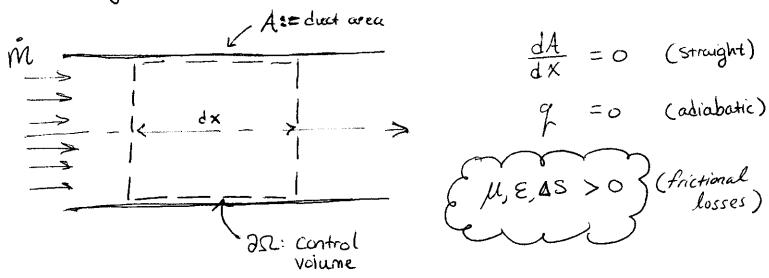
LECTURE 16: What if the walls are rough?

Now we want to look at the rough wall Simple problem. We will use a single Straight section of pipe as well.



* If we are going to consider frictional losses we mast consider shear at the wall. In

* We also wouldn't you believe it need a FANNING FRICTION FACTOR "F" which we will define as.

$$f = \frac{\tau_w}{\sqrt{2\rho V^2}} \tag{1}$$

Since we are working usually with NON-CIRCULAR DUCTS all diameters will be hydraulic 4A

$$\mathcal{D}_{H} = \frac{4A}{P}$$
 (2)

LECTURE 16:

For our mass balance of the control volume we can just use the previous result.

$$\frac{dA}{A} + \frac{d\rho}{\rho} + \frac{dV}{V} = 0$$

Like wise we will assure an ideal gas (as always).

The energy equation for a steady state gas problem is phrased in terms of outhalpy.

$$h + \frac{V^2}{2} = C_o$$
 (for all state)

All we need is a momentum relationship to tell us how pressure (forces) prescribe motion (velocity). $\Sigma F_{\text{ext}} = \int_{\partial \Omega} \rho A v(\vec{v} \cdot \vec{n}) dA$

Essentially all we do now is use all our equations to sub into our momentum relationship. But let's write them all out to see how one would come to this solution.

$$\frac{d\rho}{\rho} + \frac{dV}{V} = 0$$
 "continuity" (1)

$$P - \rho RT = 0$$
 "equation of state" (2)

$$dh + VdV = 0$$
 "energy" (3)

$$Ma^2 - \frac{V^2}{\gamma RT} = 0$$
 "Mach Definition" (4)

$$dP + \frac{4f}{D_{H}} \frac{\rho V^{2} dx + \rho V^{2} dV^{2}}{2} = 0 \quad \text{Momentum"}$$
 (6)

We have courtéem 7 unknowns and 6 equations!

This means we have to set a variable to get a solution.

What variable should we shoose to set them? Well again we are modeling the question...

How Does Friction Effect Flow?

So it's reasonable that to say we should set the friction term as an independent variable to probe it's effects on flow variables (V,P,P,T,S,Ma)!

Now this get's a little rough but let's hold onto a goal. In the end we are trying to relate everything to (Ma, 2).

$$\frac{dM_{\alpha}}{M_{\alpha}} = f_{1}(f) \qquad \frac{dP}{P} = f_{3}(f) \qquad ds = f_{5}(f)$$

$$\frac{dV}{V} = f_2(f) \qquad \frac{dT}{T} = f(f)$$

We are trying to determe these functions,
So we are going to combine all our equestions
by subbig and resubbing until we relate

You might as well see solving this many equation at least once in your undergrad. I will highlight common tricks and rational. We are going to use all (1)-(6) to arrive at 4. Fax = C (M, T) dM.

Start with momentum. Why!? Because it's the only one with the I term!

$$\frac{dP}{P} + \frac{4f}{D_H} \frac{\rho V^2}{2P} dx + \frac{\rho V^2}{2P} \frac{dV^2}{V^2} = 0$$

$$\frac{\partial V^2}{\partial P} \cdot \frac{4f}{D_{H}} dx = -\frac{dP}{P} - \frac{\rho V^2}{2P} \frac{dV^2}{V^2}$$
use (1)-(6) to get in terms of Ma.

