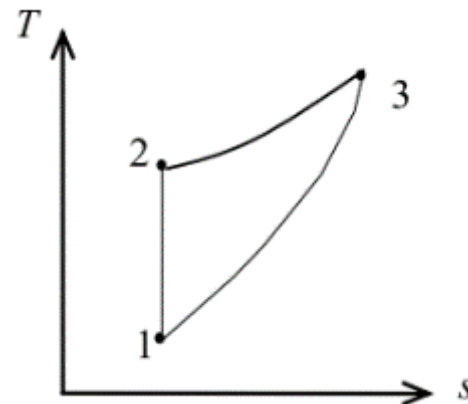
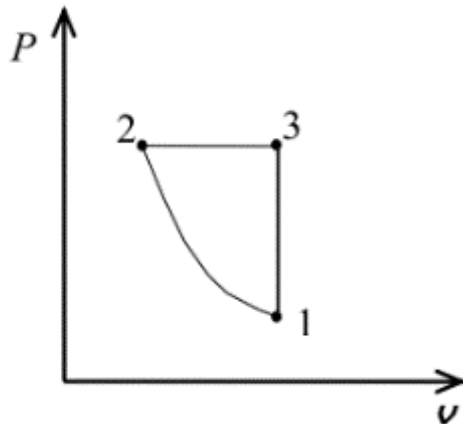


Reference Answers of Homework 8

1. An ideal gas is contained in a piston-cylinder device and undergoes a power cycle as follows: 1-2 isentropic compression from an initial temperature $T_1 = 20^\circ\text{C}$ with a compression ratio $r = 5$; 2-3 constant pressure heat addition; 3-1 constant volume heat rejection. The gas has constant specific heats with $c_v = 0.7 \text{ kJ/kg}\cdot\text{K}$ and $R = 0.3 \text{ kJ/kg}\cdot\text{K}$.
- (a) Sketch the P - v and T - s diagrams for the cycle;
 - (b) Determine the heat and work interactions for each process, in kJ/kg ;
 - (c) Determine the cycle thermal efficiency;
 - (d) Obtain thermal efficiency as a function of compression ratio r and adiabatic coefficient k .

(a) The P - v and T - s diagrams of the cycle are shown in the figures.



(b) Noting that $c_p = c_v + R = 0.7 + 0.3 = 1.0 \text{ kJ/kg} \cdot \text{K}$

$$k = \frac{c_p}{c_v} = \frac{1.0}{0.7} = 1.429$$

Process 1-2: Isentropic compression

$$T_2 = T_1 \left(\frac{v_1}{v_2} \right)^{k-1} = T_1 r^{k-1} = (293 \text{ K})(5)^{0.429} = 584.4 \text{ K}$$

$$w_{1-2,\text{in}} = c_v (T_2 - T_1) = (0.7 \text{ kJ/kg} \cdot \text{K})(584.4 - 293) \text{ K} = \mathbf{204.0 \text{ kJ/kg}}$$

$$q_{1-2} = \mathbf{0}$$

From ideal gas relation, $\frac{T_3}{T_2} = \frac{v_3}{v_2} = \frac{v_1}{v_2} = r \longrightarrow T_3 = (584.4)(5) = 2922$

Process 2-3: Constant pressure heat addition

$$\begin{aligned} w_{2-3,\text{out}} &= \int_2^3 P d v = P_2 (v_3 - v_2) = R(T_3 - T_2) \\ &= (0.3 \text{ kJ/kg} \cdot \text{K})(2922 - 584.4) \text{ K} = \mathbf{701.3 \text{ kJ/kg}} \end{aligned}$$

$$\begin{aligned} q_{2-3,\text{in}} &= w_{2-3,\text{out}} + \Delta u_{2-3} = \Delta h_{2-3} \\ &= c_p (T_3 - T_2) = (1 \text{ kJ/kg} \cdot \text{K})(2922 - 584.4) \text{ K} = \mathbf{2338 \text{ kJ/kg}} \end{aligned}$$

Process 3-1: Constant volume heat rejection

$$q_{3-1,\text{out}} = \Delta u_{1-3} = c_v (T_3 - T_1) = (0.7 \text{ kJ/kg} \cdot \text{K})(2922 - 293) \text{ K} = \mathbf{1840.3 \text{ kJ/kg}}$$

$$w_{3-1} = \mathbf{0}$$

(c) Net work is $w_{\text{net}} = w_{2-3,\text{out}} - w_{1-2,\text{in}} = 701.3 - 204.0 = 497.3 \text{ kJ/kg} \cdot \text{K}$

