# Sensitivity analysis and uncertainty in CFD simulations of multiphase flow

#### Partners & researchers involved:

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eDF	P. Noyret, E. Fayolle, JP. Minier	

#### **Objectives of the project**



Development of an open simulation platform for the simulation of scientific workflows

Simulation platform

Aim: Regroup & integrate software in a single platform

Tool: Salome

Common Data Model (CDM)

Aim: Setup scientific workflows using a single framework

Tool: Eficas

Demonstration on one selected workflow including SA & UQ

Aim: Illustrate the CDM and platform on a two-phase flow simulation

Tools: Code\_Saturne, OpenTurn



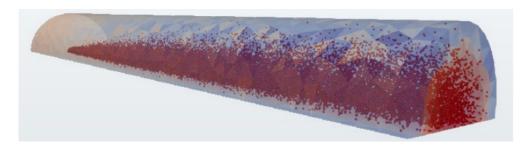
## **Presentation layout**

- Case studied: workflow
- Methodology & tools
- Results

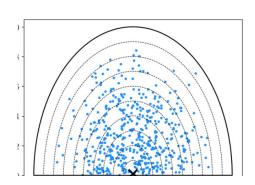


## Scientific workflow for multiphase flow

- Case studied
  - Point-source particle dispersion in a turbulent pipe flow



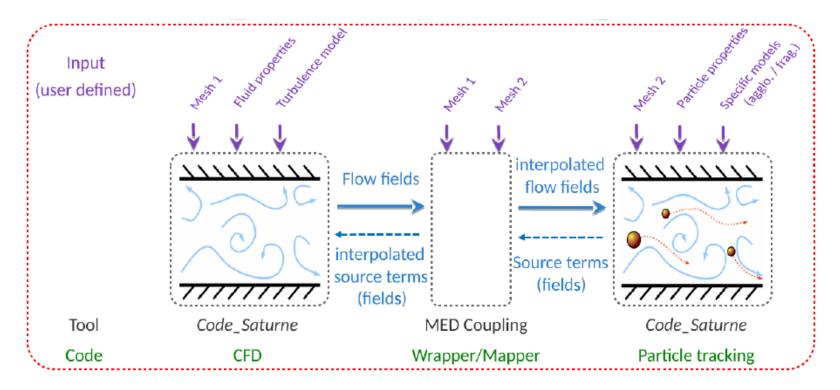
- Interest
  - Analysis of the dispersion at the outlet
  - Calibration of a model





## Scientific workflow for multiphase flow

- Definition of the workflow
  - Three steps involved





## **Workflow specification**

Fluid Wrapper Particle phase /Mapper phase

- Fluid phase
  - Inputs:
    - Physical parameters:

• Density:  $\rho = 1.17862 \text{ kg/m}^3$ 

• Temperature: T = 293.15 K

**UQ input** • Velocity: U = 1 to 4 m/s

- Model parameters:
  - Turbulence model: Rij-ɛ
- Numerical parameters:

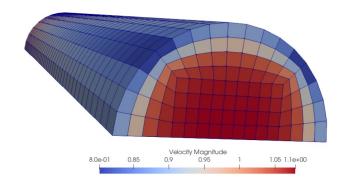
• Geometry: 1 m length, 0.1 m radius

• Mesh: Hexahedric, 15x40 resolution

• Time discretisation: 100 iterations,  $\Delta t = 0.1 \text{ s}$ 

- Software used: Code\_Saturne
- Output:

• Flow fields: pressure, velocity, Rij, epsilon

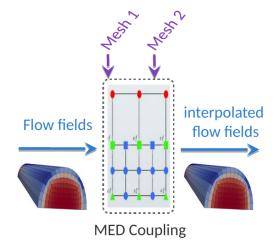




#### **Workflow specification**

Fluid Wrapper Particle phase / Mapper

- Wrapper/Mapper
  - Inputs:
    - Model parameters:
      - Interpolation: P0
    - Numerical parameters:
      - Mesh 1: Hexahedric, 15x40 resolution
      - Mesh 2: Hexahedric, 20x60 resolution
      - Exchange frequency: At initialisation (frozen field)
  - Software used:
    MED Coupling
  - Output:
    - Interpolated fields: pressure, velocity, Rij, epsilon





