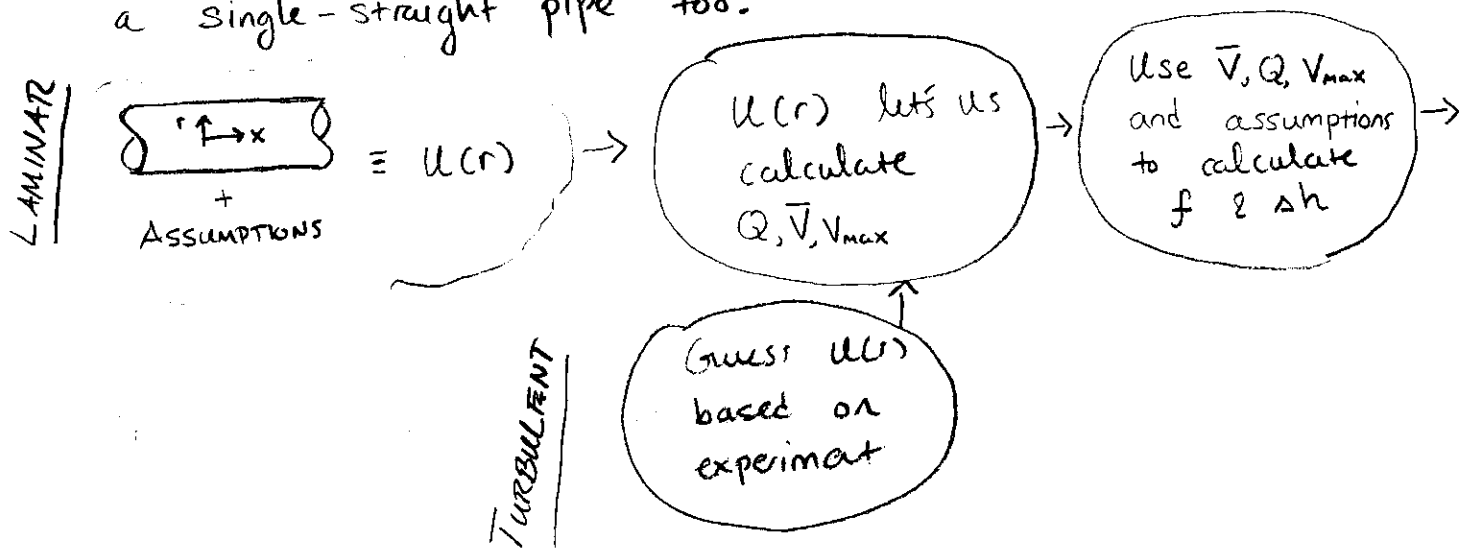
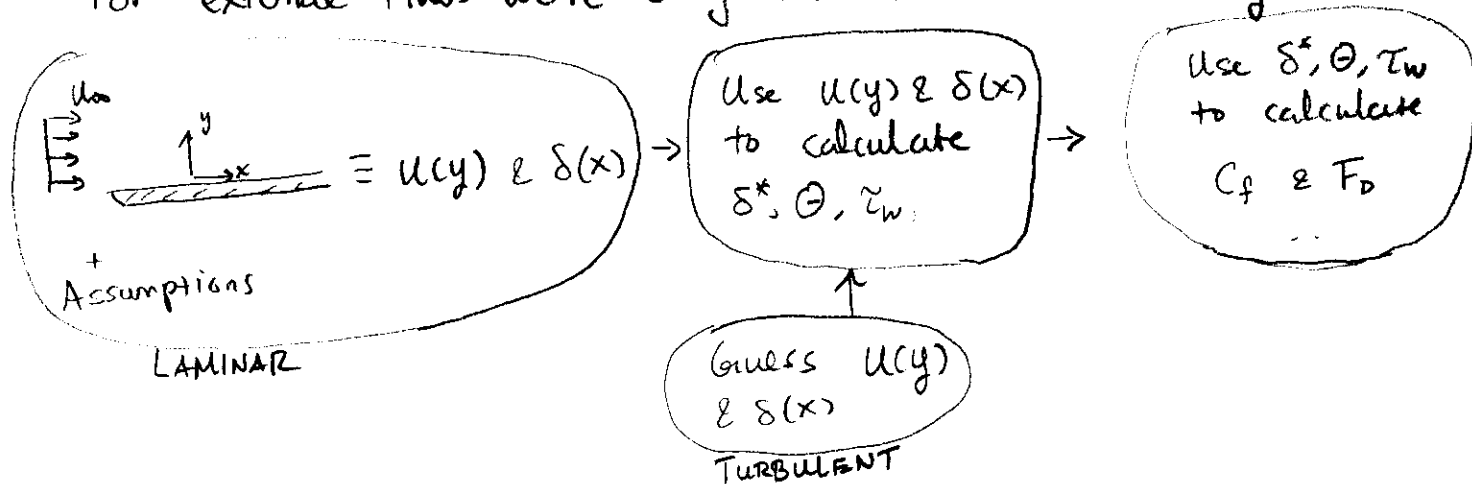


