} \quad V_1 = V_2,$$

$$\text{thus} \quad h_f = z_1 - z_2 = 100 \text{ m}$$

$$\text{Then } 100 \text{ m} = f \left(\frac{4500}{0.04} \right) \frac{V^2}{2(9.81)}, \quad \text{or} \quad fV^2 \approx 0.01744$$

Iterate with an initial guess of $f \approx 0.02$, calculating V and Re and improving the guess:

$$V \approx \left(\frac{0.01744}{0.02} \right)^{1/2} \approx 0.934 \frac{\text{m}}{\text{s}}, \quad Re \approx \frac{998(0.934)(0.04)}{0.001} \approx 37300, \quad f_{\text{smooth}} \approx 0.0224$$

$$V_{\text{better}} \approx \left(\frac{0.01744}{0.0224} \right)^{1/2} \approx 0.883 \frac{\text{m}}{\text{s}}, \quad Re_{\text{better}} \approx 35300, \quad f_{\text{better}} \approx 0.0226, \text{ etc.....}$$

This process converges to

$$f = 0.0227, \quad Re = 35000, \quad V = 0.877 \text{ m/s}, \quad Q \approx 0.0011 \text{ m}^3/\text{s} \approx \mathbf{4.0 \text{ m}^3/\text{h}}. \quad \text{Ans.}$$

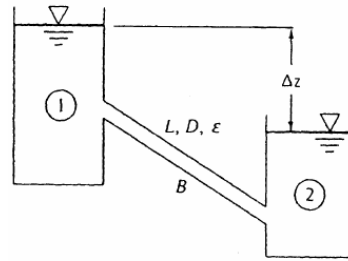


Fig. P6.55

P6.99 In Sec. 6.11 it was mentioned

that Roman aqueduct customers obtained

extra water by attaching a diffuser to their

pipe exits. Fig. P6.99 shows a simulation:

a smooth inlet pipe, with and without a 15°

diffuser expanding to a 5-cm-diameter exit.

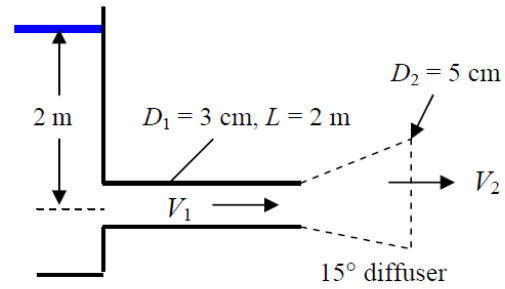


Fig. P6.99

The pipe entrance is sharp-edged.

Calculate the flow rate (a) without, and (b) with the diffuser.

Solution: For water at 20°C, take $\rho = 998 \text{ kg/m}^3$ and $\mu = 0.001 \text{ kg/m}\cdot\text{s}$. The energy equation between the aqueduct surface and the pipe exit yields

$$z_{surf} = z_2 + \frac{V_2^2}{2g} + h_f + \Sigma h_m = z_2 + \frac{V_2^2}{2g} + \frac{V_1^2}{2g} \left(f \frac{L}{D_1} + K_{entrance} + K_{diffuser} \right)$$

(a) Without the diffuser, $K_{diff} = 0$, and $V_1 = V_2$. For a sharp edge, take $K_{ent} = 0.5$. We obtain

$$2m = \frac{V_1^2}{2g} \left(1 + f \frac{2m}{0.03m} + 0.5 \right), \quad \text{with } f = fcn(\text{Re} = \rho V_1 D_1 / \mu)$$

Solve: $\text{Re} = 115,000$; $f = 0.0175$; $V_1 = 4.48 \text{ m/s}$; $Q_{without} = 0.00271 \text{ m}^3/\text{s}$ *Ans.(a)*

(b) *With* the diffuser, from Fig. 6.23, for $D_1/D_2 = 3/5 = 0.6$ and $2\theta = 15^\circ$, read $K_{\text{diffuser}} \approx 0.2$.

From one-dimensional continuity, $V_2 = V_1(3/5)^2 = 0.36V_1$. The energy equation becomes

$$2m = \frac{(0.36V_1)^2}{2g} + \frac{V_1^2}{2g} \left(1 + f \frac{2m}{0.03m} + 0.5 + 0.2\right)$$

$$\text{Solve: } \text{Re} = 134,000 ; f = 0.0169 ; V_1 = 3.84 \text{ m/s} ; Q_{\text{with}} = 0.00316 \text{ m}^3/\text{s} \quad \text{Ans. (b)}$$

Adding the diffuser increases the flow rate by **17%**. [NOTE: Don't know if the Romans did this, but a well-rounded entrance, $K_{\text{ent}} = 0.05$, would increase the flow rate by another 15%.]

6.116 For the series-parallel system of Fig. P6.116, all pipes are 8-cm-diameter asphalted cast iron. If the total pressure drop $p_1 - p_2 = 750$ kPa, find the resulting flow rate Q m^3/h for water at 20°C . Neglect minor losses.

Solution: For water at 20°C , take $\rho = 998$ kg/m^3 and $\mu = 0.001$ $\text{kg}/\text{m}\cdot\text{s}$. For

asphalted cast iron, $\varepsilon \approx 0.12$ mm, hence $\varepsilon/d = 0.12/80 \approx 0.0015$ for all three pipes. The head loss is the same through AC and BC:

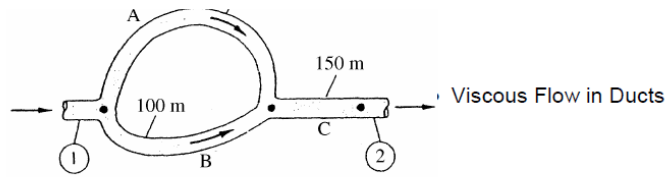


Fig. P6.116

$$\frac{\Delta p}{\rho g} = h_{fA} + h_{fC} = h_{fB} + h_{fC} = \left(f \frac{L}{d} \frac{V^2}{2g} \right)_A + \left(f \frac{L}{d} \frac{V^2}{2g} \right)_C = \left(f \frac{L}{d} \frac{V^2}{2g} \right)_B + \left(f \frac{L}{d} \frac{V^2}{2g} \right)_C$$

Since d is the same, $V_A + V_B = V_C$ and f_A , f_B , f_C are found from the Moody chart. Cancel g and introduce the given data:

$$\frac{750000}{998} = f_A \frac{250}{0.08} \frac{V_A^2}{2} + f_C \frac{150}{0.08} \frac{V_C^2}{2} = f_B \frac{100}{0.08} \frac{V_B^2}{2} + f_C \frac{150}{0.08} \frac{V_C^2}{2}, \quad V_A + V_B = V_C$$

Guess $f_{\text{rough}} \approx 0.022$ and solve laboriously: $V_A \approx 2.09 \frac{\text{m}}{\text{s}}$, $V_B \approx 3.31 \frac{\text{m}}{\text{s}}$, $V_C \approx 5.40 \frac{\text{m}}{\text{s}}$

Now compute $\text{Re}_A \approx 167000$, $f_A \approx 0.0230$, $\text{Re}_B \approx 264000$, $f_B \approx 0.0226$, $\text{Re}_C \approx 431000$, and $f_C \approx 0.0222$. Repeat the head loss iteration and we converge: $V_A \approx 2.06 \text{ m/s}$, $V_B \approx 3.29 \text{ m/s}$, $V_C \approx 5.35 \text{ m/s}$, $Q = (\pi/4)(0.08)^2(5.35) \approx \mathbf{0.0269 \text{ m}^3/\text{s}}$. *Ans.*