## Laws of Thermodynamics

- 1. Energy is conserved, it is neither created nor destroyed
  - a. dU = TdS PdV = Q + W
- 2. Entropy always increases in the universe
  - a.  $dS > \frac{dQ}{T_{surr}}$
- 3. Entropy is constant at absolute  $0 \circ K$  (pure perfect crystal  $\Rightarrow S = 0$ )
  - a.  $S_0 = k_B \ln \ln (1) = 0$
- 4. Fundamental Equation:  $dU = TdS PdV + \Sigma$  $\mu_i dN_i$

## **Properties**

- Intensive = doesn't change with system size/extent
  - $\circ T, P, \mu, \rho, c_P/c_V \qquad u, h, g, f$ s, v, nk, C, viscosity
- Extensive = changes with system size/extent
  - $\circ$   $S, V, N, m, C_P/C_V$  U, H, G, F
- Composite = combination of extensive and intensive properties
  - o Ratio of extensive properties = intensive property  $(\rho = \frac{m}{\nu})$
  - o "Specific" =  $\frac{extensive\ property}{mass}$  "Molar" =  $\frac{extensive\ property}{mole}$  = lowercase
- **Constants**:  $R = k_B N_A = 8.3144 \frac{J}{K*mol} \left( \frac{m^3*Pa}{K*mol} \right) \left( \frac{kg*m^2}{s^2*K*mol} \right) = 0.082057 \frac{L*atm}{K*mol} = 1.987204 \frac{kcal}{K*mol}$ 
  - Boltzmann:  $k_B = 1.380648x10^{-23} \frac{J}{K}$  Avogadro:  $N_A = 6.022140x10^{23} mol^{-1}$
  - <u>Faraday</u>:  $F = 96485.332 \frac{c}{mal}$ • STP° = 273.15°K, 1bar = 105Pa

### **Equations of State & Equilibrium:** f(P,V,T) = 0

- Ideal:  $PV = nRT = Nk_BT$  P = CRT  $PM_W = \rho RT$  Low P, High T
- Van der Waals, (Soave-)Redlich-Kwong, Peng-Robinson, Virial
- Antoine Equation:  $\ln \ln (P^{sat}) = A \frac{B}{C+T} A, B, C = \text{empirical constants}$  Clausius-Clapeyron Equation:  $\frac{dP}{dT} = \frac{s^{\beta} s^{\alpha}}{v^{\beta} v^{\alpha}} = \frac{\Delta H_{vap}}{(v^{\beta} v^{\alpha})T}$  for phase  $\alpha\beta$  equilibrium
- Fugacity f = P of Ideal Gas @ T & G of real gas  $\phi = \frac{I}{P} =$  fugacity coeff
  - o "Escaping tendency" different than mechanical, measured pressure
  - o Describes chemical equilibrium:  $f_a = f_b$   $\mu_i \mu_i^\circ = RT \ln \ln \left(\frac{f_i}{f_i^\circ}\right)$
  - $\circ$  Substitute for P in  $PV = nRT \Longrightarrow fV = nRT$  to describe real gases

  - o  $d\mu = dg = -sdT + vdP \implies \Delta T = 0, PV = nRT \implies d\mu = RTd \ln \ln P$ o  $\ln (\phi) = \int_0^P \frac{V V_{ideal}}{nRT} dP$   $Z = \frac{PV}{nRT} \implies \ln (\phi) = \int_0^P \frac{Z 1}{P} dP$ o Condensed phases  $\implies$  Poynting:  $f = \phi_{sat} P_{sat} e^{\frac{V(P P_{sat})}{RT}}$  because  $f_{g,sat} = f_{l,s,sat}$

  - o Lewis Fugacity rule:  $\phi_{i,pure} = \phi_{i,in\; mixture} \Longrightarrow f_{i,pure} = y_i f_{i,in\; mixture}$
- Activity  $a_i = exp \; exp \; \left(\frac{\mu_i \mu_i^{\circ}}{RT}\right) = \gamma_i x_i = \frac{f_i}{P^{\circ}} \quad \gamma_i = \text{activity coeff} \quad a_{solid, liquid} = 1$ 
  - o "Effective concentration" of a species in a mixture/reaction
  - o Akin to chemical potential in theory but used differently
  - o Integrate fugacity:  $d\mu = RTd \ln \ln P \implies \mu_i = \mu_i^{\circ} RT \ln \ln (a_i)$
  - o Substitute for C in  $K = \frac{c_C c_D}{c_A c_B}$  or  $r = k C_A^n$  to describe real solutions