#### **Workflow specification**

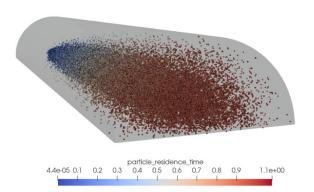
- Particle phase
  - Inputs
    - Physical parameters

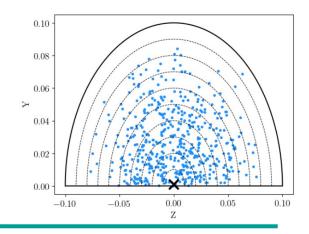
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- Particle radius:  $R = 1 \mu m \text{ to } 1 \text{ mm}$
- Particle shape: Sphere

- **UQ input** Mass flow rate: 100 to 1000 part. injected / Δt
  - Model parameters
    - Transport model: Stochastic Lagrangian model
  - Numerical parameters
    - Geometry: 1 m length, 0.1 m radius
    - Mesh: Hexahedric, 20x60 resolution
    - Time discretisation: 500 iterations,  $\Delta t = 0.01$  s
  - Software used: Code\_Saturne
  - **Output:**

UQ outputConcentration at outlet





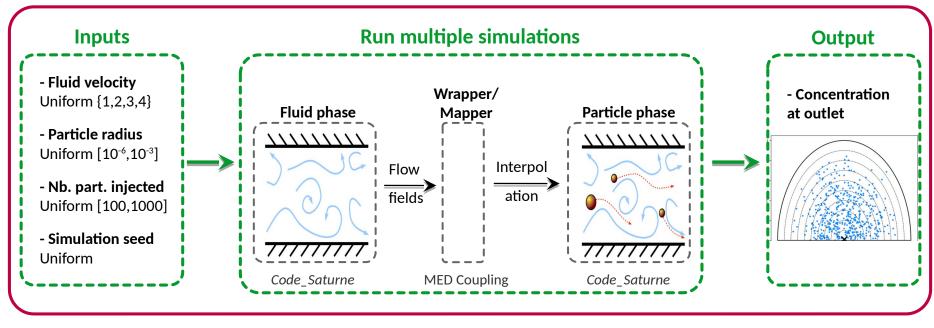


## Scientific workflow for multiphase flow

Summary of the workflow

Case studied: Particle dispersion in a turbulent pipe flow

Analysis: Sensitivity analysis & calibration of a model



(OpenTurns)