The thermal efficiency is then $\eta_{\text{th}} = \frac{w_{\text{net}}}{q_{\text{in}}} = \frac{497.3 \text{ kJ}}{2338 \text{ kJ}} = 0.213 = \mathbf{21.3\%}$

(d) The expression for the cycle thermal efficiency is obtained as follows:

$$\begin{aligned} \frac{R}{c_p} &= \frac{c_p - c_v}{c_p} = 1 - \frac{c_v}{c_p} = 1 - \frac{1}{k} \\ \eta_{\text{th}} &= \frac{w_{\text{net}}}{q_{\text{in}}} = \frac{w_{2-3,\text{out}} - w_{1-2,\text{in}}}{q_{\text{in}}} \\ &= \frac{R(T_3 - T_2) - c_v(T_2 - T_1)}{c_p(T_3 - T_2)} \\ &= \frac{R}{c_p} - \frac{c_v(T_1 r^{k-1} - T_1)}{c_p(r T_1 r^{k-1} - T_1 r^{k-1})} \end{aligned}$$

$$\begin{aligned} &= \frac{R}{c_p} - \frac{c_v T_1 r^{k-1} \left(1 - \frac{T_1}{T_1 r^{k-1}} \right)}{c_p T_1 r^{k-1} (r - 1)} \\ &= \frac{R}{c_p} - \frac{1}{k(r - 1)} \left(1 - \frac{T_1}{T_1 r^{k-1}} \right) \\ &= \frac{R}{c_p} - \frac{1}{k(r - 1)} \left(1 - \frac{1}{r^{k-1}} \right) \\ &= \left(1 - \frac{1}{k} \right) - \frac{1}{k(r - 1)} \left(1 - \frac{1}{r^{k-1}} \right) \end{aligned}$$

2. An ideal Otto cycle has a compression ratio of 8. At the beginning of the compression process, air is at 95 kPa and 27°C, and 750 kJ/kg of heat is transferred to air during the constant-volume heat-addition process. Using constant specific heats at room temperature, determine:

- (a) the pressure and temperature at the end of the heat-addition process,
- (b) the net work output,
- (c) the thermal efficiency, and
- (d) the mean effective pressure for the cycle.

(a) Process 1-2: isentropic compression.

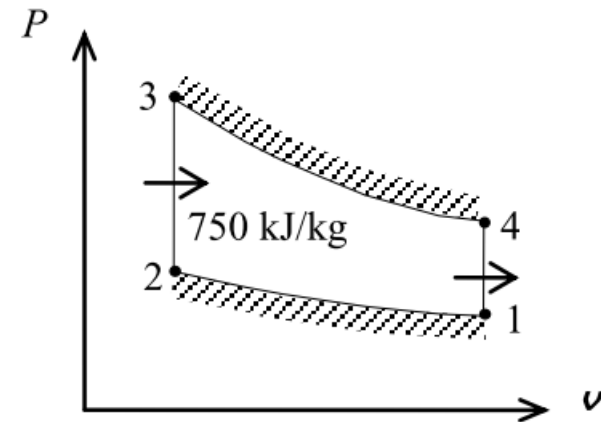
$$T_2 = T_1 \left(\frac{\nu_1}{\nu_2} \right)^{k-1} = (300\text{K})(8)^{0.4} = 689\text{ K}$$

$$\frac{P_2 \nu_2}{T_2} = \frac{P_1 \nu_1}{T_1} \longrightarrow P_2 = \frac{\nu_1}{\nu_2} \frac{T_2}{T_1} P_1 = (8) \left(\frac{689\text{ K}}{300\text{ K}} \right) (95\text{ kPa}) = 1745\text{ kPa}$$

Process 2-3: $q_{23,\text{in}} = u_3 - u_2 = c_v (T_3 - T_2)$
 $750\text{ kJ/kg} = (0.718\text{ kJ/kg} \cdot \text{K})(T_3 - 689)\text{K}$

$$T_3 = \mathbf{1734\text{ K}}$$

$$\frac{P_3 \nu_3}{T_3} = \frac{P_2 \nu_2}{T_2} \longrightarrow P_3 = \frac{T_3}{T_2} P_2 = \left(\frac{1734\text{ K}}{689\text{ K}} \right) (1745\text{ kPa}) = \mathbf{4392\text{ kPa}}$$