<u>Caloric Theory</u> = obsolete theory that heat is a self-repellent fluid called caloric that could be attached to matter and later released from it <u>Bridgeman</u> = organization of 28 elementary thermodynamic equations. Shows how T, P, V, S, U, H, G, F change with each held constant

### **Fundamental Parameters**

- Conjugate Variables: (T,S) (P,V)  $(\mu,N)$  (force, displacement) (intensive, extensive)
  - o  $T * S = Q[=]J \Rightarrow T$  gradients drive S change
    - Energy conservation, thermodynamics
  - o P \* V = W = I gradients drive V change
    - Momentum conservation, fluid dynamics
  - $\mu * N = M = J \Rightarrow \mu$  gradients drive N change
    - Mass conservation, chemistry
- <u>Temperature</u>  $T = (-1)^{\circ}K, {\circ}C, {\circ}F, {\circ}R$ 
  - Measure of submicroscopic motions and vibrations (NOT heat)
  - Thermal equilibrium  $\Rightarrow T_{sys} = T_{surr}$
- Entropy  $S = \frac{J}{\kappa}$ 
  - o Measure of disorder, always increasing in universe
  - $\circ$   $S = k_B \ln \ln (\Omega)$ ,  $\Omega = number of microstates$
  - o Only measured indirectly through Maxwell Relations
  - o At equilibrium entropy is at a maximum
- Pressure  $P = \frac{J}{m^3} = Pa = \frac{N}{m^2} = \frac{kg}{m*s^2}$ , bar, atm, mmHg
  - o Force applied over area, normal stress
  - o Mechanical equilibrium  $\Rightarrow P_{sys} = P_{surr}$
- Volume  $V = m^3 = \frac{J}{Pa}, L, ft^3$ 
  - Measure of physical space taken up by matter (NOT empty space)
- Chemical Potential  $\mu = J$  (NOT chemical potential energy)
  - o Energy changed through chemical reaction/phase transition
  - $\circ \quad \mu = (\frac{dU}{dN})_{S,V,N} = (\frac{dH}{dN})_{S,P,N} = (\frac{dG}{dN})_{T,P,N} = (\frac{dF}{dN})_{T,V,N}$
  - o Molecules move down chemical potential gradients (like gravity)
  - o Diffusive equilibrium  $\Rightarrow \mu_{sys} = \mu_{surr}$
- Composition N [=] #, unitless
  - o Measure of the number of particles in a system
  - $\circ N[=] \# n = \frac{N}{N_A} [=] mol$

## Thermodynamic Potentials

Definitions change based on context/process under consideration  $\{x,y,z\}$  = natural variables (held constant  $\Rightarrow$  potential =  $W_{max\,useful}$ )