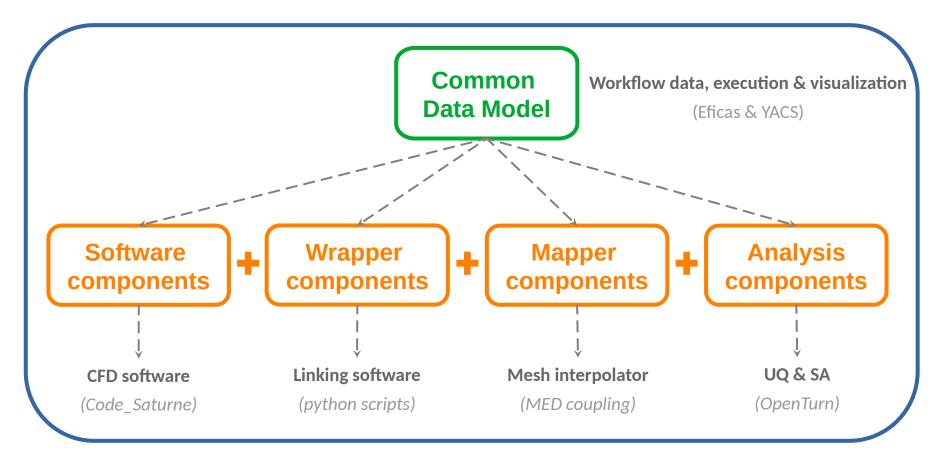


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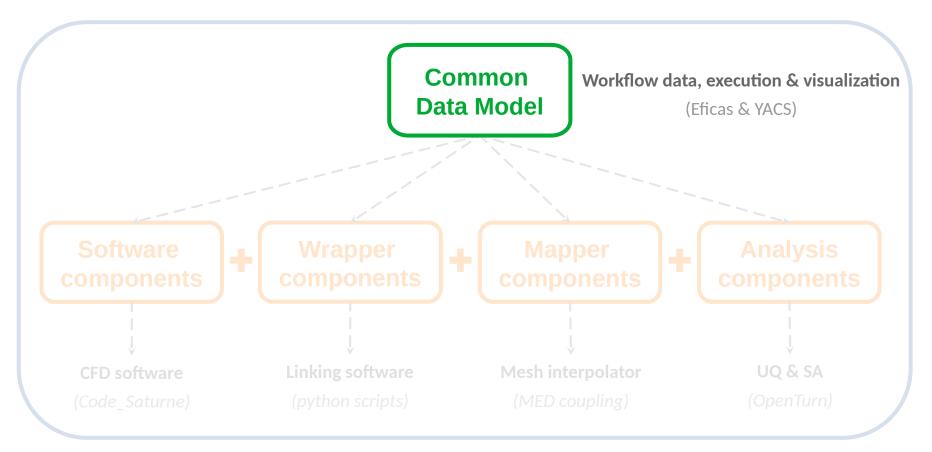
## VIMMP open simulation platform