We use (2) to get rid of dP/P. Take(d) of (2) dP = dpRT + dTpR //p

$$\frac{dP}{P} = \frac{dp}{p} + \frac{dT}{T}$$

Now we can use (1) to replace dp/p.

Where are we now that...

$$\frac{\partial V^2}{\partial P} \cdot \frac{\partial F}{\partial t} dx = \frac{dV}{V} - \frac{dT}{T} - \frac{\partial V^2}{\partial P} \frac{dV^2}{V^2}$$

Now we must get dy, dT, pv2, e dv2 terms into Ma 2 2 expressions.

Lecture 16

We use (3) and the definition of Cp (This is ow first trick but it makes sense as we want to go from th -> dT which is what Cp does!)

$$dh = -VdV = -\frac{1}{2}dV^2 = CpdT$$
 (divide by CpT)

 $d()$ basically Since $Cp = \frac{dh}{dT}$

behaves like FOR IDEAL GLAS!!!!

the derivative...

$$\frac{dT}{T} = -\frac{1}{2}\frac{dV^2}{QT} = \frac{-dV^2}{2QT}$$

We need to get to Ma relations so Go & T are problematic.

$$C_{p}-C_{R}=R \Rightarrow C_{p}=R+C_{R}=R+C_{p}-R)$$

$$C_{p}=\gamma R/(\gamma-1) \quad (a \ dirty \ trick...)$$

$$\frac{dT}{T}=\frac{-dV^{2}}{2}\frac{(\gamma-1)}{(\gamma RT)}=\frac{-dV^{2}}{V^{2}}Ma^{2}\frac{\gamma-1}{2}$$

Revaluate now...

$$\frac{eV^{2}}{2P} \cdot \frac{4F}{D_{+1}} dx = \frac{dV}{V} + \frac{\gamma_{-1}}{2} Ma^{2} \frac{dV^{2}}{V^{2}} - \frac{\rho V^{2}}{2P} \frac{dV^{2}}{V^{2}}$$

(use (4)

Leetwe 16

We now here to deal with this pV2/2P term...

$$\rho V^2 = \rho \frac{V^2}{rRT} rRT = r Ma^2 P$$
 (dirty trick...)

Revaluate..

$$\frac{4J}{D_{H}} dx = \frac{dV}{V} + \frac{\gamma - 1}{2} Ma^{2} \frac{dV^{2}}{V^{2}} - \frac{\gamma Ma^{2} P}{2P} \frac{dV^{2}}{V^{2}}$$
eliminatel pressure!!

Now we need to get dV^2/V^2 into Ma expressions abbell. Let's do a d() to (4) to build up dha/Ma from scratch.

$$dM\alpha^2 = d\left(\frac{V^2}{\gamma RT}\right) = \frac{dV^2 \gamma RT - \gamma R dT V^2}{(\gamma RT)^2}$$

$$M\alpha^2$$

$$\frac{dMa^{2}}{Ma^{2}} = \frac{dV^{2}}{\gamma RT Ma^{2}} - \frac{\gamma RV^{2} dT}{(\gamma RT)^{2} Ma^{2}}$$

$$= \frac{dV^2}{V^2} - \frac{dT}{T}$$
 (becomse $Ma^2 = \frac{V^2/\gamma RT}{T}$)

We also have an expression for dT/T thougho

$$\frac{dHa^{2}}{Ha^{2}} = \frac{dV^{2}}{V^{2}} + \frac{\gamma-1}{2} Ma^{2} \frac{dV^{2}}{V^{2}} = \left(1 + \frac{\gamma-1}{2} Ma^{2}\right) \frac{dV^{2}}{V^{2}} Box M$$

Revaluares

$$\frac{\rho V^2 + \frac{1}{2}}{2P} \frac{dV}{D_n} dx = \frac{dV}{V} + \left(\frac{r_{-1}}{2} Ma^2 - \frac{r Ma^2}{2}\right) \frac{dV^2}{V^2}$$

Lecture 18

Almost done! Fast need to take car of dV/V.

