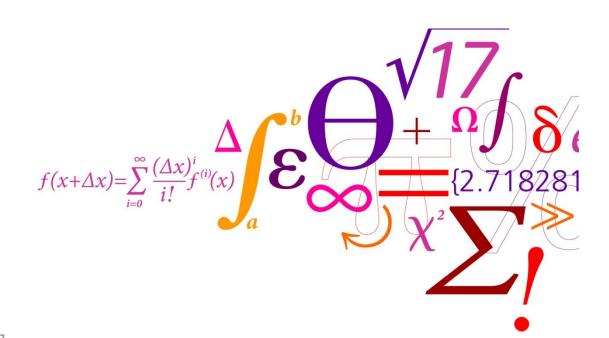


# Chemical kinetics Procida June 2015

Module 3





### Module 3

- Developing detailed chemical kinetic models (PG)
  - Approach
  - Experimental validation
  - Analysis tools
- Task 2: Engine exhaust oxidation of unburned hydrocarbons
  - Introduction (AC)
  - -Solving using OpenSMOKE++ (AC, PG)

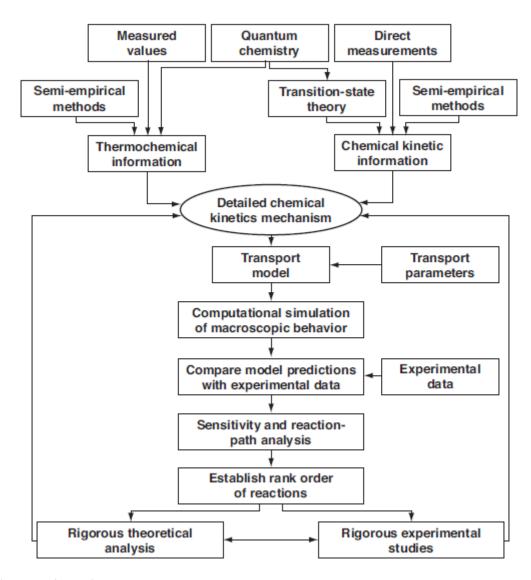


### Developing a detailed chemical kinetic model

- Compile the best available species and reaction specific data
  - Experiment
  - Theory
  - Analogy / empirical
- Compare modeling predictions with the best available non-reaction-specific experimental data
  - Ignition delays, flame speeds, explosion limits
  - Detailed characterization data (species concentrations, etc.)
- Refine
  - Microscopic accuracy (fundamental model)
  - Macroscopic accuracy (engineering model)

### Development of chemical kinetic model







### **Kinetic experiments**

- Microscopic
  - Characterization of elementary reaction
    - Determine rate coefficients
    - Identify products
- Macroscopic
  - Characterization of process
    - Identify mechanism
    - Validate model



### Macroscopic experimental techniques

- Batch reactor
  - Low to medium temperature, low to medium pressure
- Flow reactor
  - Low to high temperature, low to high pressure
- Jet-stirred reactor
  - Medium to high temperature, medium pressure
- Shock tube.
  - Medium to high temperature, medium to high pressure
- Rapid Compression Machine (RCM)
  - Medium temperature, medium to high pressure
- Laminar, premixed flames
  - Medium to high temperature, low to medium pressure

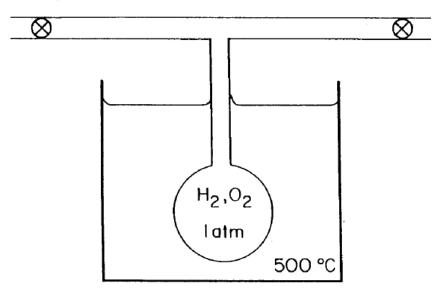


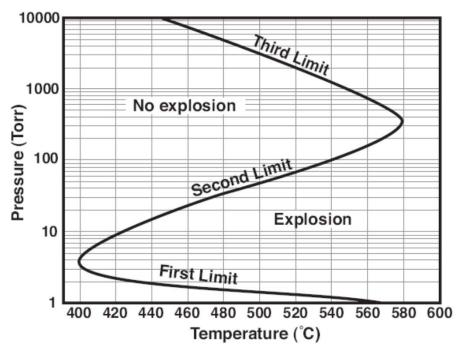
# **Experimental techniques** for model validation

	Pressure	Temperature	Dilution	Stoichiometry	Transport
Static/batch reactor	atm.	< 1000 K	yes	none	no
Stirred reactor	atm high	800 - 1400 K	yes / no	no (ext. heat) Flammability limits	no
Plug-flow reactor	atm high	800 - 1400 K	yes	none	no
Shock tube	atm high	> 1300 K	yes	none	no
Flames	atm low	800 - 2500 K	no	Flammability limits	yes