**Salome Platform** 



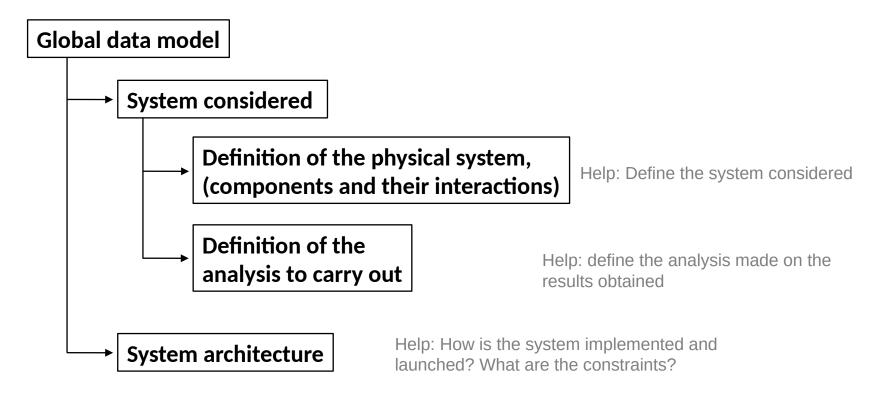
#### VIMMP open simulation platform



**Salome Platform** 

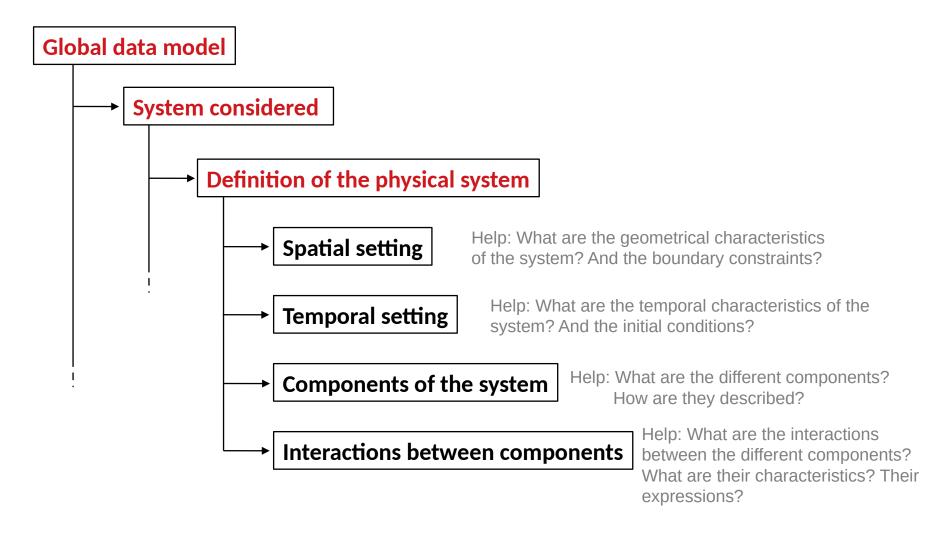


#### **Common Data Model: overview**





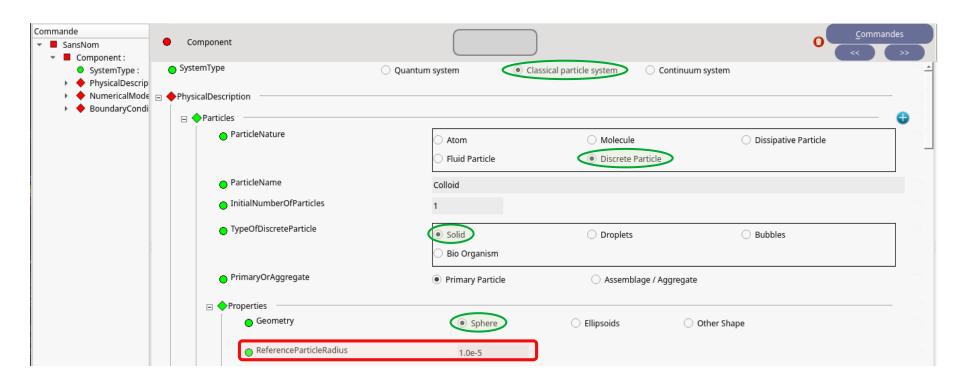
#### **Common Data Model: overview**





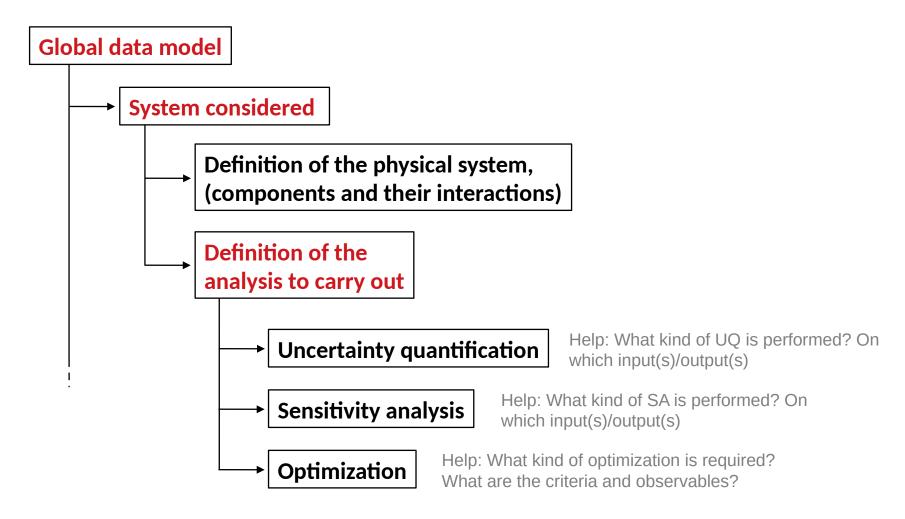
#### **Common Data Model: implementation**

- Implementation of the CDM in Eficas
  - Example (CDM filled for the current workflow)



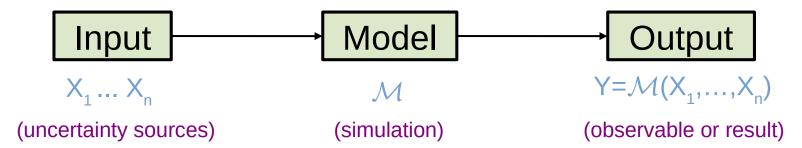


#### **Common Data Model: overview**





#### Data analysis tools



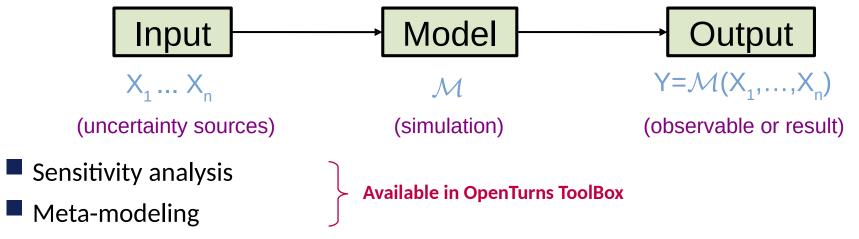
- Sensitivity analysis
  - Principle:

