

We are given a control surface as shown in fig, having unit depth into the page. Now, we consider the C.V. to be made of two faces namely O and ②. As, the flow is we incompressible and the C.V. is fired and non-deforming.

$$\frac{dPV_{e.v.}}{dt} = \frac{\partial}{\partial t} \iiint PdV + \iint P(\vec{v} \cdot \hat{n}) ds = 0$$

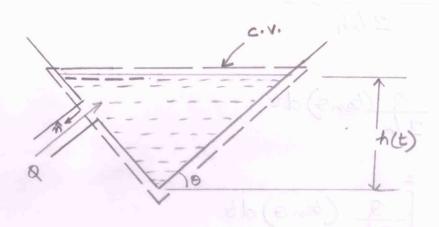
$$\Rightarrow$$
 $\oint (\vec{v}, \vec{n}) ds = 0.$

$$\iint_{S} (\vec{v} \cdot \hat{n}) \beta ds \Big|_{1} + \iint_{S} (\vec{v} \cdot \hat{n}) \beta ds \Big|_{2} = 0$$

As, the flow is steady, so to the surface 1 would be equal to the mans flux from the surface 2.

$$\dot{m}_1 + \dot{m}_2 = 0$$





Consider the control volume as shown, which is fixed as a whole and is deforming for chaning its dimensions in time.

By Reynolds transport theorm:

$$\frac{\partial}{\partial t} \iiint_{t} Pdt + \iint_{s} P(\vec{v} \cdot \hat{n}) ds = 0$$

$$\frac{\partial}{\partial t} \iiint_{t} dt + \oint_{s} (\vec{v} \cdot \hat{n}) ds = 0$$
 (as the flow is incompressible)

$$\frac{d}{dt} \left[+ \frac{1}{2} \left[+ \frac{$$

$$\frac{d}{dt} \left[\frac{1}{2} \times b \times h \times \frac{2h}{\tan \theta} \right] - Q = 0$$

(the base of the triangle is
$$\frac{2h}{\tan \theta}$$
)

$$\frac{d}{dt} \left(\frac{b h^2}{\tan \alpha} \right) - Q = 0$$

$$\frac{b}{\tan \theta} = 2h \frac{dh}{dt} - Q = 0$$

$$\Rightarrow \frac{dh}{dt} = \frac{Q(\tan \theta)}{2bh}$$

$$\frac{dh}{dt} = \frac{Q(\tan 0)}{2bh}$$

$$\frac{hdh}{dt} = \frac{Q(\tan 0)}{2}dt$$

$$\frac{hdh}{h} = \frac{Q(tano)}{2b}dt$$

$$\int_{h}^{2} \frac{dh}{dh} = \int_{1}^{2} \frac{Q}{2h} (\tan \theta) d\theta$$

$$\left|\frac{h^2}{2}\right|^2 = \frac{Q}{2h}(\tan \theta)\left|\frac{1}{t}\right|^2$$

$$\frac{h_2^2 - h_1^2}{2} = \frac{Q}{2b} \left(\tan \theta \right) \left(\frac{1}{2} - \frac{1}{2} \right) \left(\frac{1}{2}$$

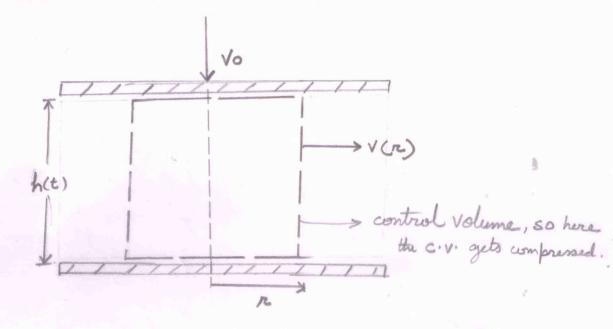
$$\frac{\left(h_2^2 - h_1^2\right)b}{Q\left(\tan \Theta\right)} = t_2 - t_1$$

$$\Rightarrow t_2 - t_1 = b (h_2^2 - h_1^2)$$

$$\Rightarrow t_2 - t_1 = \underbrace{b \left(h_2^2 - h_1^2\right)}_{\text{Q (tan o)}}$$

$$\Rightarrow d_{\text{provided with possed with p$$

Soln 3



$$\frac{\partial}{\partial t} \iiint_{Y} P dV + \iint_{S} P(\vec{v} \cdot \hat{n}) ds = 0$$

As, the flow is incompresible,

$$\frac{\partial}{\partial t} \iiint_{t} dt + \iint_{s} (\vec{v} \cdot \hat{n}) ds = 0$$

$$\frac{d}{dt} \left[\pi r^2 h \right] + \left(2\pi r h \right) V(r) = 0$$

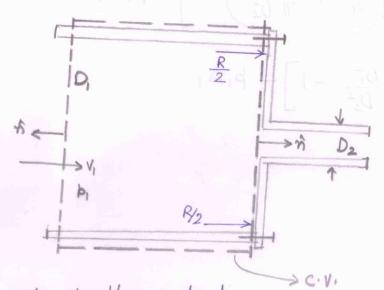
$$\frac{dh}{dt} + \frac{2h}{\pi} V(\pi) = 0$$

As,
$$-\frac{dh}{dt} = V_0$$

$$= \rangle - V_0 + \frac{2h}{\pi} V(\pi) = 0$$

$$V(r) = \frac{V_0 R}{2h}$$

Soln 4



Continuity: - As, the flow is steady,

$$\frac{\partial}{\partial t} \int P dt + \oint P(\vec{V} \cdot \hat{n}) ds = 0$$

$$\bigoplus_{c \in S} \mathcal{P}(\vec{V} \cdot \hat{n}) ds = 0$$

$$\oint_{c:s} (\vec{v} \cdot \hat{n}) ds = 0 \qquad (as flow is incompressible)$$

$$V_1A_1 = V_2A_2$$
 where $A_1 = \frac{TI}{4}D_1^2$ and $A_2 = \frac{TI}{4}D_2^2$

Momentum conservation: $-\frac{R}{2} + \frac{R}{2} = F_{\text{ent}}$ (Sum of the bolt reactions will be equal to the total entired $P_1A_1 + F_{\text{ext}} = -A_1 P V_1^2 + P V_2^2 A_2^2$ force).