### **Batch reactor**





H<sub>2</sub>/O<sub>2</sub> explosion limits

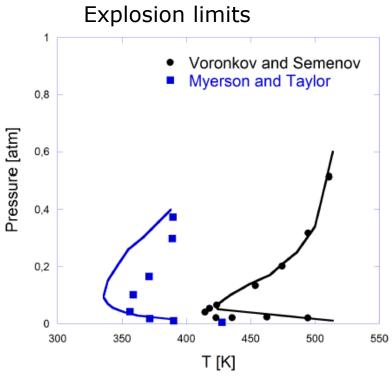
Data: Lewis and von Elbe (1987);

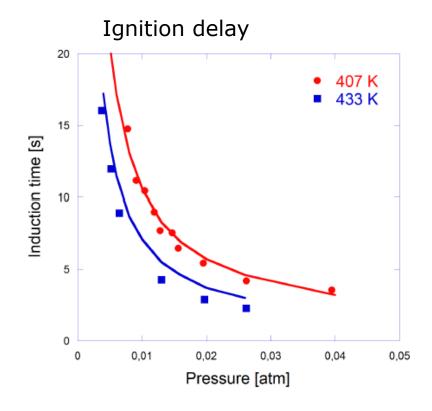
Figure: Kee et al. (2003)



## Batch reactor - CS<sub>2</sub> ignition

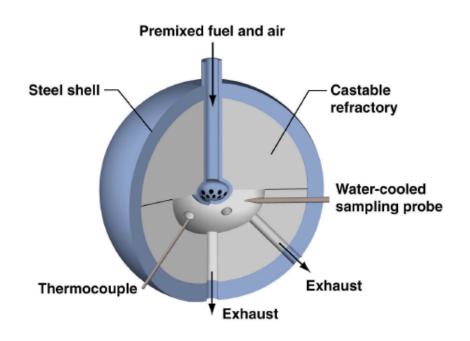
## Evaluation limits



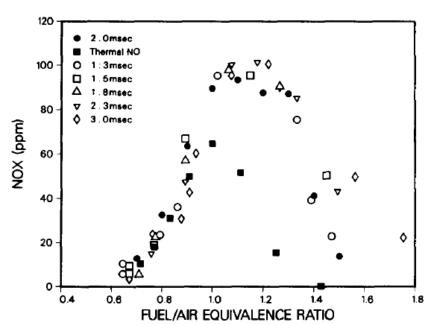




#### **Jet-stirred reactor**

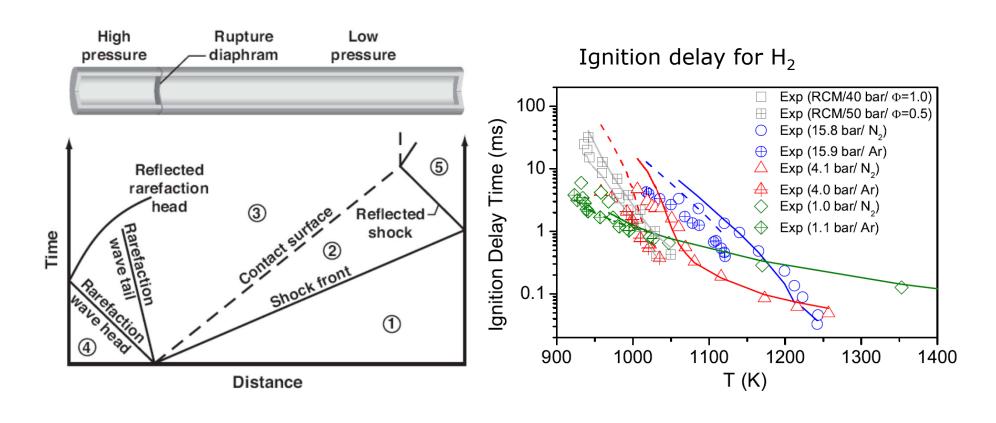


CH<sub>4</sub> oxidation (1600-2000 K) Experimental data: Bartok et al. (1972)