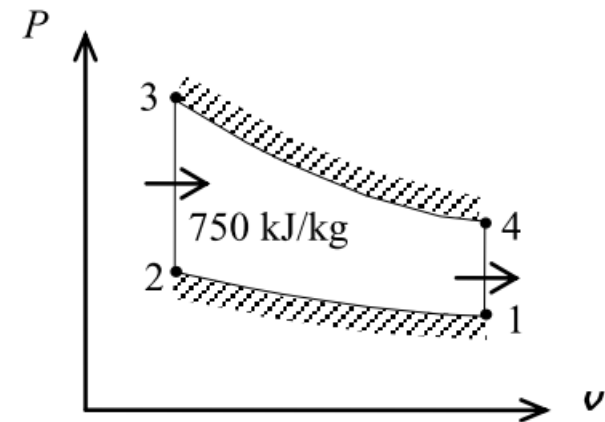
(b) Process 3-4: isentropic expansion.

$$T_4 = T_3 \left(\frac{\nu_3}{\nu_4} \right)^{k-1} = (1734 \text{ K}) \left(\frac{1}{8} \right)^{0.4} = 755 \text{ K}$$

Process 4-1: $\nu = \text{constant}$ heat rejection.

$$q_{\text{out}} = u_4 - u_1 = c_\nu (T_4 - T_1) = (0.718 \text{ kJ/kg} \cdot \text{K})(755 - 300) \text{ K} = 327 \text{ kJ/kg}$$

$$w_{\text{net,out}} = q_{\text{in}} - q_{\text{out}} = 750 - 327 = \mathbf{423 \text{ kJ/kg}}$$



(c)
$$\eta_{\text{th}} = \frac{w_{\text{net,out}}}{q_{\text{in}}} = \frac{423 \text{ kJ/kg}}{750 \text{ kJ/kg}} = \mathbf{56.4\%}$$

(d)
$$\nu_1 = \frac{RT_1}{P_1} = \frac{(0.287 \text{ kPa} \cdot \text{m}^3/\text{kg} \cdot \text{K})(300 \text{ K})}{95 \text{ kPa}} = 0.906 \text{ m}^3/\text{kg} = \nu_{\text{max}}$$

$$\nu_{\text{min}} = \nu_2 = \frac{\nu_{\text{max}}}{r}$$

$$\text{MEP} = \frac{w_{\text{net,out}}}{\nu_1 - \nu_2} = \frac{w_{\text{net,out}}}{\nu_1 (1 - 1/r)} = \frac{423 \text{ kJ/kg}}{(0.906 \text{ m}^3/\text{kg})(1 - 1/8)} \left(\frac{\text{kPa} \cdot \text{m}^3}{\text{kJ}} \right) = \mathbf{534 \text{ kPa}}$$

3. An air-standard Diesel cycle has a compression ratio of 16 and a cutoff ratio of 2. At the beginning of the compression process, air is at 95 kPa and 27°C. Using constant specific heats at room temperature, determine:

- (a) the temperature after the heat-addition process,;
- (b) the thermal efficiency;
- (c) the mean effective pressure for the cycle.

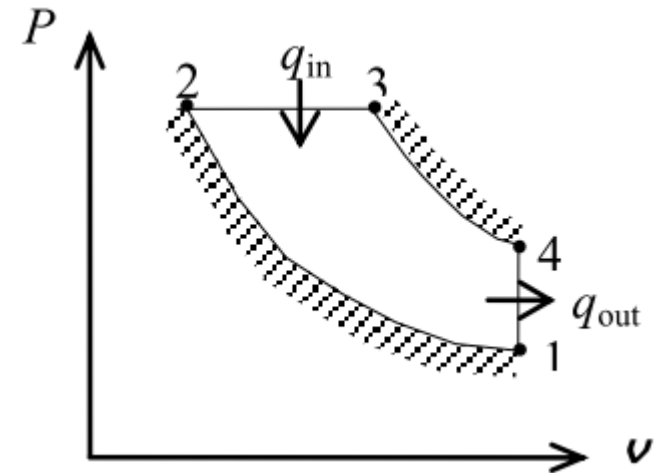
(a)

Process 1-2: isentropic compression.

