

WEEK 10 - Python Application in Chemical Engineering

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Things you can do in python

- Process simulate
- Automation of chemical data analysis
- Chemical reaction and kinetic modelling
- Data mining
- Process control and monitoring

Linear Algebra 1

```
In [6]: # import libraries (https://docs.scipy.org/doc/scipy/reference/linalg.html)
import numpy as np
import scipy as sc
```

$$x + 3y + 5z = 10$$

$$2x + 5y + z = 8$$

$$2x + 3y + 8z = 3$$

$$\begin{bmatrix} 1 & 3 & 5 \\ 2 & 5 & 1 \\ 2 & 3 & 8 \end{bmatrix} \begin{bmatrix} x \\ y \\ z \end{bmatrix} = \begin{bmatrix} 10 \\ 8 \\ 3 \end{bmatrix}$$

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```
In [10]: # define the coefficient matrix A
a = np.array([[1, 3, 5], [2, 5, 1], [2, 3, 8]])
print(a)
```

[1 3 5]

[2 5 1]

[2 3 8]

```
In [12]: # Define the right hand side vector to b
b = np.array([10, 8, 3])
print(b)
```

[10]

[8]

[3]

```
In [16]: # Calculate the inverse of A and multiply by b to find out the solution further
c = sc.linalg.inv(a).dot(b)
print(c)
```

[-2.28]

[5.16]

[0.78]

```
In [18]: # solve function to find the solution
d = sc.linalg.solve(a, b)
print(d)
```

[-2.28]

[5.16]

[0.78]

Linear Algebra Execution

```
In [23]: a = np.array([[1, 2], [1, 2]])
print(a)
```

[1 2]

[1 2]

```
In [37]: b = np.array([1, 0])
print(b)
```

[1]

[0]

```
In [39]: # solve function to find the solution
d = sc.linalg.solve(a, b) # longer version but dont need to import for every little function
print(d)
```

[-0.5]

[-0.25]

```
In [47]: solution = solve(a, b)
solution
```

```
Out[47]: array([-0.5 ,
 [-0.25])
```

```
In [43]: # ways to resolve
from scipy.linalg import solve
```

```
solution = solve(a, b) # shorter function but need to import for every little function available in library
solution
```

```
Out[45]: array([-0.5 ,
 [-0.25]))
```

Solving ODE using Runge-Kutta method

The Runge–Kutta method [edit]

The most widely known member of the Runge–Kutta family is generally referred to as "RK4", the "classic Runge–Kutta method" or simply as "the Runge–Kutta method".

Let an initial value problem be specified as follows:

$$\frac{dy}{dt} = f(t, y), \quad y(t_0) = y_0.$$

Here y is an unknown function (scalar or vector) of time t , which we would like to approximate; we are told that

$\frac{dy}{dt}$, the rate at which y changes, is a function of t and of y itself. At the initial time t_0 the corresponding y value is y_0 . The function f and the initial conditions t_0, y_0 are given.

Now pick a step-size $h > 0$ and define

$$y_{n+1} = y_n + \frac{1}{6}h(k_1 + 2k_2 + 2k_3 + k_4),$$

$$t_{n+1} = t_n + h$$

for $n = 0, 1, 2, 3, \dots$ using^[2]

$$k_1 = f(t_n, y_n),$$

$$k_2 = f\left(t_n + \frac{h}{2}, y_n + \frac{h}{2}k_1\right),$$

$$k_3 = f\left(t_n + \frac{h}{2}, y_n + \frac{h}{2}k_2\right),$$

$$k_4 = f(t_n + h, y_n + hk_3).$$

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differential eq: $dy/dx = (x-y)/2$ given: $x_0, y_0, h(\text{step size})$

```
In [81]: # def differential equation
def dydx(x, y):
    return ((x-y)/2)
```

```
In [91]: def rungeKutta(x0, y0, x, h):
    n = int((x-x0)/h)
    y = y0
    for i in range(1, n+1):
        k1 = h * dydx(x0, y)
        k2 = h * dydx(x0 + 0.5*h, y+0.5*k1)
        k3 = h * dydx(x0 + 0.5*h, y+0.5*k2)
        k4 = h * dydx(x0 + h, y+k3)
        # update value of y
        y = y + (1/6)*(k1 + 2*k2 + 2*k3 + k4)
        # update value of x
        x0 = x0 + h
    return y
```

```
In [93]: # driver method
x0 = 0
y0 = 1
x = 5
h = 0.2
print("The value of y at x is:", rungeKutta(x0, y0, x, h))
```

The value of y at x is: 3.246794758464962

Pressure profile in vessel (simulation)

Mass balance in the vessel:

$$\frac{dn}{dt} = \dot{n}_{in} - \dot{n}_{out}$$

$$PV = nRT$$

$$\frac{d(PV)}{dt} = \dot{n}_{in} - \dot{n}_{out}$$

$$\frac{V}{RT} \frac{dP}{dt} = \dot{n}_{in} - \dot{n}_{out}$$

$$\frac{dP}{dt} = \frac{\dot{n}_{in} - \dot{n}_{out}}{\frac{V}{RT}}$$

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$$\frac{dP}{dt} = \frac{\dot{n}_{in} - \dot{n}_{out}}{\frac{V}{RT}}$$

System Pressure Profile for total Volume of 1154 m^3

Pressure Increases

Original Pressure

System Pressure Profile for total Volume of (V) m^3

Time (min)

Pressure (kPa)

Time (min)