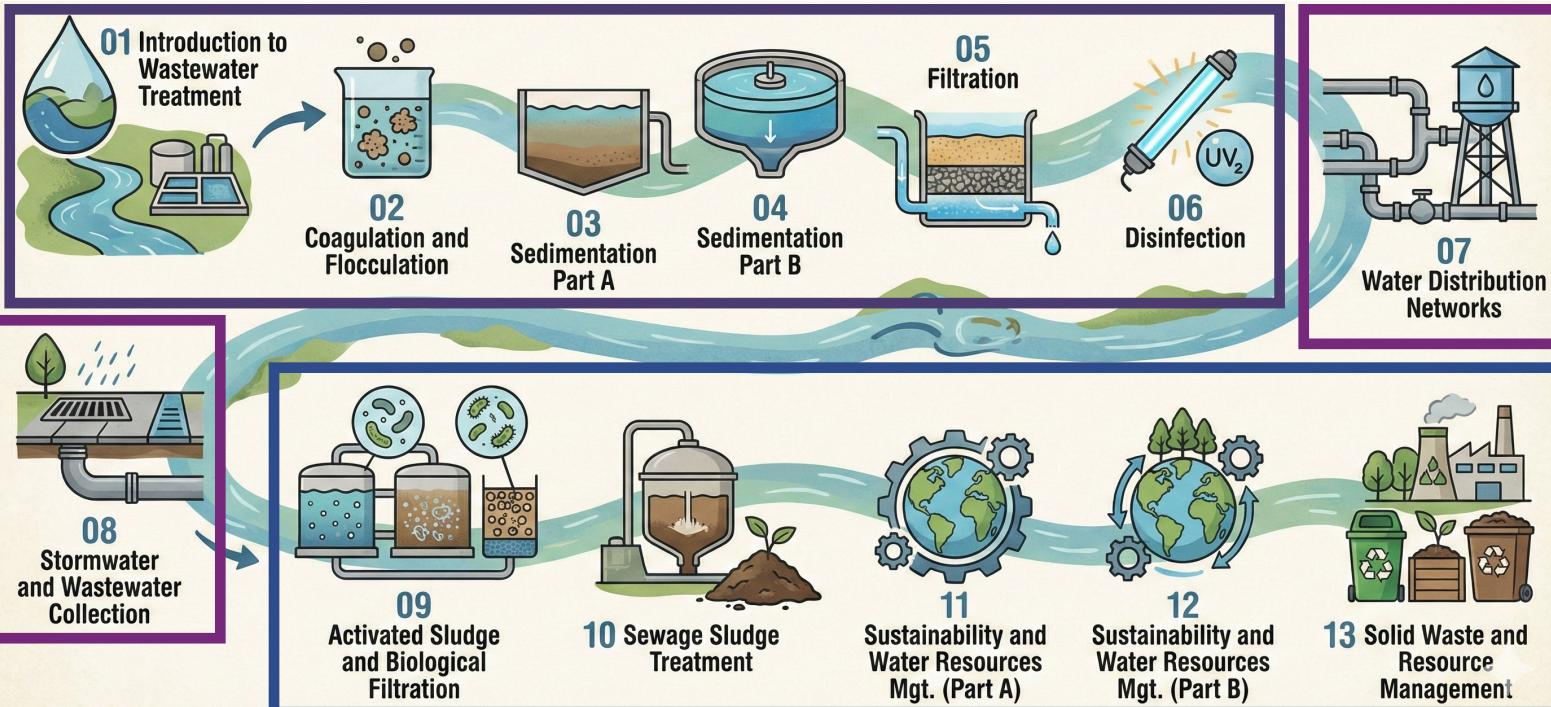


Table of Content



(L1 - L6: Traditional Water Treatment Process, L7 - L8: Water Distribution Network Management, L9 - L13: Post Treatment Phase)

NOTE THAT THIS NOTE IS ENTIRELY GENERATED BY AI, WITH LOTS OF MODIFICATION BY MYSELF, CORRECTING ERROR AND HALLUCINATIONS. HOWEVER I CANT GUARANTEE IT IS PERFECT AND THERE MIGHT BE SOME ERROR HIDDEN, AND I WOULD DEFINITELY APPRECIATE ANY REPORTS OF ERROR IF YOU CAN FIND ONE. THANKS.

Lecture 1: Introduction to Wastewater Treatment

FOUNDATIONAL CONCEPTS: SOLIDS & ORGANICS

UNDERSTANDING THE SOLIDS MATRIX

All Solids = Suspended + Dissolved
 TS = TSS + TDS
 VS = VSS + VDS
 FS = FSS + FDS

T : Total
 S : Solids or Suspended
 D : Dissolved
 V : Volatile
 F : Fixed

CALCULATION GUIDE 1: SOLIDS ANALYSIS

EXAMPLE PROBLEM WALKTHROUGH (BASED ON A 100 mL (0.1 L) SAMPLE)

EMPTY DISH	DISH + DRY SOLIDS	DISH + ASH
81.923 g	82.015 g (TS)	81.975 g (FS)
EMPTY DISH MASS: 81.923 g	DISH + DRY SOLIDS (AT 105°C): 82.015 g	DISH + ASH (AT 550°C):

CALCULATION GUIDE 2: BOD ANALYSIS

BASIC BOD FORMULA

$$BOD_5 = \frac{D_1 - D_2}{P}$$

D₁: Initial Dissolved Oxygen (DO)
 D₂: Final DO
 P: Dilution Factor

BOD KINETICS FORMULA

$$L_t = L_u(1 - 10^{-kt})$$

L_t: BOD at time t (days)
 L_u: Ultimate BOD
 k: Reaction rate constant

TOTAL SOLIDS (TS)

All material remaining after evaporating water from a sample at 105°C.

TOTAL SUSPENDED SOLIDS (TSS)

Solids large enough to be trapped by a standard 1µm filter.

TOTAL DISSOLVED SOLIDS (TDS)

Solids small enough to pass through the filter.

VOLATILE SOLIDS (VS)

The organic portion of solids, which burns off during ignition at 550°C.

FIXED SOLIDS (FS)

The inorganic ash or sand that remains after ignition at 550°C.

1. CALCULATE TOTAL SOLIDS (TS) CONCENTRATION

$$\text{Mass} = 82.015 - 81.923 = 0.092 \text{ g (92 mg).}$$

$$\text{Concentration} = \frac{92 \text{ mg}}{0.1 \text{ L}} = 920 \text{ mg/L}$$

2. CALCULATE VOLATILE SOLIDS (VS) CONCENTRATION

$$\text{Mass Lost} = 82.015 - 81.975 = 0.040 \text{ g (40 mg).}$$

$$\text{Concentration} = \frac{40 \text{ mg}}{0.1 \text{ L}} = 400 \text{ mg/L}$$

3. CALCULATE FIXED SOLIDS (FS) CONCENTRATION

$$FS = TS - VS.$$

Or you can straightaway calculate "Dish + Ash" - "Dish"

$$\text{Concentration} = 920 - 400 = 520 \text{ mg/L}$$

EXAMPLE PROBLEM WALKTHROUGH

5 mL WASTEWATER SAMPLE ADDED TO 300 mL BOTTLE INITIAL DO = 8.4 mg/L FINAL DO = 3.7 mg/L k = 0.1 d⁻¹

1. CALCULATE DILUTION FACTOR (P)

$$P = \frac{\text{Volume of Wastewater}}{\text{Total Volume}} = \frac{5 \text{ mL}}{300 \text{ mL}} = 0.0167$$

2. CALCULATE BOD₅

$$\frac{8.4 - 3.7}{0.0167} = 282 \text{ mg/L}$$

3. CALCULATE ULTIMATE BOD (L_u)

$$L_u = \frac{282}{1 - 10^{-0.1 \times 5}} = \frac{282}{1 - 10^{-0.145}} = 412 \text{ mg/L}$$

4. CALCULATE 20-DAY BOD (L₂₀)

$$L_{20} = L_u(1 - 10^{-kt}) = 412 * (1 - 10^{-(0.1 \times 20)}) = 408 \text{ mg/L}$$

BOD vs. COD: MEASURING ORGANIC CONTENT

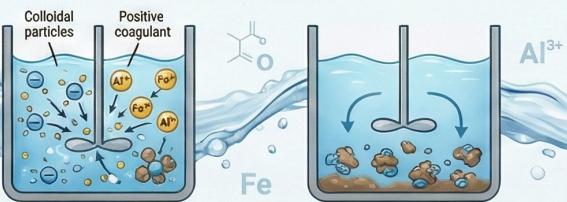
BIOCHEMICAL OXYGEN DEMAND (BOD)
 Measures the oxygen consumed by microorganisms to biologically degrade organic matter
 BOD₅: Measure over 5 days
 BOD₂₀: Total demand (estimated)

CHEMICAL OXYGEN DEMAND (COD)
 Measures the oxygen equivalent to chemically oxidise organic matter using a strong chemical agent, takes only a few hours.