$$T_2 = T_1 \left(\frac{\nu_1}{\nu_2} \right)^{k-1} = (300\text{K})(16)^{0.4} = 909.4\text{K}$$

Process 2-3: $P = \text{constant}$ heat addition.

$$\frac{P_3 \nu_3}{T_3} = \frac{P_2 \nu_2}{T_2} \longrightarrow T_3 = \frac{\nu_3}{\nu_2} T_2 = 2T_2 = (2)(909.4\text{K}) = \mathbf{1818.8\text{K}}$$



$$(b) \quad q_{in} = h_3 - h_2 = c_p (T_3 - T_2) = (1.005 \text{ kJ/kg} \cdot \text{K})(1818.8 - 909.4) \text{ K} = 913.9 \text{ kJ/kg}$$

Process 3-4: isentropic expansion.

$$T_4 = T_3 \left(\frac{v_3}{v_4} \right)^{k-1} = T_3 \left(\frac{2v_2}{v_4} \right)^{k-1} = (1818.8 \text{ K}) \left(\frac{2}{16} \right)^{0.4} = 791.7 \text{ K}$$

Process 4-1: v = constant heat rejection.

$$q_{out} = u_4 - u_1 = c_v (T_4 - T_1) = (0.718 \text{ kJ/kg} \cdot \text{K})(791.7 - 300) \text{ K} = 353 \text{ kJ/kg}$$

$$\eta_{th} = 1 - \frac{q_{out}}{q_{in}} = 1 - \frac{353 \text{ kJ/kg}}{913.9 \text{ kJ/kg}} = \mathbf{61.4\%}$$

$$(c) \quad w_{net,out} = q_{in} - q_{out} = 913.9 - 353 = 560.9 \text{ kJ/kg}$$

$$v_1 = \frac{RT_1}{P_1} = \frac{(0.287 \text{ kPa} \cdot \text{m}^3/\text{kg} \cdot \text{K})(300 \text{ K})}{95 \text{ kPa}} = 0.906 \text{ m}^3/\text{kg} = v_{max}$$

$$v_{min} = v_2 = \frac{v_{max}}{r}$$

$$\text{MEP} = \frac{w_{net,out}}{v_1 - v_2} = \frac{w_{net,out}}{v_1(1 - 1/r)} = \frac{560.9 \text{ kJ/kg}}{(0.906 \text{ m}^3/\text{kg})(1 - 1/16)} \left(\frac{\text{kPa} \cdot \text{m}^3}{\text{kJ}} \right) = \mathbf{660.4 \text{ kPa}}$$

4. Consider a simple Brayton cycle using air as the working fluid. It has a pressure ratio of 12 and a maximum cycle temperature of 600 °C. The compressor is operated with 100 kPa and 15 °C at the inlet. Please use constant specific heats at room temperature to determine which process below will have a larger impact on the back-work ratio.

(a) a compressor isentropic efficiency of 80 percent;

(b) a turbine isentropic efficiency of 80 percent.

For the compression process,

$$T_{2s} = T_1 \left(\frac{P_2}{P_1} \right)^{(k-1)/k} = (288 \text{ K})(12)^{0.4/1.4} = 585.8 \text{ K}$$

$$\eta_C = \frac{h_{2s} - h_1}{h_2 - h_1} = \frac{c_p(T_{2s} - T_1)}{c_p(T_2 - T_1)} \longrightarrow T_2 = T_1 + \frac{T_{2s} - T_1}{\eta_C}$$