## LECTURE 8 : NOTHING'S PERFECT, THE TURBULENT BOUNDARY LAYER.

In a round about way last time we found ways to calculate  $\tau_w$  and  $F_D$  based on a  $Re$  value. We have almost mimiced the story of a single-straight pipe too!



For external flows we're doing the exact same thing



So you can probably guess what's gonna happen... We're going to prescribe a  $u(y)$  based on years of experiment and get new  $C_f$  values just like we did for  $f_{turb}$ .

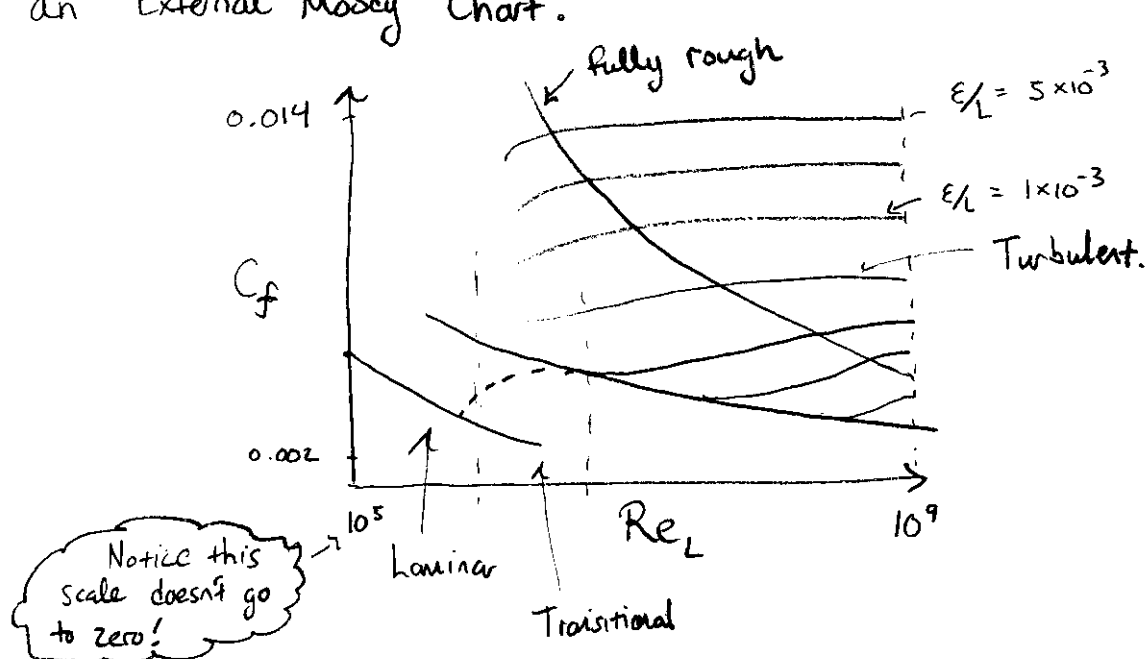
## LECTURE 8:

So first based on experiment we know we have a different critical reynold's #.

$$Re < 5 \times 10^5 \quad (\text{Laminar})$$

$$Re > 5 \times 10^5 \quad (\text{Turbulent})$$

To cut to the chase we eventually ever develop an "External" Moody Chart.