KEY FINDING: ASSESS TREATABILITY WITH THE BOD/COD RATIO
 If BOD₅/COD > 0.5, the wastewater is considered easily biodegradable and suitable for biological treatment.

Lecture 2: Coagulation and Flocculation

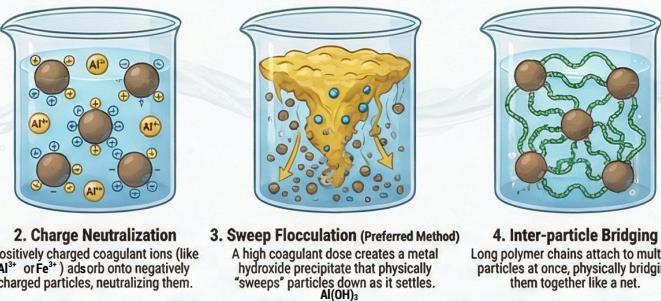
The Two-Step Process: Coagulation vs. Flocculation



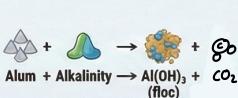
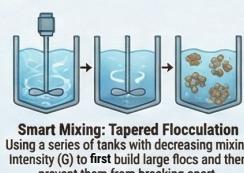
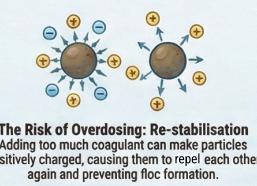
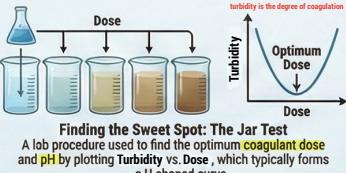
Coagulation: Destabilize Particles
The addition of chemicals (coagulants) under fast mixing conditions to neutralize the charge of colloidal particles. (colloidal particles are usually negatively charged)

Flocculation: Build Flocs
A slow mixing process that causes destabilized particles to collide and form larger, settleable aggregates called "floc".

The 4 Mechanisms of Coagulation (Exam Favorite)



Practical Application & Key Concepts



The Chemistry of Coagulation
Coagulants like Alum consume the water's natural alkalinity and produce CO_2 . Insufficient alkalinity causes pH to drop, stopping the process.



When to Use Ferric Chloride
For water with high pH or high alkalinity, Ferric Chloride is often preferred over Alum because it works effectively over a wider pH range.

Exam Calculation 1: Alkalinity Consumption

Problem: 30 mg/L of Alum (Molar Mass 600) is added to water with 100 mg/L of Alkalinity (Molar Mass 100). 1 mole of Alum consumes 3 moles of Alkalinity. Find the final alkalinity.

$$\begin{aligned} \text{Step 1: Convert Alum Dose to Moles/L} \\ 30 \text{ mg/L} \\ \frac{30}{600,000 \text{ mg/mol}} \\ = 0.00005 \text{ mol/L of Alum.} \end{aligned}$$



$$\begin{aligned} \text{Step 2: Calculate Alkalinity Consumed (Moles)} \\ 0.00005 \text{ mol/L Alum} \times 3 \\ = 0.00015 \text{ mol/L of Alkalinity consumed.} \end{aligned}$$



$$\begin{aligned} \text{Step 3: Convert Consumed Alkalinity to mg/L} \\ 0.00015 \text{ mol/L} \times 100,000 \text{ mg/mol} \\ = 15 \text{ mg/L of Alkalinity consumed.} \end{aligned}$$

$$\begin{aligned} \text{Step 4: Final Alkalinity} \\ \text{Initial (100 mg/L)} - \text{Consumed (15 mg/L)} \\ = 85 \text{ mg/L remaining.} \end{aligned}$$

if initial < 15 mg/L
→ floc wouldn't form
→ add lime / soda ash.

Exam Calculation 2: Velocity Gradient (G)

Problem: Calculate G for a tank ($V=1600 \text{ m}^3$) with a power input of 1080 W and water viscosity of $1.002 \times 10^{-3} \text{ kg/m}\cdot\text{s}$. Flow($Q=80 \text{ m}^3/\text{d}$)

The Velocity Gradient (G) Equation

$$G = \sqrt{\frac{P}{\rho V}}$$

G is mixing intensity, P is power, ρ is viscosity, and V is tank volume. A typical range for G is 20-70 s^{-1} .

$$G = \sqrt{\frac{P}{\rho V}} = \sqrt{\frac{1080}{1.002 \times 10^{-3} \times 1600}} \approx 25 \text{ s}^{-1}$$

To find Gt, first find retention time, t :

$$Q = \frac{V}{t} \Rightarrow t = \frac{V}{Q} = \frac{1600}{12885} = 12.885 \text{ days}$$

$$Gt = 25 \times 12.885 = 320 \text{ (Typical } Gt = 10^4 \text{ to } 10^5\text{)}$$

Pro Tip: Exam Variation

Solving for Tank Dimensions
Some questions give you the optimal G (from a graph) and ask you to calculate a required tank dimension, like Depth.

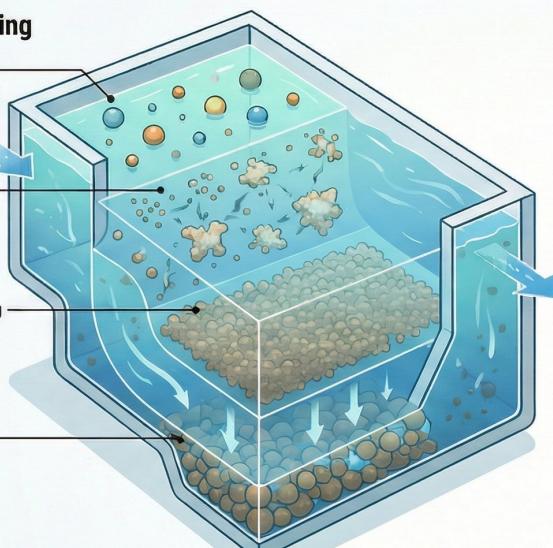
How to Solve:

1. Read optimal G from the provided graph.
2. Rearrange the formula to solve for Volume: $G^2 \cdot \rho \cdot V = Q \Rightarrow V = \frac{Q}{G^2 \cdot \rho}$
3. Calculate V, then find the missing dimension e.g., Depth = V / (Length \times Width)

Lecture 3: Sedimentation Part A - Discrete Settling

The 4 Types of Settling

Type I: Discrete Settling
Individual particles settle independently without interacting. Their size, shape, and density remain constant.
(Example: Grit removal)



Type II: Flocculent Settling
Particles collide and aggregate (flock) as they settle, increasing in size and settling faster with depth.
(Example: Alum or Iron floc)

Type III: Hindered (Zone) Settling
Particle concentration is high, causing them to hinder (block) each other and settle as a unified "blanket" with clear water above.
(Example: Sludge thickening)

Type IV: Compression Settling
Concentration is so high that particles are in physical contact. Settling occurs as the weight of the particles squeezes water out.
(Example: Bottom of a sludge tank)

Key Concepts & Formulas for Ideal Settling

(covered next chapter)



Surface Overflow Rate (v_o)
This is the critical design parameter representing the upward velocity of water. It is calculated as

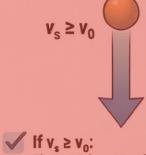
$$v_o = \frac{\text{Flow Rate (Q)}}{\text{Surface Area (A)}}$$

Stokes' Law (for Settling Velocity, v_s)

$$v_s = \frac{g(S-1)d^2}{18\nu}$$

g = Gravity (9.81 m/s^2)
S = Specific Gravity of particle
d = Particle Diameter (in meters)
 ν = Kinematic Viscosity of water (m^2/s)
→ If given dynamic viscosity, μ :
 $v_s = \frac{g(S-1)d^2}{18\mu}$

The Removal Rule

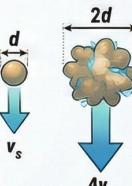


If $v_s \geq v_o$:
The particle settles faster than the upward velocity.
Result: 100% Removal.

Double the Size, Settle 4x Faster

Velocity is Proportional to Diameter Squared ($v_s \propto d^2$). This relationship from Stokes' Law is the key. Coagulation combines small particles into larger flocs, significantly increasing diameter (d). Because of the squared relationship, a small increase in particle diameter leads to a massive increase in settling velocity, making treatment much more efficient.

