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# Exercise 1 Introduction to detailed kinetic mechanisms

Combustion Fundamentals and New Technologies

Conservatorio delle Orfane a Terra Murata Isola di Procida, Napoli, Italy May 31 – June 5, 2015



# Setting up your problem

- 1. Prepare your thermodynamic/kinetic/transport files and pre-process them
- 2. Choose the most appropriate reactor model to describe your system

  For some problems the choice of reactor model is obvious. In other cases, you may have different options and the choice is not so easy. As an example, in some cases a single, a perfectly stirred reactor may be the sufficient, while in other cases your system must be described using a network of reactors.
- 3. Setup the reactor parameters and inlet/initial conditions

  Each type of reactors has specific parameters (residence time, volume, length, etc.) which have to properly setup by the user.
- 4. Setup the numerical parameters In some cases the correct setup of numerical parameters (tolerances, stopping criteria, mesh strategy, etc) is of fundamental importance to correctly solve the problem
- 5. Run the simulation
- 6. Analyze your results
  You may consider different tools (native graphical post-processor, 3<sup>rd</sup> party tools, analysis of text files, etc.)



# Setting up your problem

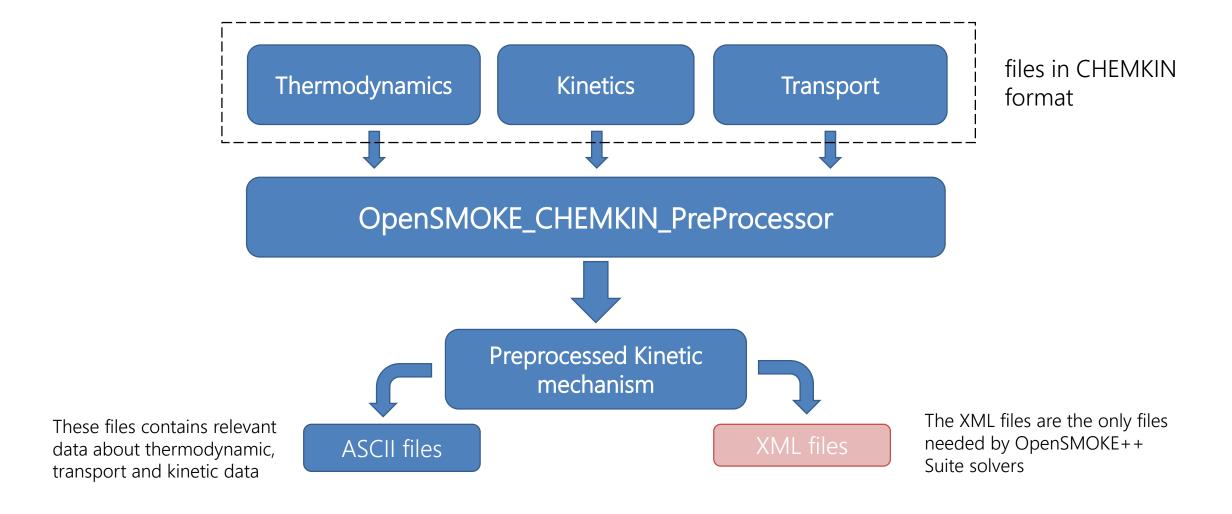
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# Kinetic pre-processing in OpenSMOKE++





### Thermodynamics: NASA coefficients

Users must first supply the thermodynamic data for each species in the chemical system. These data are in the form of polynomial fits to temperature, for species enthalpy, entropy, and specific heat capacity.

$$\frac{C_P}{R} = a_1 + a_2 T + a_3 T^2 + a_4 T^3 + a_5 T^4$$

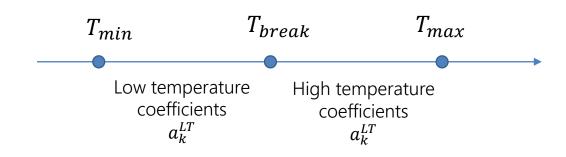
$$\frac{H}{RT} = a_1 + \frac{a_2}{2}T + \frac{a_3}{3}T^2 + \frac{a_4}{4}T^3 + \frac{a_5}{5}T^4 + \frac{a_6}{T}$$

$$\frac{S}{R} = a_1 \ln T + a_2 T + \frac{a_3}{2} T^2 + \frac{a_4}{3} T^3 + \frac{a_5}{4} T^4 + a_7$$