    Analyze the relative importance of each uncertainty source on the result
  - Ranking methods used:
    - First order Sobol indice
      - Variance-based indicator
      - Estimates the part of variance of Y due to each component X<sub>i</sub>

- Total order Sobol indice
  - Absolute ranking

$$S_i = rac{\mathsf{Var}[\mathbb{E}[Y|X_i]]}{\mathsf{Var}[Y]}$$

## Data analysis tools



- Principle:
  Build an analytic approximation of the response of a given model
- Methods used:
  - Polynomial chaos expansion
    - Spectral decomposition of random variables on the basis of orthogonal polynomials



#### **Current methodology**

Automatic launching with python script

Generation of mesh (gmsh)

Simulation of the 'fluid phase' (Code\_Saturne)

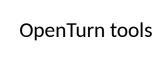
Mesh interpolation (MED Coupling)

Simulation of the 'particle phase' (Code\_Saturne)

Otwrappy for automated launching on parallel processors

Post-treatment analysis

- Sensitivity analysis
- Polynomial chaos metamodel
- Bayesian calibration of a fit model



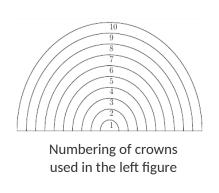


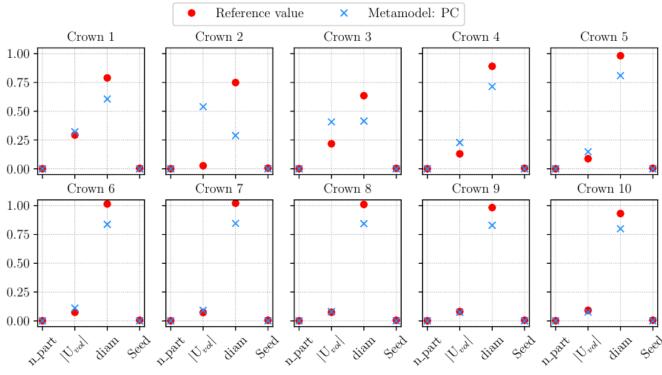
## **Presentation layout**

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- Ranking sensitivity through Sobol indices
  - Sample size: 13 200 workflow runs

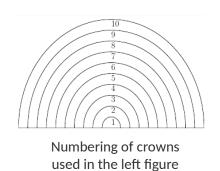


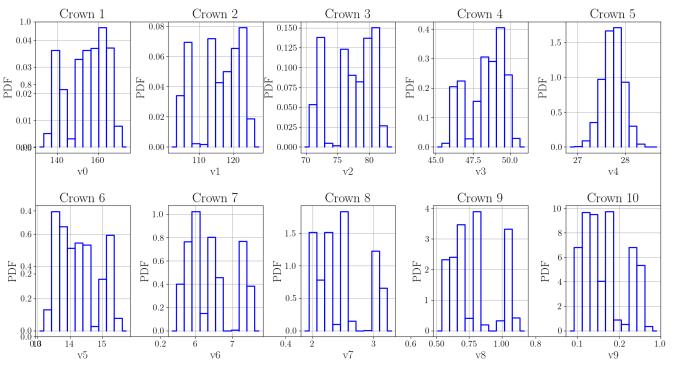


- Ranking obtained:
  - 1) Particle diameter 2) Fluid velocity
- 3) Nb. Injected Particles



