

ENGR 55500/G5300 REACTOR THERMAL-HYDRAULICS

Assignment #1 Solutions

Total = 46 marks

1. To build a containment wall for a nuclear reactor, concrete has been poured to form a 1.2m thick slab. The hydration of the concrete results in the equivalent of a constant heat source of $q_o''' = 100 \text{ W/m}^3$. If both surfaces of the concrete slab are kept at 16°C , determine the maximum temperature, T_{\max} , that would be reached, assuming a steady state condition. The thermal conductivity of the wet concrete may be taken as 0.84 W/mK .

Solution

Total = 10 marks

$$k \frac{\partial^2 T}{\partial x^2} + \dot{q}_G = \rho c \frac{\partial T}{\partial t}$$

For steady state, $\frac{\partial T}{\partial t} = 0$ therefore:

$$k \frac{d^2 T}{dx^2} + \dot{q}_G = 0$$

This is subject to the following boundary conditions:

1. By symmetry, $dT/dx = 0$ at $x = 0$

2. $T = T_s$ at $x = L$

Also note that for this problem \dot{q}_G is a constant.

Integrating the conduction equation:

$$\frac{dT}{dx} = -\frac{\dot{q}_G}{k}x + C_1$$

The constant C_1 can be evaluated using the first boundary condition:

$$0 = -\frac{\dot{q}_G}{k}(0) + C_1 \Rightarrow C_1 = 0$$

Integrating once again:

$$T = -\frac{\dot{q}_G}{2k}x^2 + C_2$$

The constant C_2 can be evaluated using the second boundary condition:

$$T_s = -\frac{\dot{q}_G}{2k}L^2 + C_2 \Rightarrow C_2 = T_s + \frac{\dot{q}_G}{2k}L^2$$

Therefore, the temperature distribution in the dam is:

$$T = T_s + \frac{\dot{q}_G}{2k}(L^2 - x^2)$$

8 marks

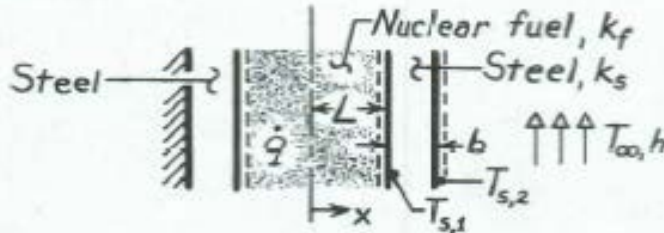
The maximum temperature occurs at $x = 0$:

$$T_{\max} = T_s + \frac{\dot{q}_G}{2k}(L^2 - (0)^2) = 16^\circ\text{C} + \frac{100 \text{ W/m}^3}{2(0.84 \text{ W/mK})}(0.6 \text{ m})^2 = 37^\circ\text{C}$$

2 marks

2. A nuclear fuel element of thickness, $2L$, is covered with a steel cladding of thickness b . Heat generated within the nuclear fuel at a rate \dot{q}_o''' (W/m^3) is removed by a coolant at T_∞ , which flows past the surface at $x = L+b$ and is characterized by a heat transfer coefficient h . The other surface at $x = -L-b$ is well insulated, and the fuel and steel have thermal conductivities of k_f and k_s , respectively.
- Obtain an expression for the temperature distribution $T(x)$ in the nuclear fuel. Express your answer in terms of \dot{q}_o''' , k_f , L , b , k_s , h and T_∞ .
 - Sketch the temperature distribution $T(x)$ for the entire system from $x = -L-b$ to $x = L+b$. At what x does the maximum temperature occur?

Total = 10 marks



ASSUMPTIONS: (1) One-dimensional heat transfer, (2) Steady-state conditions, (3) Uniform generation, (4) Constant properties, (5) Negligible contact resistance between fuel and cladding.