In order to ensure higher accuracy in the evaluation of thermodynamic properties, two sets of NASA coefficients are usually accounted for, by dividing the temperature field in 2 ranges

This means that each species is completely characterized by a total of 14 NASA coefficients

7 coefficients are required to completely characterize the thermodynamic properties of each species Additional thermodynamic quantities (free Gibbs energy, Helmotz energy, internal energy, etc.) can be evaluated from enthalpy, entropy, and specific heat capacity reported on the left



# Thermodynamic input file

the first line specifies that the following is a set of thermodynamic data, while the second line provides the three temperatures used in the fitting process (low temperature, break temperature, and high temperature).

```
THERMO ALL
300.000 1000.000 5000.000
CH2CHO
                  SAND860
                                                 300.000
                                                          5000.000
 0.05975670E+02 0.08130591E-01-0.02743624E-04
                                               0.04070304E-08-0.02176017E-12
 0.04903218E+04-0.05045251E+02
                               0.03409062E+02
                                               0.10738574E-01 0.01891492E-04
-0.07158583E-07 0.02867385E-10 0.15214766E+04 0.09558290E+02
                   62987AT
                                                 300.000
                                                          5000.000
                                                                   1000.000
AL
 0.02559589E+02-0.10632239E-03
                               0.07202828E-06-0.02121105E-09 0.02289429E-13
 0.03890214E+06 0.05234522E+02
                               0.02736825E+02-0.05912374E-02-0.04033937E-05
 0.02322343E-07-0.01705599E-10
                               0.03886794E+06 0.04363879E+02
(CH2O)3
                   70590C
                            3H
                                                 300.00
                                                          4000.00
 0.01913678E+03 0.08578044E-01-0.08882060E-05-0.03574819E-08 0.06605142E-12
-0.06560876E+06-0.08432507E+03-0.04662286E+02 0.06091547E+00-0.04710536E-03
 0.01968843E-06-0.03563271E-10-0.05665403E+06 0.04525264E+03
END
```



# Thermodynamic data: CHEMKIN format

9	name of species [1-16]	Comments [19-24]		omposition -44]	Phase [45	[] Temperatur	e intervals [46-73]	Line index [80]
	СН2СНО	SAND860	1H	3C 2	(G)	300.000 50	00.000 1000.000	
	0.05975670E+02	0.0813059	1E-01-0	0.0274362	24E-04 0.	.04070304E-0	8-0.02176017E-12	2
	0.04903218E+04-	0.0504525	1E+02 C	.0340906	2E+02 0	.10738574E-0	1 0.01891492E-04	3
\	-0.07158583E-07	0.0286738	5E-10 C	.1521476	6E+04 0	.09558290E+0	2	4
								<u>\</u> /

Very strict syntax rules apply:

High Temperature (HT) NASA coefficients

- 1. The data for each species requires 4 formatted lines of length 80 characters.
- 2. The data on the first line must be properly formatted, in fields with predefined length
- 3. The 7 HT NASA coefficients must be followed by the 7 LT NASA coefficients
- 4. The NASA coefficients have to be written in blocks of 15 chars



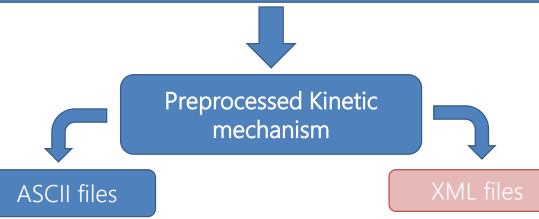
Low Temperature (LT) NASA coefficients

Objective: get familiar with the pre-processing operations and analysis of pre-processed results

Thermodynamics

Task: preprocess a thermodynamic database in CHEMKIN result, check the consistency of thermodynamic functions, and improve the polynomial fitting





For this preliminary task we will use the POLIMI\_TOT\_NOX\_1412.CKT thermodynamic database.

This is the database shared by every kinetic scheme from CRECK modeling. It is based on data available in the literature, NIST and Burcat's databases



### 1. Preparation of input data

Go to the Tasks/Task1 folder, containing the input.dic. This file contains instructions for preprocessing the thermodynamic data

```
Dictionary CHEMKIN_PreProcessor
{
    @Thermodynamics ../../Kinetics/POLIMI_TOT_NOX_1412.CKT;
    @Output thermodynamics;
}
```

#### @Thermodynamics

full path and name of file containing the thermodynamic data to be pre-processed (local or absolute paths are allowed)

#### @Output

full path and name of folder where the user want to put the results of post processing operations (local or absolute paths are allowed)



### 2. Run the kinetic preprocessor

From the same Tasks/Task1 folder, run the OpenSMOKE\_CHEMKIN\_PreProcessor utility.