This  $C_D$  is the drag-coefficient for external flows. To reiterate we use it like this.

$$F_D = C_f \cdot \frac{1}{2} \rho W L u_\infty^2$$

$$h_L = f \cdot \frac{L}{D} \frac{V^2}{2g}$$

↑  
stuff you have to calculate, some thinking required

↑  
stuff you have to book-keep and keep track of

## LECTURE 8

We define the drag-coefficient as a ratio of viscous skin friction to the inertial force.

$$C_f = \frac{F_D}{\frac{1}{2} \rho W L u_\infty^2}$$

$$= \frac{W \int_0^L \tau_w dx}{\frac{1}{2} \rho u_\infty^2 W L}$$

so if we can derive a  $\tau_w(x)$  we win.

Now, how do we figure out  $\tau_w(x)$ ? We have two ways---

1.) (Simple-Way)  $\tau_w(x) = \rho u_\infty^2 \frac{d\Theta}{dx}$

2.) (Exact Way)  $\tau_w(x) = \mu \left. \frac{\partial u}{\partial y} \right|_{y=0} \leftarrow$

This requires you to solve those governing equations using a stream function approach and another method called similarity-solutions

Why is 1.) Easy? Well because remember we have a definition for  $\Theta$ .

$$\Theta(x) = \int_0^{\delta(x)} \frac{u}{u_\infty} \left(1 - \frac{u}{u_\infty}\right) dy$$

So all you need to provide is  $u(y)$  and  $\delta(x)$ !

## LECTURE 8:

So you'll notice what's worse for external flow is we need to estimate  $\delta(x)$  and  $u(y)$ .  
More often we are trying to estimate.

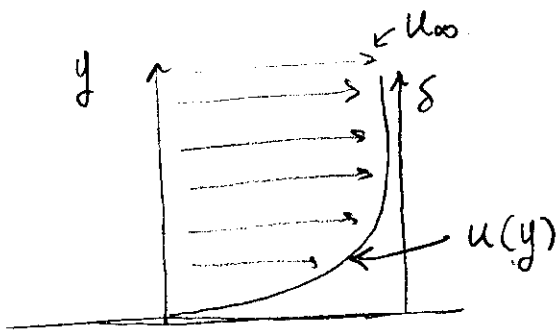
$$\delta(x) = \frac{C_0 \cdot x}{Re_x^a}$$

So experimentally we need to determine  $(C_0 \text{ \& } a)$  from lots of measurements.

Extra Credit

Devise an experiment to experimentally find constants  $a$  &  $C_0$ .

We can actually provide a guess of  $\delta(x)$  and  $u(y)$  if we provide a non-dimensional function.



$$u^* = \frac{u(y^*)}{u_{\infty}}$$

and,

$$y^* = \frac{y}{\delta}$$

Now the integral just needs  $u^*(y^*)$ .

$$\Theta(x) = \delta(x) \int_0^1 u^*(1 - u^*) dy^*$$

Extra Credit: Show why the upper limit is 1 now not  $\delta$

## LECTURE 8:

Prandtl found a good  $u^*(y^*)$  for turbulent boundary layers was

$$u^*(y^*) = y^{*1/7} = y^{*a}$$

Plug this in and we find.

$$\Theta(x) = \delta(x) \frac{7}{72} = C_1 \delta(x)$$

Now the last step is to assign  $\delta(x)$ , take a derivative.

$$\tau_w(x) = \rho u_\infty^2 \frac{d\delta}{dx} \cdot C_1$$

$$\delta(x) = \frac{C_0 \cdot x}{[Re(x)]^a}$$

$$Re(x) = \frac{\rho u_\infty x}{\mu}$$

Notice with the chain rule and calculations we get

$$\tau_w(x) = C_0 C_1 (1-a) \rho u_\infty^2 Re_x^{-a}$$

↑  
extra credit  
do this calculation

\* Notice that the power-matches the power of  $\delta(x)$ .