### Shock tube





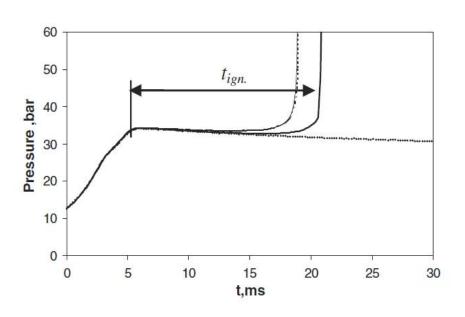
## **Rapid Compression Machine**

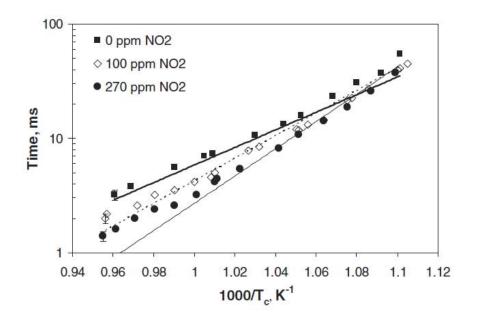




### **Rapid Compression Machine**

#### Ignition delay for CH<sub>4</sub>

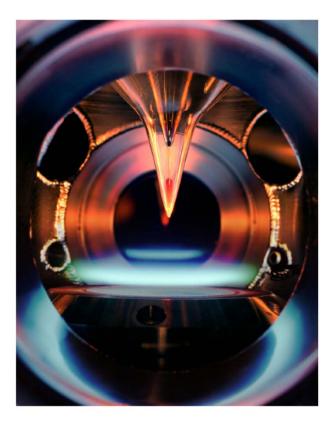


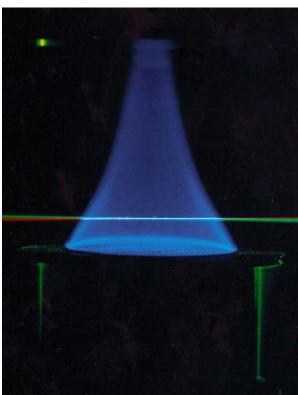


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## Low-pressure premixed flames



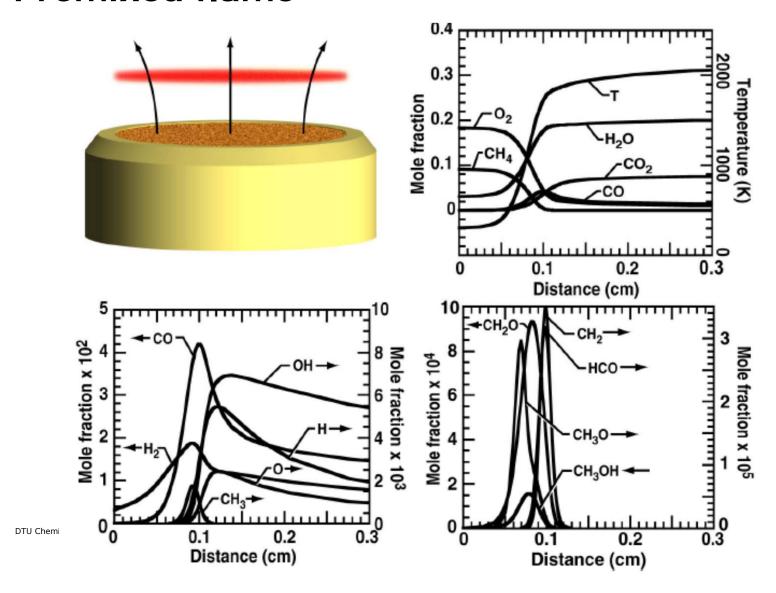


DTU Chemical Engineering, Technical University of Denmark

Photos: Sandia National Laboratories



### **Premixed flame**

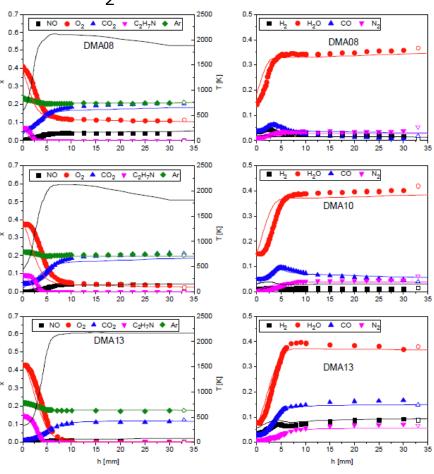




### Low-pressure, premixed flame



### C<sub>2</sub>-amine oxidation



DTU Chemical Engineering, Technical University of Denmark

Lucassen et al. (2012)