### a) Windows

Run the Run.bat file by double-clicking on it or, from the Command Prompt, type:

%OPENSMOKEPP\_EXE\_FOLDER%\OpenSMOKE\_CHEMKIN\_PreProcessor.exe --input input.dic

### b) Linux and Mac OSX

Run the Run.sh file of, from the command line, type:

OpenSMOKE\_CHEMKIN\_PreProcessor.exe --input input.dic



### 3. Analyze the pre-processing results

If everything was done properly, the thermodynamics output folder will be created, containing the following files:

### log

possible errors and/or warnings are reported here. Remember to have a look at it every time you preprocess a thermodynamic database (or more in general a kinetic mechanism)

### Thermodynamics\_Coefficients.out

for each species the 14 NASA coefficients are reported in a more readable format

### Thermodynamics\_Tables.out

for each species, the most important thermodynamic data are reported as a function of temperature, according to the 14 NASA coefficients provided in the thermodynamic database

#### kinetics.xml

this is the only file needed by OpenSMOKE++ Suite solvers



### 4. Refine the analysis of thermodynamic data

You can refine the analysis by asking additional tests to check the consistency of data supplied through the thermodynamic database

```
Dictionary CHEMKIN_PreProcessor
{
    @Thermodynamics ../../Kinetics/POLIMI_TOT_NOX_1412.CKT;
    @Output thermodynamics;
    @CheckThermodynamics true;
}
```

Additional file will be written:

Thermodynamics\_Status.out

possible existence of unphysical maxima/minima in specific heat, possible discontinuities in thermodynamic properties are detected and reported here

Thermodynamics\_Reformulated.out

if possible, a new set of 14 NASA coefficients is proposed for each species in order to ensure perfect thermodynamic consistency



### Transport properties

Characterizing the molecular transport of species, momentum, and energy in a multicomponent gaseous mixture requires the evaluation of diffusion coefficients, viscosities, thermal conductivities, and thermal diffusion coefficients.

Although evaluation of pure species properties follows **standard kinetic theory expressions**, one can choose from a range of possibilities for evaluating mixture properties. Moreover, computing the mixture properties can be expensive, and depending on the use of the results, it is often advantageous to make simplifying assumptions to reduce the computational cost (Kee et al., 2003)

For most applications, gas mixture properties can be determined from pure species properties via certain approximate mixture averaging rules. More advanced and accurate approaches are possible, but usually the computational cost increases



# Mixture averaging rules

In most cases the transport properties of the species can be evaluated by using the standard kinetic theory expressions (Hirschfelder, 1964). Then we can apply averaging rules to have the transport properties of the mixture

Thermal conductivity 
$$\lambda = \frac{1}{2} \left[ \sum_{i=1}^{N} x_i \lambda_i + \left( \sum_{i=1}^{N} \frac{x_i}{\lambda_i} \right)^{-1} \right]$$

Mixture averaged diffusion coefficient

$$\Gamma_{i,mix} = \frac{\sum_{j \neq i}^{N} x_j W_j}{W_{mix} \sum_{j \neq i}^{N} \frac{x_j}{\Gamma_{ji}}}$$

$$\eta = \sum_{i=1}^{N} \frac{x_j \eta_j}{\sum_{j=1}^{N} x_j \phi_{i,j}}$$

$$\eta = \sum_{i=1}^{N} \frac{x_j \eta_j}{\sum_{j=1}^{N} x_j \phi_{i,j}} \qquad \phi_{i,j} = \frac{1}{\sqrt{8}} \sqrt{\frac{W_j}{W_i + W_j}} \left[ 1 + \sqrt{\frac{\eta_i}{\eta_j}} \left( \frac{W_j}{W_i} \right)^{1/4} \right]^2$$

### Transport data input file

AR	0	136.5	3.33	0.	0.	0.
С	0	71.4	3.298	0.	0.	0.
С2Н2ОН	2	224.7	4.162	0.	0.	1.
C2N	1	232.400	3.828	0.	0.	1.