## LECTURE 8

Now we're in a position to get  $C_D$  based on our integral definition.

$$C_f = \frac{\int_0^L \tau_w(x) dx}{\frac{1}{2} \rho U_\infty^2 L}$$

Only true for  
 $\frac{u}{u_\infty} = \left(\frac{y}{\delta}\right)^{1/4}$  and  
 $\delta(x) = \frac{C_0 x}{[Re(x)]^a}$

$$\rightarrow = \frac{\rho U_\infty^2 C_0 C_1 (1-a) \int_0^L Re(x)^{-a} dx}{\frac{1}{2} \rho U_\infty^2 L}$$

$$= (C_0 C_1) Re_L^{-a}$$

The last toy example was to show the framework for arriving at a  $C_f$  much like getting those  $f_{turb}$  formulas. We started by assuming a  $u^*(y^*)$  function. Just like internal flows we actually have the same log-function which comes from experiment.

$$\frac{u}{u_*} = \frac{1}{K} \ln \left( \frac{y u_*}{\nu} \right) + B ; K=0.41 \text{ \& } B=5$$

$$u_* = \left( \frac{\tau_w}{\rho} \right)^{1/2}$$

So in much the same steps we can arrive at

$$C_D = \frac{0.455}{\log_{10}(Re_L)^{2.58}}$$

Turbulent  
Smooth  
Pipe

## LECTURE 8

When we consider rough plates.

$$C_f = \left[ 1.89 - 1.62 \log_{10} \left( \frac{\epsilon}{L} \right) \right]^{-2.5}$$

Completely  
Turbulent

Or

$$C_f = \frac{0.455}{[\log_{10}(Re_L)]^{2.58}} - \frac{1700}{Re_L}$$

Transitional

It's pretty amazing what you can get from simply calculating a Reynolds Number right! That completes only half of what goes into drag force. Recall.

$$F_{D, \text{TOT}} = \underbrace{\int P \cdot \hat{n} dA}_{\text{Form Drag}} + \underbrace{\int \tau_w \cdot \hat{t} dA}_{\text{Skin friction}}$$

- This is up next and we will see a boundary layer separates, why dimples make golf balls fly further, and why on airplane generators lift,

- tangential shear forces due to viscous forces of liquid
- Analysis of the Boundary Layer determined methods to calculate friction coefficients  $C_f$
- Analysis of integrals provided methods to calculate  $\delta, \delta^*, \Theta$

- Everything is a function of  $(Re, \frac{\epsilon}{L})$  just like  $f$ .

# LECTURE 8

\* A NOTE ON HOMEWORK PROBLEMS. BASED ON WHAT ASSUMED VELOCITY PROFILE YOU HAVE  $u^*(y^*)$  YOU GET DIFFERENT CONSTANTS OF PROPORTIONALITY FOR  $Re^{-1/2}$ .

Profile	$\delta Re^{1/2}/x$	$\hat{C}_f Re_x^{1/2}$ <small>pointwise coefficient</small>	$C_f Re_L^{1/2}$ <small>total skin friction coefficient</small>
* Blasius (Exact)	5.00	0.664	1.328
Linear $\frac{u}{u_\infty} = \frac{y}{\delta}$	3.46	0.578	1.156
Parabolic $\frac{u}{u_\infty} = 2 \frac{y}{\delta} - \left(\frac{y}{\delta}\right)^2$	5.48	0.730	1.460
Cubic $\frac{u}{u_\infty} = \frac{3}{2} \left(\frac{y}{\delta}\right) - \left(\frac{y}{\delta}\right)^3 \frac{1}{2}$	4.64	0.646	1.292
Sine $\frac{u}{u_\infty} = \sin\left(\frac{\pi}{2} \left(\frac{y}{\delta}\right)\right)$	4.79	0.655	1.310

Make sure you use the Blasius constants for calculations. I don't know why we give the others also... remember for shear.

$$\tau_w = 0.332 u_\infty^{3/2} \sqrt{\frac{\rho \mu}{x}} \leftarrow \text{This comes from the def of } \hat{C}_f.$$