- Internal Energy f(S, V, N)
  - $\circ \quad dU = TdS PdV + \sum \quad \mu_i dN_i \quad U = TS PV + \sum \quad \mu_i N_i \quad \Delta U = Q + W_{PV} + W_{Isochoric}$
  - o Described explicitly by microscopic energies...
    - kinetic (translation, rotation, vibration)
    - potential (chemical, electrical, nuclear)
  - $\circ dU(T,V) = C_V dT + \left(T\left(\frac{dP}{dT}\right)_V P\right) dV$
  - $0 \quad dU(T,P) = (C_P \alpha PV)dT + (\beta_T P \alpha T)VdP$
  - o Ideal Gas:  $U = \frac{3}{2}nRT$
- **Enthalpy**  $f{S,P,N}$ 
  - $\circ \quad dH = TdS + VdP + \sum \qquad \mu_i dN_i \qquad H = TS + \sum \qquad \mu_i N_i = U + PV \qquad \qquad \Delta H = Q + W_{Isochoric}$
  - $\circ$  The energy to create system plus the work to make room for it dH = d(U + PV)
  - o  $@dP = 0 \Longrightarrow \Delta H =$  heat from chemical reaction and external heat transfer
    - $\Delta H = + \Rightarrow$  endothermic reaction,  $\Rightarrow$  exothermic reaction
  - $\circ dH(T,P) = C_P dT + V(1 \alpha T) dP$
  - o Enthalpy of... formation, rxn, vap, fus, sol, combustion, mix
- Gibbs Energy  $f\{T, P, N\}$ 
  - $\circ \quad dG = -SdT + VdP + \sum \quad \mu_i dN_i \quad G = \sum \quad \mu_i N_i = H TS \quad \Delta G = \Delta H T\Delta S = W_{Isochoric}$
  - o Chemical reaction spontaneity:  $\Delta T=0, \Delta P=0 \implies$  only  $\Delta \mu \neq 0$  can vary
  - $\Delta G = \Rightarrow$  spontaneous,  $+ \Rightarrow$  non-spontaneous,  $0 \Rightarrow$  equilibrium •  $\Delta G^{\circ}_{R} = -RT \ln (K_{eq})$   $\Delta G^{\circ}_{R} = -nFE^{\circ}$   $E^{\circ} = Standard\ cell\ potential\ [=] \frac{J}{c} = V$
  - o Gibbs-Duhem:  $0 = -SdT + VdP + \sum N_i d\mu_i$
- Helmholtz Energy  $f\{T, V, N\}$ 
  - $\circ \quad dF = -SdT PdV + \sum \qquad \mu_i dN_i \qquad F = -PV + \sum \qquad \mu_i N_i = U TS \qquad \Delta F = \Delta U T\Delta S = W_{PV} + W_{Isochoric}$
  - Chemical reaction spontaneity:  $\Delta T = 0, \Delta V = 0 \implies$  only  $\Delta \mu \neq 0$  can vary  $\Delta F = \implies$  spontaneous,  $+ \implies$  non-spontaneous,  $0 \implies$  equilibrium
- d(PV) = d(H U) = d(G F) d(TS) = d(U F) = d(H G)
- Exergy (Availability)
  - $\circ \quad B = U T_R S + P_R V \sum \qquad \mu_{i,R} N_i \ B = H T_R S \qquad \qquad B = F + P_R V \qquad \qquad B = G$
  - o Exergy = U + heat/entropic loss + available PV work + available chemical energy
  - o Measures how far system is from equilibrium with surroundings
    - A system in equilibrium with its surroundings has 0 exergy
  - Describes amount of available work in a system (usefulness of streams in chemical plant)
- Free Energy: energy that is readily released/freed (G,F)
- Free Entropy: entropy that is readily released/freed

 $\circ$  Helmholtz Free Entropy (Massieu Potential)  $[\Phi]$ 

• 
$$\Phi = -\frac{F}{T} = S - \frac{1}{T}U$$
  $f\{\frac{1}{T}, V, N\}$ 

 $\circ$  Gibbs Free Entropy (Planck Potential) [arepsilon]

• 
$$\mathcal{E} = -\frac{G}{T} = \Phi - \frac{P}{T}V$$
  $f\{\frac{1}{T}, \frac{P}{V}, N\}$ 

• **Grand Potential**  $f\{T, V, \mu\}$ 

$$\circ \quad d\Phi_G = -SdT - PdV - Nd\mu \; \Phi_G = -PV$$

o The energy extractable from a system by shrinking it to nothing

Theoretical Potentials

o Potential 6  $f\{S, P, \mu\}$ 

• 
$$dP_6 = TdS + VdP - Nd\mu$$
  $P_6 = TS$ 

• The energy extractable from a system by cooling it into perfect crystal?