NPLY A =
$$\frac{dV}{V}$$
 + $\frac{dV}{V}$ + $\frac{$

This ode for Ma(x) tells us how losses effect speed as we traverse the rough duet. The ODE is found solving for dMa/dx!



We can use (**) to just back sub now for dp/p, dT/T, dp/p, and dV/V!

$$\frac{dV}{V} = \frac{\gamma Ma^2}{2(1-Ma^2)} \frac{4\mathcal{F}dx}{DH} \implies ODE for V(x)$$

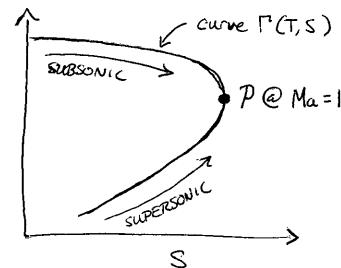
$$\frac{dP}{P} = -\frac{7Ma^{2}(1+[\Upsilon-1]Ma^{2})}{2(1-Ma^{2})} \frac{4fdx}{D+1} => ODE \text{ for } P(x)$$

$$\frac{dT}{T} = -\frac{\Upsilon(\Upsilon-1)Ma^4}{2(1-Ma^2)}\frac{4\mathcal{L}dx}{D_{+1}} \implies ODE \text{ for } T(x)$$

Lecture 16

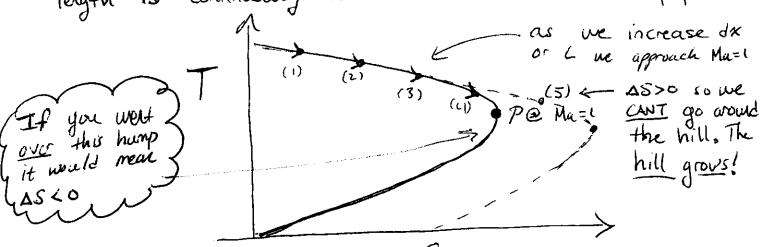
More often we actually use Fanno" Lines to analyze systems though I'll space you their derivations after that last round and just explain them.

- The cure I represents all the states possible for Famo Flow with a FIXED in and h.
- a given state at a given mass flowrate States MONE TO THE RIGHT.



I honestly believe this is the first time you have to apply the 2nd law to rationalize something. Usually its all 1st Law.

a) What happers if flow starts Ma < 1 and length is continually added to the section of pipe?



Lectur 16

As we approach Ma=1 the flow becomes choked by friction. A decrease in in results

THIS MEANS FOR A GLIVEN INLET ME CONDITION
THERE EXIST A LMAX PAST WHICH M DECREASES

* It is supprising that this compressible phenomena of "choking" or maxing out in accours even for a straight pipe due to frictional effects

The other game for Farro Flow is the use of Tables that tell the user about chatted flow

Ma T/T* P/P* Pt/Pt* V/V* FLmax/D

Where ()+ is a property at Ma=1.

Lecture 16 The <u>Values</u> in these tables come from Numerical Integration of our awful, disgusting vile, reprehensible equations we derived earlier. For example of Cupper limit we know is for Ma=12 $\int \frac{4J dx}{D_{+1}} = \int \frac{f(Ma) dMa}{\int \frac{for \ a \ discrete \ set}{of \ Ma \ values}}$ $M = Ma \in \{0.01, 0.02, \dots, 4.99, 5\}$ Vistar at any arbitrary the value $\frac{F L_{\text{max}}}{D_{+}} = \begin{cases} Make composter go brover. \end{cases}$ We do the exact same for the other relationships. $\int_{P}^{\infty} \frac{dP}{P} = \int_{Ma}^{\infty} \frac{2(1-(r-1)Ma^2)}{2(1-Ma^2)} \frac{4fdx}{D+1} \int_{Ma}^{\infty} \frac{express + his}{(**)}$ Ma number. $= \int \left[\frac{1 + (\gamma - 1) M \alpha^2}{1 + \frac{\gamma - 1}{2} M \alpha^2} \right] \frac{dM}{M} = -$ = } composter calculates for a bunch of Ma values} Lecture 16