ANALYSIS: (a) The general solution to the heat equation, Eq. 3.19,

$$\frac{d^2 T}{dx^2} + \frac{\dot{q}}{k_f} = 0 \quad (-L \leq x \leq +L)$$

is
$$T = -\frac{\dot{q}}{2k_f} x^2 + C_1 x + C_2.$$

The insulated wall at $x = -(L+b)$ dictates that the heat flux at $x = -L$ is zero (for an energy balance applied to a control volume about the wall, $\dot{E}_{in} = \dot{E}_{out} = 0$). Hence

$$\left. \frac{dT}{dx} \right|_{x=-L} = -\frac{\dot{q}}{k_f} (-L) + C_1 = 0 \quad \text{or} \quad C_1 = -\frac{\dot{q}L}{k_f}$$

$$T = -\frac{\dot{q}}{2k_f} x^2 - \frac{\dot{q}L}{k_f} x + C_2.$$

The value of $T_{s,1}$ may be determined from the energy conservation requirement that $\dot{E}_g = \dot{q}_{cond} = \dot{q}_{conv}$, or on a unit area basis.

$$\dot{q}(2L) = \frac{k_s}{b} (T_{s,1} - T_{s,2}) = h(T_{s,2} - T_\infty).$$

Hence,

$$T_{s,1} = \frac{\dot{q}(2Lb)}{k_s} + T_{s,2} \quad \text{where} \quad T_{s,2} = \frac{\dot{q}(2L)}{h} + T_\infty$$

$$T_{s,1} = \frac{\dot{q}(2Lb)}{k_s} + \frac{\dot{q}(2L)}{h} + T_\infty.$$

Hence from Eq. (1),

$$T(L) = T_{s,1} = \frac{\dot{q}(2Lb)}{k_s} + \frac{\dot{q}(2L)}{h} + T_\infty = -\frac{3}{2} \frac{\dot{q}(L^2)}{k_f} + C_2$$

which yields

$$C_2 = T_\infty + \dot{q}L \left[\frac{2b}{k_s} + \frac{2}{h} + \frac{3}{2} \frac{L}{k_f} \right]$$

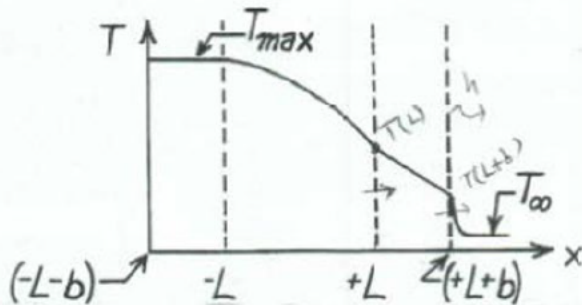
Hence, the temperature distribution for $(-L \leq x \leq +L)$ is

$$T = -\frac{\dot{q}}{2k_f} x^2 - \frac{\dot{q}L}{k_f} x + \dot{q}L \left[\frac{2b}{k_s} + \frac{2}{h} + \frac{3}{2} \frac{L}{k_f} \right] + T_{\infty}$$

a) 8 marks

(b) For the temperature distribution shown below,

$$\begin{aligned} (-L-b) \leq x \leq -L: & \quad dT/dx=0, T=T_{\max} \\ -L \leq x \leq +L: & \quad |dT/dx| \uparrow \text{ with } \uparrow x \\ +L \leq x \leq L+b: & \quad (dT/dx) \text{ is const.} \end{aligned}$$



b) 2 marks

3. Consider steady, one-dimensional heat conduction in a solid wall of thickness 15 cm without any internal heat generation. The thermal conductivity is not constant and varies with temperature as $k = 2.0 + 0.005T$ (W/mK), where T is in degrees Kelvin. If one surface of this wall is maintained at 150°C and the other at 50°C , determine the rate of heat conduction per square meter (W/m^2). Sketch the temperature distribution through the wall. Is it linear or non-linear?