o Potential 7  $f\{S, V, \mu\}$ 

• 
$$dP_7 = TdS - PdV - Nd\mu$$
  $P_7 = TS - PV$ 

o Potential 8 
$$f\{T,P,\mu\}$$
 
$$\bullet dP_8 = -SdT + VdP - Nd\mu \qquad P_8 = 0$$

## **Energy Transfer**

Path Dependent: Area under curve on graph, so curve matters, not just ends

- Heat
  - Thermal energy transfer (NOT temperature)

$$0 dQ = TdS Q = mC_P\Delta T He$$

$$dQ = TdS$$
  $Q = mC_P\Delta T$  Heat Equation:  $\frac{dT}{dt} - \alpha \nabla^2 T = 0$ 

- $\circ$  <u>TS Diagram</u>, area under/enclosed by curve is Q
  - Graph isobars & isochors for all fundamental parameters
- $\circ$  Sensible heat =  $\Delta T$ , Latent heat = phase change ( $\Delta T = 0$ )
- Work
  - Mechanical energy transfer

o 
$$dW = PdV$$
  $W = Fd = PA_s$  Wave Equation:  $\frac{d^2u}{dt^2} - c^2\nabla^2u = 0$ 

- o PV Diagram: area under/enclosed by curve is W
  - Graph isotherms & adiabats for all fundamental parameters
- o  $W_{PV} = W_{reversible} =$  Mechanical work
  - Volume change  $(\Delta V)$  caused a by gradient between system pressure and external pressure (P)
  - Can be performed by system on surroundings or by surroundings on system
- $\circ$   $W_{isochoric} = W_{shaft} = W_{irreversible} =$ Non-mechanical work
  - No volume change, like pushing a viscous fluid or friction
  - Only performed on sys by surr, never on surr by sys

## **Processes/Systems**

Model complex processes by series of these processes

Heat reservoir (water bath) ≈ Pressure reservoir (atmosphere)

- Isothermal  $\Delta T = 0$ 
  - $\circ \quad Q_{\Delta T=0} = T\Delta S = -W_{\Delta T=0} = -RT \ln \ln \left(\frac{V_2}{V_1}\right) = -RT \ln \ln \left(\frac{P_1}{P_2}\right)$
  - $\circ$   $\Delta U = 0$   $\Delta U_{IG} = f(T) \neq f(P, V)$  IG:  $P = \frac{nRT}{V}$  isotherms on PV graph
  - o Phase transitions are isothermal
- Isobaric  $\Delta P = 0$ 
  - $\circ \quad Q_{\Delta P=0} = \Delta H = C_P \Delta T \qquad \qquad W_{\Delta P=0} = P \Delta V = R \Delta T \qquad \qquad \Delta U = Q W = C_V \Delta T$
- **Isochoric**  $\Delta V = 0$ 
  - $\circ \quad Q_{\Delta V=0} = \Delta U = C_V \Delta T \qquad \qquad W_{PV,\Delta V=0} = 0 \qquad \qquad W_{isochoric,\Delta V=0} = \Delta U Q$
- Adiabatic Q = 0
  - $\circ$   $\Delta U = W = PdV = RdT$   $\Delta T = ???$
  - o Rapid processes are often idealized as adiabatic
  - Graphic adiabat = curve of constant entropy
- **Isentropic**  $\Delta S = 0$ 
  - $\circ \quad dU = C_V dT = P dV$

$$dH = C_P dT = V dP$$

- $\circ$  Compressors, Turbines, Pumps...  $\eta_{isentropic} = \frac{W_{actual}}{W_{ideal}} || \frac{W_{ideal}}{W_{actual}} = \frac{H_{2,s} H_1}{H_2 H_1}$ 
  - Either only  $W_{PV}$  (Reversible adiabatic  $\subset$  Isentropic)...
  - Or  $W_{PV} + W_{isochoric}$  and Q necessary to oppose  $W_{isochoric}$
- Isenthalpic  $\Delta H = 0$ 
  - o Irreversible adiabatic
  - o Throttling (<u>Joule-Thomson effect</u>)

• 
$$\mu_{JT} = (\frac{dT}{dP})_H = \frac{V}{CP}(\alpha T - 1)$$
  $\mu_{JT,ideal} = 0$ 