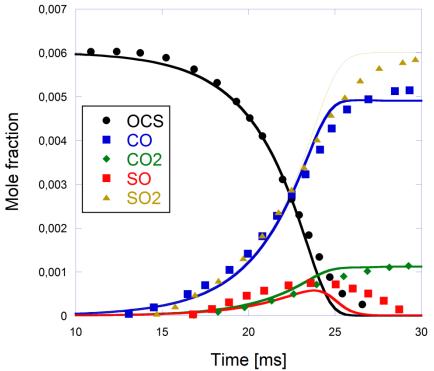


### Flow reactor



OCS oxidation 1200 K, 0.056 atm

Experimental data:
Homann et al. (1969)
Modeling:
Glarborg and Marshall (2013)

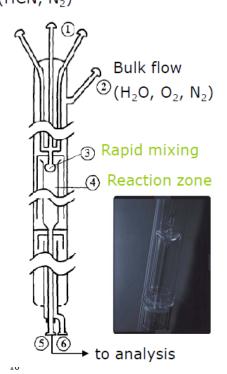


DTU Chemical Engineering, Technical University of Denmark



# Flow reactors for high-temperature or high-pressure chemistry

Injector flows 1 atm, 600-1300 K (HCN,  $N_2$ )



HCN, 1 atm

400

300

000

1000

1100

1200

1300

1400

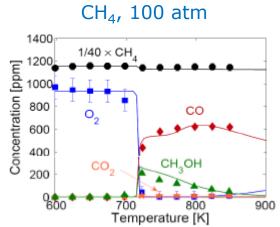
1500

T/K

Dagaut et al., 2008

1 atm, 600-1850 K 20-100 atm, 600-925 K

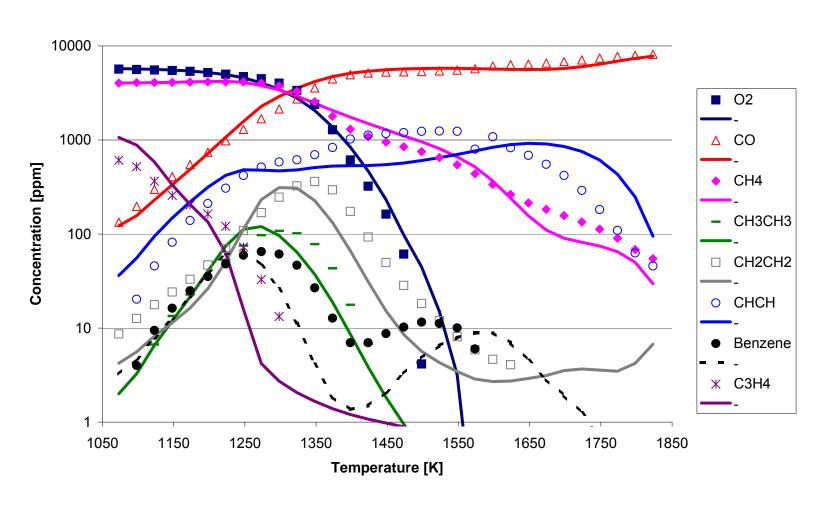




Rasmussen et al., 2008



# Flow reactor: Oxidation of CH<sub>4</sub>/C<sub>3</sub>H<sub>4</sub> mixture

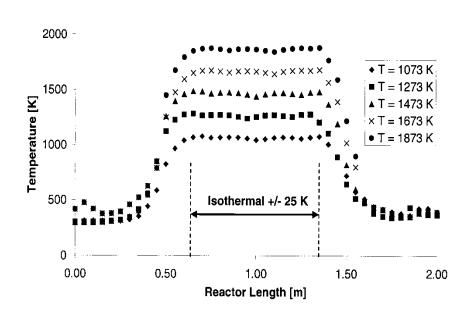


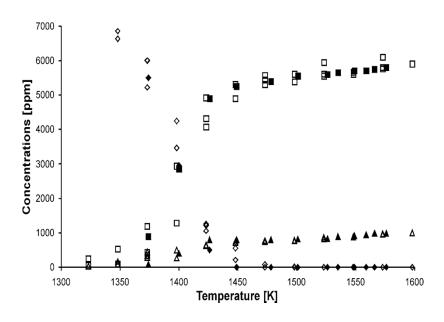
### Flow reactor issues



### **Temperature**

## **Surface reactions**

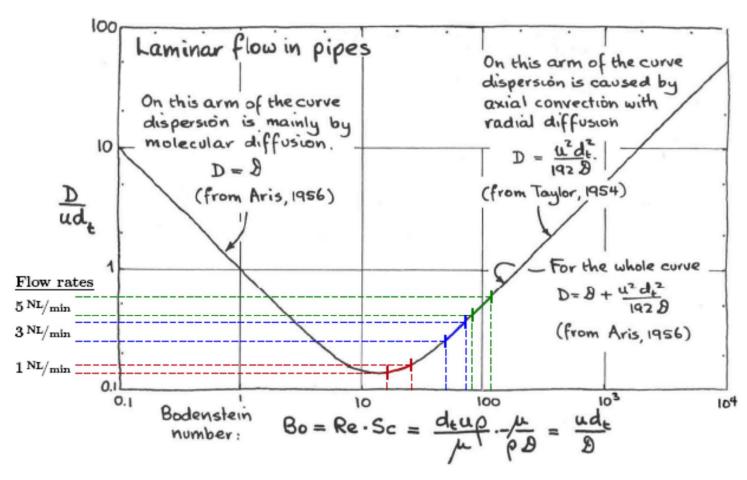




 $CH_4$  oxidation: 1.0%  $CH_4$ , 0.75%  $O_2$ ;  $N_2$  Quartz reactor (closed symbols) Alumina reactor (open symbols)