The first 16 columns in each line of the database are reserved for the species name. Columns 17 through 80 are free-format, and they contain the molecular parameters for each species.

- 1. An index indicating whether the molecule has a monatomic, linear or nonlinear geometrical configuration. If the index is 0, the molecule is a single atom; 1 means the molecule is linear; 2 the molecule is nonlinear.
- 2. The Lennard-Jones potential well depth in Kelvins.
- 3. The Lennard-Jones collision diameter in angstroms.
- 4. The dipole moment in Debye
- 5. The polarizability in cubic angstroms.
- 6. The rotational relaxation collision number at 298 K.
- 7. A "comment" line is one that has an exclamation mark (!) as the first non-blank character. In addition, on any line, any input that follows an exclamation mark is taken as a comment.



# Fitting of transport properties

To expedite the evaluation of transport properties in OpenSMOKE++, the temperature dependent parts of the pure species property expressions are fitted. This means that, rather than re-evaluating the complex expressions for the properties, only simple fits need to be evaluated. In particular, following the approach proposed by Kee et al. (1996) ad adopted in CHEMKIN, a polynomial fit of the logarithm of the property versus the logarithm of the temperature is adopted:

Viscosity

$$ln(\eta) = \sum_{k=1}^{4} b_k^{\eta} T^{k-1} = b_1^{\eta} + b_2^{\eta} T + b_3^{\eta} T^2 + b_4^{\eta} T^3$$

4 fitting coefficients

Thermal conductivity

$$ln(\lambda) = \sum_{k=1}^{4} b_k^{\lambda} T^{k-1} = b_1^{\lambda} + b_2^{\lambda} T + b_3^{\lambda} T^2 + b_4^{\lambda} T^3$$

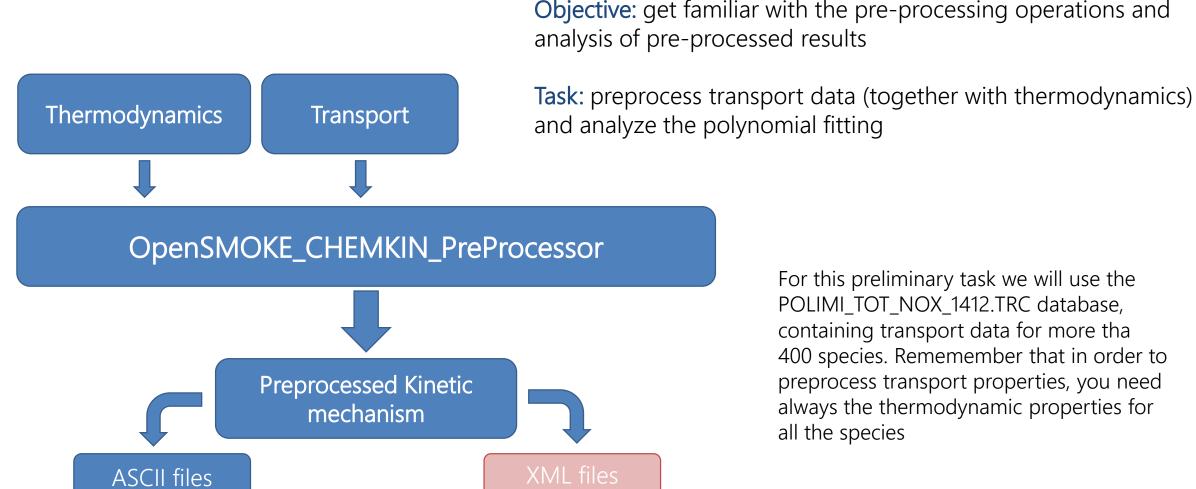
4 fitting coefficients

Binary diffusion

Binary diffusion coefficient with species j 
$$ln(\Gamma_j) = \sum_{k=1}^4 b_{j,k}^{\Gamma} T^{k-1} = b_{j,1}^{\Gamma} + b_{j,2}^{\Gamma} T + b_{j,3}^{\Gamma} T^2 + b_{j,4}^{\Gamma} T^3$$

4N fitting coefficients

# Task 2: pre-processing transport data



For this preliminary task we will use the POLIMI\_TOT\_NOX\_1412.TRC database, containing transport data for more tha 400 species. Rememember that in order to preprocess transport properties, you need always the thermodynamic properties for



# Task 2: pre-processing transport data

### 1. Preparation of input data

Go to the Tasks/Task2 folder, containing the input.dic. This file contains instructions for preprocessing the transport and thermodynamic data

#### @Transport

full path and name of file containing the transport data to be pre-processed (local or absolute paths are allowed)

#### @TransportFittingCoefficients

Use this option only if you want to write no a file the result of polynomial fitting. Please consider that this option is not compulsory and results in large output files.