Theory Explained: Why Coagulation Works



Double the Size, Settle 4x Faster
Because of the squared relationship, a small increase in particle diameter leads to a massive increase in settling velocity, making treatment much more efficient.

Exam Problem Walkthrough: Calculating Settling Distance

- Convert All Units to SI
- Calculate Settling Velocity (v_s)

Ensure all measurements are in meters (m) and seconds (s). (Example: 0.2 mm becomes 0.2 $\times 10^{-3}$ m; 10 minutes becomes 600 s).

- CRUCIAL CHECK - Reynolds Number
- Stokes' Law is only valid for laminar flow ($Re < 1$). You must check this for full marks.

Formula: $Re = (v_s \cdot d) / \nu$.

(Example: $Re = 0.67$, which is < 1, so the law is valid).

- Calculate Distance Settled
- Use the simple formula: Distance = Velocity \times Time.

(Example: $0.00282 \text{ m/s} \times 600 \text{ s} = 2.29 \text{ meters}$).

Question: How far would a discrete spherical particle of diameter 0.2 mm and specific gravity 1.2 settle in 10 minutes? Water temp is 15°C (Kinematic viscosity $\nu = 1.14 \times 10^{-6} \text{ m}^2/\text{s}$).

Advanced Exam Method: Total Removal Calculation

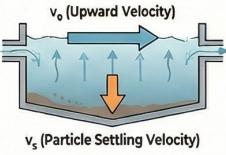
- Calculate v_s for Each Particle Size
- Compare Each v_s to the Tank's v_o
- Calculate Removal for Each Fraction
- Calculate Total Removal

Sum the removals:
Total = $\sum (\text{mass fractions for removed particles}) + \sum (\text{mass fraction of partially removed particle} \times [v_s / v_o] \times 100)$.

(covered next chapter)

Lecture 4: Sedimentation Part B - Analysis and Design

CORE CONCEPTS & TANK DESIGNS



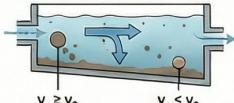
What is Surface Overflow Rate (SOR or v_o)

The "speed limit" for settling. Particles must settle faster than the upward velocity of the water (v_o) to be effectively removed.

Calculated as Flow Rate (Q) / Surface Area (A).

Horizontal Flow vs. Upflow Clarifiers

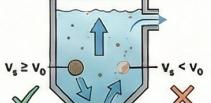
Horizontal Flow



100% Removal
 Partial Removal ($v_s/v_o \times 100\%$ removed)

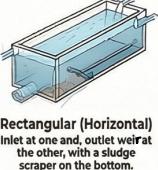
Horizontal flow tanks are more efficient because they can partially remove slow-settling particles.

Upflow Clarifier



100% Removal
 ZERO Removal
ZERO removal if $v_s < v_o$, as slow particles are carried out with the upward flow.

Common Tank Types



Rectangular (Horizontal)
Inlet at one end, outlet weir at the other, with a sludge scraper on the bottom.

Radial (Circular)
Central inlet, water flows outwards to weirs on the edge, with a rotating bridge scraper.

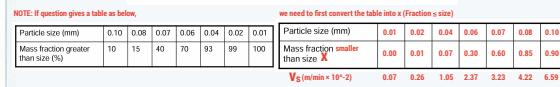
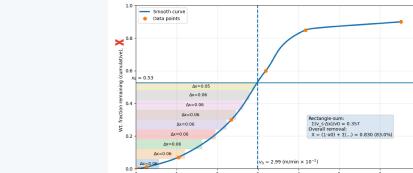
Upflow (Hopper Bottom)
Funnel shaped tank where water enters low and flows up, with sludge collecting in the pointed bottom.

HOW TO CALCULATE TOTAL REMOVAL (GRAPHICAL METHOD)

The Master Equation for Total Removal (X)

$$\text{Total Removal} = \left(\frac{\text{Removal of Fast Particles}}{\text{Fast Particles}} \right) + \left(\frac{\text{Partial Removal of Slow Particles}}{\text{Slow Particles}} \right)$$

$$\text{Formula: } X = (1 - x_0) + \int_0^{x_0} \frac{v_s}{v_o} dx; \text{ or } X = (1 - x_0) + \sum \frac{\Delta x \cdot v_{s,\text{avg}}}{v_o}$$



NOTE: If question gives a table as below,

Particle size (mm)	0.10	0.08	0.07	0.06	0.04	0.02	0.01
Mass fraction greater than size (%)	10	15	40	70	93	99	100
Particle size (mm)	0.01	0.02	0.04	0.06	0.07	0.08	0.10
Mass fraction smaller than size (%)	0.00	0.01	0.07	0.30	0.60	0.85	0.90
V_s (m/min x 10^-2)	0.07	0.26	1.05	2.37	3.23	4.22	6.59

we need to first convert the table into a (Fraction \leq size)

Particle size (mm)	0.10	0.08	0.07	0.06	0.04	0.02	0.01
Mass fraction greater than size (%)	10	15	40	70	93	99	100
Particle size (mm)	0.01	0.02	0.04	0.06	0.07	0.08	0.10
Mass fraction smaller than size (%)	0.00	0.01	0.07	0.30	0.60	0.85	0.90
V_s (m/min x 10^-2)	0.07	0.26	1.05	2.37	3.23	4.22	6.59

Step 1: (you will need to find v_o , first, and check Re)

Plot the SOR Curve. Using data from the settling velocity test, plot the fraction of particles remaining, x on the y-axis against their settling velocity, v_s , on the x-axis.

Step 3:
Calculate Removal of Fast Particles:
This is the fraction of particles with a settling velocity greater than v_o . The formula is simply $(1 - x_0)$.

Step 4:
Calculate Partial Removal of Slow Particles: This is represented by the area under the curve to the left of the v_o line. Approximate this by summing the areas of small rectangular strips under the curve.

Step 2:
Read off Cut-off Fraction (v_o): Draw a vertical line from the tank's design overflow rate (v_o) on the x-axis up to your curve. The y-value at this intersection is x_0 .

Step 5:
Find the Total Removal Efficiency (X): Add the results from Step 3 add step 4 to get the total removal efficiency.

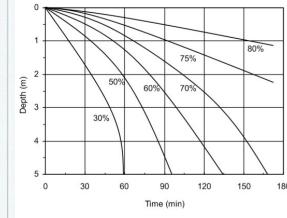
Example Result: For a design v_o of 43 m/d, the calculation yielded: 0.47 (fast particles) + 0.36 (slow particles) = 0.83, or 83% Total Removal.

HOW TO CALCULATE TOTAL REMOVAL (ISO-REMOVAL CURVES)

Understanding Iso-Removal Curves

This is an alternative data format showing contour lines of equal removal percentage on a grid of tank depth vs. time.

example of an Iso-removal Curve:



sometimes in exam it gives in the form of a table:

Time (min)	Depth (m)
50-60%	2.25
60-70%	1.35
70-75%	0.80
75-80%	0.60

(detention time = 60 min)

this table basically gives the value of all curves at t=60 min

Step 1:
Determine Key Parameters: You will need the tank's total depth (D) and the detention time (t), which is calculated as Tank Volume / Flow Rate. ($t = \frac{V}{Q} = \frac{D \cdot A}{Q}$)

Step 2:
Find the Base Removal (r_n): On the graph, find your detention time (t). The value of the iso-removal curve that intersects the bottom of the tank (depth D) at that time is your r_n . ($t = D \cdot \frac{1}{Q}$)

Step 3:
Add Partial Removal Fractions:
For each iso-removal curve above r_n , add a fraction of its removal contribution. This is calculated for each slice between curves (e.g., between the 50% and 60% lines). Formula:

$$R_{\text{total}} = r_n + \sum \left[\frac{\text{Depth}_{\text{mean}}}{D} \cdot (r_n - r_{n-1}) \right]$$

In words: Add the base removal (r_n) to the sum of each additional removal percentage (e.g., 60%-50%) multiplied by the ratio of its average depth to the total tank depth.

this section might have been removed from syllabus (not examined ~2016)

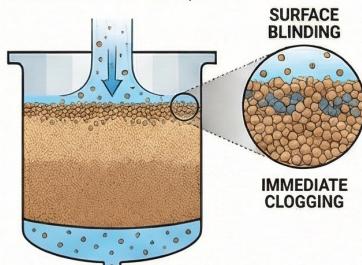
Lecture 5: Filtration

CORE FILTRATION CONCEPTS (EXAM THEORY)

THE DUAL MEDIA ADVANTAGE: WHY ANTHRACITE OVER SAND?