$$= 288 + \frac{585.8 - 288}{0.80}$$

$$= 660.2 \text{ K}$$

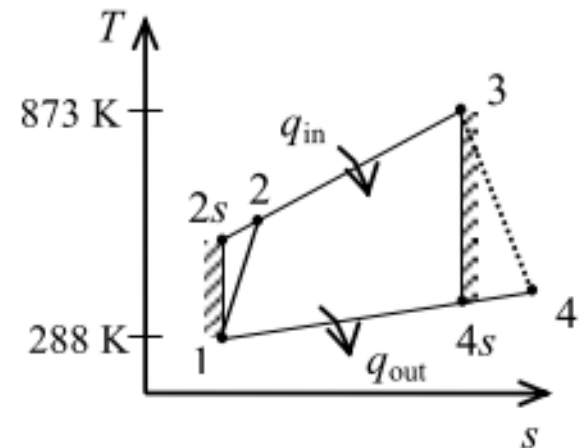
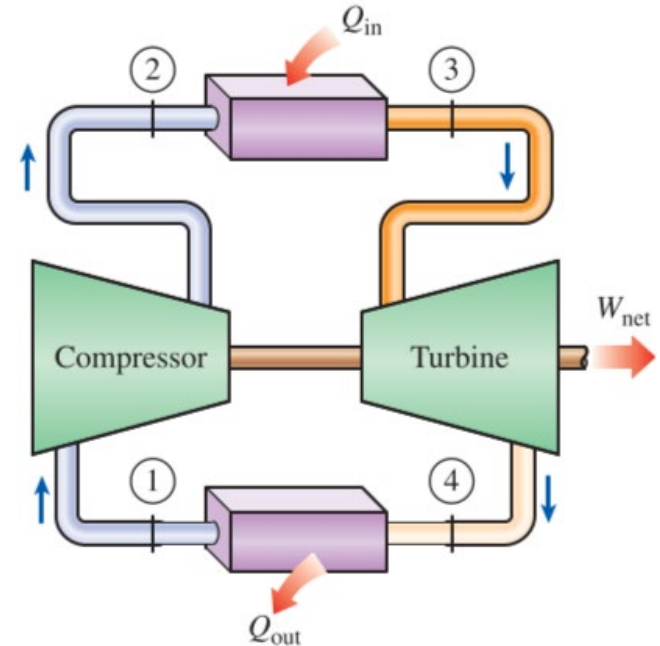
For the expansion process,

$$T_{4s} = T_3 \left(\frac{P_4}{P_3} \right)^{(k-1)/k} = (873 \text{ K}) \left(\frac{1}{12} \right)^{0.4/1.4} = 429.2 \text{ K}$$

$$\eta_T = \frac{h_3 - h_4}{h_3 - h_{4s}} = \frac{c_p(T_3 - T_4)}{c_p(T_3 - T_{4s})} \longrightarrow T_4 = T_3 - \eta_T(T_3 - T_{4s})$$

$$= 873 - (0.80)(873 - 429.2)$$

$$= 518.0 \text{ K}$$



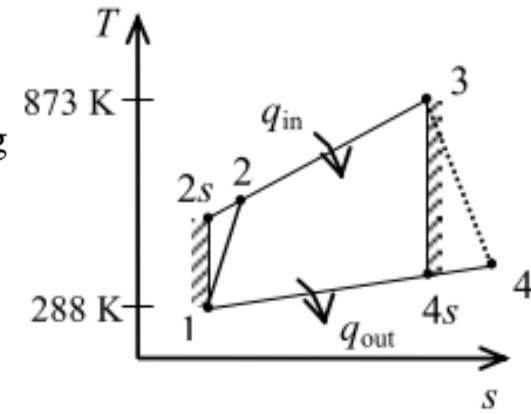
The isentropic and actual work of compressor and turbine are

$$W_{\text{Comp},s} = c_p (T_{2s} - T_1) = (1.005 \text{ kJ/kg} \cdot \text{K})(585.8 - 288) \text{ K} = 299.3 \text{ kJ/kg}$$

$$W_{\text{Comp}} = c_p (T_2 - T_1) = (1.005 \text{ kJ/kg} \cdot \text{K})(660.2 - 288) \text{ K} = 374.1 \text{ kJ/kg}$$

$$W_{\text{Turb},s} = c_p (T_3 - T_{4s}) = (1.005 \text{ kJ/kg} \cdot \text{K})(873 - 429.2) \text{ K} = 446.0 \text{ kJ/kg}$$

$$W_{\text{Turb}} = c_p (T_3 - T_4) = (1.005 \text{ kJ/kg} \cdot \text{K})(873 - 518.0) \text{ K} = 356.8 \text{ kJ/kg}$$



The back work ratio for 80% efficient compressor and isentropic turbine case is

$$r_{\text{bw}} = \frac{W_{\text{Comp}}}{W_{\text{Turb},s}} = \frac{374.1 \text{ kJ/kg}}{446.0 \text{ kJ/kg}} = \mathbf{0.8387}$$

The back work ratio for 80% efficient turbine and isentropic compressor case is

$$r_{\text{bw}} = \frac{W_{\text{Comp},s}}{W_{\text{Turb}}} = \frac{299.3 \text{ kJ/kg}}{356.8 \text{ kJ/kg}} = \mathbf{0.8387}$$

The two results are identical.