# Task 2: pre-processing transport data

### 2. Run the kinetic preprocessor

### 3. Analyze the pre-processing results

If everything was done properly, the transport output folder will be created, containing the following files (in addition to the usual files associated to thermodynamics):

### TransportProperties\_Coefficients.out

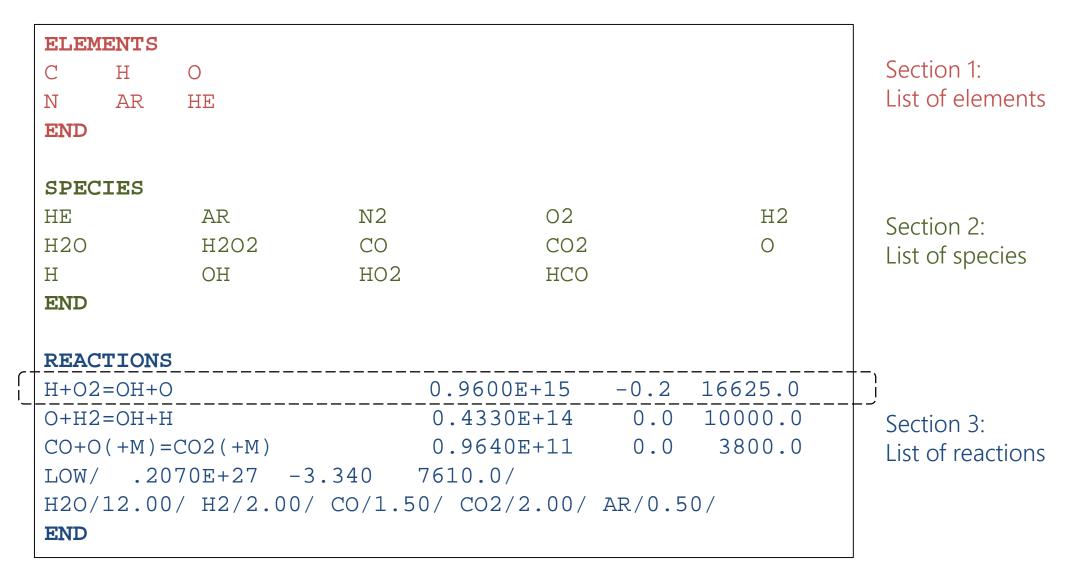
For each species and transport property, the coefficients of 4<sup>th</sup> order polynomial fitting described in previous slides are reported here (very large file!)

#### kinetics.xml

this is the only file needed by OpenSMOKE++ Suite solvers. It contains the pre-processed thermodynamic and transport data in XML format



### Kinetic file: CHEMKIN format (I)



## Kinetic file: CHEMKIN format (II)

Basic rate expression: 
$$r = r_f - r_b = k_f \prod_j C_j^{v_j^f} - k_b \prod_j C_j^{v_j^b}$$

$$r \neq \underbrace{k_f}_{j} \prod_{j} C_j^{v_j^f} - \underbrace{k_f}_{K_{eq}} \prod_{j} C_j^{v_j^b}$$

 $v_j^f$  forward stoichiometric coefficient of species j  $v_j^b$  backward stoichiometric coefficient of species j  $C_j$  concentration of species j  $K_{eq}$  equilibrium constant  $k_f$ 

$$H + O2 = OH + O$$

reactants

products

0.9600E+15

Frequency factor A [cm<sup>3</sup>/mol/s] -0.2

Temperature exponent n

16625.0

Activation energy E [cal/mol]

(Arrhenius' law)

$$k_f = AT^n e^{-\frac{E}{RT}}$$

### Kinetic file: CHEMKIN format (III)

#### Reversible reaction

$$H + O2 = OH + O$$

#### Non-reversible reaction

$$H + O2 => OH + O$$

$$-0.2$$

### Third-body reaction

```
HCO + M = CO + H + M 0.1200E+18 -1.0 17000.0
H2O/5.00/ CO2/3.00/ H2/1.90/ CO/1.90/
```

### Pressure dependent reaction

```
OH+OH (+M) = H2O2 (+M) 0.7400E+14 -0.37 0
LOW/ .1300E+19 -.900 -1700.0/
TROE / 0.7346 94.00 1756. 5182. /
H2/2.00/ H2O/6.00/ CO/1.50/ CO2/2.00/ AR/.70/ HE/0.70/ N2/0.90/
```