- $+\mu_{IT} \Rightarrow +\Delta T$ ,  $-\mu_{IT} \Rightarrow -\Delta T$ , divided by  $T_{inversion}$
- Polytropic  $PV^n = const$ 
  - $\circ$  Processes that can change all fundamental parameters T,P,V,S
  - $n=1 \Rightarrow \text{isothermal}$ o  $n=0 \Rightarrow$  isobaric
  - $n = \infty \Rightarrow isochoric$  $n = \gamma \implies$  isentropic/adiabatic
  - o  $1 < n < \gamma \Rightarrow$  heat and work in opposite directions
  - $\circ$   $\gamma < n < \infty \Rightarrow$  heat and work in same direction
- Systems
  - $\circ$  Open (m,Q,W)Closed (Q, W)
  - o <u>Isolated</u> () Equilibrium  $\Rightarrow S$  is maximized
    - Thermally Isolated (W) insulated, adiabatic
    - Mechanically Isolated (Q) rigid
- Changes

  - o Heating = heat addition = +Q = +T, +P, +V, +S o Cooling = heat rejection = -Q = -T, -P, -V, -S o Compression = volume increase = +W = +T, +P, -V, -S
  - o Expansion = volume reduction = -W = -T, -P, +V, +S

# Material Properties

#### • **Heat Capacity**

- o Measures relative temperature change in response to applied heat
- Measures capacity to store energy absorbed as heat (not conductivity)

$$\begin{array}{ll} \circ & C = \frac{dQ}{dT} [=] \frac{kg*m^2}{s^2*K} = \frac{J}{K} & C_V = (\frac{dQ}{dT})_V = (\frac{dU}{dT})_V = \frac{T}{N} (\frac{dS}{dT})_V & C_P = (\frac{dQ}{dT})_P = (\frac{dH}{dT})_P = \frac{T}{N} (\frac{dS}{dT})_P \\ \circ & C_P - C_V = VT \frac{\alpha^2}{\beta_T} & \text{Ideal } C_P - C_V = R & \frac{C_P}{C_V} = \gamma = \frac{\beta_T}{\beta_S} \end{array}$$

#### • Compressibility Coefficient

o Measures volume change in response to a pressure change

$$\beta_T = -\frac{1}{v} \left( \frac{dV}{dP} \right)_{T,N} = -\frac{1}{v} \frac{d^2 G}{dP^2}$$

$$\beta_S = -\frac{1}{v} \left( \frac{dV}{dP} \right)_{S,N} = -\frac{1}{v} \frac{d^2 H}{dP^2}$$

$$\beta_S = \beta_T - \frac{\alpha^2 T}{\rho C_P}$$

$$\beta_S = \gamma = \frac{C_P}{C_V}$$

$$\beta = \frac{m^2}{N} = Pa^{-1}$$

#### • Thermal Expansion Coefficient

o Measures volume change in response to a temperature change

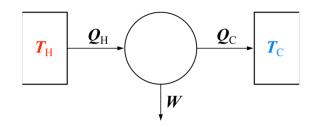
$$\circ \quad \alpha = \frac{1}{V} \left( \frac{dV}{dT} \right)_{P,N} = \frac{1}{V} \frac{d^2 G}{dP dT} = \alpha_V \qquad \qquad \alpha_L = \frac{1}{L} \left( \frac{dL}{dT} \right)_{P,N} \qquad \qquad \alpha_A = \frac{1}{A} \left( \frac{dA}{dT} \right)_{P,N} \qquad \qquad \alpha = \frac{1}{L} \left( \frac{dA}{dT} \right)_$$

## Thermodynamic Cycles

$$\Delta U_{cycle} = U_{1-2} + U_{2-3} + U_{3-4} + U_{4-1} = 0$$

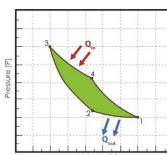
$$\begin{array}{lll} \mbox{Heat Engine} & = Q \Longrightarrow W = \eta = W/Q_H \\ \mbox{Heat Pump/Refrigerator} & = W \Longrightarrow Q = \eta = Q_C/W \end{array}$$

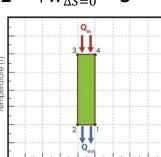
Heat Pump/Refrigerator = 
$$W \Rightarrow Q = \eta = Q_c/V$$