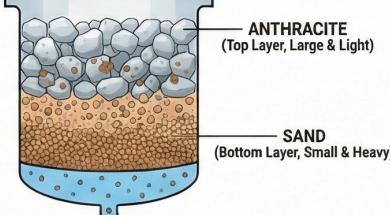
PROBLEM: SINGLE SAND FILTER

After backwashing, small sand grains settle at the top, causing immediate clogging, short filter runs, and inefficient use of the filter bed depth.



SOLUTION: DUAL MEDIA FILTER

A top layer of large, light Anthracite traps coarse particles, while a bottom layer of small, heavy Sand traps fine particles. The density difference ensures the layers automatically re-stratify correctly after every backwash. Allows for TRUE DEPTH FILTRATION.



THE HEADLOSS CALCULATION (A STEP-BY-STEP GUIDE)

THE FAIR-HATCH EQUATION

$$h_L = \frac{36kv(1-e)^2LV}{ge^3\phi^2} \times \sum \left(\frac{P_i}{d_i^2} \right)$$

KEY VARIABLES TO KNOW

- h_L : Headloss (m)
- k : Kozemey constant (~5)
- v : Kinematic viscosity (m^2/s)
- e : Porosity (e.g., 0.45)
- V : Filtration Velocity (m/h)
- g : Gravity (9.81 m/s^2)
- ϕ : Shape factor (~0.8)
- P_i : Mass fraction
- d_i : Geometric mean diameter (m)

watch out! usually given in m/h . Have to convert yourself!

STEP 1: PERFORM THE SIEVE ANALYSIS CALCULATION

Size Range (mm)	P_i (mass %)	Geometric Mean d_i (m)	Term: $P_i/d_i^2 (\text{m}^{-2})$
3.36 - 2.38	0.02	2.828 x 10 ⁻³	2,501
2.38 - 1.68	0.06	1.999 x 10 ⁻³	15,006
1.68 - 1.19	0.12	1.414 x 10 ⁻³	60,024
1.19 - 0.84	0.40	0.999 x 10 ⁻³	400,160
0.84 - 0.59	0.20	0.704 x 10 ⁻³	403,551
0.59 - 0.42	0.12	0.497 x 10 ⁻³	484,261
0.42 - 0.297	0.08	0.353 x 10 ⁻³	641,234
0.297 - 0.210	0.00	-	0
SUM	1.00	$\Sigma = 2.0068 \times 10^6$	

Convert sieve data into the summation term.
Engine of the calculation.
Convert diameters to meters.

Example question:
Size of opening (mm) % Mass retained
2.38 0
1.68 6
1.19 12
0.84 50
0.59 20
0.42 12
0.297 8
0.210 0

2.38 opening means 3.36-2.38
there is 2% mass

to find geometric mean,
 $d_g = \sqrt{\frac{3.36 \times 2.38}{2}}$
 $= 2.928 \text{ mm}$
 $= 2.928 \times 10^{-3} \text{ m}$

STEP 2: WATCH YOUR UNITS!

Most common mistake: Velocity.
Convert from m/hour to m/s .

$$5 \text{ m/h} \div 3600 \text{ s/h} = 0.001389 \text{ m/s}$$

STEP 3: PLUG IN VALUES AND SOLVE

$$h_L = \frac{36(5)(1.004 \times 10^{-6})(1 - 0.45)^2(0.001389)}{(9.81)(0.45)^3(0.8)^2} \times (2.0068 \times 10^6)$$

Substitute known values, including constants, porosity, velocity, bed depth ($L = 0.7 \text{ m}$), and the summation from the table.

$$\text{FINAL RESULT } 0.191 \text{ m}$$

*Tip: If you get a huge or tiny number, double-check your unit conversions, especially for diameter (mm to m).

ADVANCED CONCEPT: CONNECTING EQUATIONS

HEADLOSS (h_L) → BERNoulli's EQUATION

How Headloss Relates to Bernoulli's Equation: The headloss (h_L) in the Carman-Kozeny/Fair-Hatch is the "Losses" term in Bernoulli's energy equation. It quantifies the pressure drop caused by friction as water flows through the filter media.

$$\text{Bernoulli's eqn.: } P_i + \frac{1}{2} \rho u_i^2 + \rho gh_i = P_f + \frac{1}{2} \rho u_f^2 + \rho gh_f + h_L$$

Fair-Hatch's eqn.

CHOOSING YOUR DISINFECTANT: THE BIG 4

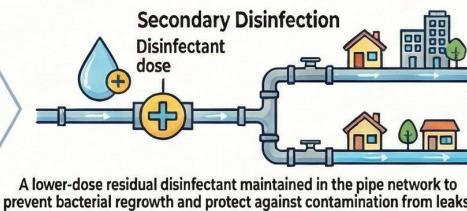
Lecture 6: Disinfection

CORE DISINFECTION PRINCIPLES

Primary Disinfection

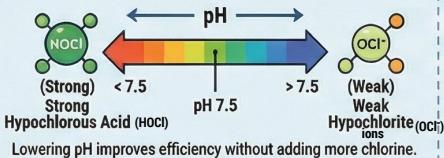


Secondary Disinfection

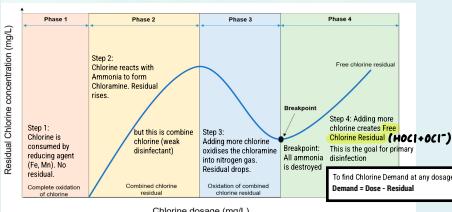


THE SCIENCE OF CHLORINE

The pH Effect: Lower pH = Stronger Disinfection



Breakpoint Chlorination



Disinfectant	Pros	Cons
Chlorine	<ul style="list-style-type: none"> Cheap effective for bacteria/viruses provides a protective residual 	<ul style="list-style-type: none"> Forms harmful by-products (THMs) pH-dependent ineffective against Cryptosporidium
Chlorine Dioxide	<ul style="list-style-type: none"> Does not react with Ammonia Much stronger than Chlorine. No strong disinfection dependence on pH. Taste and odour control Does not form THMs (unless excess chlorine present) 	<ul style="list-style-type: none"> Generation need to be well controlled to minimise excess free chlorine Must be generated on sites (unstable) Costs more than Chlorine
Ozone	<ul style="list-style-type: none"> Very strong kills Cryptosporidium improves taste and odor does not form halogenated byproducts (e.g. THMs) 	<ul style="list-style-type: none"> Expensive complex to generate leaves NO residual can form Bromate by-product
UV Light	<ul style="list-style-type: none"> Kills Cryptosporidium & Giardia no chemical by-products (no THMs) competitive costs 	<ul style="list-style-type: none"> Leaves NO residual requires clear water (low turbidity) lamps can foul no taste control doesn't remove colour

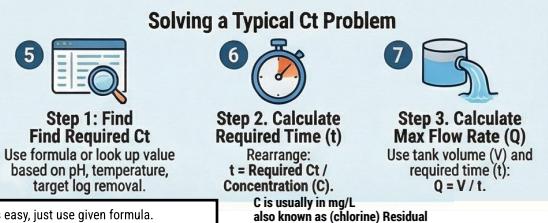
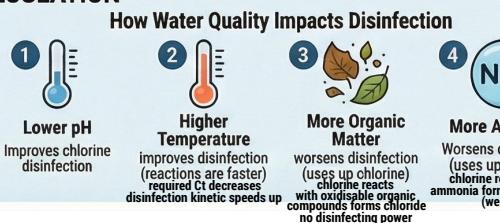
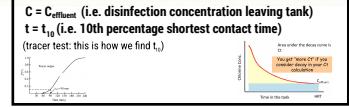
THE "Ct" CONCEPT: THE CORE CALCULATION

The Golden Rule of Disinfection

$$Ct_{(\text{calculated})} \geq Ct_{(\text{required})}$$

What is Ct?

Product of disinfectant Concentration (C, in mg/L) and effective contact time (t, in minutes), measuring overall disinfection power.



Lecture 7: Water Distribution Network

1. District Metered Areas (DMAs): The Most Common Question

How a "Single Feed DMA" Works



Main Purpose: Quantifying Leakage

DMAs are used to calculate the Net Night Flow (NNF), which helps isolate and measure water loss in a specific zone.

$$\text{Leakage} = \text{Total inflow} - \text{Legitimate night consumption}$$

Pros vs. Cons of DMAs

- | | |
|--|--|
| Pros <ul style="list-style-type: none"> Detects bursts quickly by monitoring night flow. Allows for targeted pressure management. | Cons <ul style="list-style-type: none"> If the inlet pipe fails, the entire area loses its water supply. Water Quality Risk: Closed valves create "dead ends," leading to water stagnation and sedimentation. |
|--|--|

What is a DMA?

A discrete, permanently hydraulically isolated area of a water network, typically serving 1000–3000 properties.

