Department of Chemical Engineering

Minor I - CLL222 & CHL 221 CRE -II

Time: 11 AM - 12 Noon

Date 30 August., 2015

A reaction takes place in the presence of 1% Pt/Alumina catalyst. The catalyst has a dispersion value of 80% as obtained from the hydrogen chemisorption method. Calculate the mass of the catalyst required in CSTR and in packed bed reactor for 80% conversion of A if the feed rate is $1000 \text{ m}^3/\text{hr}$ of pure gaseous A ($C_{Ao} = 100 \text{ mol/m}^3$). The stoichiometry and reaction rate are given by

$$-r'_{A} = \frac{50C_{A}}{1 + 0.02C_{A}} \frac{\text{mol}}{\text{kg} \cdot \text{hr}}$$

- 2) (a) How the BET isotherm is used for the determination of catalyst surface area.
 - (b) A solid catalyzed first-order gas phase reaction (A→ R), takes place with 50% conversionin a basket type mixed reactor. With proper explaination calculate the conversion if the reactor size is trebled and all else-temperature, amount of catalyst, feed composition, and flow rate-remains unchanged?
- 3) For a solid catalyzed reaction, $A + B \leftrightarrow R$. The following mechanism is given,

$$A + S \leftrightarrow AS$$
 $B + S \leftrightarrow BS$
 $AS + BS \leftrightarrow RS + S$
 $RS \leftrightarrow R + S$

Where, S is an active site and mechanism is dual site. Develop a rate model of Hougen-Watson type based on the above mechanism if adsorption of A is rate controlling.

(7)

(3)

(4)