#### Carnot

$$\circ$$
 **1**  $+W_{\Delta T=0}$ 





$$\circ$$
 **1**  $+W_{\Delta T=0}$  **2**  $+W_{\Delta S=0}$  **3**  $-W_{\Delta T=0}$  **4**  $-W_{\Delta S=0}$  **5**

- o Theoretical ideal cycle
- Most efficient heat engine/pump

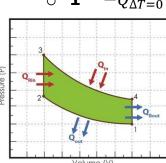
$$\circ \ W_{12,34} = RT_{1,3} \ ln \ ln \ \left(\frac{V_{2,4}}{V_{1,3}}\right) \quad W_{23,41} = C_V \Delta T_{23,41}$$

$$Q_{12,34} = -W_{12,34} Q_{23}$$

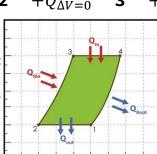
$$\begin{array}{ccc} \circ & Q_{12,34} = -W_{12,34} & Q_{23,41} = 0 \\ \circ & \eta = \frac{W_{expansion}}{Q_{heating}} = \frac{Q_{12} - Q_{34}}{Q_{12}} = 1 - \frac{T_C}{T_H} & \frac{V_1}{V_2} = \frac{V_4}{V_3} \end{array}$$

### **Sterling**

$$\circ$$
 **1**  $-Q_{\Delta T=0}$ 



$$\mathbf{2} + Q_{\Delta V=0}$$



$$+Q_{\Delta T=0}$$
 **4**  $-Q_{\Delta V=0}$   $\circlearrowleft$ 

- Ideal cycle
- o In practice stages overlap
- o Produces Simple Harmonic Motion

$$\circ W_{12,34} = RT_{1,3} \ln \ln \left( \frac{V_{2,4}}{V_{1,3}} \right) \quad W_{23,41} = 0$$

$$Q_{12,34} = -W_{12,34} Q_{23,41} = C_V \Delta T_{23,41}$$

$$Q_{12,34} = C_V \Delta T_{23,41}$$

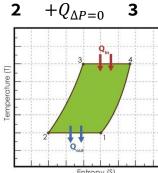
$$Q_{12,34} = C_V \Delta T_{23,41}$$

$$0 \quad \eta = 1 - T_1/T_2 = 1 - (V_2/V_1)^{\gamma - 1}$$

### **Ericsson**

Pressure (P)

$$+W_{\Delta T=0}$$



$$-W_{\Lambda T=0}$$

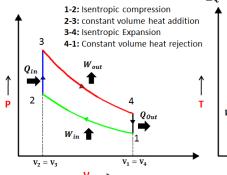
$$-W_{\Delta T=0}$$
 **4**  $-Q_{\Delta P=0}$   $\circlearrowleft$ 

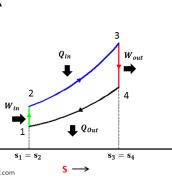
- o Ideal cycle (Ideal Brayton cycle)
- o <<<PV diagram: stage = shown 1</pre>

o 
$$W_{12,34} = RT_{1,3} \ln \ln \left( \frac{V_{2,4}}{V_{1,3}} \right)$$
  $W_{23,41} = P\Delta V = R\Delta T$ 

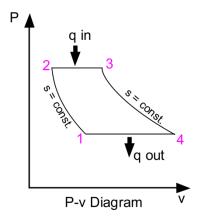
$$\begin{array}{ll} \circ & Q_{12,34} = -W_{12,34} & Q_{23,41} = C_P \Delta T_{23,41} \\ \circ & \eta = 1 - T_1/T_2 = 1 - (P_1/P_2)^{(\gamma-1)/\gamma} \\ \end{array}$$

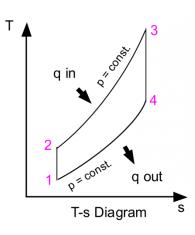
Regenerator = Heat exchanger that stores heat temporarily in thermal storage medium before transferring again. Recycles heat in a cycle <u>Intercooler</u> = cools working fluid between compression stages, decreasing the amount of work required and making compressor/pump more isothermal Reheater = reheats working fluid between expansion stages, increasing the amount of work output and making turbine more isothermal