- Calibration of a model
  - Analysis of simulations with monodispersed radius



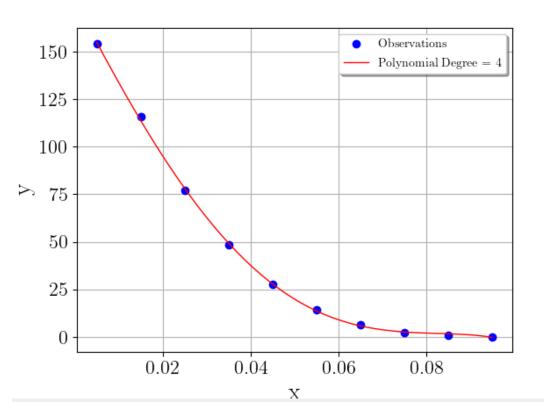


PDF of relative concentrations obtained in the various crowns



#### Calibration of a model

Analysis of simulations with monodispersed radius



Polynomial curve fitting

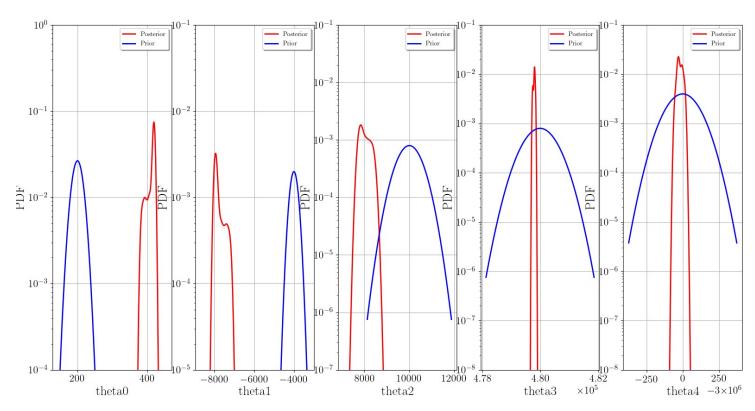
$$f(x) = a_0 + a_1 x + a_2 x^2 + a_3 x^3 + a_4 x^4$$

$\mathbf{a}_{0}$	1.76 x 10 <sup>2</sup>
a <sub>1</sub>	-4.46 x 10 <sup>3</sup>
$a_2$	1.05 x 10 <sup>4</sup>
$a_3$	4.75 x 10 <sup>5</sup>
$a_4$	-3.14 x 10 <sup>6</sup>

Polynomial curve fitting



- Calibration of a model
  - Analysis of simulations with monodispersed radius
  - Bayesian calibration on simulations with polydispersed radius





#### Conclusions

- Use of Salome tools for workflow implementation & analysis
- Data analysis
  - Results vary with the observable
    - → Requires a careful supervision (definition of inputs and outputs)!
  - Computationally-expensive workflow simulations
  - Calibration of a model

#### Perspectives

- Uncertainty quantification on particle diameter
- Resorting to several meta-modelling tools to optimize the overall computational efficiency



## Thank you for your attention





## Detail on the numerical model

#### Particle motion

- Lagrangian description Choice of a state vector: (position  $X_{p,i}$ , velocity  $U_{p,i}$ , fluid velocity  $U_{s,i}$ )
- Langevin equation for transport

$$dx_{p,i} = U_{p,i}dt$$

$$dU_{p,i} = \frac{U_{s,i} - U_{p,i}}{\tau_p}dt + K_{Bro}dW_i'$$

$$dU_{s,i} = A_i(t, U_{s,i})dt + B_i(t, U_{s,i})dW_i$$

with the relaxation time (drag force)

$$\tau_p = \frac{4\rho_p d_p}{3\rho_f C_D |U_R|} \xrightarrow{\rho_p \gg \rho_f} \frac{\rho_p d_p^2}{18\rho_f}$$

diffusion coefficient (Brownian motion)

$$K_{Br} = \sqrt{\frac{2k_BT}{m_p\tau_p}}$$

drift term (slow variations of U<sub>2</sub>)

$$A_{i}(t, U_{s,i}) = -\frac{1}{\rho_{f}} \frac{\partial \langle P \rangle}{\partial x_{i}} + (\langle U_{p,j} \rangle - \langle U_{p,j} \rangle) \frac{\partial \langle U_{f,i} \rangle}{\partial x_{j}} - \frac{U_{s,i} - \langle U_{f,i} \rangle}{T_{L,i}^{*}}$$

diffusion term (rapid fluctuations of 
$$U_s$$
)  $B_i(t, U_{s,i}) = \sqrt{\langle \varepsilon \rangle (C_0 b_i \tilde{k}/k + 2/3(b_i \tilde{k}/k - 1))}$ 

Minier and Peirano, Physics Reports, 2001