# The plug-flow approximation: Axial dispersion in the laminar flow regime





## Macroscopic experimental techniques - concerns

- Batch reactor
  - Surface reactions, conditioning, temperature
- Flow reactor
  - Surface reactions, conditioning, temperature
- Jet-stirred reactor
  - Mixing, probe system
- Shock tube.
  - Temperature and pressure
- Rapid Compression Machine (RCM)
  - Temperature and pressure
- Laminar, premixed flames
  - Interaction with burner surface, stabilization, probe effects



### Development of reaction mechanism

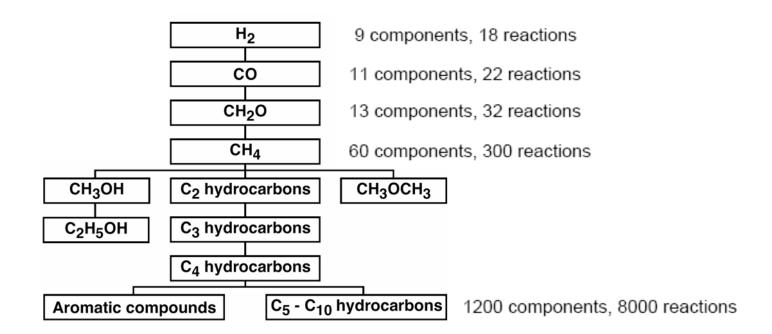
	Known territory	Unknown territory	
Small mechanism	H <sub>2</sub> oxidation	CH <sub>4</sub> +H <sub>2</sub> S oxidation	
Large mechanism	Heptane oxidation	Biofuel(s) oxidation	

Small mechanism: manageable in hand

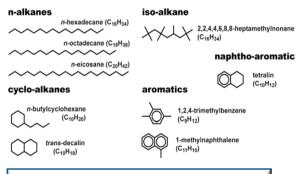
Known territory: detailed mechanisms available with some predictive reliability



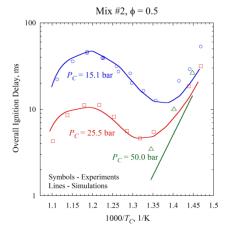
# Hierarchichal structure of combustion chemistry



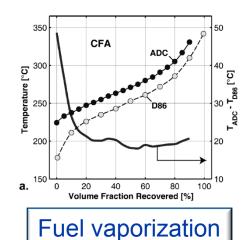
# Why are (some) mechanisms so large? Need to predict complex behavior in "real" fuels