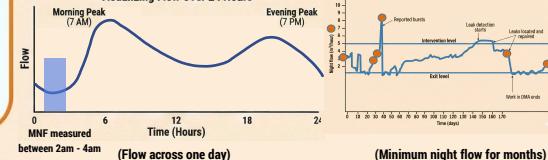


2. Minimum Night Flow (MNF): Finding Hidden Leaks

The Golden Hours for Leak Detection are 2 AM - 4 AM

During this period, legitimate customer water consumption is at its lowest and most stable, making flow from leaks much easier to identify.

Visualizing Flow Over 24 Hours



3. Pressure Management: Reducing Stress on the System

The FAVOUR Equation: Linking Leakage to Pressure

The relationship is defined as:

$$Q_{\text{leak}} \propto P^{N_1}$$

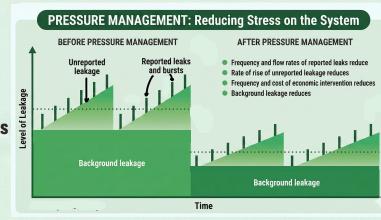
where N_1 is usually greater than 1, meaning a small pressure drop causes a large leakage reduction.

Lower Pressure = Lower Leakage & Fewer Bursts

Reducing and stabilizing pressure has multiple direct benefits for the network's health and efficiency.

Top 3 Benefits of Pressure Control

- Reduces background leakage.
- Lowers burst frequency by preventing surges (water hammer). Keeping pressure stable (calm)
- Extends the life of pipes and assets.



4. TOTEX & Risk: The Modern Approach to Pipe Renewal

What is TOTEX?

(building new things) Total Expenditure (TOTEX) = Capital Expenditure (CAPEX) + Operational Expenditure (OPEX). This holistic view considers the whole-life cost of an asset.

Strategy Shift: Replace Risky Pipes, Not Old Pipes

Modern asset management prioritizes pipes based on their risk profile rather than simply their age.

The Risk Calculation:
 $\text{Risk} = \text{Probability of Failure} \times \text{Consequence of Failure}$

5-Step Risk-Based Renewal Process

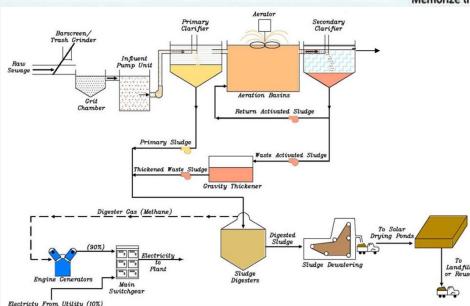


Lecture 8: Stormwater and Wastewater Collection

A visual summary of key definitions, formulas, and step-by-step calculation methods for high-probability exam questions.

The Wastewater Treatment Plant (WWTP) Process Flow

A High-Probability Exam Question
Memorize the stages and their functions.



1. A bar screen is a mechanical filter for large objects removal, such as rags, plastics etc. (Pre-treatment)
 2. A grit chambers are basins to remove the inorganic particles to prevent damage to the pumps, and to prevent their accumulation in sludge digesters. (Pre-treatment)
 3. A primary clarification objective is suspended solids (SS) removal from wastewater under gravity. The removal of particulate, suspended solids and floatable materials elimination is intended. (Primary Treatment)
 4. An aeration tank uses microbes to remove soluble matter convert it to biomass and stabilise compounds. (Secondary Treatment) **Activated Sludge**
 5. A key performance indicator to determine if treatment is effective so that the supernatant meets an effluent discharge standard. (Secondary Treatment) **Effluent Treatment**
 6. A gravity thickener is to reduce water content in the secondary sludge. (Sludge Treatment)
 7. An anaerobic digester is to convert organic biomass into biogas (mainly methane and CO₂) for energy recovery. (Sludge Treatment)
 8. A sludge dewatering system is to separate sludge into liquid ("the centre") and solid components for waste minimization. (Sludge Treatment)
 9. (There is no tertiary treatment here e.g. filtration / nutrient removal (N, P) / disinfection / polishing.)
1. Primary Treatment: The objective is to remove large solids and suspended particles through sedimentation, producing sludge.
 2. Secondary Treatment: The goal is to biologically degrade dissolved and suspended organic matter using microorganisms, further reducing the organic load.
 3. Tertiary Treatment: This stage aims to remove any remaining impurities, including nutrients, and to disinfect the effluent before it is discharged into the environment.

Core Concepts & Definitions



Dry Weather Flow (DWF)
The average daily flow in a sewer during seven consecutive days without rain.

Formula:

$$DWF = PG + I + E$$

P = Population
G = Domestic consumption per person (L/head/day)
I = Infiltration (groundwater leaking into pipes)
E = Trade Effluent (industrial waste)



Combined Sewer Overflow (CSO)
A safety valve in older sewer systems that combines rainwater and sewage in one pipe

CSO Role 1: Hydraulic Protection

Prevent flooding at the WWTP by diverting excess flow during heavy rain into river/seas



CSO Role 2: Environmental Protection
Design to retain as much solid/pollutant as possible (first flush) and only spill diluted water

What is the "First Flush"?
The highly polluted initial surge of stormwater that washes accumulated dirt from surfaces and must be captured for treatment

CSO setting (i.e. Retained flow Qs)
Other excess flow get discharged
traditional setting: Qo = 6+DWF
formula A setting: Qo = DWF + 1360P + 2E

The Two Key Calculation Methods

Method 1: Foul Sewer Design (Wastewater)

Used to calculate the peak wastewater flow to size the sewer pipe correctly.

Step 1: Calculate Average DWF

Use the formula $DWF = (P \times G) + I + E$ convert the final value from L/day to L/s by dividing by $24 \times 60 \times 60$ (86,400)

Step 3: Calculate Peak Flow

Multiply the DWF by a Peak Factor, often calculated using Babbitt's Formula

$$\text{Peak Factor} = 5 \left(\frac{P}{10^4} \right)^{0.2} \quad \text{Factor} = \frac{a}{b}$$

Babbitt's Formula Alert!
In this formula, the Population P must be in thousands. For 50,000 people, use $P=50$.

Method 2: Storm Sewer Design (The Rational Method)

A common method used to calculate the peak stormwater runoff

Step 1: Apply the Rational Formula

$$Q = 2.78 \cdot C \cdot i \cdot A$$

where Q is flow (L/s)



C = Runoff coefficient
(0.0 to 0.1, 0.7 to 0.9
for urban)

i = Rainfall intensity
(mm/hr)

A = Area (hectares)

2.78 is a unit conversion constant

Step 2: Find Rainfall Intensity (I)

I is found using a given formula

$$I = \frac{a}{D+b} \quad \begin{aligned} a &= \text{rainfall intensity (mm/hr)} \\ b &= \text{duration (hrs)} \\ &\quad \text{a/b = constant} \end{aligned}$$

Step 3: Find Duration (D)

Duration is the same as the Time of Concentration (t_c), calculated as

$$t_c = \frac{L}{V} + \frac{t_f}{2} \quad \begin{aligned} L &= \text{length of the pipe (m)} \\ V &= \text{flow rate (m/s)} \\ t_f &= \text{time of entry (s) + time of flow (s)} \\ &\quad \text{t_f = time for all the runoff to run off the pipe} \\ &\quad \text{t_f = time for all the runoff to travel through the pipe} \\ &\quad \text{(length / velocity)} \end{aligned}$$

Worked Exam Problems

Problem 1: Foul Sewer Peak Flow Calculation

Problem: For a population of 37,500, calculate the DWF and then the Peak Flow.

Solution:

1. Calculate DWF: Sum domestic, infiltration, and industrial flows. $DWF = (P \times G) + I + E$
Total = 7,250,000 L/day.
2. Convert DWF: $7,250,000 / 86,400 = 83.9 \text{ L/s}$.
3. Find Peak Factor: $P = 37.5$ (in thousands).
 $\text{Factor} = 5 / (2 \times 10^4) = 3.42$.
4. Calculate Peak Flow: $83.9 \text{ L/s} \times 3.42 = 203 \text{ L/s}$.

(Problem 1 is about how big sewage flow is)

Problem 2: CSO Setting Calculation

Problem: Determine the flow at which a CSO spills using Formula A for a population of 50,000.

Solution:

1. Calculate DWF: 80,000 people = $250 \text{ L/head/day} = 12,500,000 \text{ L/day}$.
2. Apply Formula A:
Setting = $DWF + 1360P + 2E$
 $= 12,500,000 + (1360 \times 50,000) + (2 \times 0)$
 $= 80,500,000 \text{ L/day}$
3. Convert to L/s: $80,500,000 / 86,400 = 932 \text{ L/s}$.