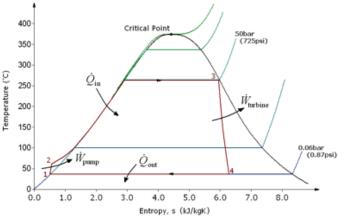


- Rankine (Q,P)
  - $\circ + W_{Q=0} + Q_{\Delta P=0} W_{Q=0} Q_{\Delta P=0} \qquad \eta = \frac{W_{turbine}}{Q_{boiler}}$
  - o Steam power plants, nuclear
  - $\circ$  Exploits phase change  $\Delta V$
  - o Pump, Boiler, Turbine, Condenser
  - o Alt: Superheat steam
- Brayton (Q,P)





- $-W_{\Delta S=0}$
- 4
- $-Q_{\Delta V=0}$  Exhaust
- O
- o Internal Combustion Engines
- o Automobile Engines
- $0 \quad \eta = 1 T_1/T_2 = 1 (V_2/V_1)^{\gamma 1}$

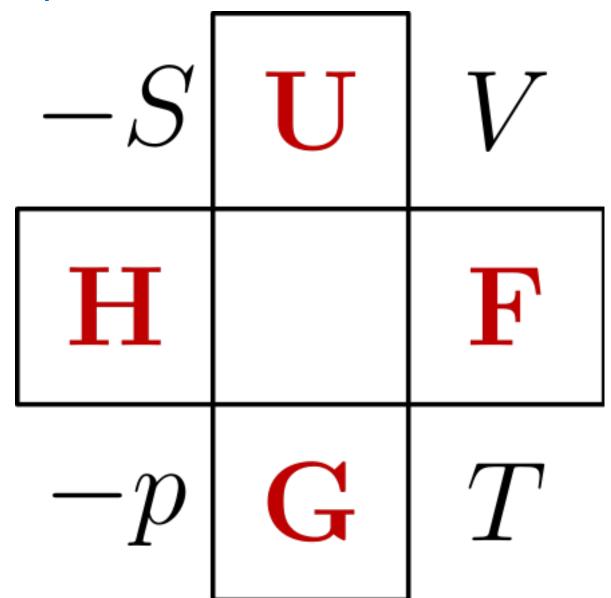


- $\circ \ \, +W_{Q=0} + Q_{\Delta P=0} W_{Q=0} Q_{\Delta P=0}$
- $\circ \ \eta = 1 T_1/T_2 = 1 (P_1/P_2)^{(\gamma 1)/\gamma}$
- $\circ$  Jet engines,  $\Delta P = 0$

## **Etymology**

- $(Latin) = calor \Rightarrow heat \Rightarrow caloric, calorie$
- $(Latin) = fugere \Rightarrow to flee \Rightarrow fugacity$
- $\varepsilon v \sim = en \sim \implies within, internal$ 
  - θάλπειν = thalpein ⇒ to heat ⇒ enthalpy
  - $\circ$   $"\epsilon \rho \gamma o \nu = ergon \implies work \implies energy"$
  - $\circ \quad \tau \rho o \pi \dot{\eta} = trope \Longrightarrow transform \Longrightarrow entropy$ 
    - $\pi o \lambda \breve{v} \varsigma = polus \Rightarrow many \Rightarrow polytropic$
- $"i\sigma o \sim = iso \sim \implies same"$ 
  - 0 θέρμη = therme  $\Rightarrow$  heat  $\Rightarrow$  isothermal
    - $\delta v \nu \alpha \mu \iota \sigma = dynamis \Rightarrow power, strength \Rightarrow thermodynamics$
  - $\circ$  βάρος = baros  $\Rightarrow$  weight  $\Rightarrow$  isobaric
  - $\circ \chi \tilde{\omega} \rho o \varsigma = choros \Rightarrow space \Rightarrow isochoric$
- $\dot{\alpha}\delta\iota\dot{\alpha}\beta\alpha\tau\circ\varsigma = adiabatos \Rightarrow impassable \Rightarrow adiabatic$ 
  - $\circ \quad \dot{\alpha} \sim = a \sim \implies not$
  - $\circ$  διάβατος = diabatos  $\Rightarrow$  passable
  - $\circ$  διά = dia  $\Longrightarrow$  through
  - ο βαῖνειν = bainein ⇒ to walk, go, come