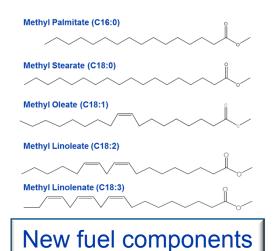


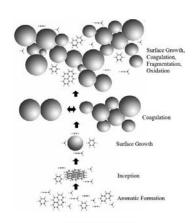
### Many fuel components



Low temperature chemistry



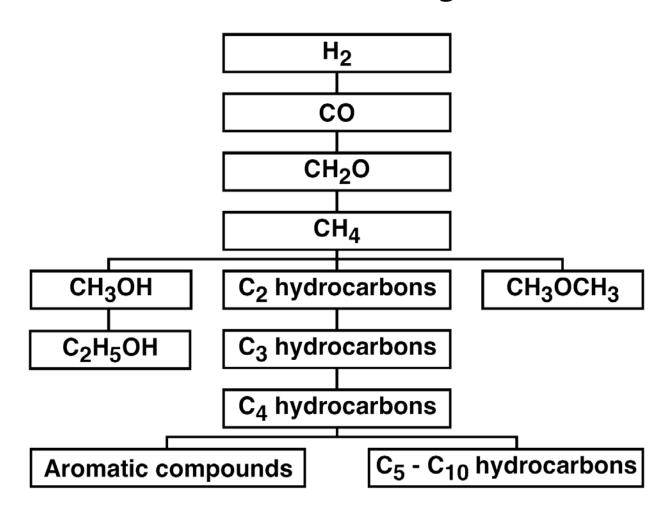




Soot



# Hierarchichal structure of combustion chemistry





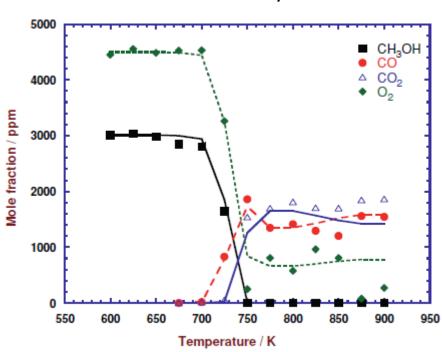
### Analysis tools for mechanism development

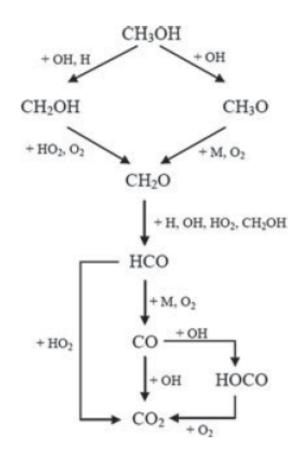
- Sensitivity analysis
- Rate-of-production analysis



### High-pressure oxidation of CH<sub>3</sub>OH

### Stoichiometric, 100 bar







### Sensitivity analysis

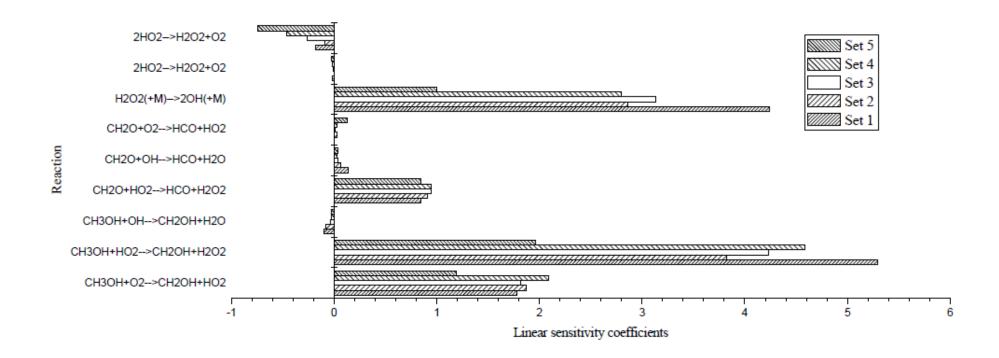
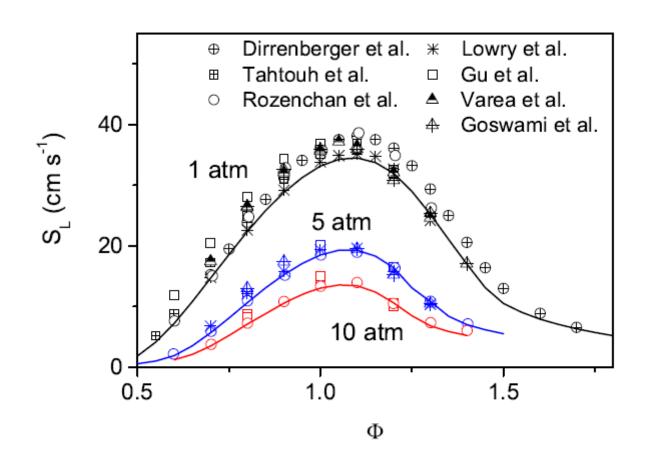


Figure 4: Linear sensitivity coefficients for CO for sets 1-5 given as  $(A_i/Y_j) \cdot (\delta Y_j/\delta A_i)$ .