(Problem 2 is about how much combined flow is retained before the excess is spilled)

Problem 3: Storm Sewer Network (Rational Method)

Pipe number	Length (m)	Contributing area (ha)	Time of concentration (min)	Runoff coefficient, Q	Peak capacity, Q (L/s)
1	240	0.8	8.5	0.1	186.1
2	180	0.6	5.5	0.5	75.9
3	120	0.4	4.0	0.8	59.8
4	180	1.0	4	5	39.5
5	120	0.6	3.5	0.5	27.5
6	120	0.6	1	11	35.7

(Problem 3 is about how big stormwater flow is)

Lecture 9: Activated Sludge and Biological Filtration

Two Core Processes: A Head-to-Head Comparison

ACTIVATED SLUDGE (AS)

Activated sludge is a secondary wastewater treatment process in which sewage is settled in a tank to maintain suspended microorganisms that biologically remove organic matter.
Activated Sludge returns to "Retained Activated Sludge".
- to ensure enough bacteria are present to treat incoming wastewater
some sludge remains as "Waste Activated Sludge".
- to prevent over accumulation of sludge

TRICKLING FILTER (TF)

Trickling filter is a secondary wastewater treatment process in which sewage flows over a bed of media supporting attached microorganisms that biologically degrade organic matter.
(Exam draw)
Trickling filters have the following components:
1. a headworks and pump station
2. a bed of randomly packed solid media
3. an underdrain system or wastewater collection
4. an air system to move media and provide oxygen
5. a system for separating the detached biomass (sludge) from treated effluent
all get removed
no "Retained Activated Sludge"

- Suspended Growth (bacteria float freely)
 - High Power (aeration pumps)
 - Complex Operation (requires monitoring)
 - Small Footprint (compact)
 - Common Issues: Sludge Bulking (poor settling)
- Attached Growth (biofilm on media)
 - Low Power (gravity, natural ventilation)
 - Simple Operation
 - Large Footprint (significant space)
 - Common Issues: Flies, odors, filter clogging

Walkthrough 1: Activated Sludge Design Problem

Goal: Find MLSS concentration (X) and Daily Sludge Production (P_x)

Given: Flow=5,000 m³/d, Influent BOD=250 mg/l, F/M=0.3, HRT=6 hours, Sludge Age=6 days

Step 1: Critical Unit Conversions

$Q = 5,000 \text{ m}^3/\text{d}$
 $S_0 = 250 \text{ mg/L}$
 $\theta = 0.25 \text{ days (HRT)}$

Step 2: Calculate Tank Volume (V)

$V = Q \times \theta$

$5,000 \times 0.25 = 1,250 \text{ m}^3$

Step 3: Calculate MLSS (X)

$$\text{Rearrange F/M: } X = \frac{Q \cdot S_0}{V \cdot F/M}$$

$$X = \frac{5,000 \cdot 250}{1,250 \cdot 0.3} = 3,333 \text{ mg/L}$$

Step 4: Calculate Daily Sludge Production (P_x)

$$\text{Rearrange Sludge Age: } P_x = \frac{V \cdot X}{\theta} = \frac{1,250 \cdot 3.333}{6} = 694 \text{ kg/day}$$

Key Performance Indicators & Definitions

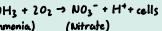
SLUDGE VOLUME INDEX (SVI)

Measures volume (ml) of 1 gram of sludge after 30 min settling. Indicates settling quality.

$$\text{SVI} = \frac{Settled Volume (ml)}{\text{MLSS (mg/L)}} \times 1000$$

$50-150 \text{ mL/g}: \text{Good Settling}$
 $>150 \text{ mL/g}: \text{Sludge Bulking (poor settling)}$

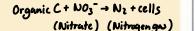
NITRIFICATION



(Ammonia) (Nitrate) (cells)

Requires Oxygen. (Aerobic)

DENITRIFICATION



(Nitrate) (Nitrogen gas) (cells)

Requires no oxygen (Anoxic)
needs carbon source.

The Activated Sludge "Holy Trinity": Essential Formulas

1. F/M RATIO (Food-to-Microorganism)

Daily food (BOD) supplied to microorganisms (MLSS). Typical range: $0.2 - 0.5 \text{ kg BOD/kg MLSS-d}$.

$$F/M = \frac{Q \cdot S_0}{V \cdot X}$$

$$Q = \text{Flow rate (m}^3/\text{d})$$

$$S_0 = \text{Influent BOD (mg/L or g/m}^3)$$

$$V = \text{Tank Volume (m}^3)$$

$$X = \text{MLSS (mg/L or g/m}^3)$$

2. HYDRAULIC RETENTION TIME (HRT or θ)

Average length of time wastewater stays in the aeration tank.

$$\theta = \frac{V}{Q}$$

$$V = \text{Tank Volume (m}^3)$$

$$Q = \text{Flow rate (m}^3/\text{d})$$

3. SLUDGE AGE (SRT or θ_c)

Average time a microorganism stays in the system before removal.

$$\theta_c = \frac{V \cdot X}{P_x}$$

$$V = \text{Tank Volume (m}^3)$$

$$X = \text{MLSS (mg/L or g/m}^3)$$

$$P_x = \text{Sludge Production Rate (kg/d)}$$

$$(P_x = Q_u \cdot X_u)$$

Walkthrough 2: Trickling Filter Loading Problem

Goal: Calculate Organic & Hydraulic Loading Rates (DLR & HLR) and check criteria.

Given: Flow=3.2 MI/d, BOD=200 mg/l, Two filters (42m diameter, 2m depth)

Step 1: Calculate Total Area and Volume

Total Surface Area = $2 * (\pi * (42/2)^2) = 2,770.8 \text{ m}^2$

Total Volume = Total Area * Depth = $2,770.8 * 2 = 5,541.6 \text{ m}^3$

Step 2: Calculate Organic Loading Rate (OLR)

$$\text{OLR} = \frac{\text{Total BOD Load}}{\text{Total Volume}}$$

$$\text{OLR} = \frac{3.2 * 10^3 * 200 * 10^{-3}}{5,541.6} = 0.115 \text{ kg BOD/m}^3\text{-d}$$

Loading rate:
Organic = Q_u / V
Hydraulic = Q / A_s

$0.06 - 0.12 \text{ kg BOD/m}^3\text{-d}$
 $0.25 - 1.2 \text{ m}^3/\text{m}^2\text{-d}$

Step 3: Calculate Hydraulic Loading Rate (HLR)

$$\text{HLR} = \frac{\text{Total Flow}}{\text{Total Surface Area}}$$

$$\text{HLR} = \frac{3,200}{2,770.8} = 1.15 \text{ m}^3/\text{m}^2\text{-d}$$

Step 4: Check Results Against Criteria

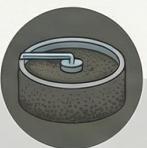
OLR (0.115) within 0.06-0.12 range: OK

HLR (1.15) within 0.25-1.2 range: OK

Lecture 10: Sewage Sludge Treatment

Key Concepts & Theory

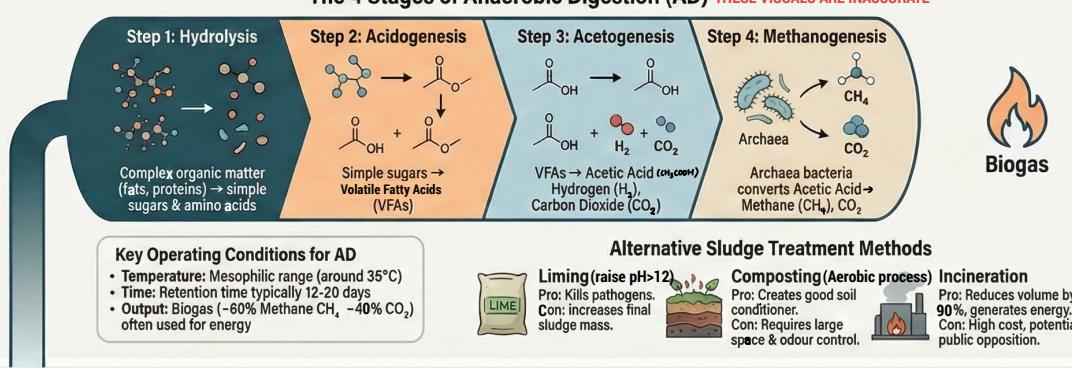
Primary vs. Secondary Sludge



Primary Sludge
(From Primary Settlement)
Granular, grey, odorous,
higher solid content (~4-6%)
Contains inorganic solids (grit)
and settleable organics.



Secondary Sludge
(From Secondary Clarifier)
Light, flocculent, brown,
mostly biomass, lower
solid content (~0.5-2%)



Calculation 1: Sludge Production Walkthrough (How much sludge is produced?)