No need to mark

$$\frac{d}{dx} \left(k \frac{dT}{dx} \right) = 0; \quad k = 2.0 + 0.005T$$

Integrate to get $k \frac{dT}{dx} = \text{constant} = -q''$ from Fourier's Law

$$-(2.0 + 0.005T) \frac{dT}{dx} = q''$$

$$-(2.0 + 0.005T) dT = q'' dx$$

Integrate again

$$-2T - \frac{0.005}{2} T^2 = q'' x + C$$

Apply B.C.'s.

$$\text{At } x=0, T=150^\circ\text{C} = 423\text{K}$$

$$-2(423) - 0.0025(423)^2 = C$$

$$\therefore C = -1293$$

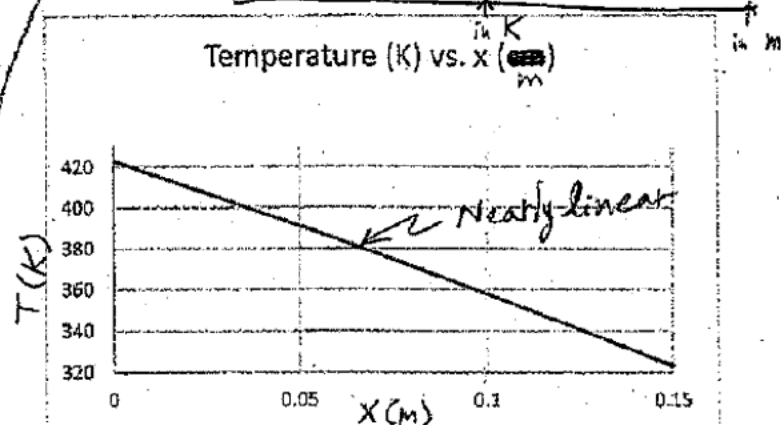
$$\text{At } x=0.15\text{m}, T=50^\circ\text{C} = 323\text{K}$$

$$-2 \times 323 - 0.0025(323)^2 = q'' \times 0.15 - 1293$$

$$q'' = 2575 \text{ W/m}^2$$

\therefore the temperature distribution is

$$0.0025T^2 + 2.0T = 1293 - 2575x$$



4. Consider a shielding wall of thickness L for a nuclear reactor. The wall receives gamma-rays such that heat is generated within the wall according to the relation,

$$q''' = q_0''' e^{-\mu x}$$

where q_0''' is incident radiation flux (constant), μ is a gamma attenuation coefficient, and x is the distance from the inner surface. Using this relation, derive expressions for the temperature distribution in the wall,

- if both the inner and outer temperatures are maintained at T_i at $x = 0$ and $x = L$,
- if the inner and outer temperatures are maintained at T_i at $x = 0$ and at T_o at $x = L$, respectively.
- For the temperature distribution obtained in (b), at what distance from the inner surface would the temperature be at a maximum?

Solution

$$q''' = q_0''' e^{-\mu x}$$

Total = 10 marks

Heat conduction eqn is $k \frac{d^2 T}{dx^2} + q_0''' e^{-\mu x} = 0$

Integrate twice to get

$$T(x) = -\frac{q_0''' e^{-\mu x}}{k\mu^2} - C_1 x - C_2$$

a) If $T(x=0) = T(x=L) = T_i$,

$$T_i = -\frac{q_0'''}{k\mu^2} - C_2$$

$$\therefore C_2 = -\left(T_i + \frac{q_0'''}{k\mu^2}\right)$$

At $x=L$,

$$T_i = -\frac{q_0''' e^{-\mu L}}{k\mu^2} - C_1 L + T_i + \frac{q_0'''}{k\mu^2}$$

$$C_1 = \frac{q_0'''}{k\mu^2 L} (1 - e^{-\mu L})$$

$$T(x) = T_i + \frac{q_0'''}{k\mu^2 L} \left[(1 - e^{-\mu x}) - \frac{x}{L} (1 - e^{-\mu L}) \right]$$

a) 2 marks

b) Apply B.C.s. $T(x=0) = T_i$ and $T(x=L) = T_o$

$$\Rightarrow T(x) = T_i + (T_o - T_i) \frac{x}{L} + \frac{q_0'''}{\mu^2 k} \left[\frac{x}{L} (e^{-\mu L} - 1) - (e^{-\mu x} - 1) \right]$$

b) 6 marks

c) Maximum temp is found at $\left. \frac{dT}{dx} \right|_{x=x_{max}} = 0$

$$x_{max} = -\frac{1}{\mu} \ln \left[\frac{\mu k}{q_0''' L} (T_i - T_o) + \frac{1}{\mu L} (1 - e^{-\mu L}) \right]$$