Fext =
$$9V_1^2 A_1 \left[\frac{\pi}{4} D_1^2 \times \frac{4}{\pi D_2^2} - 1 \right] - b_1 A_1$$

$$\Rightarrow \text{Fext} = 9V_1^2 A_1 \left[\frac{D_1^2}{D_2^2} - 1 \right] - b_1 A_1$$

$$\Rightarrow \text{deads a wide a wide a series of the series of$$

Solm 5 $u = U_{0} \begin{bmatrix} 24 \\ 8 \\ -4 \end{bmatrix}$ $u = U_{0} \begin{bmatrix} 24 \\ 8 \\ 8^{2} \end{bmatrix}$ $u = U_{0} \begin{bmatrix} 24 \\ 8 \\ 8^{2} \end{bmatrix}$

$$P(hb)U_{0} = \int_{0}^{8} PU_{0} \left[\frac{2y}{8} - \frac{y^{2}}{8^{2}} \right] b dy$$

$$h = 8 - \frac{8}{3} = \frac{28}{3}$$

$$\Rightarrow h = \frac{2}{3}8$$

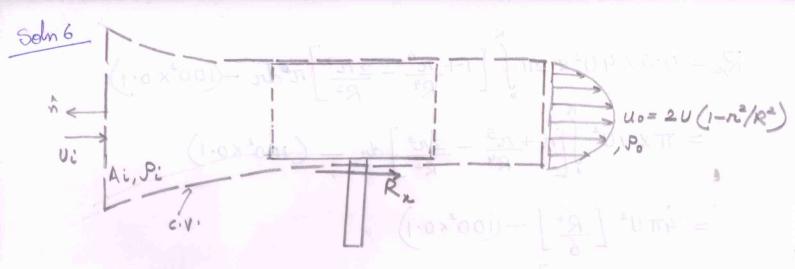
Momentum conservation:

$$-\operatorname{Fext} = \oint \mathcal{P}(\vec{v}, \hat{n}) \vec{v} ds$$

$$-F_{\text{ent}} = -90^{2} \left(\frac{2}{3}8\right) h + 90^{2} \int_{82}^{8} \left[\frac{4y^{2}}{8^{2}} + \frac{y^{4}}{8^{4}} - \frac{4y^{3}}{8^{3}}\right] dy$$

$$- \text{ Fent} = - 90^{2} \left(\frac{28}{3} \right) b + 90^{2} \left[\frac{4y^{3}}{38^{2}} + \frac{y^{5}}{58^{4}} - \frac{4y^{9}}{48^{3}} \right]^{8}$$

$$-\text{Fent} = PU_{\infty}^{2} \ln \left[-\frac{28}{15} \right]$$



Ui = 100m/s, P, = 1kg/m3, A, = 0.1m2, U = 600m/s, Po = 0.5 kg/m3

(a) average velocity at jet enit:
$$=$$

Venit average $=$

$$\int_{0}^{R} 1200 \left(1 - \frac{\pi^{2}}{R^{2}}\right) 2\pi \pi d\tau$$

TT R^{2}

Venitaurage = 600 m/s

$$Ae = \frac{10}{600 \times 0.5}$$

By momentum equation: - R
$$R_{x} = \int 0.5 \left[2U \left(1 - \frac{R^2}{R^2} \right) \right]^2 2\pi R dr - \left(1 \times 100^2 \times 0.1 \right)$$

$$R_{x} = 0.5 \times 40^{2} \times 2\pi \int_{0}^{R} \left[1 + \frac{\pi^{4}}{R^{4}} - \frac{2\pi^{2}}{R^{2}} \right] \pi d\pi - (100^{2} \times 0.1)$$

$$= \pi \times 40^{2} \int_{0}^{R} \pi + \frac{\pi^{5}}{R^{4}} - \frac{2\pi^{3}}{R^{2}} d\pi - (100^{2} \times 0.1)$$

$$= 4\pi U^{2} \left[\frac{R^{2}}{6} \right] - (100^{2} \times 0.1)$$

$$= \left[\frac{4}{6} \times 600^{2} \times \frac{10}{600 \times 0.5} \right] - 1000$$

$$= \frac{4}{6} \times 600^{2} \times \frac{10}{600 \times 0.5} - 1000$$

$$= 7000 \text{ kg/m/s}^{2}$$

$$R_{x} = 7000 \text{ N}$$
So, the unit force will be $\vec{F} = -R_{x}\hat{i} = -7000 \text{ N} \hat{i}$
Thrust with constant or uniform exit velocity:

c) Thrust with constant or uniform enit velocity:-

$$R_{n} = \int_{e}^{2} U_{e}^{2} A_{e} - \int_{e}^{2} U_{e}^{2} A_{e}^{2}$$

$$= 0.5 \times 600^{2} \times \frac{10}{600 \times 0.5} - (00^{2} \times 0.1)$$

$$A_{3} = \frac{10}{600 \, \text{k o} \cdot 5}$$