Key Formulas: Mass & Volume

$$\begin{aligned}\text{Primary Mass } (M_{ps}) &= \epsilon \times SS_{in} \times Q \\ \text{Secondary Mass } (M_{ss}) &= Y_{obs} \times BOD_{removed} \times Q \\ \text{Sludge Volume } (V_{sludge}) &= \frac{\text{Mass of Dry Solids}}{\text{density of Sludge}} \times \% \text{ Dry Solids}\end{aligned}$$

Example Problem: Daily Sludge Volume

A WWTP treats 10,000 m³/d of wastewater.
Influent SS = 300 mg/L
Influent BOD = 250 mg/L
Primary Tank: Removes 60% of SS and 35% of BOD.
Primary sludge is 9% Dry Solids (DS).
Secondary tank: Removes 95% of remaining BOD.
VSS (K_{ds}) = 0.44 kg SS / kg BOD. Secondary sludge is 0.9% DS.
Calculate Total Daily Sludge Volume (m³/d) produced.

$$\begin{aligned}\text{Step 1: Calculate Primary Sludge Mass } (M_{ps}) & 0.6 \times (0.3 \text{ kg/m}^3) \times (10,000 \text{ m}^3/\text{d}) \\ & = 1,800 \text{ kg/day}\end{aligned}$$

$$\begin{aligned}\text{Step 2: Calculate Primary Sludge Volume } (V_{ps}) & \frac{1,800}{1000 \times 0.008} \\ & = 36 \text{ m}^3/\text{day}\end{aligned}$$

$$\begin{aligned}\text{Step 3: Calculate BOD removed in secondary treatment} & \text{Initial BOD (250 mg/L)} \\ & \cdot 1 - 0.6 = 0.4 \text{ removes 35\%} \\ & \text{BOD after primary (250} \times 0.65 = 162.5 \text{ mg/L}) \\ & \cdot \text{secondary treatment removes another 95\%} \\ & \text{BOD removed in secondary treatment} \\ & = 0.95 \times 162.5 = 154.4 \text{ mg/L} = 0.1544 \text{ kg/m}^3\end{aligned}$$

$$\begin{aligned}\text{Step 3: Calculate Secondary Sludge Mass } (M_{ss}) & 0.4 \times (0.1544 \text{ kg/m}^3) \times (10,000 \text{ m}^3/\text{d}) \\ & = 617.6 \text{ kg/day}\end{aligned}$$

$$\begin{aligned}\text{Step 4: Calculate Secondary Sludge Volume } (V_{ss}) & \frac{617.6}{1000 \times 0.008} \\ & = 77.2 \text{ m}^3/\text{day}\end{aligned}$$

$$\begin{aligned}\text{Step 5: Calculate Total Daily Volume} & 36 \text{ m}^3/\text{day} + 77.2 \text{ m}^3/\text{day} \\ & = 113.2 \text{ m}^3/\text{day}\end{aligned}$$

Calculation 2: Lab Solids Analysis Walkthrough

Key Formulas: Lab Analysis

$$\begin{aligned}\text{Total Solids (TS)} &= \frac{\text{Mass Dried @ 105°C} - \text{Mass Dish}}{\text{Sample Volume}} \\ \text{Volatile Solids (VS)} &= \frac{\text{Mass Dried @ 105°C} - \text{Mass Burnt @ 500°C}}{\text{Sample Volume}}$$

Example Problem: Solids Concentration

For a 100 mL sample:

- Dish = 81.923 g
- Dish + Dry Solids = 82.015 g
- Dish + Ash = 81.975 g

Step 1: Calculate Total Solids (TS) Concentration

$$\begin{aligned}\text{Mass of Dry Solids} &= 82.015 \text{ g} - 81.923 \text{ g} = 0.092 \text{ g (92 mg)} \\ TS &= \frac{92 \text{ mg}}{0.1 \text{ L}} = 920 \text{ mg/L}\end{aligned}$$

Step 2: Calculate Volatile Solids (VS) Concentration

$$\begin{aligned}\text{Mass of Volatiles (lost on ignition)} &= 82.015 \text{ g} - 81.975 \text{ g} = 0.040 \text{ g (40 mg)} \\ VS &= \frac{40 \text{ mg}}{0.1 \text{ L}} = 400 \text{ mg/L}\end{aligned}$$

$$\begin{aligned}\text{Step 3: Calculate Fixed Solids (Ash)} & 75 - VS = 920 \text{ mg/L} - 400 \text{ mg/L} = 520 \text{ mg/L}\end{aligned}$$

(covered in chapter 1)

Lecture 11: Sustainability and Water Resource Management Part A

1. The Life Cycle Assessment (LCA) Framework



Life Cycle Assessment (LCA)

A methodology (ISO 14040/14044) for assessing the environmental impacts associated with all stages of a product's life.

Phase 1: Goal & Scope

Define the purpose, the functional unit (e.g., "Treatment of 1 m³ of wastewater"), and the system boundaries.

Phase 2: Inventory Analysis (LCI)

Collect data on all inputs (energy, materials) and outputs (emissions, waste) for the system.

Phase 3: Impact Assessment (LCIA)

Convert the inventory data into potential environmental impacts, such as converting methane to CO_2 equivalents.

Phase 4: Interpretation

Identify significant issues ("hotspots"), draw conclusions, and make recommendations for improvement.

Essential LCA Vocabulary

- Functional Unit: The reference unit for comparison (e.g., Treatment of 1 m³ of wastewater).
- System Boundaries: Defines the scope, from "Cradle-to-Graue" or "Cradle-to-Gate".
- Hotspot: The stage or process with the largest environmental impact.

2. The Calculation: Carbon Footprint Formula



Carbon Footprint (Global Warming Potential - GWP)

A measure of the total greenhouse gas emissions caused by an activity, expressed as a single unit: kg CO_2 equivalents (kg CO_2e).

$$\text{Total GWP} = \sum (\text{Mass of Emission} \times \text{Characterisation Factor})$$

This formula converts different greenhouse gases into a common unit based on their global warming potential relative to CO_2 .

Greenhouse Gas	IPCC Characterisation Factor
CO_2	1
CH_4	~28
N_2O	~265

3. Walkthrough: Calculating a WWTP's Carbon Footprint



EXAMPLE SCENARIO: A WWTP treats 50,000 m³/day of wastewater. We will calculate its total annual carbon footprint and specific footprint per cubic meter of water treated.



Step 1: Calculate Scope 1 (Direct Emissions)

Convert all direct gas emissions from the plant into CO_2 equivalents.

$$\begin{aligned}\text{CO}_2: 1,200,000 \text{ kg} \times 1 &= 1,200,000 \text{ kg CO}_2\text{e} \\ \text{CH}_4: 8,000 \text{ kg} \times 27.2 &= 217,600 \text{ kg CO}_2\text{e} \\ \text{N}_2\text{O}: 1,200 \text{ kg} \times 273 &= 327,600 \text{ kg CO}_2\text{e}\end{aligned}$$

$$\text{Total Scope 1} = 1,745,200 \text{ kg CO}_2\text{e/year}$$



Step 2: Calculate Scope 2 (Indirect Energy Emissions)

Multiply energy consumption by grid emission factors to find the associated carbon footprint.

$$\text{Electricity: } 12,000,000 \text{ kWh} \times 0.233 = 2,796,000 \text{ kg CO}_2\text{e}$$

$$\text{Natural Gas: } 500,000 \text{ kWh} \times 0.184 = 92,000 \text{ kg CO}_2\text{e}$$

$$\text{Total Scope 2} = 2,888,000 \text{ kg CO}_2\text{e/year}$$



Step 3: Calculate Total Carbon Footprint

Add Scope 1 and Scope 2 emissions together for the final annual total.

$$1,745,200 + 2,888,000 = 4,633,200 \text{ kg CO}_2\text{e/year}$$



Step 4: Calculate Specific Footprint

Divide the total footprint by the annual volume of treated water to get the footprint per functional unit (1 m³).

$$\text{Total Annual Flow} = 50,000 \text{ m}^3/\text{day} \times 365 \text{ days}$$

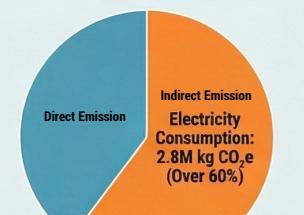
$$= 18,250,000 \text{ m}^3/\text{year}$$

$$\frac{4,633,200 \text{ kg CO}_2\text{e}}{18,250,000 \text{ m}^3} = 0.254 \text{ kg CO}_2\text{e/m}^3$$

$$0.254 \text{ kg CO}_2\text{e/m}^3$$

4. Interpretation: Identify the Hotspot & Suggest Improvements

Hotspot Identified: Electricity Consumption



Solution A: Decarbonise Power
Install on-site renewable energy like solar panels or switch to a green electricity tariff from the provider.