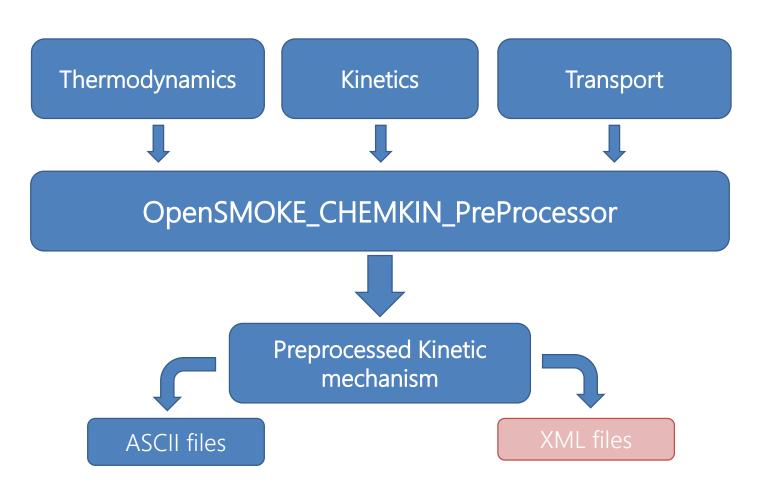


### Kinetic file: CHEMKIN format (IV)

Additional types of reactions and options available in OpenSMOKE++

- Chebyshev Polynomial Rate Expressions (CHEB)
- Power series within the exponential of a modified Arrhenius expression (FIT1)
- Janev-Langer reaction rates (JAN)
- Landau-Teller reaction rates (LT)
- Pressure Dependence Through Logarithmic Interpolation (PLOG)
- Explicit reverse reaction rates (REV)
- Explicit reaction orders (FORD and RORD)





Objective: get familiar with the pre-processing operations and analysis of pre-processed results

**Task:** preprocess a complete kinetic mechanism (together with thermodynamics and transport properties)

For this task we will use the POLIMI\_H2CO\_1412.CKI kinetic mechanism, describing the combustion chemistry of hydrogen and carbon monoxide (14 species and 33 reactions)

Remember that in order to preprocess a kinetic mechanism, the thermodynamic properties are needed.



### 1. Preparation of input data

Go to the Tasks/Task3 folder, containing the input.dic. This file contains instructions for preprocessing the complete kinetic mechanism

@Kinetics

full path and name of file containing the transport data to be pre-processed (local or absolute paths are allowed)



### 2. Run the kinetic preprocessor

### 3. Analyze the pre-processing results

If everything was done properly, the kinetics output folder will be created, containing the following files (in addition to the usual files associated to thermodynamics):

### Kinetics\_Summary.out

This file simply contains the kinetic mechanism written in a more readable format

### kinetics.xml reaction\_names.xml

these are the only file needed by OpenSMOKE++ Suite solvers. They contain the pre-processed thermodynamic (and transport) data together with the whole reaction mechanism in XML format



### 4. Refine the analysis

We can refine the analysis by performing additional tests to check the consistency of reactions or asking for additional data in output files

@ReactionTables

For each reaction detailed information is reported on a file (kinetic constants, change of moles, etc.)

@ReverseFitting

For each reversible reaction the reverse kinetic constants are estimated assuming the Arrhenius' law

### References

J. O. Hirschfelder, C. F. Curtiss, and R. B. Bird, *Molecular Theory of Gases and Liquids (Revised Edition)*, John Wiley and Sons, New York (1964)

Kee, R., Coltrin, M., Glarborg, P., Chemical Reacting Flows: Theory and Practice. Wiley-Interscience (2003)

Kee, R., Rupley, F., Meeks, E., Miller, J., CHEMKIN-III: A FORTRAN chemical kinetics package for the analysis of gas phase chemical and plasma kinetics, SAND96-8216 Techical Report (1996)

Curtiss, C., Hirschfelder, J., *Transport properties of multicomponent gas mixtures*, Journal of Chemical Physics 17, 550 (1949)