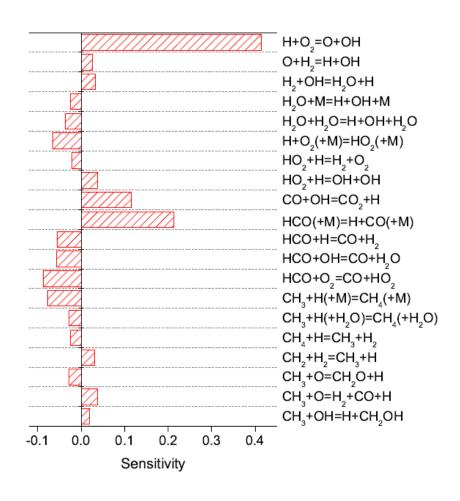


## Laminar flame speed for CH<sub>4</sub>



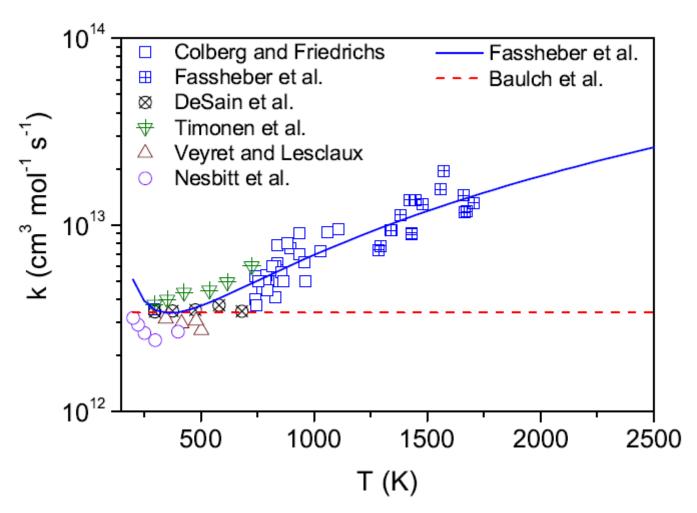


### CH<sub>4</sub> flame speed – sensitivity analysis





### Rate constant for HCO+O<sub>2</sub>

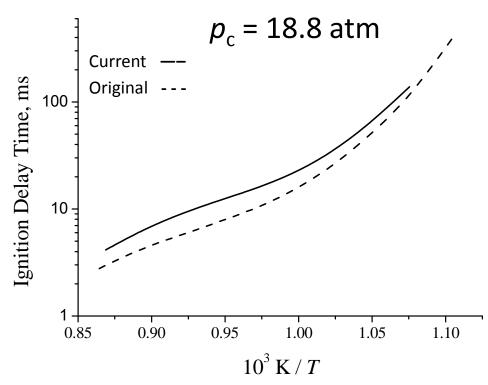






- $\dot{C}H_3 + O_2 \rightleftharpoons CH_3\dot{O}_2$
- $\bullet CH_3\dot{O}_2 + \dot{C}H_3 = CH_3\dot{O} + CH_3\dot{O}$

### CH<sub>4</sub>/air oxidation





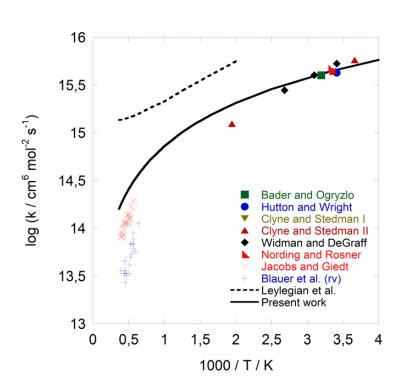
### Developing a detailed chemical kinetic model

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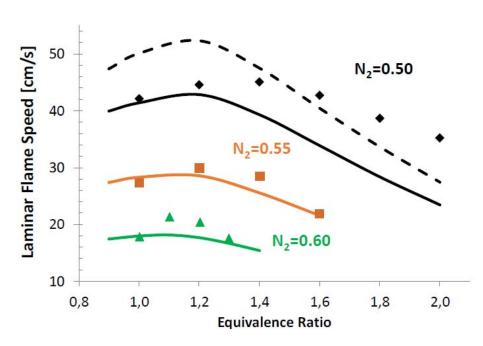


### Modeling approaches

#### Microscopic accuracy



#### Macroscopic accuracy





### Engineering (optimized) models



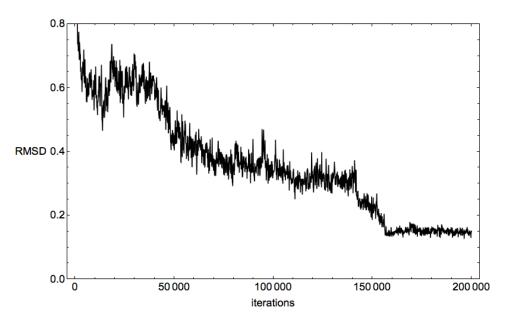
Do not make changes

- Thermo
- Rate constants

- Often impressive predictive capabilities
- Tend to disguise scientific issues



### Fundamental (non-optimized) models



- Scientifically sound
- Represent the present understanding of the chemistry
- Often lower accuracy compared to engineering models (within optimized regime)