Solution B: Improve Energy Efficiency
Implement measures like replacing old, inefficient pumps and optimising the aeration control systems.

Solution C: Generate Your Own Energy
Install an Anaerobic Digester to convert sludge into biogas, which can be used to generate electricity and heat (CHP).

Lecture 12: Sustainability and Water Resource Management Part B

THE CORE THEORY:
TWO CYCLES OF THE CIRCULAR ECONOMY

BIOLOGICAL CYCLE:
Material that can biodegrade and safely return to earth.

TECHNICAL CYCLE:
Product can be used rather than consumed. Focus on how each step allow material to remain in use.

KEY RESOURCE RECOVERY TECHNOLOGIES

- Carbon: Biogas (via Anaerobic Digestion)
- Phosphorus: Struvite Precipitation (creates fertilizer)
- Nitrogen: Ammonia Stripping
- Water: Membrane Filtration (for water reuse)

Problem Walkthrough: Closing Mass Balance

A WWTP treats 12,000 m³/d. You are given inlet loads, some outlet data, emission factors, and biogas data. You need to close the mass balance (complete the table) and calculate recovery rates. Which resource has the greatest potential for improvement, and what technology could be used?

	Inlet	Wastewater	Outlet
Water	10,000	9,990	9,975
Nitrogen	0	0	0
Phosphorus	0.95	0.95	0.95
Carbon (CO ₂)	2.6	2.6	2.6
	(100%)	(99.9%)	(99.8%)

Gas Streamflow, Dissolved Gases, and Emissions

	Gas Streamflow	Dissolved Gases	Emissions
Water	1,000	0	0
Phosphorus	0.05	0.05	0.05
Carbon	0.05	0.05	0.05
Nitrogen	1.0	1.0	1.0
Biogas	0.4	0.4	0.4
Carbon (CO ₂)	0.5135	0.5135	0.5135
Nitrogen (NO)	0.065	0.065	0.065
Nitrogen (NO ₂)	0.01	0.01	0.01
Phosphorus (PO ₄)	0.005	0.005	0.005
Carbon (CO ₂)	0.691	0.691	0.691
Water	0	0	0
Phosphorus	0	0	0
Carbon	0	0	0

Step 1: Calculate Fugitive Gas Emissions

Calculate the mass of Carbon and Nitrogen lost to the atmosphere as leaks.

- Methane (CH₄):**
 - Total Mass CH₄ = 0.0075 × 7.1 (COD load) = **0.05325 t/d.**
 - Carbon Fraction in CH₄; 12/(12 + 4) = 0.75.
 - CO₂ Mass: 0.05325 × 0.75 = **0.040 t/d.**
- Nitrous Oxide (NO_x):**
 - Total Mass NO_x = 0.02 × 1.0 (N load) = **0.02 t/d.**
 - Nitrogen Fraction in NO_x; (2 × 14)/(2 × 14 + 16) = 28/44 = 0.636.
 - NO_x Mass: 0.02 × 0.636 = **0.0127 t/d.**

Step 2: Calculate Biogas Composition

Calculate the mass of Carbon recovered in the Biogas stream.

- Methane (CH₄):**
 - Volume = 1.565 × 0.65 = 1,017.25 m³.
 - Mass = 1,017.25 × 0.66 (density) = 671.4 kg = **0.671 t/d.**
 - Carbon Fraction in CH₄; 12/(12 + 4) = 0.75.
 - Carbon Mass: 0.671 × 0.75 = **0.503 t/d.**
- Carbon Dioxide (CO₂):**
 - Volume = 1.565 × 0.35 = 547.75 m³.
 - Mass = 547.75 × 1.98 (density) = 1,084.5 kg = **1.085 t/d.**
 - Carbon Fraction in CO₂; 12/(12 + 32) = 0.275.
 - Carbon Mass: 1,085 × 0.275 = **0.296 t/d.**

Step 3: Calculate Mass Balance (The "Fill the Gap" Step)

Use the previous input + Sum(Outputs). We are solving for the unknown Biosolids.

- Water Balance:**
 - Biosolids_{water} = In - (Effluent + Solid Waste)
 - Biosolids_{water} = 12,000 - (11,990 + 1.0) = **9 m³/d**
- Nitrogen Balance:**
 - Biosolids_N = In - (Effluent + Gas N_x + Fugitive N₂O)
 - Biosolids_N = 1.0 - (0.05 + 0.65 + 0.0127)
 - Biosolids_N = 1.0 - 0.7127 = **0.287 t/d**
- Phosphorus Balance:**
 - Biosolids_P = In - (Effluent)
 - Biosolids_P = 0.15 - 0.01 = **0.14 t/d**
- Carbon Balance:**
 - Biosolids_C = In - (Effluent + Solid Waste + Gas CO₂ + Fugitive CH₄ + Biogas C)
 - Biosolids_C = 2.5 - (0.05 + 0.35 + 0.4 + 0.90 + 0.799)
 - Biosolids_C = 2.5 - 1.639 = **0.861 t/d**
 - Biosolids_C = 2.5 - 1.639 = **0.861 t/d**

Step 4: Calculate Recovery Rates

Treat Biosolids and Biogas as "Recovered Products". Treat Effluent and Emissions as "Losses".

- Water Recovery:**
 - Biosolids Water = $\frac{9}{12,000} = 0.075\%$
 - Total Input = 12,000
 - (Not all effluent is discharged to sea, not reused).
- Carbon Recovery:**
 - Recovered = Biosolids C + Biogas C = 0.861 + 0.799 = 1.66 t/d
 - Ratio = $\frac{1.66}{12,000} = 66.4\%$
- Nitrogen Recovery:**
 - Recovered = Biosolids N = 0.287 t/d
 - Ratio = $\frac{0.287}{1.0} = 28.7\%$
- Phosphorus Recovery:**
 - Recovered = Biosolids P = 0.14 t/d
 - Ratio = $\frac{0.14}{0.15} = 93.3\%$

Step 5: Interpretation & Improvement Strategy

This is the final part of the exam question (usually worth 2-4 marks).

Question: Which resource has the greatest potential for improvement, and what technology could be used?

- Identify the Weakness:**
 - CO₂ has the lowest rates: P (93%), C (68%), N (29%), Water (0.075%).
 - Water is the highest priority for improvement (it is currently treated as waste).
- Suggest Technology:**
 - To turn the effluent (currently "waste") into a "product", we need **Tertiary Treatment**.
 - Combination: Add Ultrafiltration (UF) and Reverse Osmosis (RO) followed by UV disinfection.
- Suggest Use Case:**
 - This treated water can be used for **non-potable applications**: Irrigation (agriculture/parks), Industrial process water, or toilet flushing.

Lecture 13: Solid Waste and Resource Management

Municipal Solid Waste (MSW)
Waste from households plus similar waste from commercial or institutional sources that is collected by the municipality.

End-of-Waste Status
The point at which waste undergoes a recovery operation and is officially considered a product, not waste.

The Main Calculation: Infrastructure Planning

4-Step Logic for Planning

This process determines how many new facilities (e.g., Energy from Waste plants) are needed to meet future waste diversion targets.

Example Calculation (2035 Target)

Step	Calculation	Result
1. Future Waste (2035)	$15,000,000 \text{ tpa} \times (1 + 0.01)^{10}$	16,569,000 tpa
2. Target Mass (60%)	16,569,000 tpa × 0.60	9,941,400 tpa
3. Number of Plants	9,941,400 tpa / 400,000 tpa/plant	25 Plants (Rounded Up)
4. Total Energy	25 Plants × 25 MW/plant	625 MW

Foundational Concepts

The Waste Hierarchy (Must Be Memorized in Order)

Solid Recovered Fuel (SRF)
A fuel produced by shredding and dehydrating solid waste, commonly used in energy-intensive industries like cement kiln

Plastic Pollution Terms

Calculating the 'True' Recycling Rate

Collection Rate vs. True Rate

The initial amount collected for recycling is not what's actually recycled. True rates must account for losses.

Step 1: Account for Sorting Rejects
Initial Collection (e.g., 100 tonnes)

Step 2: Account for Reprocessing Loss
From the sorted material, subtract contamination and other rejects at the sorting facility.
Example: 100 tonnes collected × (1 - 0.20 reject rate) = 80 tonnes.
Example: 80 tonnes × (1 - 0.10 process loss) = 72 tonnes.

Final Net Recycling Rate: 72%
The final mass (72) divided by the initial mass (100) gives the true rate, which is much lower than a misleading 100% "collection rate".