Make sure you realize that you have to exponentiate the right-hand side after the composter is done integrating, because say you get a value of a for integration. $\int_{P}^{+} \frac{dP}{P} = \ln(P) \Big|_{P}^{+} = \ln\left(\frac{P_{+}}{P}\right) = \propto \Rightarrow \frac{P_{+}}{P} = e^{\kappa}$

SO WHEN CONNECTING 2 STATES OF GAS
FLOW THAT FALL IN THE FANNO ASSUMPTIONS
YOU MUST CONSULT A TABLE/DATABASE AND
RELATE A STATE TO A CHOKED/MAXIMUM FLOW

Some qualitative proporties that can be drawn from Fano Lines.

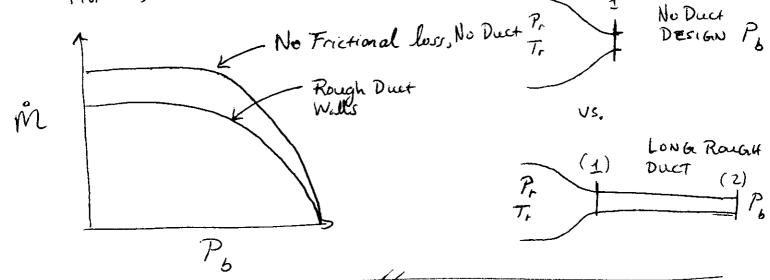
If Ma < 1 => T \ as Ma \ Tf Ma > 1 => T \ as Ma \

Some tricks using tables..., say you want to get from state 1 to 2 but don't have to consider ()* properties in your problem?

 $\frac{P_2/P_*}{P_1/P_*} = \frac{P_2}{P_1} \quad \text{dirty trick right...}$

Lecture 16 More on the "flow" of using tables is that you must specify the Ma value Or the friction term 4 & Lmax Dn to Start solving anything. This is because this will tell your which row you're on. Problem Types Lmax1-(2). (<u>1</u>) • 0.6 = Ma, Determine exit properties at (2)? $\alpha = \frac{\mathcal{F}L_{\text{max}_1}}{\mathcal{D}_{\text{H}}} = \frac{\mathcal{F}L_{\text{max}_2}}{\mathcal{D}_{\text{H}}} + \frac{\mathcal{F}L}{\mathcal{D}_{\text{H}}}$ * you can get this number from a table because Ma,=0.6 which specifies a now to lock up the FLmax2 = FLmax, - X * Since this specifies another row both States are now completely specified and both stater can be related by $\frac{()_2}{()_1} = \frac{()_2/()_*}{()_1/()_*}$

If we recall ow in graphs from less time this frictional loss is reducing in max from the ideal case.



However. would you believe that people actually figured out all those integrals? Thru crazy algebra you can show...i.e. (partial fractions)

$$\frac{4L_{\text{max}}}{D_{\text{H}}}\mathcal{F} = \frac{1-Ma^2}{\gamma_{\text{Ma}^2}} + \frac{\gamma+1}{2\gamma} \ln \left(\frac{(\gamma+1)Ma^2}{2(1+\frac{\gamma-1}{2}Ma^2)}\right) \tag{1}$$

$$\frac{V}{V_{*}} = M\alpha \left\{ \frac{\sigma+1}{2+(\sigma-1)M\alpha^{2}} \right\}^{1/2}$$

$$\frac{P}{P_{*}} = \left\{ \frac{\gamma + 1}{M_{\alpha}^{2} (2 + (\gamma - 1) M_{\alpha}^{2})} \right\}^{1/2}$$

$$\frac{T}{T} = \frac{\gamma+1}{\gamma+(\gamma-1)Ma^2}$$

$$\frac{0}{P_{*}} = \frac{V^{*}}{V} \quad \text{and} \quad \frac{S-S_{*}}{C_{P}} = \ln \left\{ M_{a}^{2} \right\} \left\{ \frac{r_{+1}}{M_{a}^{2} [2+(r_{-1})M_{a}^{2}]} \right\}^{\frac{r_{+1}}{2r}}$$

(2)

(4)