c) 2 marks

5. Consider a nuclear fuel shaped as a long slab of thickness, 7.5 cm, and with $k = 12 \text{ W/m}^\circ\text{C}$. The fuel generates heat internally at a rate of 10^5 W/m^3 . One side of the wall at $x = 0$ is insulated and the other side at $x = 7.5 \text{ cm}$ is exposed to a convection environment with a heat transfer coefficient of $h = 500 \text{ W/m}^2\text{C}$ and a fluid temperature of 90°C . Determine the temperature profile in the slab and calculate the maximum temperature in $^\circ\text{C}$ assuming steady one-dimensional heat conduction.

Total = 10 marks

Heat conduction eqn is

$$k \frac{d^2 T}{dx^2} + \dot{q}''' = 0 \quad (1)$$

B.C.s are : (i) $\frac{dT}{dx} = 0$ at $x = 0$ insulated surface

(ii) $-k \frac{dT}{dx} = h(T - T_f)$ at $x = L$ Convection

Integrate eqn (1) once

$$\frac{dT}{dx} = -\frac{\dot{q}'''}{k} x + C_1$$

Apply B.C. (i) $0 = 0 + C_1 \Rightarrow C_1 = 0$

Integrate again to get $T(x) = -\frac{\dot{q}'''}{2k} x^2 + C_2$

Apply B.C. (ii) $-k(-\frac{\dot{q}'''}{k} L) = h(-\frac{\dot{q}'''}{2k} L^2 + C_2 - T_f)$

$$\Rightarrow C_2 = \frac{\dot{q}''' L}{h} + \frac{\dot{q}'''}{2k} L^2 + T_f$$

$$\therefore T(x) = -\frac{\dot{q}'''}{2k} x^2 + \dot{q}''' L \left(\frac{1}{h} + \frac{L}{2k} \right) + T_f$$

$$= T_f + \frac{\dot{q}'''}{2k} \left(L^2 + \frac{2kL}{h} - x^2 \right)$$

7 marks

The max. temperature occurs at $x = 0$

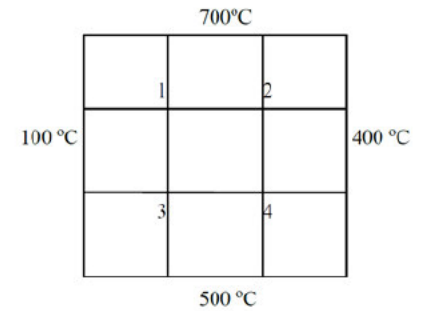
$$\therefore T_{\max} = T_f + \frac{\dot{q}'''}{2k} \left(L^2 + \frac{2kL}{h} \right)$$

$$= 90 + \frac{10^5}{2 \times 12} \left((0.075)^2 + \frac{2 \times 12 \times 0.075}{500} \right)$$

$$= \underline{\underline{128^\circ\text{C}}}$$

3 marks

6. For the square solid without any heat generation shown on the right, numerically solve the steady state 2-D heat conduction equation for the temperatures $T_1 - T_4$. Thermal conductivity is $k = 1.5 \text{ W/mK}$ and each square mesh is 2 cm wide. The four surfaces are kept at constant temperatures as shown.



Total = 6 marks

Solution:

Since

$$T_{m+1,n} + T_{m-1,n} + T_{m,n+1} + T_{m,n-1} - 4T_{m,n} = 0$$

2 marks for this equation

For node 1, $700 + 100 + T_2 + T_3 - 4T_1 = 0$

For node 2, $700 + T_1 + T_4 + 400 - 4T_2 = 0$

For node 3, $T_1 + 100 + 500 + T_4 - 4T_3 = 0$

For node 4, $T_2 + T_3 + 500 + 400 - 4T_4 = 0$

$$T_1 = 412.5 \text{ } ^\circ\text{C}$$

$$T_2 = 487.5 \text{ } ^\circ\text{C}$$

$$T_3 = 362.5 \text{ } ^\circ\text{C}$$

$$T_4 = 437.5 \text{ } ^\circ\text{C}$$

4 marks (1 mark for each correct answer)