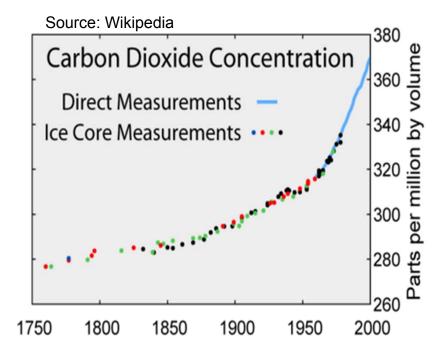
### Research issues

- Control pollutant formation
  - Unburned hydrocarbons
  - PAH
  - Soot
  - Nitrogen oxides
- Abate global warming
  - Use of biomass and bio-derived fuels
    - Formation of liquid bio-derived fuels
    - Kinetics of bio-derived fuels
    - Use of alcohols such as ethanol in Diesel engines
    - Chemistry of KCl
  - Oxy-fuel combustion
  - Formation and oxidation of soot



## The largest challenge: the climate issue





- A dramatic reduction of the CO<sub>2</sub> emission is required, according to UN recommendations
- The power industry, as a major contributor, is dedicated to this challenge



### Clean thermal energy: Combustion of hydrogen

$$H_2 + \frac{1}{2}O_2 \square H_2O$$



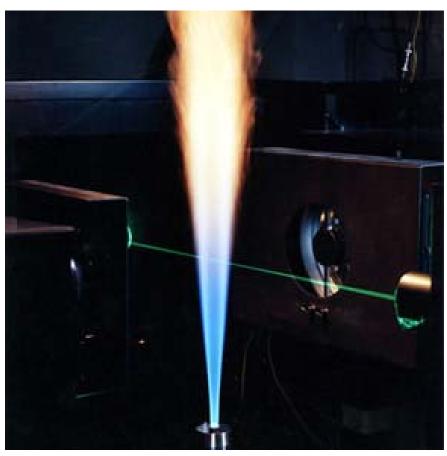


## The cleanest fossil fuel: natural gas

Natural gas is an easy fuel



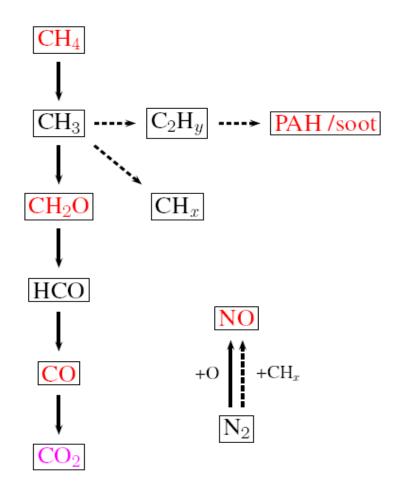
Yilmaz et al., 2009



Source: Sandia National Laboratories



## Pollutant formation - gaseous fuels





Emission control:
Combustion modification
Flue gas cleaning
Change of fuel
Increase efficiency

### **Solid fuels**





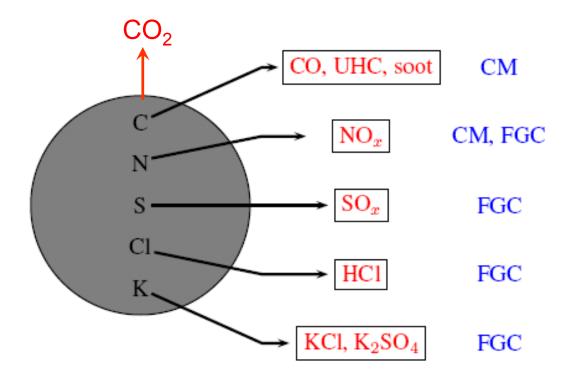
Solid fuels are challenging: handling, combustion, emissions, residual products



For coal: also CO<sub>2</sub>



### Pollutant formation – solid fuels



**CM**: Combustion modification

FGC: Flue gas cleaning



### **Sustainable Thermal Processes - Challenges**



- Thermal processes remain important:
  - Heat and power production
  - -Transport
  - Industrial processes
- Challenges:
  - Pollutant formation
  - Greenhouse gases
    - Efficiency
    - Fuel switching
    - New thermal processes