### **Born Square**



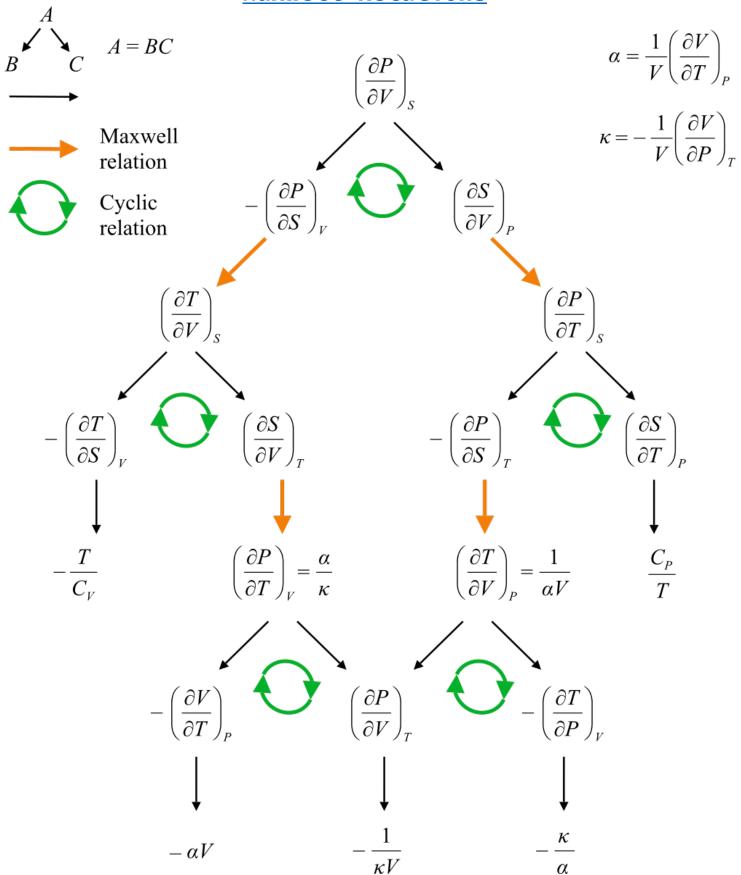
**Faces** = thermodynamic potentials, adjacent to natural variables (&N)  $U = f\{S, V\}$   $H = f\{S, P\}$   $G = f\{T, P\}$   $F = f\{T, V\}$ 

Cross corners = fundamental parameters/conjugate variables:  $(T,S)(P,V)(\mu,N)$ 

**U shapes** = Maxwell Relations ( $\Delta N=0$ ), beware -'s includes constant var Or differentiate potentials by natural variables (<u>Symmetry of 2nd Derivs</u>) Or use natural vars as denominator/constant, numerators = remaining, add negatives for U & G

$$-\frac{d^2F}{dTdV} = \left(\frac{dP}{dT}\right)_V = \left(\frac{dS}{dV}\right)_T \qquad \bullet \bullet \qquad \left(\frac{dS}{dP}\right)_T = -\left(\frac{dV}{dT}\right)_P = \frac{d^2G}{dTdP}$$
$$\frac{d^2H}{dSdP} = \left(\frac{dV}{dS}\right)_P = \left(\frac{dT}{dP}\right)_S \qquad \bullet \bullet \bullet \qquad \left(\frac{dT}{dV}\right)_S = -\left(\frac{dP}{dS}\right)_V = \frac{d^2U}{dSdV}$$

# **Maxwell Relations**



<sup>\*</sup>Information in this document is compiled from Wikipedia, which is often doubted for itself being a compilation of sources. However, as a source of scientific information that is very well established like in Thermodynamics, I consider it a reliable source.